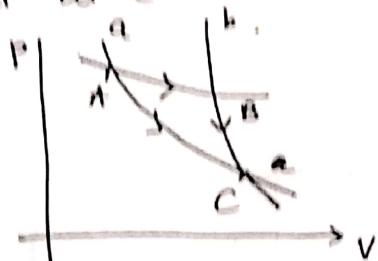


Solution Set for HW 2

1. Assume that two reversible adiabatic lines a, b intersect at C .



Consider an isothermal line that intersects with a, b at A, B . [Convince yourself that such a line can always be found.]

Then the cycle $A \rightarrow B \rightarrow C \rightarrow A$ can be considered as a reversible cycle in which the system takes a positive amount of heat Q_s from the environment only during the leg $A \rightarrow B$ and does positive work $W = (\text{area } ABC)$. By first law $Q_s = W$ since $\Delta U = 0$.

So in this cycle the system has taken a positive amount of heat Q_s from a source and converted it entirely into work without any other change \Rightarrow contradicts Kelvin-Planck statement.

$\Rightarrow a, b$ cannot intersect.

Note: As brought up in class, this does not hold true for a reversible and irreversible adiabatic curve. e.g. You can start out an adiabatic quasistatic process and an adiabatic free expansion from the same initial conditions. Of course a free expansion curve cannot be plotted on a PV diagram.

- 2 (a) From Maxwell relations.

$$(5) \quad \left(\frac{\partial S}{\partial V} \right)_T = \left(\frac{\partial P}{\partial T} \right)_V = \frac{P}{T}, \quad P, T > 0$$

Here $P = kT$.

$$\left(\frac{\partial P}{\partial T} \right)_V = k = \frac{P}{T}$$

$$\left(\frac{\partial S}{\partial V} \right)_T > 0.$$

entropy increases with volume.

$$2(b) . \quad (5) \quad \left(\frac{\partial H}{\partial P} \right)_T$$

$$dH = TdS + VdP.$$

$\frac{\partial H}{\partial P}$ Isenthalpic process. ($J-T$)

$$dH = 0$$

Joule Thomson coeff.

$$\left(\frac{\partial T}{\partial P} \right)_H > 0 \text{ for cooling.}$$

$$\text{Now; } \left(\frac{\partial H}{\partial P} \right)_T = - \frac{\left(\frac{\partial H}{\partial T} \right)_P}{\left(\frac{\partial P}{\partial T} \right)_H} = - \frac{C_P}{\left(\frac{\partial P}{\partial T} \right)_H}.$$

$$C_P > 0.$$

$$\therefore \left(\frac{\partial H}{\partial P} \right)_T = - \frac{C_P}{\left(\frac{\partial P}{\partial T} \right)_H} < 0$$

3. (i). Equation of state.

$$(5) \quad PV = \frac{1}{3}U ; \quad \phi = \frac{1}{3}u. \quad \text{--- ①}$$

We have derived in class

$$\left(\frac{\partial U}{\partial V} \right)_T = T \left(\frac{\partial P}{\partial T} \right)_V - P \quad \text{--- ②}$$

[Using ① in ②]

$$u = \frac{1}{3} T \frac{du}{dT} - \frac{1}{3} u.$$

$$4 \frac{dT}{T} = \frac{du}{u}.$$

$$\boxed{u = cT^4}.$$

$$(ii) \quad TdS = dU + \phi dV.$$

3 (ii)

(5)

entropy density.

$$Tds = dU + pdV \quad \left. \begin{array}{l} U = cT^4 V \\ dU = cT^4 dV + 4cT^3 V dT \end{array} \right\}$$

$$Tds = cT^4 dV + 4cT^3 V dT$$

$$+ \frac{C}{3} T^4 dV$$

$$ds = \frac{4}{3} cT^3 dV + 4cT^2 V dT$$

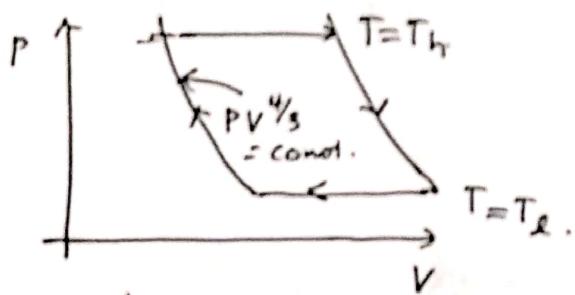
$$ds = d\left(\frac{4}{3} cT^3 V\right)$$

$$S = \frac{4}{3} cT^3 V + S_0 \text{ by given bdy condn.}$$

$$\boxed{S = \frac{S}{V} = \frac{4}{3} cT^3}$$

(iii) Adiabatic for this gas. $\Rightarrow VT^3 = \text{const.}$ isothermal $P = \text{const.} \rightarrow PV^{4/3} = \text{const.}$

(5)



\hookrightarrow Carnot cycle.

⑩
4.
(10)

$$\text{Heat Capacity } C = aT^3 = \left(\frac{\partial U}{\partial T}\right)_V.$$

$$dQ_L = aT_L^3 dT_L.$$

For the refrigerator

$$Q_L + W = Q_h.$$

$$dW = \left(1 - \frac{T_L}{T_h}\right) Q_h. = \left(I_h - \frac{T_L}{T_h}\right) \frac{Q_L}{T_L}.$$

$$dW = \left(T_h - T_L\right) \frac{dQ_L}{T_L}$$

$$= a \left(\frac{T_h}{T_L} - 1\right) a T_L^3 dT_L \quad \left. \begin{array}{l} T_h = T_i, \text{ if } T_L \\ dT_L \end{array} \right\}$$

$$W = T_h \int_{T_i}^0 a T_L^3 dT_L - \int_{T_i}^0 a T_L^3 dT_L.$$

$$W = \frac{a}{3} \left(-T_i^3 T_h\right) + a \frac{T_i^4}{4}. \quad T_h = T_i$$

$$W = -\frac{a}{3} T_h^4 + a \frac{T_h^4}{4}.$$

$$\downarrow = -\frac{a T_h^3}{12} - \frac{a T_h^4}{12}.$$

work done by the system

$$\text{Electrical energy required} = \frac{a T_h^4}{12}.$$

5.

 T_h and T_l

$$(10) \quad W = (T_h - T_l) \frac{Q_l}{T_l}.$$

$$\stackrel{?}{=} \left(\frac{T_h}{T_l} - 1 \right) Q_l.$$

$$P = \left(\frac{T_h}{T_l} - 1 \right) \frac{dQ_l}{dt}.$$

$$= \left(\frac{T_h}{T_l} - 1 \right) A (T_h - T_l).$$

$$\Rightarrow \frac{P}{A} T_l = (T_h - T_l)^2.$$

$$\Rightarrow T_l^2 - 2 T_l T_h + \frac{P}{A} T_l + T_h^2 = 0.$$

$$\boxed{T_l = T_h + \frac{P}{2A} - \sqrt{\left(T_h + \frac{P}{2A}\right)^2 - T_{h2}}}$$

minus sign taken since
 $T_l < T_h$