

# ME-474 Numerical Flow Simulation

## Exercise: 1D steady diffusion

Fall 2021

Implement a FVM code in Matlab to solve a 1D steady-state heat conduction problem.

Equation:

$$\frac{\partial}{\partial x} \left( k(x) \frac{\partial T}{\partial x} \right) + S(x) = 0$$

Domain:  $x \in [0, L]$ ,  $L = 1$  m.

Assume the thermal conductivity is constant:  $k = 400$  W/(K.m).

1. Consider Dirichlet boundary conditions:  $T(0) = T_a = 300$  K,  $T(L) = T_b = 320$  K. Assume the source term is constant:  $S = S_c = 5000$  W/m<sup>3</sup>.

- Define a uniform grid of  $n$  nodes:  $x_1 = 0$ ,  $x_2 = \Delta x = L/(n-1) \dots$ ,  $x_n = L$ . Start with  $n = 21$ .
- Recall the discretized equation

$$a_P T_P = a_W T_W + a_E T_E + b,$$

or in vectorial form  $\mathbf{AT} = \mathbf{b}$ . Define the  $n \times n$  matrix  $\mathbf{A}$ , and the  $n \times 1$  right-hand side vector  $\mathbf{b}$ . Implement boundary conditions in equations 1 and  $n$ .

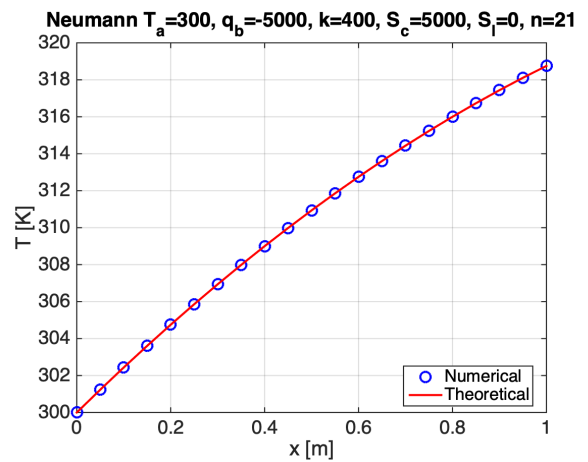
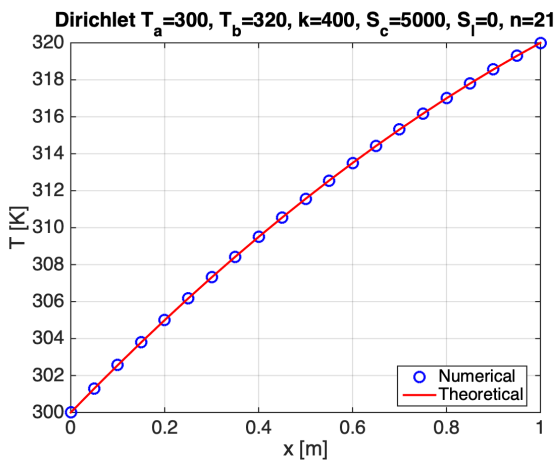
- Solve for  $\mathbf{T}$  and plot  $T(x)$ .
- Compare with the theoretical solution ( $T'' = -S/k = cst \rightarrow$  quadratic  $T(x)$ ):

$$T_{theo}(x) = \left( -\frac{S_c}{2k} \right) x^2 + \left( \frac{T_b - T_a}{L} + \frac{S_c L}{2k} \right) x + T_a.$$

- Check that the mean error

$$\frac{1}{n} \sum_i |T_i - T_{theo,i}|$$

is exactly zero whatever the value of  $n$ . Why?



2. Consider now the same Dirichlet boundary condition on the left,  $T(0) = T_a = 300$  K, but a Neumann boundary condition on the right,  $q_b = -k(\partial T/\partial x)_{x=L} = -5000$  W/m<sup>2</sup>.
  - Modify the implementation of the boundary conditions. (It may be a good idea to save two different versions of your code.)
  - Solve for  $\mathbf{T}$  and plot  $T(x)$ .
  - Compare with the theoretical solution:

$$T_{theo}(x) = \left(-\frac{S_c}{2k}\right)x^2 + \left(\frac{S_c L - q_b}{k}\right)x + T_a.$$

- Check that the mean error per control volume is exactly zero whatever the value of  $n$ . Why?
3. Finally, come back to Dirichlet boundary conditions on both ends like in Q1, but assume now that the source term varies linearly with temperature:

$$S = S_c + S_l T.$$

Take for instance  $S_c = 5000$  for the constant component, and  $S_l = -100$  for the linear coefficient. Note that the integration of this source term over a control volume yields

$$\int_{x_w}^{x_e} S dx \approx \bar{S} \Delta x = (S_c + S_l T_P) \Delta x,$$

so now the constant right-hand side is  $b = S_c \Delta x$ , while the solution-dependent term  $S_l T_P \Delta x$  goes into the diagonal coefficient  $a_P T_P$ .

- Modify the matrix  $\mathbf{A}$  accordingly.
- Solve for  $\mathbf{T}$  and plot  $T(x)$ .
- Compare with the theoretical solution, that can be obtained as the sum of (i) a particular solution of the full equation  $kT'' + S_l T = -S_c$ , i.e.  $T = -S_c/S_l$ , and (ii) the general solution of the homogeneous equation  $kT'' + S_l T = 0$ , which is  $T = c_1 e^{\mu x} + c_2 e^{-\mu x}$ , with  $\mu = \sqrt{-S_l/k}$ , and  $c_1$  and  $c_2$  such that boundary conditions are satisfied, which yields:

$$T_{theo}(x) = -\frac{S_c}{S_l} + c_1 e^{\mu x} + c_2 e^{-\mu x}, \quad c_1 = \frac{T_b - \left(\frac{S_c}{S_l} + T_a\right) e^{-\mu L} + \frac{S_c}{S_l}}{e^{\mu L} - e^{-\mu L}}, \quad c_2 = T_a + \frac{S_c}{S_l} - c_1.$$

- Observe that the mean error per control volume is not zero. Why? How does it decrease with  $n$ ? (Plot the mean error as a function of  $n$  in log-log scale.)

