

filtration velocity :  $Q_e/A$  (m/min).  
 filtration time  $\rightarrow t_f$   
 for con

filtration area  $A = Q_e t_f / v_f$

capacity =  $V_G / \text{time}$ .  
 cleaning of Bag House  $\rightarrow$   
 i) Mechanical shaking  
 ii) pulse-jet bag filter  
 iii) Reverse jet bag filter.

$t_f$  - time of filtration

$t_c$  - time of cleaning

Maximum capacity =  $\frac{V_G}{t_f}$

Overall capacity =  $\frac{V_G}{t_f + t_c}$

for optimum capacity for design purpose  $t_f = t_c$ .

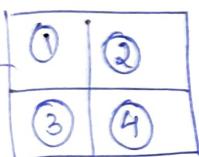
$t_c = 0$   
 for maxm capacity



→ Sizing of Bag  
no bag should be more than 3-4 times  
typical diameter 40-50 cm

### Guideline for Bag filter area in m<sup>2</sup>

<u>Area in (m<sup>2</sup>)</u>	<u>No. of compartments</u>
1 - 200	1-2
201 - 600	3 - 4
601 - 1000	5 - 7
1001 - 1600	8 - 10
1601 - 2200	11 - 13
2201 - 3000	14 - 16
3001 - 4100	17 - 20
> 4100	> 20



1, 3, 4, → working

minimum pressure drop - 30-40 cm of water column.

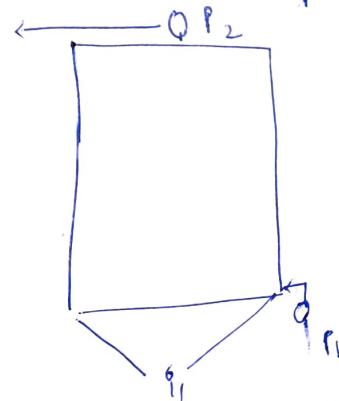
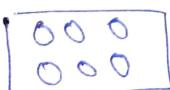
maximum pressure drop - 150 cm of water column.

cake is forming in bag filter - known by pressure drop  
choking of bag filter. → rupture of bag filter.

If pressure drop - 3-4 cm of water column.

→ If rupture of bag - replace the choked or ruptured bag.

$$N = \text{No. of bags.}$$



## constant rate filtration :-

$$\Delta P = B Q^2 t + C Q$$

at  $t=0$

$$\Delta P = CQ$$

$t=t$

$$\Delta P = BQ^2 t + CQ$$

$$Q = \frac{V_g}{t}$$

$t_f =$

rupture of bag (i) chocking of bag  
(ii) huge quantity of

Air to cloth ratio =  $\frac{Q}{\text{total filtration area of bag house}}$

1.2 to 2.5 m/min for pulse-jet bag filter.

If the air to cloth ratio is very small  $\rightarrow$  almost nothing.  
Max temp a bag filter withstand is  $280^\circ\text{C}$  by

## Properties of filter media:-

### Fibre:-

① Cotton

### Strength

strong

### Max temp

80

### Remarks

Not suitable  
for acidic  
dusts,

② Nylon

strong

100

easy to clean.

Excellent  
for abrasive  
material.

③ Polyester

strong

135

easy to clean.

④ Teflon

medium

260

expensive.

⑤ Glass fiber

strong

280

poor resistance to  
abrasive.

⑥ Nomex

strong

280

poor resistance to  
moisture.

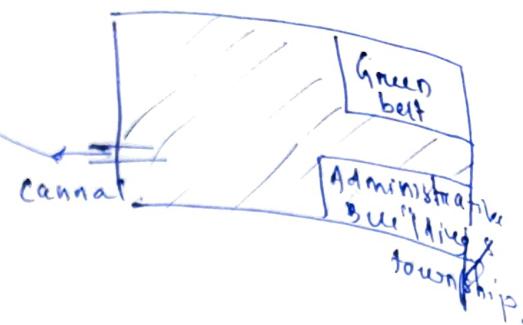
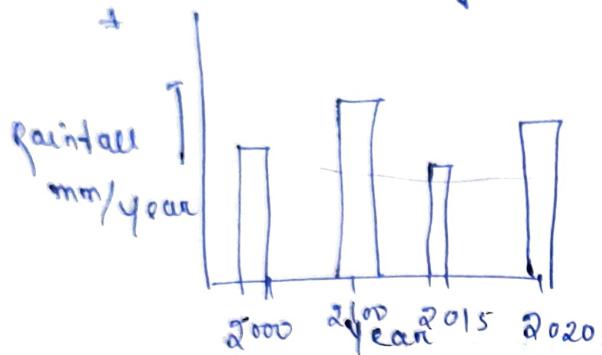
⑦ Nylon

18C class 13 Oct 2025 :-

## Surface runoff management:-

ETP

Zero liquid discharge



$$\text{Average rainfall} = \frac{\sum h_i}{\sum \text{Year}}$$

$$Q_s = \frac{\text{Area}}{(\text{m}^2)} \times \frac{h}{(\text{m})} \times \text{Co. efficient.}$$

$$\text{water demand} = Q_D - Q_T - Q_s$$

$$ETP = 200 \text{ m}^3/\text{hr.}$$

$$Q_D = 4000 \text{ m}^3/\text{hr.}$$

↓

$$50 \text{ m}^3/\text{hr}$$

Type

Area

$T_1$

$A_1$

$T_2$

$A_2$

$$\sum A_i = \text{Area.}$$

$T_3$

$A_3$

$T_n$

$\vdots$

Surface runoff calculation:-

Rational method

$$Q = C_i i A$$

$Q$  = Peak rate of runoff  $\text{m}^3/\text{day}$

$C$  = Runoff coefficient

$i$  = Av. intensity of rainfall in  $\text{mm/day}$ .

$A$  = water shed area in  $\text{Acre}$ .

$$C_{eq} = \frac{A_1 C_1 + A_2 C_2 + A_3 C_3 + \dots}{A_1 + A_2 + A_3 + \dots}$$

$A_1, A_2, A_3 \dots$  the area of different land type

$C_1, C_2, C_3 \dots$  corresponding runoff coefficient for these land types

This weighted average approach ensure that the varied soil cover condition are accurately represented in the runoff calculation.

Example:-  
Surface description C-value

Asphalt and concrete  $0.70 - 0.95$

Roof  $0.75 - 0.95$

woodland

$0.05 - 0.25$

sandy soil, flat  $0.05 - 0.10$

heavy soil, flat  $0.13 - 0.17$

Total rainfall on yearly basis.

Year	Rainfall mm
------	-------------

April 2019 - March 2020	1989
-------------------------	------

April 2020 - March 2021	1920
-------------------------	------

April 2021 - March 2022	2287
-------------------------	------

April 2022 - March 2023	1575
-------------------------	------

April 2013 - March 2019 - 1122

Total  
average

8894

1179

Yes

i value

$$i = 1222 \text{ min}$$

$$= 1.2 \text{ m}$$

~~1.2 m~~

### Mitigation Measures:

- \* Pond sizing Based on Peak discharge  $\Rightarrow$  The calculated Peak discharge during monsoon month helps to determine the required volume of ponds or reservoir.

Q

An old Bag filter from a discontinuous process is to be utilized for constant pressure filtration at  $0.2 \text{ cm/s}$  of water column the bag house has 20 bags of  $432.24 \text{ cm}^2$  each. Cleaning time of bag  $\Rightarrow$  determined as 45 min, for the given pressure filtration, the following expression can be used

$$t = 674.82 V_g^2$$

$t = \text{time, min}$

$V_g$  - volume of gas filter. ( $\text{m}^3/\text{cm}^2$ )

determine the maximum capacity of the bag house & overall capacity of bag house under the given wind.

$$\text{Maximum capacity} = \frac{V_g}{t_f}$$

$$t_f = t_c$$

total surface area :-

$$\text{total surface area} = 7432.24 \times 20 \\ = \underline{148644. \text{ cm}^2}$$

$$t_f = 674.82 V_y 2 \\ = 14.86 \text{ m}^2$$

$$= 14.86 \text{ m}^2$$

$$V_y = 0.258 \text{ m}^3/\text{cm}^2$$

$$\text{maxm capacity} = \frac{V_y}{t_f} \\ = \frac{0.258}{14.86} \text{ m}^3 \\ = \frac{38350 \text{ m}^3}{95 \text{ min}} \\ = 51133.81 \text{ m}^3/\text{hr}$$

$$t_f = 45 \text{ min} \\ = \underline{3.83 \text{ m}^3}$$

overall capacity :-

$$V_y/t_f t_c = \frac{38350.358 \text{ m}^3}{90 \text{ min}}$$

$$t_f t_c = 90 \text{ min} \\ = 255.66.90 \text{ m}^3/\text{hr}$$

Q1.04 X 0.2529 x 300000

Q1.04 A filter is operating at constant rate on an optimum cycle. The filtration equation is given by

$$V_y^2 = 2.623 \times 10^6 \times t \times P^{0.65}$$

$P$  = cm of water column

$V_y$  = m<sup>3</sup> of gas filtered

$t$  = time of filtration, in min.

The filtration time is 45 mins and cleaning time is 8 min the maximum allowable pressure is 10.16 cm of H<sub>2</sub>O column.

Pressure is 10.16 cm of H<sub>2</sub>O column.

calculate i) max<sup>m</sup> overall capacity of bag house  
 ii) It is necessary to increase the capacity of bag house it has suggested that by additional unit identical to the present one take installed. both bag filter would work from the same 1B hrs ~~is~~ which has ample capacity and the filtration to be carried out at the same max<sup>m</sup> pressure as at present. The time required to save and clear two bag houses is estimated as 4 min. What is the % increase in the overall capacity that could be attained by adapting this cond?

$$\text{max}^m \text{ capacity} = V_g / t_f$$

$$V_g^2 = 2.623 \times 10^6 \times t \times P^{0.65}$$

$$= 2.623 \times 10^6 \times \frac{45}{60} \text{ min} \times 10.16$$

$$V_g^2 =$$

$$\Rightarrow V_g = 23080.53 \text{ m}^3$$

$$\text{max}^m \text{ capacity} = \frac{23080.53 \text{ m}^3}{45/60 \text{ hr}}$$

$$= 30774.04 \text{ m}^3/\text{hr}$$

$$\text{overall capacity} = \frac{23080.53}{45+8/60} = 26128.909 \text{ m}^3/\text{hr}$$

(01)

Overall capacity of two bag

$$2 \times 23080.534$$

$$\cancel{4574/60}$$

$$56523.758 \text{ m}^3/\text{hr.}$$

$$\cancel{28261.87 \text{ m}^3/\text{hr.}}$$

$$56523.758 - \cancel{28261.87} \times 100$$

1. increase =  $\frac{28128.909}{28128.909} \times 100$

$$= 116.328\%$$

Q A bag house is to construct using bags of  $30\text{cm}$  in diameter and  $6\text{m}$  long. The bag gas enter the bag house and  $36000 \text{ m}^3/\text{hr}$  the filter velocity has been determined  $2 \text{ m}/\text{min}$  calculate no. of bags required for a continuous operation of bag house.

$$\text{Area of bag} = \frac{30\text{cm} \times 30\text{cm}}{1.80 \text{ cm}^2} = 1.8 \text{ m}^2$$

$$\text{filtration velocity} = 2 \text{ m}/\text{min}$$

$$\text{filtration velocity} = 2 \text{ m}/\text{min}$$

The gas enter:  $36000 \text{ m}^3/\text{hr}$

$$\Rightarrow \frac{36000 \text{ m}^3/\text{hr}}{2 \text{ m}/\text{min}/60 \text{ hr}} = \frac{36000 \text{ m}^3/\text{hr}}{2 \times 60 \text{ m}/\text{hr}} = \frac{300}{2} = \frac{3000}{20} = 300 \text{ m}^3$$

$$\text{Area of bag} = \frac{\pi D^2}{4} + \pi \times 0.3 \times 6$$

$$\text{Area of bag} = \frac{\pi D^2}{4} + \pi \times 0.3 \times 6$$

## Klasse waden :- 2/act

IPC Wet - Scrubbers (control of particulate & gaseous pollutant)

$\text{SO}_2$        $\text{HCl}$   
 $\text{NH}_3$       acid mist  
 $\text{H/C}$   
 $\text{CO}$   
 $\text{H}_2\text{S}$

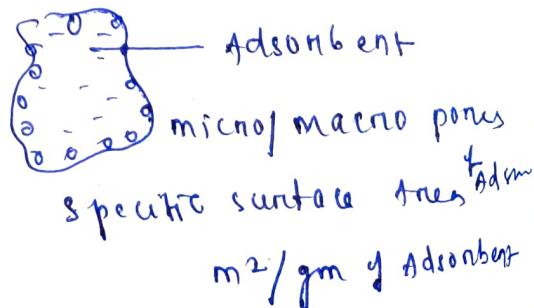
}      not used ESP for baghouse  
 Gravity settling chamber  
 cyclone

Adsorber

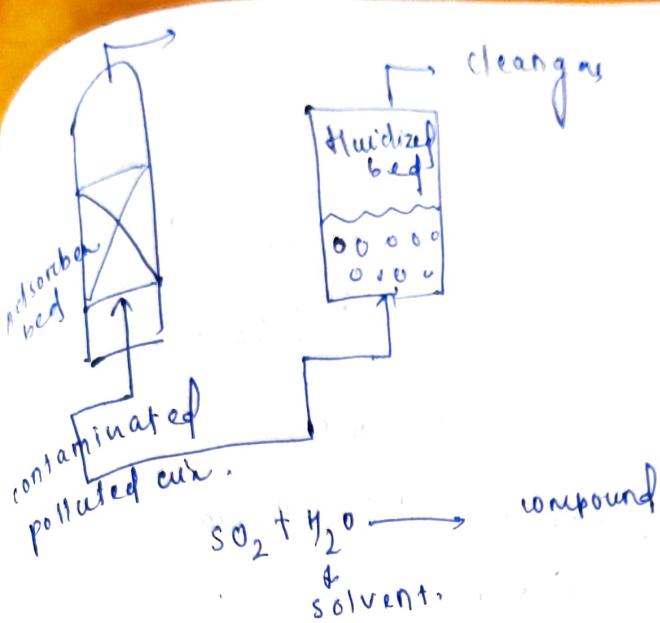
Adsorption (wet scrubber).

## Gaseous pollutants

- Adsorption
- Absorption
- Condensation
- Combustion.



Adsorption Capacity  
 $\text{mg/gm of Adsorbent}$



### wet scrubber

- transfer pollutant from air to water
- further treatment may be necessary
- pollutant must be slightly soluble in water.
- for less soluble material (a chemical may be added to water)
- SO<sub>2</sub> may be removed by reacting with lime stone.
- in pollution control gases and vapors
- SO<sub>2</sub>, NO<sub>x</sub>, VOCs, HAPS, CO

### slurries

wet scrubber advantages | Disadvantages

### wet collectors

#### Bag filter problem

- It is required to remove the dust from an iron ore grinding plant. The gas flows from the mill at 45°C, 31.680 m<sup>3</sup>/hr. The gas filtering velocity 1.5 m/min determine the cloth area required to process if the diameter of bag is

20cm and length is 5m how many bags will be required for continuous cleaning of bags for unit.

flow rate ( $Q$ ) =  $31680 \text{ m}^3/\text{hr}$   
 $= 31680 / 60 = \dots$  please

filtrating velocity = 1.5 m/min.

Diameter of bag = 20cm = 0.2m.

length = (1) 5m.

total cloth

$$Q/A_c = v$$

total cloth Area  $\Rightarrow A_c = Q/v = \frac{528 \text{ m}^3/\text{min}}{1.5 \text{ m/min}}$

$A_c = 352 \text{ m}^2$

$$A_c = N \times (\pi \times D \times l + \pi/4 D^2)$$

$$N \times (3.14 \times 0.2 \times 5 + 3.14/4 (0.2)^2)$$

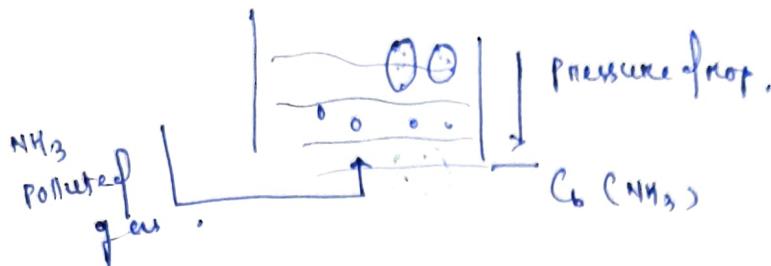
352  
Area of cloth  
100% loss  
100% loss

$$N = 110.9 \text{ bags}$$

$$= 111 \text{ bags}$$

growth of movie  
gauge consumed  
single movie = 1000 m

$$\text{Removal} = K_{\text{overall}} (C_b - C_f)$$

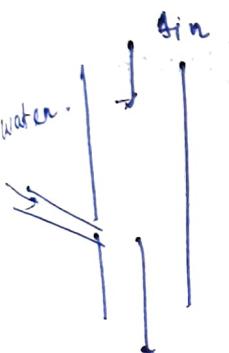


$C_f$  - final conc.

$$\text{Removal} = K_{\text{overall}} (C_b - C_f) = k_1 a (\Delta C)$$

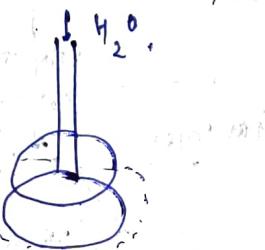
$a$  = interfacial area of contact.

$$a = (m^2/m^3)$$



by changing  $a$  we can change the scrubber.

gandu  
ra

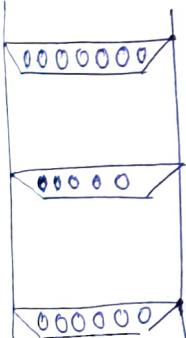


Rotating plate droplet generator.

Spray tower -  $70-78\%$  removal  
but pressure drop is high  
so useful.

cyclonic scrubber

6912 80% 60%?



0+ 28/10/25

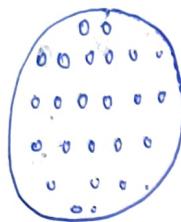
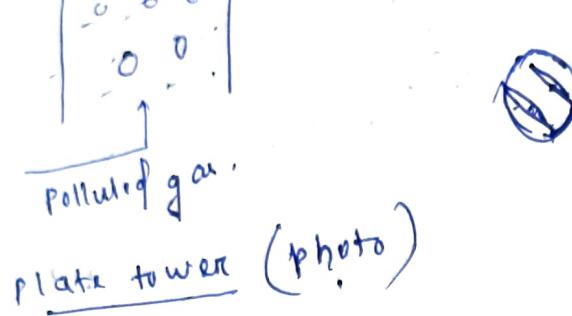
photos

particulate (photos)

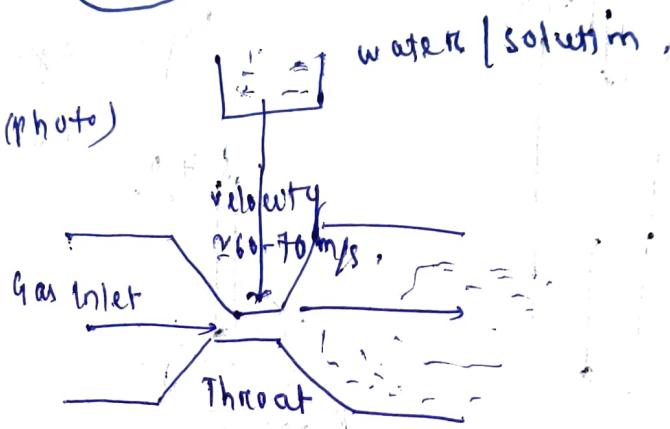
Design the wet scrubber;

Spray tower (photo review)

droplet size distribution - spray tower.



not used for industrial purpose.



Packed tower

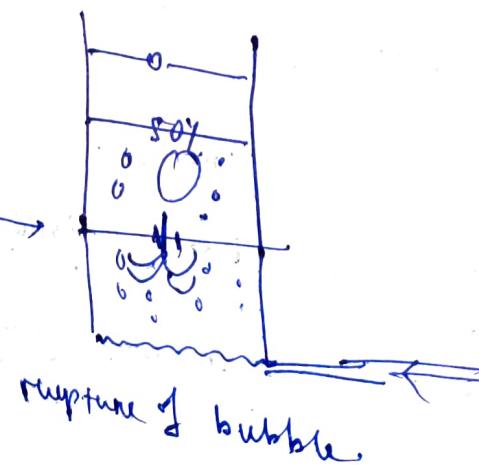
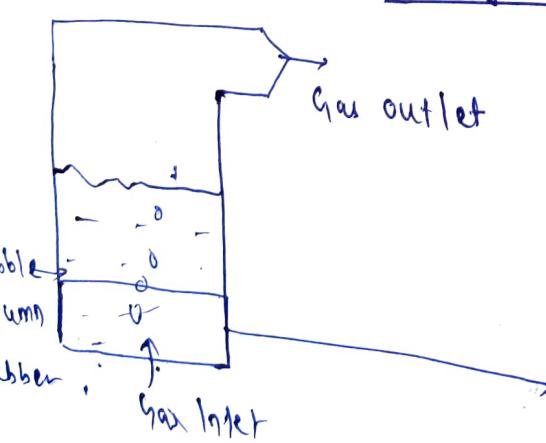
Spray tower

① Working principle of all

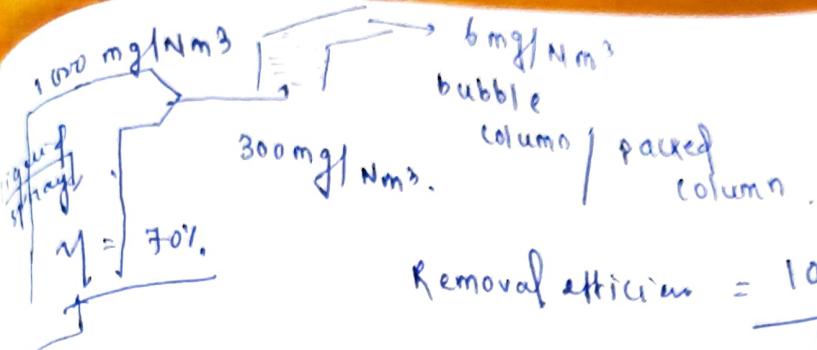
② design- packed, spray, plate

③ You develop design problem yourself.

Handbook by parry



Air/gas

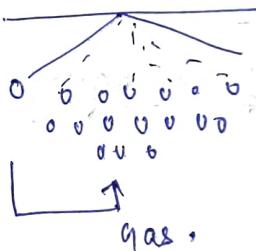
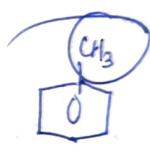
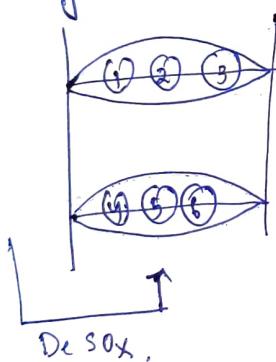


20 June

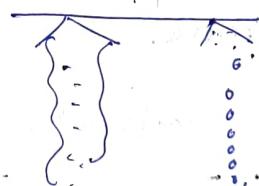
$$\text{Removal efficiency} = \frac{1000 - 6}{1000} \times 100.$$

Q A sulphuric acid manufacturing plant emitting  $\text{SO}_2$ . Exhaust stream of the plant contain mainly  $\text{SO}_2$  about 15% by volume and carrier gas.

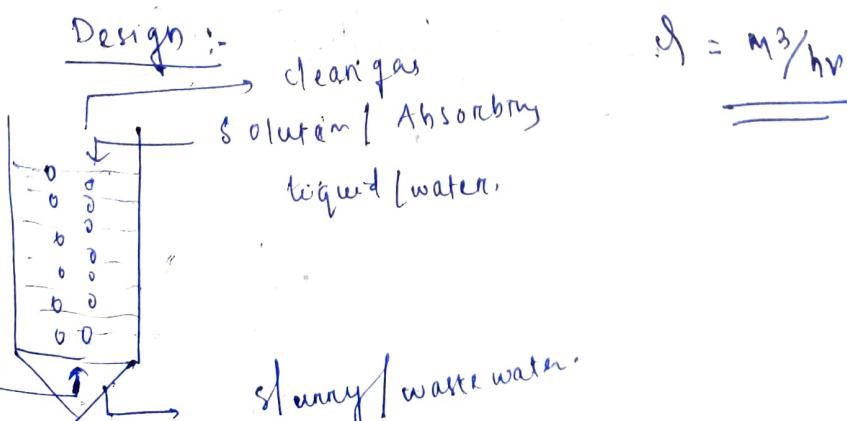
Monday 2.11.25. scrubber:-



Type of nozzle



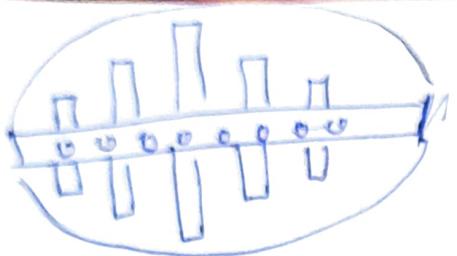
Scrubber Nozzles:-



$$Q = \text{m}^3/\text{hr}$$

====

large q = less

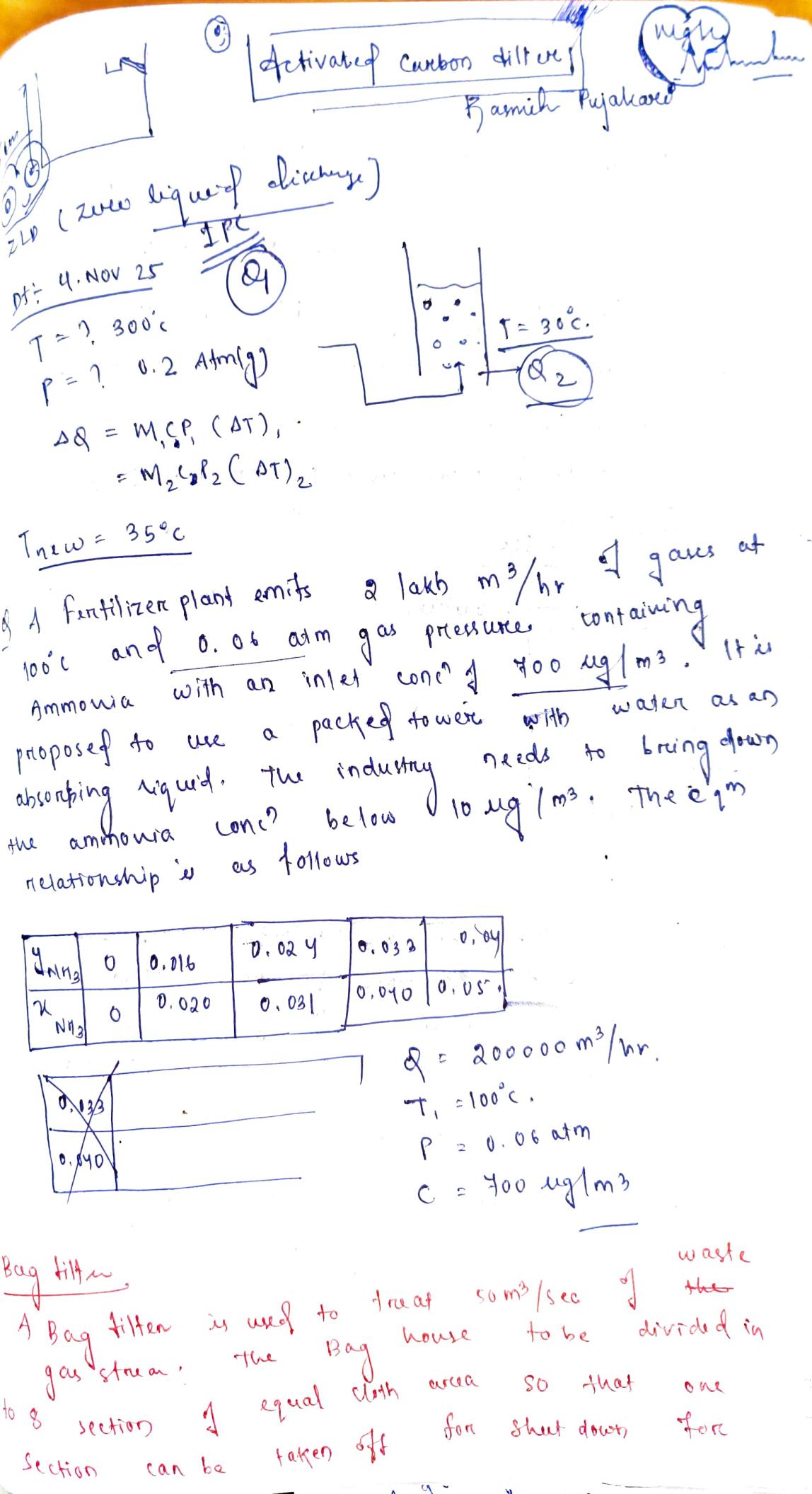


*Diagram*

Q A gas holder is operating at a constant gas rate for 30 min during which  $70.8 \text{ m}^3$  of gas from a unit will operate is processed. The initial & final pressure drop of the unit is  $10.16 \text{ mm}$  of water column  $\times 101.6 \text{ mm}$  of water column respect - If the unit is further operated for 1 hr at the final pressure calculate the quantity of additional gas which can be treated by this unit.

$$Q = \dots \text{ or } m =$$

*from  
note  
book*



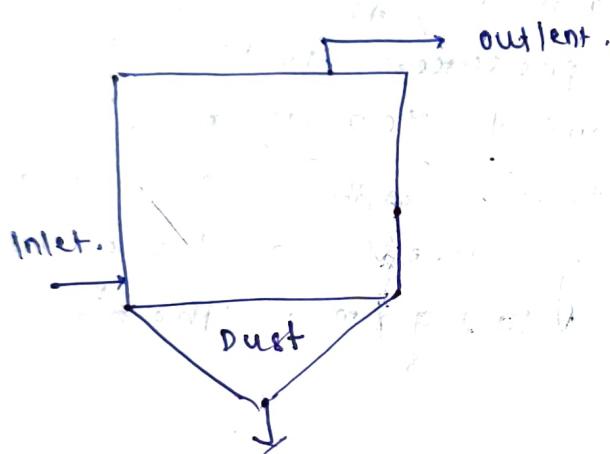
Cleaning & maintenance of other remaining in working cond'. The gas to cloth area ratio  $9 \text{ m}^3/\text{min}/\text{m}^2$  is used which provide sufficient surface area for the cleaning of the flow gas.

The bags are 25 cm diameter & 7 m long. Calculate the No of bags & physical arrangement required ~~for~~ to above meet the above requirement.

→ 8 section.

→ 7 used & one used by stand by mode

$$Q = 50 \text{ m}^3/\text{sec}$$



Q An old Bag filter from a discontinued process is to be utilised for constant pressure filtration at 120 mm of water, the filter has 40 bags of  $6000 \text{ cm}^2$  each. The filtration time is given as 50 min & filtration eq<sup>n</sup> is  $A_f = 674.85 V_h^2$

where  $V_h$  = volume of gas filtered per unit area in  $\text{m}^3/\text{sec}^2$

$t$  = time in min

calculate overall capacity of the bag filter under given cond?

ii) max<sup>m</sup> overall capacity

- iii) If another three, <sup>addition</sup> identical old bug houses are installed to increase the capacity what is max?
- 4). increase in the overall capacity for new arrangement  
Assume total cleaning time with new arrangement  
is 20 min.

ANSWER