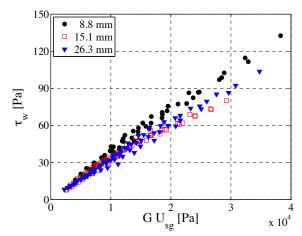
ENU 4134/6135 - Some Notes on Handling Data

Fall 2018

Something to consider...

Similar, but not identical, data range to Mini-Project 1.



Metrics of Average Error

$$MeanError = \frac{1}{n_{FC}} \sum_{FC} \frac{XX_{corr} - XX_{exp}}{XX_{exp}} \times 100\%$$
 (1)

$$MAE = \frac{1}{n_{FC}} \sum_{FC} \left| \frac{XX_{corr} - XX_{exp}}{XX_{exp}} \right| \times 100\%$$
 (2)

$$MAE = \frac{1}{n_{FC}} \sum_{FC} \left| \frac{XX_{corr} - XX_{exp}}{XX_{exp}} \right| \times 100\%$$
 (2)

$$RMS = \sqrt{\frac{1}{n_{FC}} \sum_{FC} \left(\frac{XX_{corr} - XX_{exp}}{XX_{exp}} \times 100\% \right)^2}$$
 (3)

These averages are:

- Constant under multiplication of data and correlation by a constant (e.g., m vs. ft).
- Not Always Constant if data shifted by an additive constant (e.g. temperature scale).
- ► Constant if data non-dimensionalized using dimensional variables (e.g., ΔP vs friction factors).

Correlating - No Single Algorithm

There is no single method to develop the equation to correlate experimental data, once you've determined which parameters to include.

Power laws (such as $Nu = ARe^B Pr^C$) are the customary first approach, but have no guarantee of success. They are especially poor in two-phase (in which both gas-based and liquid-based parameters have the same dimensions).

Suggestion: find a group of parameters that match dp/dz in dimension and then multiply by a dimensionless factor (friction factor, f). For example: a density times a velocity times a velocity divided by a length. Or: a mass flux times a velocity divided by a length. There should be "good-ish" correlation between your group of parameters and dp/dz, since f will not be terribly powerful.

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Using Flow-by-Flow Errors in Two-Phase Data

Consider making a spreadsheet grid of your data (with gas flow rising left-to-right, liquid rising bottom-to-top) and showing the error for each flow in the form.

- ▶ If left side is negative, right positive (or vice versa), gas effect mispredicted
- ▶ If top negative, bottom positive (or vice versa), liquid effect mispredicted
- ▶ If top left (high water, low gas) is positive, bottom right (low water, high gas) is negative (or vice versa), quality effect
- ▶ If top right (high water, high gas) is positive, bottom left (low water, low gas) is negative (or vice versa), total mass flow effect misprediced.
- ▶ If two opposite corners high, the other two low... your correlation is probably non-physical. (But may give OK results for MAE/RMS and an OK-to-good grade.)

ME, MAE, RMS Observations

- ▶ For an optimization correlation, ME should be very close to 0 (1% or less)
- ▶ MAE is the most useful metric to minimize
- ▶ The further MAE and RMS diverge, the more physical your correlation is likely to be (1.25 ratio from simulated data with random Gaussian uncertainty)

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Statistical Metrics of Correlation

Correlation coefficient:

$$R = \frac{1}{n-1} \sum_{i=1}^{n} \left(\frac{X_i - \overline{X}}{s_x} \right) \left(\frac{Y_i - \overline{Y}}{s_y} \right)$$
 (4)

 \dots where X_i and Y_i are (in either order) correlated and experimental results.

Often reported as R^2 .

 R^2 is:

- Constant under multiplication of data and correlation by a constant (e.g., m vs. ft).
- Constant if data shifted by an additive constant (e.g. temperature scale).
- ▶ Not Always Constant if data non-dimensionalized using dimensional variables (e.g., ΔP vs friction factors).

Which to Use?

The dominant means of reporting accuracy in the literature in with an error statistic – Mean Error, MAE, or RMS. The second most popular is by citing the fraction of data within a specific band (e.g., 80%) of the data within 20%).

Recommendations:

- ▶ Use MAE unless there is a compelling reason to do otherwise.
- ▶ If there is not a physically meaningful zero, consider using R^2 instead (or re-defining the zero so that it will have meaning).
- It is often a good idea to compute both, even if you don't use them. Example: even a poor friction factor correlation (judged by R²) can have a good MAE if the range of ρv² is very wide.

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