Moose Project

Part 2

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March 2025

1 Introduction

In order to introduce well founded regulation for nuclear fuel it is important to have a robust computational modeling framework that accurately predicts the thermal and mechanical behavior of the fuel elements in question. In part one of this project we introduced a one dimensional heat transport model to examine the thermal properties of a UO_2 fuel pellet, with a Helium gap and Zr4 cladding. In this study we will extend the model to a 1[m] smeared pellet 2D model. While this project will not provide sufficiently comprehensive modeling inform actual regulation, it is important for developing our understanding of computational methods that reflect analytical and observed phenomena. Key to this process is the mesh refinement studies which provide confidence that the computational model is effectively capturing analytical and observed behaviors. Finding a well defined mesh, we utilize MOOSE to simulate the fuel element under a steady state as well as a transient. The axial temperature profiles are observed and reported under both circumstances.

2 Setup and Mesh Refinement

2.1 Material Properties and Model

To model our 1-D simulation we begin by finding material properties in the literature.[1-7] For our mesh convergence study in 1-D we start by finding material properties in literature. The relevant material properties are listed in Table 1. Table 2.

Material	Specific Heat (J/kg·K)	Density (kg/cm ³)
\mathbf{UO}_2 (Fuel)	296.7	0.01097
Helium (Gap)	5190	0.000000164
Zircaloy-4 (Cladding)	2850	0.00656

Table 1: Utilized specific heat and density values for UO₂, helium, and Zircaloy-4. Some values were lightly modified from sources in literature.

Material	Thermal Conductivity Model (W/cm·K)
\mathbf{UO}_2	$k = \frac{1}{2(1.48 + 0.04 \max(T, 300))}$
Helium	k = 0.0025 + 0.00002T
Zircaloy-4	k = 0.18 - 0.00002T

Table 2: Temperature-dependent thermal conductivity models for UO_2 , helium, and Zircaloy-4. Temperature (T) is in Kelvin. Again, some coefficients were lightly modified from values in literature.

These functions were defined in the functions block and referenced in each heat conduction material's thermal conductivity temperature function. Auxiliary variables and kernels were set up so that the thermal conductivity can be checked at different points in the material and at different times (in the transient simulation).

In the 1-D case a heat conduction kernel is implemented with a volumetric heating rate of $q=\frac{350}{0.25\pi}$, derived from the $LHR=350\frac{[\mathrm{W}]}{[\mathrm{cm}]}$ given in the problem statement. This volumetric heating rate will redefined to vary axially, and again temporally in the latter stages of implementation. In addition, two boundary conditions were implemented, a Dirichlet boundary condition for constant coolant temperature in the 1-D case - convective cooling BC in the 2-D case - and a Neumann boundary condition in all models, to prevent heat transfer across the centerline of the rod.

2.2 1-D Refinement

To start building our mesh we consider the basics of the problem, building out from a 1-D mesh. We recognize that it is important to have nodes located at the interface of each material and on the corners of our model. To achieve this we define 3 generated meshes, one on the domain $x \in [0,0.5], y \in 0,0.1$ for the fuel, one on $x \in [0.5,0.505], y \in [0,0.1]$ for the gap, and one on $x \in [0.505,0.605], y \in [0,0.1]$. We start by meeting the minimum mesh requirements with an n_x of 3, which yields one solid block on each subdomain. Then we use the stitched mesh generator to combine our generated meshes, and finally the subdomain bounding box generator to redefine out subdomains that were lost in the stitching. This yields the mesh we see in the simulation depicted in Fig. 1.

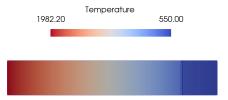


Figure 1: Heat map for simulated fuel rod with $n_x = 3$

[H] We can clearly see that the heat is uniformly diffusing across the fuel element. To resolve this numerical inaccuracy, we need to refine our mesh. In order to systematically control the mesh refinement process, I incrementally increased the number of subdivisions uniformly across each component, so that for $n_x = 9$, there are three nodes in the fuel, three across the gap, and three across the clad. Through this process, I began slowly increasing the number of subdivisions, then taking larger steps as convergence slowed, until we reached a sufficiently small change in center-line temperature between iterations in mesh refinement. The general refinement process can be seen in Fig. 2.

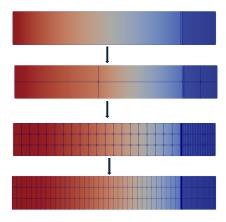


Figure 2: Abstracted flowchart of the mesh refinement process.

This ultimately yielded a change in temperature of $\Delta T_0 = 0.04^{\circ} K$ for an increase of 1 in n_x . We reached this tolerance at $n_x = 102$, or 35 subdivisions across each material (i.e. fuel, gap, clad). See a plot of our convergence by ΔT_0 vs n_x in Fig. 3.



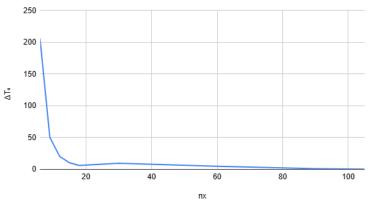


Figure 3: Convergence plot of change in center-line temperature as mesh is refined.

Not having a specified tolerance, I chose to stop here, as further refinement slowed the convergence of our thermal conductivity solver without yielding large improvements in calculated center-line temperature.

2.2.1 1-D Results

For our 1-D mesh refinement study in the solid state case we found a centerline temperature $T_0 \approx 1590$ K. This was close to the analytical solution for the steady state heat profile. Transient simulations were also performed but the steady-state results are far more helpful for validating the accuracy of our extension into 2-D. For the sake of completeness we will show the transient data $(LHR(t) = 350 \cdot e^{-\frac{(t-20)^2}{2}} + 350$, defined in the problem statement) so that the steady-state solution can be observed after recovery (e.g. t = 80[s] Find the results for the transient 1-D simulations shown in Fig. 4.

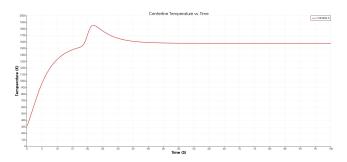


Figure 4: Centerline temperature vs. time for 1-D simulation of fuel pellet undergoing transient.

2.3 2-D Refinement

The 2-D refinement study is very similar to the 1-D case. The y component of the subdomains is extended to 1m, then the model is solved for various n_y values and the solutions are compared. To make it physically representative we implemented an LHR that varies axially

$$q(y) = \frac{\left(350 \cdot \cos\left(1.2 \cdot \left(\frac{y}{50} - 1\right)\right)\right)}{0.25 \cdot \pi}$$

We also implement a convective cooling boundary condition using the equation covered in class. T_{∞} is defined axially by the equation:

$$T_{\infty}(y) = 500 + \frac{1}{1.2} \cdot \frac{50 \cdot 350}{(.085 \cdot 4180) \cdot (\sin(1.2) + \sin(1.2 \cdot ((\frac{y}{50}) - 1)))}$$

The coolant specific heat, and flow rate values were determined to be reasonable compared to reported values in literature. [8,9] A bash script was implemented to automate the refinement study increasing n_y by increments of 10 from 10 to 110. The results of this study are seen in Figure 5.

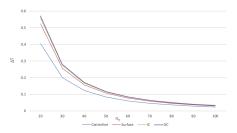


Figure 5: Residual convergence plot for mesh refinement in y direction.

The residual convergence (ΔT) was found through the following equation:

$$\Delta T(n_y) = \int_0^{100} |T_{n_y}(y) - T_{n_y-1}(y)| \, dy$$

Numerically, the residual convergence was computed as a Riemann sum with $\Delta y = \frac{1}{1000}$. The residual convergence alone appears to display favorable convergence behavior after $n_y \approx 50$ with $\Delta T \approx 0.1$, we observe further convergence to $\Delta T \approx 0.025$ K without significantly slowing the solver at $n_y = 100$. Given the lack of solver convergence at such a high refinement, $n_y = 100$ was determined to be sufficient refinement. One other reason for this is the aspect ratio of the elements. It is established that in finite element analysis large aspect ratios can introduce error into the solver.[10] Under $n_y = 10$ our aspect ratio a = 68,000, but increasing n_y to 100 gives us an aspect ratio of 6,800. Improving our aspect ratio by an order of magnitude promises to help mitigate the error of our numerical solver. It should be noted that in the 2-D refinement we operated in a constant step of y_n of 10, so the values of ΔT here overestimate the actual convergence behavior.

3 Steady State Simulation

To solve the temperature profile along this 2-D smeared pellet model, this model was ultimately the result of our final refined mesh. We observe the axial temperature profiles at key points in the fuel element in Fig. 6.

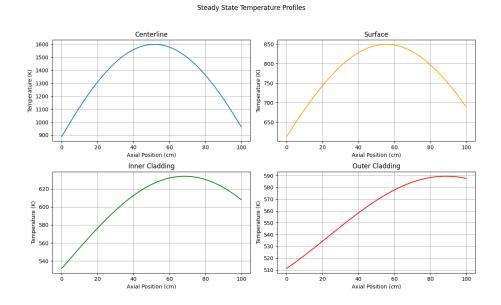


Figure 6: Axial temperature profiles for steady state simulation.

Given these temperature profiles we find that the temperature peaks at $y \approx 52 [\mathrm{cm}]$ on the centerline, and the peak moves up the rod as we move radially outward. This gives the outer clad a peak temperature located at $y \approx 89 [\mathrm{cm}]$. The axial temperature profile on the outer cladding is reasonable, despite peaking closer to the top than necessarily expected. This is likely due to the relatively low mass flow rate implemented for the coolant. Generally, all of the axial temperature profiles follow the expected cosine shape indicating that our steady-state solver is likely accurate. The peak centerline temperature of roughly $T_{\mathrm{max}} \approx 1592 \ \mathrm{K}$ aligns with the results from our 1-D refinement study which found a similar value of $T_0 \approx 1590 \ \mathrm{K}$ with $LHR = 350 \frac{[\mathrm{W}]}{[\mathrm{cm}]}$. Any discrepancy between the two is likely due to axial diffusion of heat, as well as a different coolant temperature due to the convective cooling boundary condition.

4 Transient Simulation

To implement the transient simulation we simply scale LHR_0 by the transient equation given in the problem statement from part 1.

$$q(y,t) = \frac{\left(350 \cdot e^{-\frac{(t-20)^2}{2}} + 350\right) \cdot \cos\left(1.2 \cdot \left(\frac{y}{50} - 1\right)\right)}{0.25 \cdot \pi}$$

The transient implementation is very similar to the steady state simulation, with the addition of a time derivative kernel. In the transient simulation, we observe more dynamic behavior. In Fig. 7 we can see that the axial position of the peak temperature drops as the transient peaks. This is due to the fact that the periodicity in the cosine function defining q(y,t) is constant despite a changing amplitude. This creates a higher axial thermal gradient which accelerates thermal diffusion in the axial direction. At the peak of the transient this thermal diffusion dominates the convective cooling and attracts the axial temperature profiles across the other components to the same profile as the LHR profile.

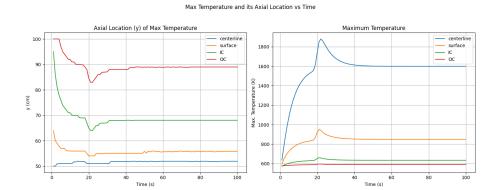


Figure 7: Plots of axial position of maximum temperature vs. time (left), and maximum temperature vs. time (right).

In the beginning of the simulation the IC, OC, and Surface of the fuel element are dominated by the convective cooling condition and due to the initial low temperature of the fuel 500 K, the convective cooling skews the temperature profile towards the top of the fuel element. 500 K was determined to be a suitable initial condition as it is the coolant inlet temperature provided in the problem statement. We also note that the widths of the minima in axial position correspond to what we might expect given the low thermal conductivity and moderately high specific heat compared to the cladding. The larger minima in axial position seen in $y(T_{\text{max}})$ is another indicator that the simulation is accurately modeling the transient. To gain further insight into the dynamics of the temperature profile we may refer to Fig. 8. This shows us the consistent

profile that we've come to expect from analytical solutions of axial temperature profiles (quadratic across the fuel and linear in gap and clad).

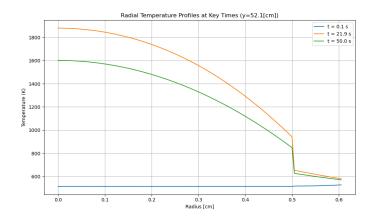


Figure 8: Radial temperature profiles at t = 0.1, 21.9, 50[s].

5 Conclusion

In this project we simulated the temperature profile and heating behavior of a 2-D smeared pellet fuel element. Mesh refinement studies were performed radially in 1-D and axially in 2-D. We found axial temperature profiles on the centerline, surface of the fuel, inner cladding, and outer cladding to be reasonable compared to expectations. We implemented a transient model and observed the variation in $y(T_{\rm max})$ as the fuel rod underwent the transient. Future studies would benefit from modeling the impact of micro-structural evolution of the fuel over time, thermal expansion of the fuel pellets, and fuel clad interaction. It would also be interesting to explore different criteria for convergence, rather than the residual convergence, it may be interesting to compare the axial locations of peak temperatures along the fuel element and the convergence behavior compared to the one presented here.

References:

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