

SAC design

Deconstructing Combustor Design: A Technical Analysis of a Single Annular Combustor (SAC) Methodology

1. Introduction: Automating Preliminary Combustor Design

The design of Gas Turbine Combustors (GTC) is an inherently complex and time-intensive process, involving coupled non-linear equations and extensive calculations. The source paper addresses this challenge by presenting a detailed, automated methodology for the preliminary design phase. The primary objective is to create a systematic, step-by-step procedure for a Fuel Rich Dome Combustor (also referred to as a Single Annular Combustor or SAC).

This technical analysis performs a deep dive into the paper's methodology. It extracts the key governing equations, critical design assumptions, and performance evaluation criteria that form the foundation of this automated approach.

2. Foundational Inputs and Air Distribution Logic

The design process originates from a set of required parameters derived from the engine's thermodynamic cycle. These inputs define the operational requirements:

- m_a : Compressor exit mass flow rate
- T_{03} : Compressor exit total temperature
- P_{03} : Compressor exit total pressure
- **FAR**: Fuel-to-Air Ratio
- **TIT**: Turbine Inlet Total Temperature
- π_b : Combustor pressure ratio
- $\Delta P_b/P_{03}$: Total pressure loss through the combustor
- **NFN**: Number of fuel nozzles

The first critical step is **air distribution**. The goal is to apportion total airflow (m_a) between the dome (m_{dome}) and the liner passage ($m_{passage}$). This is essential for managing fuel atomization, flame stabilization, and liner cooling.

Key Calculations

The process begins with an energy balance to determine the required fuel flow rate (m_f) and subsequent ratios.

Total Fuel Flow Rate (m_f):

$$m_f = \frac{m_a \cdot C_{pa} \cdot (TIT - T_{03})}{HV \cdot \eta_b}$$

(Where C_{pa} is the specific heat of air, HV is the fuel heating value, and η_b is combustion efficiency)._

Air-to-Fuel Ratio (AFR) & Equivalence Ratio (Φ_{PZ}):

These are derived directly from the calculated m_f and the input air mass flow.

Distribution Assumptions

The logic relies on typical values derived from conventional designs:

| Parameter / Ratio | Assumed Value / Range | Purpose / Rationale |
|-------------------|--|---|
| $m_{a,atom}/m_f$ | 2 to 3 | Ensure sufficient atomization of fuel. |
| m_{dome}/m_a | 10–15% | Typical for conventional combustors. |
| Φ_{PZ} | 1.4 to 1.5 | Avoid low efficiency at idle and smoke at high power. |
| ω_3 | $0.75 \text{ kg s}^{-1} \text{ m}^{-2} \text{ atm}^{-1}$ | Typical combustor loading parameter. |

3. Combustor Sizing and Reference Velocity

Once the air distribution is defined, the combustor's main physical dimensions are estimated using the **velocity method**. This anchors the initial layout in established practice by constraining flow characteristics.

Reference Velocity (V_{ref}):

$$V_{ref} = \frac{m_a}{\rho_3 A_{ref}}$$

(Where ρ_3 is the air density at the compressor exit and A_{ref} is the combustor reference area)._

Combustor Length (L):

The length is determined by scaling laws involving the length-to-diameter ratio and pressure drop factors:

$$L \cdot f\left(\frac{L}{ref}, \frac{\Delta P_L}{q_{ref}}\right)$$

(Where $\Delta P_L/q_{ref}$ is the liner pressure drop normalized by the reference dynamic head).—

Note: The methodology assumes a combustor velocity (V_c) between **35–60 m/s** and a dome velocity (V_d) between **7–12 m/s**.

4. Aerodynamic Performance: Pre-Diffuser Design

The pre-diffuser recovers inlet dynamic head, converting kinetic energy into static pressure before the air enters the combustion zone.

Ideal Pressure Recovery Coefficient (C_{pi}):

This represents the theoretical maximum recovery assuming no frictional losses.

$$C_{pi} = 1 - \frac{1}{A^2}$$

(Where A is the diffuser Area Ratio, A_{exit} / A_{inlet}).

The design process iterates the Area Ratio (A) from **1.4 to 3.0** to minimize total pressure loss. The diffusion angle (θ) is constrained to **4°–8°** to prevent flow separation.

5. Fuel Atomization and Flame Stabilization

Effective fuel preparation and flame anchoring are contingent on the fuel injection and air swirl subsystems.

5.1. Dual Orifice Fuel Nozzle

A dual-orifice design is mandated to handle the wide turndown ratio of gas turbines.

- **Primary (Pilot):** For low-flow/idle conditions ($C_{d,p} \approx 0.36$).
- **Secondary (Main):** For high-power conditions ($C_{d,s} \approx 0.27$).

Nozzle Flow Number (F_I):

$$F_I = \frac{m_f}{\Delta P_f \rho_f}$$

(Where ΔP_f is pressure drop across the nozzle and ρ_f is fuel density).

5.2. Axial Swirler Design

The swirler generates a Central Recirculation Zone (CRZ) to recirculate hot combustion products and anchor the flame.

Swirl Number ():

To establish a stable CRZ, the Swirl Number must typically be 0.6.

$$= \frac{2}{3} \left[\frac{1 - (d_h/d_o)^3}{1 - (d_h/d_o)^2} \right] \tan \phi$$

(Where d_h is hub diameter, d_o is outer diameter, and ϕ is the vane angle).

6. Thermal Management and Liner Cooling

With gas temperatures exceeding **2000°C**, active cooling is mandatory. The methodology employs a heat transfer balance model accounting for convection, radiation, and conduction.

Film Cooling Effectiveness (η_f):

This defines the performance of the cooling air film in insulating the wall.

$$\eta_f = \frac{T_g - T_{aw}}{T_g - T_c}$$

(Where T_g is hot gas temp, T_{aw} is adiabatic wall temp, and T_c is cooling air temp).

Thermal Barrier Coating (TBC) Conduction:

If a ceramic coating is used, the temperature drop across the coating is calculated as:

$$Q_{cond} = \frac{k_{TBC}}{t_{TC}} (T_{w1} - T_{if})$$

(Where k_{TBC} is thermal conductivity, t_{TC} is thickness, and T_{if} is the interface temperature).

7. Performance Evaluation: Emissions and Droplet Lifetime

The final step evaluates the combustor's efficiency and environmental impact.

7.1. Fuel Spray and Evaporation

For complete combustion, the droplet lifetime (d) must be less than the residence time ($_{res}$).

Droplet Lifetime (D-squared Law):

$$d = \frac{d_0^2}{K}$$

(Where d_0 is the initial droplet diameter and K is the evaporation constant).

7.2. NOx and CO Emissions

Empirical NOx Estimation:

Useful for rapid system-level trade-offs.

$$I = 0.15 \times 10^{16} (_{res})^1 \exp\left(\frac{-71100}{T_{st}}\right) P_{03}^{0.25} (V_c)^{-1}$$

Physics-Based Zeldovich Mechanism:

For fundamental analysis, the thermal NOx formation is modeled using three core reactions:

1. $+ \text{O}_2 + \text{N}_2 \rightarrow \text{NO} + \text{O}_2$
2. $+ \text{O}_2 + \text{H}_2 \rightarrow \text{H}_2\text{O} + \text{O}$
3. $\text{O} + \text{H}_2 \rightarrow \text{H}_2\text{O} + \text{H}$

These are combined into a final rate generation equation:

$$\frac{d[\text{NO}]}{dt} = \frac{2[\text{O}_2]_{f1} \left(1 - \frac{b_1 b_2 [\text{NO}]^2}{f_1 f_2 [\text{O}] [\text{NO}]} \right)}{1 + \frac{b_1 [\text{O}]}{f_2 [\text{O}_2] + f_3 [\text{H}]}}$$

8. Conclusion

The technical methodologies extracted from the source paper form a cohesive framework for the preliminary design of a Fuel Rich Dome Combustor. By balancing empirical correlations for rapid sizing with first-principles calculations for kinetics and heat transfer, this automated tool allows designers to efficiently explore the design space and assess performance trade-offs.