

# Varmefördi - Damsblad 3

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\* 0.7

$$m = 1,3 \text{ kg}, \quad V_1 = 7,5 \text{ m}^3, \quad P = 180 \text{ kPa}$$

$$R_{\text{helium}} = 2,077 \frac{\text{kJ}}{\text{kg} \cdot \text{K}}$$

The initial temperature:

$$PV_1 = mR_{\text{helium}} T_1 \Rightarrow T_1 = \frac{P_1 V_1}{m R_{\text{helium}}}$$

$$\Rightarrow T_1 = \frac{180 \text{ kPa} \cdot 7,5 \text{ m}^3}{1,3 \text{ kg} \cdot 2,077 \frac{\text{kJ}}{\text{kg} \cdot \text{K}}} \approx \underline{\underline{500 \text{ K}}}$$

Final temperature:

$$\frac{P_1 V_1}{T_1} = \frac{P_2 V_2}{T_2} \Rightarrow T_2 = \frac{T_1 P_2 V_2}{P_1 V_1} = \frac{T_1 V_2}{V_1}$$

$$\Rightarrow T_2 = \frac{500 \text{ K} \cdot 2,5 \text{ m}^3}{7,5 \text{ m}^3} = \underline{\underline{166,7 \text{ K}}}$$

Total work:

$$W_b = P \cdot (V_2 - V_1) = 180 \text{ kPa} \cdot (2,5 \text{ m}^3 - 7,5 \text{ m}^3) \\ = \underline{\underline{-900 \text{ kJ}}}$$

Which means that the work required for the compression is 900 kJ

\* Q2)  $T = 320^\circ\text{C}$ ,  $V_1 = 2,1\text{m}^3$ ,  $x = 0,8$

Table A4 gives:

$$P_{@320^\circ\text{C}} = 11284 \text{ kPa}$$

and

$$v_f = v_{f@320^\circ\text{C}} = 0,001499 \frac{\text{m}^3}{\text{kg}}$$

$$v_g@320^\circ\text{C} = 0,015470 \frac{\text{m}^3}{\text{kg}}$$

Now we can find  $v_2$

$$v_2 = v_f + x v_g = v_f + x(v_g - v_f)$$

$$= 0,001499 \frac{\text{m}^3}{\text{kg}} + 0,8 \cdot (0,015470 - 0,001499) \frac{\text{m}^3}{\text{kg}}$$

$$= 0,0127 \frac{\text{m}^3}{\text{kg}}$$

Then we can find the volume in the end:

$$\frac{V_2}{v_2} = \frac{V_1}{v_1} \Rightarrow V_2 = \frac{V_1}{v_1} \cdot v_2 = \frac{2,1\text{m}^3 \cdot 0,0127 \frac{\text{m}^3}{\text{kg}}}{0,001499 \frac{\text{m}^3}{\text{kg}}}$$

$$\Rightarrow V_2 = 17,79 \text{ m}^3$$

We can assume constant pressure so:

$$W_b = P(V_2 - V_1) = 11284 \text{ kPa} (17,79 - 2,1) \text{ m}^3$$

$$\approx 177046 \text{ kJ}$$

$$\approx 1,77 \cdot 10^5 \text{ kJ}$$



\* Q5  $V_1 = 0.75 \text{ m}^3$ ,  $P_1 = 14 \text{ bar}$ ,  $P_2 = 55 \text{ bar}$ ,  $x_1 = 1$

In the beginning we have (from table A12)

$$V_1 = v_{g @ 14 \text{ bar}} = 0.014107 \frac{\text{m}^3}{\text{kg}}$$

At 55 bar we have

$$v_{f @ 55 \text{ bar}} = 0.0008130 \frac{\text{m}^3}{\text{kg}}$$

$$v_{g @ 55 \text{ bar}} = 0.037408 \frac{\text{m}^3}{\text{kg}}$$

And since  $V_1 = V_2$  because it's a rigid tank:

$$x_2 = \frac{V_2 - V_f}{V_g - V_f} = \frac{0.014107 \frac{\text{m}^3}{\text{kg}} - 0.0008130 \frac{\text{m}^3}{\text{kg}}}{0.037408 \frac{\text{m}^3}{\text{kg}} - 0.0008130 \frac{\text{m}^3}{\text{kg}}} = 0.363 \text{ which is a saturated mixture}$$

Final temp is then:

$$T_{\text{sat} @ 55 \text{ bar}} = 18.73^\circ \text{C}$$

Now we have

$$m_{\text{total}} = \frac{V_1}{v_1} = \frac{0.75 \text{ m}^3}{0.014107 \frac{\text{m}^3}{\text{kg}}} = 53.17 \text{ kg}$$

and we know that  $x_2 = 0.363$

so amount condensed is:

$$\begin{aligned} m_f &= (1 - x_2) m_{\text{total}} \\ &= (1 - 0.363) \cdot 53.17 \text{ kg} \\ &= 33.87 \text{ kg} \end{aligned}$$

\* Q7]  $V_1 = 0,065 \text{ m}^3$ ,  $P_1 = 230 \text{ kPa}$ ,  $T_1 = 55^\circ\text{C} = 328 \text{ K}$ ,  
 $W = 8,3 \text{ kJ}$

In table A2 we get  $R_{\text{nitro}} = 0,2968 \frac{\text{kJ}}{\text{kg K}}$   
 $C_v = 0,743 \frac{\text{kJ}}{\text{kg K}}$

Using ideal gas equation we get:

$$P_1 V_1 = m R T_1 \Rightarrow m = \frac{P_1 V_1}{R T_1}$$

$$\Rightarrow m = \frac{230 \text{ kPa} \cdot 0,065 \text{ m}^3}{0,2968 \frac{\text{kJ}}{\text{kg K}} \cdot 328 \text{ K}} = 0,1536 \text{ kg}$$

The equation for the work is:

$$W = m \cdot C_v \cdot (T_2 - T_1)$$

$$\Rightarrow T_2 = \frac{W}{m \cdot C_v} + T_1 = \frac{8,3 \text{ kJ}}{0,1536 \text{ kg} \cdot 0,743 \frac{\text{kJ}}{\text{kg K}}} + 328 \text{ K}$$

$$\Rightarrow T_2 \approx 1400 \text{ K}$$



\* Q5

$$m = 5,4 \text{ kg}, \quad p = 215 \text{ kPa}, \quad T = 37^\circ \text{C} = 310 \text{ K}$$

$$W_{\text{out}} = 14,7 \text{ kJ}, \quad W_{\text{in}} = 3,56 \text{ kJ}$$

Since this is a closed system we have

$$E_{\text{in}} - E_{\text{out}} = \Delta E_{\text{system}}$$

$$\Rightarrow Q_{\text{in}} + W_{\text{in}} - W_{\text{out}} = m C_v (T_2 - T_1)$$

Now we know since this is an isothermal process that  $T_1 = T_2$  so

$$Q_{\text{in}} + W_{\text{in}} - W_{\text{out}} = 0$$

$$\Rightarrow Q_{\text{in}} = W_{\text{out}} - W_{\text{in}} = 14,7 \text{ kJ} - 3,56 \text{ kJ} \\ = 11,14 \text{ kJ}$$