

		[4]					
OR	iii.	A steel rod ( $k = 30 \text{ W/m-deg}$ ) 1 cm in diameter and 5 cm long protrudes from a wall which is maintained at $100^\circ\text{C}$ . The rod is insulated at its tip and is exposed to an environment with $h = 50 \text{ W/m}^2\text{-deg}$ and $t_a = 30^\circ\text{C}$ . Calculate the fin efficiency, temperature at the tip of fin and the rate of heat dissipation.	8	4	3	3	3
Q.5	i.	Explain Fick's law of diffusion.	2	1	2	4	2
	ii.	What is the limitation of LMTD method? How effectiveness – NTU method superior to it.	3	1	3	4	2
	iii.	A heat exchanger is to be designed to condense 8 kg/s of an organic liquid ( $t_{\text{sat}} = 80^\circ\text{C}$ ; $h_{\text{fg}} = 600 \text{ kJ/kg}$ ) with cooling water available at $15^\circ\text{C}$ and at a flow rate of 60 kg/s. The overall heat transfer coefficient is $480 \text{ W/m}^2\text{-deg}$ . Calculate the number of tubes required. The tubes are to be of 25 mm outer diameter, 2 mm thickness and 4.85 m length.	5	4	3	4	3
OR	iv.	Derive the expression for the LMTD for the parallel flow arrangement.	5	3	2	4	2
Q.6	i.	What is mean by fouling factor? How does it affect the performance of a heat exchanger?	4	2	2	5	3
	ii.	A black body of total area $0.045 \text{ m}^2$ is completely enclosed in a space bounded by 5 cm thick walls. The walls have a surface area $0.5 \text{ m}^2$ and thermal conductivity $1.07 \text{ W/m-deg}$ . If the inner surface of the enveloping wall is to be maintained at $215^\circ\text{C}$ and the outer wall surface is at $30^\circ\text{C}$ , calculate the temperature of the black body. Neglect the difference between inner and outer surface areas of enveloping material.	6	4	3	5	2
OR	iii.	The flat floor of a hemispherical furnace is at 800 K and has an emissivity of 0.5. The corresponding values for the hemispherical roof are 1200 K and 0.25. Determine the net radiation heat transfer from the roof to floor.	6	4	3	5	2

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Total No. of Questions: 6

Total No. of Printed Pages:4

Enrollment No.....



Faculty of Engineering  
End Sem Examination Dec 2024  
ME3CO32 Heat & Mass Transfer

Programme: B.Tech.

Branch/Specialisation: ME

Duration: 3 Hrs.

Maximum Marks: 60

Note: All questions are compulsory. Internal choices, if any, are indicated. Answers of Q.1 (MCQs) should be written in full instead of only a, b, c or d. Assume suitable data if necessary. Notations and symbols have their usual meaning.

		Marks	BL	PO	CO	PSO
Q.1	i. A composite plane wall is made up of two different materials of the same thickness and having thermal conductivities of $k_1$ and $k_2$ respectively. The equivalent thermal conductivity of the slab is: (a) $k_1 + k_2$ (b) $k_1 k_2$ (c) $(k_1 + k_2) / k_1 k_2$ (d) $2 k_1 k_2 / (k_1 + k_2)$	1	1	1	1	3
	ii. Heat is conducted through a 10 cm thick wall at the rate of $30 \text{ W/m}^2$ when the temperature difference across the wall is $10^\circ\text{C}$ . What is the thermal conductivity of the wall? (a) $0.03 \text{ W/mK}$ (b) $0.3 \text{ W/mK}$ (c) $3.0 \text{ W/mK}$ (d) $30.0 \text{ W/mK}$	1	2	1	1	3
	iii. The ratio of energy transferred by convection to that by conduction is called- (a) Stanton number (b) Nusselt number (c) Biot number (d) Precllet number	1	1	2	2	2
	iv. Air at $20^\circ\text{C}$ blows over a hot plate of $50 \times 60 \text{ cm}$ made of carbon steel maintained at $220^\circ\text{C}$ . The convective heat transfer coefficient is $25 \text{ W/m}^2\text{K}$ . What will be the heat loss from the plate? (a) $1500\text{W}$ (b) $2500 \text{ W}$ (c) $3000 \text{ W}$ (d) $4000 \text{ W}$	1	2	3	2	3
	v. Which one of the following is correct?	1	1	1	3	3

P.T.O.

[2]					
The effectiveness of a fin will be maximum in an environment with					
(a) Free convection					
(b) Forced convection					
(c) Radiation					
(d) Convection and radiation					
vi.	Addition of fin to the surface increases the heat transfer if $hA/KP$ is:	1	2	2	3 3
(a) Equal to one					
(b) Greater than one					
(c) Less than one					
(d) Greater than one but less than two					
vii.	In a heat exchanger, the hot liquid enters with a temperature of 180°C and leaves at 160°C. The cooling fluid enters at 30°C and leaves at 110°C. The capacity ratio of the heat exchanger is:	1	2	3	4 2
(a) 0.25 (b) 0.40					
(c) 0.50 (d) 0.55					
viii.	In case of liquids, what is the binary diffusion coefficient proportional to?	1	1	2	4 3
(a) Pressure only (b) Temperature only					
(c) Volume only (d) All of these					
ix.	In radiative heat transfer, a gray surface is one-	1	1	1	5 3
(a) Which appears gray to the eye					
(b) Whose emissivity is independent of wavelength					
(c) Which has reflectivity equal to zero					
(d) Which appears equally bright from all directions.					
x.	If the temperature of a solid state changes from 27°C to 627°C, then emissive power changes which rate?	1	2	3	5 2
(a) 6 : 1 (b) 9 : 1					
(c) 27 : 1 (d) 81 : 1					
Q.2 i.	Explain critical thickness of insulation taking example of steam carrying pipe.	4	3	3	1 3
ii.	A furnace wall is a made up of steel plate 10 mm thick ( $k = 62.8$ kJ/m-hr-deg) lined on inside with	6	4	3	1 2

[3]					
silica bricks 150 mm thick ( $k = 7.32$ kJ/m-hr-deg) and on the outside with magnesia bricks 200 mm thick ( $k = 18.84$ kJ/m-hr-deg). The inside and outside surfaces of the wall are at temperature 650°C and 125°C respectively. Make calculations for the heat loss from unit area of the wall.					
OR	iii.	Derive an expression of general heat conduction equation in Cartesian coordinate.	6	3	3 1 3
Q.3	i.	Distinguish between natural and forced convection heat transfer.	2	2	2 2 3
	ii.	Calculate the rate of heat loss from a human body which may be considered as a vertical cylinder 30 cm in diameter, and 175 cm high while standing in a 30 km/hr wind at 15°C. The surface temperature of the human is 35°C. The thermo-physical properties of air at mean film temperature of 25°C are as follows: $\nu = 15.33 \times 10^{-6}$ m <sup>2</sup> /s; $k = 0.0263$ W/m-deg; $Pr=0.7$	8	4	3 2 2
OR	iii.	The oil pan of an engine approximates a flat plate 0.3 m wide by 0.45 m long and protrudes below the framework of the automobile. The engine oil is at 95°C and the ambient air temperature is 35°C. If the automobile runs at 36 km/hr, make calculations for the rate of heat transfer from the oil-pan surface. Assume negligible resistance to conduction through the oil pan. The thermo-physical properties of air at mean film temperature of 65°C are as follows: $\nu = 18.46 \times 10^{-6}$ m <sup>2</sup> /s; $k = 0.0293$ W/m-deg; $Pr=0.695$	8	4	3 2 2
Q.4	i.	How does a fin enhance heat transfer at a surface?	2	2	3 3 3
	ii.	Derive an expression for heat dissipation from a fin insulated at the tip.	8	3	3 3 3

**Marking Scheme**  
ME3CO32 (T) Heat & Mass Transfer (T)

Q.1	i)	(d) $2 k_1 k_2 / (k_1 + k_2)$	1
	ii)	(b) 0.3 W/mK	1
	iii)	(b) Nusselt number	1
	iv)	(a) 1500W	1
	v)	(a) Free convection	1
	vi)	(c) Less than one	1
	vii)	(a) 0.25	1
	viii)	(b) Temperature only	1
	ix)	(b) Whose emissivity is independent of wavelength	1
	x)	(d) 81: 1	1
Q.2	i.	Definition of critical thickness with Rate of heat transfer vs length or radius diagram	2
		Explanation of condition for critical thickness of insulation for steam carrying pipe	2
	ii.	Calculation of thermal resistance in steel plate, silica bricks, and magnesia bricks	3
		Calculation of total thermal resistance of the composite wall	
		Calculation of heat loss from the wall (1*3M)	
OR	iii.	Heat influx and efflux in x, y, and z direction	3
		Total heat generated in control volume	
		Energy balance and final expression (1*3M)	
Q.3	i.	Brief but clear distinctions with examples	2
	ii.	Calculation of Reynolds number 2M	8
		Calculation of Nusselt number 2M	
		Calculation of convective heat transfer coefficient 2M	
		Calculation of convective heat loss 2M	
OR	iii.	Calculation of Reynolds number 2M	8
		Calculation of Nusselt number 2M	
		Calculation of convective heat transfer coefficient 2M	
		Calculation of convective heat flow 2M	

Q.4	i.	Clear and concise answer with an example	2
	ii.	Boundary conditions 2M	8
		Stepwise derivation 4M	
		Final Expression 2M	
OR	iii.	Calculation of parameter 'm' 2M	8
		Calculation of the fin efficiency 2M	
		Calculation of temperature at the tip of fin 2M	
		Calculation of rate of heat dissipation. 2M	
Q.5	i.	Statement of Fick's law of diffusion	2
	ii.	Explanation of LMTD limitations 1.5M	3
		Advantages of effectiveness-NTU 1.5M	
	iii.	Calculation of outlet temperature of water 1M	5
		Calculation of LMTD 2M	
		Calculation of no. of tubes 2M	
OR		Step-by-step derivation 3.5M	5
		Correct final expression 1.5M	
Q.6	i.	Definition of fouling factor 2M	4
		Explanation of its impact on performance 2M	
	ii.	Calculation of net heat radiated from black body to wall 2M	6
		Calculation of heat conducted through wall 2M	
		Calculation of temperature of black body 2M	
OR	iii.	Calculation of grey body factor from floor to roof 4M	6
		Calculation of net radiation heat transfer from the roof to floor 2M	

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