



Convection

Numerical Flow Simulation

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Simple "model" equations

General conservation equation:

$$\frac{\partial(\rho\phi)}{\partial t} + div(\rho\phi\mathbf{u}) = div(\Gamma grad(\phi)) + S$$
 unsteadiness convection diffusion source

Steady/unsteady diffusion (e.g. heat conduction):

$$\frac{div(\Gamma grad(\phi))}{\partial t} + S = 0$$

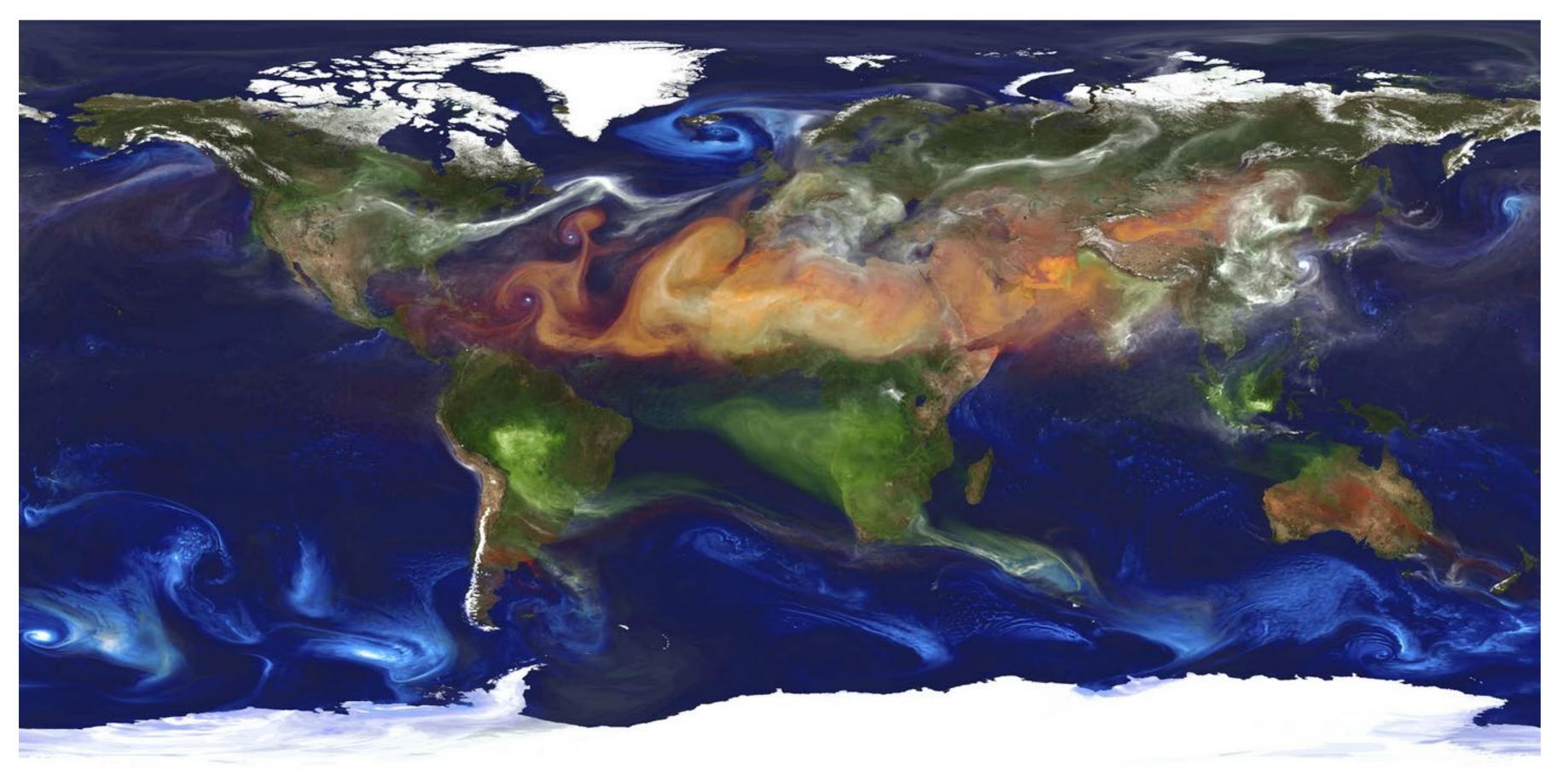
$$\frac{\partial(\rho\phi)}{\partial t} = div(\Gamma grad(\phi))$$

Steady convection-diffusion (transport of a scalar, e.g. dye, salt, chemical species):

$$div(\rho\phi\mathbf{u}) = div(\Gamma \operatorname{grad}(\phi))$$



Convection-diffusion



Atmospheric simulation (GEOS-5 simulation, 10-km grid size), NASA Center for Climate Simulation at Goddard Space Flight Center. Dust (red) is lifted from the surface, sea salt (blue) swirls inside cyclones, smoke (green) rises from fires, and sulfate particles (white) stream from volcanoes and fossil fuel emissions.

1D steady convection-diffusion

$$\frac{d(\rho\phi u)}{dx} = \frac{d}{dx} \left(\Gamma \frac{d\phi}{dx} \right)$$

$$\oint_{A} \rho \phi \mathbf{u} \cdot \mathbf{n} \, dA = \oint_{A} \Gamma \, grad(\phi) \cdot \mathbf{n} \, dA$$

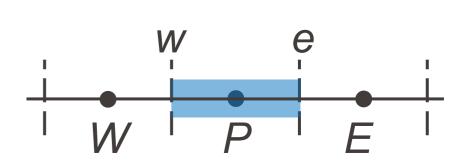
Assume the density and velocity are known, and satisfy continuity:

$$\frac{d(\rho u)}{dx} = 0 \quad \to \quad (\rho u)_e - (\rho u)_w = 0$$
$$F_e - F_w = 0$$

denoting $F = \rho u$ the convective mass flux

Integration over CV:

$$F_e \phi_e - F_w \phi_w = \Gamma_e \left. \frac{d\phi}{dx} \right|_e - \Gamma_w \left. \frac{d\phi}{dx} \right|_w$$



Use CD to discretize the diffusion term, as usual:

$$F_e \phi_e - F_w \phi_w = \Gamma_e \frac{\phi_E - \phi_P}{\delta x_{PE}} - \Gamma_w \frac{\phi_P - \phi_W}{\delta x_{WP}}$$

$$F_e\phi_e - F_w\phi_w = D_e(\phi_E - \phi_P) - D_w(\phi_P - \phi_W)$$

$$F_e\phi_e - F_w\phi_w = D_e(\phi_E - \phi_P) - D_w(\phi_P - \phi_W)$$
 denoting $D_e = \frac{\Gamma_e}{\delta x_{PE}}, D_w = \frac{\Gamma_w}{\delta x_{WP}}$

What about the convection term? How to discretize the face values?

1D steady convection-diffusion: central differencing

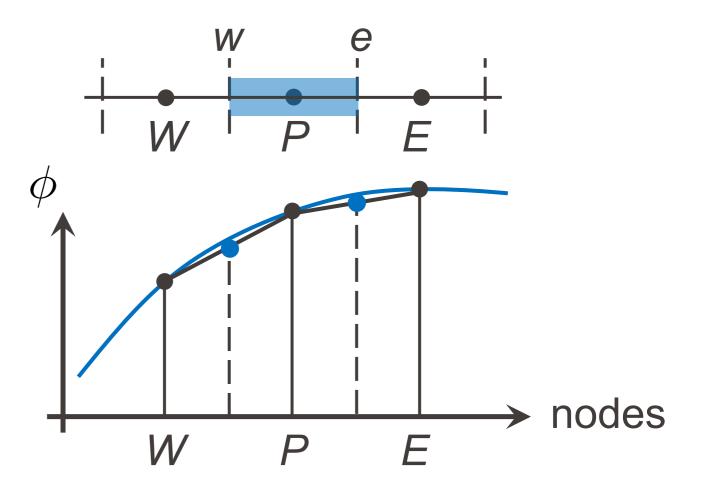
$$F_e\phi_e - F_w\phi_w = D_e(\phi_E - \phi_P) - D_w(\phi_P - \phi_W)$$

Linear interpolation

On a uniform grid:
$$\phi_w pprox \frac{\phi_W + \phi_P}{2}$$
 $\phi_e pprox \frac{\phi_P + \phi_E}{2}$

Governing equation becomes:

$$\frac{F_e}{2}(\phi_P + \phi_E) - \frac{F_w}{2}(\phi_W + \phi_P) = D_e(\phi_E - \phi_P) - D_w(\phi_P - \phi_W)$$



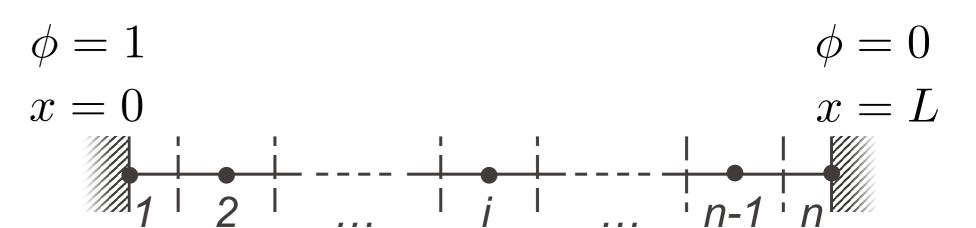
• Algebraic equation: $a_P \phi_P = a_W \phi_W + a_E \phi_E$

$$a_W = D_w + \frac{F_w}{2}, \quad a_E = D_e - \frac{F_e}{2}, \quad a_P = \left(D_w + D_e - \frac{F_w}{2} + \frac{F_e}{2}\right) = a_W + a_E + (F_e - F_w)$$

 Same form as steady diffusion eq. (but additional terms for convection). Note: by continuity, $F_e = F_w$

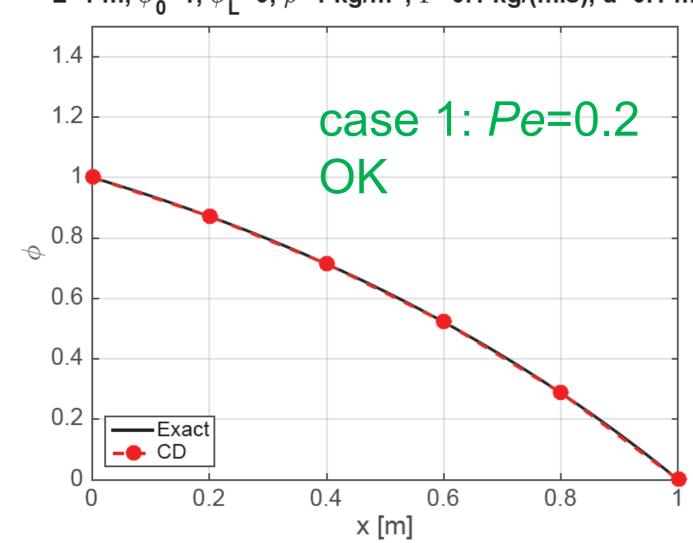
1D steady convection-diffusion: central differencing

Example: domain [0,1] m $\rho = 1 \text{ kg/m}^3, \Gamma = 0.1 \text{ kg/(m.s)}$



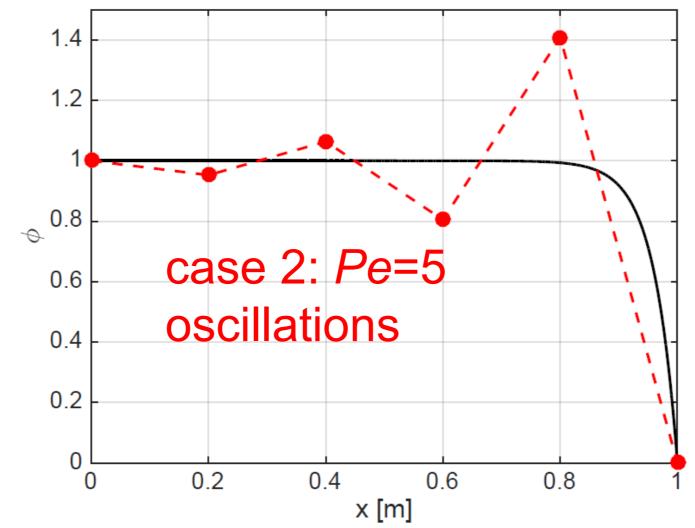
$$u = 0.1 \text{ m/s}, n = 6$$

L=1 m,
$$\phi_0$$
=1, ϕ_L =0, ρ =1 kg/m³, Γ =0.1 kg/(m.s), u=0.1 m/s



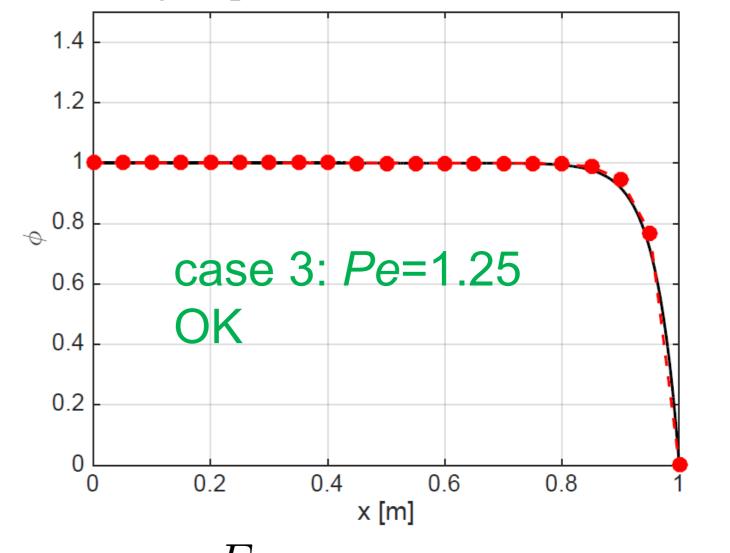
$$u = 2.5 \text{ m/s}, n = 6$$

L=1 m,
$$\phi_0$$
=1, ϕ_L =0, ho =1 kg/m³, Γ =0.1 kg/(m.s), u=2.5 m/s



$$u = 2.5 \text{ m/s}, n = 21$$

L=1 m,
$$\phi_0$$
=1, ϕ_L =0, ρ =1 kg/m³, Γ =0.1 kg/(m.s), u=2.5 m/s



Influence of the (numerical) Péclet number:
$$Pe = \frac{\rho u}{\Gamma/\delta x} = \frac{F}{D}$$

$$e = \frac{\rho u}{\Gamma/\delta x} = \frac{F}{D}$$

Properties of discretization schemes

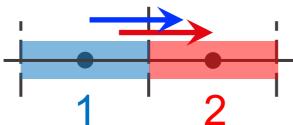
- Why do we need to discuss that?
 - In theory, better accuracy when refining the mesh, for all discretization schemes.
 - In practice, can only use a finite number of CVs.
 - On a finite-size mesh, numerical results are physically realistic only when the scheme has some fundamental properties.
- In particular, a discretization scheme must be:
 - 1. Conservative
 - 2. Bounded
 - 3. Transportive

Numerical Flow Simulation

Properties of discretization schemes

1. Conservativeness

 Local CV conservation ensures global conservation only if the flux leaving a CV across a face is equal to the flux entering the neighboring CV across the same face. (Relevant to both convective and diffusive terms.)

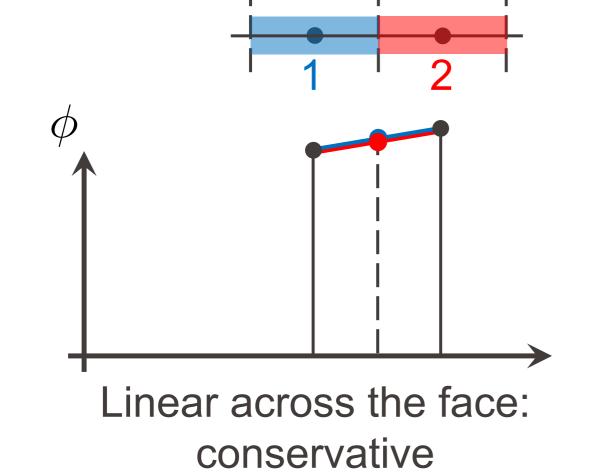


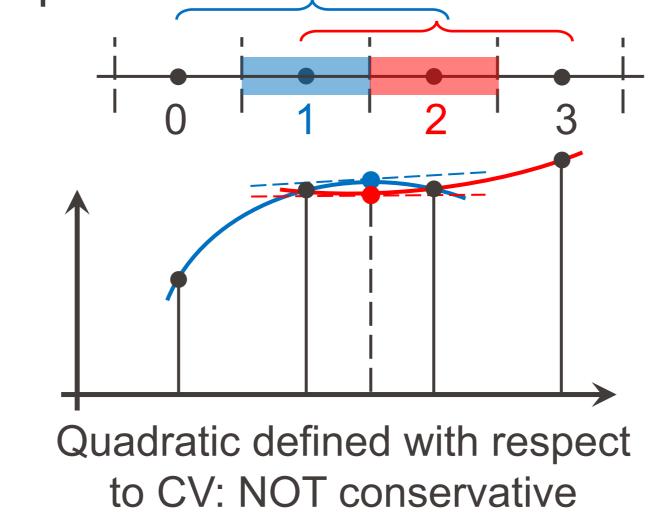
$$(\rho u\phi)_{e1} = (\rho u\phi)_{w2}$$

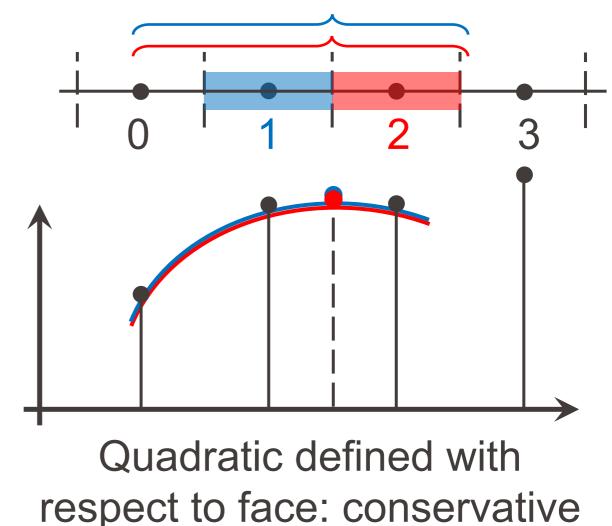
$$(\rho u\phi)_{e1} = (\rho u\phi)_{w2}$$

$$\left(\Gamma \frac{\partial \phi}{\partial x}\right)_{e1} = \left(\Gamma \frac{\partial \phi}{\partial x}\right)_{w2}$$

 To achieve this, the flux must be represented in a consistent way in both CVs, i.e. with the same expression.

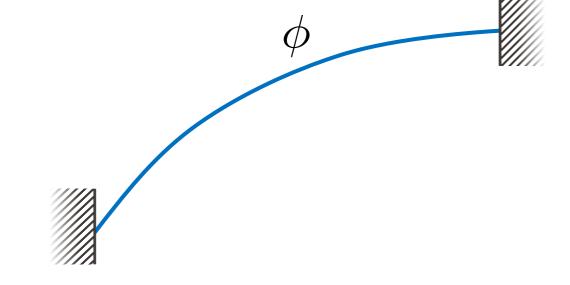






Properties of discretization schemes

2. Boundedness



- In the absence of sources, internal values of ϕ must be **bounded** by the boundary values (no local min. or max.).
- One way of achieving boundedness: if all coefficients of the algebraic equation $a_P\phi_P=a_W\phi_W+a_E\phi_E+\dots$

have the **same sign**. Physical interpretation: all else being equal, an increase in ϕ at one node should yield an increase of ϕ at neighboring nodes. With different signs, the solution may not converge or may contain unphysical oscillations.

 One desirable feature for satisfying boundedness: if the matrix A of the linear system is strictly diagonal dominant:

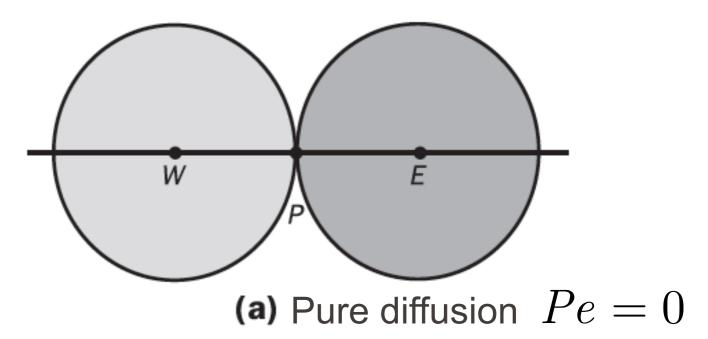
Strict diagonal dominance is a sufficient condition for the **convergence** of iterative methods (Scarborough criterion).

$$|a_{i,i}| \geq \sum_{i \neq j} |a_{i,j}|$$
 for all rows i , $|a_{i,i}| > \sum_{i \neq j} |a_{i,j}|$ for at least one row i .

Properties of discretization schemes

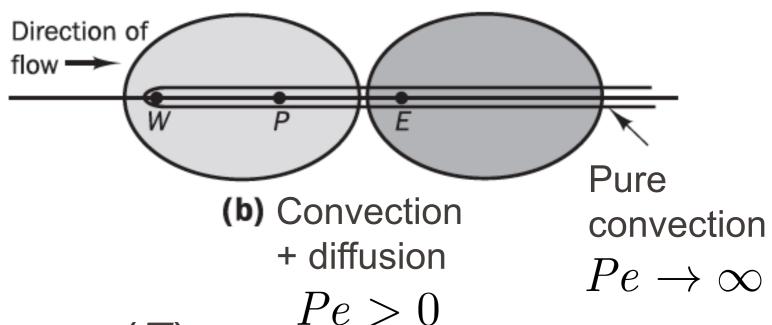
3. Transportiveness

 With convection, the influence of neighboring nodes is not symmetric.



Characterized by the Péclet number:

$$Pe = \frac{\text{convective flux}}{\text{diffusive flux}} = \frac{\rho u \phi}{\Gamma \operatorname{grad}(\phi)} = \frac{\rho u}{\Gamma/L}$$



- In the limit of pure convection: $\phi_P = \phi_W$. Upstream influence (*W*) only, no downstream influence (*E*).
- Numerical schemes should account for the asymmetry, the flow direction, and the relative strengths of convection/diffusion (*Pe*).

Steady convection-diffusion: central differencing CD

- Bounded?
 - Satisfies the Scarborough criterion...
 - ... but coefficients can become negative: $a_E = D_e \frac{F_e}{2} < 0$ if Pe > 2
- Transportive?
 - Not transportive: symmetric, too much weight on *E*.
- Conservative?
 - Yes
- Accuracy: 2nd-order

Numerical Flow Simulation

Steady convection-diffusion: upwind differencing UD

$$F_e \phi_e - F_w \phi_w = D_e (\phi_E - \phi_P) - D_w (\phi_P - \phi_W)$$

 Constant interpolation, taking into account the flow direction (use upstream node):

if
$$F_w$$
, $F_e > 0$: $\phi_w \approx \phi_W$, $\phi_e \approx \phi_P$

if
$$F_w$$
, $F_e < 0$: $\phi_w \approx \phi_P$, $\phi_e \approx \phi_E$

Governing equation becomes:

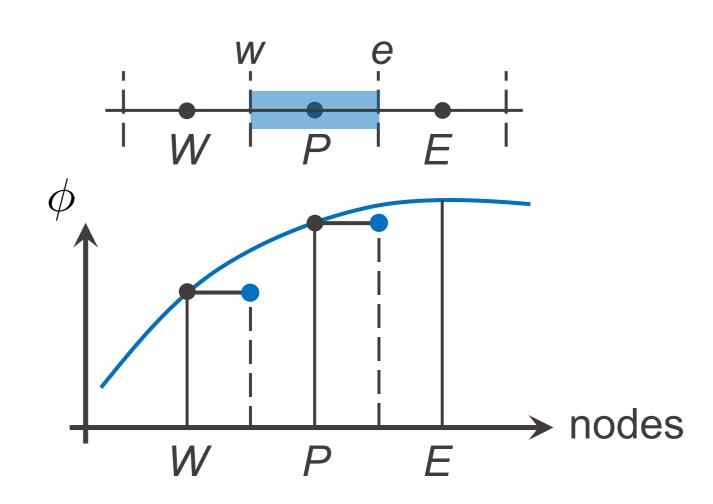
if
$$F_w$$
, $F_e > 0$: $(D_w + D_e + F_e)\phi_P = (D_w + F_w)\phi_W + D_e\phi_E$

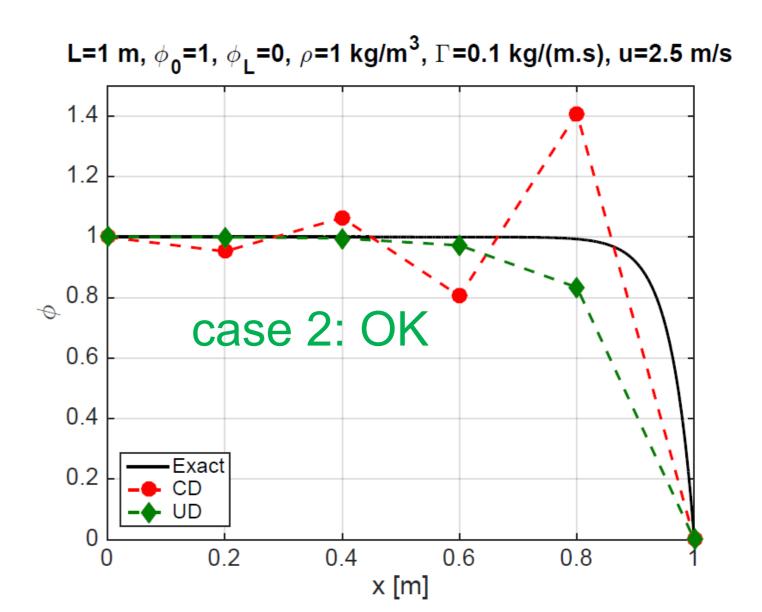
if
$$F_w$$
, $F_e < 0$: $(D_w + D_e - F_w)\phi_P = D_w\phi_W + (D_e - F_e)\phi_E$

• General expression: $a_P\phi_P=a_W\phi_W+a_E\phi_E$

$$a_W = D_w + \max(0, F_w)$$
 $a_E = D_e + \max(0, -F_e)$
 $a_P = a_W + a_E + (F_e - F_w)$

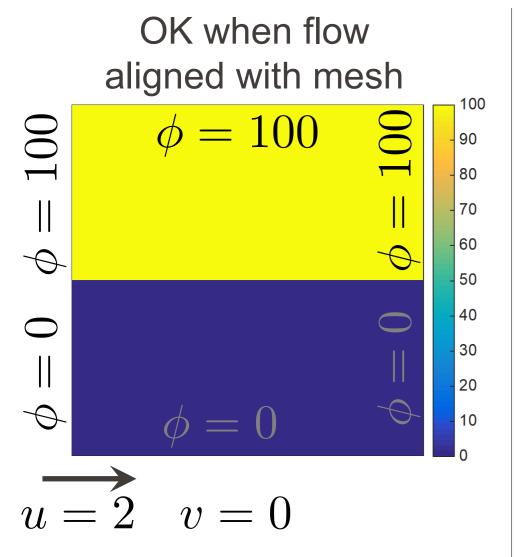
Coefficients always positive.

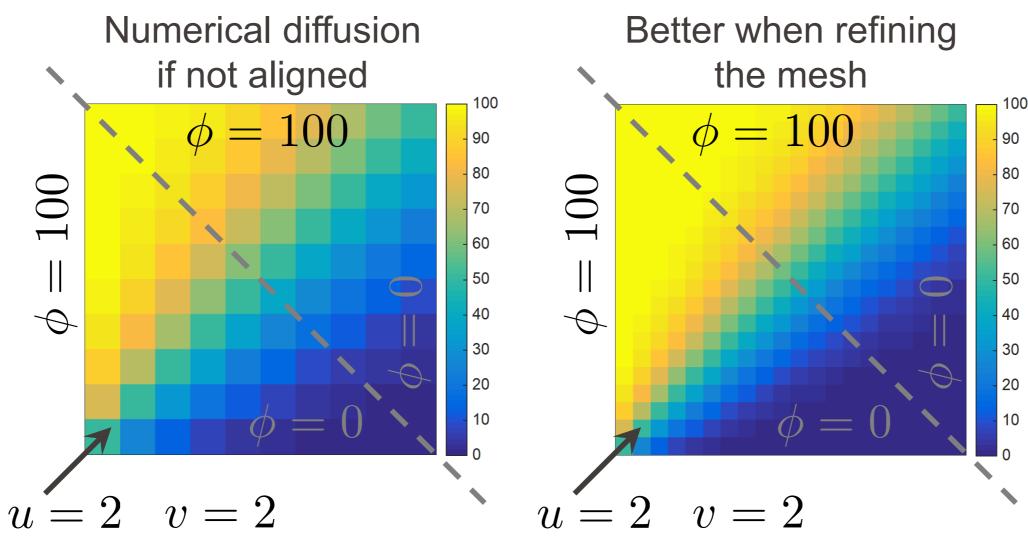


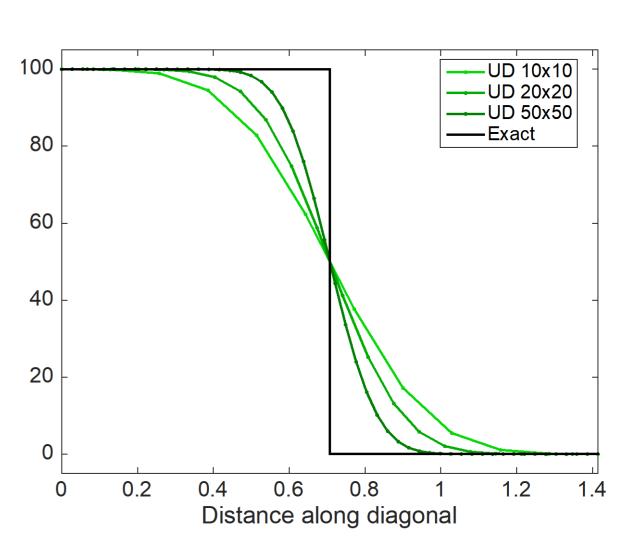


Steady convection-diffusion: upwind differencing UD

- Drawback: numerical diffusion ("false diffusion") when flow not aligned
- Example: 2D pure convection ($\Gamma = 0$), prescribed velocity field







Can be understood: $0 = F_e \phi_e - F_w \phi_w + F_n \phi_n - F_s \phi_s \approx F_e \phi_P - F_w \phi_W + F_n \phi_P - F_s \phi_S$

$$F_e = F_w > 0, F_n = F_s = 0$$

$$\to \phi_P = \phi_W$$

$$F_e = F_w = F_n = F_s$$

$$\to \phi_P = (\phi_W + \phi_S)/2$$

 Need higher-order scheme and/or finer mesh.

Steady convection-diffusion: upwind differencing UD

- Bounded?
 - Satisfies the Scarborough criterion
 - Coefficients always positive
- Transportive?
 - Yes by construction
- Conservative?
 - Yes
- Accuracy: 1st-order, numerical diffusion

Numerical Flow Simulation

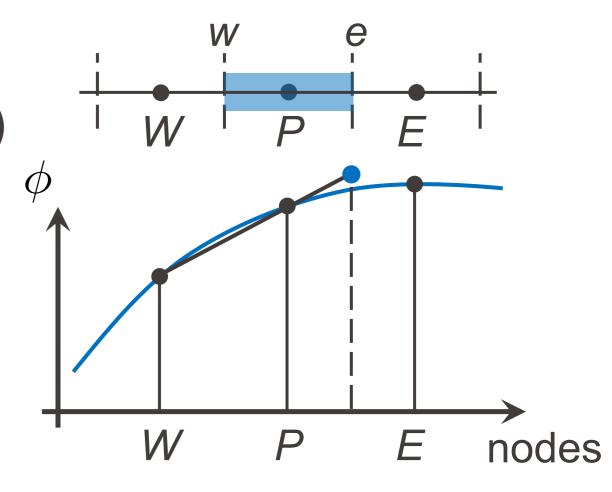
Steady convection-diffusion: LUD (SOU)

- "Linear upwind differencing" (or "second-order upwind")
- 2nd-order extension of UD: linear interpolation, taking into account the flow direction (use 2 upstream nodes)

if
$$F_w$$
, $F_e > 0$: $\phi_e \approx \phi_P + \left. \frac{\partial \phi}{\partial x} \right|_P \delta x_{Pe} \approx \phi_P + \frac{\phi_P - \phi_W}{\delta x_{WP}} \delta x_{Pe}$

On a uniform grid: $\phi_w pprox \frac{3\phi_W - \phi_{WW}}{2}$ $\phi_e pprox \frac{3\phi_P - \phi_W}{2}$

$$\phi_e \approx \frac{3\phi_P - \phi_W}{2}$$



• Governing equation becomes:
$$a_P\phi_P=a_{WW}\phi_{WW}+a_W\phi_W+a_E\phi_E$$

$$a_{WW} = -\frac{F_w}{2}$$

$$a_W = D_w + \frac{F_e}{2} + \frac{3F_w}{2}$$

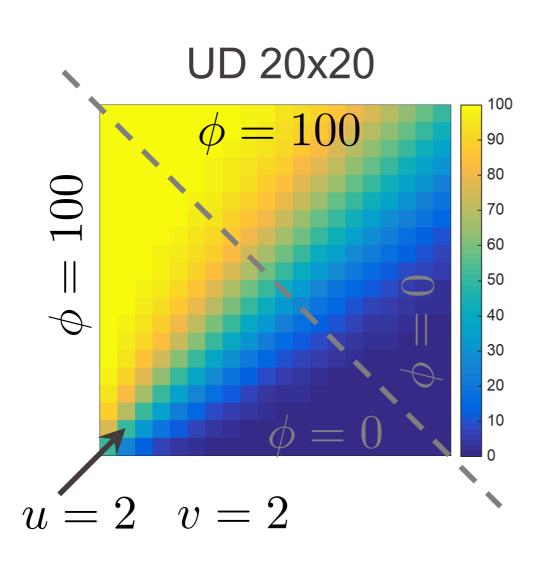
$$a_E = D_e$$

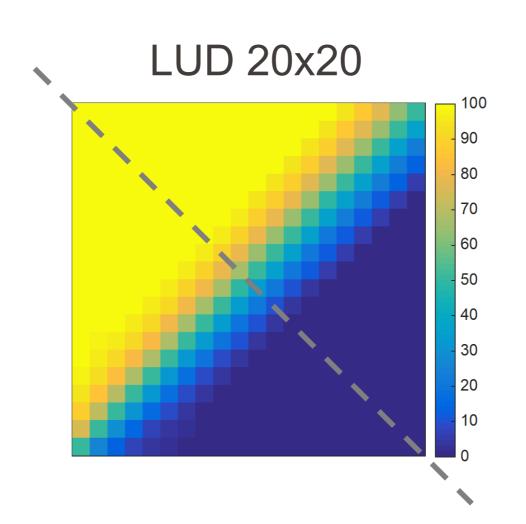
$$a_P = a_{WW} + a_W + a_E + (F_e - F_w)$$

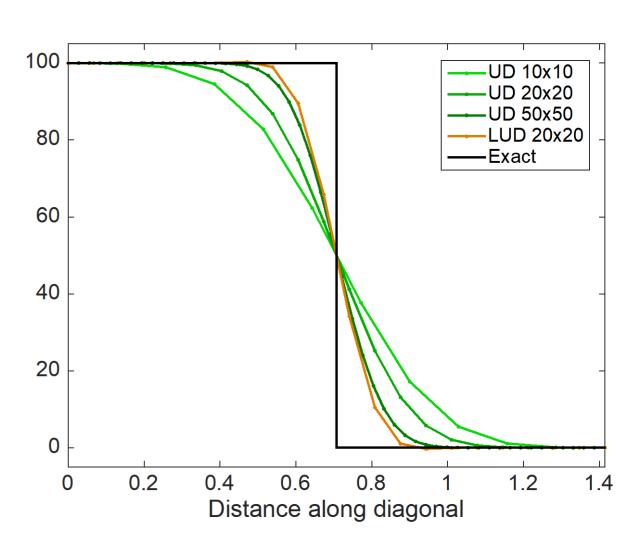
One negative coefficient.

Steady convection-diffusion: LUD (SOU)

■ LUD (2nd-order) more accurate but less stable.







Note: for nonlinear problems, 1st-order schemes (like UD) are useful to get a first solution, that can then be used as initial guess for a second calculation with a higher-order scheme (like LUD). This two-step procedure is generally faster than starting directly with a higher-order calculation from a poor initial guess.

In this example, LUD 20x20 better than UD 50x50

Steady convection-diffusion: LUD (SOU)

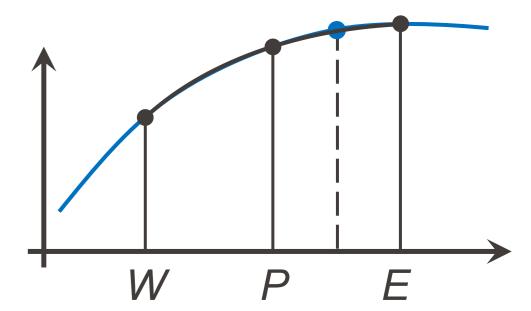
- Bounded?
 - Satisfies the Scarborough criterion
 - One negative coefficient
- Transportive?
 - Yes by construction
- Conservative?
 - Yes
- Accuracy: 2nd-order

Numerical Flow Simulation

Steady convection-diffusion: QUICK

- "Quadratic upstream interpolation for convective kinetics"
- W e H

 Quadratic interpolation, taking into account the flow direction (use 2 upstream / 1 downstream nodes):



On a uniform grid:

if
$$F_w$$
, $F_e > 0$: $\phi_w = \frac{-\phi_{WW} + 6\phi_W + 3\phi_P}{8}$ $\phi_e = \frac{-\phi_W + 6\phi_P + 3\phi_E}{8}$ if F_w , $F_e < 0$: $\phi_w = \frac{3\phi_W + 6\phi_P - \phi_E}{8}$ $\phi_e = \frac{3\phi_P + 6\phi_E - \phi_{EE}}{8}$

• Governing equation becomes for F_w , $F_e > 0$:

$$\frac{F_e}{8}(-\phi_W + 6\phi_P + 3\phi_E) - \frac{F_w}{8}(-\phi_{WW} + 6\phi_W + 3\phi_P) = D_e(\phi_E - \phi_P) - D_w(\phi_P - \phi_W)$$

Steady convection-diffusion: QUICK

• Governing equation becomes for F_w , $F_e > 0$:

$$\frac{F_e}{8}(-\phi_W + 6\phi_P + 3\phi_E) - \frac{F_w}{8}(-\phi_{WW} + 6\phi_W + 3\phi_P) = D_e(\phi_E - \phi_P) - D_w(\phi_P - \phi_W)$$

■ General expression: $a_P\phi_P = a_{WW}\phi_{WW} + a_W\phi_W + a_E\phi_E + a_{EE}\phi_{EE}$

$$a_{WW} = -\max\left(0, \frac{F_w}{8}\right)$$

$$a_W = D_w + \max\left(0, \frac{6F_w}{8}\right) + \max\left(0, \frac{F_e}{8}\right) - \max\left(0, -\frac{3F_w}{8}\right)$$

$$a_E = D_e - \max\left(0, \frac{3F_e}{8}\right) + \max\left(0, -\frac{6F_e}{8}\right) + \max\left(0, -\frac{F_w}{8}\right)$$

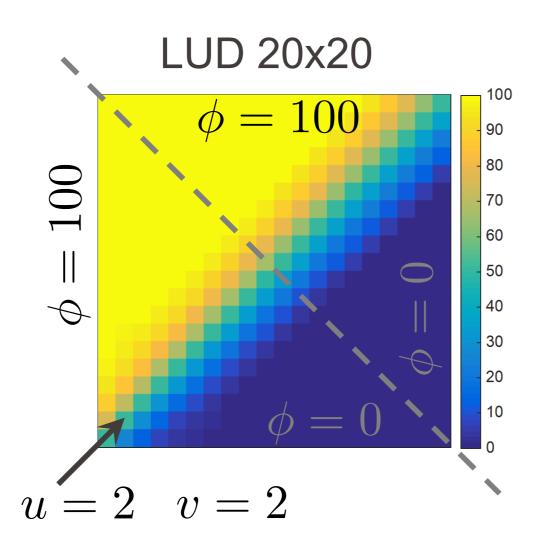
$$a_{EE} = -\max\left(0, -\frac{F_e}{8}\right)$$

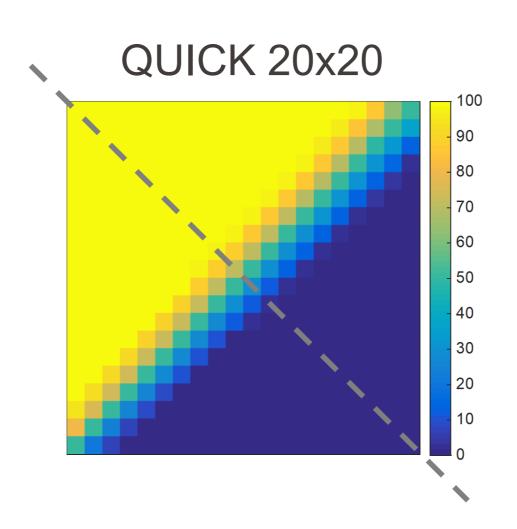
$$a_P = a_{WW} + a_W + a_E + a_{EE} + (F_e - F_w)$$
Coefficient

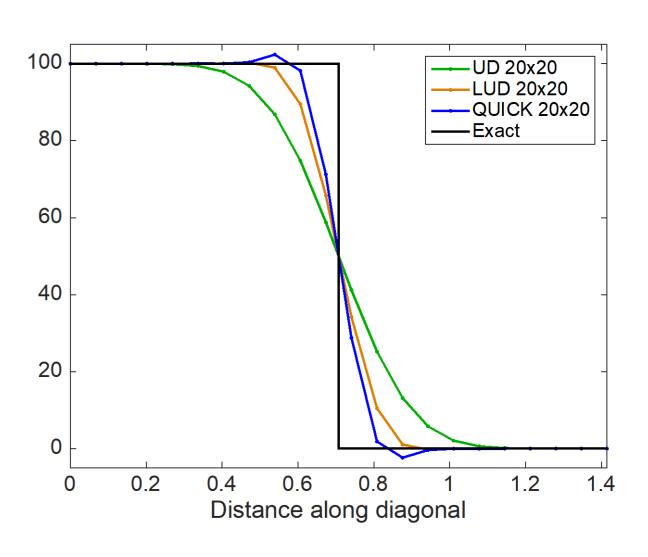
Coefficients can be negative.

Steady convection-diffusion: QUICK

 QUICK is more accurate and has less numerical diffusion, but may produce minor under/overshoots.







Steady convection-diffusion: QUICK

- Bounded?
 - Satisfies the Scarborough criterion
 - Coefficients can be negative
- Transportive?
 - Yes by construction
- Conservative?
 - Yes
- Accuracy: 3rd-order, but may give rise to slight under/overshoots

Numerical Flow Simulation

Deferred correction

- Procedure to facilitate convergence despite negative coefficients: "deferred correction".
- Place troublesome coefficients in the source term, to retain positivity:

Governing equation becomes:

$$F_e\left(\phi_P + \frac{-\phi_W^* - 2\phi_P^* + 3\phi_E^*}{8}\right) - F_w\left(\phi_W + \frac{-\phi_{WW}^* - 2\phi_W^* + 3\phi_P^*}{8}\right) = D_e(\phi_E - \phi_P) - D_w(\phi_P - \phi_W)$$

Only positive coefficients:

$$(F_e + D_e + D_w)\phi_P = D_e\phi_E + (D_w + F_w)\phi_W + S_{dc}$$

$$a_P \phi_P = a_E \phi_E + a_W \phi_W + S_{dc}$$

Deferred correction source term:

$$a_{P}\phi_{P} = a_{E}\phi_{E} + a_{W}\phi_{W} + S_{dc}$$

$$S_{dc} = -\frac{F_{e}}{8}(-\phi_{W}^{*} - 2\phi_{P}^{*} + 3\phi_{E}^{*}) + \frac{F_{w}}{8}(-\phi_{WW}^{*} - 2\phi_{W}^{*} + 3\phi_{P}^{*})$$

Use guess values for starred quantities, and iterate until convergence.

Summary of discretization schemes (convective term)

- UD: bounded, transportive, but 1st-order (numerical diffusion)
- CD: 2nd-order, but not transportive and can be unbounded (oscillations)
- LUD, QUICK: 2nd/3rd-order, transportive, but can be unbounded (oscillations)
- Would like higher order without oscillations.
- Observation: higher-order schemes can be written as an extension of UD:

• UD:
$$\phi_e = \phi_P$$

• CD:
$$\phi_e = \frac{\phi_P + \phi_E}{2} = \phi_P + \frac{1}{2}(\phi_E - \phi_P)$$

• LUD:
$$\phi_e = \phi_P + \frac{1}{2}(\phi_P - \phi_W) = \phi_P + \frac{1}{2}\left(\frac{\phi_P - \phi_W}{\phi_E - \phi_P}\right)(\phi_E - \phi_P)$$

• QUICK:
$$\phi_e = \phi_P + \frac{1}{8} \left(-\phi_W - 2\phi_P + 3\phi_E \right) = \phi_P + \frac{1}{2} \left[\frac{1}{4} \left(3 + \frac{\phi_P - \phi_W}{\phi_E - \phi_P} \right) \right] \left(\phi_E - \phi_P \right)$$

• General form:
$$\phi_e = \phi_P + \frac{\psi(r)}{2}(\phi_E - \phi_P)$$

where
$$r = \frac{\phi_P - \phi_W}{\phi_E - \phi_P}$$

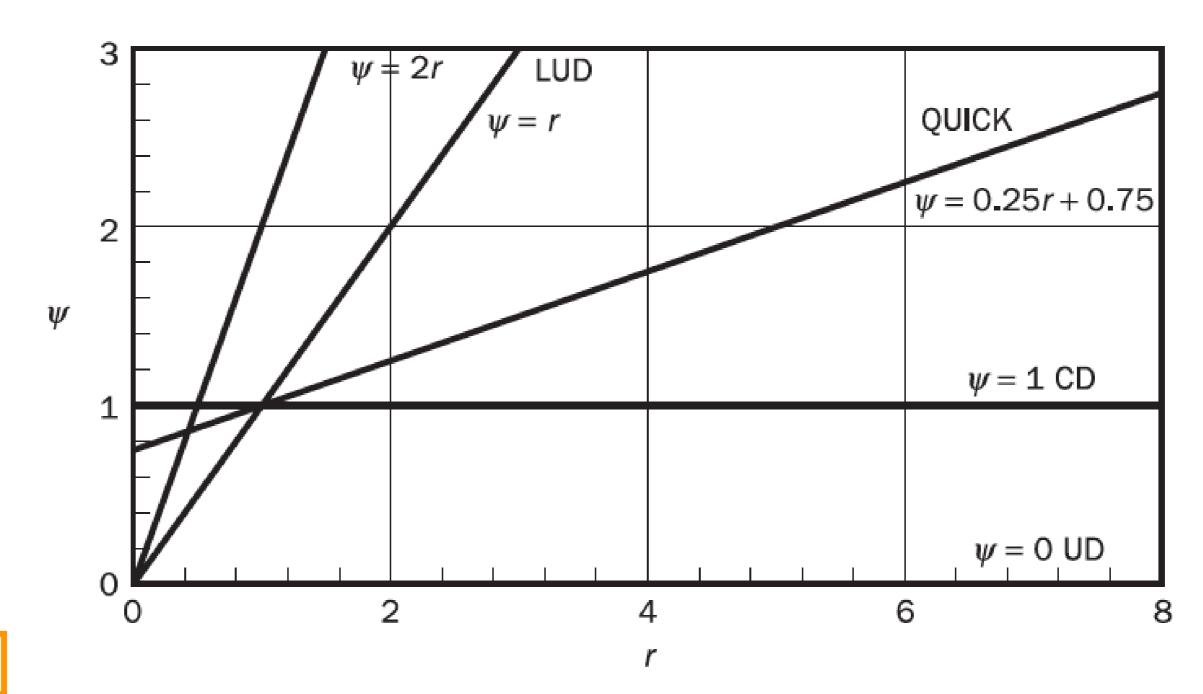
$$\psi(r) = 0$$

$$\psi(r) = 1$$

$$\psi(r) = r$$
3

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Summary of discretization schemes (convective term)



• UD:
$$\phi_e = \phi_P$$

• CD:
$$\phi_e = \frac{\phi_P + \phi_E}{2} = \phi_P + \frac{1}{2}(\phi_E - \phi_P)$$

• LUD:
$$\phi_e = \phi_P + \frac{1}{2}(\phi_P - \phi_W) = \phi_P + \frac{1}{2}\left(\frac{\phi_P - \phi_W}{\phi_E - \phi_P}\right)(\phi_E - \phi_P)$$

■ QUICK:
$$\phi_e = \phi_P + \frac{1}{8} \left(-\phi_W - 2\phi_P + 3\phi_E \right) = \phi_P + \frac{1}{2} \left[\frac{1}{4} \left(3 + \frac{\phi_P - \phi_W}{\phi_E - \phi_P} \right) \right] \left(\phi_E - \phi_P \right)$$

• General form:
$$\phi_e = \phi_P + \frac{\psi(r)}{2}(\phi_E - \phi_P)$$

$$\frac{1}{2}\left[\frac{1}{4}\left(3+\frac{\phi_P-\phi_W}{\phi_E-\phi_P}\right)\right](\phi_E-\phi_P)$$
 where $r=\frac{\phi_P-\phi_W}{\phi_E}$

$$\psi(r) = 1$$

$$\psi(r) = r$$

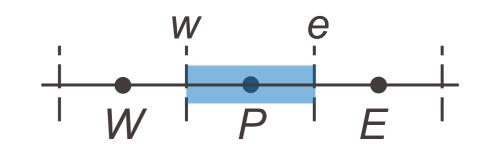
 $\psi(r) = 0$

$$\psi(r) = \frac{3+r}{4}$$

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Numerical Flow Simulation

TVD schemes



■ General form: upwind flux + correction flux (related to gradient $\frac{\partial \phi}{\partial x}\Big|_e \approx \frac{\phi_E - \phi_P}{\Delta x}$) $\phi_e = \boxed{\phi_P} + \boxed{\frac{\psi(r)}{2}(\phi_E - \phi_P)}$ $r = \frac{\phi_P - \phi_W}{\phi_E - \phi_P}$ ratio of upstream to downstream gradients

$$\phi_e = \phi_P + \frac{\psi(r)}{2}(\phi_E - \phi_P)$$

$$r = \frac{\phi_P - \phi_W}{\phi_E - \phi_P}$$

Can also be seen as a linear combination of UD and CD:

$$\phi_e = (1 - \psi(r)) \phi_e^{UD} + \psi(r) \phi_e^{CD} = (1 - \psi(r)) \phi_P + \psi(r) \left(\frac{\phi_P + \phi_E}{2}\right)$$

Idea of "total-variation diminishing" (TVD) schemes: evaluate the convective flux with the above form, choosing a suitable $\psi(r)$ to achieve higher-order accuracy without introducing new extrema.

TVD schemes

Criteria for boundedness:

$$\psi(r) \le 2r \text{ for } 0 < r < 1$$

 $\psi(r) \le 2 \text{ for } 1 \le r$

 $\psi(r)$ is called "flux limiter" since it limits the higher-order correction flux:

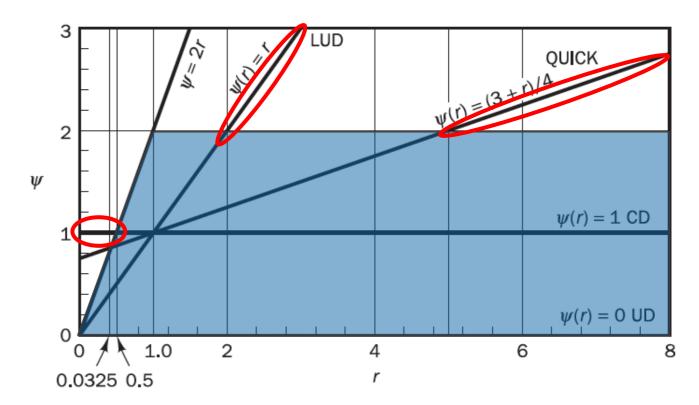
$$\phi_e = \phi_P + \frac{\psi(r)}{2} (\phi_E - \phi_P)$$

Criteria for 2nd-order accuracy:

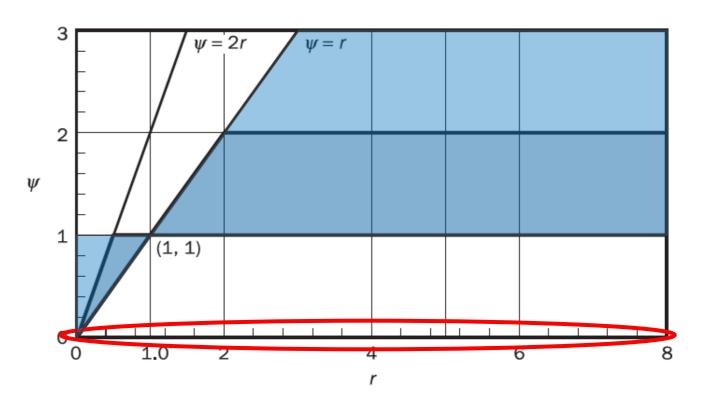
$$\psi(1) = 1$$

$$r \le \psi(r) \le 1 \text{ for } 0 < r < 1$$

$$1 \le \psi(r) \le r \text{ for } 1 \le r$$



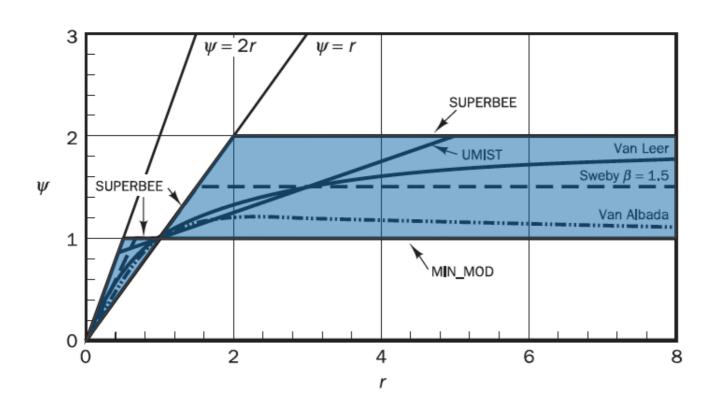
Check: CD, LUD and QUICK are not bounded for some values of *r*.



Check: UD is not 2nd-order accurate.

TVD schemes

Some examples:



| Name | Limiter function $\psi(r)$ | Source |
|------------|---|--------------------------|
| Van Leer | $\frac{r+ r }{1+r}$ | Van Leer (1974) |
| Van Albada | $\frac{r+r^2}{1+r^2}$ | Van Albada et al. (1982) |
| Min-Mod | $\psi(r) = \begin{cases} \min(r, 1) & \text{if } r > 0 \\ 0 & \text{if } r \le 0 \end{cases}$ | Roe (1985) |
| SUPERBEE | $\max[0, \min(2r, 1), \min(r, 2)]$ | Roe (1985) |
| Sweby | $\max[0, \min(\beta r, 1), \min(r, \beta)]$ | Sweby (1984) |
| QUICK | $\max[0, \min(2r, (3+r)/4, 2)]$ | Leonard (1988) |
| UMIST | $\max[0, \min(2r, (1+3r)/4,$ | Lien and Leschziner |
| | (3+r)/4, 2) | (1993) |

Governing equation becomes for
$$F_w$$
, $F_e > 0$:
$$r_e = \frac{\phi_P - \phi_W}{\phi_E - \phi_P} \quad r_w = \frac{\phi_W - \phi_{WW}}{\phi_P - \phi_W}$$
$$F_e \left(\phi_P + \frac{\psi(r_e)}{2}(\phi_E - \phi_P)\right) - F_w \left(\phi_W + \frac{\psi(r_w)}{2}(\phi_P - \phi_W)\right) = D_e(\phi_E - \phi_P) - D_w(\phi_P - \phi_W)$$

With deferred correction approach:

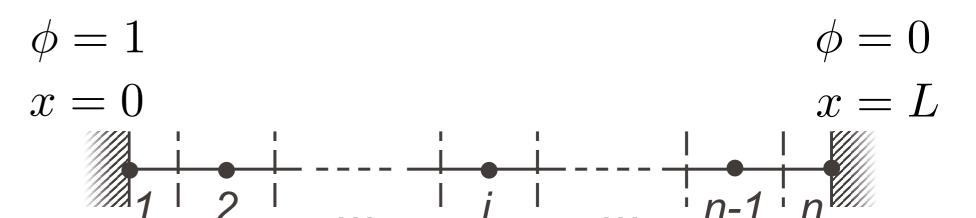
$$(D_e + D_w + F_e) \phi_P = D_e \phi_E + (D_w + F_w) \phi_W + \left[F_w \frac{\psi(r_w^*)}{2} (\phi_P^* - \phi_W^*) - F_e \frac{\psi(r_e^*)}{2} (\phi_E^* - \phi_P^*) \right]$$

$$a_P \phi_P = a_E \phi_E + a_W \phi_W + S_{dc}$$

TVD schemes

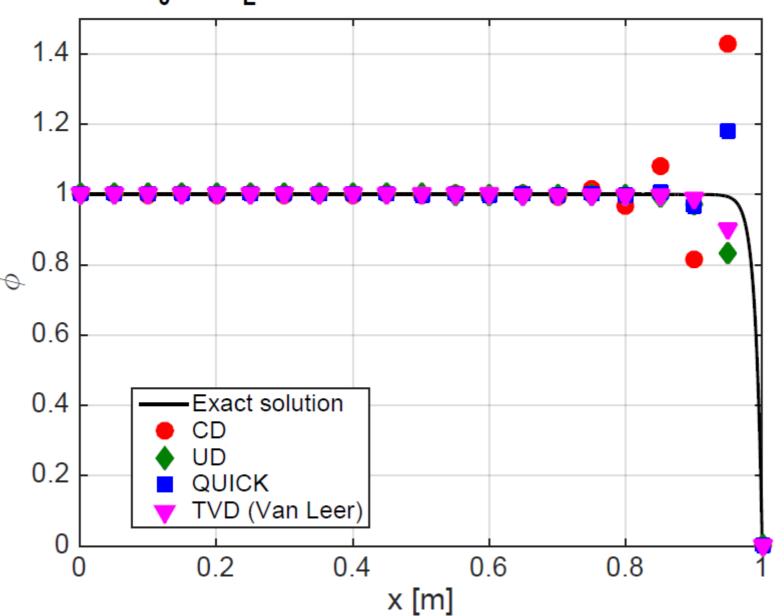
■ 1D example: domain [0, 1] m

$$\rho = 1 \text{ kg/m}^3, \, \Gamma = 0.1 \text{ kg/(m.s)}$$



$$u = 10 \text{ m/s}, n = 21$$

L=1 m, ϕ_0 =1, ϕ_L =0, ρ =1 kg/m³, Γ =0.1 kg/(m.s), u=10 m/s



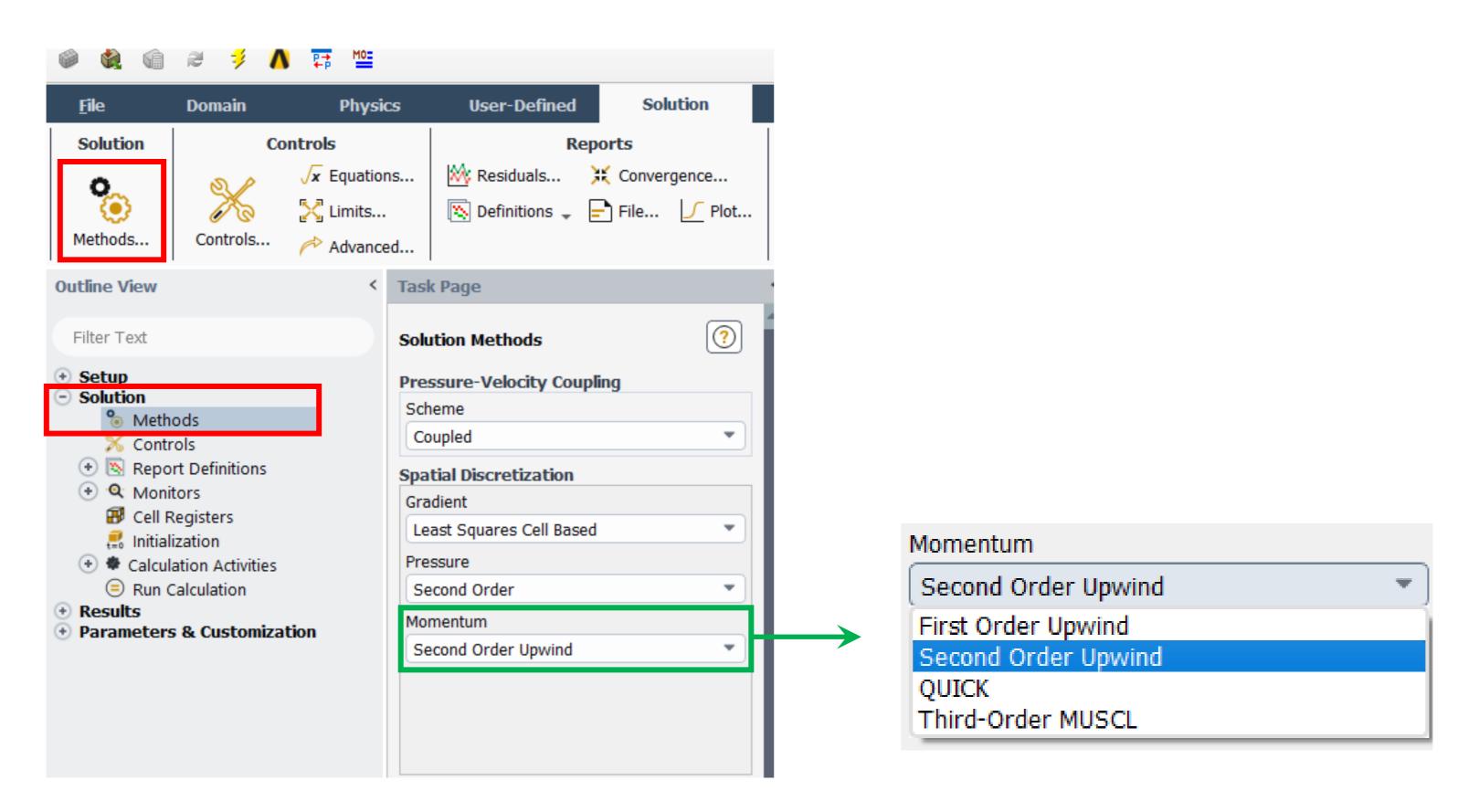
Summary and guidelines

- **CD** can be used for the **diffusion** term, but rarely for the convection term.
- For the **convection** term, **UD** most stable, but large numerical diffusion. Can be used to get an initial solution, before switching to a higher-order scheme.

- LUD (SOU) and QUICK more accurate.
- TVD schemes avoid oscillations.

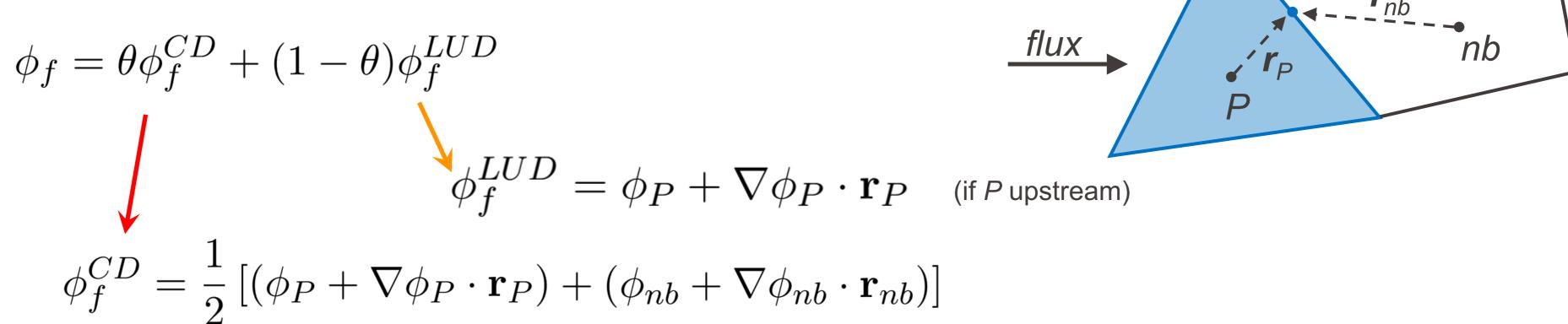
Appendix: Fluent specifics - Discretization schemes

Discretization schemes available: UD, LUD (SOU), QUICK and MUSCL.



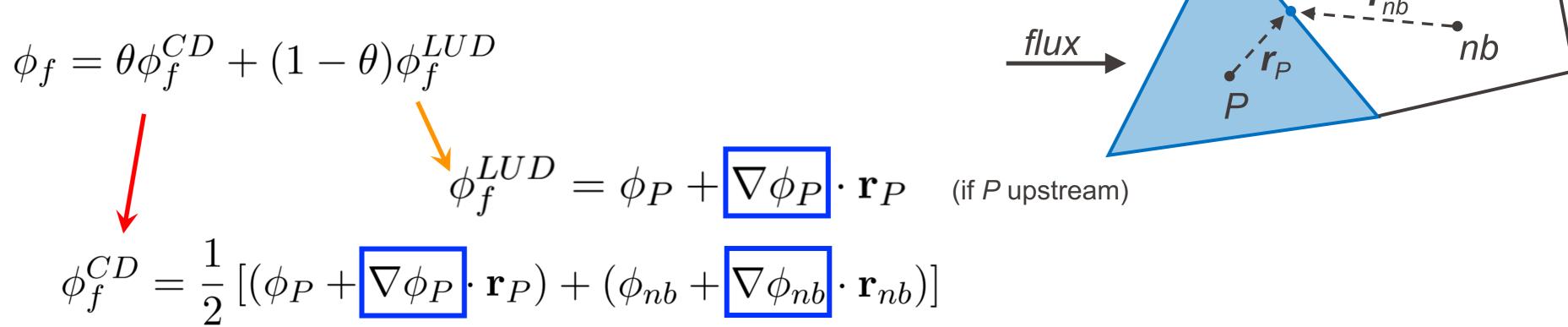
Appendix: Steady convection-diffusion: MUSCL

- Fluent has a 3rd-order, "QUICK-like" scheme for **unstructured** meshes (where it may not always be possible to uniquely identify "upstream" and "downstream" nodes): **MUSCL** ("monotone upstream-centered scheme for conservation laws").
- Blends the two 2nd-order schemes CD and LUD:



Appendix: Steady convection-diffusion: MUSCL

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- Blends the two 2nd-order schemes CD and LUD:



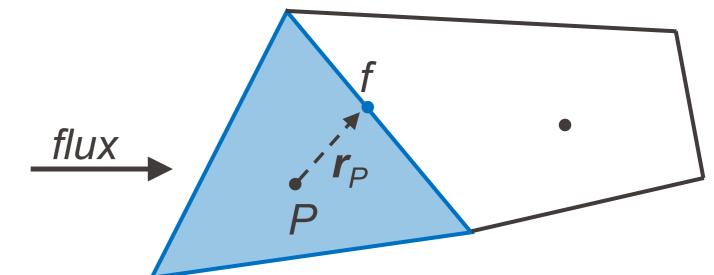
 Note: on unstructured meshes, all schemes except UD require evaluating the gradient in the CV from neighboring nodal values (→ additional cost).

- Nodal gradient reconstruction:
 - We saw (week 2) that for the diffusive term we need to evaluate the gradient on faces:

 $\int_{V} div(\Gamma \operatorname{grad}(\phi)) \, dV = \oint_{A_{i}} \Gamma \operatorname{grad}(\phi) \cdot \mathbf{n} \, dA$

• For the **convective term**, it seems we just need the solution on faces, but if we want better accuracy than 1st-order UD, we actually need to evaluate the **gradient at nodes** (slide 24):

$$\int_{V} div(\rho\phi\mathbf{u})\,dV = \oint_{A_{i}} \rho\underline{\phi}\mathbf{u}\cdot\mathbf{n}\,dA$$
 For ex. (LUD):
$$\phi_{f}^{LUD} = \phi_{P} + \nabla\phi_{P}\cdot\mathbf{r}_{P}$$



- Two methods to compute the nodal gradient:
 - 1. "Green-Gauss"
 - 2. Least squares

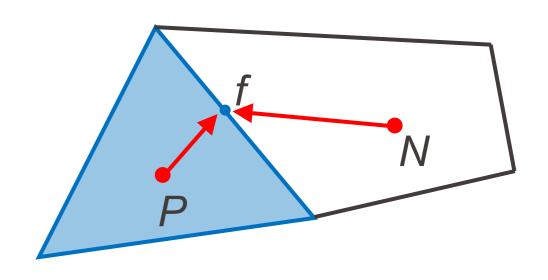
1. From the divergence theorem: So, since $\int_V \nabla \phi \, dV \approx \nabla \phi_P \, V$, the **nodal** gradient can be approximated as:

$$\int_{V} \nabla \phi \, dV = \int_{V} \operatorname{div}(\phi \mathbf{I}) \, dV = \oint_{A} \phi \mathbf{n} \, dA$$

$$\nabla \phi_P \approx \frac{1}{V} \sum_f \phi_f \mathbf{n}_f A_f$$

Here, each **face value** ϕ_f can be evaluated as:

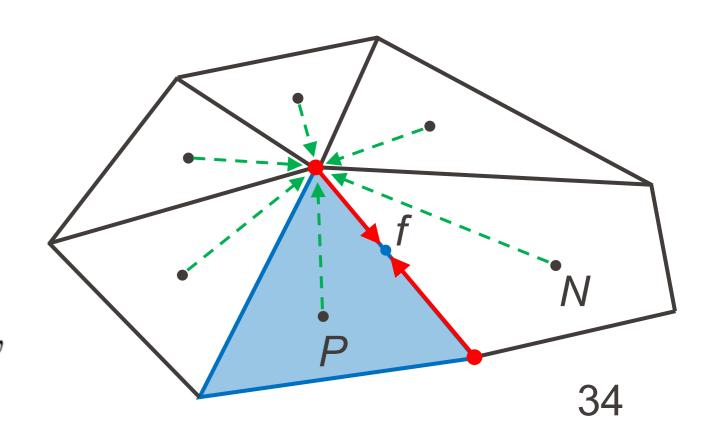
• the mean of the 2 neighboring cell values ("Green-Gauss, cell based"), $\phi_f \approx \frac{1}{2} (\phi_P + \phi_N)$



 or the mean of the N_v face vertex values ("Green-Gauss, node based"), each of them evaluated as a weighted average of all surrounding cell values.

More accurate, but more expensive.

$$\phi_f \approx \frac{1}{N_v} \sum_{v=1}^{N_v} \phi_v$$



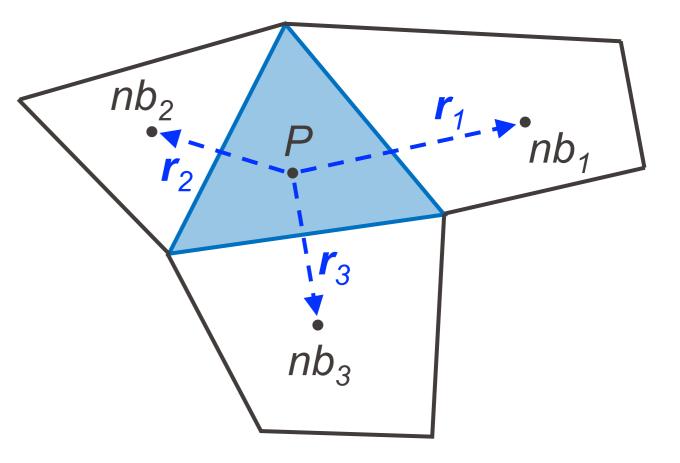
2. Least squares: in each neighboring node nb_i , write the solution as a Taylor expansion about P:

$$\begin{cases}
\phi_{nb_1} = \phi_P + \nabla \phi_P \cdot \mathbf{r}_1 \\
\phi_{nb_2} = \phi_P + \nabla \phi_P \cdot \mathbf{r}_2
\end{cases}$$
....

This is a small (N_{nb} x 3) overdetermined linear system to be solved for the gradient:

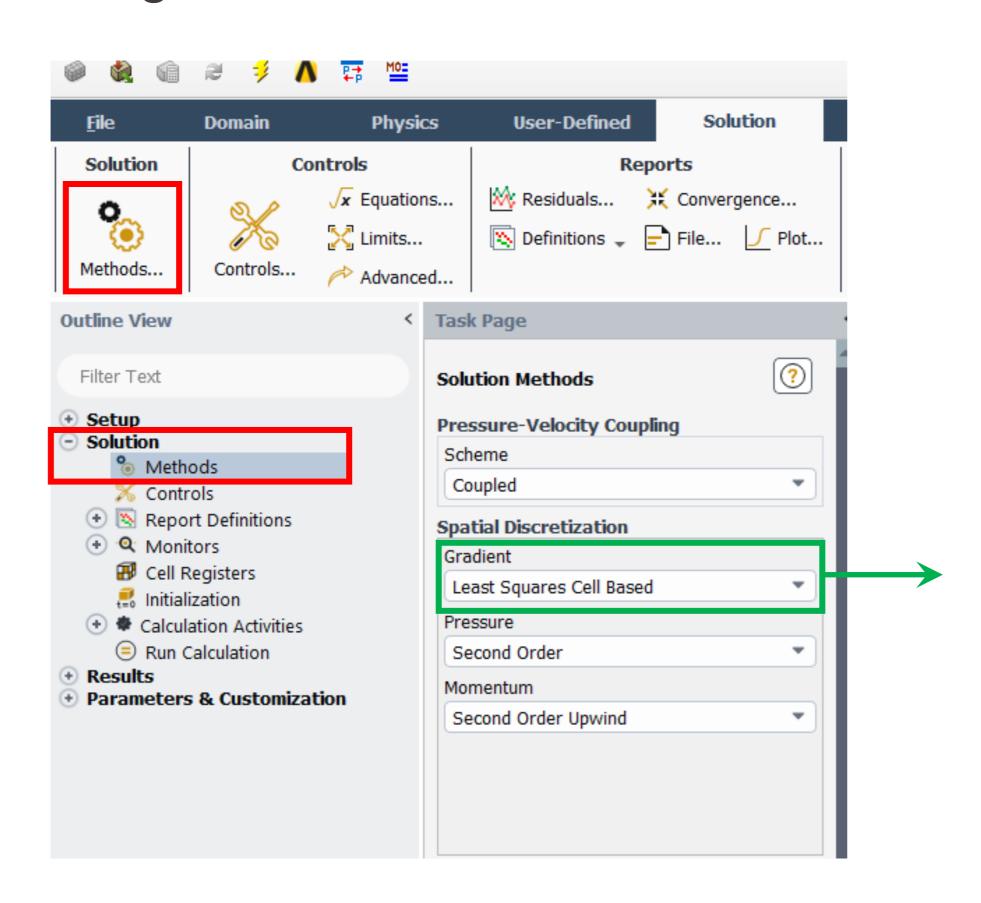
$$\mathbf{J}\,\nabla\phi_P = \boldsymbol{\phi_{nb}} - \boldsymbol{\phi_P}$$

$$\begin{bmatrix} r_{1,x} & r_{1,y} & r_{1,z} \\ r_{2,x} & r_{2,y} & r_{2,z} \\ \vdots & \vdots & \vdots \end{bmatrix} \begin{pmatrix} \nabla \phi_{P,x} \\ \nabla \phi_{P,y} \\ \nabla \phi_{P,z} \end{pmatrix} = \begin{pmatrix} \phi_{nb_1} - \phi_P \\ \phi_{nb_2} - \phi_P \\ \vdots & \vdots & \end{pmatrix}$$



As accurate as the "Green-Gauss node based" reconstruction, but faster. Default setting in Fluent.

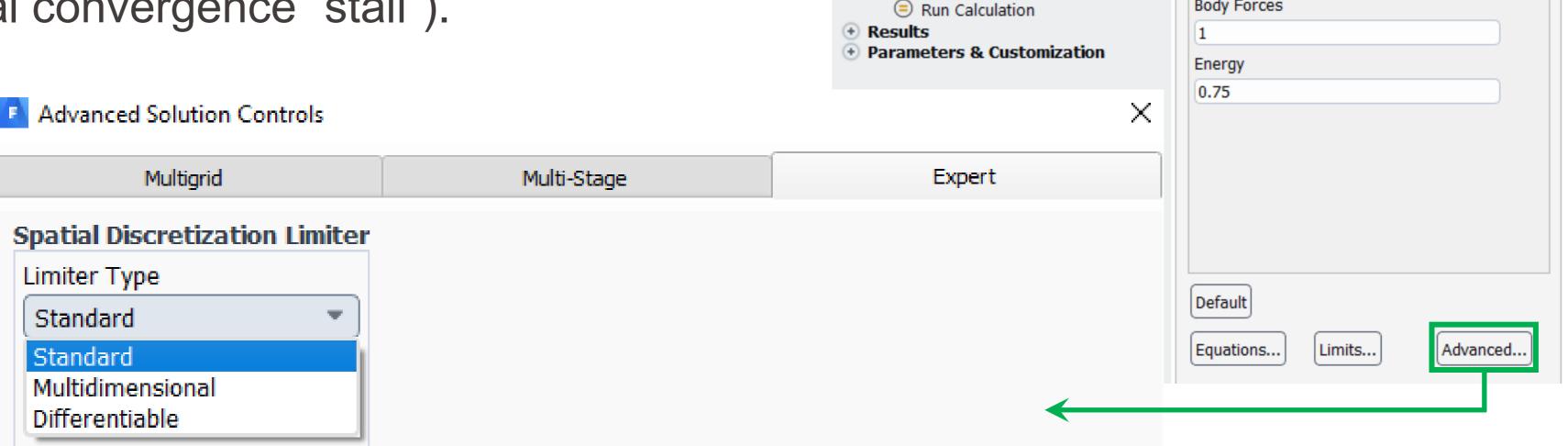
Nodal gradient reconstruction:



- Green-Gauss, cell based,
- Green-Gauss, node based,
- Least squares (default)

Appendix: Fluent specifics – TVD

- TVD: can choose among
 - standard Min-Mod (default; limits gradient) in all directions),
 - multi-dimensional Min-Mod (limits normal gradient only \rightarrow less dissipative),
 - differentiable limiter (helps to avoid residual convergence "stall").



Domain

Controls

/x Equations...

Advanced...

< Task Page

Pressure

Momentum

Body Forces

0.5

0.5

Density

Solution Controls

X Limits...

Solution

Q,

Methods...

Outline View

Filter Text

Solution

Methods

Controls

Monitors

Report Definitions

Cell Registers

Calculation Activities

Setup

but you don't really need to modify that.

Solution

?

★ Convergence...

User-Defined

Residuals...

Reports

Definitions - File... | Plot...

Pseudo Transient Explicit Relaxation Factors