

# Taking the Devil Out of the Details

- The St. Helens Wastewater Treatment Plant in Tasmania, Australia, utilizes multi-barrier membrane technology approach from a Chicago-area company to meet stringent effluent quality.**

**O**n the island of Tasmania off Australia's southeast coast, the AquaMB Process® from Aqua-Aerobic Systems Inc. is utilized as an alternate to membrane biological reactors (MBRs) in the town of St. Helens. This technology was selected due to the comparable effluent quality to the MBR system and lower cost of ownership.

## A MULTI-BARRIER APPROACH

The multi-barrier membrane system integrates biological treatment, cloth media filtration and microfiltration into a single process with resulting savings in membrane



**Figure 1.** Aerial shot of St. Helens Wastewater Treatment Plant

area of greater than 50% compared to a typical MBR configuration.

The plant is designed to treat an average flow of 0.4 million gallons per day (mgd) of domestic sewage from the local community. In addition to the savings in lifecycle cost, the multi-barrier process provides flexibility and ease of operation. These are the main reasons why this process was selected over MBR. Operators take advantage of this flexibility, especially since St. Helens is a coastal holiday destination, and the population typically increases by up to 50% for a two-month period in summer.

## PROCESS DESCRIPTION

Raw wastewater comes into the plant from St. Helens. The influent pump station sends the wastewater through a grit removal system and a 6 mm perforated influent screen. If the 6 mm screen needs to be taken offline for maintenance, there's a backup 20 mm bar screen available onsite.

The secondary process includes a dual basin AquaSBR® system designed for biological nutrient removal (BNR). Alkalinity is supplemented in the biological reactors in the form of Soda Ash. Effluent from the sequencing batch reactor (SBR) goes to a post equalization basin and a flocculation tank, before entering the tertiary filtration.

To supplement the biological phosphorus removal of the SBR, the operator can add alum into the biological reactors, the flocculation tank and/or the post equalization basin, if required.

The clarified effluent of the SBR is pumped from the post equalization to a flocculation tank and then flows by gravity through the cloth media of the stationary hollow disks. The filtrate exits through a hollow shaft that supports the individual disks and flows to the effluent channel.

Tertiary effluent flows into a pump station and is then pumped to the external membranes. Due to high quality effluent from the cloth media filter, with a total suspended solids (TSS) concentration of less than 5 mg/L, the membrane area is reduced significantly. The St. Helens plant includes 1,300 m<sup>2</sup> of membrane area. The membrane effluent goes through UV disinfection prior to discharge.

The treated effluent is discharged into nearby St. George Bay, which is utilized for sensitive aquaculture and thus has specific effluent quality requirements (see *Table 1*).

## PLANT OPERATION

Based on the multi-barrier approach of the process and the high quality effluent from each of the processes, operators are able to discharge directly from the filter or membranes. Although not available in this site, an option could be added to discharge directly from the SBR, by-passing the filters and membranes. The plant had a test period that allowed it to discharge less than ultimate effluent quality. The operators took advantage of the multi-barrier and were



**Figure 2.** St. Helens WWTP Multiple-Barrier Treatment Process\*

\* Consists of a 2-basin sequencing batch reactor, cloth media disk filter, and external membranes.

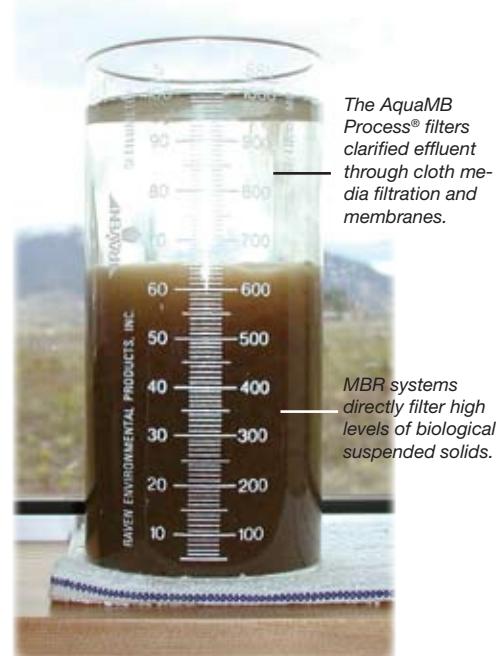
# Membrane Separation

able to commission the plant in stages and still meet effluent targets.

During the test period, the operators were able to run the dual basin SBR system in a single basin mode, utilizing one of the SBR basins as a Pre-EQ basin. The plant received an average of 36% of its design flow. In the Pre-EQ/SBR mode of operation, however, this equates to an average of 72% of design flow. At this time, the BOD

TP value while meeting effluent quality limits for all other parameters.

Chemicals for the membrane cleaning processes include citric acid, sodium hydroxide and sodium hypochlorite. The recommended cleaning intervals are every 30-60 days for membranes in an AquaMB Process®. Still, the low loading, as well as the mechanical cleaning regime of air scour/reverse filtration and enhanced flux maintenance (which uses a small amount of sodium hypochlorite) provided sufficient cleaning to return the transmembrane pressure to an "as new" condition.



A settleometer test on system effluent showing MBR treatment quality below and the cloth filter and AquaMB Process® level of treatment above.

**Table 1.** Design Parameters

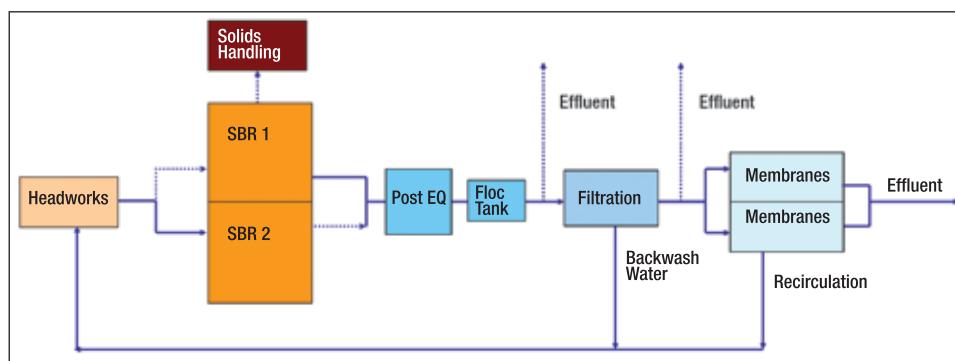
Parameter	Design Influent	Effluent Required
Average Flow (MGD)	0.4	--
Maximum Flow (MGD)	0.8	--
BOD5 (mg/L)	230	2
TSS (mg/L)	150	4
TKN (mg/L)	52	--
NH3-N (mg/L)	--	0.7
Total Nitrogen (mg/L)	--	7
Total Phosphorus (mg/L)	10	1

**Table 2.** Test Period Plant Effluent

Parameter	Effluent Required During Testing	Effluent Achieved During Test
BOD5 (mg/L)	10	<2*
TSS (mg/L)	10	<3*
NH3-N (mg/L)	1.0	0.3
Total Nitrogen (mg/L)	15	6.9
Total Phosphorus (mg/L)	8.5	3.8 / 0.1**
Turbidity (NTU)	0.37	--
E. Coli (orgs/100 mL)	10	0

\*BOD and TSS values were recorded below the detectable levels shown  
\*\*TP of 0.1 mg/L was met consistently with the addition of metal salt

**Figure 3.** Multiple-Barrier Treatment Process Flow Schematic



load was 39% – which equates to 78% of the design loading in this mode of operation. As expected, there was a gradual increase in loads as more tourists arrived over the summer months.

Daily measurements of key influent and effluent parameters were performed during the test period, proving compliance during the course of this evaluation (see *Table 2*). All the effluent requirements were met during the test period. In fact, effluent quality exceeded the treatment required to the point that all parameters of the ultimate effluent required were met. Addition of alum was minimal during the test period; but, to demonstrate the capacity of the system to reduce the total phosphorus, alum was dosed into the flocculation tank, after the test period. The alum dosing regime was determined to achieve a final 0.1 mg/L effluent

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