

Microscopic Simulation of Solid State Sintering Regarding Irregularly Shaped Powder Particles

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July 31, 2023

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Preface

1 Introduction

1.1 The RefraBund Project

1.1.1 Aim and Scope

1.1.2 Project Structure

1.1.3 Process Routes

1.2 State of the Art

1.2.1 Basic Theory of Sintering

1.2.2 Sintering Models with Sharp Interfaces

1.2.3 Sintering Models with Diffuse Interfaces

1.2.4 Monte-Carlo-Methods (MCM)

Classic Monte Carlo Methods

Kinetic Monte Carlo Methods

1.2.5 The Thermodynamic Extremal Principle (TEP)

General things about internal state and non-equilibrium
Applications

Classic Formulation

The classic formulation of the principle was basically formulated by Svoboda and Turek [4], however dependent on the works of Ziegler [5, 6] and Onsager [3]. It is based on the assumption, that the dissipation in the system is always maximized with respect to thermodynamic and kinetic constraints. This is equivalent to the statement, that the system always tries to approach the equilibrium as fast as possible.

The dissipation \mathcal{D} can be formulated as in Equation 1.1a in dependence on the vector of external state variables \mathbf{X} , the vector of internal state variables \mathbf{x} and the velocity vector of internal state variables $\dot{\mathbf{x}}$. It is a bilinear form in the velocity vector of internal state variables and the vector of thermodynamik forces. The latter can be expressed as $\partial G(\mathbf{X}, \mathbf{x})/\partial \mathbf{x}$, where G is the Gibbs energy of the system. The Gibbs energy is as state function independent of $\dot{\mathbf{x}}$, thus the thermodynamic forces do not include any kinetic constraints. Since \mathcal{D} is linear in $\dot{\mathbf{x}}$, maximizing without further constraints is not meaningful. Therefore, an additional dissipation function \mathcal{Q} is introduced, which must be always equal to \mathcal{D} , since both describe the dissipation of the process (compare Equation 1.1b). However, \mathcal{Q} is formulated in terms of the kinetic conditions of the process and is generally and non-linear form in $\dot{\mathbf{x}}$, often a quadratic form. The actual form of

\mathcal{Q} heavily depends on the regarded process, but it commonly includes empirical kinetic material parameters such as diffusion coefficients or mobilities.

$$\mathcal{D}(\mathbf{X}, \mathbf{x}, \dot{\mathbf{x}}) = \frac{\partial G(\mathbf{X}, \mathbf{x})}{\partial \mathbf{x}} \cdot \dot{\mathbf{x}} \rightarrow \max_{\dot{\mathbf{x}}} \quad (1.1a)$$

$$\mathcal{D}(\mathbf{X}, \mathbf{x}, \dot{\mathbf{x}}) - \mathcal{Q}(\mathbf{X}, \mathbf{x}, \dot{\mathbf{x}}) = 0 \quad (1.1b)$$

The constrained optimization problem in Equation 1.1 can be solved using the Lagrange formalism. The problem is reformulated as the Lagrange functional \mathcal{L} in Equation 1.2 with the additional parameter λ .

$$\mathcal{L} = \mathcal{D}(\mathbf{X}, \mathbf{x}, \dot{\mathbf{x}}) + \lambda (\mathcal{D}(\mathbf{X}, \mathbf{x}, \dot{\mathbf{x}}) - \mathcal{Q}(\mathbf{X}, \mathbf{x}, \dot{\mathbf{x}})) \quad (1.2)$$

Setting the gradient of \mathcal{L} with respect to $\dot{\mathbf{x}}$ and λ equal zero gives the optimum of the dissipation \mathcal{D} under the given constraints. Note that the derivative with respect to λ is always identical to the constraint equation.

$$\mathcal{L}_{\dot{\mathbf{x}}} = (1 + \lambda) \frac{\partial G(\mathbf{X}, \mathbf{x})}{\partial \mathbf{x}} - \lambda \frac{\partial \mathcal{Q}(\mathbf{X}, \mathbf{x}, \dot{\mathbf{x}})}{\partial \dot{\mathbf{x}}} \stackrel{!}{=} 0 \quad (1.3a)$$

$$\mathcal{L}_{\lambda} = \mathcal{D}(\mathbf{X}, \mathbf{x}, \dot{\mathbf{x}}) - \mathcal{Q}(\mathbf{X}, \mathbf{x}, \dot{\mathbf{x}}) \stackrel{!}{=} 0 \quad (1.3b)$$

For the simple case of \mathcal{Q} being quadratic in $\dot{\mathbf{x}}$ the solution of the system is given in Equation 1.4, which is a linear system of equations of the same size as $\dot{\mathbf{x}}$. Compare Svoboda and Turek [4] and Fischer, Svoboda, and Petryk [1] on this.

$$-\frac{\partial G(\mathbf{X}, \mathbf{x})}{\partial \mathbf{x}} = \frac{1}{2} \frac{\partial \mathcal{Q}(\mathbf{X}, \mathbf{x}, \dot{\mathbf{x}})}{\partial \dot{\mathbf{x}}} \quad (1.4)$$

Note, that for this formulation it is required, that the dissipation \mathcal{D} and the dissipation function \mathcal{Q} must depend on the same kinetic variables $\dot{\mathbf{x}}$. Often the fluxes \mathbf{j} are used therein.

Generalized Formulation

Recently, Hackl, Fischer, and Svoboda [2] published a generalized formulation of the principle breaking up the need to have the same kinetic variables in the dissipation \mathcal{D} and the dissipation function \mathcal{Q} . The following elaborations use a different notation than in the reference, which fits better to the needs of the application in section 4.6, but the meaning is generally equivalent. The dissipation \mathcal{D} is defined in the same way as before, but the dissipation function \mathcal{Q} does not include the velocities of internal state $\dot{\mathbf{x}}$, but instead the fluxes \mathbf{j} as in Equation 1.5b. Note, that the velocities $\dot{\mathbf{x}}$ are *not* required to be identical to the fluxes \mathbf{j} here. The connections between the velocities $\dot{\mathbf{x}}$ and the fluxes \mathbf{j} are introduced by the constraints \mathbf{f} as in Equation 1.5c. These are required to be able to solve the problem, so they shall be called *required* constraints hereinafter. The sizes of $\dot{\mathbf{x}}$, \mathbf{j} and \mathbf{f} must be equal. But it is also possible to include several *additional* constraints \mathbf{g} . These may be used for other requirements on the validity of the model, for example geometric constraints. See section 4.6 for details on their application.

$$\mathcal{D}(\mathbf{X}, \mathbf{x}, \dot{\mathbf{x}}) = \frac{\partial G(\mathbf{X}, \mathbf{x})}{\partial \mathbf{x}} \cdot \dot{\mathbf{x}} \rightarrow \max_{\dot{\mathbf{x}}} \quad (1.5a)$$

$$\mathcal{D}(\mathbf{X}, \mathbf{x}, \dot{\mathbf{x}}) - \mathcal{Q}(\mathbf{X}, \mathbf{x}, \mathbf{j}) = 0 \quad (1.5b)$$

$$\mathbf{f}(\mathbf{X}, \mathbf{x}, \dot{\mathbf{x}}, \mathbf{j}) = 0 \quad (1.5c)$$

$$\mathbf{g}(\mathbf{X}, \mathbf{x}, \dot{\mathbf{x}}, \mathbf{j}) = 0 \quad (1.5d)$$

With this generalized formulation the Lagrange functional writes as in Equation 1.6. Here we have more Lagrange parameters. λ_1 is equivalent to the classic formulation. The vector parameters λ_2 and λ_3 for the required and additional constraints are of the same size as \mathbf{f} resp. \mathbf{g} .

$$\mathcal{L} = \mathcal{D}(\mathbf{X}, \mathbf{x}, \dot{\mathbf{x}}) + \lambda_1 (\mathcal{D}(\mathbf{X}, \mathbf{x}, \dot{\mathbf{x}}) - \mathcal{Q}(\mathbf{X}, \mathbf{x}, \dot{\mathbf{x}})) + \lambda_2 \cdot \mathbf{f}(\mathbf{X}, \mathbf{x}, \dot{\mathbf{x}}, \mathbf{j}) + \lambda_3 \cdot \mathbf{g}(\mathbf{X}, \mathbf{x}, \dot{\mathbf{x}}, \mathbf{j}) \quad (1.6)$$

As before, the gradient of \mathcal{L} is set equal to zero to obtain the constrained optimum. Finding a simplified equation system as done above (Equation 1.4) is here not possible due to the constraints.

$$\mathcal{L}_{\dot{\mathbf{x}}} = (1 + \lambda_1) \frac{\partial G(\mathbf{X}, \mathbf{x})}{\partial \mathbf{x}} - \lambda_1 \frac{\partial \mathcal{Q}(\mathbf{X}, \mathbf{x}, \dot{\mathbf{x}})}{\partial \dot{\mathbf{x}}} + \lambda_2 \frac{\partial \mathbf{f}(\mathbf{X}, \mathbf{x}, \dot{\mathbf{x}}, \mathbf{j})}{\partial \dot{\mathbf{x}}} + \lambda_3 \frac{\partial \mathbf{g}(\mathbf{X}, \mathbf{x}, \dot{\mathbf{x}}, \mathbf{j})}{\partial \dot{\mathbf{x}}} \stackrel{!}{=} 0 \quad (1.7a)$$

$$\mathcal{L}_{\lambda_1} = \mathcal{D}(\mathbf{X}, \mathbf{x}, \dot{\mathbf{x}}) - \mathcal{Q}(\mathbf{X}, \mathbf{x}, \dot{\mathbf{x}}) \stackrel{!}{=} 0 \quad (1.7b)$$

$$\mathcal{L}_{\lambda_2} = \mathbf{f}(\mathbf{X}, \mathbf{x}, \dot{\mathbf{x}}, \mathbf{j}) \stackrel{!}{=} 0 \quad (1.7c)$$

$$\mathcal{L}_{\lambda_3} = \mathbf{g}(\mathbf{X}, \mathbf{x}, \dot{\mathbf{x}}, \mathbf{j}) \stackrel{!}{=} 0 \quad (1.7d)$$

1.2.6 Miscellaneous

2 Aim and Scope

3 Powder Analysis and Representation

3.1 Classic Methods of Powder Characterization

3.2 Particle Description by Parametrized Shape Functions

3.3 Characterization of Powders and Powder Mixtures

4 Model Development

4.1 A Discrete Model of Powder Particles

- Particles, Coordinate System
- Node Types
- Multi-Scale Considerations, Matrix

4.2 Considerations on Free Surfaces

4.3 Considerations on Grain Boundaries

4.4 Considerations on Sinter Necks

4.5 Considerations on Grain-Matrix Interfaces

4.6 Application of the Thermodynamic Extremal Principle (TEP)

5 Software Implementation of the Model

Reference to open source code

5.1 Representation of Particles and Nodes

- Classes
- Tree Structure
- Coordinate Systems

5.2 Numerical Solution Procedure

- TEP Solution
- Time Step
- Monte-Carlo Drawing

5.3 Calculation and Extraction of Key Features

- Volume Cell, Shrinkage
- Neck Measures

6 Model Validation

6.1 Investigations on Simple Test Cases

6.1.1 A Single Particle Free in Space

6.1.2 A Particle Pair Free in Space

6.1.3 A Particle Pair at Different Contact Angles

6.1.4 A Particle Pair with Asymmetric Material Properties

6.1.5 A Single Particle Embedded in a Matrix

6.1.6 A Particle Pair Embedded in a Matrix

6.2 Experimental Validation Counter Bulk Sintering Trials

7 Summary and Outlook

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