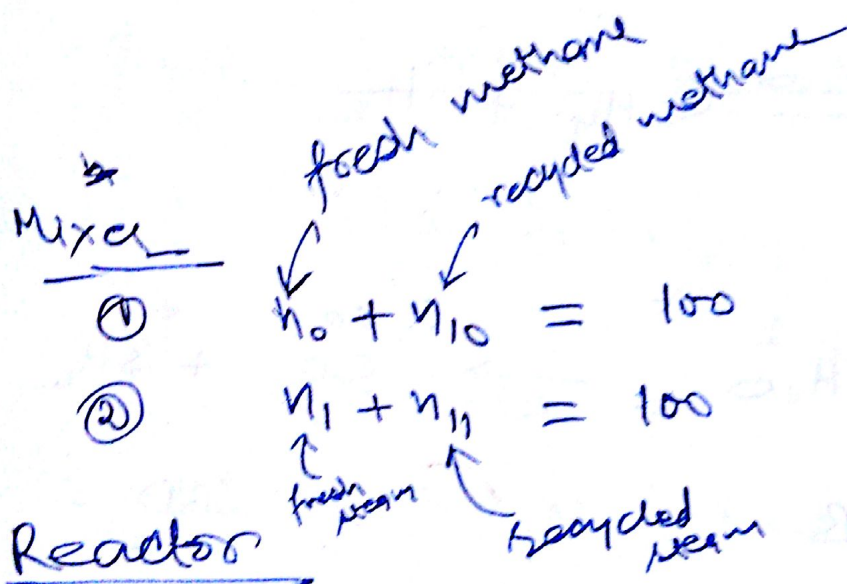
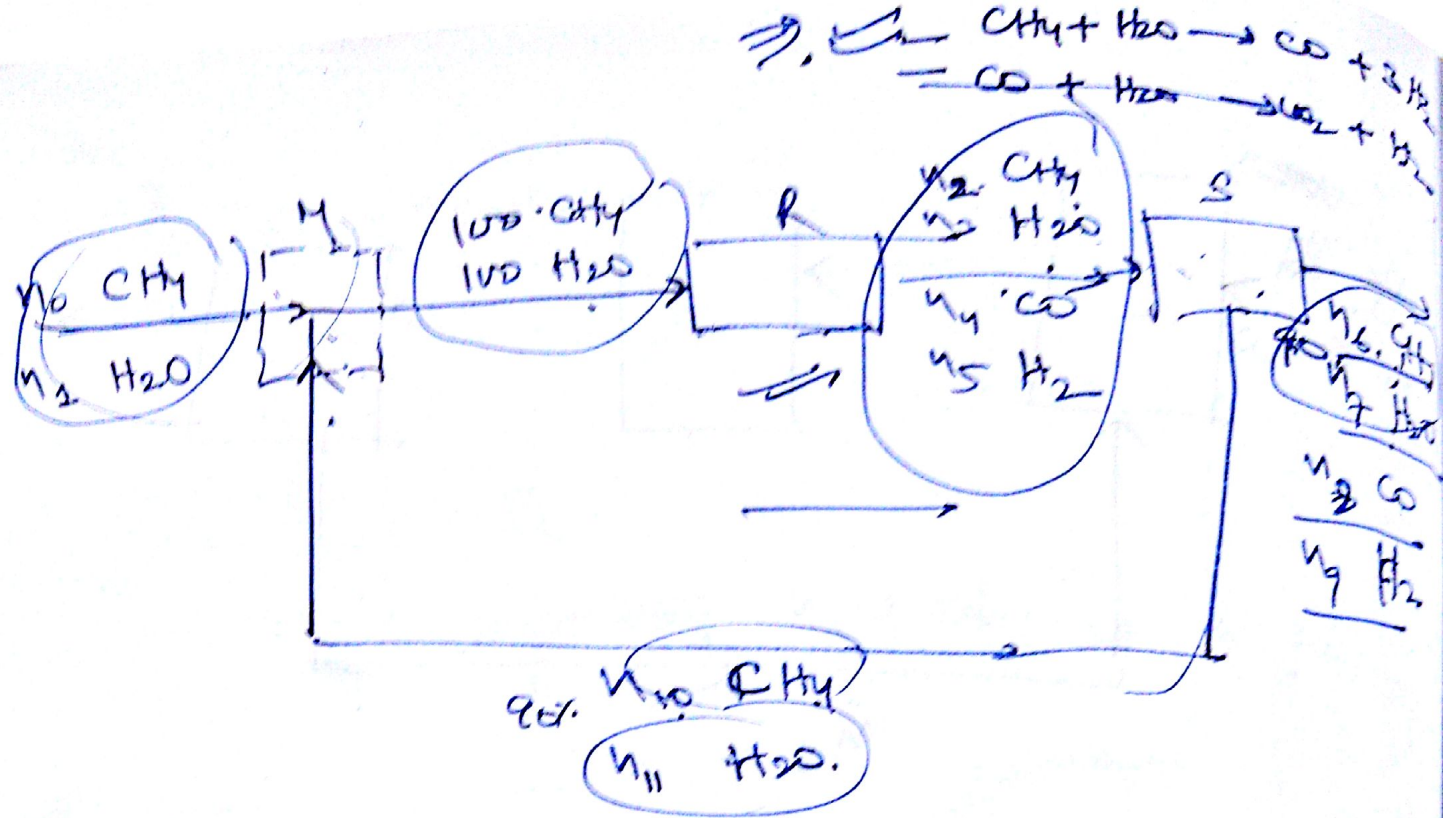


for 99.1.

$$\frac{0.91 \times 2.97^3}{0.01 \times 0.01}$$

for 20.1.

$$\frac{0.9 \times 2.7^3}{0.1 \times 0.1}$$



③ $n_0 = n_1$
 ④ $n_{10} = n_{11}$

Reactor

$$n_2 = 100 - \Sigma_1$$

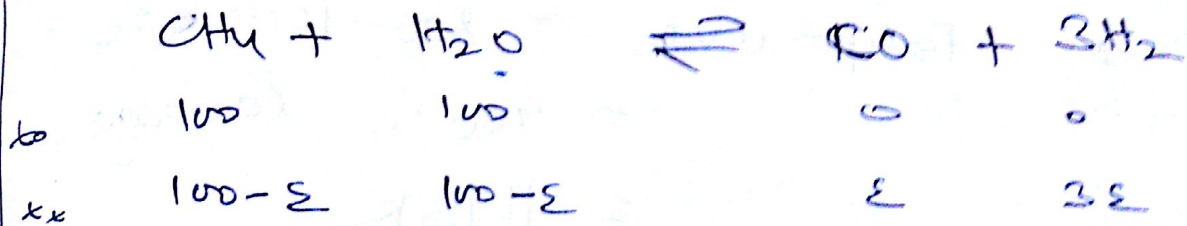
$$n_3 = n_2 = 100 - \Sigma_1$$

$$n_4 = \Sigma_1$$

$$n_5 = 3\Sigma_1 = 3n_4$$

$$\begin{aligned}
 n_{\text{tot}} &= n_2 + n_3 + n_4 + n_5 \\
 &= 200 + 2\Sigma_1
 \end{aligned}$$

Assuming 90% conversion



for 90% conv,

$$\frac{\Sigma (3\Sigma)^3}{(200 + 2\Sigma)^2 (100 - \Sigma)(100 - \Sigma)} = \frac{0.9 \times 2 \times (3 \times 0.9)^2}{(1 + 1.8)^2 (1 - 0.9)(1 - 0.9)}$$

or simply

$\Sigma = 0.9$

 $\Sigma = 90$

Separator (assuming separator efficiency 90%)
Methane / steam split

$$\left. \begin{aligned} n_6 &= 0.01 n_2 \\ n_2 &= n_6 + n_{10} \end{aligned} \right\} \text{for CH}_4$$

$$\left. \begin{aligned} n_7 &= 0.01 n_3 \\ n_3 &= n_7 + n_{11} \end{aligned} \right\} \text{for H}_2\text{O}$$

Typical

Typically

$$\begin{aligned} \rightarrow \text{Temperature} &\sim 800-1000^\circ\text{C} \\ &\equiv 900^\circ\text{C} \text{ (average)} \\ &\equiv 1173\text{K} \end{aligned}$$

$$\begin{aligned} \rightarrow \text{Pressure} &\sim 30-40 \text{ bar} \\ &\equiv 35 \text{ bar (average)} \end{aligned}$$

From "Case Modules on energy
in the curriculum"

$$K_{SR} = \frac{y_{\text{H}_2}^3 y_{\text{CO}}}{y_{\text{CH}_4} y_{\text{H}_2\text{O}}} P_{\text{Tot}}^2$$

$$= \frac{n_{\text{H}_2}^3 n_{\text{CO}}}{n_{\text{CH}_4} n_{\text{H}_2\text{O}} n_{\text{Tot}}^2} P_{\text{Tot}}^2$$

$$= \exp\left(\frac{30.42 - 27106}{RT}\right)$$

$$= \exp\left(30.42 - \frac{27106}{1173}\right) \quad \left[\text{for } T=1173\text{K}\right]$$

$$= 1617.2$$

going by this approach

$$\frac{\varepsilon (3\varepsilon)^2}{(200 + 2\varepsilon)^2 (100 - \varepsilon)(100 - \varepsilon)} = 1617.2$$

becomes our equilibrium relation

