

RISK ASSESSMENT FORM

Department/ Area	FYIP - FYNAG
Job type/ Equipt System	FYNAG Manual choke and Flowline
Process	NAG Flow and Pressure Management from W/153
Task	Temporary Disconnection of HH and LL instrumentation (100 PZS 104A/B) from the process

Risk Assessment No.

	CONSEQUENCES				INCREASING LIKELIHOOD									
-			+	3000	Α	В	С	D Has happened at the Location or more than once per year in the Organisation	Has happened more than once per year at the Location					
SEVERITY	People	Assets	Environment	Reputation	Never heard of in the Industry	Heard of in the Industry	Has happened in the Organisation or more than once per year in the Industry							
o	No injury or health effect	No damage	No effect	No impact										
1	Slight injury or health effect	Slight damage	Slight	Slight										
2	Minor injury or health effect	Minor damage	Minor	Minor impact										
3	Major injury or health effect	Moderate damage	Moderate effect	Moderate impact										
4	PTD or up to 3 fatalities	Major damage	Major effect	Major impact										
5	More than 3 fatalities	Massive damage	Massive effect	Massive impact										

No.	To all Assistan	Risk/Hazard	Threats	To Essat & Comment	RAM Rating			g	Existing Controls	Recommendations	Action Party
No.	Task/Activity	Kisk/Hazard	1 nreats	Top Event & Consequence P A C E							
1	i. Do not disconenct HH and LL instrumentation (100 PZS 104A/B) from the process	1. Hydrocarbon gas under pressure	1. Over pressurisation of the instrumentation lines due to action of SDV (100 XZV 104)	1. LOPC with potential for fire, explosion and personnel injury	СЗ	C2	NA	C1	1. 1Disconenct HH and LL instrumentation (100 PZS 104A/B) the process.		Om Discipline, PMT
2		All construction and fabrication risks will be managed with JHA and PtW processes			NA	NA	NA	NA			
3	Post Implementation Risk - Temporarily disconenct HH and LL instrumentation (100 PZS 104A/B) from the process	1. Hydrocarbon gas under pressure	1.Third Party damage/process hazards or risks that would result to a line rupture	1. Subsea leak with potential for escalations	С3	C2	C1	C2	1. 100 PZL 101LL 2. 3123 PZL 001 LL		
			2. Potential over pressure of downstream equipmentsand Slugcatcher at the CPF at higher than required bean size	2.LOPC with potential for fire, explosion and personnel injury	C4	C2	NA	C2	1. 3123 PZA 001 HH at Pig receiver 2. Slug cacther Relifef valve -3123 RV 100 4. Flow line is fully rated	Ensure production Bean sizes are within the acceptable range for landing pressures and flow required at the CPF Ensure set point of 3123 PZA 001 HH is set at 88barg and always enabled	Production Technologist/ Asset

Risk Assessment Team								
Name:	Ajilore Linda	Position: Senior Process Engineer	Sign:	Date:				
Name:	Ebinum Olise	Position: Senior PACO Engineer	Sign:	Date:				
Name:	lloma Izu	Position: Process Safety Specialist	Sign:	Date:				
Name:	Egodo Edward	Position: Field operations Supervisior, Forcados	Sign:	Date:				
Name:	Okoro Felix	Position: Production Technologist, Forcados	Sign:	Date:				
Name	Okolomma Emmanuel	Position: Senior Wells Engineer (CWI)	Sign:	Date:				
Approva	ıl		Sign:	Date:				
Name:	Nwandu Eze	Position; Lead, FYIP Onshore	Sign:	Date:				
Name:	Olowu Adesegun	Position; Engineering Lead	Sign:	Date:				

Reference documents:

