

1- There is certain number of oxygen atoms in UO_2 crystal structure depending on the charge state of the U atom. UO_2 stoichiometry represents the ratio of the oxygen to uranium metal. and O/M ratio means oxygen to metal ratio. In a perfect UO_2 lattice, this ratio is equal to 2. However, it can vary during the reactor operation which ends up the stoichiometry to go up and down.

Since it is very difficult to measure UO_2 stoichiometry, oxygen potential (which can be defined as how likely is the oxygen atom to go after to something else) can be used to determine the stoichiometry.

UO_2 stoichiometry is extremely important for the fuel performance since it impacts melting temp, thermal conductivity, grain growth, fission gas release, creep, chemical state and behavior of fission products, chemical reactions at inner cladding surface.

Q-2)

a) The grain boundary mobility, M_{GB} is given with the following equation:

$$M_{GB} = M_0 \exp\left[-\Theta/k_B T\right] \quad \text{where} \quad \begin{aligned} \Theta &= 2.77 \text{ eV} \\ k_B &= 8.62 \times 10^{-5} \text{ eV/K} \\ M_0 &= 4.6 \times 10^{-3} \text{ m}^4/\text{J.s} \end{aligned}$$

Temperature, T , can be calculated by using: $T(r) = T_s + \frac{q'}{4\pi k_f} \left[1 - \frac{r^2}{R_f^2}\right]$ where $\begin{aligned} q' &= 250 \text{ W/cm} \\ k_f &= 0.028 \text{ W/mK} \\ R_f &= 0.45 \text{ cm} \end{aligned}$

<u>$r[\text{cm}]$</u>	<u>$T[\text{K}]$</u>	<u>$M_{GB} [\times 10^{-18} \text{ m}^4/\text{J.s}]$</u>
@ $r = 0$	1511	2.65
@ $r = R_f/3$	1432	0.82
@ $r = R_f$	800	1.7×10^{-8}

b) Average grain size can be obtained by solving following equation numerically:

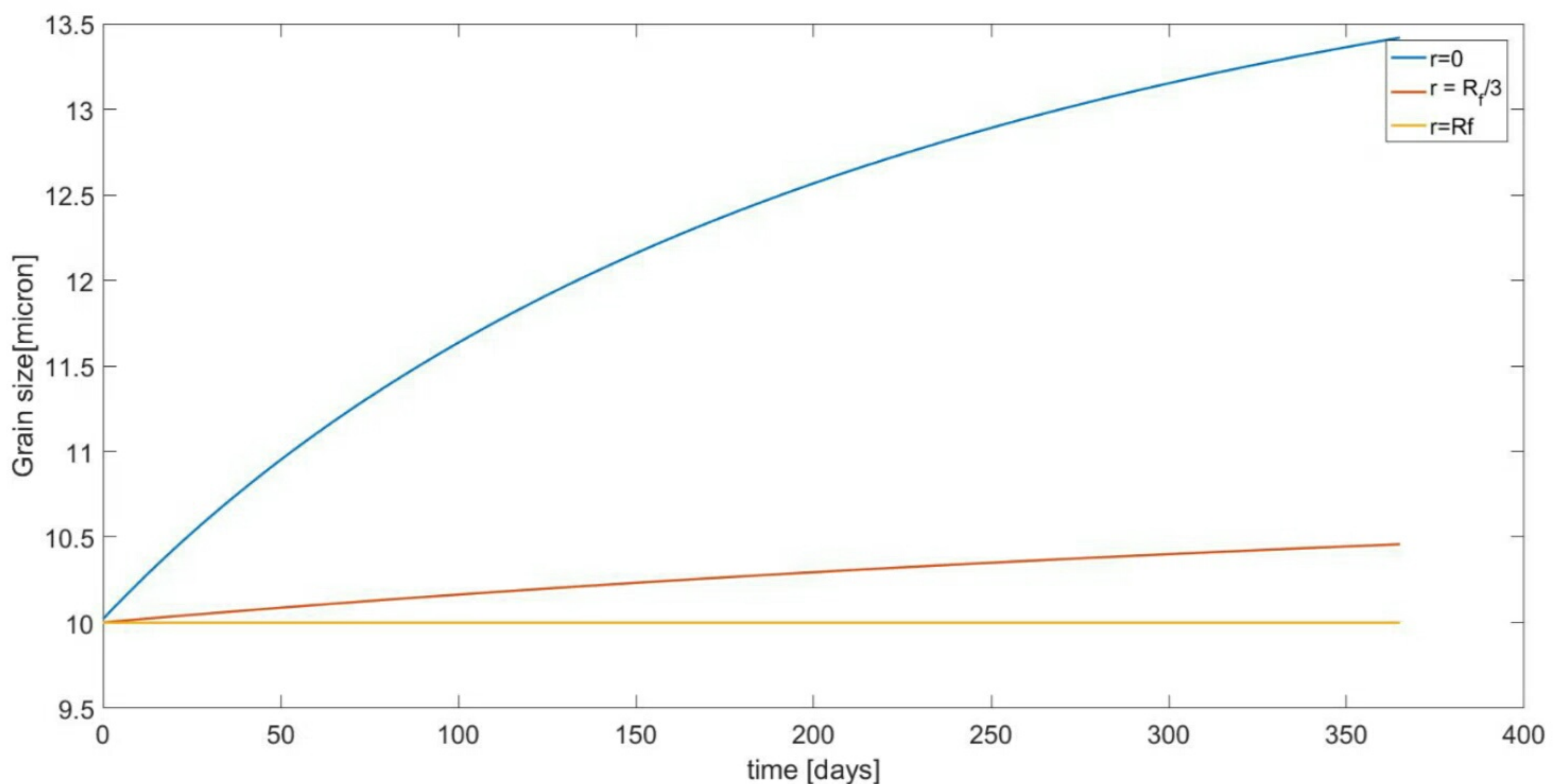
$$\frac{dD}{dt} = k \left(\frac{1}{D} - \frac{1}{D_m} \right) \quad \text{where} \quad \begin{aligned} k &= 2 M_{GB} V_{GB} \\ D_m &= 2.23 \times 10^3 \exp(-7620/T) \end{aligned}$$

$$\frac{dD}{dt} = k \left(\frac{1}{D} + \frac{1}{D_m} \right)$$

$$D[t+dt] = D(t) + dt \cdot k \left[\frac{1}{D(t)} + \frac{1}{D_m} \right]$$

By using M_{GB} values obtained in part (a); we can calculate the grain size after 1 year:

Distance [cm]	T [K]	$M_{GB} [m^4/Js]$	$k [m^2/s]$	$D_m [\mu m]$	$D [\mu m]$	
					$e_{t=0}$	$e_{t=1 \text{ year}}$
$r=0$	1511	2.65×10^{-18}	8.38×10^{-18}	14.4	10	13.42
$r = R_f/3$	1432	0.82×10^{-18}	2.59×10^{-18}	10.9	10	10.46
$r = R_f$	800	1.66×10^{-26}	5.22×10^{-26}	0.16	10	10



c) Grain size, D , stops evolving with time if $\frac{dD}{dt} = 0$ which yields $D = D_m$. Based on the results obtained in part b, this is satisfied at $r = R_f$. On the other hand, it takes more than 3 years for the grains at $r=0$ and $r = R_f/3$ to stop evolving with time.

$\Theta-3)$ a) $PV = n_{He} RT$ where $P = 2 \text{ MPa}$
 $T = 273 \text{ K}$
 $R = 8.314 \text{ MPa-cm}^3/\text{mol-K}$

$$\begin{aligned}
 V &= V_{\text{gap}} + V_{\text{plenum}} = \pi [R_{ci}^2 - R_f^2] h_{\text{pellet}} + \pi R_{ci}^2 h_{\text{plenum}} \\
 &= \pi \cdot (10 \times 0.119) (0.418^2 - 0.41^2) + \pi (0.418^2)(0.6) \\
 &= 0.577 \text{ cm}^3
 \end{aligned}$$

$$n_{He} = \frac{(2)(0.577)}{(8.314)(273)}$$

$$\boxed{n_{He} = 5.1 \times 10^{-4} \text{ moles}}$$

b) Temperature change across the fuel pellet is given as $\Delta T(r) = \frac{LHR}{4\pi k_f} \left[1 - \frac{r^2}{R_f^2} \right]$.

The average temperature can then be written as:

$$\begin{aligned}
 \overline{\Delta T} &= \frac{1}{\pi R_f^2} \int_0^{R_f} \Delta T(r) 2\pi r dr \\
 &= \frac{1}{\pi R_f^2} \int_0^{R_f} [A + Br^2] 2\pi r dr \quad \text{where } A = \frac{LHR}{4\pi k_f} \\
 &\quad B = -\frac{LHR}{4\pi k_f R_f^2} \\
 &= \frac{1}{\pi R_f^2} \left(\frac{2\pi r^2}{2} A + \frac{2\pi r^4}{4} B \right) \Big|_0^{R_f} \\
 &= \frac{1}{\pi R_f^2} \left[\pi R_f^2 A + \frac{\pi R_f^4 B}{2} \right] \\
 \downarrow \\
 \overline{\Delta T} &= A + \frac{BR_f^2}{2} \\
 &= \frac{LHR}{4\pi k_f} - \frac{LHR}{4\pi k_f R_f^2} \left(\frac{R_f^2}{2} \right) \\
 &= \frac{LHR}{4\pi k_f} \left(1 - \frac{1}{2} \right) \\
 \downarrow \\
 \overline{\Delta T} &= \frac{LHR}{8\pi k_f}
 \end{aligned}$$

→

$$\Delta \bar{T} = \frac{LHR}{8\pi k_f}$$

$$k_f = 0.03 \text{ W/cm K}$$

$$LHR = \frac{\Phi}{\pi R_f^2} = 246 \text{ W/cm} \rightarrow \text{calculated for } \begin{matrix} \phi = 2.75 \times 10^{13} \text{ n/cm}^2\text{s} \\ q = 4.2 \text{ wt.}\% \end{matrix}$$

$$\Delta \bar{T} = \frac{246}{8\pi(0.03)} = 326 \text{ K}$$

c) Since $\phi \rightarrow \phi(t)$, then $\dot{F} \rightarrow \dot{F}(t)$ and therefore $N_{FG} = y \dot{F} t \rightarrow N_{FG} = y \int_0^{2\text{yr}} \dot{F}(t) dt$

$$N_{FG} = y \int_0^{t_1} \dot{F}(t) dt$$

$$= y \left[\int_0^{t_r} \dot{F}_1(t) dt + \int_{t_r}^{t_1} \dot{F}_2(t) dt \right] \quad \text{where}$$

$$\dot{F}_1(t) = q N_u \sigma_f \phi_0 \frac{t}{3 \times 3600}$$

$$\dot{F}_2(t) = q N_u \sigma_f \phi_0$$

$$t_r = 3 \times 3600 \text{ s}$$

$$t_1 = 2 \times 365 \times 24 \times 3600 \text{ s}$$

$$= y \left[\int_0^{t_r} q N_u \sigma_f \phi_0 \frac{t}{t_r} dt + \int_{t_r}^{t_1} q N_u \sigma_f \phi_0 dt \right]$$

$$= y \left[q N_u \sigma_f \phi_0 \frac{t^2}{2t_r} \Big|_0^{t_r} + q N_u \sigma_f \phi_0 t \Big|_{t_r}^{t_1} \right]$$

$$= y \left[q N_u \sigma_f \phi_0 \frac{t_r}{2} + q N_u \sigma_f \phi_0 (t_1 - t_r) \right]$$

$$= y q N_u \sigma_f \phi_0 \left(t_1 - \frac{t_r}{2} \right)$$

$$= (0.3)(0.042)(2.44 \times 10^{22})(550 \times 10^{-24})(2.75 \times 10^{13}) \left(2 \times 365 \times 24 \times 3600 - \frac{2 \times 3600}{2} \right)$$

$$N_{FG} = 2.93 \times 10^{20} \text{ fission gas atoms/cm}^3$$

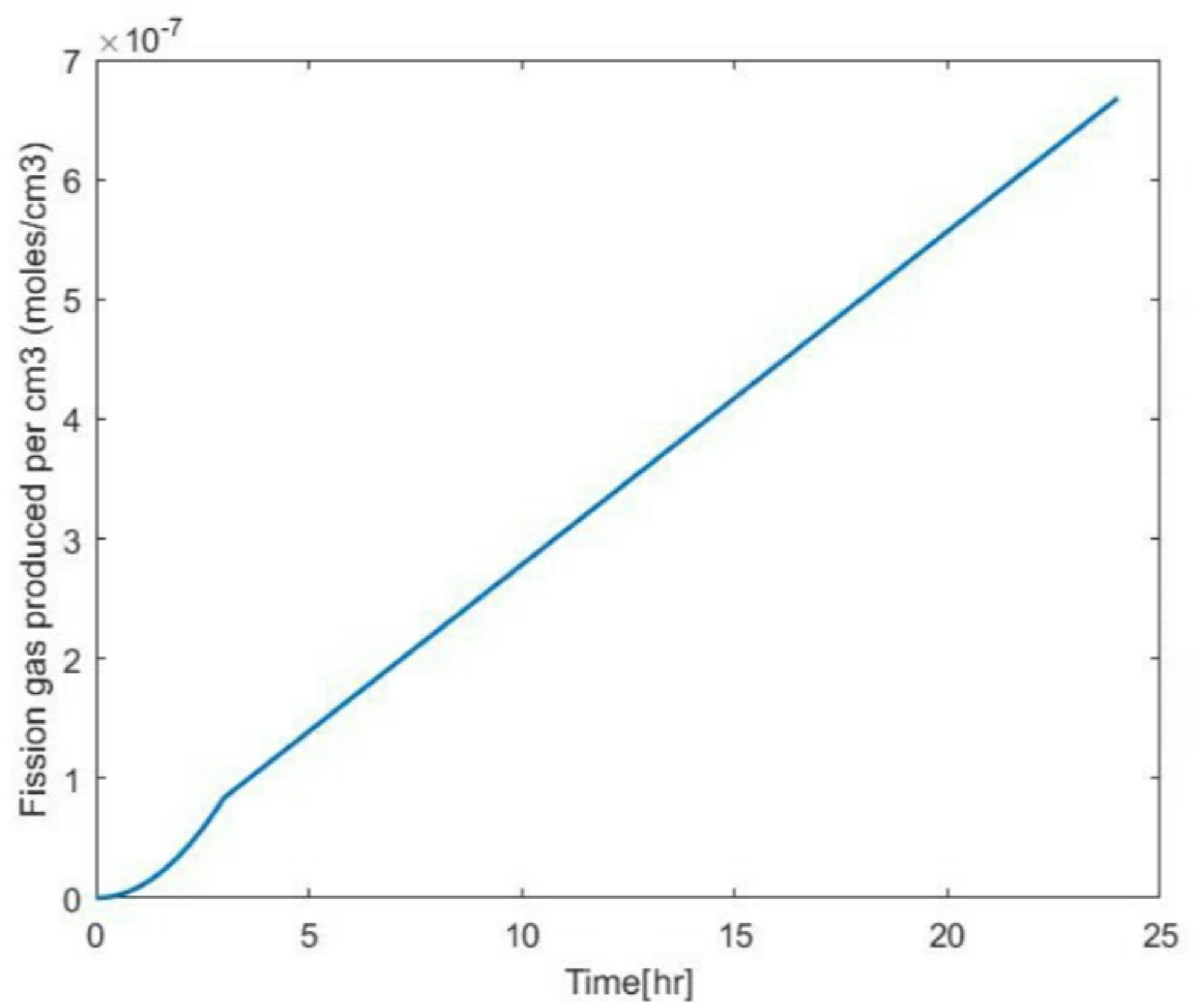
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$$N_{\text{gas}} = N_{\text{FG}} \cdot \text{Volume}$$

$$= (2.93 \times 10^{20}) (0.577 \text{ cm}^3)$$

$$N_{\text{gas}} = 1.69 \times 10^{20} \text{ fission gas atoms}$$

$$\text{or} \\ = 2.81 \times 10^{-4} \text{ moles}$$



d)

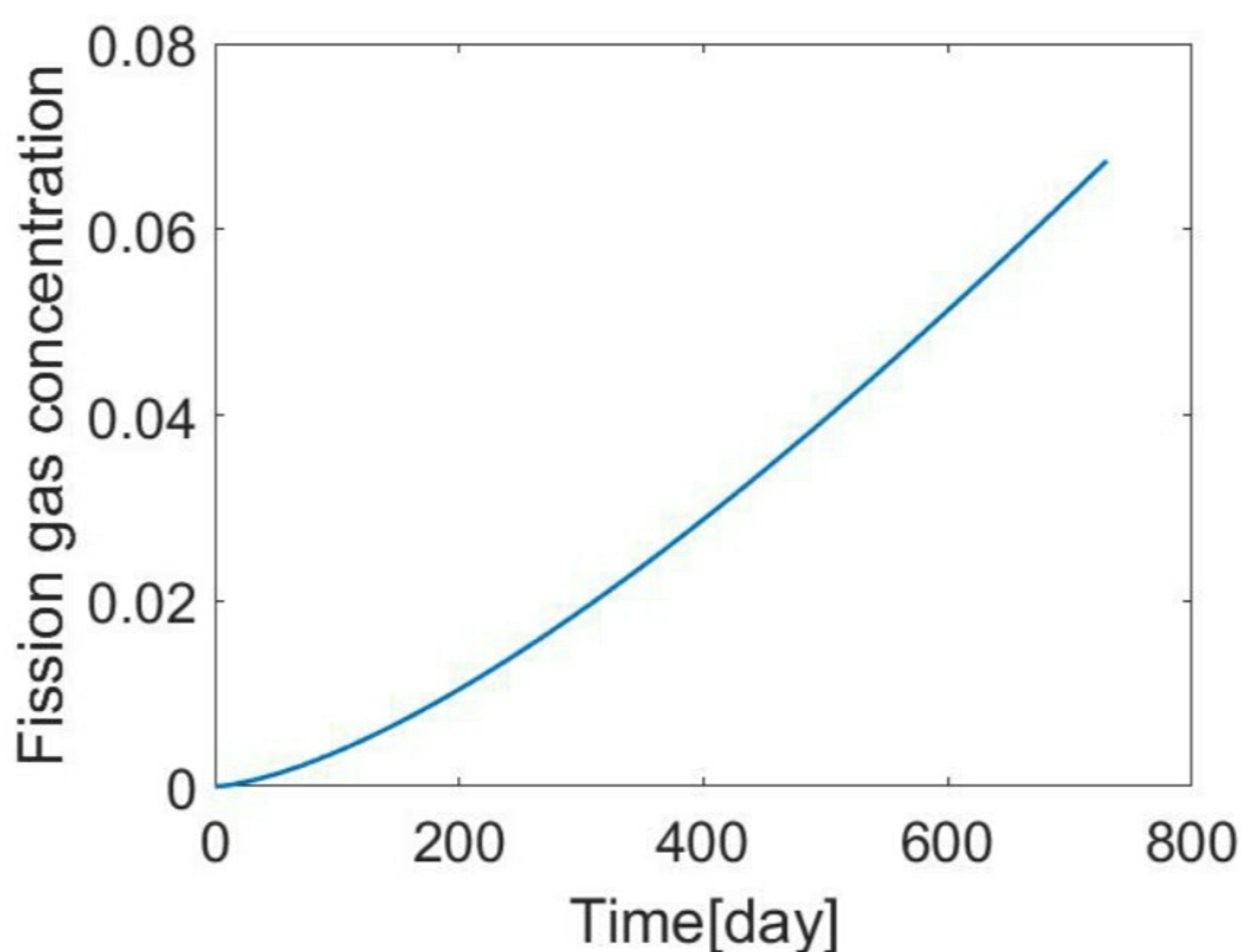
The amount of fission gas released to the gap can be calculated if fraction of fission gas released, f , is known. It can be obtained by using following equations:

$$f = 4 \sqrt{\frac{D t}{\pi a^2}} - \frac{3}{2} \frac{D t}{a^2} \quad \text{where } D = D_1 + D_2 + D_3$$

$\xrightarrow{\text{green}} 2 \times 10^{-36} \dot{F}$
 $\xrightarrow{\text{blue}} 1.41 \times 10^{-21} \exp\left(\frac{-1.19}{k_B T}\right) \cdot \sqrt{\dot{F}}$ and $T \rightarrow \bar{T}$
 $\xrightarrow{\text{red}} 7.6 \times 10^{-6} \exp\left(\frac{-2.03}{k_B T}\right)$ and $\dot{F} \rightarrow \dot{F}(t)$

Concentration of fission gas in the gap and plenum then can be calculated as:

$$C = \frac{f \cdot N_{\text{gas}}}{N_{\text{gas}} + N_{\text{He}}}$$



e) This equations can be simply added inside of a MATLAB function similar to what was done in the homework. Every time step, the amount fission gas released to the gap will be calculated. By using new concentration value, gap conductivity will be calculated.

0-4) a) Total volumetric change in a fuel pellet through the time is calculated as:

$$\epsilon_{\text{total}} = \underbrace{\epsilon_{\text{th}}}_{\text{thermal expansion}} + \underbrace{\epsilon_{\text{D}}}_{\text{densification}} + \underbrace{\epsilon_{\text{SFP}}}_{\text{solid swelling}} + \underbrace{\epsilon_{\text{GFP}}}_{\text{Gaseous swelling}}$$

Now, we will calculate volumetric change due to each mechanism:

Thermal expansion:

$$\epsilon_{\text{th}} = \alpha [\bar{T} - T_{\text{fab}}] \quad \text{where} \quad \alpha = 11 \times 10^{-6} \text{ } ^\circ\text{K}^{-1}$$

$$= 11 \times 10^{-6} [1126 - 300]$$

$$\bar{T} = 1126 \text{ K}$$

$$T_{\text{fab}} = 300 \text{ K}$$

$$\epsilon_{\text{th}} = 9.1 \times 10^{-3}$$

Densification:

$$\epsilon_{\text{D}} = \Delta \rho_0 \left[\exp \left(\frac{\beta \epsilon 0.01}{C_D \beta_D} \right) - 1 \right] \quad \text{where}$$

$$= 0.01 \left[\exp \left(\frac{0.04 \epsilon 0.01}{1 \cdot 0.0053} \right) - 1 \right]$$

$$\epsilon_{\text{D}} \approx -0.01$$

$C_D = 1$, because we are higher than 750°C

$$\beta_D = 5/950 = 0.0053 \text{ FIMA}$$

$$\Delta \rho_0 = 0.01$$

$$\beta = \frac{\int_0^t \dot{F}(t) dt}{Nu} \quad \text{where} \quad \int_0^t \dot{F}(t) dt = q \sigma_f Nu \phi_0 \left[t_i - \frac{t_R}{2} \right] \quad \text{from previous question}$$

$$\beta = q \sigma_f \phi_0 \left[t_i - \frac{t_R}{2} \right]$$

$$= (0.042) (550 \times 10^{-24}) (2.75 \times 10^{13}) \left[2 \times 365 \times 24 \times 3600 - \frac{2 \times 3600}{2} \right]$$

$$\beta = 0.04 \text{ FIMA}$$

Solid fission product swelling:

$$\epsilon_{\text{SFP}} = 5.577 \times 10^{-2} \rho \beta \quad \text{where} \quad \rho = \text{initial } \text{UO}_2 \text{ density} = 10.97$$

$$= 5.577 \times 10^{-2} (10.97) (0.04) \quad \beta = 0.04 \text{ FIMA}$$

$$\epsilon_{\text{SFP}} = 0.025$$

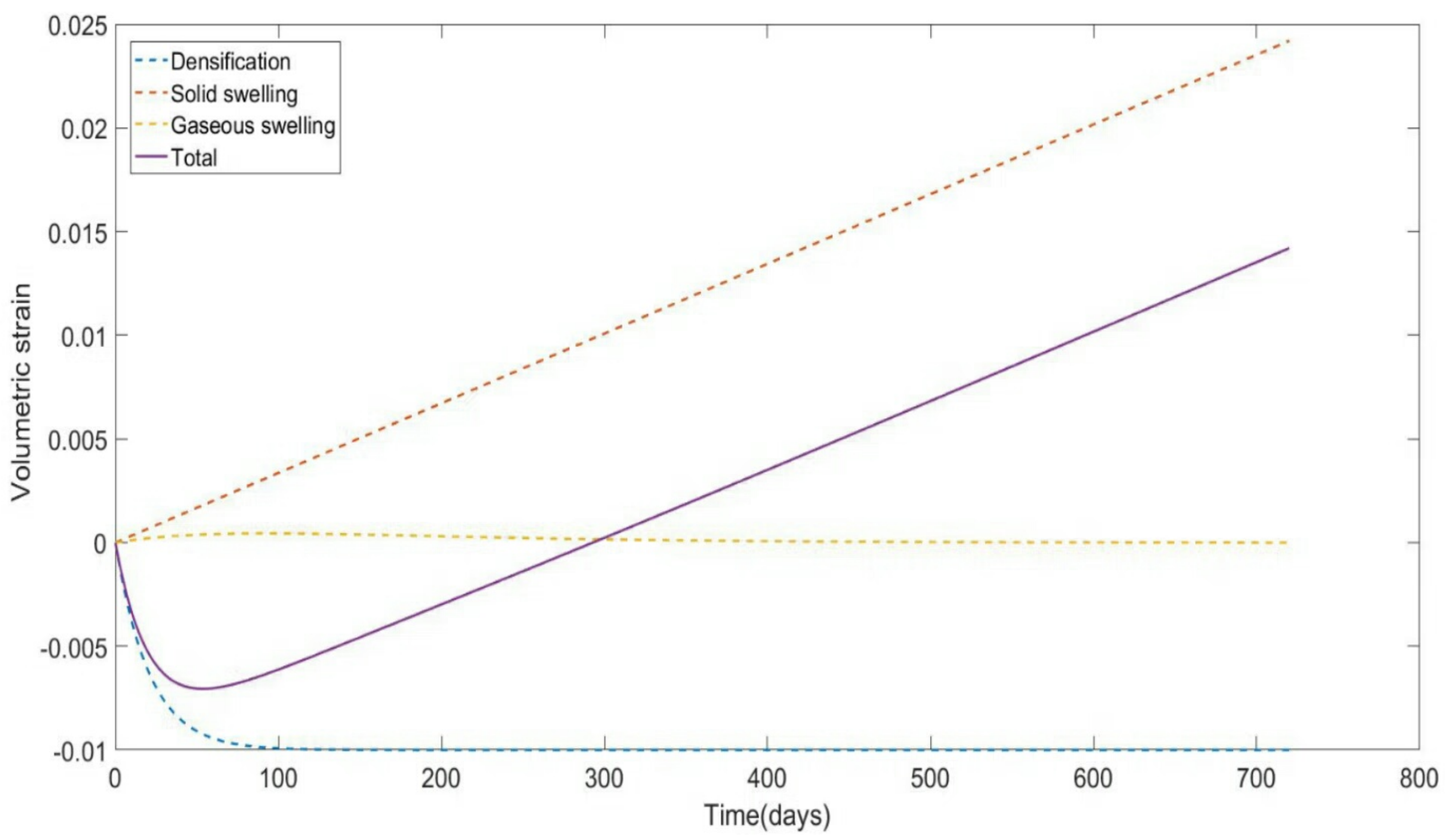
Gaseous fission product swelling:

$$\epsilon_{\text{GFP}} = 1.96 \times 10^{-28} \rho \beta (2800 - T)^{11.73} e^{-0.0162(2800 - T)} e^{-17.9 \rho \beta}$$

$$= 1.96 \times 10^{-28} (10.97) (0.04) (2800 - 1126)^{11.73} e^{-0.0162(2800 - 1126)} e^{-17.9(10.97)(0.04)}$$

$$\epsilon_{\text{GFP}} = 3.8 \times 10^{-6}$$

$$\epsilon_{\text{tot}} = 9.1 \times 10^{-3} - 0.01 + 0.025 + 3.8 \times 10^{-6} = 0.024$$



b) In this part, we will follow the same procedure as HW3-Q1. However, we will not only have thermal expansion but also contribution from densification, solid/gaseous fission products as well.

while

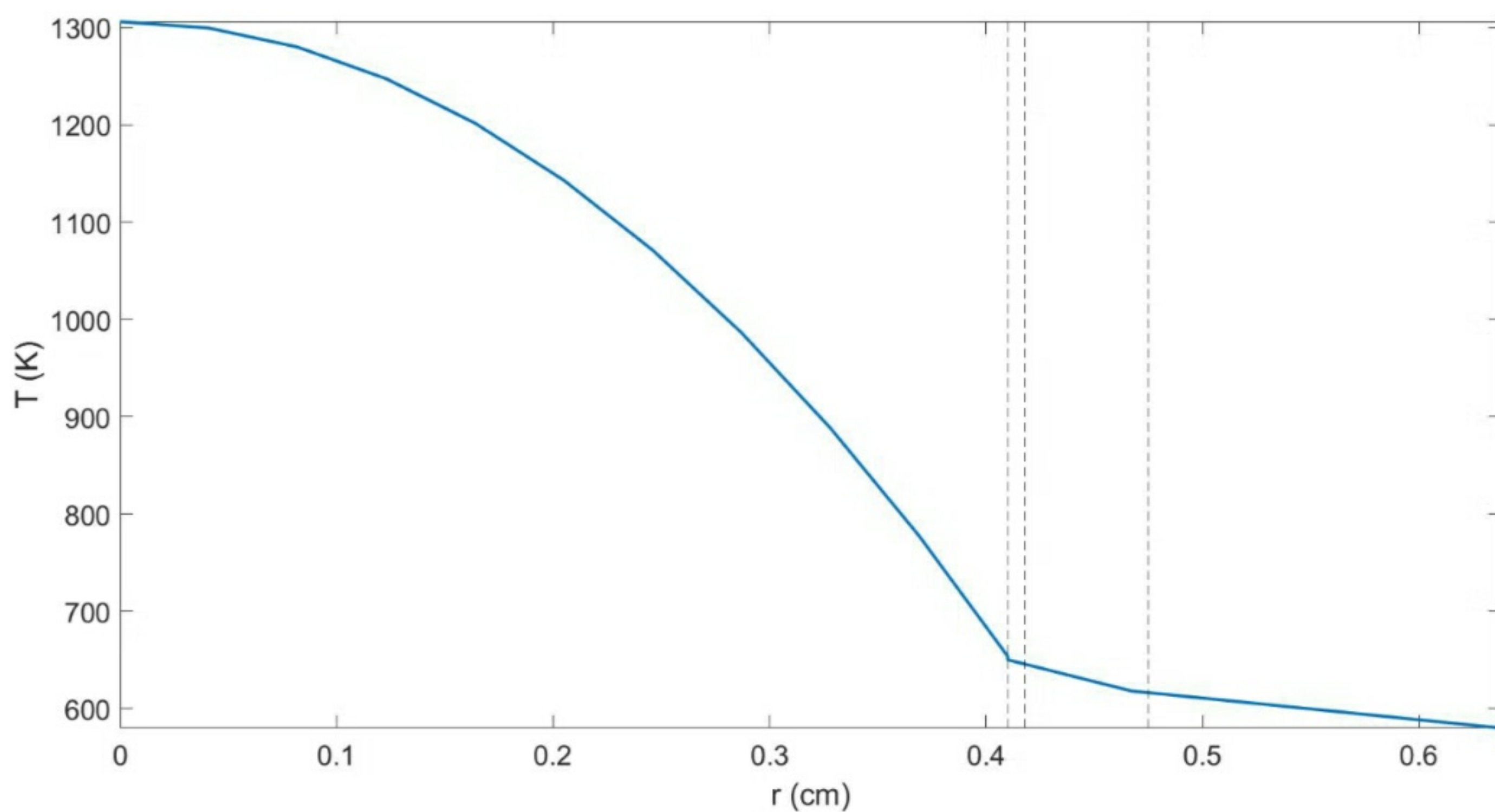
$$\left. \begin{aligned} \epsilon_{th} &= \dots \\ \epsilon_D &= \dots \\ \epsilon_{SFP} &= \dots \\ \epsilon_{GFP} &= \dots \end{aligned} \right\} \text{these values are calculated for the end of life of the fuel rodlet.}$$

$$\epsilon_{tot} = \epsilon_{th} + \epsilon_D + \epsilon_{SFP} + \epsilon_{GFP}$$

$$Ch_fuel = \epsilon_{tot} + R_p$$

< SAME AS HW3-Q1 >

end



c) These equations can be simply added inside of a MATLAB function similar to what was done in the homework. Every time step, the amount volumetric change in fuel will be calculated. By using this information, gap size (and conductance) will be calculated iteratively.

0-5)

$$k = (1 - R_f(T))k_{ph1}(T, \beta) + R_f(T)k_{ph2}(T, \beta) + k_{cl}(T)$$

$$R_f(T) = \frac{1}{2} \left(1 + \tanh \left(\frac{T - 900}{150} \right) \right)$$

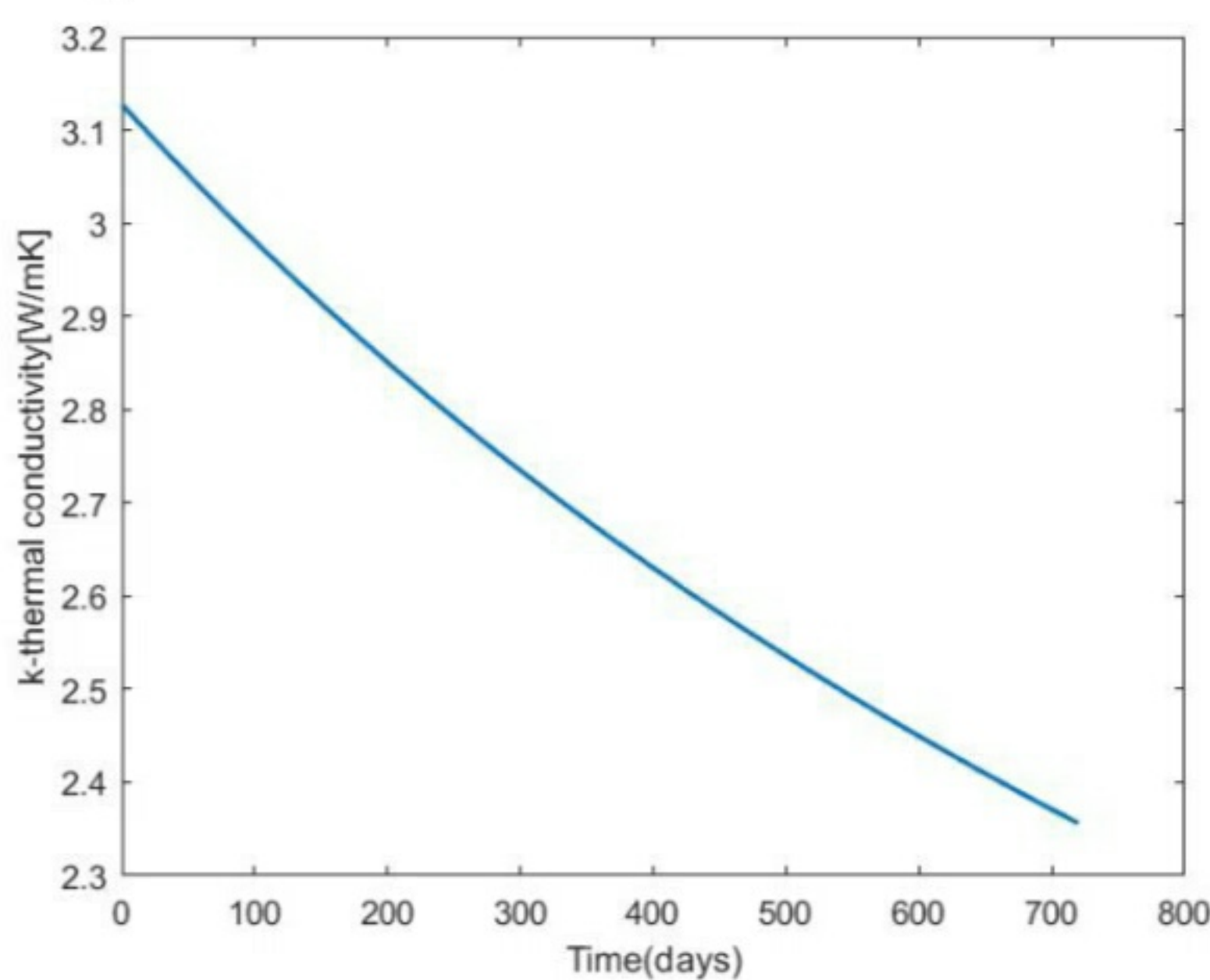
$$k_{ph1} = \frac{1}{(9.592 \times 10^{-2} + 6.14 \times 10^{-3}\beta - 1.4 \times 10^{-5}\beta^2 + (2.5 \times 10^{-4} - 1.81 \times 10^{-6}\beta)T)}$$

$$k_{ph2} = \frac{1}{(9.592 \times 10^{-2} + 2.6 \times 10^{-3} \cdot \beta + (2.5 \times 10^{-4} - 2.7 \times 10^{-7}\beta)T)}$$

$$k_{cl} = 1.32 \times 10^{-2} e^{1.88 \times 10^{-3}T}$$

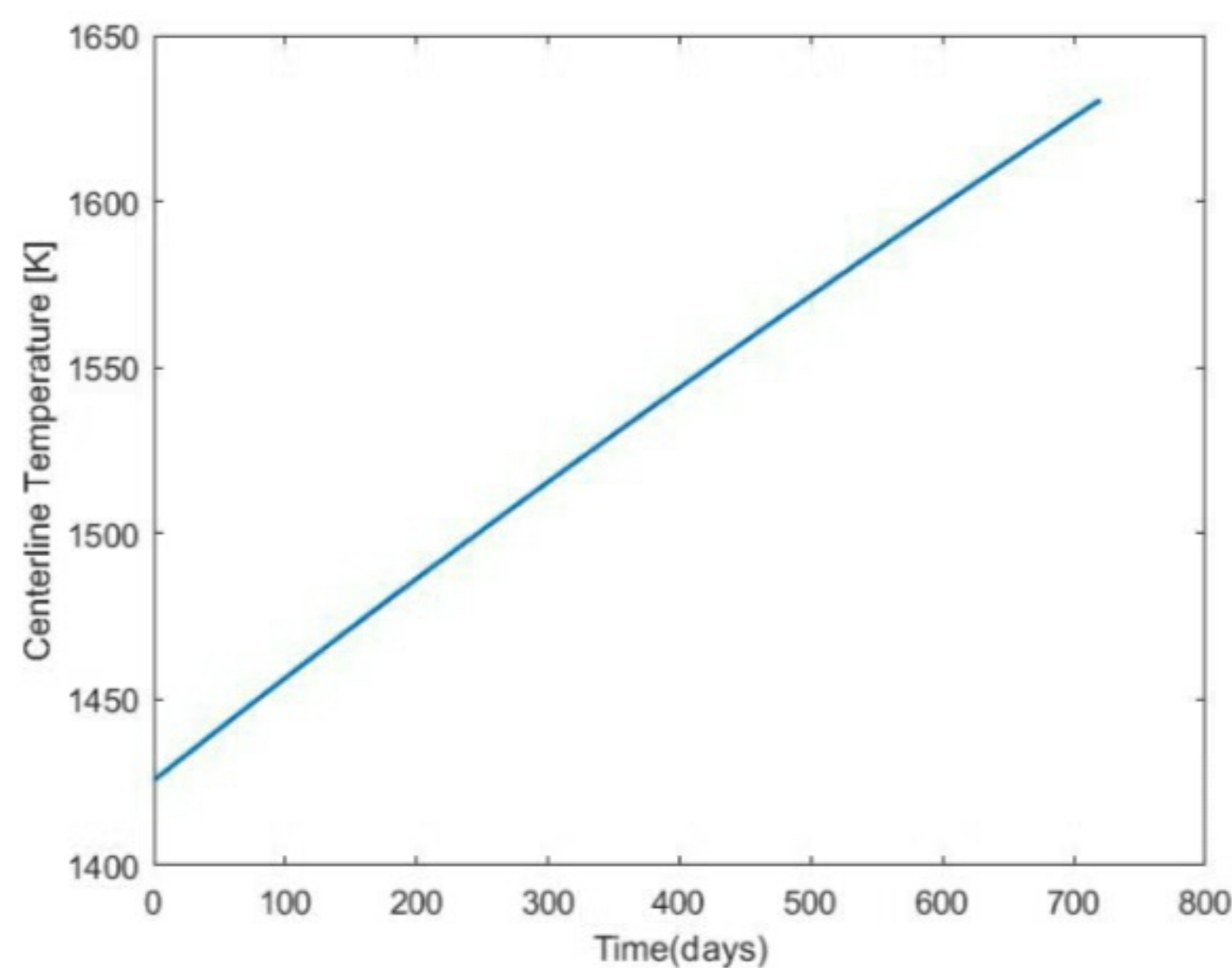
Note that $T \rightarrow ^\circ\text{C}$
 $\beta \rightarrow \text{MWd/kgU}$

a)



b)

$$T_0 = T_s + \frac{\text{LHR}}{4\pi k}$$



c) These equations can be simply added inside of a MATLAB function similar to what was done in the homework. Every time step, the fuel thermal conductivity will be calculated as a function of burnup. Then, the temperature @ new time step will be calculated by using new k .