

# SOLAR COOLING

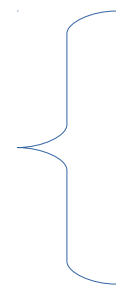
**Dr. Herena Torio**

# Outline

## INTRODUCTION

- Cooling market
- Psychrometric processes
- Basic principle

## AVAILABLE TECHNOLOGIES

- Compression chillers
  - TDCs:
    - Absorption chillers
    - Adsorption chillers
  - Desiccant systems
- 
- Principles
  - Thermodynamic analysis
  - System performance

# Thermally driven compression chiller Principle

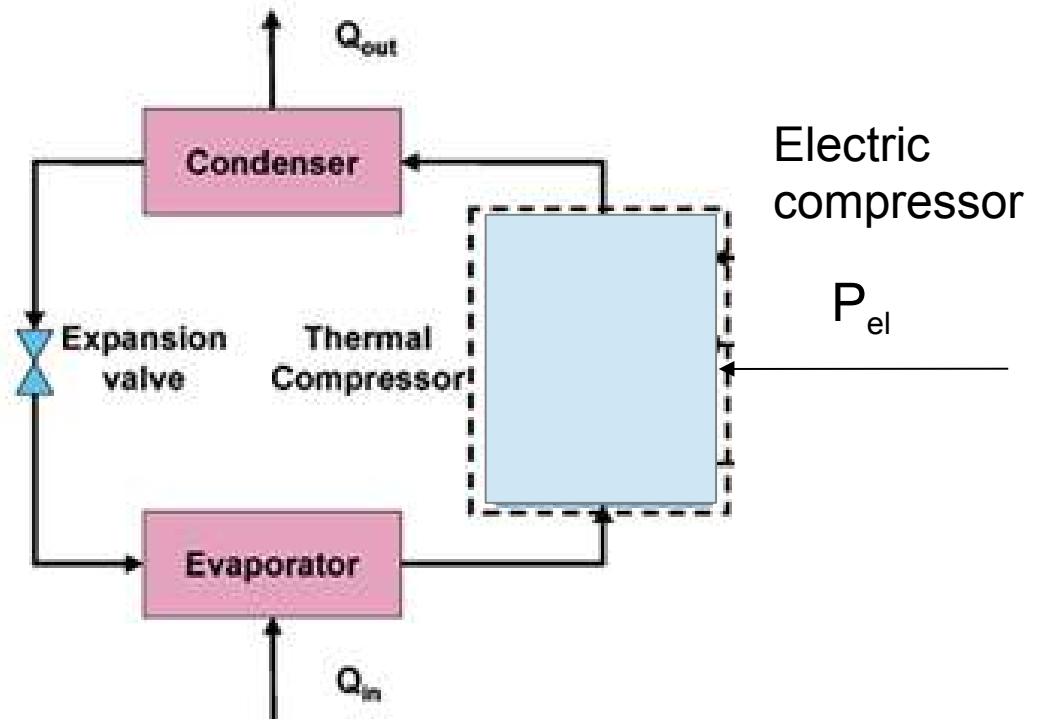
## Principle:

Substitute **mechanical compression**

by

**thermal compression**

→ **ABSORPTION**  
→ **ADSORPTION**



# Thermally driven compression chiller Principle

Principle:

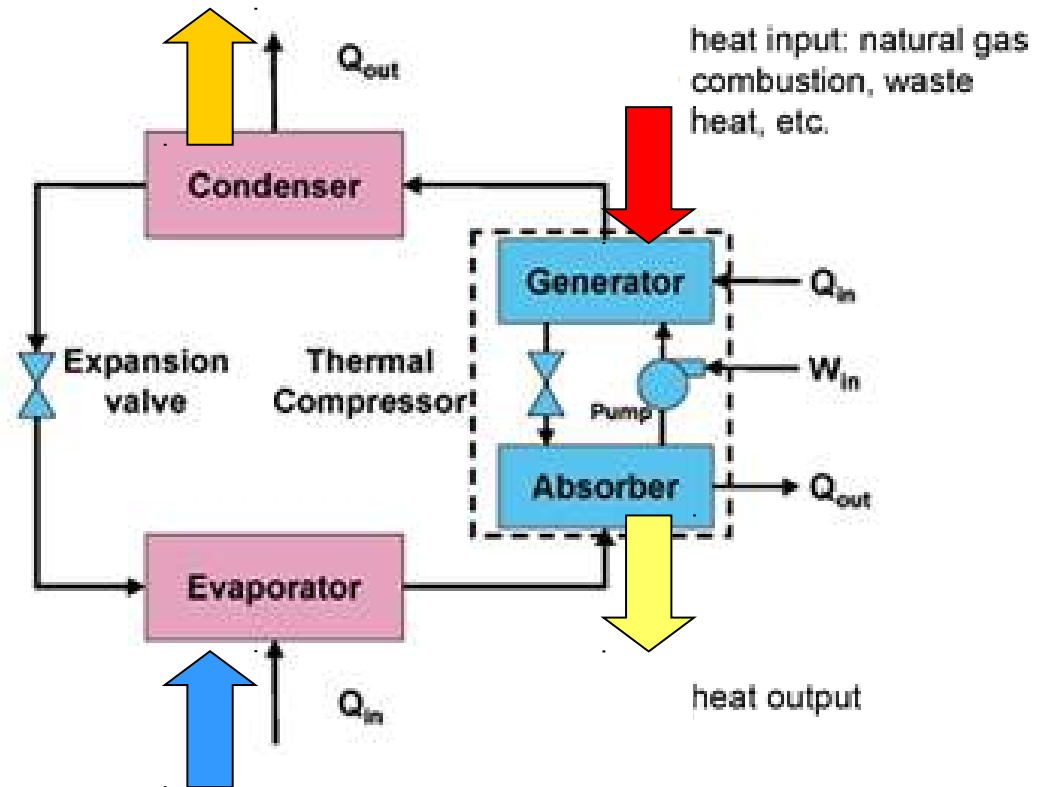
Substitute mechanical  
compression

by

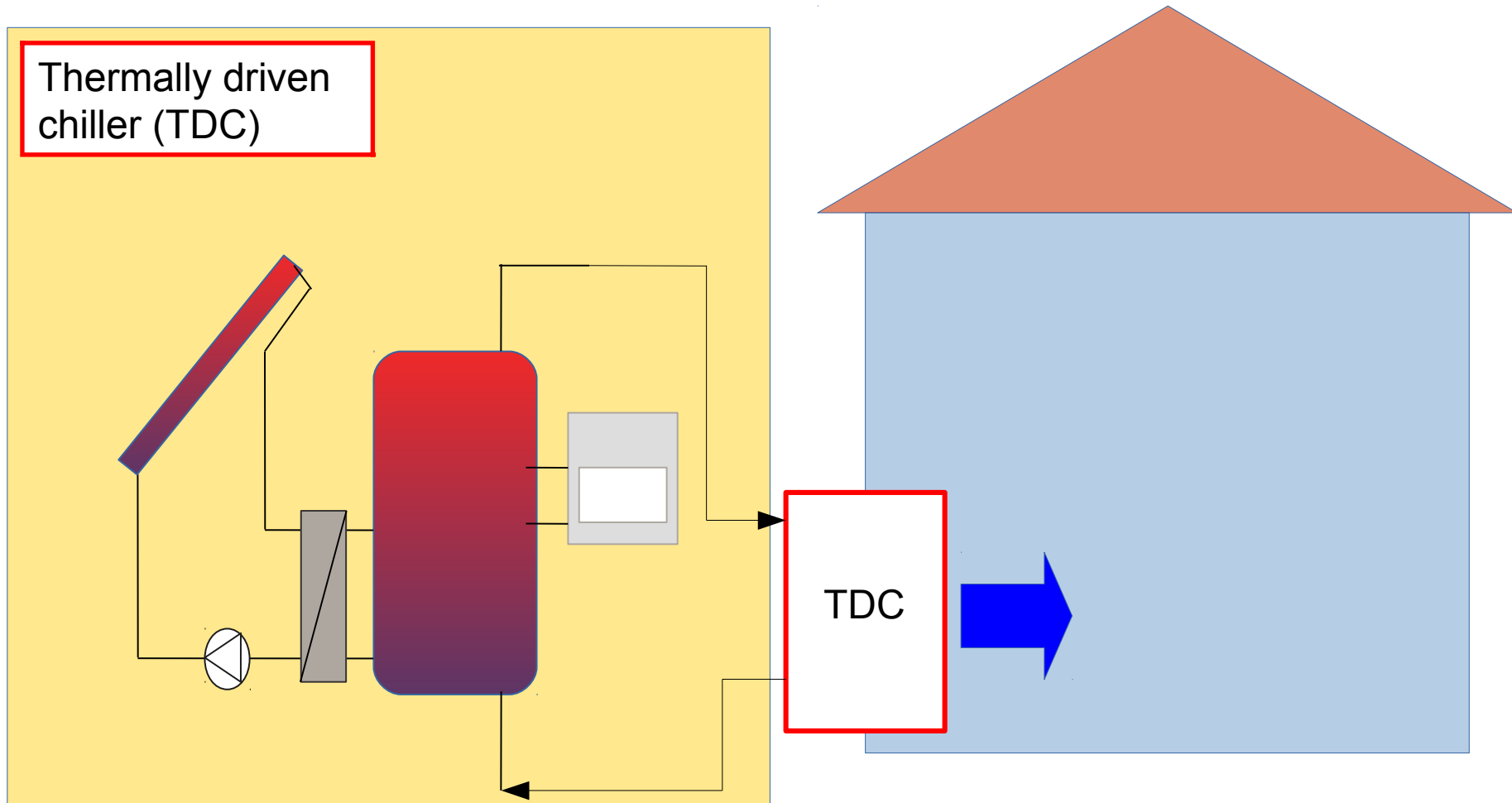
Thermal compression

ABSORPTION

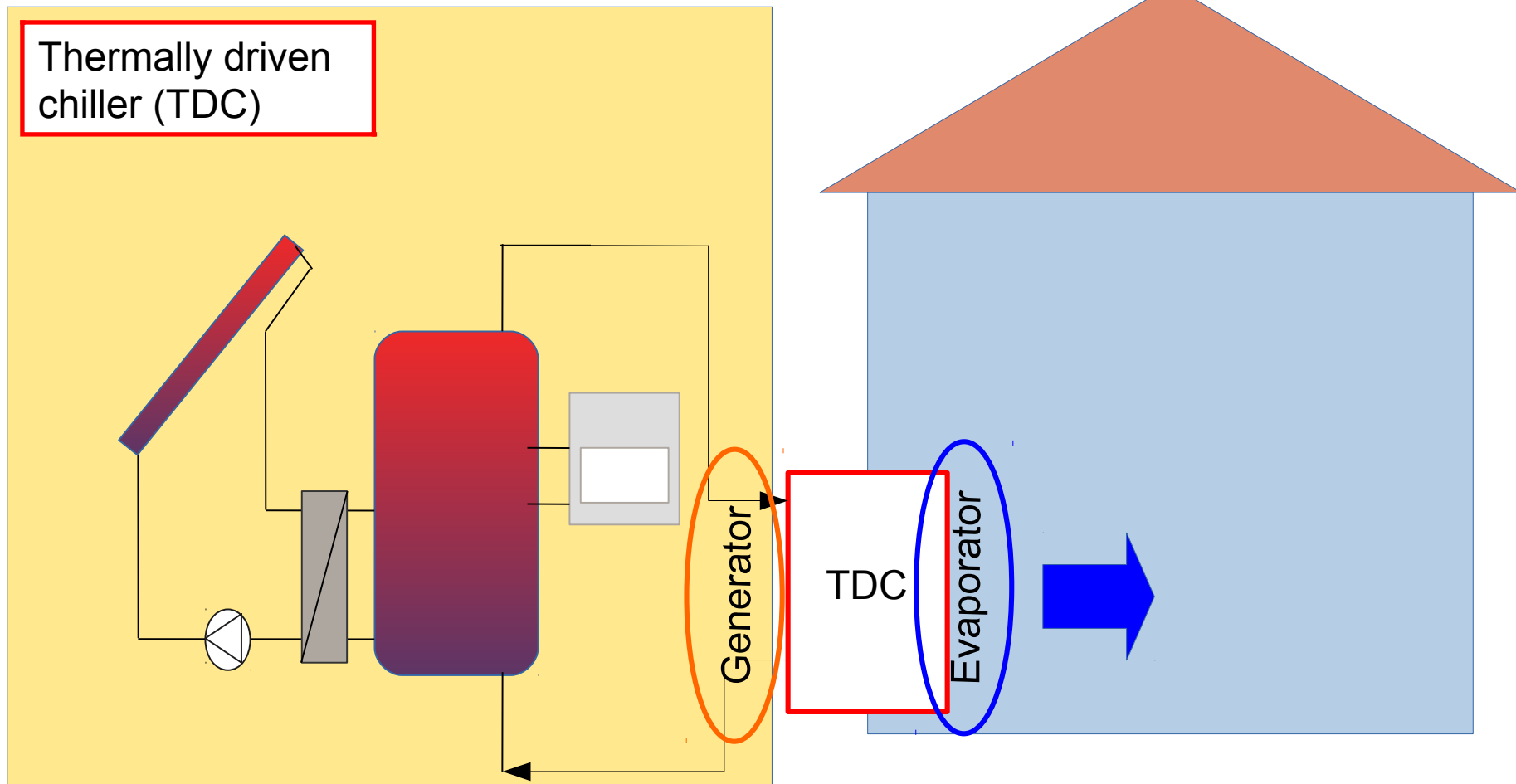
ADSORPTION



# Thermally driven compression chiller ...within the whole system



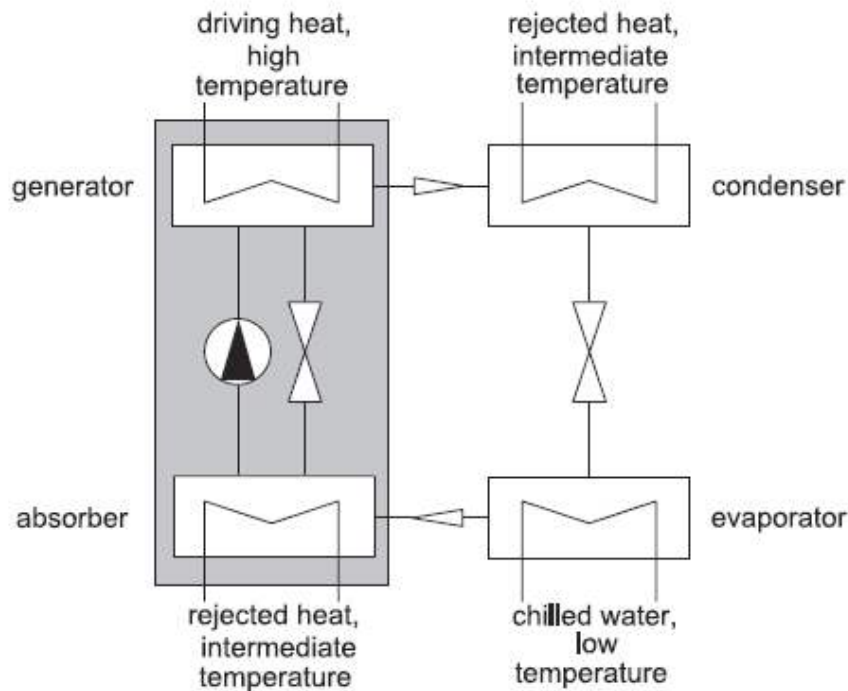
# Thermally driven compression chiller ...within the whole system



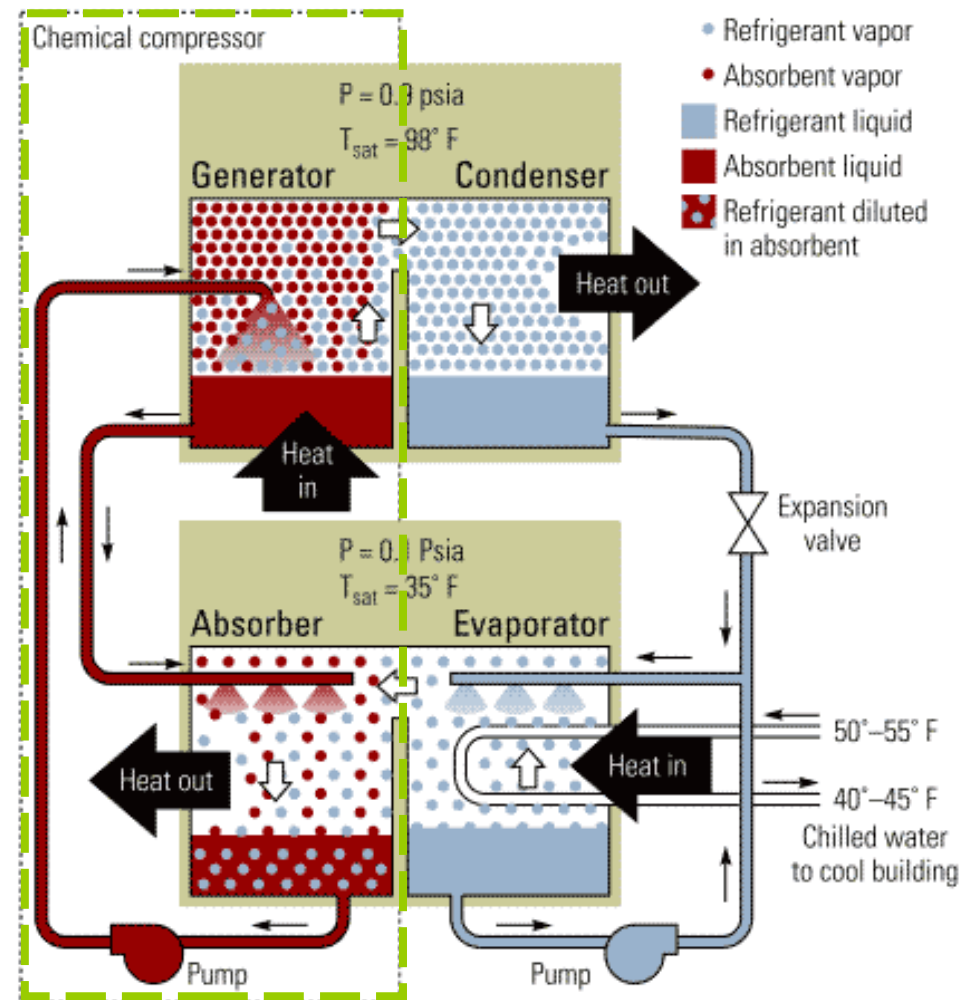
# Absorption chillers: principle

Refrigerant: Water

Absorbent: LiBr



Source: Henning, 2003



# Absorption chillers

**LiBr – Water (refrigerant): if  $T_{\text{chilled}}(T_{\text{evap}}) > 5^{\circ}\text{C}$**

- Water cooled
- Water freezes at  $0^{\circ}\text{C}$  -> lower limit for  $T_{\text{cool}}$ !!
- LiBr soluble in water if its concentration  $> 70\%$   
-> max.  $T_{\text{middle}}$  (absorber temperature)

**Ammonia (refrigerant) – Water : if  $T_{\text{chilled}}(T_{\text{evap}}) < 5^{\circ}\text{C}$**

- Water or air cooled

Electric power consumption (pumps) 1-5% of cooling power

$$T_{\text{middle}} = T_{\text{cond}} = 27 - 32^{\circ}\text{C}$$

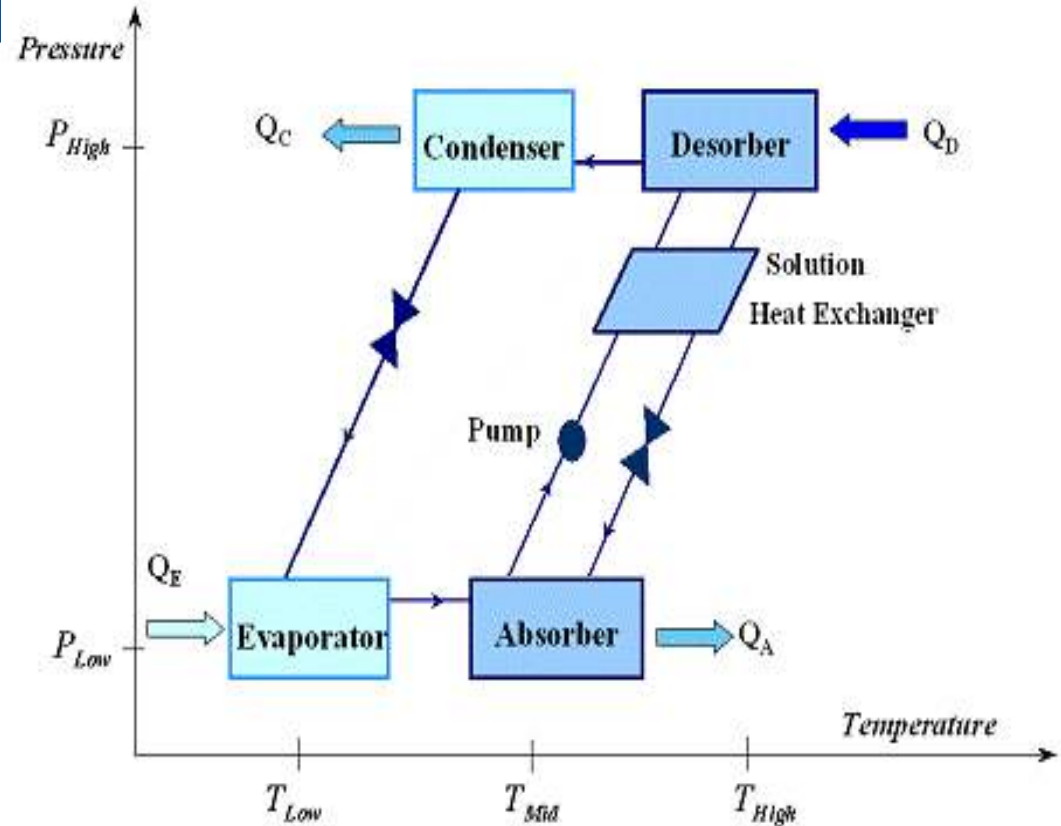
$$T_{\text{chilled}} = T_{\text{evap}} = 5 - 16^{\circ}\text{C}$$



# Absorption chillers

## Single-effect

- COP: 0.7-0.8
- $T_{\text{driving}} = 75\text{-}90^{\circ}\text{C}$



Source: APEP-UCI, 2017

# Absorption chillers

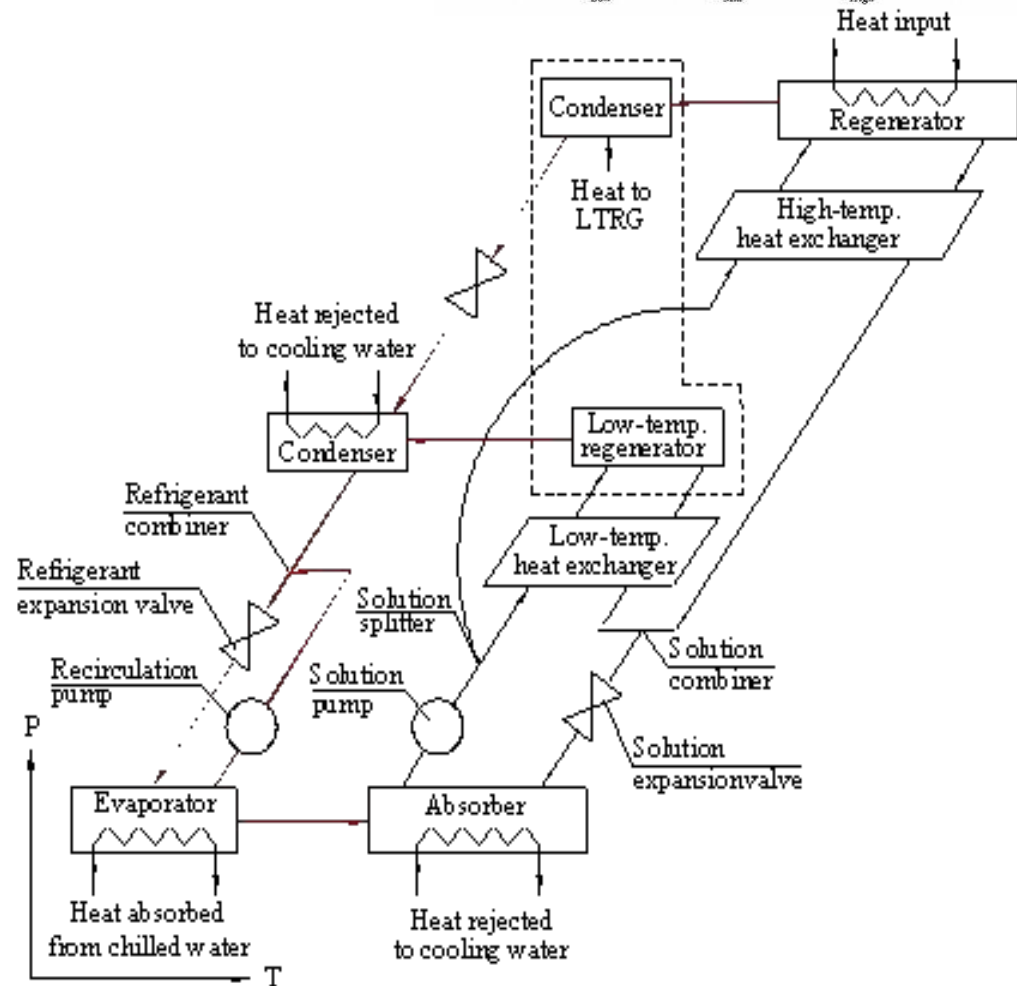
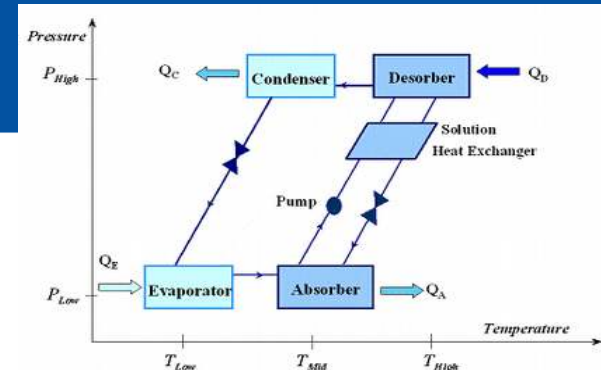
## Single-effect

COP: 0.7-0.8

$T_{\text{driving}} = 75-90^{\circ}\text{C}$

## Double-effect

- COP: around 1.1
- $T_{\text{driving}} = 140-160^{\circ}\text{C}$



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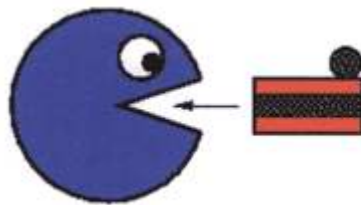
- Compression chillers
- TDCs:
  - Absorption chillers
  - Adsorption chillers
- Desiccant systems

# Adsorption chillers

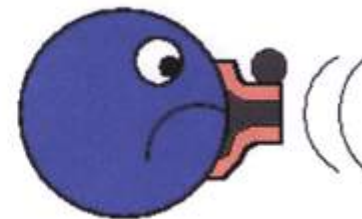
**Absorption = Molecules are taken up by the volume**

**Adsorption = Molecules are take up by the surface**

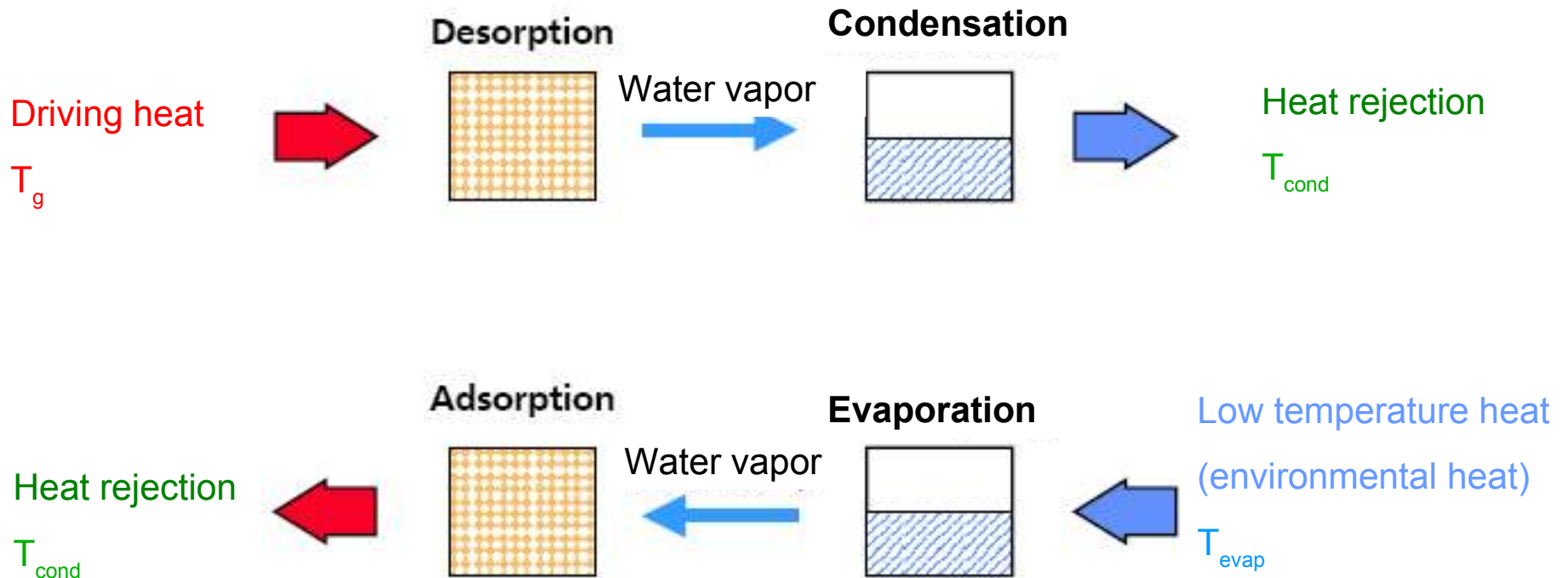
Absorption



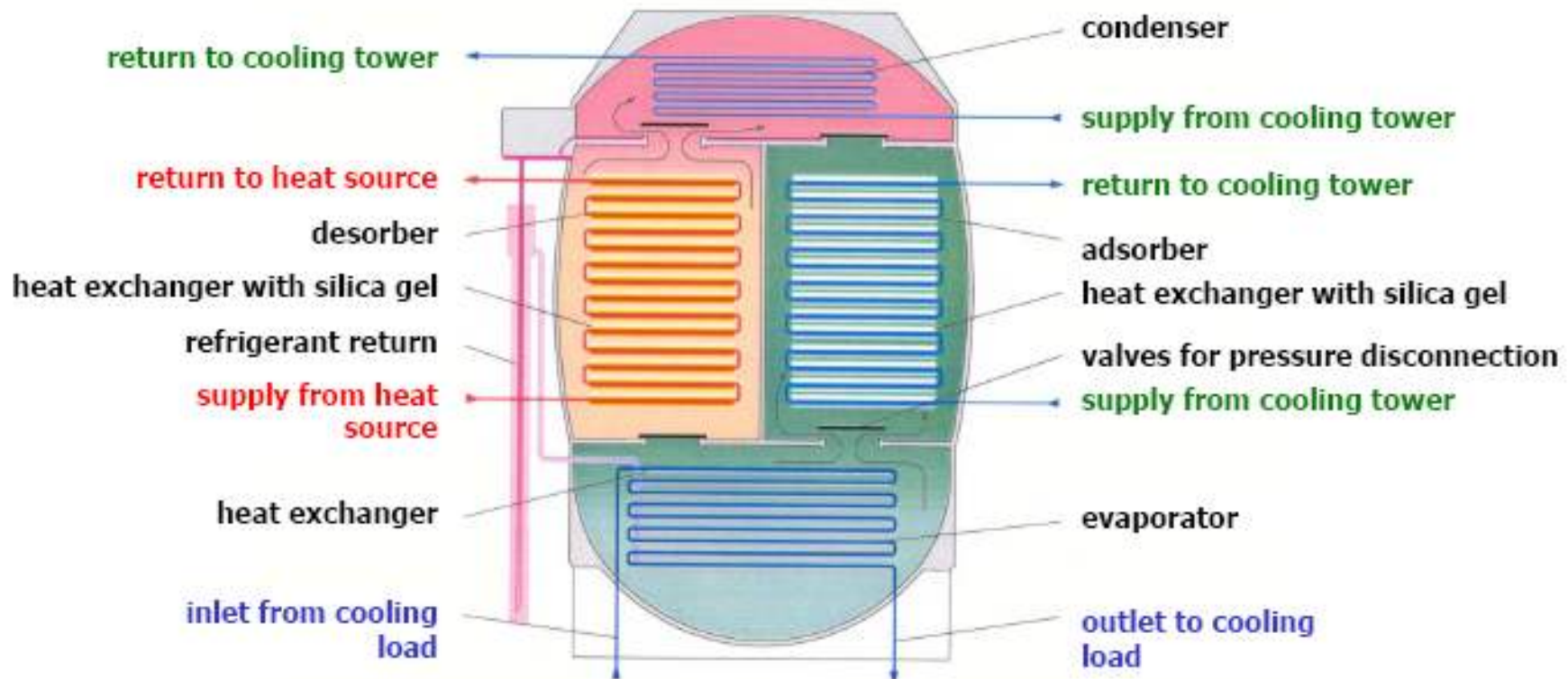
Adsorption



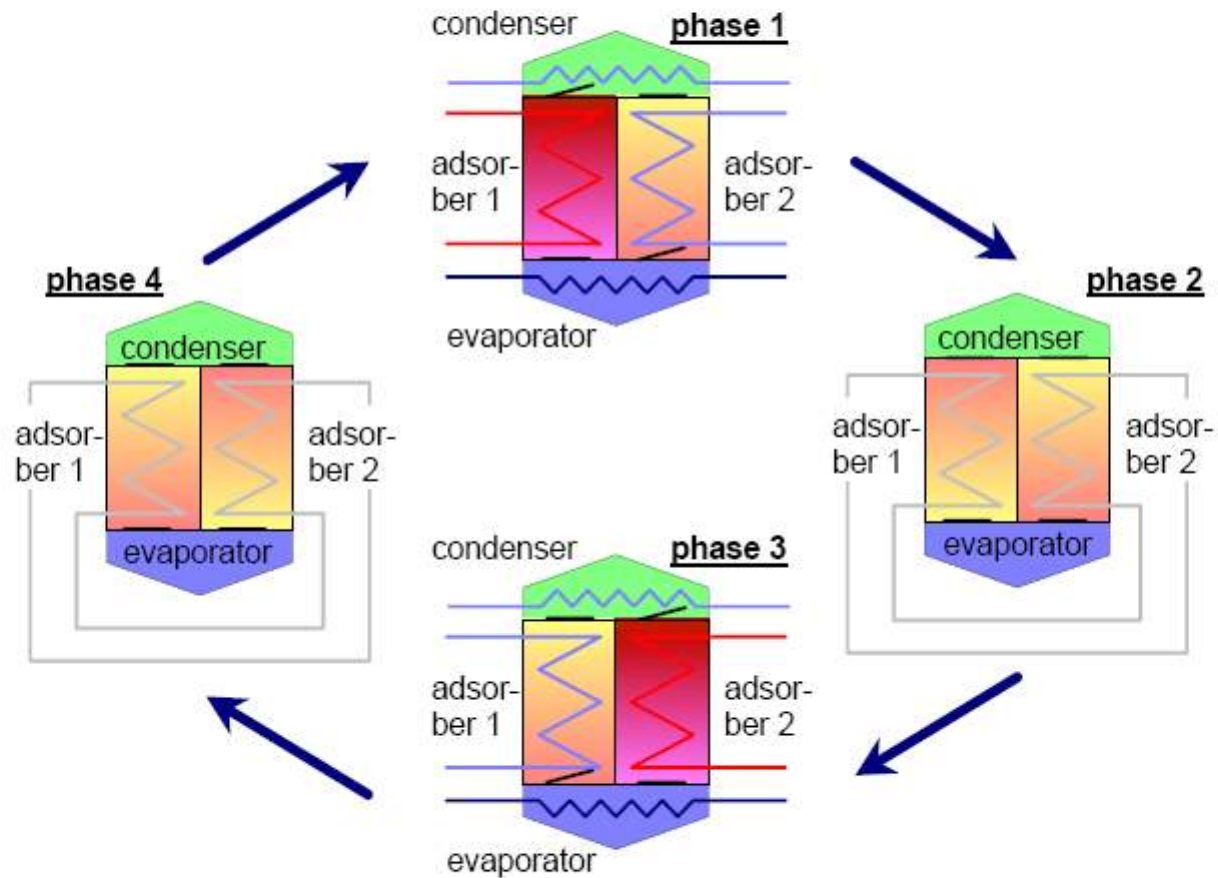
# Adsorption chillers



# Adsorption chillers



# Adsorption chillers



# Comparison: absorption and adsorption chillers

**Single effect absorption: >100kW (few <100kW)**

**water/LiBr or ammonia/water**

**COP ca. 0.7;  $T_{\text{drive}} = 75-110^{\circ}\text{C}$**

**Double effect absorption: no product <100kW)**

**mainly water/LiBr**

**COP ca. 1.1-1.3;  $T_{\text{drive}} = 140-160^{\circ}\text{C}$**

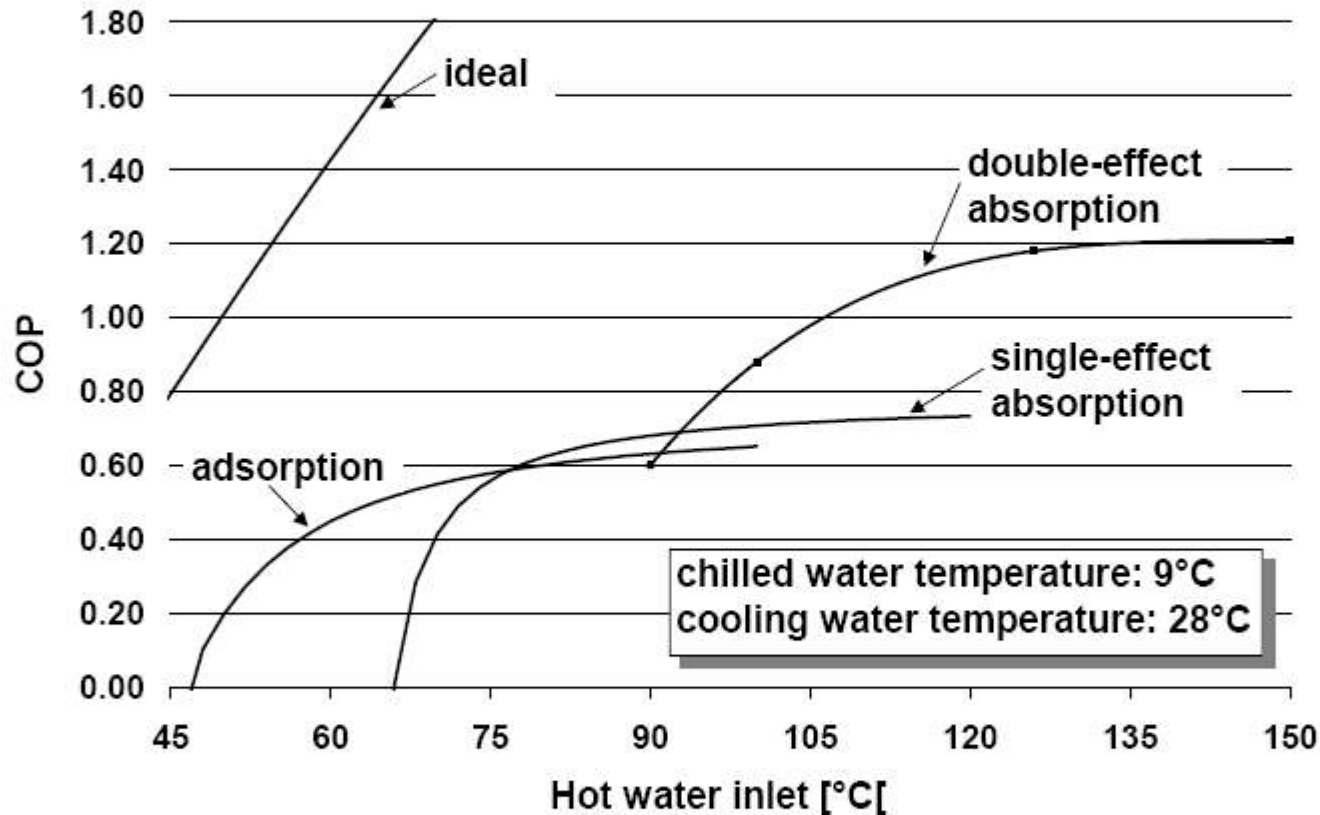
**Adsorption: few products (large and heavy)**

**water/silica gel or zeolite/water**

**COP ca. 0.6 - 0.7;  $T_{\text{drive}} = 65-95^{\circ}\text{C}$**



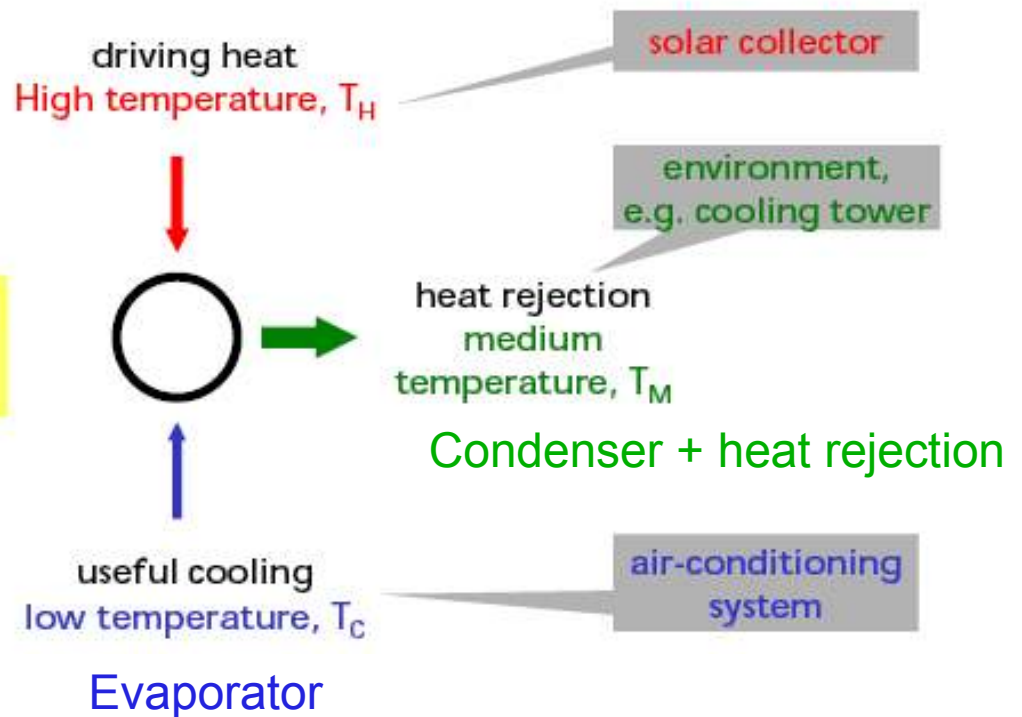
# Comparison: absorption and adsorption chillers



# Thermodynamic analysis

## Temperature levels

useful temperature lift  
 $\Delta T = T_M - T_C$



# Thermodynamic analysis

- Coefficient of performance COP

$$\text{COP} = \frac{\text{useful cooling}}{\text{driving heat}}$$

- Carnot efficiency factor

$$\xi_{\text{Carnot}} = \frac{\text{COP}_{\text{real}}}{\text{COP}_{\text{ideal}}}$$

- Reversible  $\text{COP}_{\text{ideal}}$

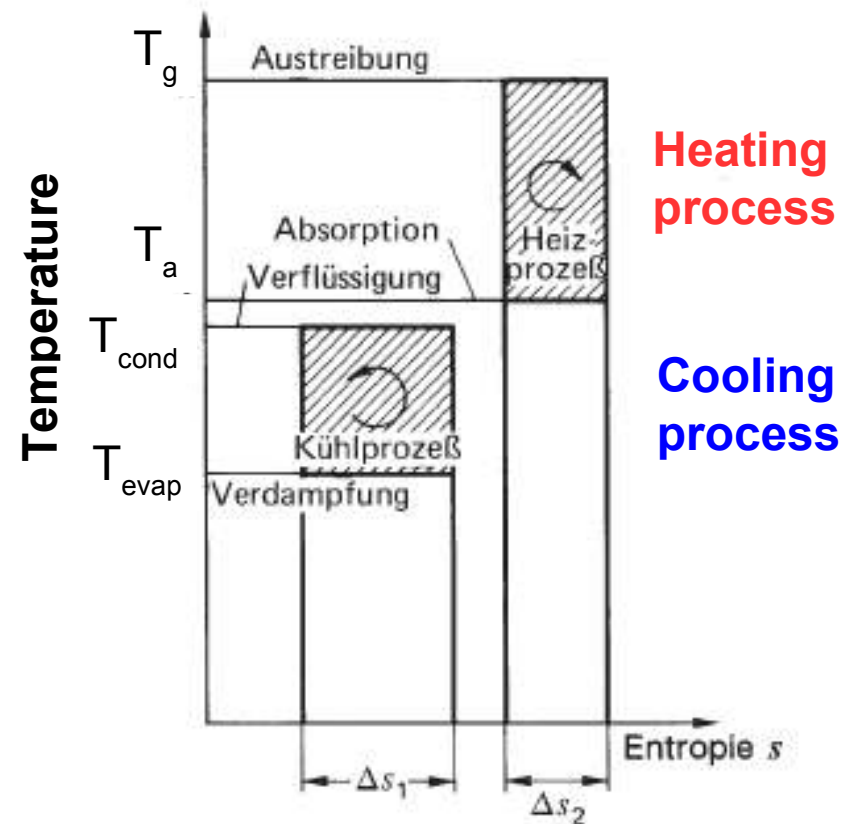
$$\text{COP}_{\text{ideal}} = \frac{T_{\text{C}}}{T_{\text{H}}} \cdot \frac{T_{\text{H}} - T_{\text{M}}}{T_{\text{M}} - T_{\text{C}}}$$

- Typical range of  $\xi_{\text{Carnot}}$  for real machines:

$$0.3 \leq \xi_{\text{Carnot}} \leq 0.4$$

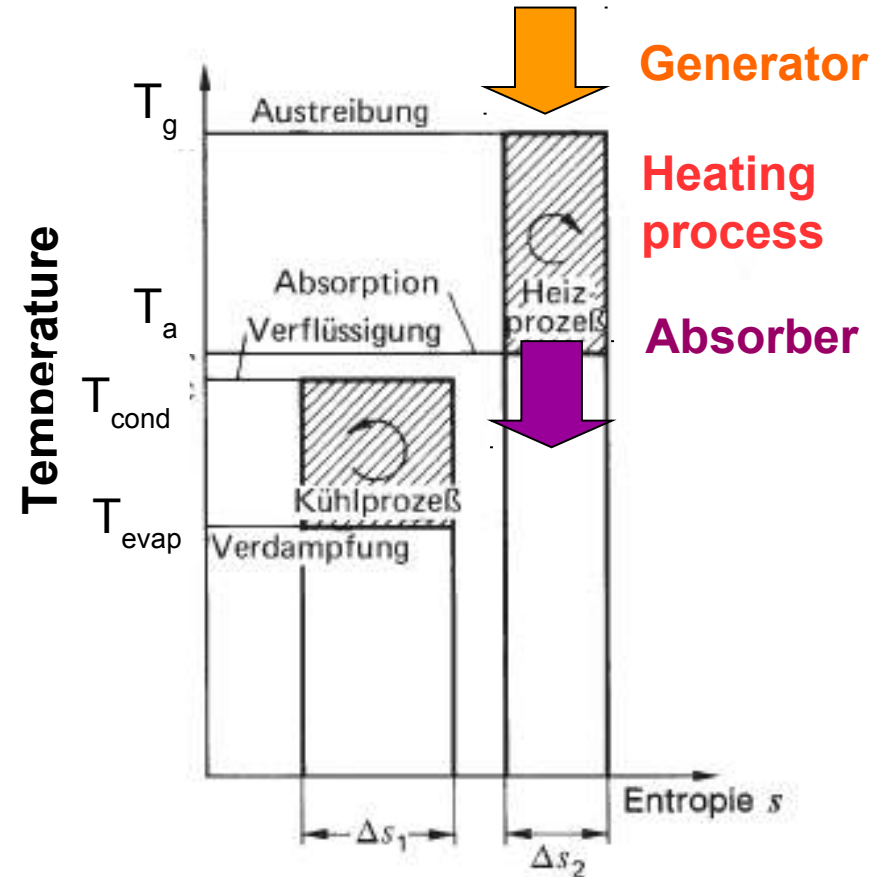
# Thermodynamic analysis

## Absorption chiller



# Thermodynamic analysis

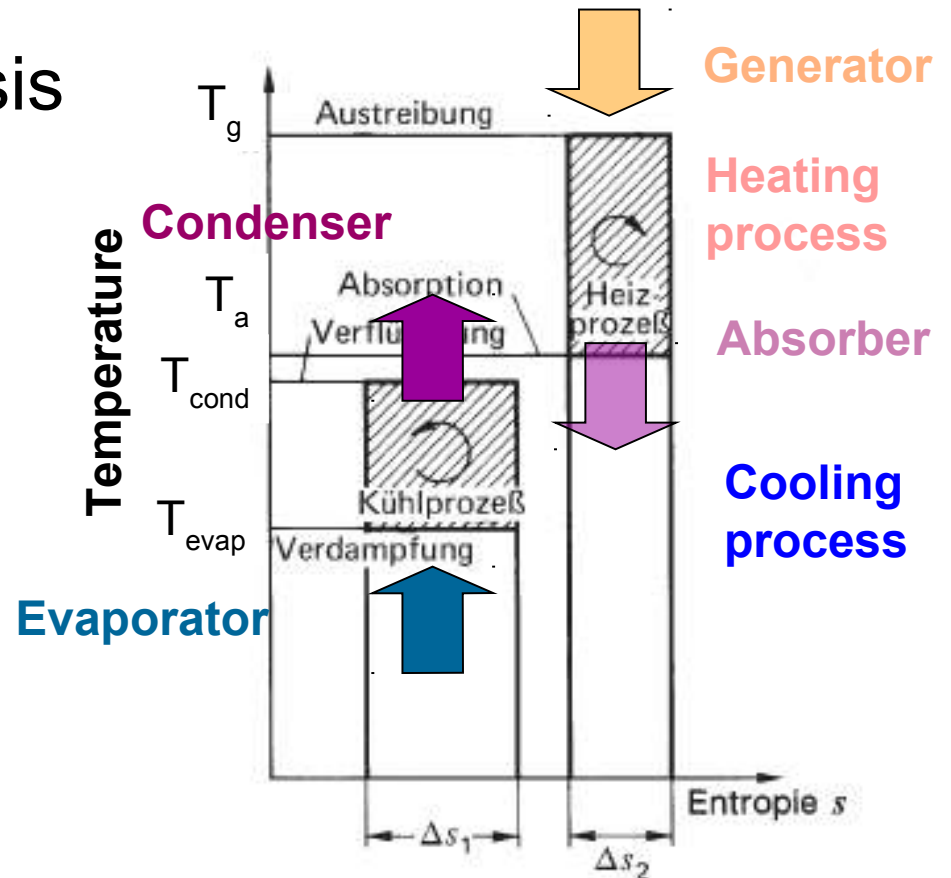
## Absorption chiller



$$COP_{cool} = \frac{Q_{evap}}{Q_g} = \frac{T_g - T_a}{T_g} \cdot \frac{T_{evap}}{T_{cond} - T_{evap}}$$

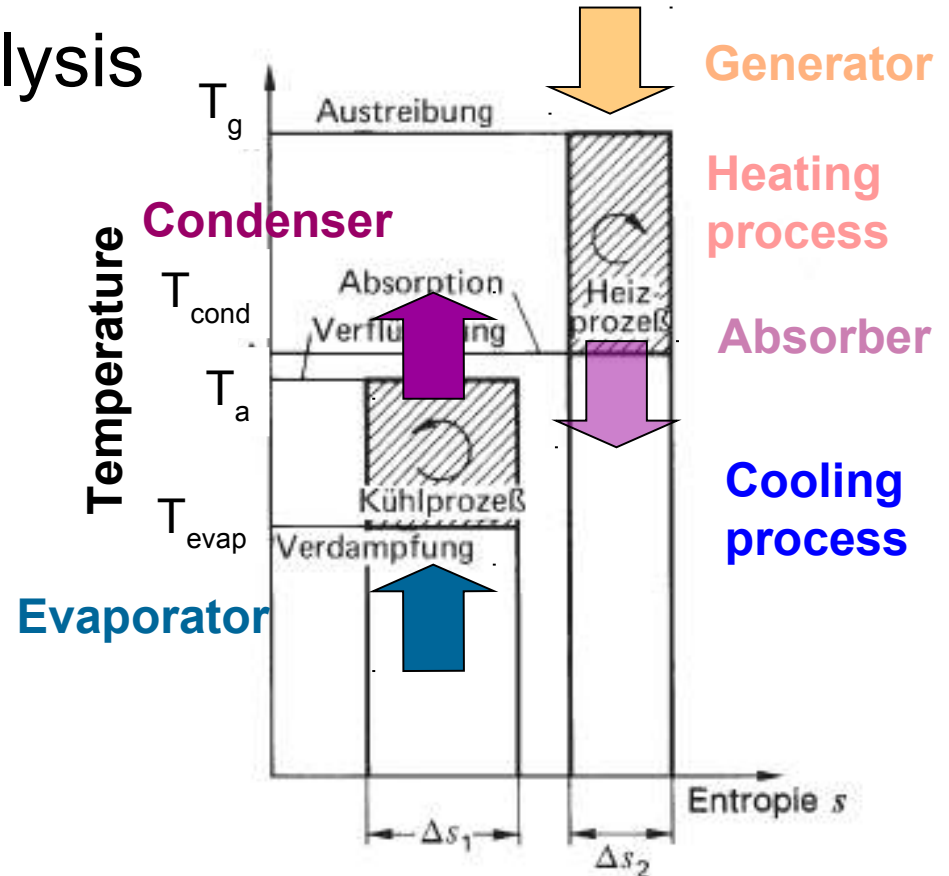
# Thermodynamic analysis

## Absorption chiller



# Thermodynamic analysis

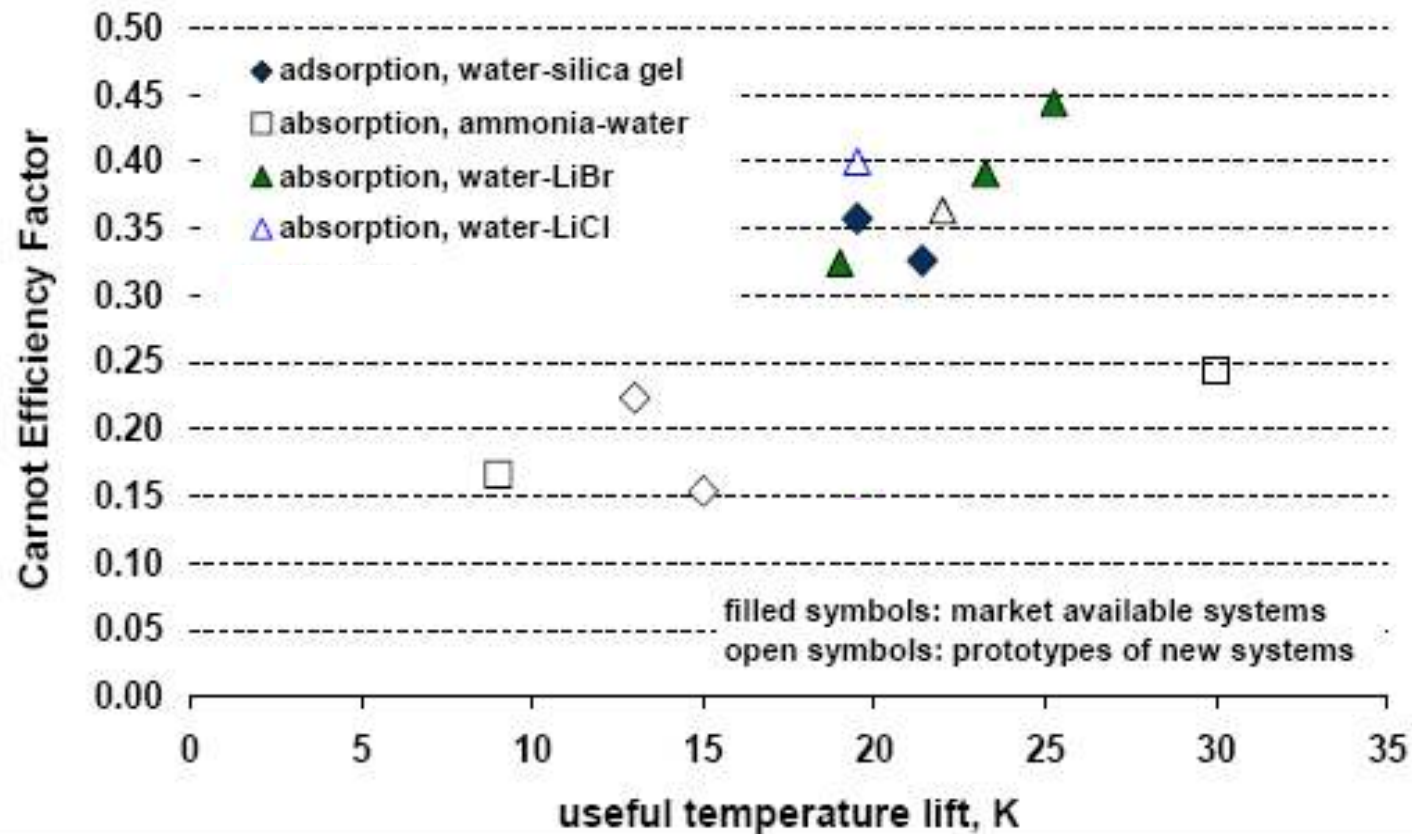
## Absorption chiller



$$COP_{cool} = \frac{Q_{evap}}{Q_g} = \frac{T_g - T_a}{T_g} \cdot \frac{T_{evap}}{T_{cond} - T_{evap}}$$

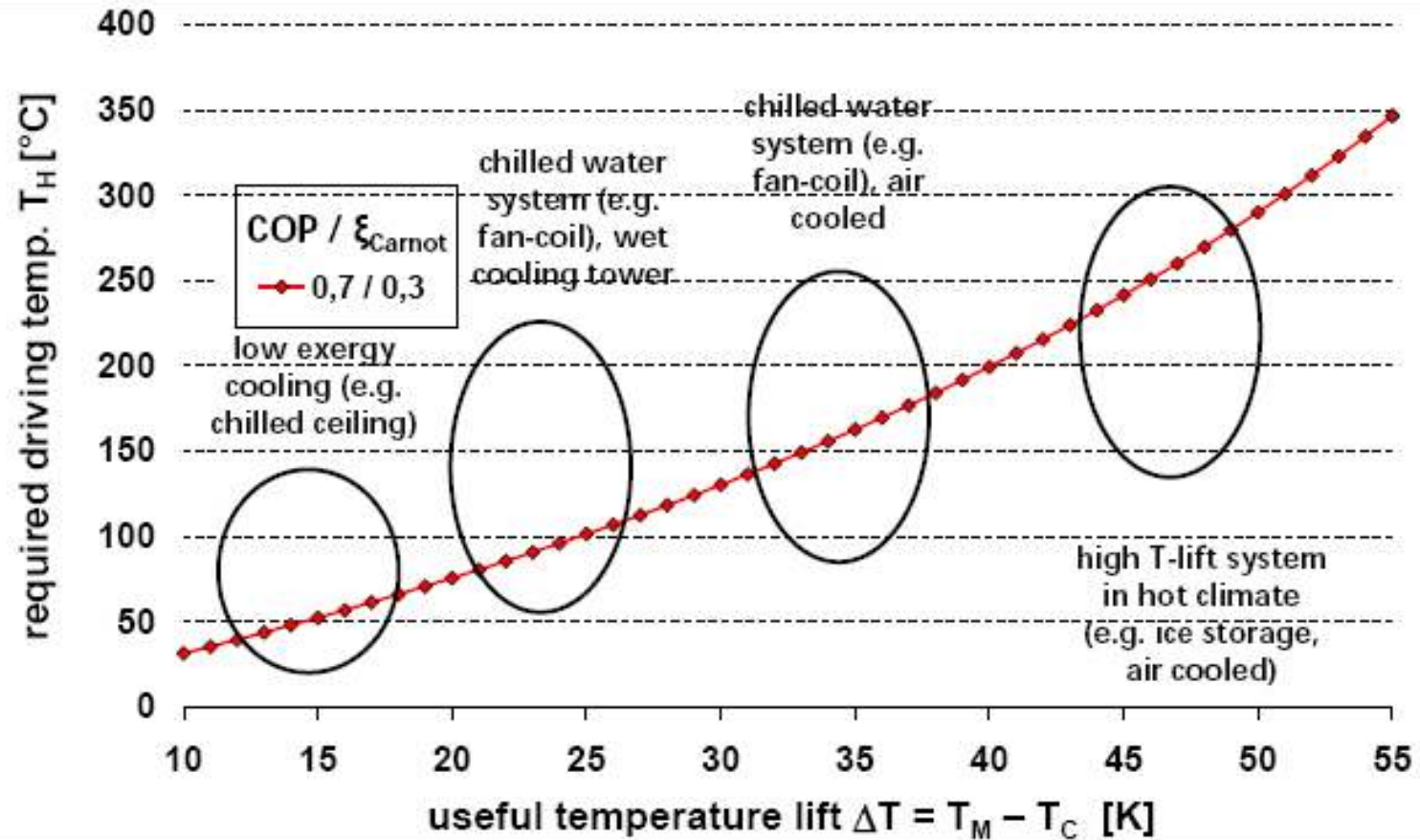
# Thermodynamic analysis

## Comparison of absorption and adsorption chillers

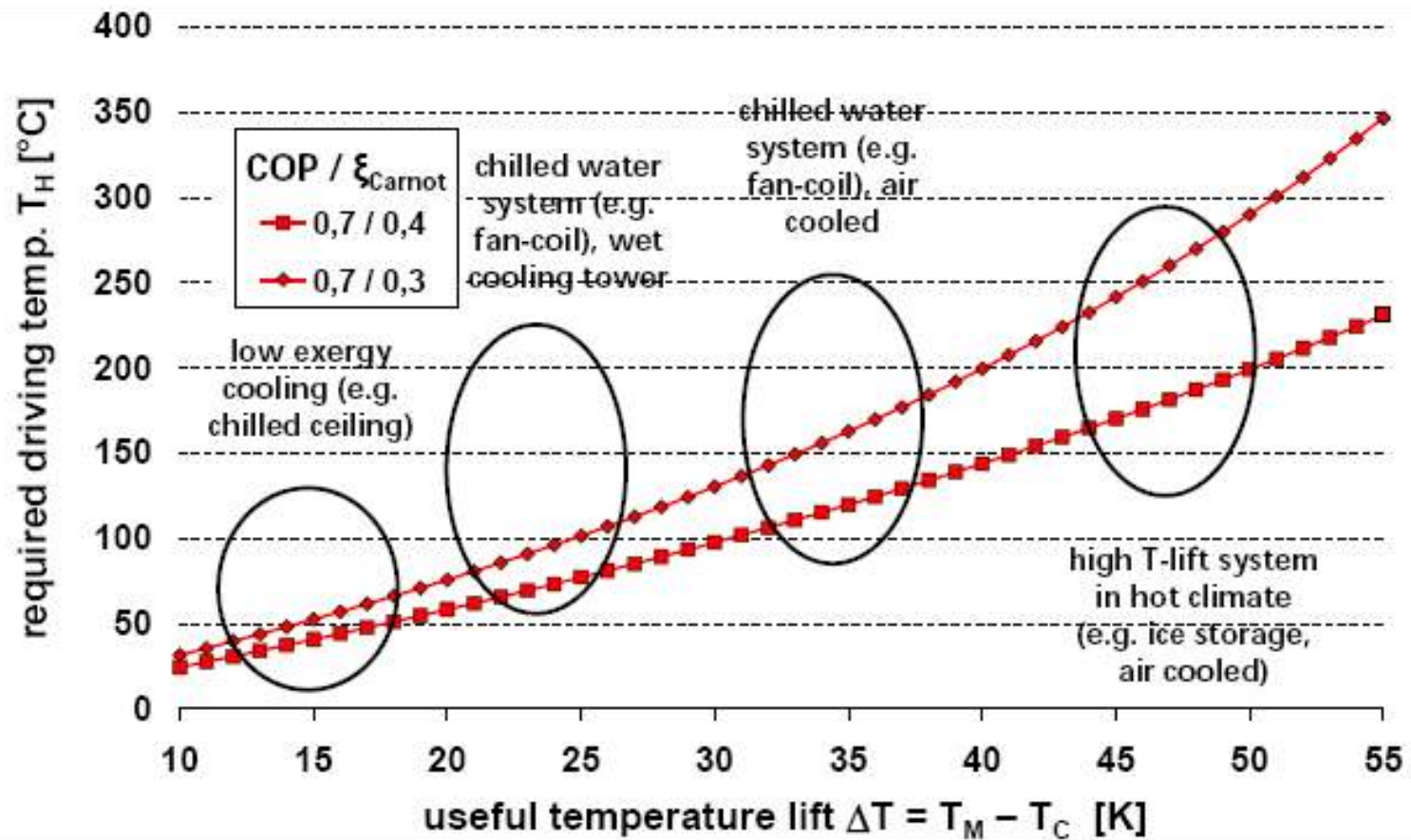




# Thermodynamic analysis

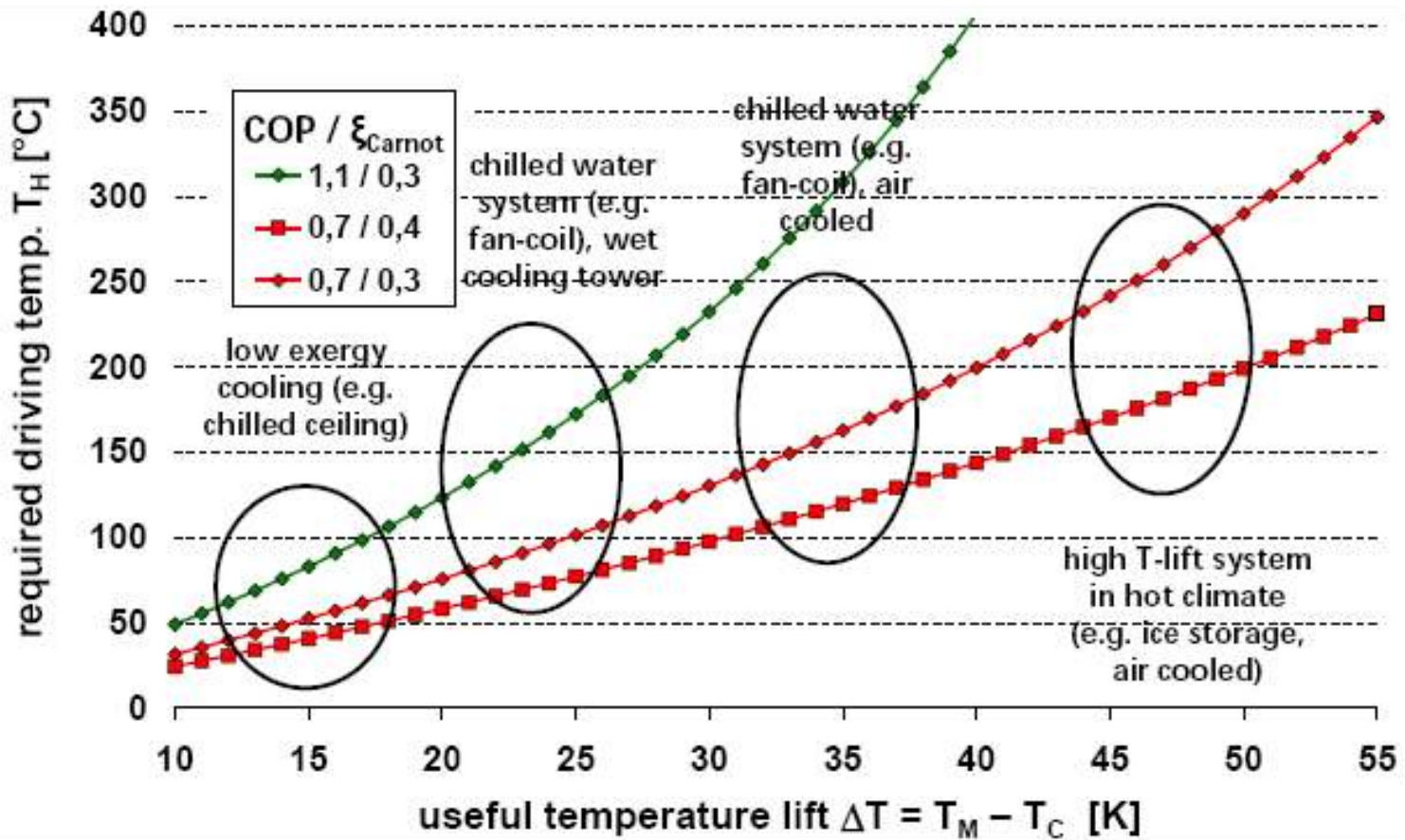


# Thermodynamic analysis



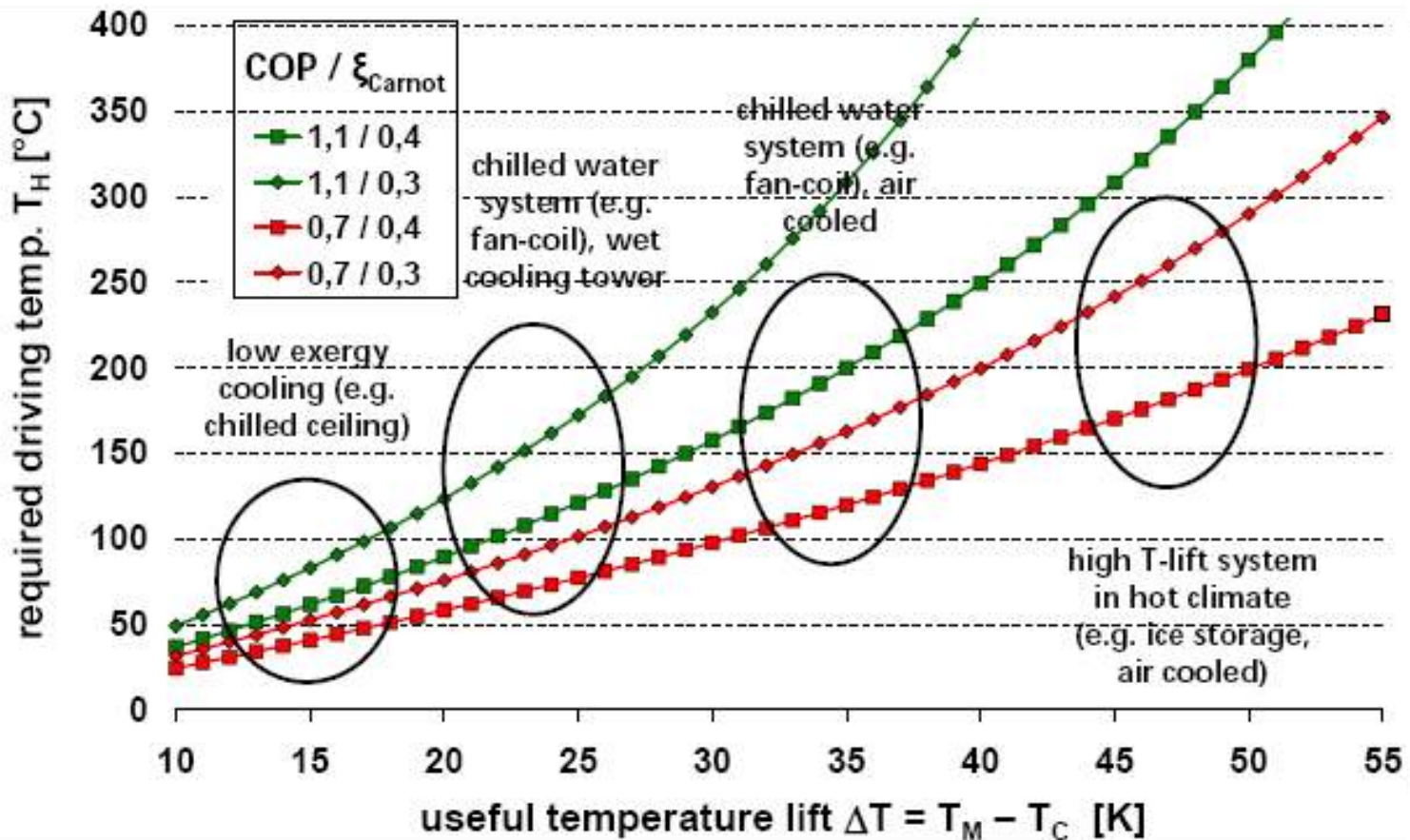
Source: Henning 2003

# Thermodynamic analysis



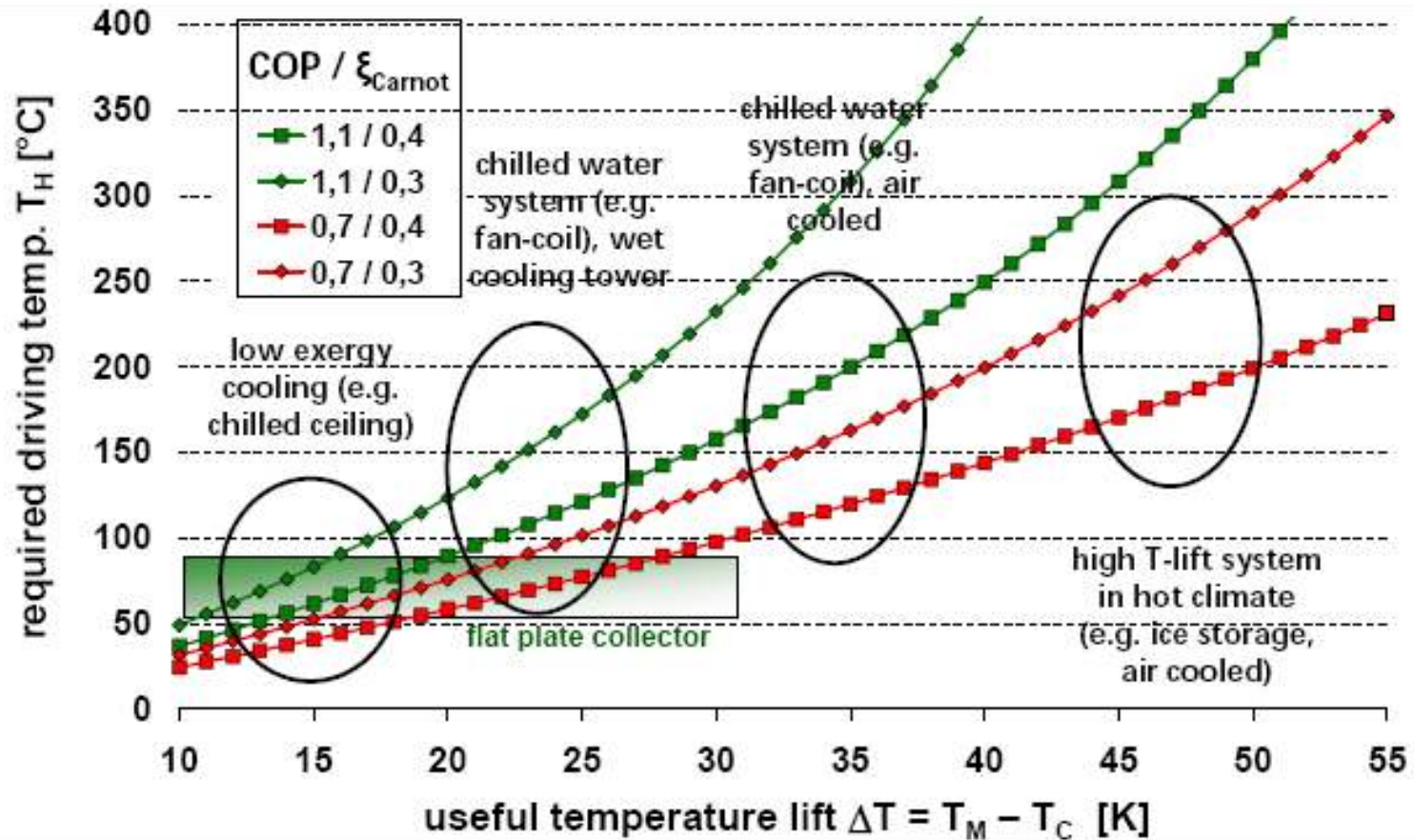
Source: Henning 2003

# Thermodynamic analysis

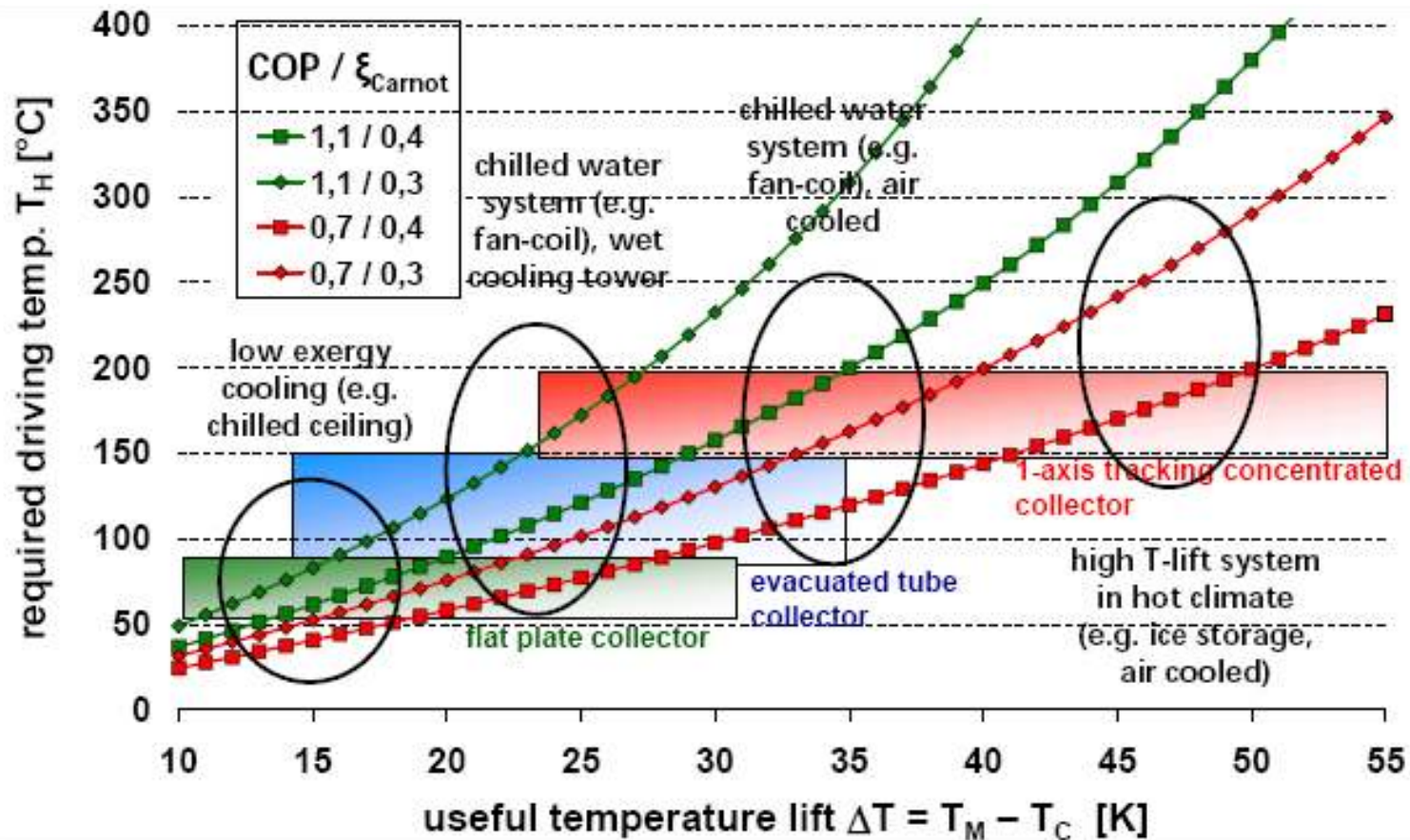




# Thermodynamic analysis



# Thermodynamic analysis



# Thermodynamic analysis

## Driving temperatures: solar collectors

SAC = solar air coll.

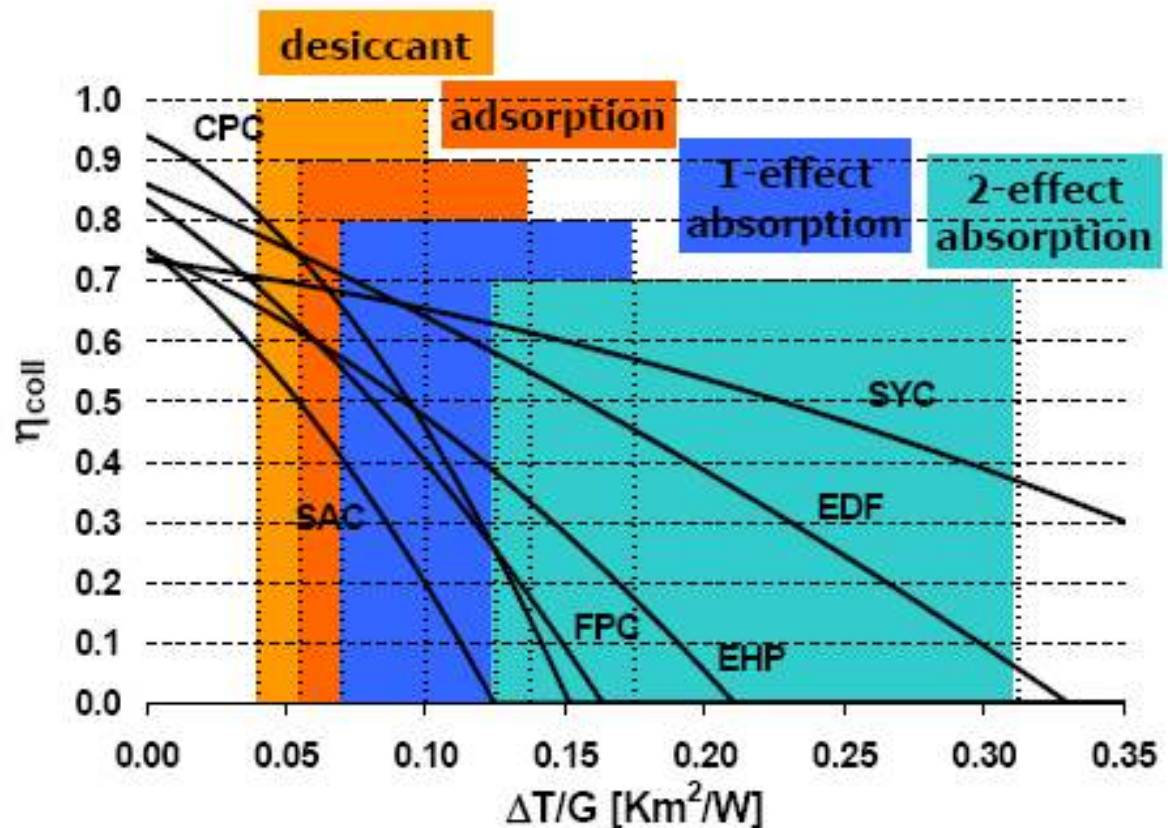
CPC = stationary  
CPC

FPC = selectively  
coated flat plate

EHP = evacuated  
heat-pipe

EDF = evacuated,  
direct flow

SYC = stationary  
concentrated,  
Sydney-type



# System performance

## Efficiency of cold generation

Example:

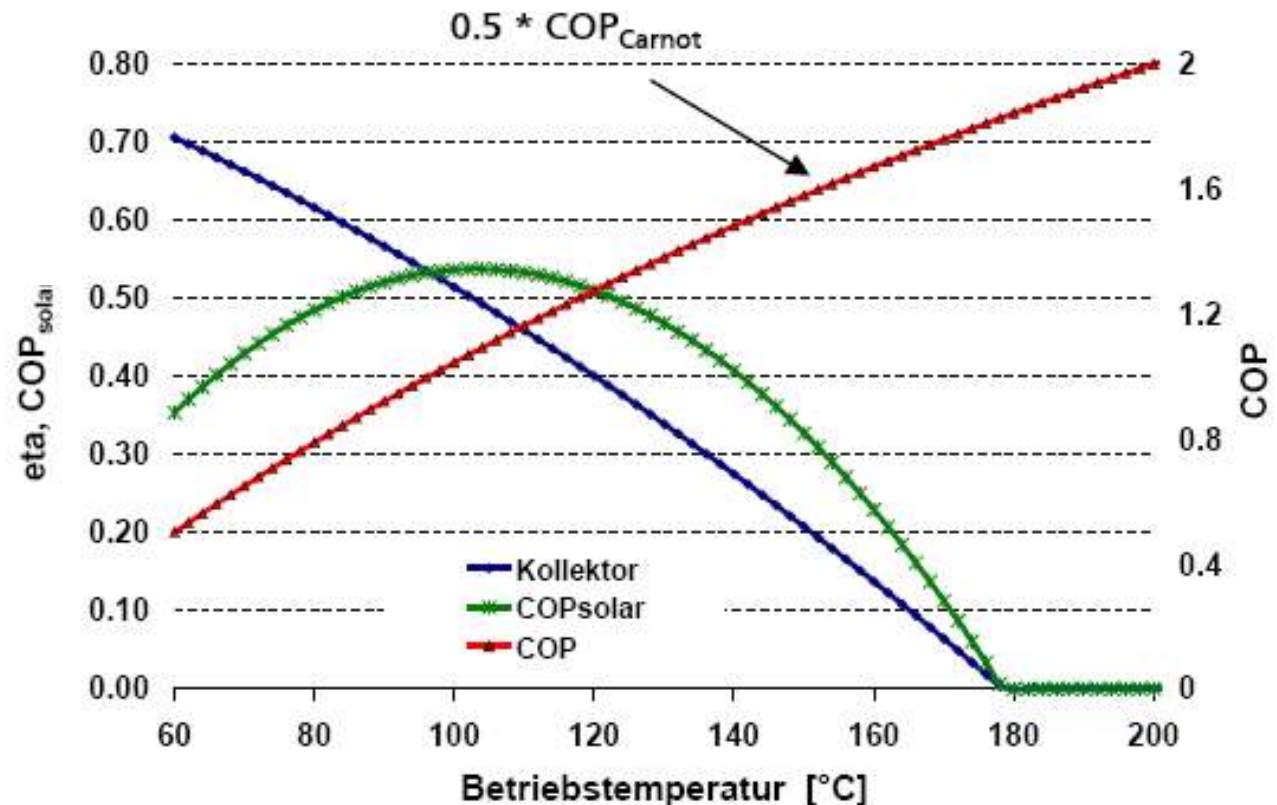
Flat plate collector

Radiation= 1000 W/m<sup>2</sup>

$$\text{COP}_{\text{sol}} =$$

$$\text{COP}_{\text{thermisch}} *$$

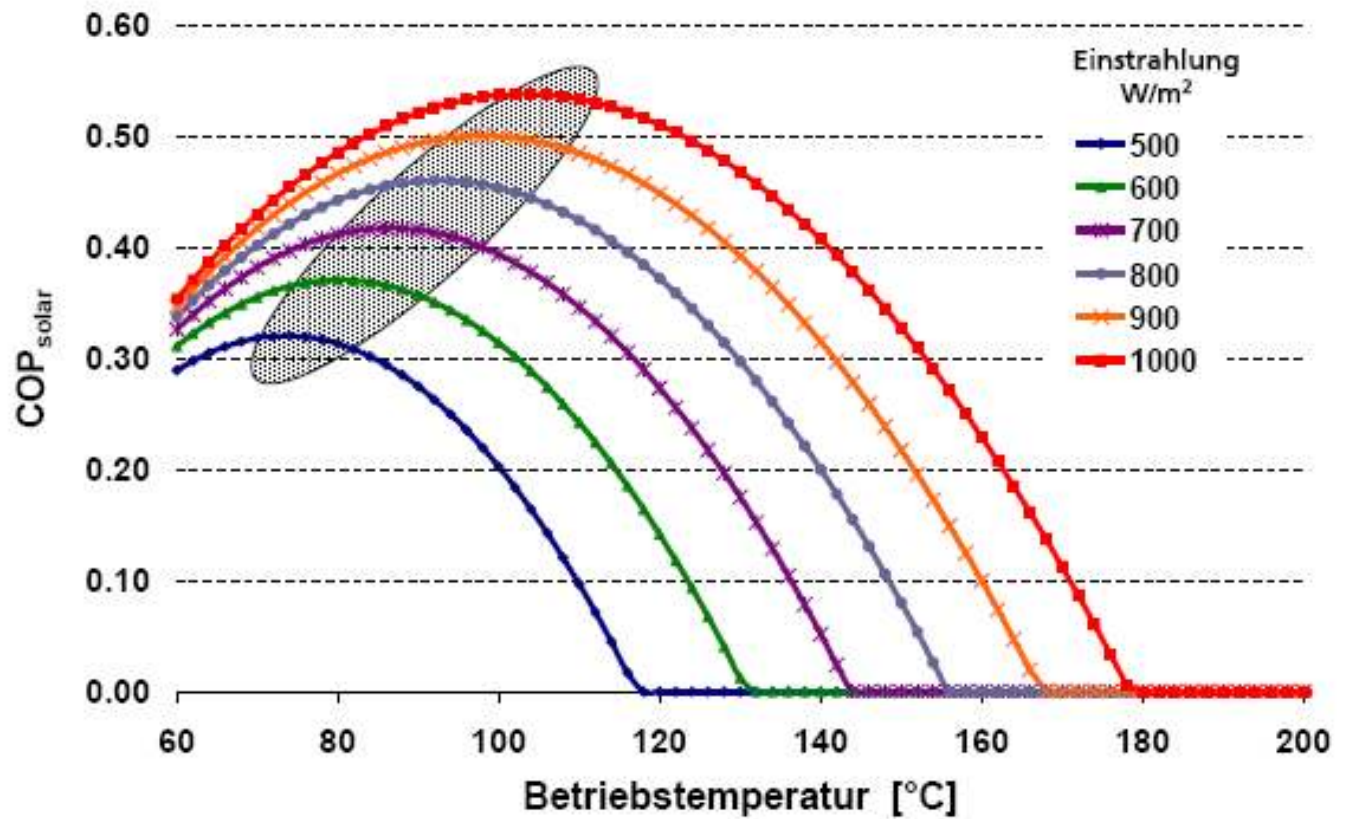
$$\eta_{\text{Kollektor}}$$





# System performance

## Efficiency of cold generation



Optimal driving temperature for solar-cooling system depends on the incident radiation strahlung ab

$$COP_{solar} = \eta_{coll} * COP_{TDC, carnot}$$

Source: Henning 2007

# System performance

## Primary energy balance

$$E_{PE} = Q_{bu} / \varepsilon_{fossil} + E_{elec} / \varepsilon_{elec}$$

$$E_{PE,save} = E_{PE,reference} - E_{PE,solar}$$

$$PE_{spec,conv} = \frac{1}{(\varepsilon_{elec} \cdot COP_{conv})}$$

$$PE_{spec,sol} = \frac{1}{\varepsilon_{fossil} \cdot COP_{thermal}} \cdot (1 - SF_{cool}) + PE_{spec,cooling\ tower}$$

$$Q_{use} = Q_{tot} - Q_{bu}$$

$$E_{PE,save,rel} = \frac{E_{PE,save}}{E_{PE,reference}}$$

$$E_{PE,save,spec} = \frac{E_{PE,save}}{A_{coll}}$$

$E_{spec,cooling\ tower}$

6-10 W/kW<sub>cooling,power</sub> (axial)

10-20 W/kW<sub>cooling,power</sub> (radial)

$$PE_{spec,cooling\ tower} = \frac{E_{spec,cooling\ tower}}{\varepsilon_{elec}} \cdot \left( 1 + \frac{1}{COP_{thermal}} \right)$$

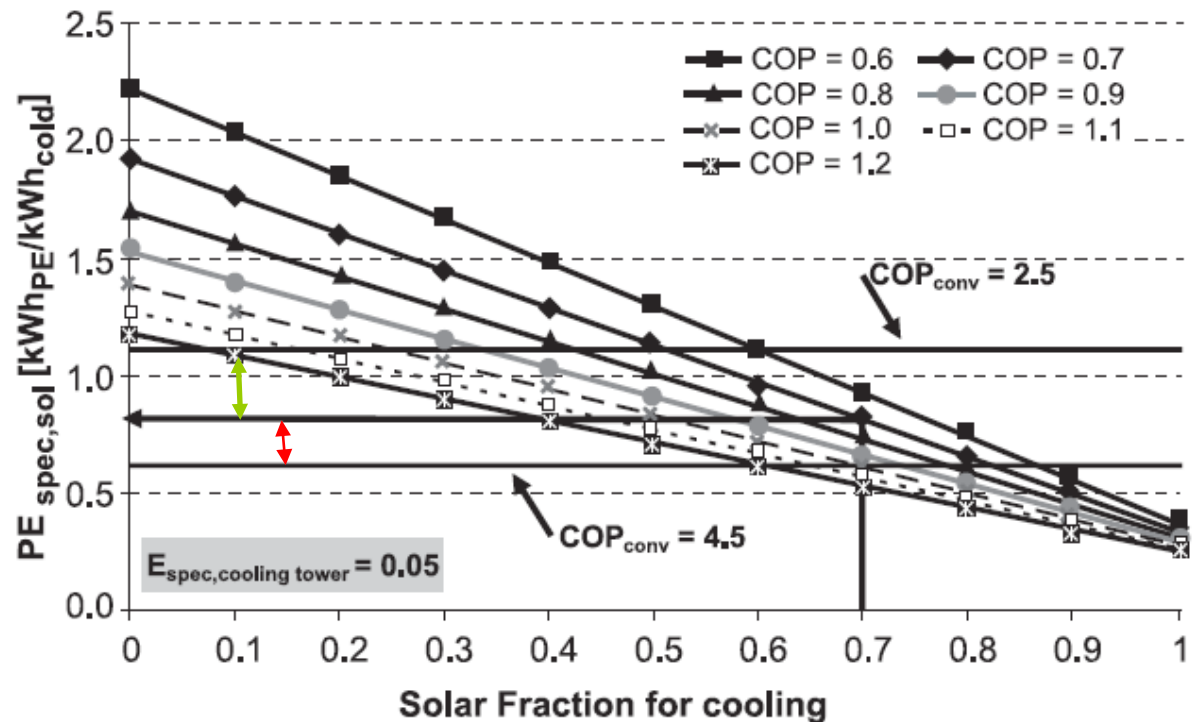
# System performance

## Primary energy balance

Example:

Cooling tower:  $0,05 \text{ kWh}_{\text{el}}/\text{kWh}_{\text{cool}}$ ;  $\text{COP} = 0,7$ ;  $F_p = 2,7$  ( $\varepsilon = 1/f_p$ )

Solar fraction: 0.7



27% lower

32% higher



# References

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