NE 591 - EXAM 3

$$\begin{array}{lll}
\boxed{D} & \alpha = 8 \text{ p/m}; \quad \overrightarrow{F} = 2 \times 10^{14} \text{ fish}/(\text{cm}^3 \cdot \text{S}); \quad T = 1200 \text{K}. & \text{Vol} = \frac{\pi \alpha^3}{6} = 2.68 \times 10^{-10} \text{ cm}^3 \\
\boxed{\alpha} & D_4 = 4.6 \times 10^{-6} \text{ e}^{-3.03 \text{eV}/(2.614 \times 10^{-5})(1200)} = 1.428 \times 10^{-18} \text{ cm}^2/\text{S} & \overrightarrow{f} = 5.26 \times 10^{\frac{1}{4}} \text{ k/s}/\text{S} \\
\boxed{D}_2 = 1.41 \times 10^{-18} \text{ e}^{-1.19 \text{ eV}/(8614 \times 10^{-5})(1200)} & \sqrt{5.26 \times 10^{\frac{1}{4}}} = 3.28 \times 10^{-21} \text{ cm}^2/\text{S} \\
\boxed{D}_3 = 2.0 \times 10^{-20} (5.36 \times 10^4) = 1.04 \times 10^{-25} \text{ cm}^2/\text{S}} \\
\boxed{D} = \boxed{D}_1 + \boxed{D}_2 + \boxed{D}_3 = 1.43 \times 10^{-19} \text{ cm}^2/\text{S}
\end{array}$$

b)
$$6 = \frac{Dt}{a^2} = \frac{(6x10^{-16})(2.365.24.60.60)}{(8x10^{-4})^2} = 0.05913 < \pi^{-2} = 0.101$$

$$f = 4 \sqrt{\frac{(1.43 \times 10^{-18})(6.3 \times 10^{4})}{\pi (8 \times 10^{-4})^{2}}} - \frac{3}{2} \frac{(1.43 \times 10^{-18})(6.3 \times 10^{4})}{(8 \times 10^{-4})^{2}} = 2.65 \times 10^{-2}$$

total gas produced: $g = 0.3017(2\times10^{14})(6.3\times10^{7}) = 38\times10^{21}$ at /an³ total gas released: $(3.8\times10^{21})(2.65\times10^{-2}) = 1\times10^{20}$ at/cm³

c)
$$T = 2000K$$
, assuming $D = DL$
 $D = \pm .6 \times 10^{-6} e^{-3.03 eV/(8.61 \times 10^{-5})(2000)} = 1.46 \times 10^{-13} cm^{2}/5$

for $E > T^{-2}$, $f = -\frac{1}{4} + \frac{G}{\pi^{2}} e^{-\frac{1}{4}^{2}(1.46 \times 10^{-13}) \pm /(8 \times 10^{-4})^{2}} = -0.3$
 $e^{-2.42 \times 10^{-6}} = \frac{(1-0.3)\pi^{2}}{515725} = \frac{1.15}{515725}$

(2)
$$L^*(A) = 6.62 \times 10^{\frac{7}{2}} \exp\left(\frac{11947}{600}\right) = 295 \text{ days}$$

$$\delta^*(Wm) = 5.1 \exp\left(\frac{-550}{600}\right) = 2.04 \text{ MeV}$$

$$k_L \cdot \int .28 \times 10^6 \text{ Mp} \left(\frac{-12500}{600}\right) = 6.5 = \times 10^{-\frac{5}{2}} \text{ Ulm/d}$$

$$\delta(Vm) = 2.04 + 6.52 \times 10^{-3} \left(365 - 295\right) = 2.5 \text{ U/mV} \text{ on the Heighton}$$

$$\delta(Vm) = 300 \text{ MeV}, \quad LHR = 350 \text{ W/mV}$$

$$\epsilon_{WN} = 0.0 \int_0^{4\pi} \int_0^{4\pi} \int_0^{4\pi} \int_0^{4\pi} \int_0^{4\pi} \left(\frac{1}{3} \times 10^{44}\right) = 1.05 \times 10^{44}$$

$$c_1 = 0.95$$

$$c_2 = 1$$

$$\epsilon_{WN} = (2.414 \times 10^{-24}) \left(1.05 \times 10^{44}\right)^{0.81} \left(\frac{3}{3} \times 0\right) = 1.85 \times 10^{-10} \text{ s}^{-1}$$

$$\epsilon_{WN} = 5.84 \times 10^{-3} = 0.58 \frac{3}{4}$$

$$\delta_{WN} = 11 \times 10^{-6}$$

total volume change

GTOT = 0.0165 - 0.01 + 0.01193 + 0.01328 = 0.03171 - \$. 17%

- → Soluble oxides (Y, La and the rare earths)
 - Insoluble oxides (zn, Ba and Sr)
 - Metals (Mo, Ru, Pol and Tc)
 - Volatiles (Br, Rb, Te, I and Cs)
 - Noble gases (Xe, Kr)
- 5 st 1: gas atoms are produced in the fuel and differe towards grain boundaries,
- St 2: gas bubbles nucleate on GBs, growing and interconnecting st 3: gas travels through such interconnected bubbles to a free surface (leaves the full)
- (6) Naharro-Herring creep is based on bulk diffusion Coble creep is based on grain boundary diffusion
- De The models are based on the state of the microstructure instead of based one burnup. The material properties of fuel and cladding are determined from microstructure, and property relationships that are functions of materials state variables and current fuel conditions. It is valuable because there is a potential to provide a more predictive fuel performance capability
- 8 Low neutron cross section: almost no interaction with neutrons leaving them free for firming.

 Good thermal conductivity: important for cooling.

 Affordable cost

- D when the ful contains En, it diffuses via somet diffusion to the higher temperature region (anter of the slug radially). Having different concentrations of 2r along the fuel, the melting temperature is affected and different phases are formed in the slug, with different clastic and turnal properties
- DA Reactivity Initiated Accident is an accident caused by a large reactivity insertion in the cone, that can be caused by the sudden removal of the control rods. When there is a large reactivity insertion, the temperature increases rapidly and that can cause many consequences in the fuel, ultimately causing fuel melting
- Hydrides respond to temperature and stress graduants, so their ancentrations are not uniform; if mores toward lower temperatures causing a less of ductility and leading to early failure.

 They are formed on the dadding outer wall where there is

Ourosion