1-----

We have two heat transfers:

Convection - Which is the heat transfer between a fluid and a solid

Conduction- Which is the heat transfer inside the solid

Example of convection and conduction is that - Inside a wall we have **Conduction** and outside we have **Convection**

So when we need to find the temperature of the wall and not the temperature inside we have to combine convection and conduction

We have to types of convection, which are: Natural and Forced

The rate of convective heat transfer depends on:

- Variation of the heat
- Speed of air (velocity of liquid or gas)
- Kind (type) of liquid or gas

Newtons Law of Cooling

Qconv. = $h \times As \times (Ts - T\infty)$

Temp. of the surface Ts and Temp. of the room inside the room T∞

$$Rconv = \frac{1}{h x As}$$

According to this formula the higher the air the less resistant (higher the h less resistance we have), because resistance R

Is not proportional to h

$$Q = \frac{T \infty 1 - T \infty 2}{R \ total}$$

R total = Rcon1 + Rwall + Rcon2 = $\frac{1}{h_{1A}} + \frac{L}{kA} + \frac{a}{h_{2A}}$

$$Rg = \frac{L}{k \times A}$$

The glass doesn't have a big role in heat transfer (thermal resistance of convection-glass is very small compared to conduction - glass and air), so if we raise the thickness L still the same

temperature goes inside or a very slight difference which is not to be considered.

2-----

The reason I resulted on wrong answer was the problem of calculation (Math part), the other part of the assignment went well .

3-----

Consider a 0.8-m-high and 1.5-m-wide double-pane window consisting of two 6-mm-thick layers of glass (k= 0.78 W/m. $^{\circ}$ C) separated by a 13-mm-wide stagnant air space (k= 0.026 W/m. $^{\circ}$ C). Determine the steady rate of heat transfer through this double-pane window and the temperature of its inner surface.

Take the convection heat transfer coefficients on the inner and outer surfaces of the window to be $h1=10 \text{ W/m2} \cdot {}^{\circ}\text{C}$ and $h2=40 \text{ W/m2} \cdot {}^{\circ}\text{C}$, which includes the effects of radiation.

$$A = 0.8 \text{m x } 1.5 \text{m} = 1.2 \text{ m} 2$$

Rcon1 =
$$\frac{1}{h_{1xA}} = \frac{1}{10x_{1.2}} = 0.0833^{\circ}C/W$$

Rcon2 =
$$\frac{1}{h2xA}$$
 = $\frac{1}{40x1.2}$ = 0.0208° $\frac{C}{W}$

Rglass =
$$\frac{1}{k \ glassxA} = \frac{0.006}{0.78x1.2} = 0.0064^{\circ} \frac{C}{W}$$

R air =
$$\frac{1}{k \ airxA} = \frac{0.013}{0.026x1.2} = 0.4167^{\circ} \frac{C}{W}$$

Rtot = Rcon1 + Rglass1 + Rair + Rglass2 + Rcon2 = $0.0833+0.0064+0.4167+0.0064+0.0208 = 0.5336 \circ \frac{C}{W}$

$$Q = \frac{T \infty 1 - T \infty 2}{Rtot} = \frac{20 - (-10)}{0.5336} = \frac{30^{\circ} C}{0.5336^{\circ} C/w} = 56.221W$$

$$Q = \frac{T \infty 1 - T1}{Rcon1} =$$

T1 = $t \approx 1 - Q \times Rcon1 = 20^{\circ}C - 56.221W \times 0.0833^{\circ}C/W \approx 15.3^{\circ}C$