

CL202: Fluid Mechanics

## Introductory Concepts



Raghvendra Gupta  
Department of Chemical Engineering  
Indian Institute of Technology Guwahati

# What has been covered till now?

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Let us list down

- Definition of a fluid
- Applications
- Three approaches to analyse fluid flow problems
- Continuum hypothesis
- No-slip condition
- Eulerian and Lagrangian descriptions
- System and control volume

# Velocity field

- Field: A quantity that has a value at each point in time and space (continuum)
- Velocity  $\vec{v}(x, y, z, t)$  or  $\mathbf{v}(x, y, z, t)$  is a vector quantity

$$\mathbf{v}(x, y, z, t) = u(x, y, z, t)\hat{i} + v(x, y, z, t)\hat{j} + w(x, y, z, t)\hat{k}$$

- **Indicates the velocity of a fluid particle that is at point P(x, y, z) at time t in**

## **Eulerian description**

- P(x,y,z) are coordinate of a point fixed in space not the position of the fluid particle
- Steady flow:

$$\frac{\partial \mathbf{v}}{\partial t} = 0$$

# Stress Field

The force acting on a fluid particle can be:

➤ Body forces e.g. gravitational force, electromagnetic force

➤ Force acts on an element of fluid volume

$$\text{Gravitational force} = \rho \mathbf{g} dV$$

$$\text{Gravitational force per unit volume} = \rho \mathbf{g}$$

$$\text{Gravitational force per unit mass} = \mathbf{g}$$

➤ Surface forces e.g. pressure, friction

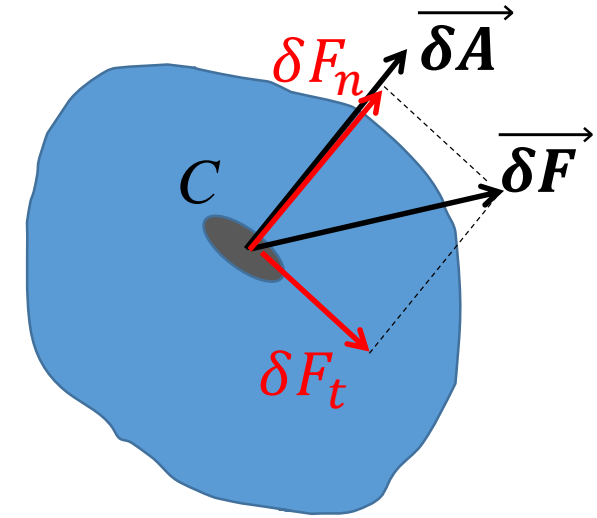
➤ Force acts on the boundary of the fluid medium

➤ The force is transmitted throughout the medium

➤ Stress is developed in the fluid medium

# Stress Field

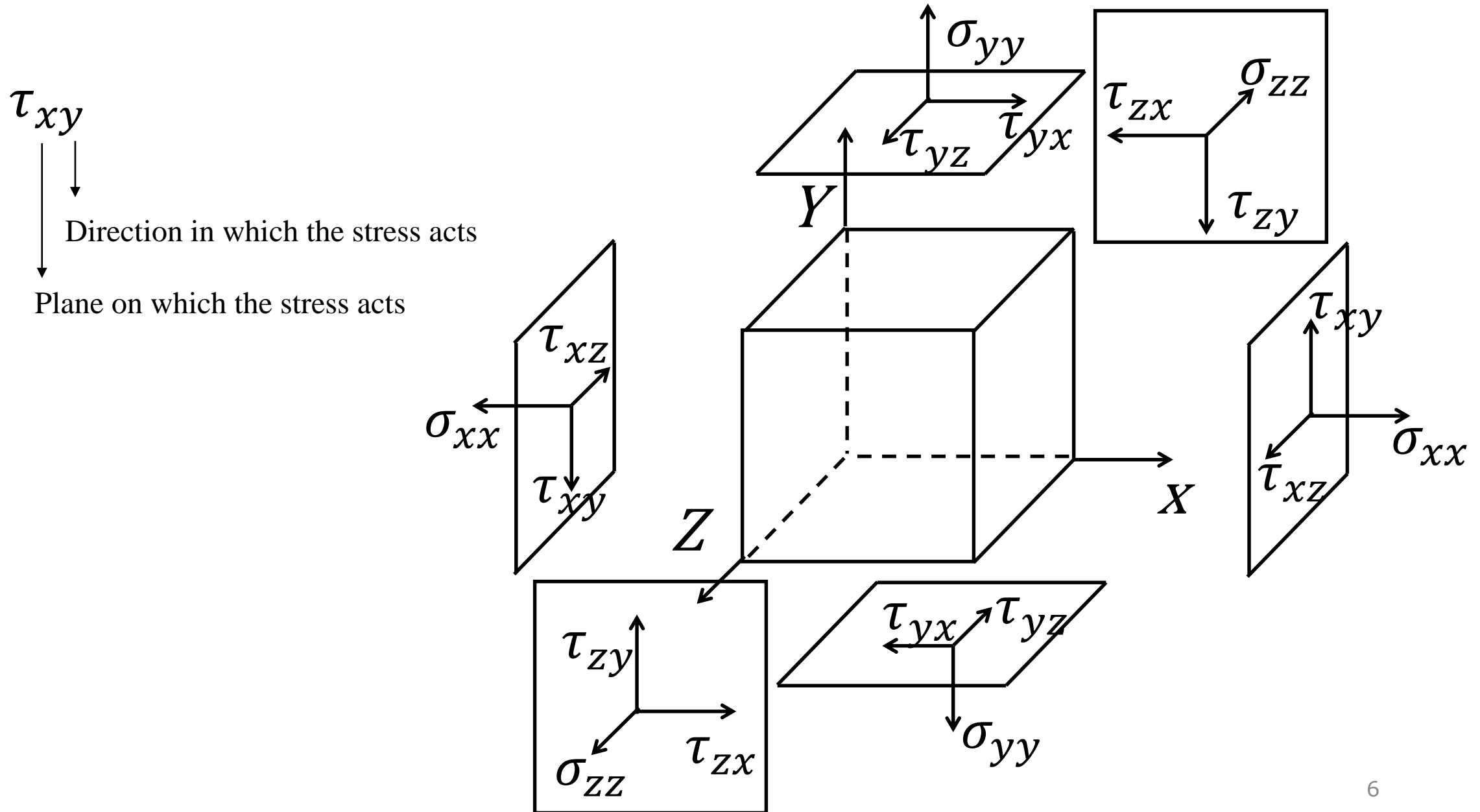
- Stress: defined as force per unit area
- Consider a small area  $\delta A$  on the surface of a fluid particle which is in contact with other fluid particles
  - Note that area is a vector and its direction is along the outward normal with respect to the particle
- We can resolve the force in components tangential and normal to the surface



$$\text{Normal stress } \sigma_n = \lim_{\delta A_n \rightarrow 0} \frac{\delta F_n}{\delta A_n}$$

$$\text{Shear (tangential) stress } \tau_n = \lim_{\delta A_n \rightarrow 0} \frac{\delta F_t}{\delta A_n}$$

# Stress Field



# Stress Field

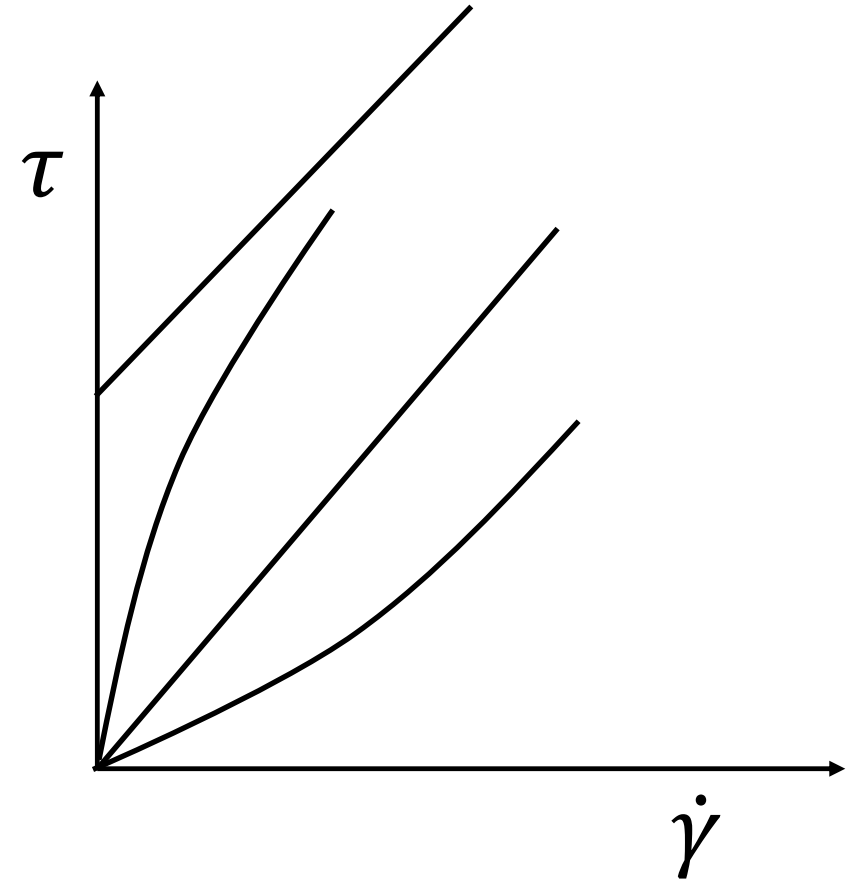
- The state of stress at a point can be described by the stresses acting on any three mutually perpendicular planes.
- The stress at a point has nine components

$$\begin{vmatrix} \sigma_{xx} & \tau_{xy} & \tau_{xz} \\ \tau_{yx} & \sigma_{yy} & \tau_{yz} \\ \tau_{zx} & \tau_{zy} & \sigma_{zz} \end{vmatrix}$$

- Sign convention for stress:
  - Positive when the direction of stress component and that of the normal on the plane both are positive or both are negative.

# Rheology

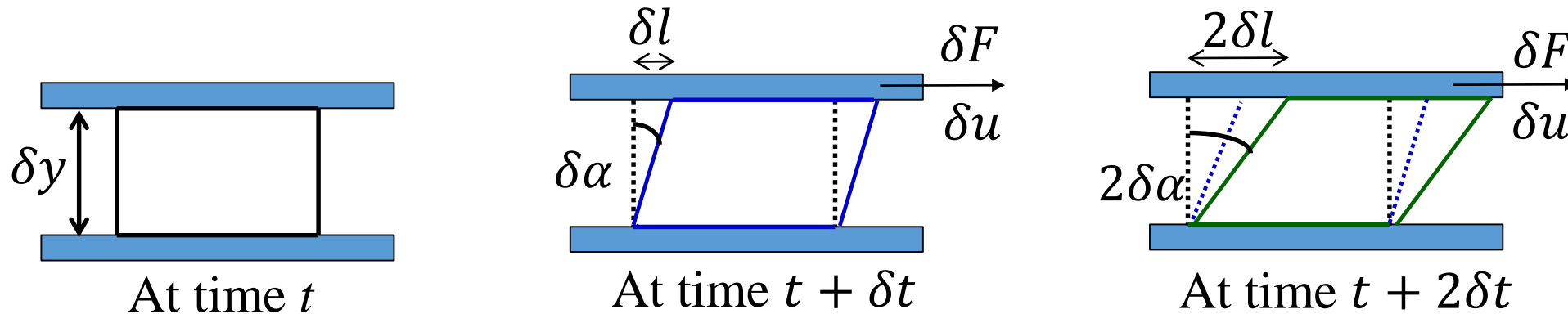
- Fluids are characterized by the relationship between shear stress ( $\tau$ ) and rate of deformation/ rate of strain ( $\dot{\gamma}$ ) in a fluid
- A constitute equation gives the relationship between stress and rate of strain.
- Rheology
- Rheometers





# Rate of strain

- What is  $\dot{\gamma}$ ?
  - Rate of deformation or shear rate or rate of strain
  - Shear strain: Relative displacement of particles in the body
- Consider flow between two parallel plates with the upper plate moving



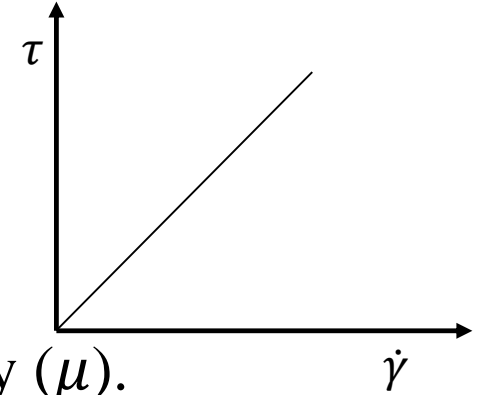
- Rate of deformation  $\dot{\gamma} = \lim_{\delta t \rightarrow 0} \frac{\delta \alpha}{\delta t}$
- $\delta l = \delta u \delta t = \delta \alpha \delta y \quad \longrightarrow \quad \frac{\delta \alpha}{\delta t} = \frac{\delta u}{\delta y}$   
 $\dot{\gamma} = \frac{d\alpha}{dt} = \frac{du}{dy}$

# Viscosity

- For most of the common fluids, shear stress is directly proportional to the rate of strain

$$\tau \propto \dot{\gamma}$$

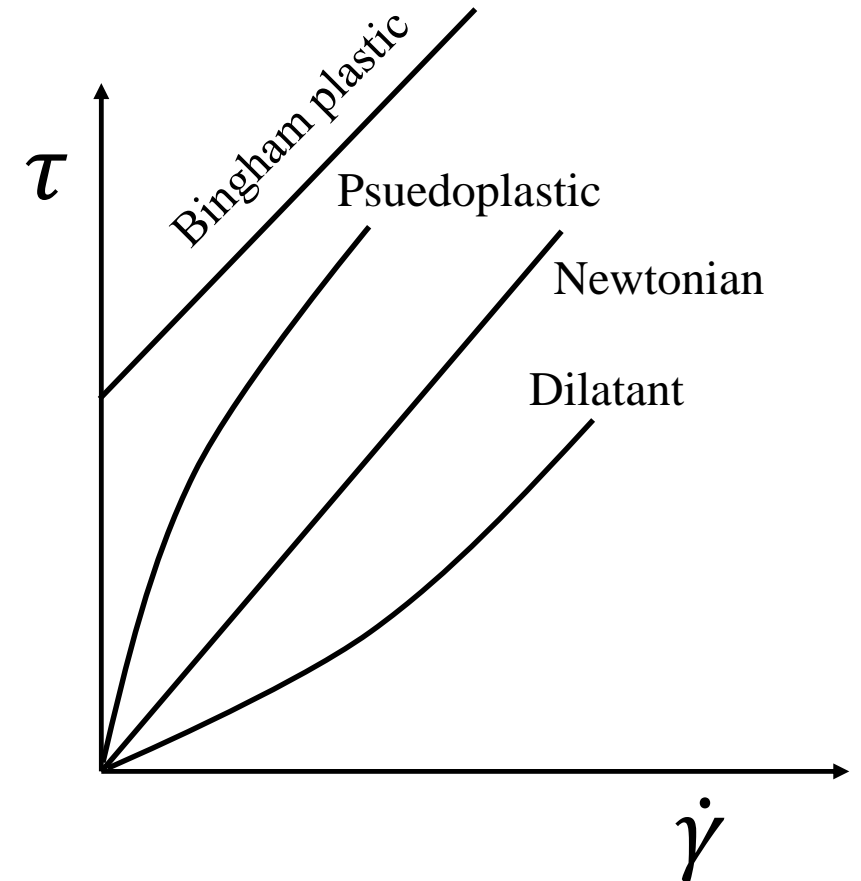
$$\tau_{yx} = \mu \dot{\gamma}$$



- This is known as Newton's law of viscosity.
- The proportionality constant is known as dynamic or absolute viscosity ( $\mu$ ).
- The fluids following Newton's law of viscosity are known as Newtonian fluids.
- Unit of viscosity-  $\text{kg m}^{-1}\text{s}^{-1}$ , Pa.s, Poise in CGS.
- Kinematic viscosity ( $\nu$ ): ratio of dynamic viscosity and density ( $\mu/\rho$ )
  - Unit:  $\text{m}^2/\text{s}$  or Stokes
- Viscosity of gases increases with increase in temperature whereas those of liquid decreases.

# Non-Newtonian Fluids

- Fluids that do not follow Newton's law of viscosity.
- Bingham plastic fluids:
  - Yield stress
  - Toothpaste, drilling mud, clay suspensions
- Psuedoplastic (shear thinning)
  - Apparent viscosity decreases with increasing shear rate
  - Polymer solutions, colloidal suspension
- Dilatant (shear thickening)
  - Apparent viscosity increases with increasing shear rate
  - Suspension of starch, sand



# Non-Newtonian Fluids

## ➤ Herschel-Bulkley model:

$$\tau_{yx} = \tau_y + k\dot{\gamma}^n$$

➤  $\tau_y$ : Yield stress

➤  $k$ : Consistency index

➤  $n$ : Flow behaviour index

➤ For Bingham plastic fluid

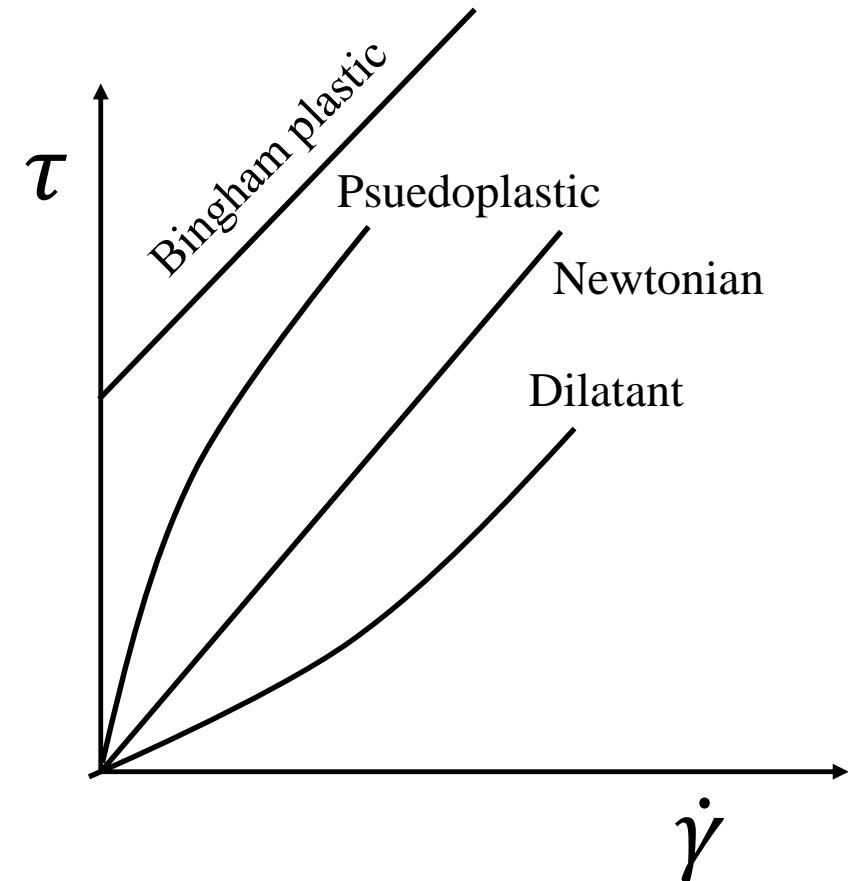
➤ Yield stress ( $\tau_y$ ) non-zero,  $n = 1$

➤ Psuedoplastic fluids:

➤ Yield stress zero,  $n < 1$

➤ Dilatant fluid

➤ Yield stress zero,  $n > 1$



# Non-Newtonian Fluids

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- The apparent viscosity may be time-dependent
- Thixotropic fluids:
  - Decrease in apparent viscosity with time
- Rheopectic fluids:
  - Increase in apparent viscosity with time
- Viscoelastic fluids:
  - Partially regain the original shape when the applied stress is released