

# **Process Design & Development**

## **Energy Balance**

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# Role of Energy Balance Concept

Energy balance is crucial in project engineering for designing systems such as reactors, heat exchangers, and distillation units. It ensures optimal energy utilization, system efficiency, and safety. When chemical reactions are involved, the system's energy balance must account for reaction enthalpies in addition to physical energy changes.

# Energy Balance Without Chemical Reaction

This applies to systems where there is no chemical transformation. It primarily deals with heat transfer, work, and changes in sensible or latent heat.

**General Energy Balance Equation:**

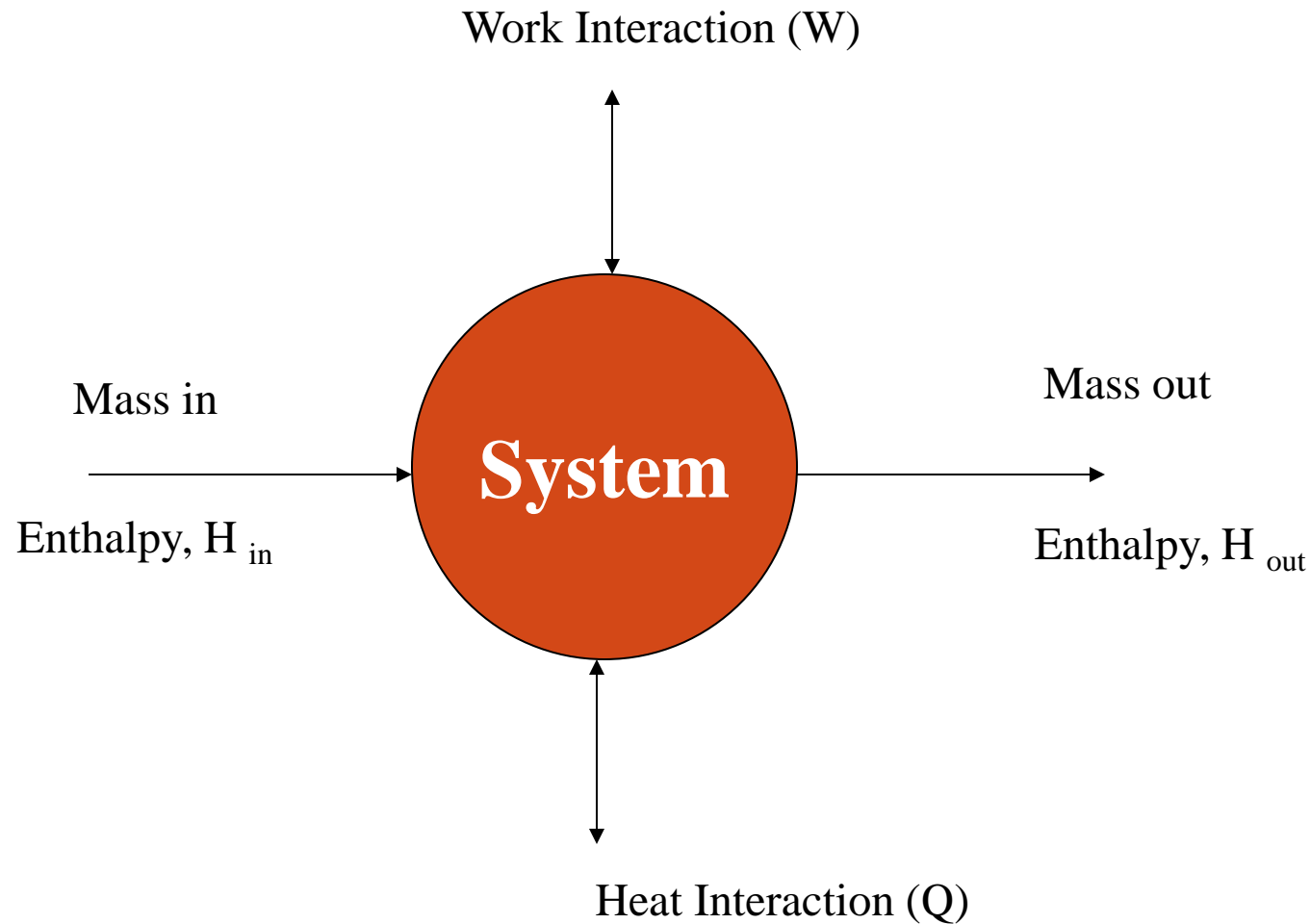
$$\Delta H + \Delta KE + \Delta PE = Q - W$$

- $\Delta H$ : Enthalpy change due to heating/cooling.
- $\Delta KE$ : Change in kinetic energy.
- $\Delta PE$ : Change in potential energy.
- $Q$ : Heat transfer to/from the system.
- $W$ : Work done by/on the system.

# Forms of energy

- Potential energy (P.E) =  $(mgh)$
- Kinetic energy (K.E) =  $(1/2 mv^2)$
- Thermal energy – heat (Q)
  - $Q = -ve$ , removed from a process
  - $Q = +ve$ . supplied to a system
- Work energy – e.g. work done by a pump (W) to transport fluids
  - $W = -ve$ , Work done by the system
  - $Q = +ve$ . Work done on the system
- Internal energy (U) of molecules

# Energy balance



# Steady state/non-steady state

- Non steady state - accumulation/depletion of energy in system

- Closed system

$$\Delta U = Q + W$$

- Open system

$$\Delta H + \Delta P.E + \Delta K.E = Q + W$$

$$\Delta H + \frac{\Delta u^2}{2} + g \Delta z = Q + W_s$$

## Enthalpy balance

- P.E, K.E, W terms = 0
- $Q = H_2 - H_1$  or  $Q = \Delta H$

where

$H_2$  = the total enthalpy of output streams and

$H_1$  = the total enthalpy of input streams,

$Q$  = the difference in total enthalpy i.e. the enthalpy (heat) transferred to or from the system

# Enthalpy changes

- Change of T at constant P
- Change of P at constant T
- Change of phase
- Solution
- Mixing
- Chemical reaction
- Crystallisation



# Latent heats (phase changes)

- Vaporization (L to V)
- Melting (S to L)
- Sublimation (S to V)

# Mechanical energy balance

- Consider mechanical energy terms only
- Application to flow of liquids
- $\frac{\Delta P}{\rho} + \frac{\Delta v^2}{2} + \Delta h + h_{fs} = W$

where

$W$  is work done on system by a pump and

$h_{fs}$  is frictional energy loss in system (J/kg)

$$\Delta P = P_2 - P_1; \Delta v^2 = v_2^2 - v_1^2; \Delta h = h_2 - h_1$$

• Bernoulli equation ( $P=0$ ,  $W=0$ )

# Sensible heat/enthalpy calculations

- ‘Sensible’ heat – heat/enthalpy that must be transferred to raise or lower the temperature of a substance or mixture of substances.
- Heat capacities/specific heats (solids, liquids, gases, vapours)
- Heat capacity/specific heat at constant P,  $C_p(T) = dH/dT$  or  $\Delta H = \int C_p(T) dT$  between limits  $T_2$  and  $T_1$
- Use of mean heat capacities/specific heats over a temperature range
- Use of simple empirical equations to describe the variation of  $C_p$  with  $T$

e.g.  $C_p = a + bT + cT^2 + dT^3$   
, where a, b, c, d are coefficients

$\Delta H = \text{integral } C_p dT \text{ between limits } T_2, T_1$

$$\Delta H = [aT + \frac{bT^2}{2} + \frac{cT^3}{3} + \frac{dT^4}{4}]$$

Calculate values for  $T = T_2, T_1$  and subtract

Note: T may be in deg cent or K - check units for  $C_p$ !

## **Example** Heating Water in a Heat Exchanger Problem:

In a heat exchanger, 500 kg/hr of water is heated from 25°C to 75°C. Calculate the required heat (Q) if the specific heat capacity of water (Cp) is 4.18 kJ/kg·°C.

**Solution:**

$$1. \Delta H = m \cdot C_p \cdot \Delta T$$

$$\Delta T = T_2 - T_1 = 75 - 25 = 50^\circ\text{C}$$

$$Q = 500 \text{ kg/hr} \cdot 4.18 \text{ kJ/kg}^\circ\text{C} \cdot 50^\circ\text{C}$$

## Example 2

Calculate the enthalpy required to heat a stream of nitrogen gas flowing at 100 mole/min., through a gas heater from 20 to 100 deg. cent.

(use mean  $C_p$  value  $29.1 \text{ J mol}^{-1} \text{ K}^{-1}$  **or**  $C_p = 29 + 0.22 \times 10^{-2}T + 0.572 \times 10^{-5}T^2 - 2.87 \times 10^{-9}T^3$ , where  $T$  is in deg cent)

# Energy Balance With Chemical Reaction

When chemical reactions occur, the system must account for the energy released or absorbed during the reaction ( $\Delta H_r$ ).

**General Energy Balance Equation:**

$$\Delta H + \Delta KE + \Delta PE + \Delta H_r = Q - W$$

**Where:**  $\Delta H_r$  : Enthalpy of reaction, which depends on the extent of the reaction ( $\xi$ ) and the reaction enthalpy.

- $\Delta H$ : Enthalpy change due to heating/cooling.
- $\Delta KE$ : Change in kinetic energy.
- $\Delta PE$ : Change in potential energy.
- $Q$ : Heat transfer to/from the system.  $W$ : Work done by/on the system.

# Example – change of phase

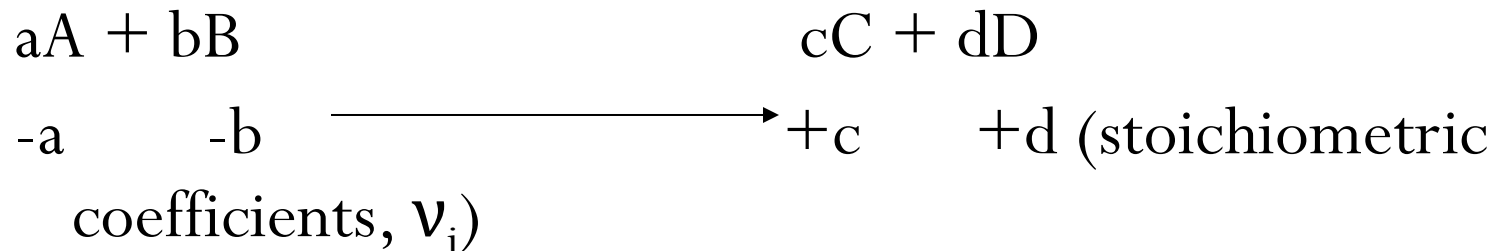
A feed stream to a distillation unit contains an equimolar mixture of benzene and toluene at 10 deg cent. The vapour stream from the top of the column contains 68.4 mol % benzene at 50 deg cent. and the liquid stream from the bottom of the column contains 40 mol% benzene at 50 deg cent.

[Need  $C_p$  (benzene, liquid),  $C_p$  (toluene, liquid),  $C_p$  (benzene, vapour),  $C_p$  (toluene, vapour), latent heat of vapourisation benzene, latent heat of vapourisation toluene.]



# Energy balances on systems involving chemical reaction

- Standard heat of formation ( $\Delta H^\circ_f$ ) – heat of reaction when product is formed from its elements in their standard states at 298 K, 1 atm. (kJ/mol)



$\Delta H^\circ_{fA}, \Delta H^\circ_{fB}, \Delta H^\circ_{fC}, \Delta H^\circ_{fD}$  (heats of formation)

$$\Delta H^\circ_R = c \Delta H^\circ_{fC} + d \Delta H^\circ_{fD} - a \Delta H^\circ_{fA} - b \Delta H^\circ_{fB}$$

# Heat (enthalpy) of reaction

- $\Delta H^\circ_{\text{R}}$  -ve (**ex**othermic reaction)
- $\Delta H^\circ_{\text{R}}$  +ve (**endo**thermic reaction)

# Enthalpy balance equation - reactor

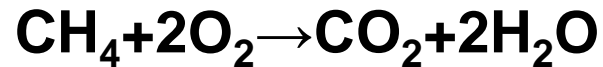
$$Q_p = H_{\text{products}} - H_{\text{reactants}} + Q_r$$

$Q_p$  – heat transferred to or from process

$Q_r$  – reaction heat ( $\zeta \Delta H^\circ_R$ ), where  $\zeta$  is extent of reaction and is equal to [moles component, i, out – moles component i, in] /  $\nu_i$

## Example3: Methane Combustion in a Reactor

Methane ( $\text{CH}_4$ ) is combusted with excess air in a reactor. The reaction is:



Given: 5 mol of  $\text{CH}_4$  reacts; Heat of reaction ( $\Delta H_r$ ) =  $-890 \text{ kJ/mol}$

- Calculate the total heat released.

**Solution:**

1. Total moles of methane reacting:  $\xi = 5 \text{ mol}$

2. Total heat released:  $Q = \xi \cdot \Delta H_r = 5 \cdot (-890) = -4450 \text{ kJ}$

# References

- *The Properties of Gases and Liquids*, R. Reid
- *Elementary Principles of Chemical Processes*, R.M.Felder and R.W.Rousseau

Thank you