

# **Validere**

## **Crude oil blending problem**

**Anyang Peng, Oct 18 2022**

# Problem Statement

- Given distillation profiles of two crude oils, create a model which will give an approximate distillation profile of the mixture of the two oils with specified volumes.
- (Note: thinking of the distillation profiles as **snapshots** of functions is the recommended view.) The percentages to use (and get at the end) are the same as the ones in the above example, namely: [ 5, 10, 20, 30, 40, 50, 60, 70, 80, 90, 95, 99]. Explain any assumptions or simplifications made.

05% : 45°C

10% : 95°C

20% : 101°C

30% : 140°C

40% : 179°C

50% : 210°C

60% : 225°C

70% : 260°C

80% : 310°C

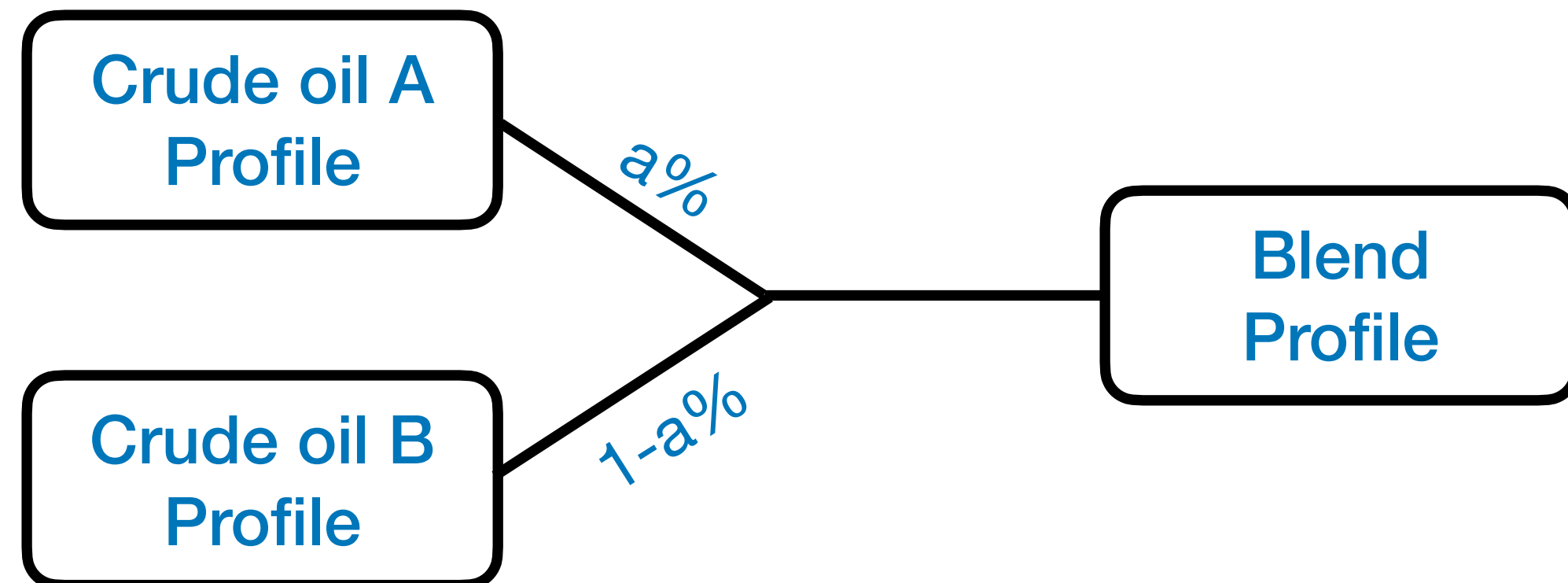
90% : 330°C

95% : 360°C

99% : 381°C

# Objectives

- Create a mathematical model to predict the distillation profile of the blend given the distillation profiles of two crude oils and the mixing ratio.

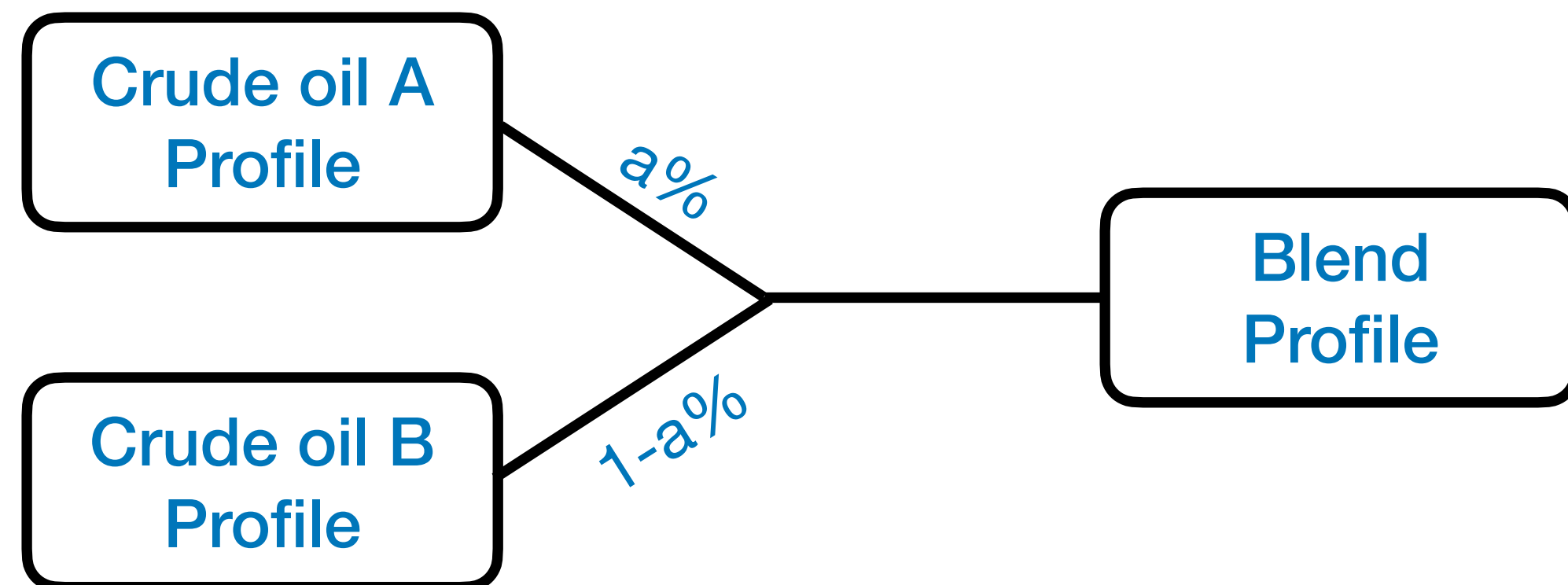


# Approaches

- Rule-based approach: derive the model from physics.
- Machine learning approach: learn the model from large amount of data

# Objectives

- Create a mathematical model to predict the distillation profile of the blend given the distillation profiles of two crude oils and the mixing ratio.



# Approaches

- Rule-based approach: derive the model from physics.
- Machine learning approach: learn the model from large amount of data
- Comparison
- Uncertainty

# Rule-based Approach

## Background

- Distillation: the process to separate chemicals based on the difference between their boiling points.

# Rule-based Approach

## Background

- Distillation: the process to separate chemicals based on the difference between their boiling points.
- What controls the boiling point?

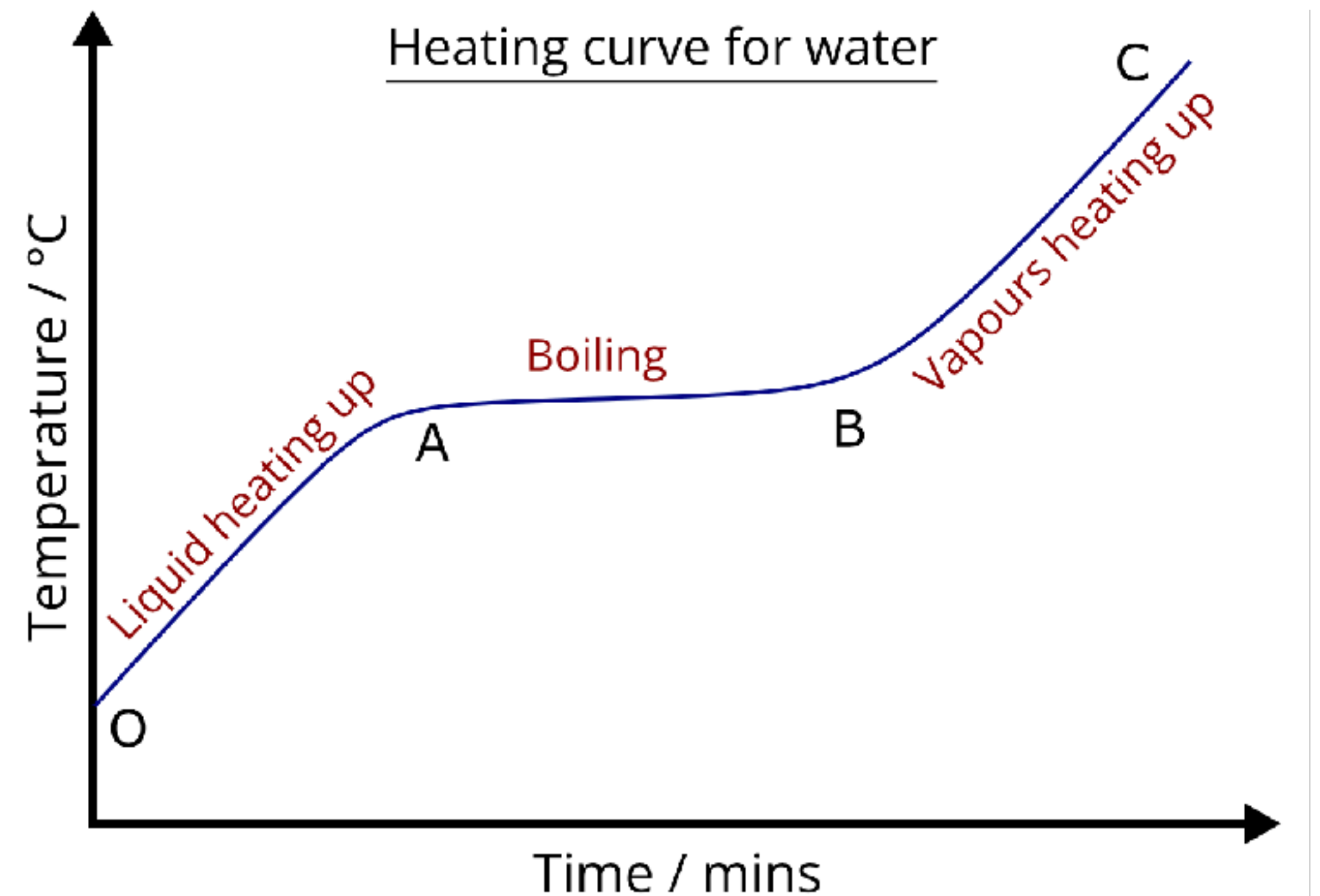
# Rule-based Approach

## Background

- Distillation: the process to separate chemicals based on the difference between their boiling points.

- What controls the boiling point?

The liquid boils when the vapor pressure is equal to the pressure of the environment



# Rule-based Approach

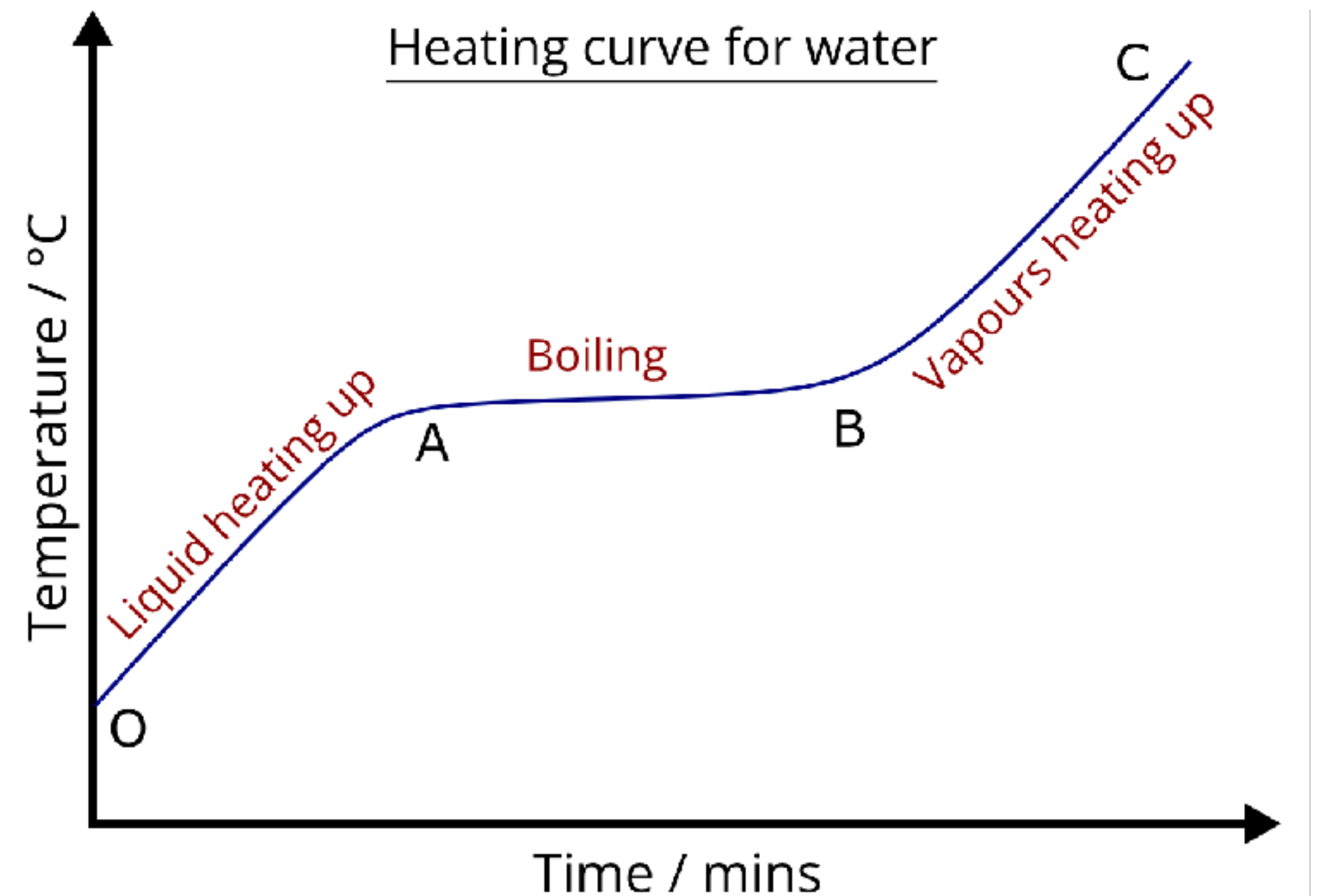
## Background

- Distillation: the process to separate chemicals based on the difference between their boiling points.

- What controls the boiling point?

The liquid boils when the vapor pressure is equal to the pressure of the environment

- How does distillation occur in mixtures?





# Rule-based Approach

## Background

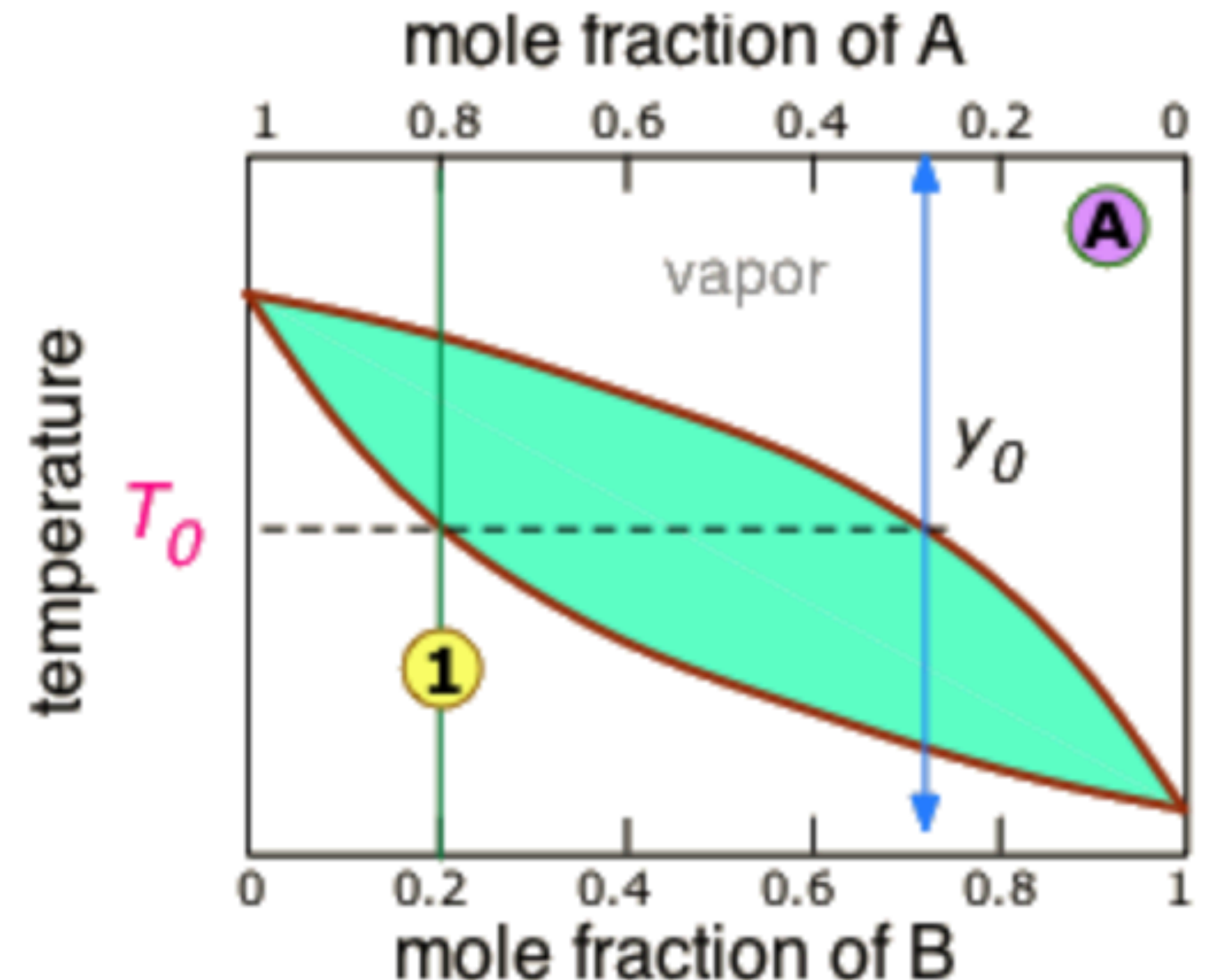
- Distillation: the process to separate chemicals based on the difference between their boiling points.

- What controls the boiling point?

The liquid boils when the vapor pressure is equal to the pressure of the environment

- How does distillation occur in mixtures?

For a binary mixture, the temperature at which the mixture boils depends on the composition of the mixture, and it changes throughout the boiling process.



# Rule-based Approach

## Background

- What about our problem?
  - Our system is not binary.
  - We don't know the exact composition.
  - No well defined boiling points, boiling ranges overlap.

It is impossible to solve this problem analytically with the given information using the approach mentioned for the binary system.

We need to simplify the system by making assumptions

# Rule-based Approach

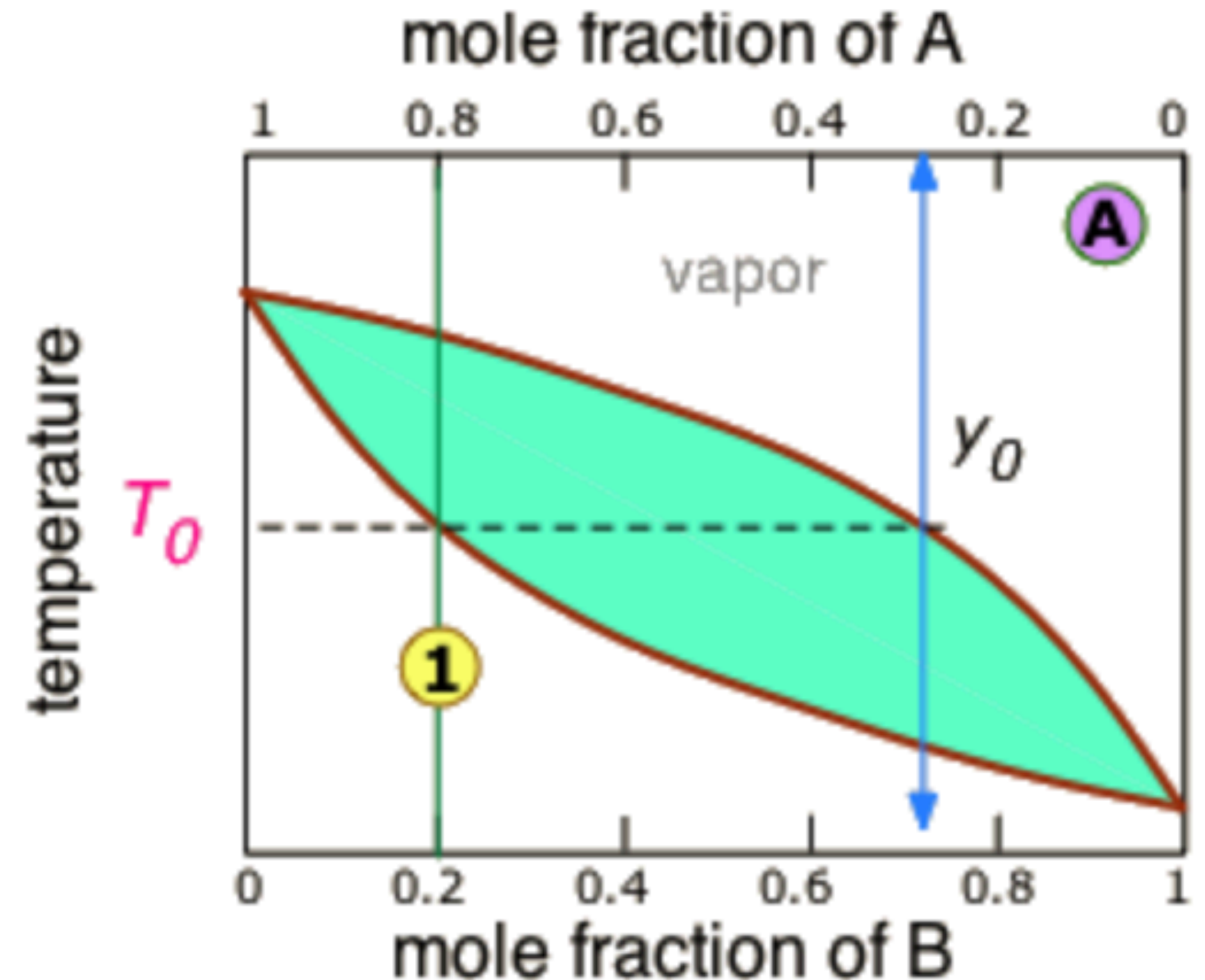
## Assumptions

- I assume the distillation settings are all the same (ramping rate, heat transfer, mixing, etc.) **Fair assumption.**

# Rule-based Approach

## Assumptions

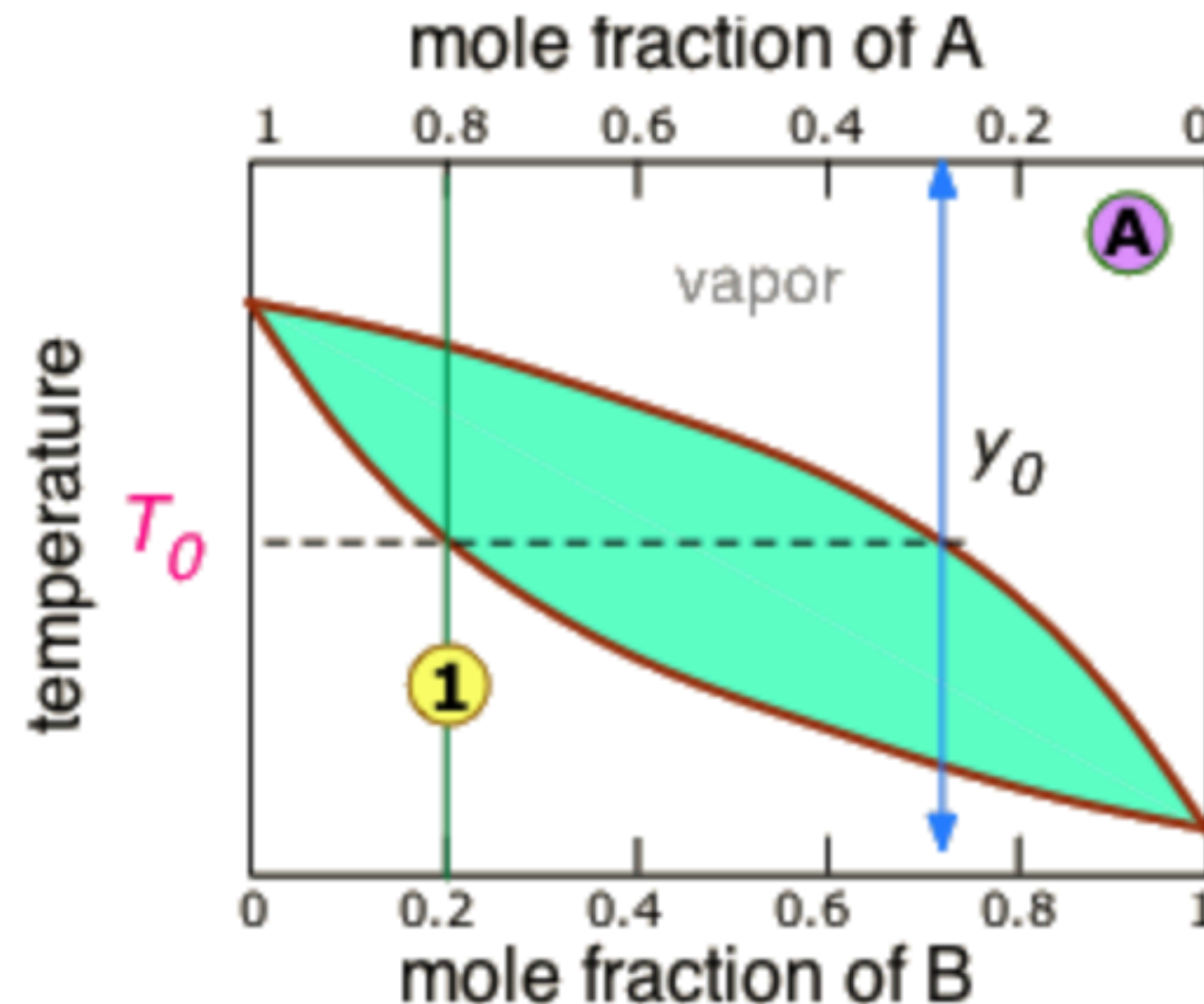
- I assume the distillation settings are all the same (ramping rate, heat transfer, mixing, etc.) **Fair assumption.**
- Based on the composition list, I assume azeotropic composition is not an issue. In other words the boiling point moves along the bubble point curve in the above figure (if we consider a binary mixture) **Fair assumption.**



# Rule-based Approach

## Assumptions

- I simplify the curve to a straight line. As a result, the boiling temperature is approximately linearly dependent on the composition within a small range  
OK assumption.



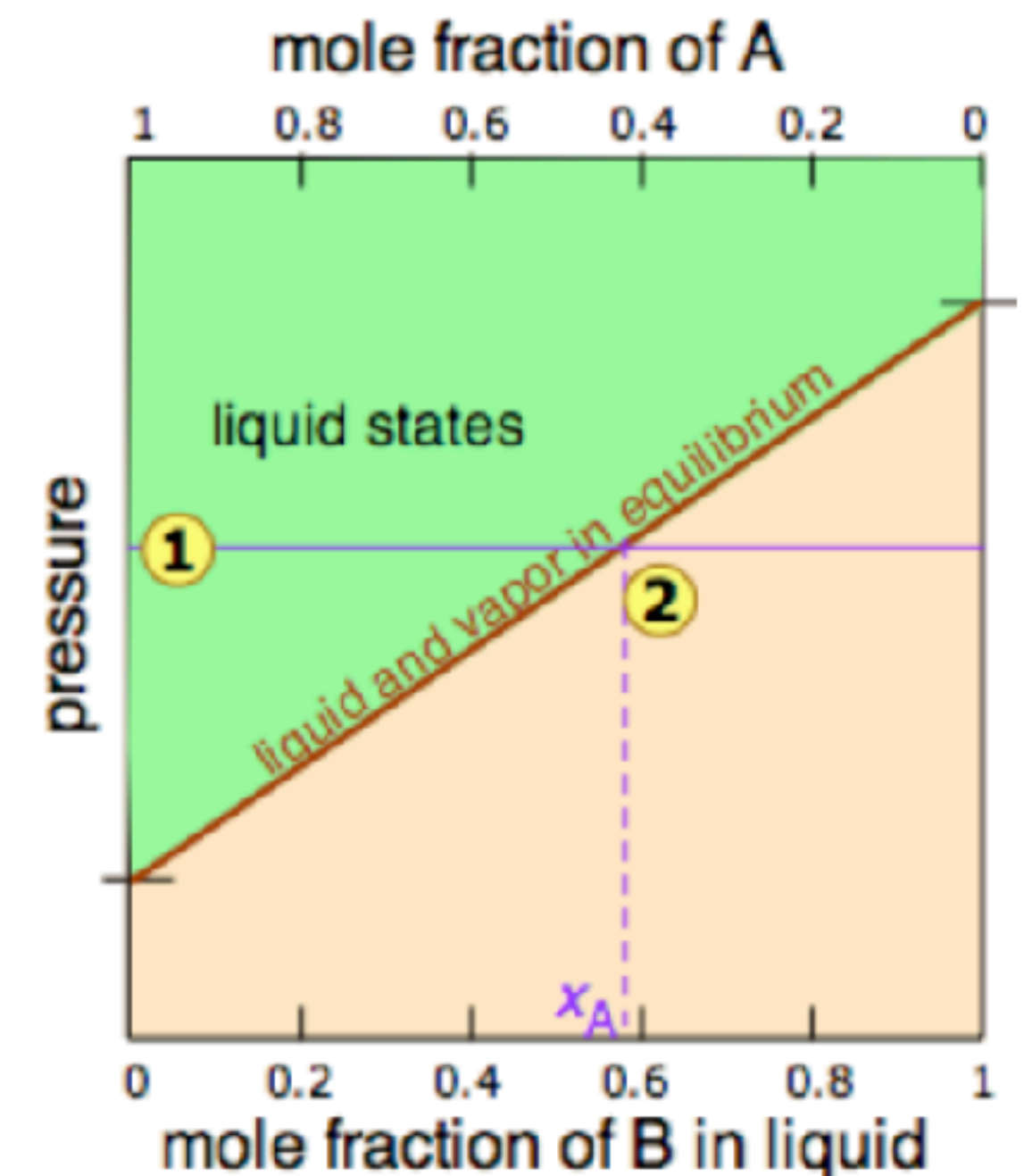


# Rule-based Approach

## Assumptions

- I simplify the curve to a straight line. As a result, the boiling temperature is approximately linearly dependent on the composition within a small range  
OK assumption.

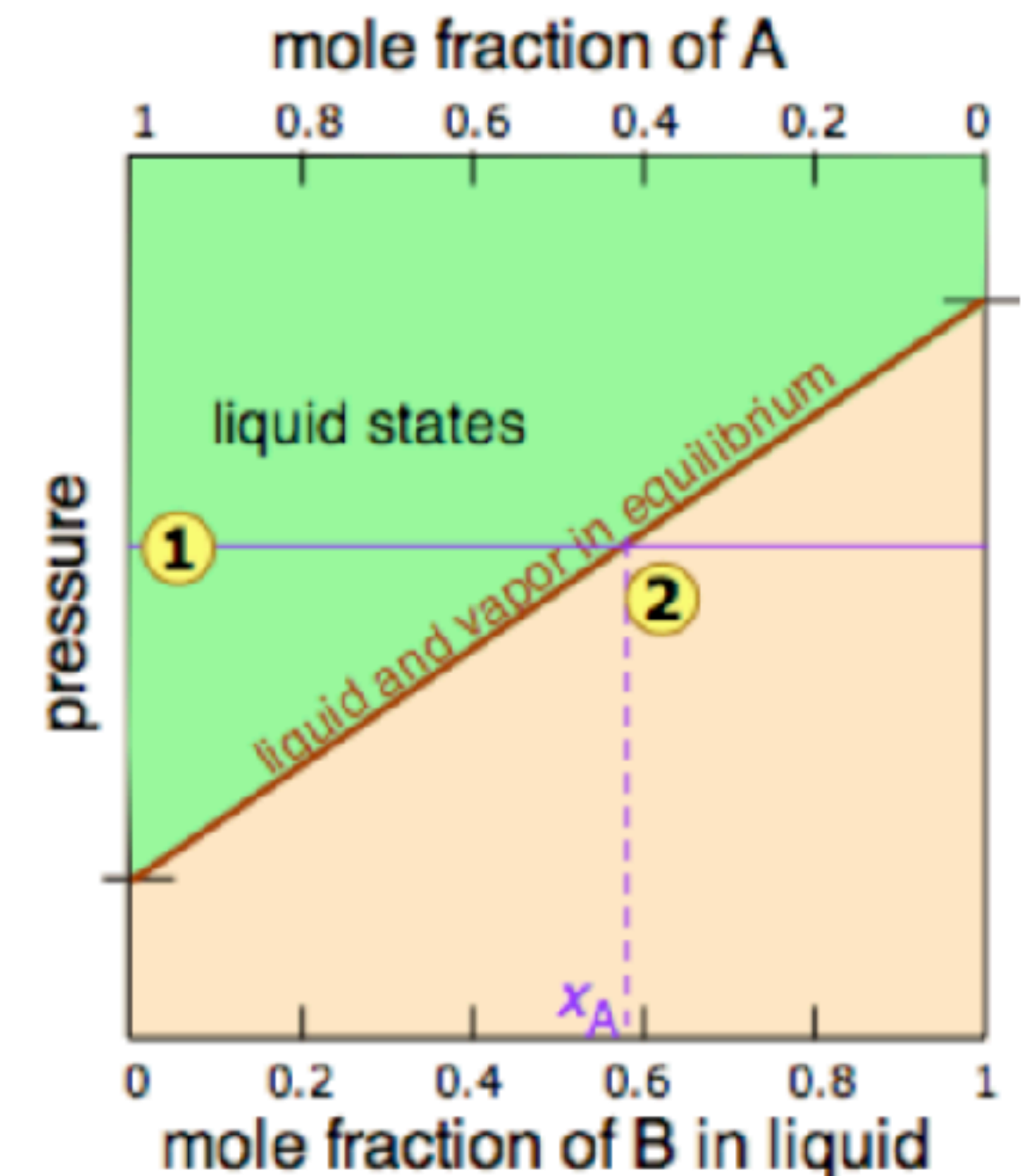
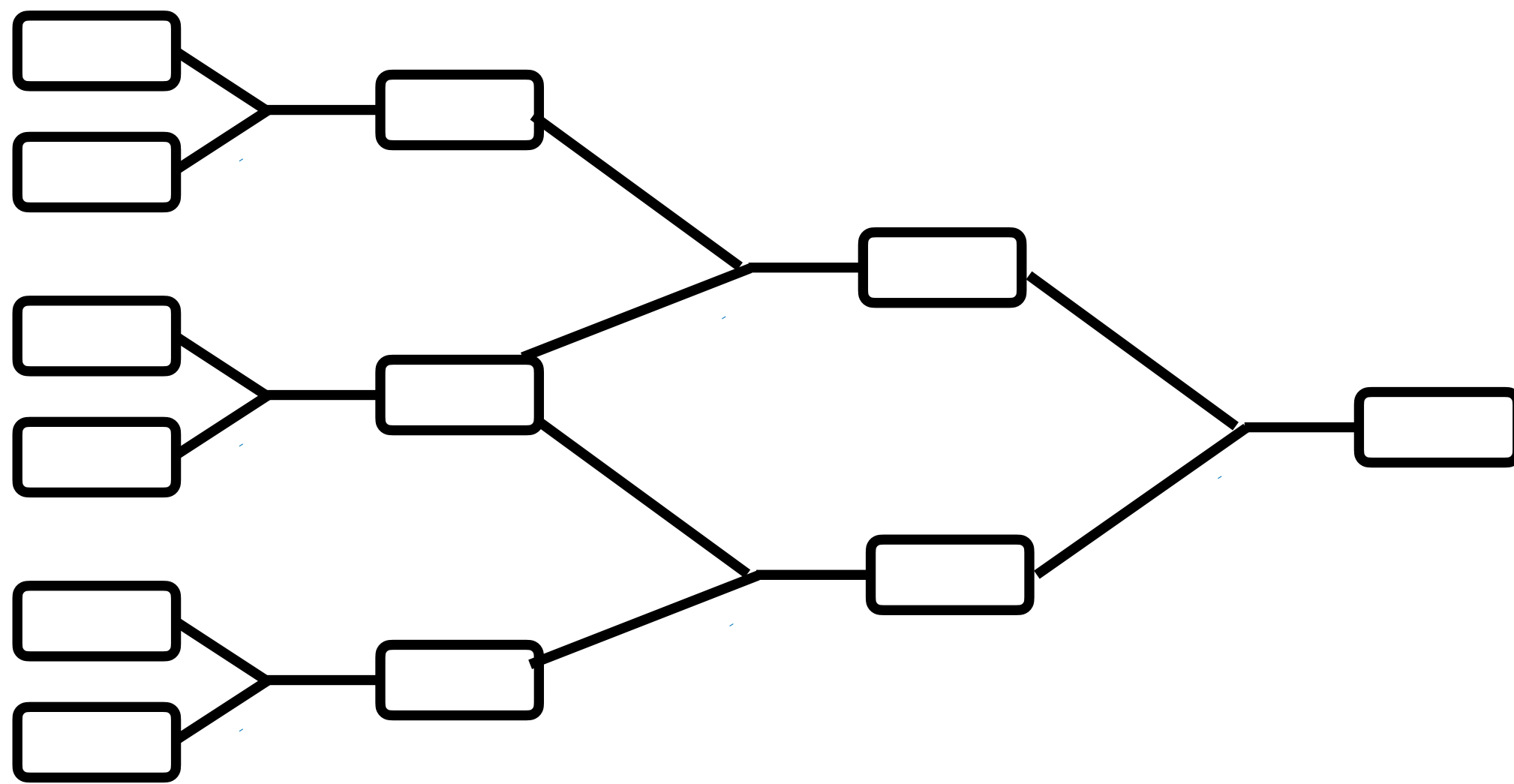
- This also implies the dew point curve is close to the boiling point curve, and the distillation does not change the molar fraction of each components in the liquid phase. (This is not a valid assumption, but necessary to simplify the problem.)



# Rule-based Approach

## Assumptions

- At each time snapshot, microscopically, I simplify the multi-component mixture to many binary mixture systems (this neglects the interaction between those systems which inevitably leads to error). **This is a bold assumption, but necessary to simplify the problem.**



# Rule-based Approach

## Demo

*Given the above information, we can get a very rough estimation on the distillation profile of the blend using a linear combination of the starting crude oil.*

- Sanity Check
  - 50% A + 50% A = A
  - 99% A + 1% B should be similar to A.
  - 1% A + 99% B should be similar to B.
  - if A has no residue, B has 20% residue, mix in a 1:1 ratio, we should have 10% residue.

```
if __name__ == '__main__':  
    #A is BG past Avg(Feb 04, 2008), B is AWB past Avg(Jun 29, 2010)  
    compA = Distill([28.0, 52.7, 78.7, 117.9, 160.2, 207.9, 264.8, 324.9, 393.3, 478.7, 571.4, 619.2, 685.2])  
    compB = Distill([34.2, 46.8, 82.5, 235.4, 350.8, 426.4, 498.3, 582.4, 658.7, 708.9, float('inf'), float('inf'), float('inf')])  
  
    m = Model(compA, compB)  
    print(m.blend(0.8))  
    assert m.blend(0) == compB.temp  
    assert m.blend(1) == compA.temp
```

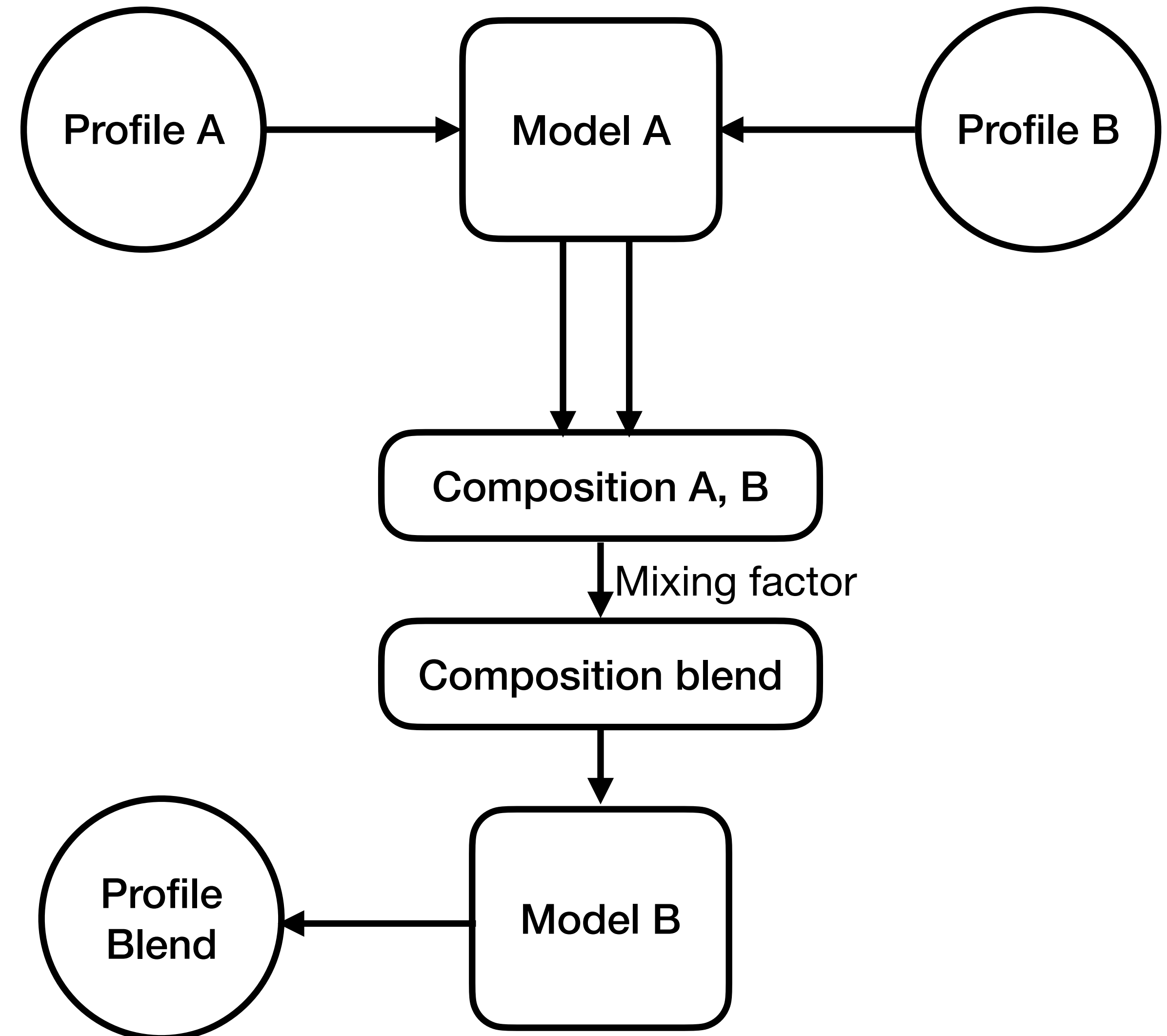
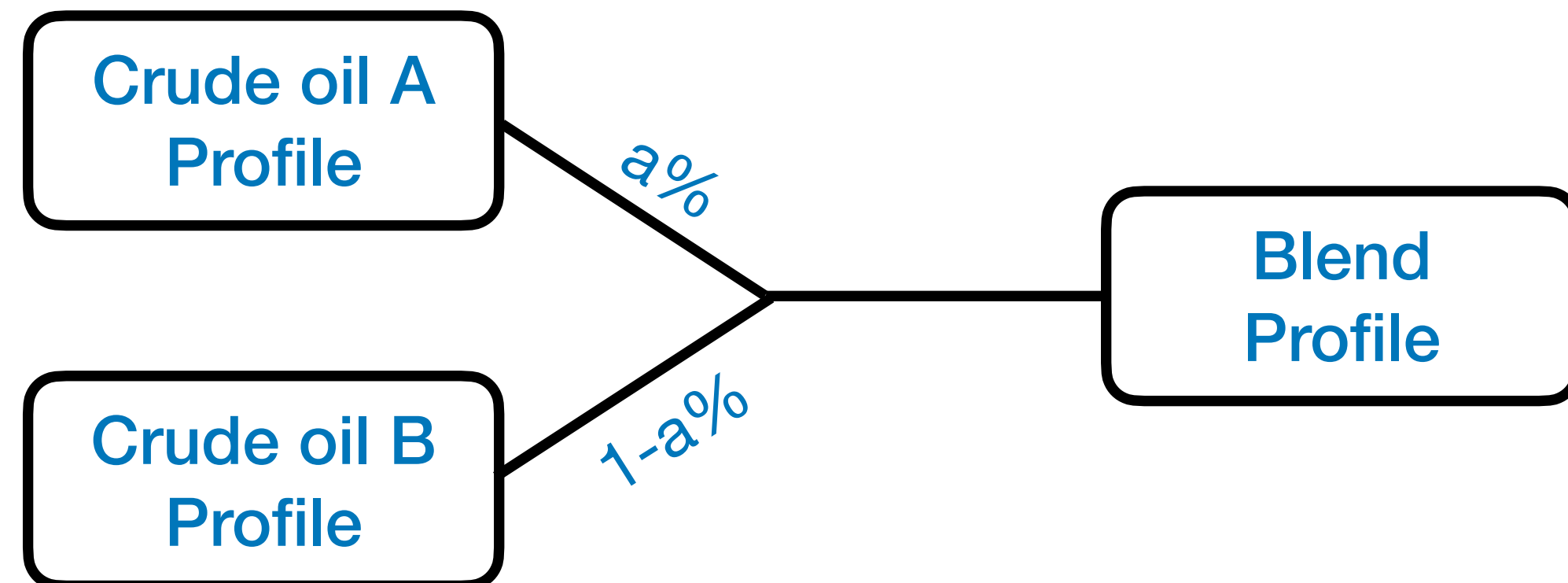
```
[(base) Anyangs-MacBook-Pro-2:Desktop anyangpeng$ python basemode.py  
[29.24, 51.52, 79.46, 141.4, 198.32, 251.6, 311.5, 376.4, 446.38, 524.74, 619.2, 685.2, inf]
```



# Machine Learning Approach

## Problem statement

- Input: 2\* List [float] + float
- Output: List [float]



# Machine Learning Approach

## Data

- ~5000 reports from the Crude Monitor database

<https://crudemonitor.ca/library/archives/batch/BDY/BDY090831.pdf>

**Crude:** Boundary Lake  
**Batch:** BDY-831

**Location:** Kamloops  
**SampleDate:** August 31, 2009

### Yield on Crude (Vol %)

	Observed	Past Avg	Std Dev
C4 and lighter (mass%)	1.8	1.8	0.3
Naphtha (C5 - 190°C)	-	22.8	2.3
Kerosine (190°C - 277°C)	-	17.7	0.7
Distillate (277°C - 343°C)	-	13.1	1.6
Gas Oil (343°C - 565°C)	-	31.5	1.8
Residue (565°C +)	-	13.1	1.9

### Distillation Information (°C)

% Off	Observed	Past Avg	Std Dev
IBP	-	32.4	5.5
1%	-	34.7	4.6
5%	-	87.7	10.9
10%	-	112.6	7.1
15%	-	137.3	6.0
20%	-	162.6	6.0
25%	-	188.0	7.2
30%	-	215.1	7.1
35%	-	240.0	7.1
40%	-	264.3	7.5
45%	-	290.0	8.1
50%	-	314.0	8.3
55%	-	339.8	9.8
60%	-	368.0	10.2
65%	-	397.7	10.6
70%	-	427.8	10.4
75%	-	460.3	11.7
80%	-	497.3	13.5
85%	-	543.2	18.5
90%	-	604.5	25.8
95%	-	668.1	32.0
98%	-	691.7	17.3
99%	-	696.7	2.2
100%	-	-	-
FBP	-	701.4	6.7
Residue (%)	-	5.35	1.93

# Machine Learning Approach

## Data

Web Scrape  
with  
Selenium

1 AWB100629  
2 AWB100527  
3 AWB100428  
4 AWB100323  
5 AWB100216  
6 AWB100122  
7 AWB091222  
8 AWB091122  
9 AWB091023  
10 AWB090920  
11 AWB090827  
12 AWB090723  
13 AWB090628  
14 AWB090616  
15 AWB090528  
16 AWB090516  
17 AWB090429  
18 AWB090415  
19 AWB090329  
20 AWB090315

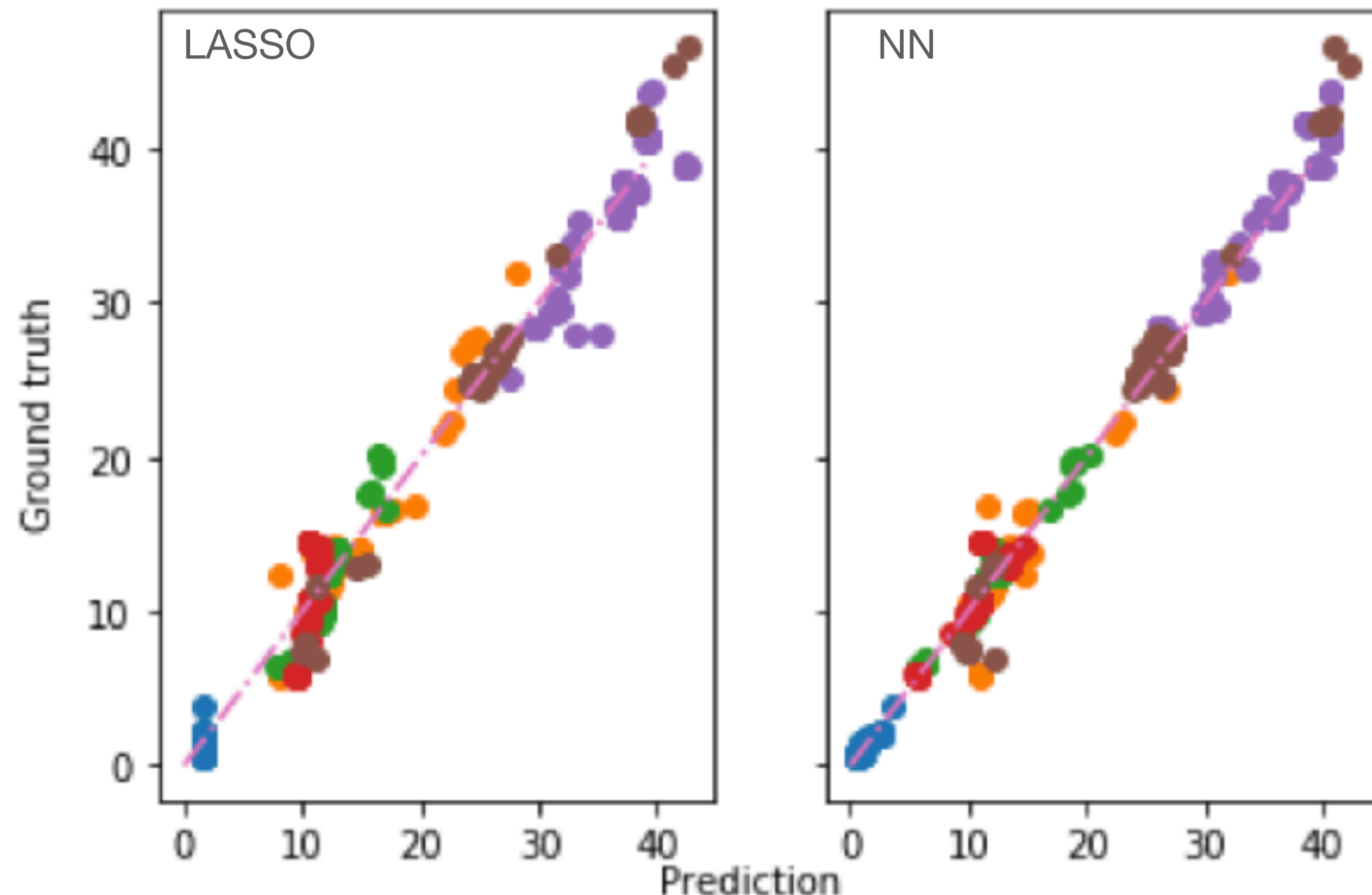
[https://crudemonitor.ca/library/  
archives/batch/BDY/BDY090831.pdf](https://crudemonitor.ca/library/archives/batch/BDY/BDY090831.pdf)

	Observed.1	Past Avg.1	Std Dev.1
[			
% Off			
IBP	2000	34.20	2.30
1%	2000	34.70	2.30
5%	2000	46.80	9.70
10%	2000	82.50	15.10
15%	2000	139.50	40.70
20%	2000	235.40	42.50
25%	2000	306.00	24.30
30%	2000	350.80	20.80
35%	2000	390.00	19.40
40%	2000	426.40	17.60
45%	2000	461.20	19.00
50%	2000	498.30	20.30
55%	2000	538.60	22.80
70%	2000	658.70	22.90
75%	2000	685.70	14.70
80%	2000	708.90	10.90
85%	2000	719.00	2000.00
90%	2000	2000.00	2000.00
95%	2000	2000.00	2000.00
98%	2000	2000.00	2000.00
99%	2000	2000.00	2000.00
100%	2000	2000.00	2000.00
FBP	2000	716.80	1.40
Residue (%)	2000	21.23	3.56,
		Obs	His
Std			
Composition			
C4 and lighter (mass%)	0.9	0.7	0.2
Naphtha (C5 - 190°C)	-	16.3	2.5
Kerosine (190°C - 277°C)	-	6.9	0.4
Distillate (277°C - 343°C)	-	6.0	0.3
Gas Oil (343°C - 565°C)	-	28.4	0.5
Residue (565°C +)	-	41.7	2.7]

# Machine Learning Approach

## Model A

- Use distillation profile to predict composition.
- Map the dataset from (500,22) to (500,6).



The real compositions from reprot are

- A: [3.9, 31.8, 16.6, 10.7, 24.9, 12.0]
- B: [0.7, 16.3, 6.9, 6.0, 28.4, 41.7]

Model Prediction

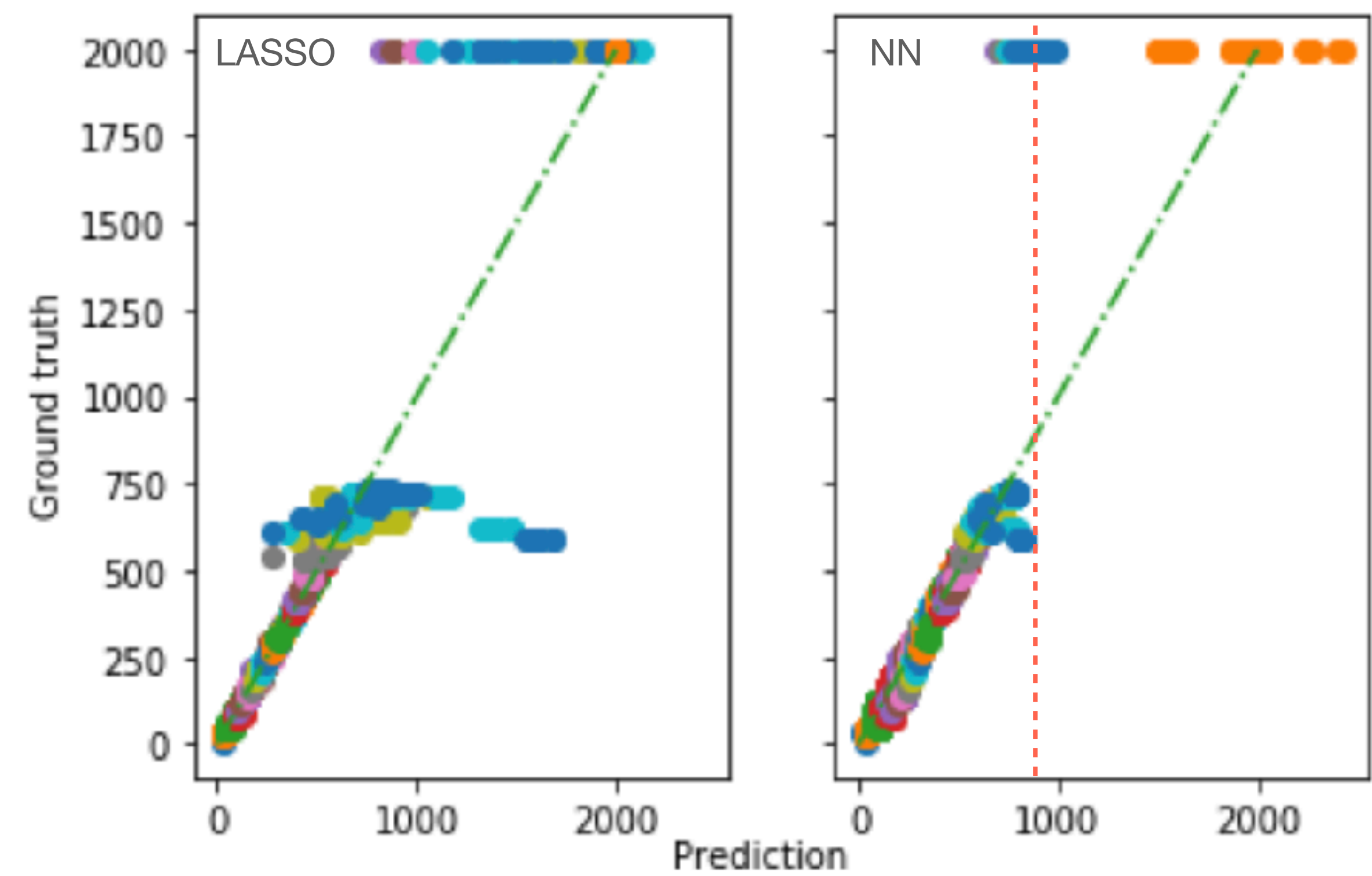
- A: [3.7, 31.0, 16.5, 11.0, 24.5, 11.6]
- B: [0.5, 15.1, 6.7, 6.2, 29.4, 40.4]



# Machine Learning Approach

## Model B

- Use composition to predict distillation profile.
- Map the dataset from (500,6) to (500,22).

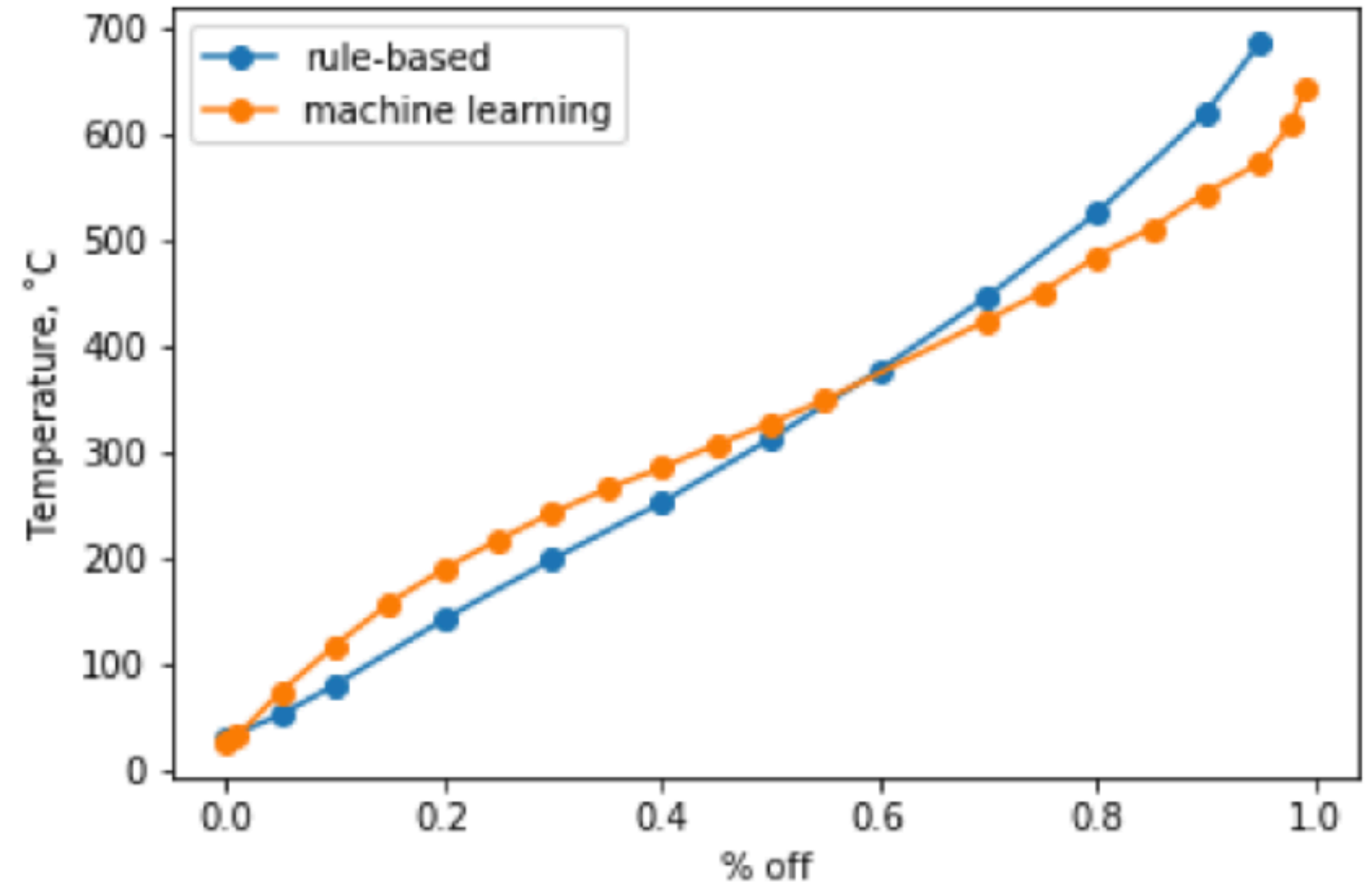


	Observed.1	Past Avg.1	Std Dev.1
[ % Off			
IBP	2000	34.20	2.30
1%	2000	34.70	2.30
5%	2000	46.80	9.70
10%	2000	82.50	15.10
15%	2000	139.50	40.70
20%	2000	235.40	42.50
25%	2000	306.00	24.30
30%	2000	350.80	20.80
35%	2000	390.00	19.40
40%	2000	426.40	17.60
45%	2000	461.20	19.00
50%	2000	498.30	20.30
55%	2000	538.60	22.80
70%	2000	658.70	22.90
75%	2000	685.70	14.70
80%	2000	708.90	10.90
85%	2000	719.00	2000.00
90%	2000	2000.00	2000.00
95%	2000	2000.00	2000.00
98%	2000	2000.00	2000.00
99%	2000	2000.00	2000.00
100%	2000	2000.00	2000.00
FBP	2000	716.80	1.40
Residue (%)	2000	21.23	3.56,
Obs His Std			
Composition			
C4 and lighter (mass%)	0.9	0.7	0.2
Naphtha (C5 – 190°C)	–	16.3	2.5
Kerosine (190°C – 277°C)	–	6.9	0.4
Distillate (277°C – 343°C)	–	6.0	0.3
Gas Oil (343°C – 565°C)	–	28.4	0.5
Residue (565°C +)	–	41.7	2.7]

# Results

## Comparison

- The rule-based model only provide a rough estimation of the distillation profile.
- The machine learning model seems to have much better performance.



# Uncertainties

## Dollar values

- Mostly two sources of uncertainties, from the data and from the model. The uncertainty on the data is provided in the distillation profile by standard deviations.
- We can try to estimate the uncertainties from the model by looking at the differences between predictions and ground truth values.

```
[2.6661078674044294,  
3.7853287583453232,  
20.804998521404688,  
30.627578859785025,  
33.540537474328026,  
30.219574970287837,  
29.818411406191093,  
30.46654935382515,  
30.646288539084285,  
29.953156852905387,  
28.231576679813745,  
25.90739039826376,  
23.870054884760066,  
19.383965422277242,  
nan,  
nan,  
nan,  
nan,  
nan,  
nan,  
nan,  
nan]
```



# Uncertainties

## Dollar values

How can we add dollar value to the error? Few facts before we make the estimation (in US\$):

- A barrel of crude oil is 42 gal, which can be made into ~20 gal gasoline (C4-C12 ), ~12 gal diesel fuel (C9-C25). Most of this product comes out below 350°C
- Refinery cost \$3 per barrel.
- Crude oil cost ~\$85 per barrel.
- Gasoline is ~\$4 per gal, diesel is ~\$6 per gal

Looking at the estimated error of the model (+- ~30°C), let's consider the case where we only collected products below 320°C (350-30=320), we could potentially lose about 10% of the product which is equal to  $(20 * 4 + 12 * 8) * 10\% = \$18$  per barrel. The error at a higher temperature may not be as important because most profitable products have come out already.