

PISCES: PSEUDO INCOMPRESSIBLE SPECTRAL-CARTESIAN ELEMENT SOLVER

JUSTIN M. BROWN

Department of Astronomy & Astrophysics
 University of California Santa Cruz
 201 Interdisciplinary Sciences Building
 Santa Cruz, CA 95064

PASCALE GARAUD

Applied Mathematics & Statistics
 Baskin School of Engineering
 1156 High Street
 Mail Stop SOE2
 Santa Cruz, CA 95064
Draft version May 30, 2014

ABSTRACT

Subject headings: Convection, Diffusion, Hydrodynamics, Instabilities, Stars: Evolution

1. MODEL

1.1. Pseudo-Incompressible Equations

We start from the fully compressible equations of hydrodynamics in an irrotational system without magnetic fields (e.g. Braginsky & Roberts (2006)),

$$\rho \frac{D}{Dt} \mathbf{u} = -\nabla p - \rho \nabla \Phi + \nabla \cdot \mathbf{\Pi}, \quad (1a)$$

$$\frac{D}{Dt} \rho = -\rho \nabla \cdot \mathbf{u}, \quad (1b)$$

$$\rho T \frac{D}{Dt} s = \nabla \mathbf{u} : \mathbf{\Pi} + \sum_i \mu_i \nabla \cdot \mathbf{C}_i - \nabla \cdot \mathbf{H}, \quad (1c)$$

$$\rho \frac{D}{Dt} \xi_i = -\nabla \cdot \mathbf{C}_i, \quad (1d)$$

where ρ is the mass density, \mathbf{u} is the velocity, Φ is the gravitational potential energy, s is the entropy, and ξ_i is the fractional abundance of the i th compositional component of the fluid.

Given an equation of state of the form $e(\rho, s, \xi_1, \xi_2, \dots)$, we can formally define

$$p \equiv \rho^2 \frac{\partial e}{\partial \rho}, \quad (2a)$$

$$T \equiv \frac{\partial e}{\partial s}, \quad (2b)$$

$$\mu_i \equiv \frac{\partial e}{\partial \xi_i}, \quad (2c)$$

which are the pressure, temperature, and chemical potentials, respectively. The remaining quantities, $\mathbf{\Pi}$, \mathbf{H} , and \mathbf{C}_i are the stress tensor, heat flux vector, and compositional flux vectors, respectively.

These equations as they are conserve momentum through Equation 1a, mass through Equation 1b, and energy as follows:

$$\rho \frac{D}{Dt} \left(\mathbf{u}^2/2 + e + \Phi \right) + \nabla \cdot \mathbf{u} = \nabla \cdot (\mathbf{\Pi} \cdot \mathbf{u} - \mathbf{H}), \quad (3)$$

which can be derived trivially using Equations 1a through 1d and the first law of thermodynamics:

$$de = Tds + \frac{p}{\rho^2} d\rho + \sum_i \mu_i d\xi_i. \quad (4)$$

Vasil et al. (2013) show that in the absence of any nonconservative effects, such as diffusion, and under the approximation that the fluid is constrained to be in pressure balance, the pseudo-incompressible equations take the following form:

$$\rho \frac{D}{Dt} \mathbf{u} = -\nabla p_0 - p_0^{\frac{c_p}{c_v}} \nabla \left(\frac{p_1}{p_0^{\frac{c_p}{c_v}}} \right) - \rho \nabla \Phi, \quad (5a)$$

$$\frac{D}{Dt} \rho = -\rho \nabla \cdot \mathbf{u}, \quad (5b)$$

$$\nabla \cdot p_0^{\frac{c_p}{c_v}} \mathbf{u} = 0, \quad (5c)$$

where p_0 is a nonuniform but static reference pressure, p_1 is a small pressure perturbation, and c_v and c_p are the specific heat capacities at constant volume and pressure, respectively. As an additional assumption to arrive at this expression, it must be assumed that $\frac{c_p}{c_v} = \frac{\rho}{p} \frac{\partial p}{\partial \rho} \Big|_s$ is constant, which is the case for an ideal gas. It should be noted that these equations do not take the same form as those from the original ones in Durran (1989), rather they are derived to conserve mass and energy.

Wood (private communication) has used these results to derive a set of equations with varying composition and allowing for diffusion while still conserving energy

and mass:

$$p_0(\mathbf{x}) = p(\rho, s, \xi_1, \xi_2, \dots), \quad (6a)$$

$$\rho \frac{D}{Dt} \mathbf{u} = -\nabla(p_0 + p_1) + \frac{p_1}{\rho} \left(\frac{\partial p}{\partial \rho} \right)^{-1} \nabla p_0 - \rho \nabla \Phi + \nabla \cdot \mathbf{\Pi}, \quad (6b)$$

$$\frac{D}{Dt} \rho = -\rho \nabla \cdot \mathbf{u}, \quad (6c)$$

$$\rho T \frac{D}{Dt} s = \nabla \mathbf{u} : \mathbf{\Pi} + \sum_i \mu_i \nabla \cdot \mathbf{C}_i - \nabla \cdot \mathbf{H}, \quad (6d)$$

$$\rho \frac{D}{Dt} \xi_i = -\nabla \cdot \mathbf{C}_i, \quad (6e)$$

where the quantities T and μ_i are still the “true” values of temperature and chemical potential, but due to the approximation of the equation of state by fixing the pressure, these may no longer be the derivatives of e . He has shown that to conserve energy and mass,

$$T = \frac{\partial e}{\partial s} + p_1 \frac{\partial \frac{\partial e}{\partial s} / \partial \rho}{\partial p / \partial \rho}, \quad (7a)$$

$$\mu_i = \frac{\partial e}{\partial \xi_i} + p_1 \frac{\partial \frac{\partial e}{\partial \xi_i} / \partial \rho}{\partial p / \partial \rho}. \quad (7b)$$

This necessitates the use of an equation of state.

1.2. Equation of State

The nature of the equations derived in 1.1 requires an equation of state to determine the true temperature, T , and chemical potential, μ . Unfortunately, unlike in the original Durran (1989) formulation of the pseudo-incompressible equations, we cannot assume an ideal gas as our system has multiple chemical components. There does exist a formulation, known as an ideal mixture or solution XX REFERENCE XX, which describes a gas with multiple ideal components. In particular, this system has the properties that n , the total number density, is related to the component number densities, n_i , and fractional abundance, ξ_i by

$$n_i = \xi_i n, \quad (8)$$

where we require the fractional abundances to sum to unity. From this, we can derive the relationship between the mass densities:

$$\frac{\rho_i}{m_i} = \xi_i \frac{\rho}{\bar{m}}, \quad (9)$$

where m_i is the mass of one particle in the corresponding component, and \bar{m} is the mean particle weight in the system, weighted by the fractional abundances.

Recall that the specific energy of an ideal gas can be expressed as

$$e(\rho, s) = \frac{c_V}{m} \left(\frac{\rho}{m} \phi e^{\frac{ms}{k}} \right)^{\frac{k}{c_V}}, \quad (10)$$

where k is the Boltzmann constant, c_V is the specific heat capacity at constant volume ($3k/2$ for a perfect monatomic gas), m is the particle mass, s is the specific entropy, ϕ is a constant but can vary for different gases. In an ideal mixture, we can add the specific energies as

follows:

$$\bar{m}e(\rho, s_1, s_2, \dots, \xi_1, \xi_2, \dots) = \sum_i m_i \xi_i e_i(\rho, s_i, \xi_i), \quad (11)$$

$$= \sum_i c_V \left(\frac{\rho \xi_i}{m_i} \phi_i e^{\frac{m_i s_i}{k}} \right)^{\frac{k}{c_V}}, \quad (12)$$

where subscripted quantities are specific to gas components. Given that we have evolution equations for the density, fractional abundances, and total entropy, we'd like to have our equation of state as a function of only those quantities. For an ideal mixture, we can relate the specific entropies as follows:

$$\bar{m}s = \sum_i m_i \xi_i s_i - k \sum_i \xi_i \ln \xi_i. \quad (13)$$

The last summation is known as the entropy of mixing and comes from the increased number of possible states due to the introduction of non-identical particles.

This unfortunately is insufficient to express the internal energy solely in terms of the global entropy; we must make an additional approximation. We choose to assume that the temperature of the individual components, $T_i \equiv \partial e_i / \partial s_i$, are the same. While this assumption does not usually hold in systems with few collisions (e.g. the interstellar medium), it is typically a good approximation in gases with frequent collisions.

$$T_i = \frac{\partial e_i}{\partial s_i}, \quad (14)$$

$$= \left(\frac{\rho \xi_i \phi_i}{\bar{m}} e^{\frac{m_i s_i}{k}} \right)^{\frac{k}{c_V}}, \quad (15)$$

so for all the T_i to be equal,

$$\left(\xi_i \phi_i e^{\frac{m_i s_i}{k}} \right) = \left(\xi_j \phi_j e^{\frac{m_j s_j}{k}} \right). \quad (16)$$

In a two-component gas, we can use this to relate the entropies by using Equation 13:

$$e^{\frac{m_1 s_1}{k}} = \left(\frac{\xi_2 \phi_2}{\xi_1 \phi_1} \right)^{\xi_2} e^{\frac{\bar{m}s}{k} + \xi_1 \ln \xi_1 + \xi_2 \ln \xi_2}, \quad (17)$$

$$e^{\frac{m_2 s_2}{k}} = \left(\frac{\xi_1 \phi_1}{\xi_2 \phi_2} \right)^{\xi_1} e^{\frac{\bar{m}s}{k} + \xi_1 \ln \xi_1 + \xi_2 \ln \xi_2}. \quad (18)$$

We can thus express the specific internal energies as

$$e_1(\rho, s, \xi_1, \xi_2) = c_V \left(\frac{\rho \xi_1 \phi_1}{m_1} \left[\frac{\xi_2 \phi_2}{\xi_1 \phi_1} \right]^{\xi_2} e^{\frac{\bar{m}s}{k} + \xi_1 \ln \xi_1 + \xi_2 \ln \xi_2} \right)^{\frac{k}{c_V}}, \quad (19)$$

$$e_2(\rho, s, \xi_1, \xi_2) = c_V \left(\frac{\rho \xi_2 \phi_2}{m_2} \left[\frac{\xi_1 \phi_1}{\xi_2 \phi_2} \right]^{\xi_1} e^{\frac{\bar{m}s}{k} + \xi_1 \ln \xi_1 + \xi_2 \ln \xi_2} \right)^{\frac{k}{c_V}}, \quad (20)$$

$$\bar{m}e(\rho, s, \xi_1) = \sum_i m_i \xi_i e_i(\rho, s, \xi_1, 1 - \xi_1). \quad (21)$$

It can be shown nontrivially that the derived pressure from this formulation, $p \equiv \rho^2 \partial e / \partial \rho$, is

$$p = \frac{k\rho T}{\bar{m}}, \quad (22)$$

where $T \equiv \partial e / \partial s$, which is what one would expect naïvely of an ideal gas with multiple components.

1.3. Perfect Gas

Unfortunately, the form of Equation 6d is exceedingly difficult to work with in a spectral sense. In the assumption of a perfect gas, i.e. $de = c_V dT$, we can produce a more desirable system from Equations 4, 6d, and 6e:

$$\frac{D}{Dt} e = \frac{\partial e}{\partial s} \frac{D}{Dt} s + \frac{p}{\rho^2} \frac{D}{Dt} \rho + \sum_i \frac{\partial e}{\partial \xi_i} \frac{D}{Dt} \xi_i = c_V \frac{D}{Dt} T, \quad (23)$$

$$c_V \rho \frac{D}{Dt} T = \frac{1}{T} \frac{\partial e}{\partial s} \left(\nabla \mathbf{u} : \mathbf{\Pi} + \sum_i \mu_i \nabla \cdot \mathbf{C}_i - \nabla \cdot \mathbf{H} \right) + p \nabla \cdot \mathbf{u} - \sum_i \frac{\partial e}{\partial \xi_i} \nabla \cdot \mathbf{C}_i. \quad (24)$$

At first glance, it doesn't appear that we've made much progress; however, we note that we can expand $\frac{1}{T} \frac{\partial e}{\partial s}$ into

$$\frac{1}{T} \frac{\partial e}{\partial s} = \frac{1}{1 + \frac{p_1}{T} \frac{\partial \frac{\partial e}{\partial s} / \partial \rho}{\partial p / \partial \rho}} = 1 - \frac{p_1}{T} \frac{\partial \frac{\partial e}{\partial s} / \partial \rho}{\partial p / \partial \rho} + O(p_1^2), \quad (25)$$

which is a fine approximation since p_1 must be a small quantity for the pseudo-incompressible approximation to work at all. A similar relation can be derived for μ_i . Using this, we can look at the temperature evolution equation up to first order in p_1 :

$$c_V \rho \frac{D}{Dt} T = \nabla \mathbf{u} : \mathbf{\Pi} - \nabla \cdot \mathbf{H} - p \nabla \cdot \mathbf{u} - \frac{p_1}{T} \frac{\partial \frac{\partial e}{\partial s} / \partial \rho}{\partial p / \partial \rho} \left(\nabla \mathbf{u} : \mathbf{\Pi} + \sum_i \frac{\partial e}{\partial \xi_i} \nabla \cdot \mathbf{C}_i - \nabla \cdot \mathbf{H} \right) + \sum_i \frac{p_1}{\mu_i} \frac{\partial \frac{\partial e}{\partial \xi_i} / \partial \rho}{\partial p / \partial \rho} \nabla \cdot \mathbf{C}_i + O(p_1^2). \quad (26)$$

In this formulation, the strongest diffusive term is now a simple second derivative, which is much more conducive to a spectral solution. All terms of order p_1 must be solved through nonlinear means.

ACKNOWLEDGEMENTS

REFERENCES

- Braginsky, S. I. & Roberts, P. H. 2006, 37
Durrant, D. R. 1989, *Journal of the Atmospheric Sciences*, 46, 1453
Vasil, G. M., Lecoanet, D., Brown, B. P., Wood, T. S., & Zweibel, E. G. 2013, 23