

filtration velocity : Q_0/A (m/min)
 filtration time $\rightarrow t_f$
 for con

Capacity = V_f / time

cleaning of Bag House mechanism \rightarrow

- i) Mechanical shaking
- ii) pulse-jet Bag filter
- iii) Reverse jet Bag filter.

t_f - time of filtration

t_c - time of cleaning

Maximum capacity = $\frac{V_f}{t_f}$

Overall capacity = $\frac{V_f}{t_f + t_c}$

$t_c = 0$
 for max capacity.

for optimum capacity for design purpose $t_f = t_c$



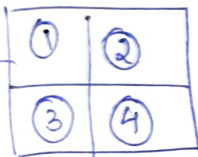
→ Sizing of Bag.
no bag should be more than 3-4 m.
typical diameter 40-50 cm

Guideline for Bag filter area in m²

Area in (m²)

No of compartments

1 - 200	1 - 2
201 - 600	3 - 4
601 - 1000	5 - 7
1001 - 1600	8 - 10
1601 - 2200	11 - 13
2201 - 3000	14 - 16
3001 - 4100	17 - 20
> 4100	> 20



1, 3, 4, → working

Minimum pressure drop - 30-40 cm of water column.

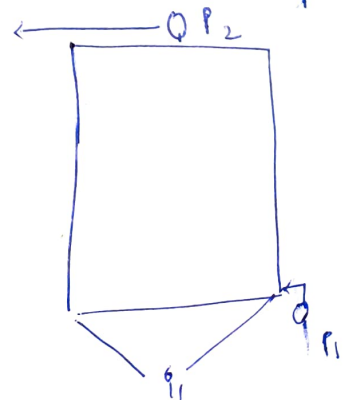
Maximum pressure drop - 150 cm of water column.

cake is form in Bag filter - Known by high pressure drop
choking of bag filter. rupture of Bag filter.

If pressure drop - 3-4 cm of water column.

→ If rupture of Bag - replace the choked or rupture Bag.

N = No of Bag.



constant rate filtration:-

$$\Delta P = B Q_t^2 + CQ$$

at $t=0$
 $t=t$

$$\Delta P = CQ$$

$$\Delta P = BQ^2 t + CQ$$

$$Q = \frac{V_f}{t}$$

$t_f =$

rupture of bag (i) chocking of Bag
(ii) huge quantity of.

Air to cloth ratio = $\frac{Q}{\text{total filtration area of Bag house}}$

1. 2 to 2.5 m/min for pulse-Jet Bag filter.

If the air to cloth ratio is very small \rightarrow Almost nothing.
Max temp a bag filter withstand is 280°C by

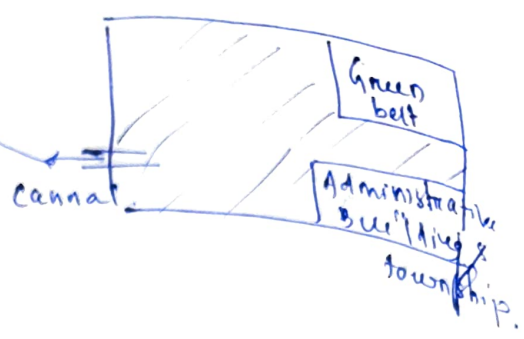
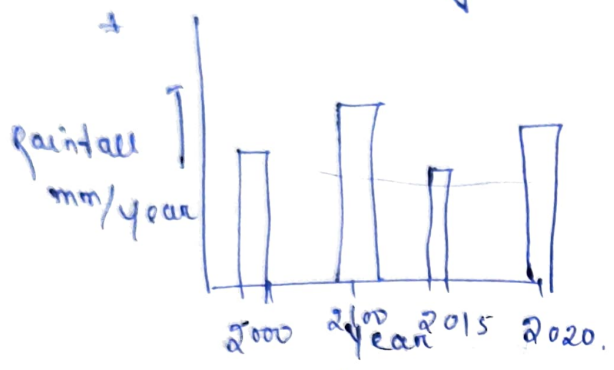
Properties of filter media:- Bag filter fiber materials:-

<u>fibres:-</u>	<u>strength</u>	<u>max temp</u>	<u>Remarks:-</u>
Cotton	strong	80	low cost Not suitable for acidic dusts.
Nylon	strong	100	easy to clean excellent for Abrasive material.
Polyester	strong	135	easy to clean.
Tetlon	medium	260	expensive.
Glass fiber	strong	280	poor resistance to abrasive.
Woven Nylon	strong	230	poor resistance to moisture.

① IPC class 13 oct 2025 :-
Surface runoff management:-

ETP

Zero liquid discharge



$$\text{Average rainfall} = \frac{\sum h_i}{\sum \text{year}}$$

$$Q_s = \frac{\text{Area} \times h}{(\text{m}^2) \quad (\text{m})} \times \text{co efficient.}$$

$$\text{water demand} = Q_D - Q_T - Q_s$$

$$ETP = 200 \text{ m}^3/\text{hr.}$$

$$Q_D = 4000 \text{ m}^3/\text{hr.}$$

$$\downarrow$$

$$50 \text{ m}^3/\text{hr}$$

Type	Area
T ₁	A ₁
T ₂	A ₂
T ₃	A ₃
⋮	⋮
T _n	⋮

$$\sum A_i = \text{Area.}$$

Surface runoff calculation:-

Rational method

$$Q = C \times i \times A$$

Q = Peak ~~to~~ Rate of Runoff m³/day

C = Runoff coefficient

i = A.V. intensity of Rainfall in mm/day.

A = water shed Area in Acre.

$$C_{eq} = \frac{A_1 C_1 + A_2 C_2 + A_3 C_3 + \dots}{A_1 + A_2 + A_3 + \dots}$$

A_1, A_2, A_3, \dots the area of different land type.

C_1, C_2, C_3, \dots corresponding runoff coefficient for these land type.

This weighted average approach ensure that the varied soil cover condition are accurately represented in the runoff calculation.

Example:-

<u>Surface description</u>	<u>C-value</u>
Asphalt and concrete	0.70 - 0.95
Roof	0.75 - 0.95
woodland	0.05 - 0.25
sandy soil, flat	0.05 - 0.10
heavy soil, flat	0.13 - 0.17

Total rainfall on yearly basis:-

<u>Year</u>	<u>Rainfall mm</u>
April 2019 - March 2020	1189
April 2020 - March 2021	1920
April 2021 - March 2022	2287
April 2022 - March 2023	1575

April 2013 - March 2014

Total
Average

8894
1179

Yes

i value

$$i = 1222 \text{ mm}$$

$$= 1.2 \text{ m}$$

Mitigation Measures:

- * Pond sizing Based on Peak discharge: The calculated Peak discharge during monsoon month helps to determine the required volume of ponds or reservoir.

Q

An old Bag filter from a discontinue process is to be utilized for constant pressure filtration at 12.7 cm of water column. The bag house has 20 bags of 7432.24 cm^2 each. Cleaning time of bag is determined as 45 min. For the given pressure filtration the following expression can be used

$$t = 674.82 V_g^2$$

t = time (min)

V_g = volume of gas filter. (m^3/cm^2)

determine the maximum capacity of the bag house & overall capacity of bag house under the given width.

$$\text{Maximum capacity} = V_g / t_f$$

$$t_f = t_c =$$

total surface area =

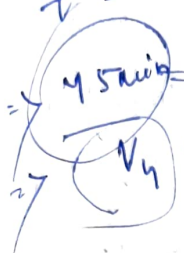
$$\text{total surface area} = 7432.24 \times 20$$

$$= \frac{148644.8}{1000} \text{ cm}^2$$

$$= 148.64 \text{ m}^2$$

$$t = 674.82 V_f^2$$

$$= 148.64 \text{ m}^2$$



$$V_f = 0.258 \text{ m}^3/\text{cm}^2$$

$$\text{max}^m \text{ capacity} = V_f / t_f$$

$$= \frac{38350.17}{45 \text{ min}}$$

$$= 51133.81$$

$$= \frac{0.258}{148.64} \text{ m}^3/\text{hr}$$

$$= \frac{38350.17}{45 \text{ min}} = 51133.81$$

$$t_f = 45 \text{ min}$$

$$= 38350.17 \text{ m}^3$$

overall capacity :-

$$V_f / t_f + t_c$$

$$= \frac{38350.17 \text{ m}^3}{90 \text{ min}}$$

$$t_f + t_c = 90 \text{ min}$$

$$= 25566.90 \text{ m}^3/\text{hr}$$

A filter is operating at constant rate on an optimum cycle. The filtration equation is given

$$V_f^2 = 2.623 \times 10^6 \times t \times p^{0.65}$$

p = cm of water column

V_f = m³ of gas filtered

t = time of filtration, in min.

The filtration time is 45 mins and cleaning time is 8 mins the maximum allowable

pressure is 10.16 cm of H₂O column.

calculate i) max^{overall} capacity of bag h^h
 ii) It is necessary to increase the capacity of bag house it has suggested that an additional unit identical to the present one ~~is~~ ^{has} been installed. both bag filter would work ~~from the~~ same 13 bar ~~installed~~ which has ample capacity and the filtration to be carried out at the same max^{overall} pressure as at present. The time required to save and clear two bag houses is estimated as 45 min. What is the % increase in the overall capacity that could be attained by adapting this condⁿ.

$$\text{max capacity} = V_g / t$$

$$V_g^2 = 2.623 \times 10^6 \times t \times P^{0.65}$$

$$= 2.623 \times 10^6 \times \frac{45}{60} \times 10.16^{0.65}$$

$$V_g^2 =$$

$$\Rightarrow V_g = 23080.534 \text{ m}^3$$

$$\text{max capacity} = \frac{23080.53 \text{ m}^3}{45/60 \text{ hr}}$$

$$= 30774.04 \text{ m}^3/\text{hr}$$

$$\text{overall capacity} = \frac{23080.53}{45+8/60} = 26128.909 \text{ m}^3/\text{hr}$$

(41)

Overall capacity of two bag

$$2 \times 23080.534$$

$$4574/60$$

$$= \cancel{28261.87 \text{ m}^3/\text{hr}}$$

$$56523.756$$

$$\cancel{28261.87}$$

$$56523.756 \text{ m}^3/\text{hr.}$$

$$26128.909$$

$$\times 100$$

% increase =

$$26128.909$$

$$116.32\%$$

A bag house is to be constructed using bags of 30cm in diameter and 6m long. The bag gas velocity has been determined as 2 m/min. Calculate no. of bag required for a continuous operation of bag house.

$$\text{Area of bag} = \cancel{6000 \text{ cm} \times 30 \text{ cm}} \\ = \cancel{180000 \text{ cm}^2} \\ = \cancel{1.8 \text{ m}^2}$$

$$\text{Filteration velocity} = 2 \text{ m/min}$$

$$\text{Filteration velocity} = 2 \text{ m/min}$$

The gas enter: 36000 m³/hr

$$= \frac{36000 \text{ m}^3/\text{hr}}{2 \text{ m/min} \times 60 \text{ hr}}$$

$$36000 \text{ m}^3/\text{hr}$$

$$2 \times 60 \text{ m/hr}$$

$$300$$

$$36000$$

$$120$$

$$= 300 \text{ m}^3$$

$$\text{Area of bag} = \frac{\pi D^2}{4} + \pi \times 0.3 \times 6$$

Waste water :- 2 loc

IPC Wet - Scrubbers (control of Particulate & Gaseous Pollutant)

SO₂ HCl
NH₃ acid mist
H₂C
CO
H₂S



not used ESP or baghouse
gravity settling chamber
cyclone

Adsorbent

Adsorption (wet scrubber).

Gaseous pollutants

- Adsorption
- Absorption
- Condensation
- Combustion



Adsorbent

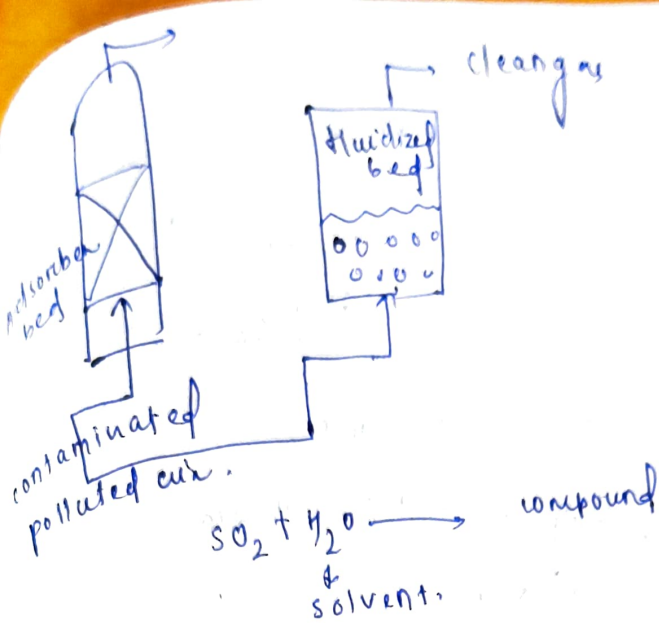
micro/macro pores

specific surface area $\frac{m^2}{gm}$ of Adsorbent

$\frac{m^2}{gm}$ of Adsorbent

Adsorption Capacity

$\frac{mg}{gm}$ of Adsorbent



wet scrubber

- Transfer pollutant from air to water
- further treatment may be necessary
- pollutant must be highly soluble in water.
- for less soluble material, a chemical may be added to water
- SO_2 may be removed by reacting with lime stn.

Asn pollution control gases and vapors.

SO_x , NO_x , VOCs, HAPs, CO

slides

wet scrubbers advantages / disadvantages

wet collectors

Bag filter problem

It is required to remove the dust from an iron ore grinding count separation mill. The gas flows from the mill at $45^\circ C$, $31680 m^3/hr$. The gas filtering velocity $1.5 m/min$ determine the cloth area required to process if the diameter of bag is

20cm and length is 5m how many bag will be required for continuous cleaning of bag filter.

$$\text{Flow rate } (Q) = 31680 \text{ m}^3/\text{hr}$$

$$= 31680/60 =$$

Please

$$\text{Filtering velocity} = 1.5 \text{ m/min.}$$

$$\text{Diameter of bag} = 20\text{cm} = 0.2\text{m.}$$

$$\text{length} = (L) 5\text{m.}$$

~~total cloth~~ $Q/A_c = V$

$$\text{total cloth Area} \Rightarrow A_c = Q/V = \frac{528 \text{ m}^3/\text{min}}{1.5 \text{ m/min}}$$

$$A_c = 352 \text{ m}^2$$

$$A_c = N \times (\pi \times D \times L + \pi/4 D^2)$$

$$N \times (3.14 \times 0.2 \times 5 + \frac{3.14}{4} (0.2)^2)$$

$$N = 110.9 \text{ bags}$$

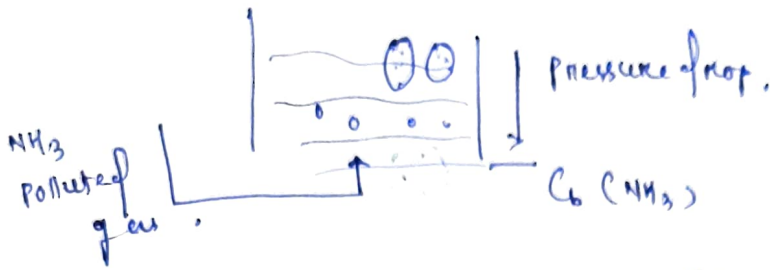
$$= 111 \text{ bags}$$

growth of micro-organisms consumed
Movie =

352
Rammur
Lond chiva

single
achem

$$R_{\text{removal}} = k_{\text{overall}} (C_b - C_i)$$



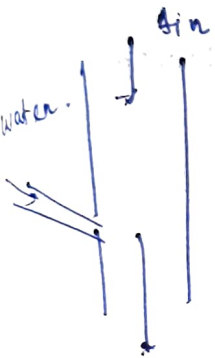
C_i - final conc.

$$\text{Removal} = \cancel{k_{\text{overall}} (C_b - C_i)}$$

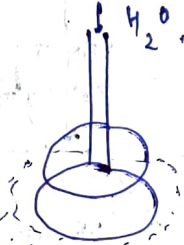
$$= k_i a (\Delta C)$$

a = interfacial area of contact.

$$a = \left(\frac{m^2}{m^3} \right)$$



by changing a we can change the scrubber.



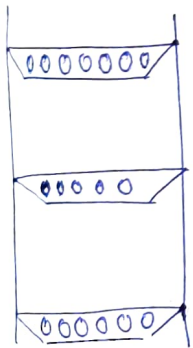
sandhya re

Rotating plate droplet generator.

spray tower - 70-78% but pressure drop is high so use.

cyclonic scrubber

6/11/2021 6/11/2021



Air scrubber
photos

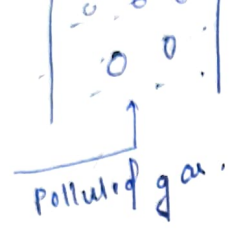
04/28/10/25

particulate (photos)

Design the wet scrubber:

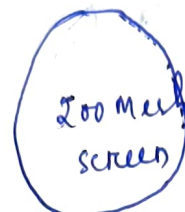
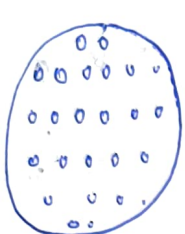
spray tower (photo subject)

droplet size distribution - spray tower.



Polluted gas.

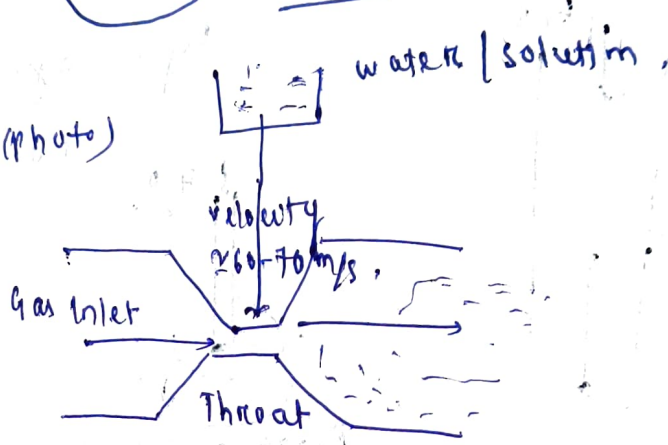
plate tower (photo)



not used for industrial purpose.

75 μ m

Venturi scrubber (photo)

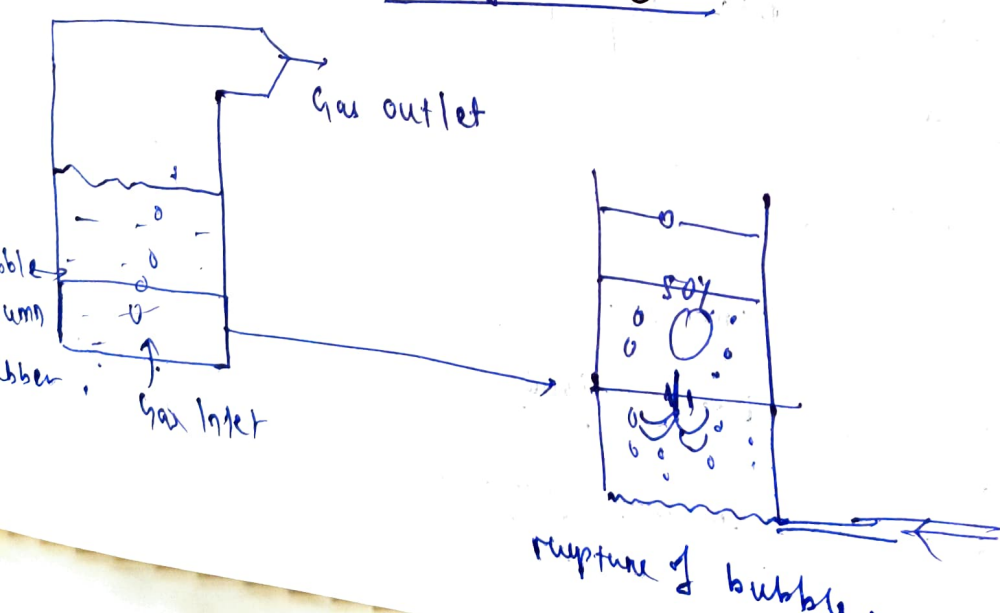


Packed tower

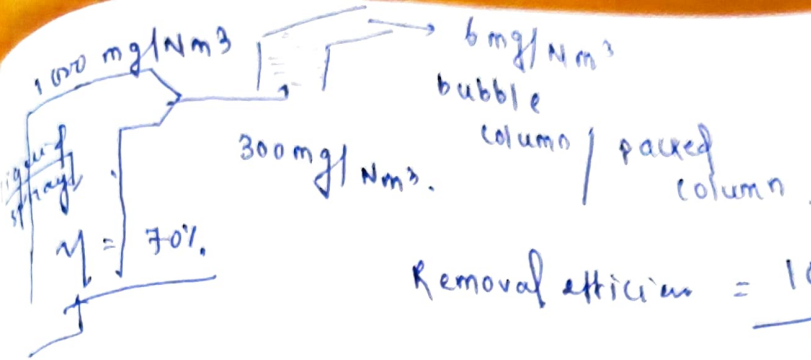
spray tower

- ① working principle of all
- ② design- packed, spray, plate
- ③ You develop design problem yourself.

Handbook by percy



Air/gas



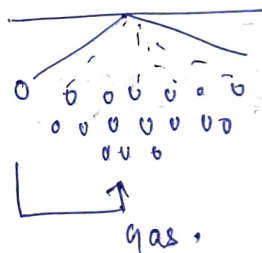
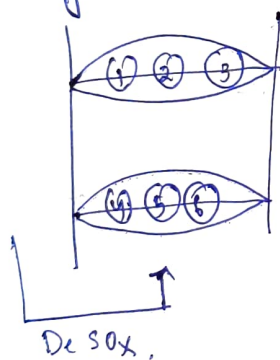
20 June

$$\text{Removal efficiency} = \frac{1000 - 6}{1000} \times 100$$

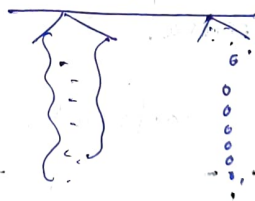
Q A sulphuric acid manufacturing plant emitting SO₂ Exhaust stream of the plant contains mainly SO₂ about 15% by volume and carrier gas.

Monday 2.11.25

scrubber:-



Type of nozzle



scrubber Nozzles:-

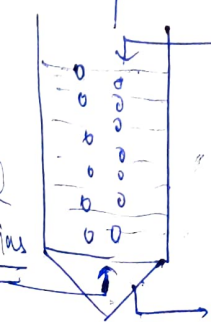
Design :-

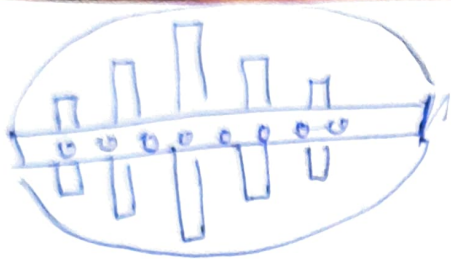
clean gas

solution / Absorbing liquid (water)

slurry / waste water

$$Q = \text{m}^3/\text{hr}$$






~~Original Defining~~

Q A bag house is operating at a constant gas rate for 30 min during which 40.8 m^3 of gas from a cement mill operation is processed. The initial & final pressure drop of the unit is 10.16 mm of water column & 101.6 mm of water column respectively. If the filter is further operated for 1 hr at the final pressure calculate the quantity of additional gas which can be treated by this unit.

$$Q = \dots \text{ hr} + \text{min} -$$

5/11/2022



ZLD (zero liquid discharge)

DT: 4. NOV 25

T = ? 300°C

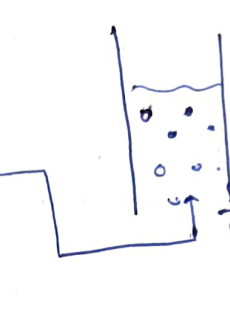
P = ? 0.2 Atm(g)

$\Delta Q = M_1 C_p (\Delta T)_1$
 $= M_2 C_p (\Delta T)_2$

$T_{new} = 35^\circ C$

Activated Carbon filter

Ramish Pujakare




T = 30°C

Q1

Q2

A fertilizer plant emits 2 lakh m^3/hr of gases at $100^\circ C$ and 0.06 atm gas pressure containing ammonia with an inlet conc of $700 \mu g/m^3$. It is proposed to use a packed tower with water as an absorbing liquid. The industry needs to bring down the ammonia conc below $10 \mu g/m^3$. The eq^m relationship is as follows

y_{NH_3}	0	0.016	0.024	0.032	0.04
x_{NH_3}	0	0.020	0.031	0.040	0.05



0.033

0.040

$Q = 200000 m^3/hr.$

$T_1 = 100^\circ C.$

$P = 0.06 atm$

$C = 700 \mu g/m^3$

Bag filter

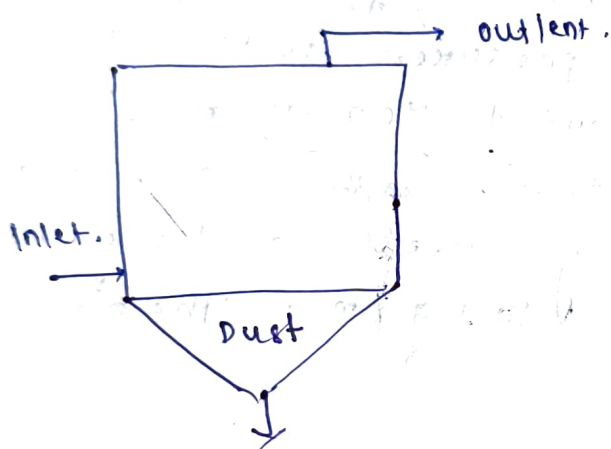
A Bag filter is used to treat $50 m^3/sec$ of the waste gas stream. The Bag house to be divided in to 8 section of equal cloth area so that one section can be taken off for shut down for

Cleaning & maintenance & other remaining in working condⁿ. The air to cloth area ratio $9 \text{ m}^3/\text{min}/\text{m}^2$ is used which provide sufficient surface area for the cleaning of the flow gas. The Bags are 25 cm diameter & 7 m long. Calculate the No of Bags & physical arrangement required ~~for~~ to ~~above~~ meet the above requirement.

→ 8 section.

→ 7 used & one used by stand by mode

$$Q = 50 \text{ m}^3/\text{sec}$$



Q An old Bag filter from a discontinued process is to be utilised for constant pressure filtration at 120 mm of water. The filter has 40 bags of 6000 cm^2 each. The filtration time is given as 50 min & filtration

eqⁿ is $t_f = 6.94 \cdot 85 V_h^2$

where V_h = volume of gas filtered per unit area in m^3/sec^2

t = time in min

calculate overall capacity of the bag filter under given condⁿ

ii) max^m overall capacity

iii) If another ^{addition} three, identical old bag houses are installed to increase the capacity what is max^m % increase in the overall capacity for new arrangement
Assume total cleaning time with new arrangement is 20 min.

Ques