

Cyclus Fuel Cycle Simulation Capabilities with the Cyder Disposal System Model

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Kathryn D. Huff
katyhuff.github.com

University of Wisconsin-Madison / University of California - Berkeley

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Outline

① Motivation

- Future Fuel Cycle Options
- Geologic Disposal Concept Options
- Fuel Cycle Simulator Capabilities

② Modeling Capabilities

- Cyder Overview
- Radionuclide Transport in Cyder
- Thermal Transport in Cyder

③ Conclusion



Future Fuel Cycle Options

Domestic Fuel Cycle Options

Title	Description	Challenges
Open	Once Through Current US PWR Fleet No Separations No Recycling Higher Burnups	High Temperatures, Volumes
Modified Open	Partial Recycling Next Gen. PWR Fleet Limited Separations Limited Transmutation Advanced Fuel Forms HLW treatment	Both high volumes and variable spent fuel streams
Closed	Full Recycling Full Separations Full Recycling VHTGR, SFRs, other transmutation HLW treatment	Variable spent fuel streams

Table 1 : Domestic Fuel Cycle Options



Disposal Geology Options Considered

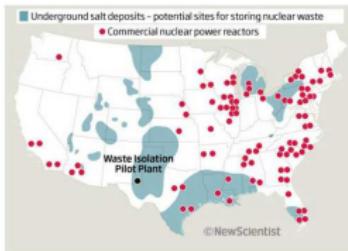


Figure 1 : U.S. Salt Deposits, ref. [26].

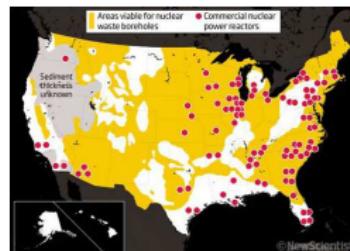


Figure 3 : U.S. Crystalline Basement, ref. [26].

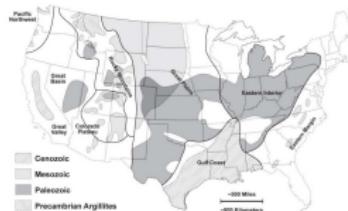


Figure 2 : U.S. Clay Deposits, ref. [11].



Figure 4 : U.S. Granite Beds, ref. [6].



Cyclus Top Level Fuel Cycle Simulator

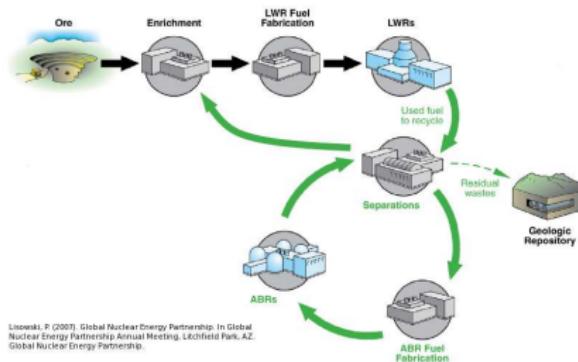


Figure 5 : Top level simulators are intended to model the collective behavior of various fuel cycle decisions and strategies [24].



Figure 6 : cyclus.github.com [17].



Need For an Integrated Repository Model

Repository Capabilities within Systems Analysis Tools

Tool	Institution	Fuel Disposition	Radionuclide Transport	Heat Transport
NUWASTE[2]	NWTRB	yes	no	no
VISION [38]	INL	yes	no	YMR only
DANESS [34]	ANL	no	no	no
COSI [3]	CEA	yes	no	yes
NFCSim [31]	LANL	no	no	no
CAFCA [14]	MIT	no	no	no
ORION [14]	BNL	no	no	no
TSM [33]	OCRWM	yes	no	YMR only

Table 2 : System tools are lacking in radionuclide transport and heat transport calculations in generic geologic media.



Contributions from This Work

This work has provided a platform capable of bridging the gap between fuel cycle simulation and repository performance analysis.

- Conducted thermal transport sensitivity analyses. [19, 18]
- Conducted contaminant transport sensitivity analyses. [20]
- CYDER achieved integration with a fuel cycle simulator.
- Abstracted physical models of thermal and contaminant transport. [22]
- Demonstrated dominant physics of those models in CYDER, integrated with CYCLUS. [23, 17]
- Published source code, documentation, and testing to facilitate extension by external developers. [21]



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Cyder Paradigm : Waste Stream Acceptance

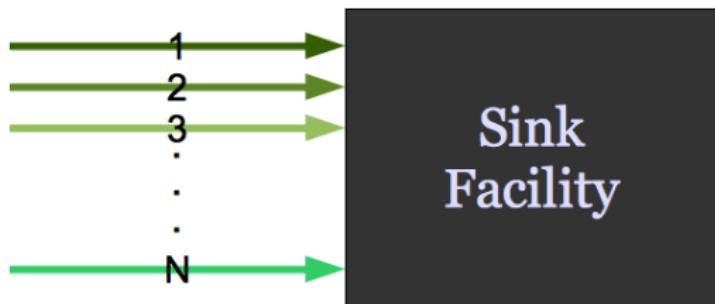


Figure 7 : To participate in a CYCLUS fuel cycle simulation, CYDER must accept arbitrary spent fuel and high level waste **material data objects**.



Cyder Paradigm : Waste Stream Conditioning

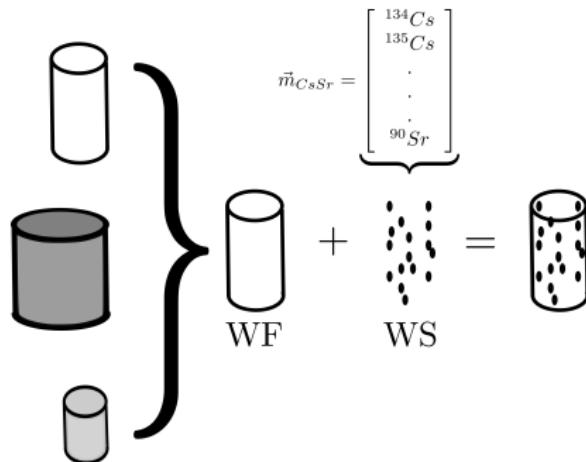


Figure 8 : In Cyder, discrete waste streams are conditioned into the appropriate discrete waste form according to user-specified pairings.



Cyder Paradigm : Waste Form Packaging

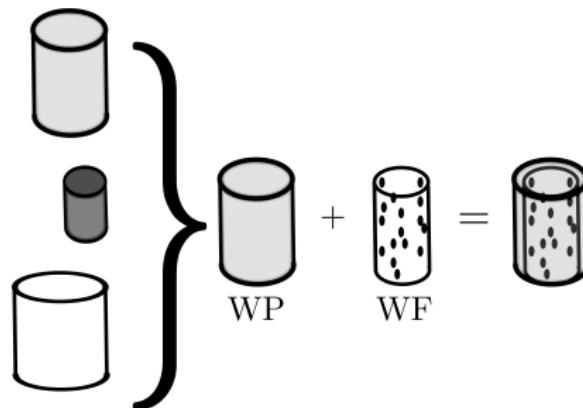


Figure 9 : In Cyder, one or more waste forms are loaded into the appropriate waste package according to user-specified pairings.



Cyder Paradigm : Waste Package Emplacement

Finally, the waste package is **emplaced** in a buffer component, which contains many other waste packages, spaced evenly in a grid. The grid is defined by the user input and depends on repository depth, Δz , waste package spacing, Δx , and tunnel spacing, Δy as in Figure 10.

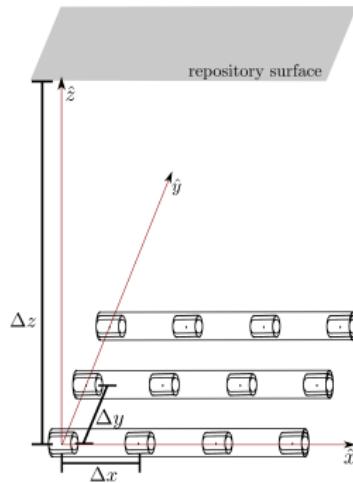


Figure 10 : The repository layout has a depth and a uniform package spacing.



Cyder Paradigm : Modularity

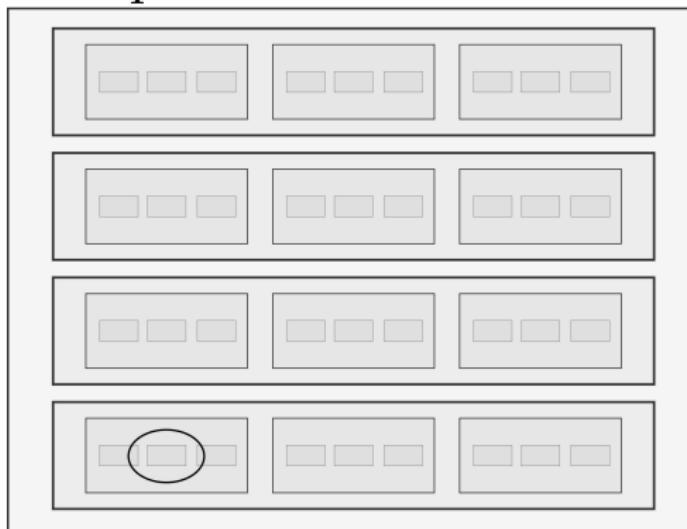
Components





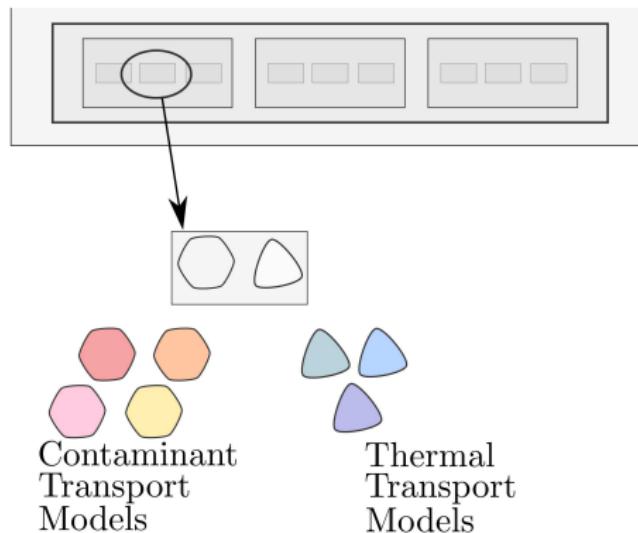
Cyder Paradigm : Modularity

Components





Cyder Paradigm : Modularity





Clay GDSM Sensitivity Analysis

- Barrier Degradation
- Sorption
- Solubility
- Advective Velocity
- Diffusivity

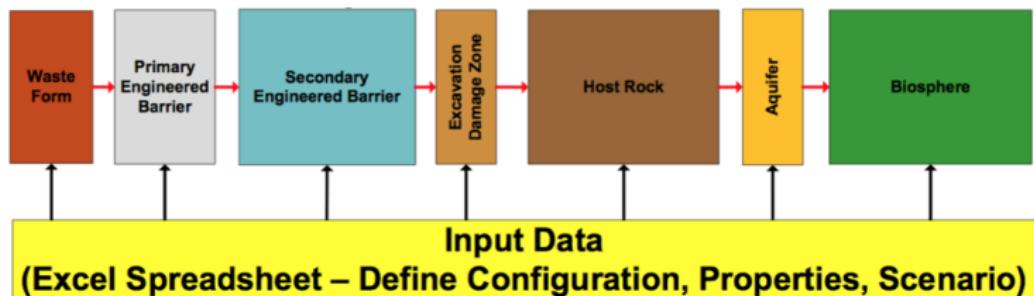


Figure 11 : The Clay Generic Disposal System Model (GDSM) was used for preliminary sensitivity analysis, abstraction iteration, and validation. This figure was reproduced from Figure 3.3-2 in [9].



Nested Components

The NuclideModel in a Component can be interchangeably represented by any of the four nuclide transport models.

- Degradation Rate Based Failure Model
- Mixed Cell with Degradation, Sorption, Solubility Limitation
- Lumped Parameter Model
- 1 Dimensional Approximate Advection Dispersion Solution, Brenner [4]



Radionuclide Transport: Degradation Rate Based Release

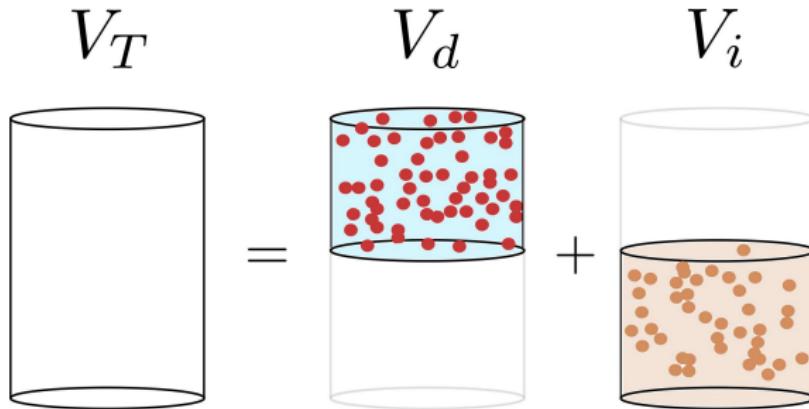


Figure 12 : The control volume contains an intact volume V_i and a degraded volume, V_d . Contaminants in V_d are available for transport, while contaminants in V_i are contained.



Radionuclide Transport : Mixed Cell with Sorption and Solubility

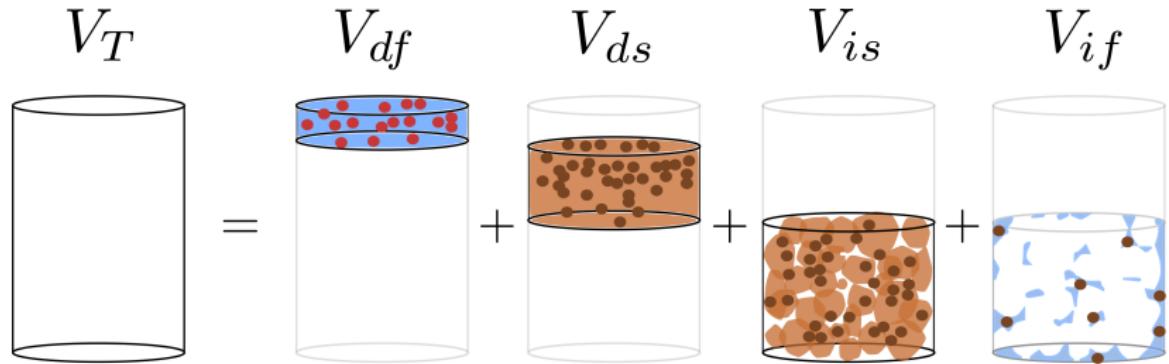


Figure 13 : The degraded volume is modeled as a solid degraded volume, V_{ds} , and a fluid degraded volume, V_{df} . The intact volume is modeled as an intact solid volume, V_{is} , and an intact fluid volume V_{if} . Only contaminants in V_{df} are available for transport.



Radionuclide Transport : Mixed Cell Sorption

The mass of contaminant sorbed into the degraded and precipitated solids can be found using a linear isotherm model [32], characterized by the relationship

$$s_i = K_{di} C_i \quad (1)$$

where

s_i = the solid concentration of isotope i [kg/kg]

K_{di} = the distribution coefficient of isotope i [m^3/kg]

C_i = the liquid concentration of isotope i [kg/m^3].



Radionuclide Transport : Mixed Cell Solubility Limitation

In addition to engineered barriers, contaminant transport is constrained by the solubility limit [16],

$$m_{s,i} \leq V_w C_{sol,i}, \quad (2)$$

where

$m_{s,i}$ = solubility limited mass of isotope i in volume $V_w [kg]$

V_w = volume of the solution $[m^3]$

$C_{sol,i}$ = solubility limit, the maximum concentration of i $[kg/m^3]$.



Radionuclide Transport: Lumped Parameter Transport Model

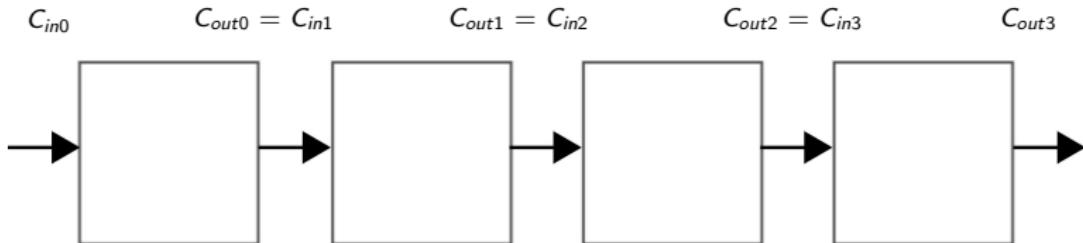


Figure 14 : The method by which each lumped parameter component is modeled is according to a relationship between the incoming concentration, $C_{in}(t)$, and the outgoing concentration, $C_{out}(t)$.

$$C_{out}(t) = \int_0^{\infty} C_{in}(t - t') g(t') e^{-\lambda t'} dt' \quad (3)$$

where

t' = time of entry [s]

$t - t'$ = transit time [s]

$g(t - t')$ = response function, a.k.a. transit time distribution [-]

λ = radioactive decay constant [s^{-1}].



Radionuclide Transport: 1D Finite, Cauchy B.C.

$$-D \frac{\partial C}{\partial z} \Big|_{z=0} + vC = \begin{cases} vC_0 & t < t_0 \\ 0 & t > t_0 \end{cases} \quad \frac{\partial C}{\partial z} \Big|_L = 0$$

The diagram shows a horizontal line segment representing a 1D domain. The left endpoint is labeled $z = 0$. Above the line at this point is the equation $C(z, 0) = C_i$. The right endpoint is labeled $z = L$. Above the line at this point is the equation $\frac{\partial C}{\partial z} \Big|_L = 0$.

Figure 15 : A one dimensional, finite, unidirectional flow, solution with Cauchy and Neumann boundary conditions [35, 4].



Clay GDSM Degradation Rate Sensitivity

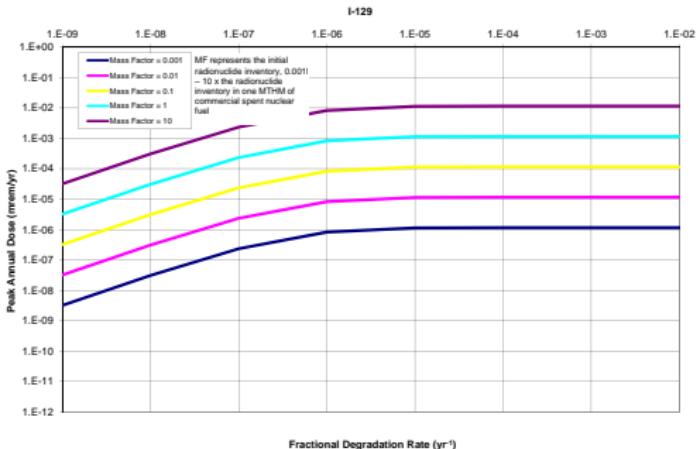


Figure 16 : ^{129}I waste form degradation rate sensitivity.



Cyder Degradation Rate Sensitivity

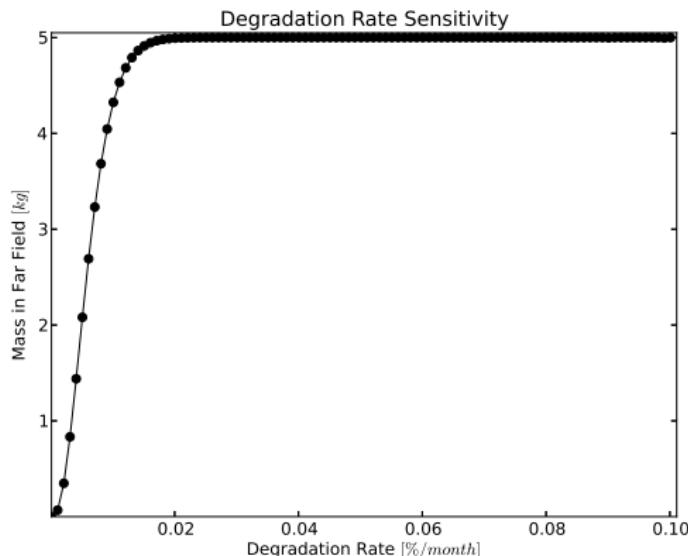


Figure 17 : Sensitivity demonstration of the degradation rate in CYDER for an arbitrary isotope.



Clay GDSM Sorption Sensitivity

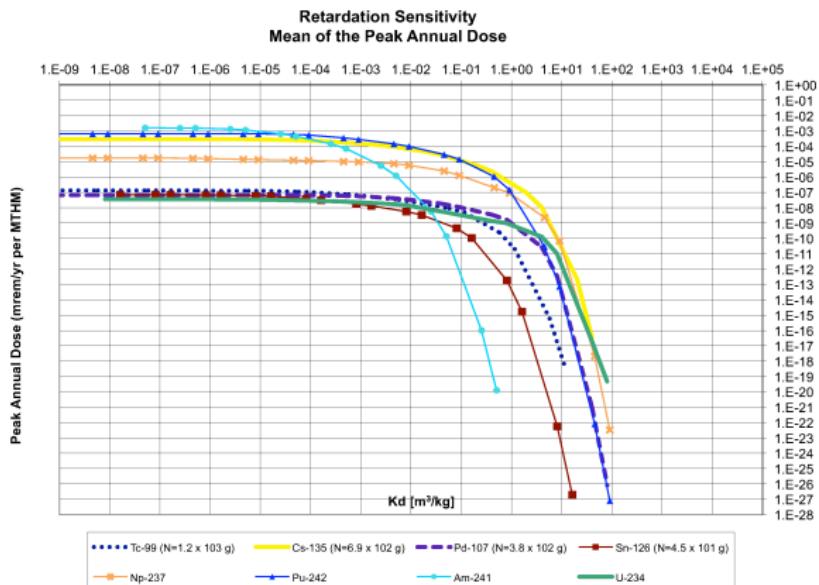


Figure 18 : K_d sensitivity. The peak annual dose due to an inventory, N , of each isotope.



Cyder Sorption Sensitivity

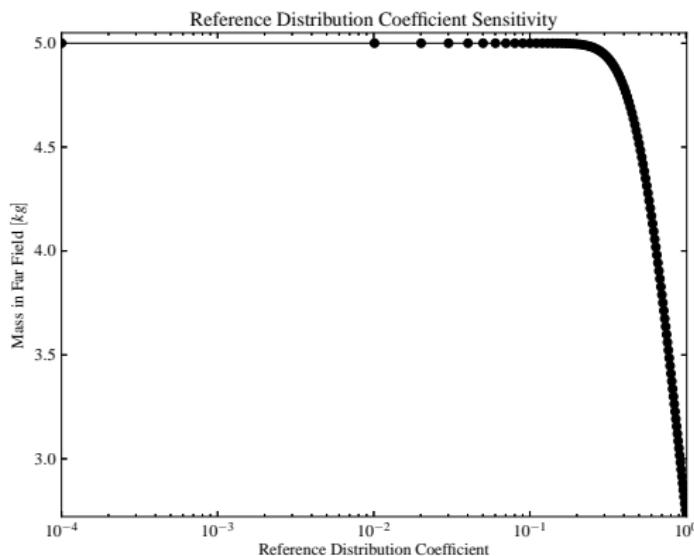


Figure 19 : K_d factor sensitivity in the CYDER tool for an arbitrary isotope assigned a variable K_d coefficient.



Clay GDSM Solubility Sensitivity

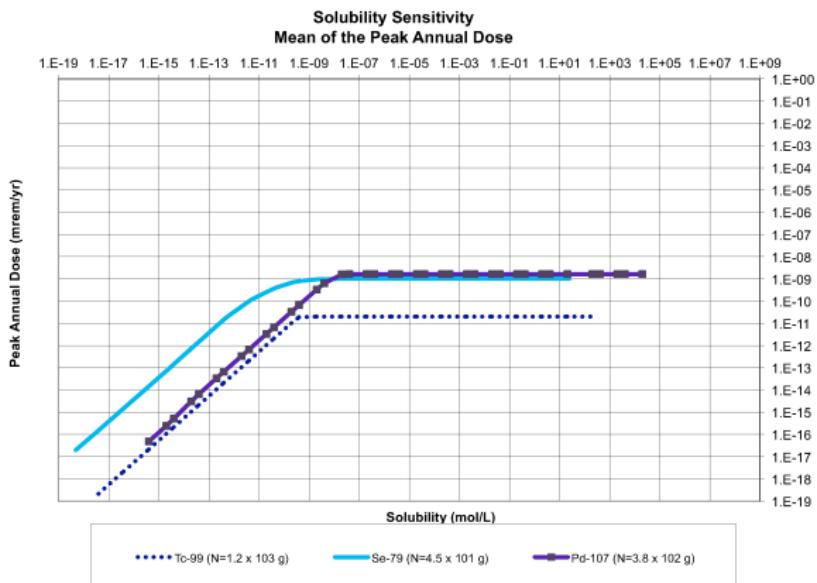


Figure 20 : Solubility limit sensitivity. The peak annual dose due to an inventory, N , of each isotope.



Cyder Solubility Sensitivity

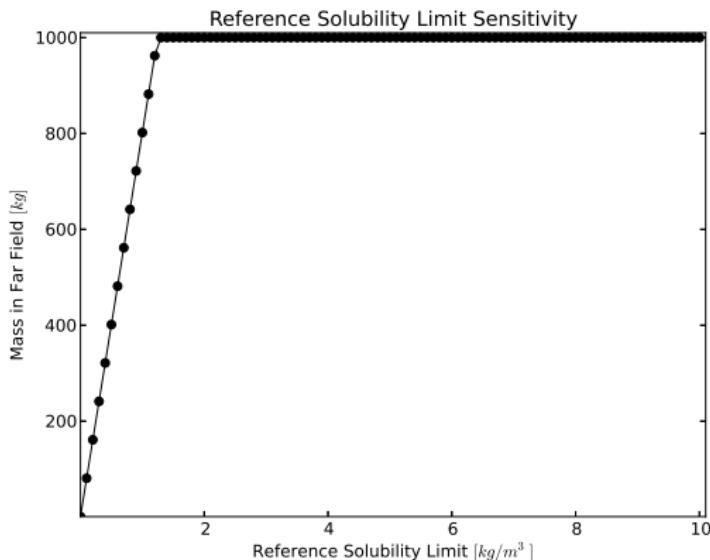


Figure 21 : Sensitivity demonstration of solubility limitation in CYDER for an arbitrary isotope assigned a variable solubility limit.



Specific Temperature Change Calculations

A reference data set of temperature change curves was calculated. Repeated runs of a detailed model ([15, 13, 12]) over the range of values in Table 4 determined Specific Temperature Change (STC) values over that range.

Thermal Cases

Parameter	Symbol	Units	Value Range
Diffusivity	α_{th}	$[m^2 \cdot s^{-1}]$	$1.0 \times 10^{-7} - 3.0 \times 10^{-6}$
Conductivity	K_{th}	$[W \cdot m^{-1} \cdot K^{-1}]$	0.1 – 4.5
Spacing	S	$[m]$	2, 5, 10, 15, 20, 25, 50
Radius	r_{lim}	$[m]$	0.1, 0.25, 0.5, 1, 2, 5
Isotope	i	$[-]$	$^{241,243}Am$, $^{242,243,244,245,246}Cm$, $^{238,240,241,242}Pu$, $^{134,135,137}Cs$, ^{90}Sr

Table 3 : A thermal reference dataset of STC values as a function of each of these parameters was generated by repeated parameterized runs of the LLNL MathCAD model[12, 13].



Thermal Base Case Demonstration

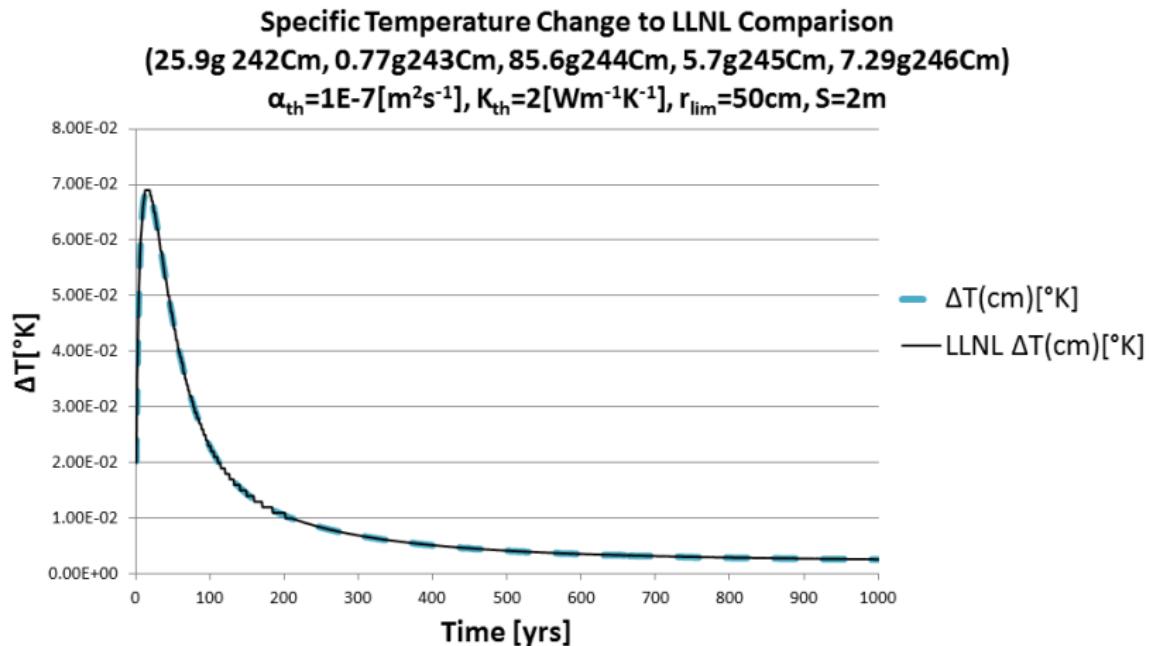


Figure 22 : This comparison of STC calculated thermal response from Cm inventory per MTHM in 51Gwd burnup UOX PWR fuel compares favorably with results from the semi-analytic model from LLNL



Thermal Base Case Demonstration

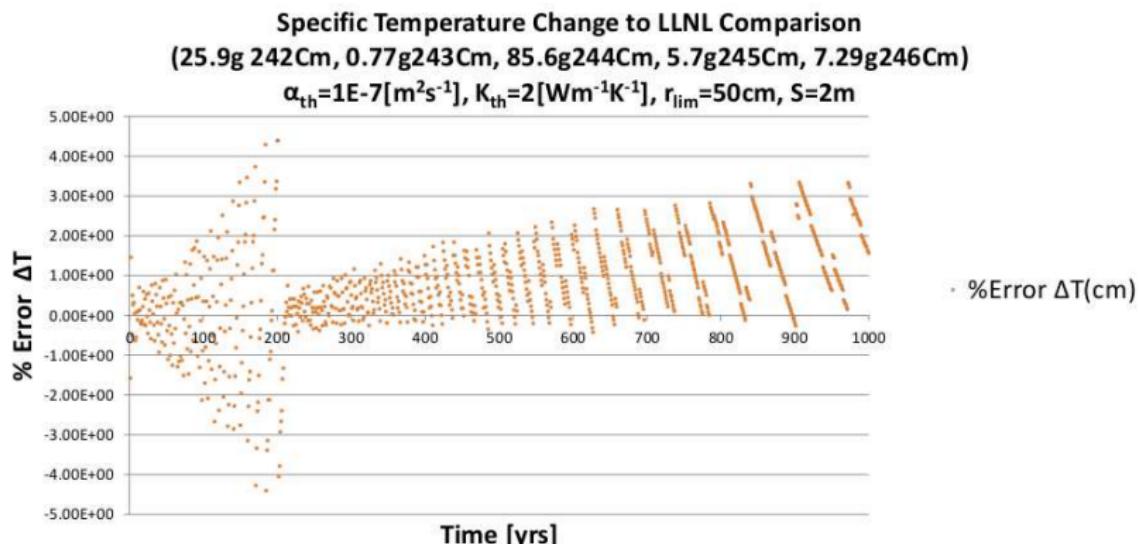


Figure 23 : Percent error between the semi-analytic model from LLNL and the STC calculated thermal response from *Cm* inventory per MTHM in 51GWd burnup UOX PWR fuel demonstrates a maximum percent error of 4.4%.



LLNL Model Thermal Conductivity Sensitivity

Thermal Conductivity Sensitivity, LLNL Model Results,
 $t=30y$, $s=25m$, $r_{lim}=50cm$, 1kg Cm242 + Daughters

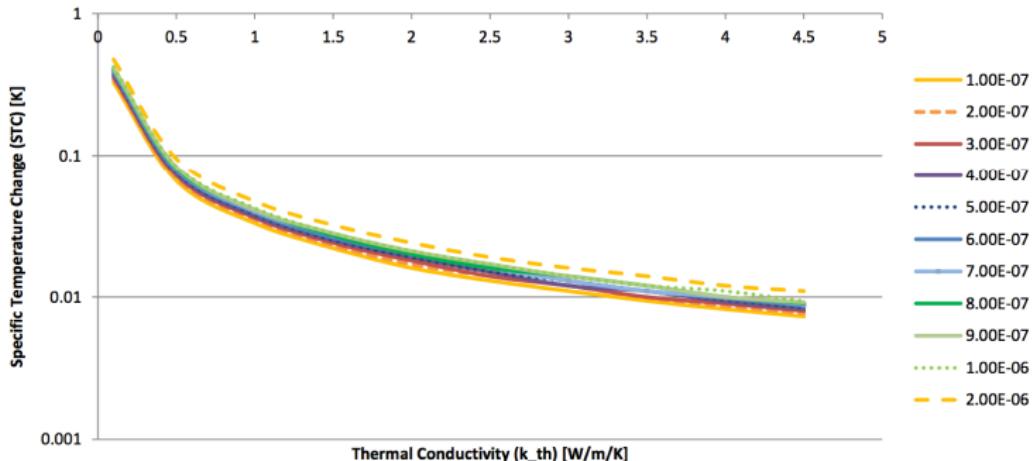


Figure 24 : Increased thermal conductivity decreases the temperature (here represented by STC) at the limiting radius.



Cyder Thermal Conductivity Sensitivity

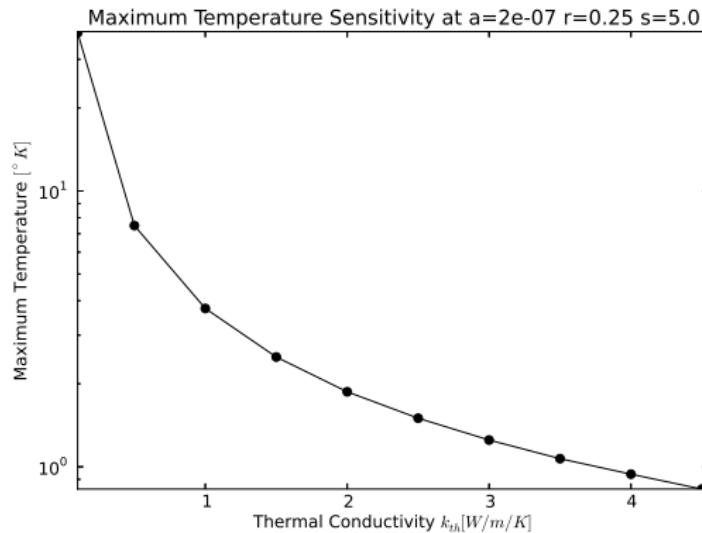


Figure 25 : Cyder results agree with those of the LLNL model. Increased K_{th} decreases temperature change at the limiting radius. The above example thermal profile results from 10kg of ^{242}Cm , $\alpha_{th} = 2 \times 10^{-7}$, $s = 5m$, and $r_{lim} = 0.25m$.



LLNL Model Thermal Diffusivity Sensitivity

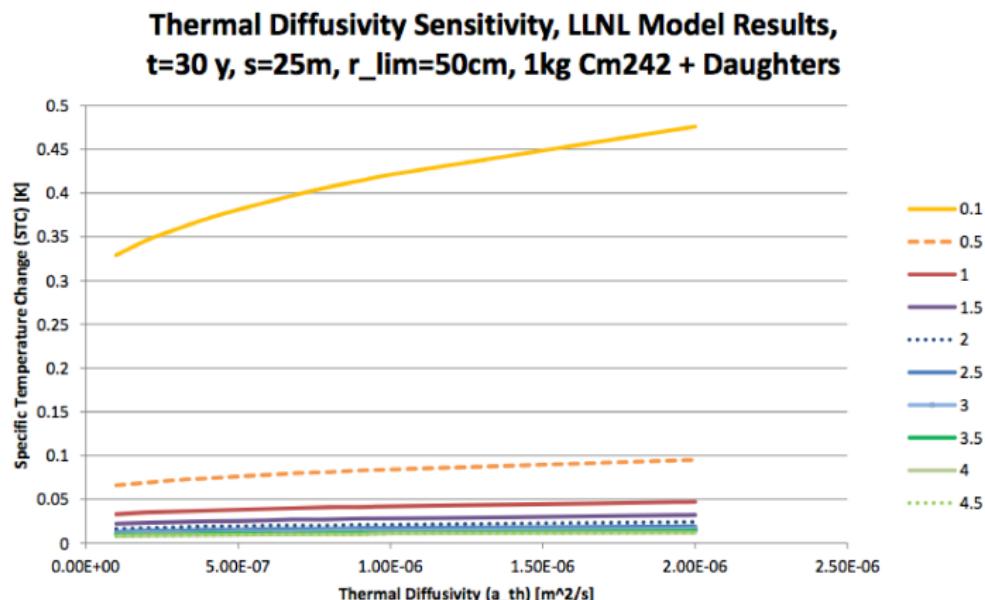


Figure 26 : Increased thermal diffusivity decreases temperature change (here represented by STC) at the limiting radius (here $r_{\text{calc}} = 0.5\text{m}$).



Cyder Thermal Diffusivity Sensitivity

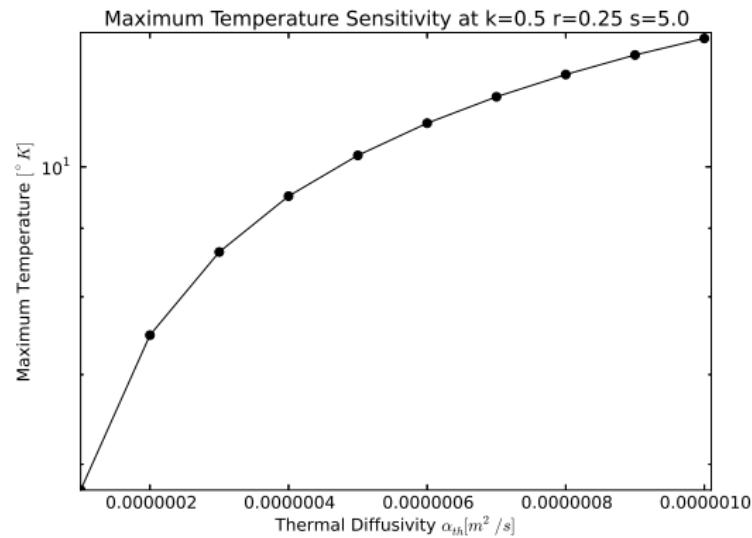


Figure 27 : Cyder trends agree with those of the LLNL model, in which increased thermal diffusivity results in reduced temperature change at the limiting radius. The above example thermal profile results from 10kg of ^{242}Cm .



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Conclusion : Summary of Contributions

This work has provided a software platform capable of bridging the gap between fuel cycle simulation and repository performance analysis.

- Conducted thermal transport sensitivity analyses. [19, 18]
- Conducted contaminant transport sensitivity analyses. [20]
- CYDER achieved integration with a fuel cycle simulator.
- Abstracted physical models of thermal and contaminant transport. [22]
- Demonstrated dominant physics of those models in CYDER, integrated with CYCLUS. [23, 17]
- Published source code, documentation, and testing to facilitate extension by external developers. [21]



Conclusion : Suggested Future Work

Further work could include

- cultivation of a developer community,
- more detailed benchmarking validation against sophisticated tools,
- comparison against experimental data, where available,
- demonstration of dynamic fuel cycle feedback sensitivities,
- additional physics (fracture models, biosphere models),
- and additional supporting data.

Acknowledgements



This work was carried out with the generous support of the **UFD Campaign** at **Argonne National Laboratory**. This work is supported by the U.S. Department of Energy, Basic Energy Sciences, Office of Nuclear Energy, under contract # DE-AC02-06CH11357.



Figure 28 : This work relied on CYCLUS, the next generation fuel cycle simulator, and its team. cyclus.github.com



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GDSM Model Advective Diffusive Sensitivity

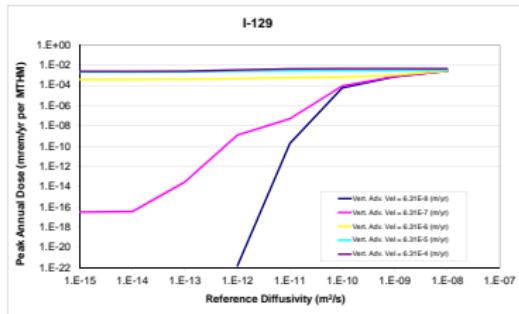


Figure 29 : ^{129}I / reference diffusivity sensitivity.

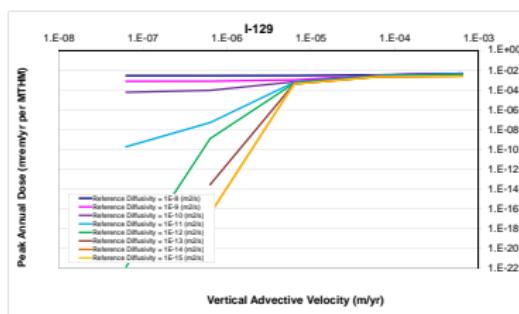


Figure 30 : ^{129}I / vertical advective velocity sensitivity.



Cyder Advective Diffusive Sensitivity

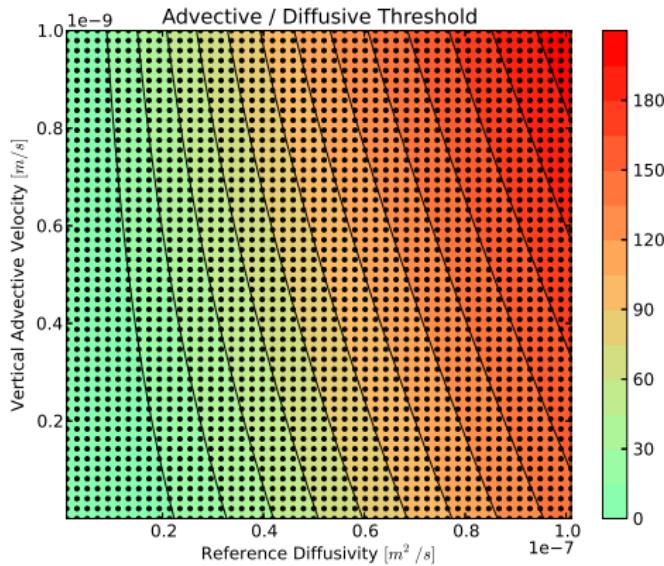


Figure 31 : Dual advective velocity and reference diffusivity sensitivity for a non-sorbing, infinitely soluble nuclide. This demonstration utilized the Degradation Rate model and the coupled advective dispersive mass transfer mode.



Outline

- ④ Thermal Methodology
- ⑤ Nuclide Transport Methodology
- ⑥ LLNL Model Background
 - Analytical Model Background
- ⑦ Geologic Media and Concepts
- ⑧ Mixed Cell Model



Thermal Modeling in Cyder

Two types of thermal modeling occur in Cyder.

- The first is **capacity estimation** for waste stream acceptance.
- The next is **heat evolution** which determines heat evolution in the modules over repository lifetime.



Thermal Modeling in Cyder

Each can be achieved with one thermal model,

- This model employs a Specific Temperature Change algorithm [30, 29] and
- relies on a supporting **response database** combining detailed spent nuclear fuel composition data [8] with a detailed thermal repository performance analysis tool from Lawrence Livermore National Lab (LLNL) and the Used Fuel Disposition (UFD) campaign [12].
- This method is capable of rapid estimation of temperature increase near emplacement tunnels as a function of
 - waste composition,
 - limiting radius, r_{lim} ,
 - waste package spacing, S ,
 - near field thermal conductivity, K_{th} ,
 - and near field thermal diffusivity, α_{th} .



Specific Temperature Change Method

Introduced by Radel, Wilson et al., the Specific Temperature Change (STC) method uses a linear approximation to arrive at the thermal loading density limit [29, 30].

First, ΔT is determined for a limiting loading density of the particular material composition then it is normalized to a single kilogram of that material, Δt , the so called STC.

$$\Delta T(r_{lim}) = m \cdot \Delta t(r_{lim}) \quad (4)$$

where

ΔT = Temperature change due to m [K]

m = Mass of heat generating material [kg]

Δt = Temperature change due to 1 kg [K/kg]

r_{lim} = Limiting radius [m].



Specific Temperature Change Superposition

For an arbitrary waste stream composition, scaled curves, Δt_i , calculated in this manner for individual isotopes can be superimposed for each isotope to arrive at an approximate total temperature change.

$$\Delta T(r_{lim}) \sim \sum_i m_i \Delta t_i(r_{lim}) \quad (5)$$

where

i = An isotope in the material [—]

m_i = mass of isotope i [kg]

Δt_i = Specific temperature change due to i [K].

LLNL UFD MathCAD Model



The analytic model used to populate the reference dataset was created at LLNL for the UFD campaign [15, 13, 12]. It employs an analytic model from Carslaw and Jaeger and is **implemented in MathCAD** [7, 28]. The integral solver in the MathCAD toolset is the primary calculation engine for the analytic MathCAD thermal model, which relies on superposition of point, finite-line, and line source integral solutions.



Specific Temperature Change Calculations

A reference data set of temperature change curves was calculated. Repeated runs of a detailed model over the range of values in Table 4 determined Specific Temperature Change (STC) values over that range.

Thermal Cases

Parameter	Symbol	Units	Value Range
Diffusivity	α_{th}	$[m^2 \cdot s^{-1}]$	$1.0 \times 10^{-7} - 3.0 \times 10^{-6}$
Conductivity	K_{th}	$[W \cdot m^{-1} \cdot K^{-1}]$	0.1 – 4.5
Spacing	S	$[m]$	2, 5, 10, 15, 20, 25, 50
Radius	r_{lim}	$[m]$	0.1, 0.25, 0.5, 1, 2, 5
Isotope	i	$[-]$	$^{241,243}Am$, $^{242,243,244,245,246}Cm$, $^{238,240,241,242}Pu$, $^{134,135,137}Cs$, ^{90}Sr

Table 4 : A thermal reference dataset of STC values as a function of each of these parameters was generated by repeated parameterized runs of the LLNL MathCAD model[12, 13].



Scaling Demonstration

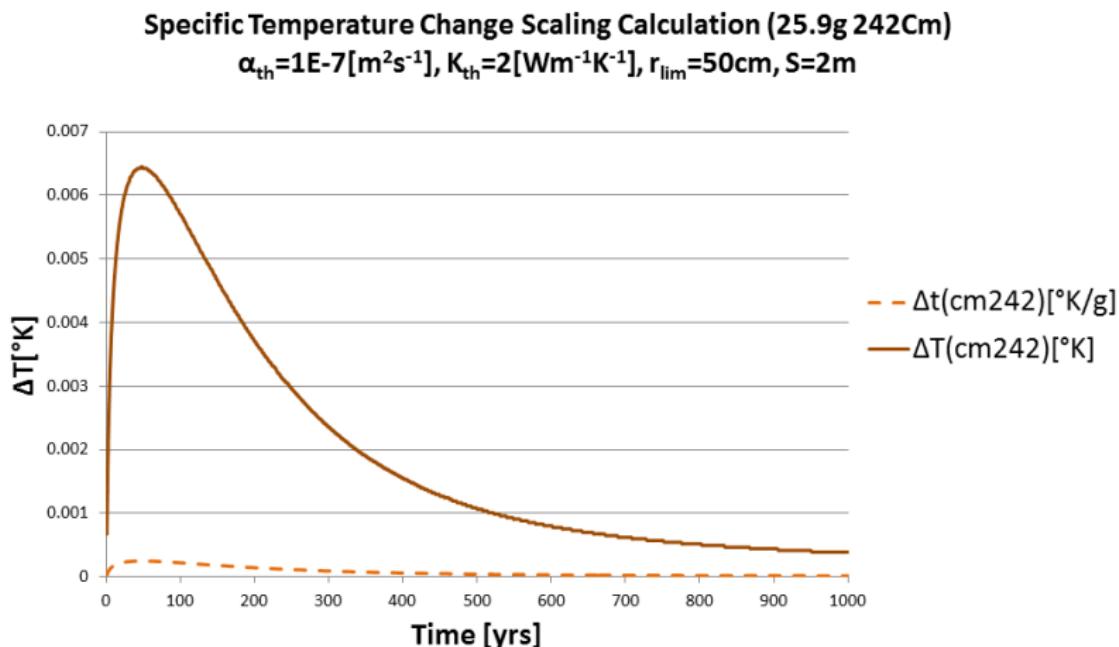


Figure 32 : As a demonstration of the calculation procedure, the temperature change curve for one initial gram of ^{242}Cm and is scaled to represent 25.9g, approximately the ^{242}Cm inventory per MTHM in 51GWD burnup UOX PWR fuel.



Superposition Concept

The supporting database was limited to some primary heat contributing isotopes present in traditional spent nuclear fuel, H , such that the superposition in equation (5) becomes

$$\Delta T(r_{lim}, S, K_{th}, \alpha_{th}) \sim \sum_{i \in H} m_i \Delta t_i(r_{lim}, S, K_{th}, \alpha_{th}) \quad (6)$$

where

$$\begin{aligned} H &= \text{set of high heat isotopes } [-] \\ S &= \text{uniform waste package spacing } [m] \\ K_{th} &= \text{thermal conductivity } [W \cdot m^{-1} \cdot K^{-1}] \\ \alpha_{th} &= \text{thermal diffusivity } [m^2 \cdot s^{-1}] \end{aligned} \quad (7)$$



Superposition Demonstration

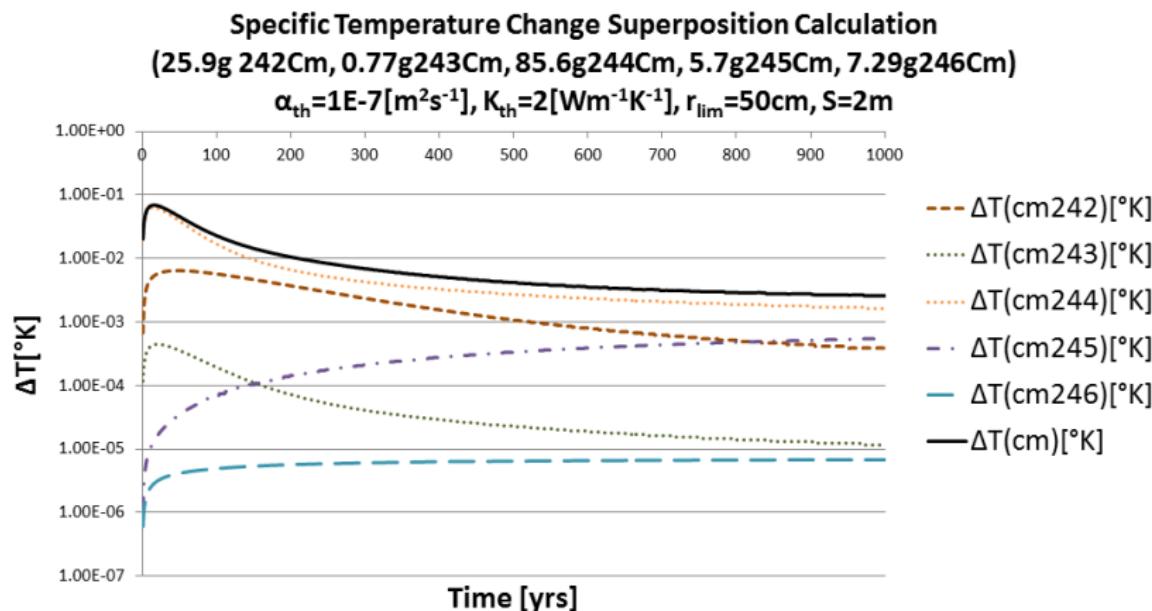


Figure 33 : As a demonstration of the calculation procedure, scaled temperature change curves for five curium isotopes are superimposed to achieve a total temperature change (note log scale)



Outline

④ Thermal Methodology

⑤ Nuclide Transport Methodology

⑥ LLNL Model Background
Analytical Model Background

⑦ Geologic Media and Concepts

⑧ Mixed Cell Model



Timestepping Algorithm

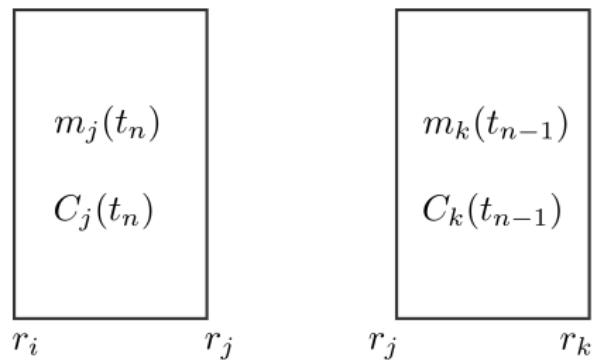


Figure 34 : Two components share an interface at r_j and contain mass and concentration profiles at the beginning of timestep t_n .



Timestepping Algorithm

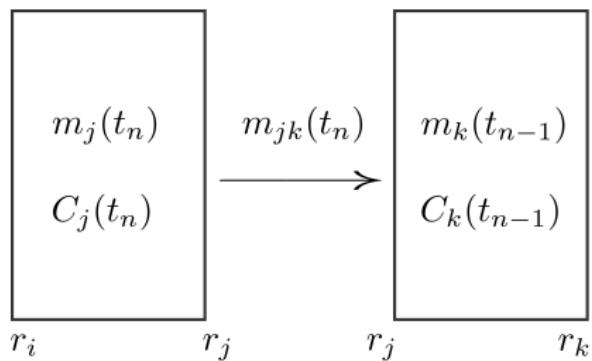


Figure 35 : The mass balance model in component k calculates the appropriate mass transfer based on boundary information from component j.



Timestepping Algorithm

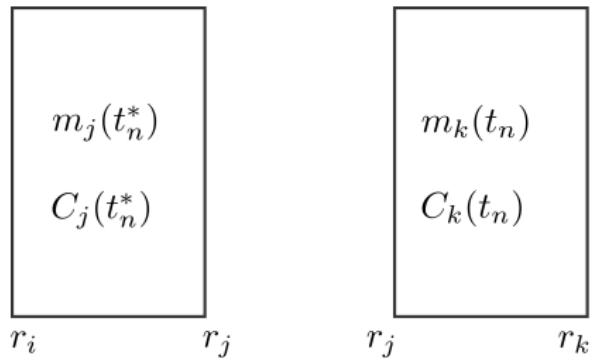


Figure 36 : Based on the mass transfer, both components update their mass and concentration profiles based on their mass balance model.



Advection Dispersion Equation

In a saturated, reducing environment, contaminants are transported by **dispersion** and **advection** [32, 37, 35]:

$$\begin{aligned}
 J &= J_{dis} + J_{adv} \\
 &= -\theta(D_{mdis} + \tau D_m)\nabla C + \theta vC \\
 &= -\theta D\nabla C + \theta vC
 \end{aligned} \tag{8}$$

where

J_{dis} = Total Dispersive Mass Flux [$kg/m^2/s$]

J_{adv} = Advective Mass Flux [$kg/m^2/s$]

τ = Toruosity [-]

θ = Porosity [-]

D_m = Molecular diffusion coefficient [m^2/s]

D_{mdis} = Coefficient of mechanical dispersivity [m^2/s]

D = Effective Dispersion Coefficient [m^2/s]

C = Concentration [kg/m^3]

v = Fluid Velocity in the medium [m/s].



Radionuclide Transport: Lumped Parameter Transport Model

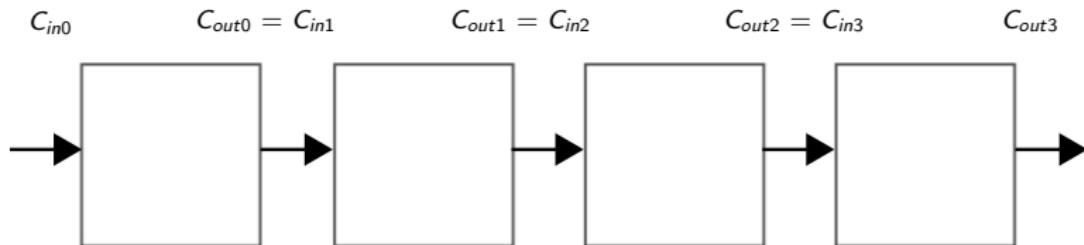


Figure 37 : The method by which each lumped parameter component is modeled is according to a relationship between the incoming concentration, $C_{in}(t)$, and the outgoing concentration, $C_{out}(t)$.

$$C_{out}(t) = \int_0^{\infty} C_{in}(t - t') g(t') e^{-\lambda t'} dt' \quad (9)$$

where

t' = time of entry [s]

$t - t'$ = transit time [s]

$g(t - t')$ = response function, a.k.a. transit time distribution [-]

λ = radioactive decay constant [s^{-1}].



Radionuclide Transport: Lumped Parameter Transport Model

Some response functions used commonly in chemical engineering applications include the Piston Flow Model (PFM), Exponential Model (EM), and the dispersion model (DM). The solutions to these for constant concentration at the source boundary are given in [25],

$$C(t) = \begin{cases} PFM & C_0 e^{-\lambda t_t} \\ EM & \frac{C_0}{1+\lambda t_t} \\ DM & C_0 e^{\frac{Pe}{2}} \left(1 - \sqrt{1 + \frac{4\lambda t_t}{Pe}} \right) \end{cases} \quad (10)$$



Lumped Parameter Model Base Case

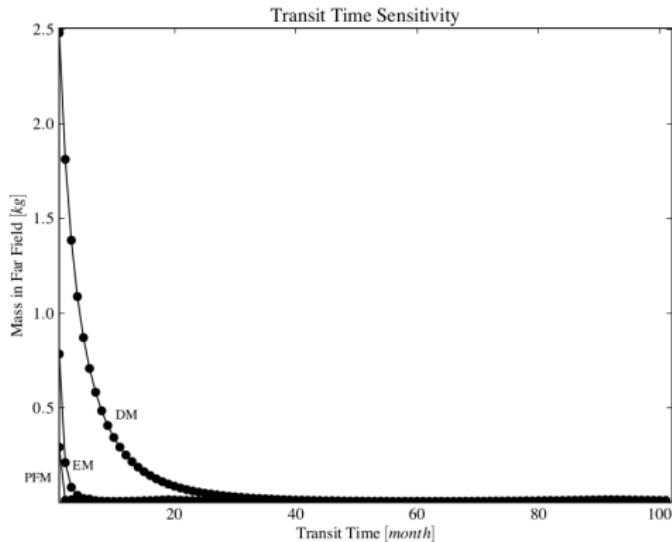


Figure 38 : The transit time parameterization of the lumped parameter model has a strong effect on the material reaching the far field after 30 months. The choice of model also strongly affects the results.



Radionuclide Transport: 1D Finite, Cauchy B.C.

For the boundary conditions,

$$-D \frac{\partial C}{\partial z} \Big|_{z=0} + v_z c = \begin{cases} v_z C_0 & (0 < t < t_0) \\ 0 & (t > t_0) \end{cases} \quad (11)$$

and

$$\frac{\partial C}{\partial z} \Big|_{z=L} = 0 \quad (12)$$

and the initial condition,

$$C(z, 0) = C_i, \quad (13)$$

the solution is given as

$$C(z, t) = \begin{cases} C_i + (C_0 - C_i) A(z, t) & 0 < t \leq t_0 \\ C_i + (C_0 - C_i) A(z, t) - C_0 A(z, t - t_0) & t \geq t_0. \end{cases} \quad (14)$$



Radionuclide Transport: 1D Finite, Cauchy B.C.

For the vertical flow coordinate system, A is defined as

$$\begin{aligned}
 A(z, t) = & \left(\frac{1}{2} \right) \operatorname{erfc} \left[\frac{Rz - vt}{2\sqrt{DRt}} \right] \\
 & + \left(\frac{v^2 t}{\pi RD} \right)^{1/2} \exp \left[-\frac{(Rz - vt)^2}{4DRt} \right] \\
 & - \frac{1}{2} \left(1 + \frac{vz}{D} + \frac{v^2 t}{DR} \right) \exp \left[\frac{vz}{D} \right] \operatorname{erfc} \left[\frac{Rz + vt}{2\sqrt{DRt}} \right] \\
 & + \left(\frac{4v^2 t}{\pi RD} \right)^{1/2} \left[1 + \frac{v}{4D} \left(2L - z + \frac{vt}{R} \right) \right] \exp \left[\frac{vL}{D} - \frac{R}{4Dt} \left(2L - z + \frac{vt}{R} \right)^2 \right] \\
 & - \frac{v}{D} \left[2L - z + \frac{3vt}{2R} + \frac{v}{4D} \left(2L - z + \frac{vt}{R} \right)^2 \right] \exp \left[\frac{vL}{D} \right] \operatorname{erfc} \left[\frac{R(2L - z) + vt}{2\sqrt{DRt}} \right]
 \end{aligned}$$

where

L = Extent of the solution domain [m]

R = Retardation factor [-].



Outline

④ Thermal Methodology

⑤ Nuclide Transport Methodology

⑥ LLNL Model Background

Analytical Model Background

⑦ Geologic Media and Concepts

⑧ Mixed Cell Model

Analytical Model : Background



The analytical model

- was created at LLNL (H. Greenberg, J. Blink, et. al) [15, 13, 12]
- employs an analytic model from Carslaw and Jaeger [7]
- is implemented in MathCAD [28]
- seeks to inform heat limited waste capacity calculations for
 - arbitrary geology
 - arbitrary waste package loading densities
 - arbitrary homogeneous decay heat source



Analytical Model : Geometry

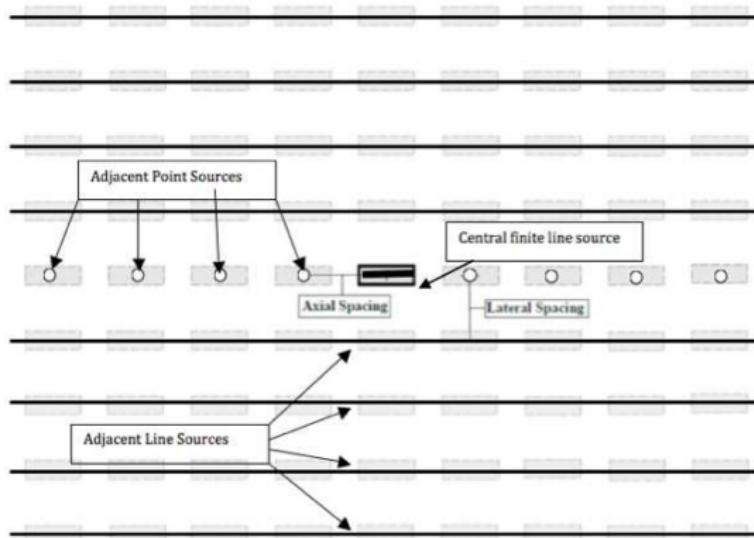


Figure 39 : Vertical, horizontal, alcove, and borehole emplacement layouts can be represented by a line of point sources and adjacent line sources [13].

Analytical Model : Calculation Method



LLNL's model is a MathCAD solution of the transient homogeneous conduction equation,

$$\nabla^2 T = \frac{1}{\alpha} \frac{\partial T}{\partial t}, \quad (15)$$

in which superimposed point and line source solutions approximate the repository layout.

Analytical Model : Calculation Method



The model consists of two conceptual regions, an external region representing the host rock and an internal region representing the waste form, package, and buffer Engineered Barrier System within the disposal tunnel wall.

- Since the thermal mass of the EBS is small in comparison to the thermal mass of the host rock, the internal region may be treated as quasi-steady state.
- The transient state of the temperature at the calculation radius is found with a convolution of the transient external solution with the steady state internal solution.
- The internal and external regions are **approximated** to be a single homogeneous medium.
- The process is then iterated with a one year resolution in order to arrive at a temperature evolution over the lifetime of the repository.



Analytical Model : Calculation Method

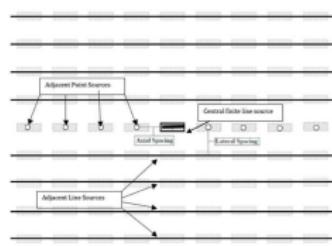


Figure 40 : The central package is represented by a finite line source [13].

The geometric layout of the analytic LLNL model in Figure 42 shows that the central package is represented by the finite line solution

$$T_{line}(t, x, y, z) = \frac{1}{8\pi K_{th}} \int_0^t \frac{q_L(t')}{t - t'} e^{-\frac{(x^2+z^2)}{4\alpha(t-t')}} \cdot \left[\operatorname{erf} \left[\frac{1}{2} \frac{(y + \frac{l}{2})}{\sqrt{\alpha(t-t')}} \right] - \operatorname{erf} \left[\frac{1}{2} \frac{(y - \frac{l}{2})}{\sqrt{\alpha(t-t')}} \right] \right] dt'. \quad (16)$$



Analytical Model : Calculation Method

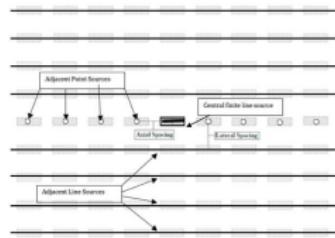


Figure 41 : Adjacent packages are represented as point sources [13].

Adjacent packages within the central tunnel are represented by the point source solution,

$$T_{point}(t, r) = \frac{1}{8K_{th}\sqrt{\alpha}\pi^{\frac{3}{2}}} \int_0^t \frac{q(t')}{(t - t')^{\frac{3}{2}}} e^{\frac{-r^2}{4\alpha(t-t')}} dt'. \quad (17)$$



Analytical Model : Calculation Method

Adjacent disposal tunnels are represented by the infinite line source solution,

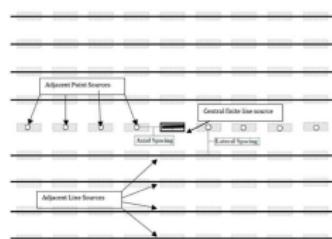


Figure 42 : The non-central disposal tunnels are represented as infinite line sources [13].

in infinite homogeneous media, where

$$\alpha = \text{ thermal diffusivity } [m^2 \cdot s^{-1}]$$

$$q(t) = \text{ point heat source } [W]$$

and

$$q_L(t) = \text{ linear heat source } [W \cdot m^{-1}]$$

Superimposed point and line source solutions allow for a notion of the repository layout to be modeled in the host rock.



Outline

- ④ Thermal Methodology
- ⑤ Nuclide Transport Methodology
- ⑥ LLNL Model Background
 - Analytical Model Background
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Repository Components

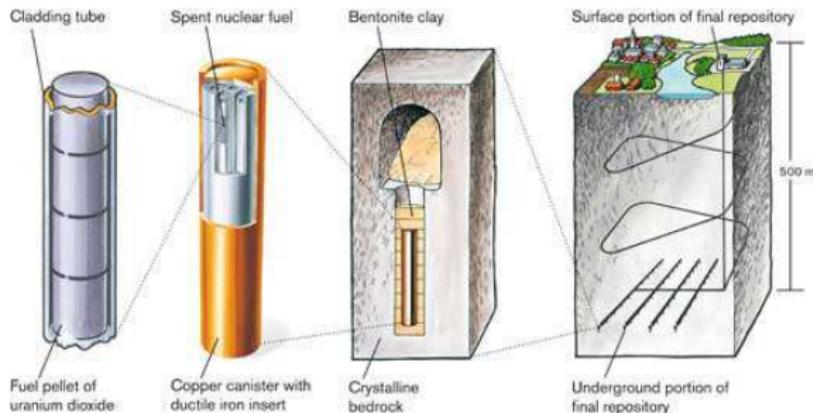


Figure 43 : Geologic disposal systems typically employ engineered barrier systems as well as natural barrier systems. This is a Swedish concept in granite [1].



Clay Disposal Environments

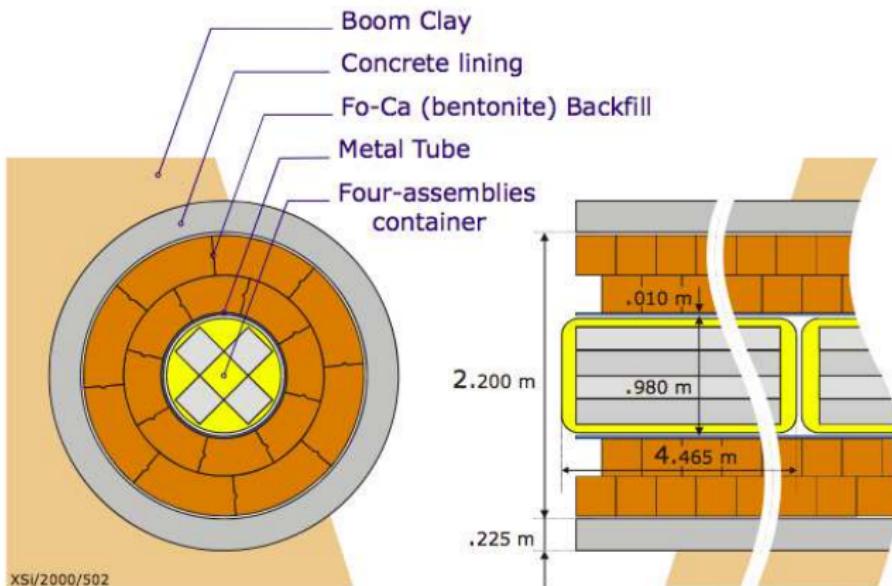


Figure 44 : Belgian reference concept in Boom Clay [36].



Granite Disposal Environments

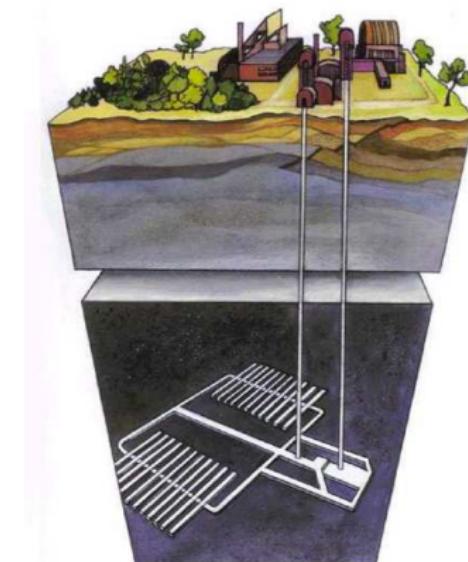


Figure 45 : Czech reference concept in Granite [36].



Salt Disposal Environments

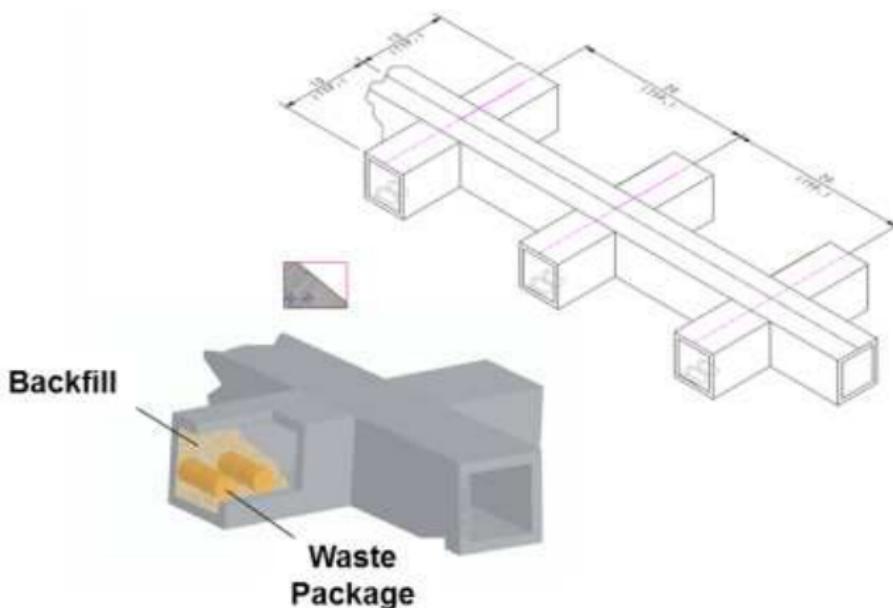


Figure 46 : DOE-NE Used Fuel Disposition Campaign concept in Salt [15].



Salt Disposal Environments

**Recess for
better heat
transfer**

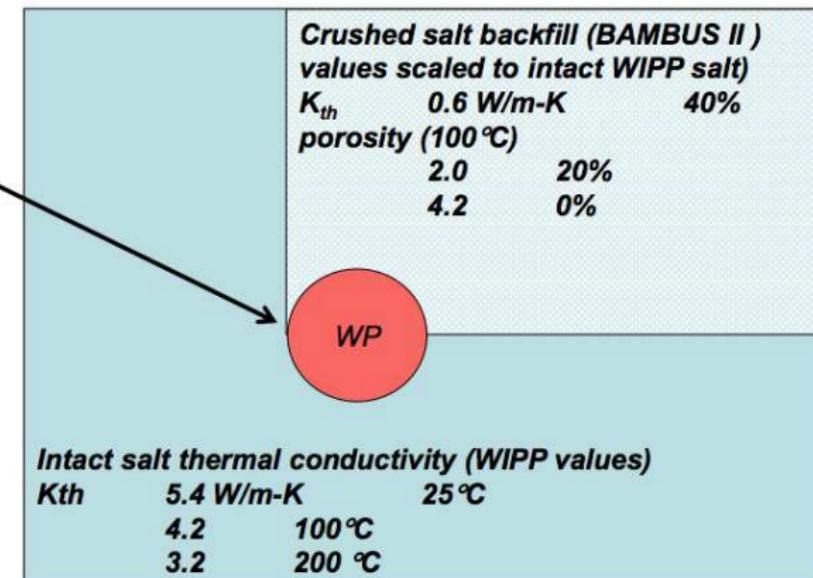


Figure 47 : DOE-NE Used Fuel Disposition Campaign concept in Salt [15].



Deep Borehole Disposal Environment

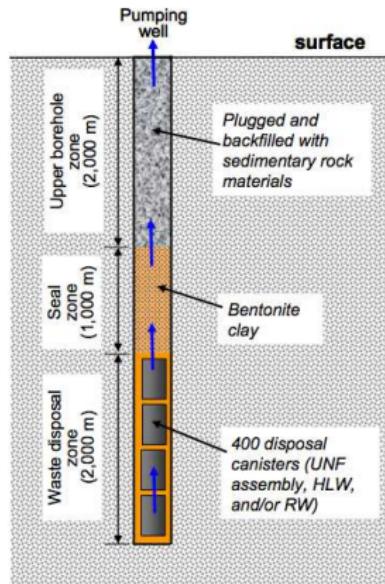


Figure 48 : DOE-NE Used Fuel Disposition Campaign Deep Borehole concept [15].



Engineered Barriers : Waste Forms

The first line of defense is the waste form.

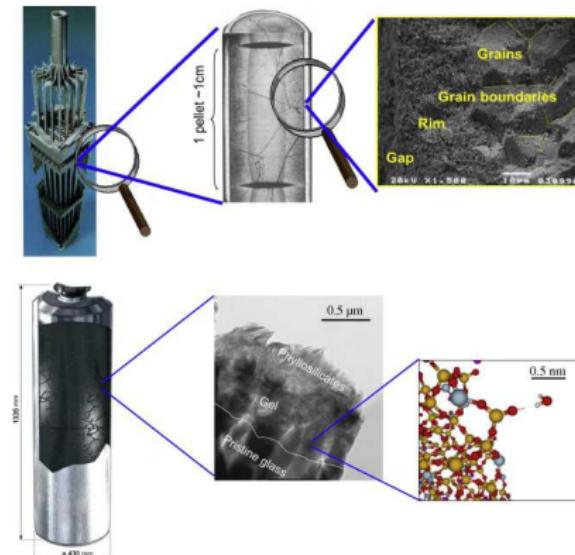


Figure 49 : A comparison of uranium oxide and borosilicate glass waste forms [27].



Engineered Barriers : Waste Packages

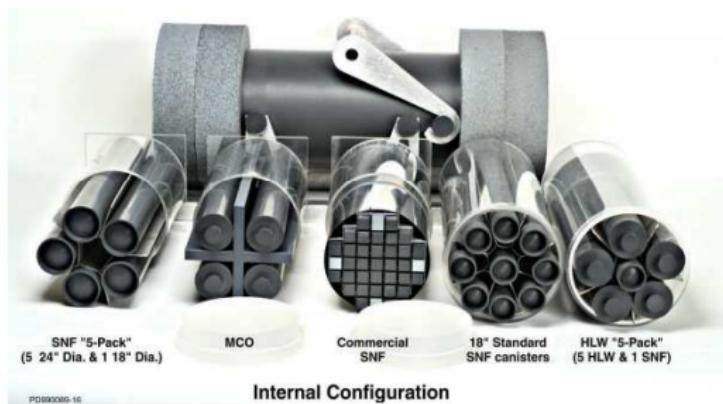


Figure 50 : Conceptual mockup of waste packages around waste forms [5].



Engineered Barriers : Disposal Cask



Figure 3. Conceptual design model.

Figure 51 : Conceptual mockup of a transport and disposal cask [5].



Engineered Barriers : Buffer

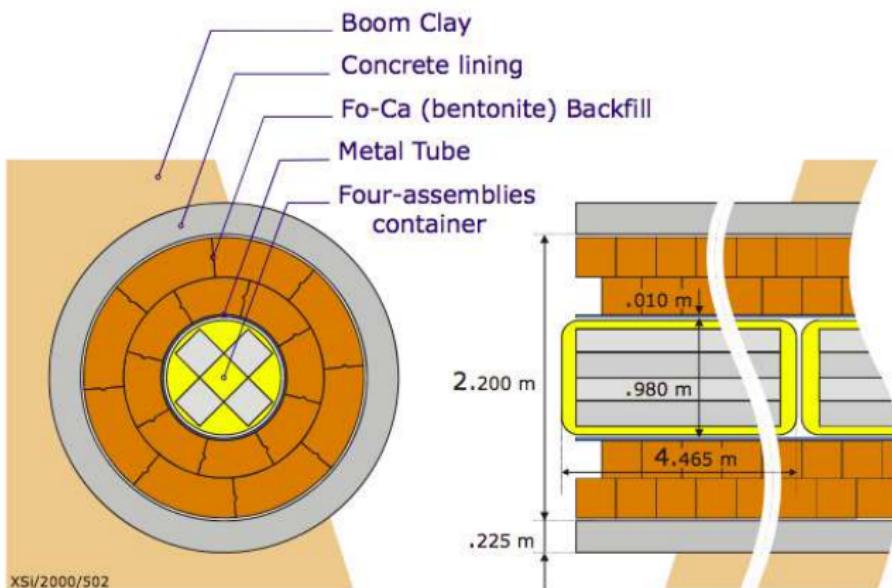


Figure 52 : Belgian reference concept in Boom Clay [36].



Natural Barrier : Geology

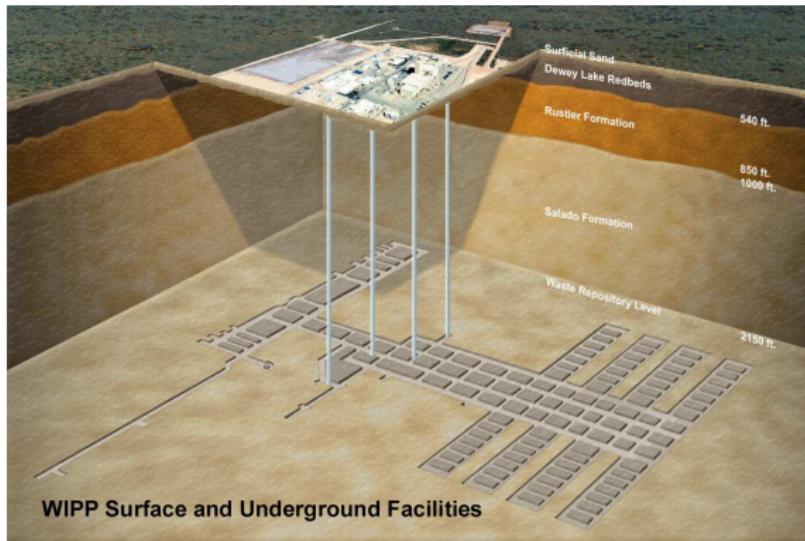
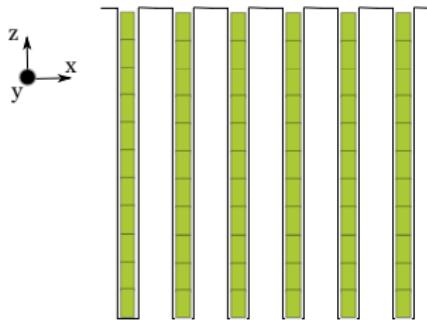


Figure 53 : The Waste Isolation Pilot Plant has many geologic layers above the salt bed [10].

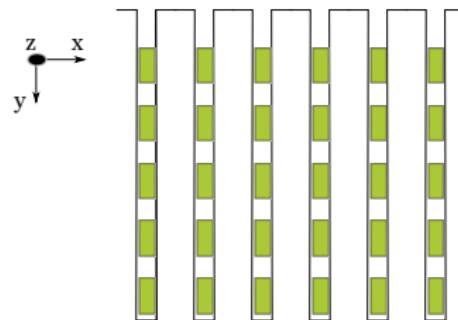


Repository Layouts

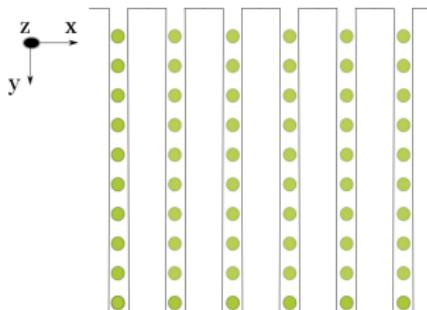
Deep Boreholes



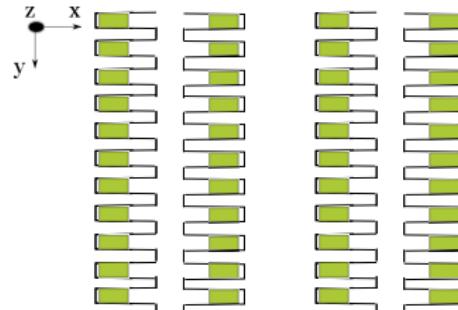
Horizontal In-Tunnel



Vertical In-Tunnel



Alcoves





Outline

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 - Analytical Model Background
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- ⑧ Mixed Cell Model



Radionuclide Transport : Mixed Cell Sorption

The mass of contaminant sorbed into the degraded and precipitated solids can be found using a linear isotherm model [32], characterized by the relationship

$$s_i = K_{di} c_i \quad (19)$$

where

s_i = the solid concentration of isotope i [kg/kg]

K_{di} = the distribution coefficient of isotope i [m^3/kg]

c_i = the liquid concentration of isotope i [kg/m^3].

From the sorbed contaminant mass, we find the non-sorbed contaminant mass in the free fluid,

$$\begin{aligned} m_{ffl} &= m_{ffT} - \frac{1}{2} \left(m_{ffT} - m_{psm} - \frac{V_{ff}}{K_d} \right) \\ &\mp \frac{1}{2} \sqrt{m_{ffT}^2 + 2m_{ffT} \left(m_{psm} - \frac{V_{ff}}{K_d} \right) + \left(m_{psm} + \frac{V_{ff}}{K_d} \right)^2}. \end{aligned} \quad (20)$$

where

m_{ffT} = total degraded contaminant mass [kg]

m_{psm} = noncontaminant mass in degraded and precipitated solids [kg]

m_{psc} = contaminant mass in degraded and precipitated solids [kg]

ρ_b = bulk (dry) density of the medium [kg/m^3].