## INDIAN INSTITUTE OF TECHNOLOGY KHARAGPUR

## Mid-Spring Semester Examination 2022-23

Date of Examination: 22/02/2023.	_ Session: (FN/AN) ANDuration: 2 hrs. Full Marks: 30
Subject No.: CH21204	Subject: Heat Transfer
Department/Center/School: Chemical Engineering _	
Specific charts, graph paper, log book etc., required	
Special Instructions (if any):	

1. Assume a fluid is flowing over an isothermally flat plate. If the free-stream velocity of the fluid is doubled (flow is still laminar), then estimate the change in the drag force on the plate and the rate of heat transfer between the fluid and the plate.

(3+3=6)

For the lancinar flow of a fluid over a flat blate maintained at a constant temperature the drag force is given by:

$$F_{D1} = GA_S \frac{9V_0^2}{2} \text{ where } G = \frac{1.328}{\sqrt{Re}}$$
Therefore,

$$F_{D1} = \frac{1.328}{\sqrt{Re}} A_S \frac{9V_0^2}{2}$$
Substituting Reynolds number relation, we get,

$$F_{D1} = \frac{1.328}{\sqrt{Ne}} A_S \frac{9V_0^2}{2} = 0.664 (\frac{1.8V_0}{2})^{\frac{3}{2}} A_S \frac{9}{\sqrt{10}}$$
When the free stream relocity of fluid is about el, the nuovalue of the drag force on the plate becomes

$$F_{D2} = \frac{1.328}{(2V_0)L} A_S \frac{9(2V_0)}{2} = 0.664(2V_0)^{\frac{3}{2}} A_S \frac{90S}{2}$$
The ratio of drag forces corresponding to  $V_{00}$  and  $V_{00}$  is, 
$$F_{D2} = \frac{(2V_0)^{\frac{3}{2}}}{V_0} = \frac{3}{2}$$
For change in hate of heat transfer between the fluid and the plate,

$$Q_1 = hA_S(T_S - T_0) = (\frac{4}{2}L_1 N_1L_2) A_S(T_S - T_0)$$

$$= \frac{1.9664}{L} \frac{V_00}{L} \frac{K}{L} P_1 V_2 A_S(T_S - T_0)$$

$$= 0.664 \sqrt{V_00} \frac{K}{L} P_1 V_2 A_S(T_S - T_0)$$

when the free stream velocity of the fluid is aboutled, the new value of the heat transfer rate between the fluid and the folate becomes

then the vation is,

$$\frac{\dot{Q}_2}{\dot{Q}_1} = \sqrt{\frac{2 v_{\infty}}{v_{\infty}}} = \sqrt{2}$$

2. Air at 20 °C is flowing at 15 m/s over an isothermally heated plate (0.5 m length X 0.5 m width, k = 0.0292 W/m K), maintained at 110 °C. What are the average heat transfer coefficient and the total amount of transferred heat? What are h,  $\delta_t$ , and  $\delta$  at the trailing edge? Consider, Pr = 0.7, and  $\nu$  = 0.0000195 m²/s of air at 65 °C.

We evaluate the properties at 
$$T_{4} = \frac{110+20}{2} = 65^{\circ}$$
  
Then,  $Pr = 0.7$   
 $Re_{L} = \frac{U_{00}L}{7} = \frac{15 \times 0.5}{0.0000195} = \frac{384600}{2} 384615$   
 $NU_{K} = 0.332 Re_{V}^{V2} Pr^{V/3}$ ; for  $Pr_{V}$ ,  $O.6$   
 $NU_{L} = 0.664 Re_{L}^{V2} Pr^{V/6} = \frac{hL}{K}$ ; for  $Pr_{V}$ ,  $O.6$   
 $NU_{L} = 0.664 \times Re_{L}^{V2} \times Pr^{V/3}$   
 $= 0.664 \times (384615)^{V2} \times (0.7)^{V3}$   
 $= 365.67 \frac{K}{L} = \frac{365.67 \times (0.292)}{2}$   
 $\therefore R = 365.67 \frac{K}{L} = \frac{365.67 \times (0.0292)}{2} = 10.67 \frac{W}{m^{2}} \times (0.5)^{2} \times (0$ 

$$S_{t} = \frac{8}{3\sqrt{Pr}} = \frac{3.97 \times 10^{-3}}{3\sqrt{0.7}} = 4.47 \times 10^{-3} = 4.47 \times 10^{-3}$$

3. In case of laminar flow over an isothermal flat plate, the local Nusselt number (Nu) for the entire range of Prandtl number (Pr) is given by:

$$Nu_x = \frac{0.339 \text{ Re}_x^{1/2} \text{ Pr}^{1/3}}{\left[1 + (0.0468/\text{Pr})^{2/3}\right]^{1/4}}$$

Derive the expression for the average Nu for a laminar boundary layer over that plate for the identical condition.

(4)

$$Nu_x = A Re_x^{1/2}$$

where A = 
$$\frac{0.339 \text{ Pr}^{1/3}}{[1+(0.0468/\text{Pr})^{2/3}]^{1/4}}$$

Furthe, we know that  $q_x = \frac{k \Delta T}{x} N \mathbf{u}_x$ .

Now, integrating  $q_x$  over the length of the flat plate, we get

$$\overline{q}_{L} = \frac{k \, A \, \Delta T}{L} \int_{0}^{L} \sqrt{\frac{u_{\infty} x}{v}} \frac{1}{x} dx$$

$$\Rightarrow \overline{q}_L = \frac{2 k A \Delta T}{L} \sqrt{\frac{u_{\infty} L}{v}}$$

$$\Rightarrow \overline{q}_L = \frac{2 \ k \ \text{A} \ \Delta T}{L} \text{Re}_L^{1/2}$$

Therefore, the average Nusselt number:

$$\overline{Nu}_L = \frac{\overline{q}_L L}{k \Delta T}$$

$$\Rightarrow \overline{\mathrm{Nu}}_L = 2 \,\mathrm{A} \,\mathrm{Re}_L^{1/2}$$

$$\Rightarrow \overline{\mathrm{Nu}}_{L} = \frac{0.678 \; \mathrm{Pr}^{1/3} \; \mathrm{Re}_{L}^{1/2}}{\left[1 + \left(0.0468/\mathrm{Pr}\right)^{2/3}\right]^{1/4}}$$