

porousIcoFoam - Documentation

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Abstract

Documentation for porousIcoFoam, a transient, incompressible OpenFOAM solver for the laminar flow of Newtonian fluids including regions of clear fluid and porous media including:

- Details of the Darcy Brinkman Forchheimer governing equations.
- Details of the solution algorithm and finite volume discretization relevant to the implementation of porousIcoFoam.
- Calculation of the forces and moments acting on porous bodies.

Chapter 1

The Darcy Brinkman Forchheimer governing equations

The unsteady, incompressible Darcy Brinkman Forchheimer (DBF) continuity and momentum equations are given by:

$$\nabla \cdot \mathbf{u} = 0 \quad (1.1)$$

$$\frac{1}{\phi} \frac{\partial \mathbf{u}}{\partial t} + \frac{1}{\phi^2} (\mathbf{u} \cdot \nabla \mathbf{u}) = -\nabla p^* + \frac{\nu}{\phi} \nabla^2 \mathbf{u} - \frac{\nu}{K} \mathbf{u} - \frac{c_F}{\sqrt{K}} |\mathbf{u}| \mathbf{u} \quad (1.2)$$

where $\phi = V_f/V$ is porosity, a dimensionless scalar field defined as the ratio of fluid volume, V_f to total volume, V inside a finite control volume. p^* is kinematic pressure [$m^2 s^{-2}$]. K is permeability [m^2]. The value of the coefficient K depends on the geometry of the medium. For the special case where the porous media is isotropic, K is a scalar field; for the more general case of anisotropic porous media, K is a tensor field. c_F is a dimensionless form-drag constant.

Equation 1.2 is a macroscopic momentum equation. It should be noted $\mathbf{u} = \phi \mathbf{u}_f$ is the “Darcy velocity” and similarly $p^* = \phi p_f^*$, where \mathbf{u}_f and p_f^* are the volumetric average (macroscopic)¹ fluid velocity and kinematic pressure respectively. Hsu and Cheng [1] derive equation 1.2 by volume averaging of the microscopic Navier Stokes conservation equations (2.1, 2.2) over a representative volume.

¹The volumetric average (macroscopic) fluid velocity and pressure are those averaged over V in contrast to the true local pore scale fluid velocity and pressure inside the porous media which the macroscopic momentum equation does not resolve.

Chapter 2

Solving the system of equations in OpenFOAM

2.1 icoFoam solver

Lets consider the unsteady, incompressible Navier Stokes continuity and momentum equations:

$$\nabla \cdot \mathbf{u} = 0 \quad (2.1)$$

$$\frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} = -\nabla p^* + \nu \nabla^2 \mathbf{u} + S_i \quad (2.2)$$

where S_i represents source terms. All other symbols take their usual meaning. Hence we have four equations and four unknowns (u, v, w, p^*). There is no equation for pressure. This is the system of equations solved for in OpenFOAM for the unsteady, incompressible solver icoFoam.

To proceed, the momentum equation (2.2) is constructed in matrix form as:

$$\mathbf{M}\mathbf{U} = -\nabla p^* \quad (2.3)$$

Considering the x components of the momentum equation; in expanded form we have n equations, one for each cell centroid:

$$\begin{pmatrix} M_{1,1} & M_{1,2} & M_{1,3} & \dots & M_{1,n} \\ M_{2,1} & M_{2,2} & M_{2,3} & \dots & M_{2,n} \\ M_{3,1} & M_{3,2} & M_{3,3} & \dots & M_{3,n} \\ \vdots & \vdots & \vdots & \ddots & \vdots \\ M_{n,1} & M_{n,2} & M_{n,3} & \dots & M_{n,n} \end{pmatrix} \begin{pmatrix} U_1 \\ U_2 \\ U_3 \\ \vdots \\ U_n \end{pmatrix} = \begin{pmatrix} (\partial p^* / \partial x)_1 \\ (\partial p^* / \partial x)_2 \\ (\partial p^* / \partial x)_3 \\ \vdots \\ (\partial p^* / \partial x)_n \end{pmatrix} \quad (2.4)$$

We require to solve for the unknown vector \mathbf{U} . Note that \mathbf{U} is a vector containing \mathbf{u} at all the cell centroids. The matrix of coefficients, \mathbf{M} , is known and populated using the finite volume method. Terms on the diagonal of \mathbf{M} pertain to contributions by the owner cell while off diagonal terms contain contributions from neighboring cells.

To proceed, the matrix of coefficients, \mathbf{M} is separated into diagonal components, \mathbf{A} and off-diagonal components, \mathbf{H} . Equation 2.3 then takes the form:

$$\mathbf{A}\mathbf{U} - \mathbf{H} = -\nabla p^* \quad (2.5)$$

The matrix \mathbf{A} contains the diagonal components of \mathbf{M} :

$$\mathbf{A} = \begin{pmatrix} A_{1,1} & 0 & 0 & \dots & 0 \\ 0 & A_{2,2} & 0 & \dots & 0 \\ 0 & 0 & A_{3,3} & \dots & 0 \\ \vdots & \vdots & \vdots & \ddots & \vdots \\ 0 & 0 & 0 & \dots & A_{n,n} \end{pmatrix} \quad (2.6)$$

The matrix \mathbf{A} is sometimes denoted a_p in the literature. \mathbf{A} is easily inverted resulting in \mathbf{A}^{-1} :

$$\mathbf{A}^{-1} = \begin{pmatrix} 1/A_{1,1} & 0 & 0 & \dots & 0 \\ 0 & 1/A_{2,2} & 0 & \dots & 0 \\ 0 & 0 & 1/A_{3,3} & \dots & 0 \\ \vdots & \vdots & \vdots & \ddots & \vdots \\ 0 & 0 & 0 & \dots & 1/A_{n,n} \end{pmatrix} \quad (2.7)$$

The matrix \mathbf{A}^{-1} is sometimes denoted $1/a_p$ in the literature. The matrix \mathbf{H} is evaluated explicitly using the velocity from the previous iteration. Hence it is known:

$$\mathbf{H} = \mathbf{A}\mathbf{U} - \mathbf{M}\mathbf{U} \quad (2.8)$$

We proceed with deriving a pressure equation. This is done by multiplying both sides of equation 2.5 by \mathbf{A}^{-1} and rearrange for \mathbf{U} :

$$\mathbf{U} = \mathbf{A}^{-1}\mathbf{H} - \mathbf{A}^{-1}\nabla p^* \quad (2.9)$$

Substituting equation 2.9 into the continuity equation (2.1) and rearranging we arrive at a Poisson equation for pressure:

$$\nabla \cdot (\mathbf{A}^{-1}\nabla p^*) = \nabla \cdot (\mathbf{A}^{-1}\mathbf{H}) \quad (2.10)$$

where p^* is unknown. Equation 2.10 is used to couple pressure and velocity given \mathbf{A}^{-1} and \mathbf{H} .

Notation for \mathbf{M} , \mathbf{A} etc. used in `icoFoam.C` is documented in table 2.1.

Algebraic	C++
\mathbf{M}	<code>UEqu</code>
\mathbf{A}	<code>UEqu.A()</code>
\mathbf{H}	<code>UEqu.H()</code>
\mathbf{A}^{-1}	<code>rAU</code>
$\mathbf{A}^{-1}\mathbf{H}$	<code>HbyA</code>

Table 2.1: Notation used in `icoFoam.C`.

The `volVectorField`, `HbyA`, is also represented as a `surfaceScalarField` (i.e. the flux of `HbyA`) by interpolating onto cell faces and taking the dot product of the face normal vectors. This `surfaceScalarField` is denoted `phiHbyA` and is used in solving the pressure Poisson equation.

2.2 PISO algorithm

The icoFoam solver uses the PISO (Pressure-Implicit with Splitting of Operators) pressure-velocity coupling algorithm to solve the governing equations and iterate forward in time.

2.2.1 PISO algorithm steps

Each step of the algorithm is documented here with reference to the icoFoam source code.

Step 1: Solve the momentum predictor

Given the current pressure and velocity fields; solve the momentum equation (2.3) for \mathbf{U} :

```
fvVectorMatrix UEqn
(
    fvm::ddt(U)                // Local acceleration term
    + fvm::div(phi, U)         // Convective acceleration term
    - fvm::laplacian(nu, U)    // Viscous term
);

if (piso.momentumPredictor())
{
    solve(UEqn == -fvc::grad(p));
}
```

This yields a velocity field which does not satisfy the continuity equation (2.1).

Step 2: Calculate \mathbf{A}^{-1} and $\mathbf{A}^{-1}\mathbf{H}$ fields

Calculate the \mathbf{A}^{-1} and $\mathbf{A}^{-1}\mathbf{H}$ fields from the current velocity field:

```
volScalarField rAU(1.0/UEqn.A());

volVectorField HbyA(constrainHbyA(rAU*UEqn.H(), U, p));
```

Step 3.1: Calculate phiHbyA

Calculate the flux of HbyA as the surfaceScalarField phiHbyA:

```
surfaceScalarField phiHbyA
(
    "phiHbyA",
    fvc::flux(HbyA)
    + fvc::interpolate(rAU)*fvc::ddtCorr(U, phi)
);
```

The second term in phiHbyA is the Rhie-Chow corrector [2]???

Step 3.2: Adjust boundary faces

Adjust the balance of fluxes on boundary faces (inlets and outlets) to obey continuity:

```
adjustPhi(phiHbyA, U, p);
```

Update the pressure on boundary faces where pressure flux is imposed:

```
constrainPressure(p, U, phiHbyA, rAU);
```

Step 4: Solve the pressure equation (non-orthogonal corrector loop)

Solve the Poisson equation (2.10) for the updated pressure field. Repeat for n non-orthogonal corrector loops:

```
fvScalarMatrix pEqn
(
    fvm::laplacian(rAU, p) == fvc::div(phiHbyA)
);
```

```
pEqn.setReference(pRefCell, pRefValue);
```

```
pEqn.solve();
```

On the final non-orthogonality correction, correct the flux using the most up-to-date pressure field:

```
if (piso.finalNonOrthogonalIter())
{
    phi = phiHbyA - pEqn.flux();
}
```

Step 5: Using updated pressure field, calculate flux-corrected velocity field

With the updated pressure field, calculate the corrected velocity field via equation 2.9:

```
U = HbyA - rAU*fvc::grad(p);
```

Impose boundary conditions on bounding faces:

```
U.correctBoundaryConditions();
```

The resulting velocity field now satisfies the continuity equation (2.1).

Step 6: Using flux-corrected velocity field repeat PISO corrector loop

Using the flux-corrected velocity field return to Step 2 and repeat Step 2 to Step 5 for n PISO corrector loops. This way the momentum predictor is solved once per iteration. Several PISO corrector inner loops are preformed per iteration. In practice, two PISO corrector loops are typically performed per iteration to arrive at a “converged” pressure field.

2.2.2 PISO algorithm functions

Details of PISO loop functions found in `icoFoam.C` are documented in table 2.2.

Function	Description
<code>constrainHbyA()</code>	Ensure equation 2.9 is satisfied on boundary faces.
<code>fvc::flux()</code>	Return surfaceScalarField representing cell face flux obtained from a given volVectorField.
<code>fvc::interpolate()</code>	Interpolate cell centered field onto cell faces.
<code>fvc::ddtCorr()</code>	Included as part of the correction to the Rhie-Chow interpolation [2]???
<code>adjustPhi()</code>	Adjust balance of fluxes on boundary faces (inlets and outlets) to obey continuity.
<code>constrainPressure()</code>	Update the pressure on boundary faces where a pressure flux is imposed.

Table 2.2: Table to test captions and labels.

2.3 porousIcoFoam solver

Following the same solution algorithm detailed in §2.1 and §2.2, a new solver has been implemented in OpenFOAM to solve the DBF governing equations (1.1, 1.2). This solver is a modified version of the built in icoFoam solver called porousIcoFoam. The main modification is in the definition of the UEqn in porousIcoFoam.C which becomes:

```
fvVectorMatrix UEqn
(
    (1.0/pty)*fvm::ddt(U)                // Local acceleration term
    + (1.0/sqr(pty))*fvm::div(phi, U)     // Convective acceleration term
    - (1.0/pty)*fvm::laplacian(nu, U)     // Viscous term
    + fvm::SuSp(nu/K_, U)                 // Darcy term
    + fvm::SuSp((cf/sqrt(K_))*mag(U), U)  // Forchheimer term
);
```

where `pty` and `K_` are porosity (volScalarField) and permeability (volScalarField) respectively and `cf` is the dimensionless form-drag constant (dimensionedScalar). These new parameters are read into the solver via the `creatFields.H` header file and must be correctly defined in the `./0/*` and `./constant/transportProperties` dictionaries in case directory.

2.3.1 poroucIcoFoam case setup

2.3.2 poroucIcoFoam verification

Neale and Nadar [3] present an analytical solution for the velocity profile for flow within a channel bound above by a solid wall ($y = h$) and below by a porous medium ($0 > y > H$) for the Brinkman extended Darcy law (i.e. dropping the material derivative and Forchheimer terms in equation 1.2). For the channel flow problem considered here, the DBF momentum equation takes the form:

$$\frac{\mu}{K}u + \frac{\mu}{\phi} \frac{d^2u}{dy^2} = \frac{dp}{dx} \quad (2.11)$$

The analytical solution is analogous to the solution of Poiseuille pipe flow. The no slip condition is applied on the upper bounding wall ($y = h$) in the clear fluid region and a slip condition is applied on the lower wall ($y = H$) of the porous media region. Full expressions for the analytical solution for the velocity profiles in the clear fluid and porous media regions are given in Neale and Nadar [3] but are omitted here for brevity.

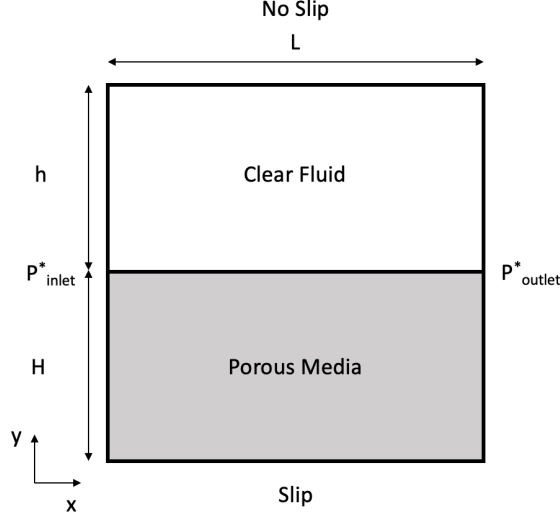


Figure 2.1: Verification domain.

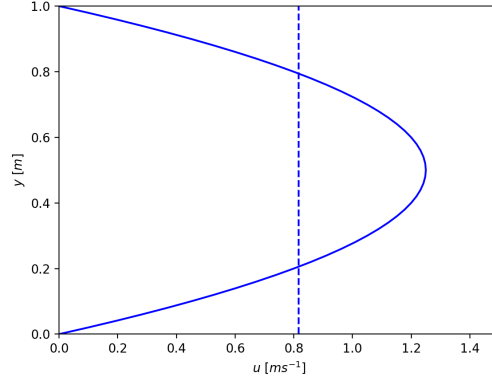
It is possible to solve the channel flow problem numerically applying a constant pressure gradient along the length of a two-dimensional domain and no slip/slip boundary conditions at the upper and lower bounds of the domain respectively. A simulation domain is set up with $h = H = 1 \text{ m}$, $L = 2 \text{ m}$ and $dP^*/dx = 1 \text{ ms}^{-2}$. Kinematic viscosity, ν , is equal to $0.1 \text{ m}^2\text{s}^{-1}$. Density, ρ is set to unity, hence $\mu \equiv \nu$ and $p \equiv p^*$. The numerical solution is solved for on an orthogonal, uniform 200×200 rectilinear grid with 0.01 m cell size. A matrix of analytical and numerical solutions for the velocity profile in the channel are presented in figure 2.2 for $\phi = [0.75, 0.95]$ and $Da = [10^{-2}, 10^{-4}]$ where $Da = K/l^2$ is the Darcy number, a dimensionless number describing porous media permeability. l is the characteristic length and is set equal to h . Results are presented in non-dimensional form with the characteristic velocity, U_∞ , taken as the mean flow velocity in the clear fluid region when it is bound above and below by a solid wall with the no slip boundary condition (Poiseuille pipe flow, see Figure 2.2a). $U_\infty = 0.8167 \text{ ms}^{-1}$ and hence, the Reynolds number, $Re = 8.167$. Neale and Nadar [3] provide an expression for mass flow rate per unit width, M , expressed as M/M_0 where M_0 denotes the flow which would prevail in the clear fluid region if the lower wall were impermeable (Poiseuille pipe flow, see Figure 2.2a). Results for $M/M_0|_{\text{analytical}}$ are compared against those for $M/M_0|_{\text{numerical}}$ in table 2.3.

Varying Da has a greater impact on the velocity profile compared with varying ϕ . With decreasing Da the problem approximates Poiseuille pipe flow where there is negligible fluid flow in the porous media region. It is evident from the velocity profiles in figure 2.2 and M/M_0 results in table 2.3 that the numerical solutions do not match exactly the analytical solutions. It is posed that these discrepancies originate from the implementation of the convective term in equation 1.2. According to the Dupuit-Forchheimer relationship a factor

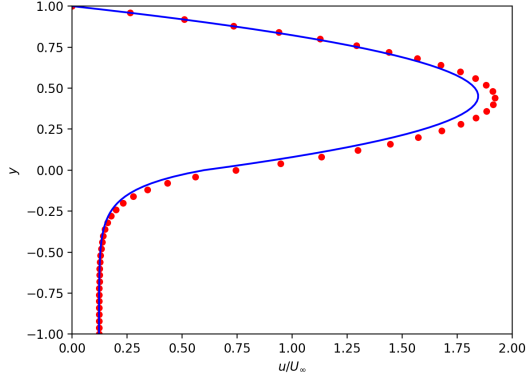
	$M/M_0 _{analytical}$	$M/M_0 _{numerical}$	Difference (%)
$\phi = 0.75 \ Da = 10^{-2}$	1.294319	1.346897	3.90
$\phi = 0.75 \ Da = 10^{-4}$	1.026353	1.033239	0.67
$\phi = 0.95 \ Da = 10^{-2}$	1.321106	1.317734	0.26
$\phi = 0.95 \ Da = 10^{-4}$	1.030367	1.029552	0.08

Table 2.3: Mass flow rate per unit width, M/M_0 results.

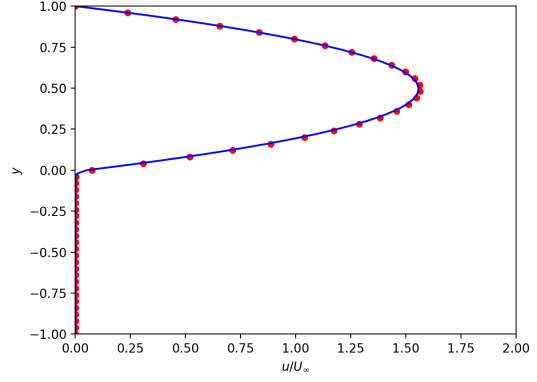
of $1/\phi$ should be taken inside the gradient term to account for non-homogeneous porosity in the single domain model; neglecting to do so is a simplification which assumes negligible spatial variation in porosity. The largest discrepancy between analytical and numerical solutions being in the case of $\phi = 0.75$, $Da = 10^{-2}$ corroborates this. The effect of porosity variation is not required for a high-porosity medium, but it should be considered for a dense porous medium [4].



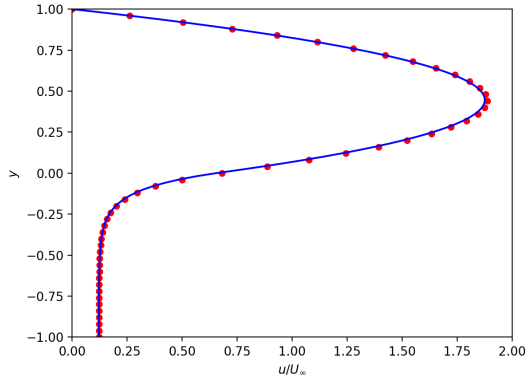
(a) Poiseuille pipe flow. Velocity profile, $u(y)$ (solid blue line). Mean velocity, U_∞ (dashed blue line).



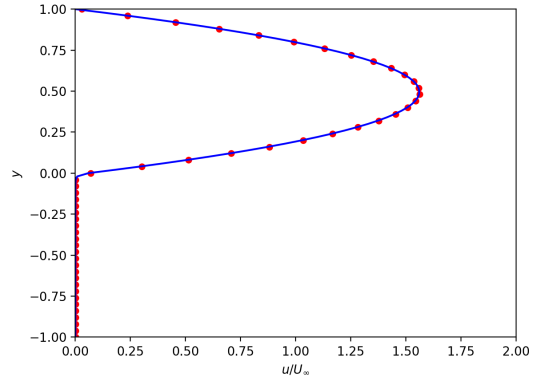
(b) $\phi = 0.75$ $Da = 10^{-2}$



(c) $\phi = 0.75$ $Da = 10^{-4}$



(d) $\phi = 0.95$ $Da = 10^{-2}$



(e) $\phi = 0.95$ $Da = 10^{-4}$

Figure 2.2: porousIcoFoam verification cases. Analytical velocity profile (solid blue line), numerical velocity profile (red dots) for cases b), c), d) and e).

Chapter 3

Forces and moments acting on porous bodies

3.1 Conventional forces and moments calculation

The conventional forces and moments calculation considers the various contributions to the total forces and moments acting on a porous body as described by the DBF momentum equation (1.2). These include normal pressure, tangential viscous, Darcy and Forchheimer contributions.

3.1.1 Normal pressure contribution

The normal pressure force contribution is calculated as a surface integral at the clear fluid - porous media interface. This is written in discrete form as:

$$d\mathbf{F}_p|_i = \rho \mathbf{A}_i (p_i^* - p_{ref}^*) \quad (3.1)$$

$$\mathbf{F}_p = \sum_i d\mathbf{F}_p|_i \quad (3.2)$$

where \mathbf{A}_i is the i^{th} boundary face area vector. The normal pressure moment contribution is given, in discrete form, as:

$$d\mathbf{M}_p|_i = \mathbf{r}_i \times d\mathbf{F}_p|_i \quad (3.3)$$

$$\mathbf{M}_p = \sum_i d\mathbf{M}_p|_i \quad (3.4)$$

where \mathbf{r}_i is the i^{th} boundary face position vector.

3.1.2 Tangential viscous contribution

The tangential force contribution is calculated as a surface integral at the clear fluid - porous media interface. This is written in discrete form as:

$$d\mathbf{F}_v|_i = \mathbf{A}_i \cdot \boldsymbol{\tau}_i \quad (3.5)$$

$$\mathbf{F}_v = \sum_i d\mathbf{F}_v|_i \quad (3.6)$$

where $\boldsymbol{\tau}_i$ is the viscous stress tensor on the boundary face. The tangential viscous moment contribution is given, in discrete form, as:

$$d\mathbf{M}_v|_i = \mathbf{r}_i \times d\mathbf{F}_v|_i \quad (3.7)$$

$$\mathbf{M}_v = \sum_i d\mathbf{M}_v|_i \quad (3.8)$$

3.1.3 Darcy contribution

The Darcy force contribution is calculated as a volume integral. Considering the third term on the RHS of equation 1.2 the Darcy force contribution is given, in discrete form, as:

$$d\mathbf{F}_d|_i = \rho \mathbf{V}_i \left(\frac{\nu}{K} \mathbf{u} \right) \quad (3.9)$$

$$\mathbf{F}_d = \sum_i d\mathbf{F}_d|_i \quad (3.10)$$

where \mathbf{V}_i is the i^{th} volume element (inside the porous media). The Darcy moment contribution is calculated, in discrete form, as:

$$d\mathbf{M}_d|_i = \mathbf{r}_i \times d\mathbf{F}_d|_i \quad (3.11)$$

$$\mathbf{M}_d = \sum_i d\mathbf{M}_d|_i \quad (3.12)$$

3.1.4 Forchheimer contribution

The Forchheimer force contribution is calculated as a volume integral. Considering the forth term on the RHS of equation 1.2 the Forchheimer force contribution is given, in discrete form, as:

$$d\mathbf{F}_f|_i = \rho \mathbf{V}_i \left(\frac{c_F}{\sqrt{K}} |\mathbf{u}| \mathbf{u} \right) \quad (3.13)$$

$$\mathbf{F}_f = \sum_i d\mathbf{F}_f|_i \quad (3.14)$$

The Forchheimer moment contribution is calculated, in discrete form, as:

$$d\mathbf{M}_f|_i = \mathbf{r}_i \times d\mathbf{F}_f|_i \quad (3.15)$$

$$\mathbf{M}_f = \sum_i d\mathbf{M}_f|_i \quad (3.16)$$

3.2 Vorticity-moment theorem (impulse theory) forces and moments calculation

An alternative method for calculating the forces and moments acting on a body is to use the vorticity-moment theorem, or impulse theory. This method has its origins in the general formulas relating aerodynamic forces and moments to rates of change of vorticity moments originally presented by Wu [5]. The aerodynamic force acting on a solid body immersed in

a fluid region extending to infinity, R_f , with a reference frame fixed with the body, is given by:

$$\mathbf{F} = -\frac{\rho}{2} \frac{d}{dt} \iiint_{R_f} \mathbf{r} \times \boldsymbol{\omega} dR \quad (3.17)$$

The aerodynamic moment acting on a solid body immersed in R_f , with a reference frame fixed with the body, is given by:

$$\mathbf{M} = \frac{\rho}{2} \frac{d}{dt} \iiint_{R_f} |\mathbf{r}|^2 \boldsymbol{\omega} dR \quad (3.18)$$

Equations 3.17 and 3.18 are taken from Elements of Vorticity Aerodynamics [6] which discusses in detail the vorticity-moment theorem and presents versions of 3.17 and 3.18 where the body is moving and rotating relative to the fluid.

Bibliography

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