

# How Complex are Complex Fluids?

## PSS Talk

Christian Jones



September 9, 2024

# About Me



Doran, J., 2023

- 3<sup>rd</sup> year SAMBa student.
- Working towards a PhD involving **viscoelastic fluids!**
- Former PSS organiser (with Corin)
- Tuba player with City of Bath.

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- Tuba player with City of Bath.
- From North Wales!

# Amdanaf Fi



Doran, J., 2023

- Myfyriwr 3ydd blwyddyn SAMBa.
- Gweithio tuag at PhD gan gynnwys hylifau fiscoelastig!
- Cyn-drefnydd PSS (gyda Corin)
- Chwaraewr Tiwba gyd band City of Bath
- Yn dod o Ogledd Cymru!

# Complex Fluids?

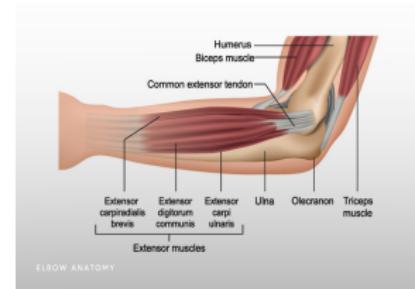
- Many materials we encounter have **viscoelastic** properties.
  - Viscosity: measure of resistance to flow.
  - Elasticity: ability of a material to return to its original state after removal of deforming forces.
- Characterised by a *relaxation time* — quantifies ‘memory’ of deformation history.



eggs.ca, 2023



iStock, 2021



Verma, N., 2023

# Polymeric Fluids

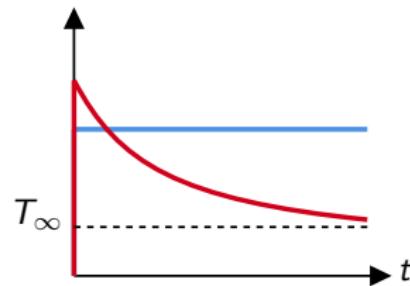
- Polymer — long chain molecule formed of repeating units/monomers.
- Polymer melt — a thermoplastic heated to a temperature above its melting point.
- (Dilute) polymer solution — polymer molecules suspended in a solvent.



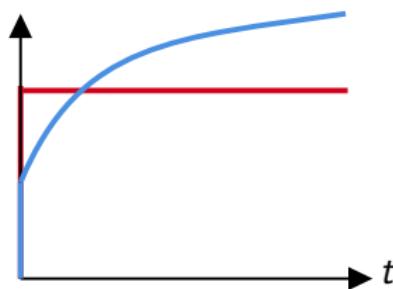
Cabrera, X., 2020.

# Properties of Polymeric Fluids

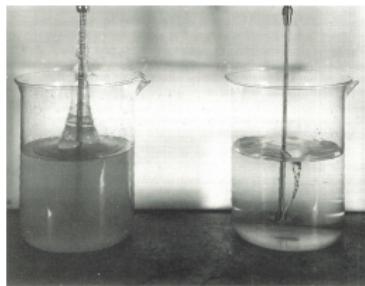
Stress Relaxation:



Creep:

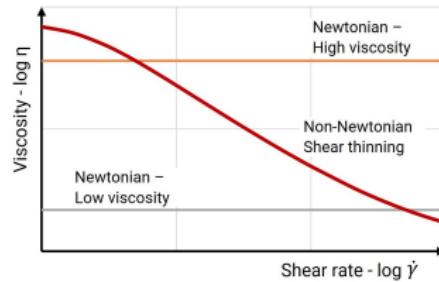


Normal Stress Effects:



Tanner, R. I., 2000

'Variable' Viscosity:

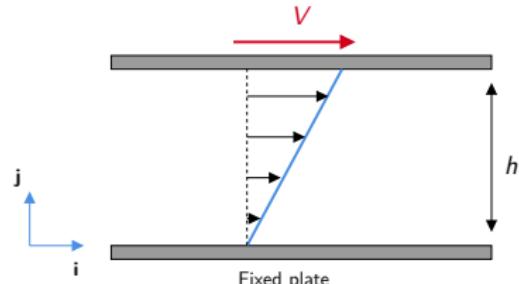


Østergård, A. L., 2020.

# Variable Viscosity

- Shear thinning — shear viscosity  $\eta_s$  should drop with shear rate  $\dot{\gamma}$ .

$$\mathbf{u} = (\dot{\gamma}y, 0, 0)^T, \dot{\gamma} = \frac{V}{h}$$



- Strain hardening — elongational viscosity  $\eta_e$  should increase with elongation rate  $\dot{\epsilon}$ .

$$\mathbf{u} = (\dot{\epsilon}x, -\frac{1}{2}\dot{\epsilon}y, -\frac{1}{2}\dot{\epsilon}z)^T$$



# Viscoelastic Modelling

## Overview

Q. How can we model these materials?

A. Use **conservation laws**.

1 Mass:

$$\nabla \cdot \mathbf{u} = 0.$$

2 Momentum:

$$\rho \left( \frac{\partial \mathbf{u}}{\partial t} + (\mathbf{u} \cdot \nabla) \mathbf{u} \right) = -\nabla p + \nabla \cdot \mathbf{T}, \quad \mathbf{T}^T = \mathbf{T}.$$

With this notation, we also have

$$\eta_s = \frac{T_{12}}{\dot{\gamma}}, \quad \eta_e = \frac{T_{11} - T_{22}}{\dot{\epsilon}}.$$

# Viscoelastic Modelling

## Specifying $\mathbf{T}$

We still need to specify  $\mathbf{T}!$

$$\rho \left( \frac{\partial \mathbf{u}}{\partial t} + (\mathbf{u} \cdot \nabla) \mathbf{u} \right) = -\nabla p + \nabla \cdot \mathbf{T}.$$

- $\mathbf{T} = \mathbf{0} \rightarrow \text{inviscid fluids.}$
- $\mathbf{T} = \eta [\nabla \mathbf{u} + \nabla \mathbf{u}^T] := 2\eta \mathbf{D} \rightarrow \text{Newtonian fluids.}$
- $\mathbf{T} = 2\eta(\dot{\gamma}) \mathbf{D} \rightarrow \text{generalised Newtonian fluids.}$

None of these really help us...

# Viscoelastic Modelling

## Constitutive Equations

Can we do better?

# Viscoelastic Modelling

## Constitutive Equations

Can we do better?

- Acierno et. al.
- Chang et. al.
- Chilcott-Rallison
- Corotational Jeffreys
- Corotational Maxwell
- Curtiss-Bird
- Doi-Edwards
- Elastic Dumbbell
- Extended Pom-Pom
- Extended WM
- FENE
- FENE-P
- Giesekus
- Green-Tobolsky
- Jeffreys
- Johnson-Segelman
- Kaye-BKZ
- Kelvin-Voigt
- Leonov
- Lodge
- Maxwell
- Maxwell-Wiechert
- Modified UCM
- Oldroyd 8 Constant
- Oldroyd-B
- Phan-Thien-Tanner
- Pom-Pom
- Rolie-Poly
- Rouse
- Tanner-Simmons
- Upper Convected Maxwell
- White-Metzner
- Yamamoto

# Viscoelastic Modelling

## Constitutive Equations

Can we do better?

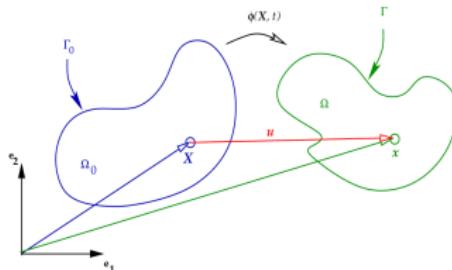
- Acierno et. al.
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# Viscoelastic Modelling

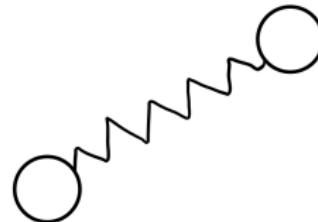
## Constitutive Equations

Models fall into four categories:

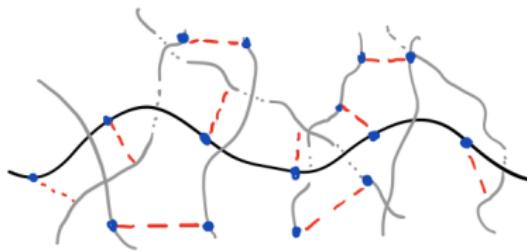
Continuum:



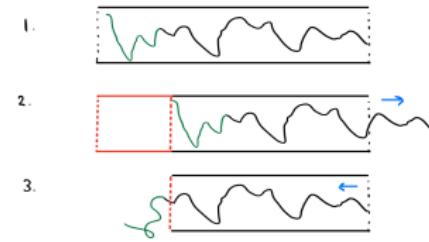
Dumbbell:



Network:



Reptation:



# Maxwell Model

## Spring-Dashpot Schematics

- Need to capture effects of elasticity and viscosity.
- Initially work in 1D.
- Represent materials schematically.

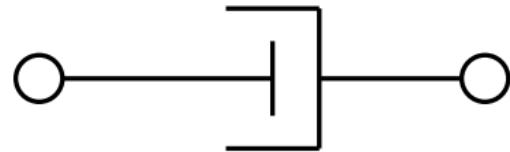
Hookean springs

$E$



Newtonian dashpots

$\eta_0$

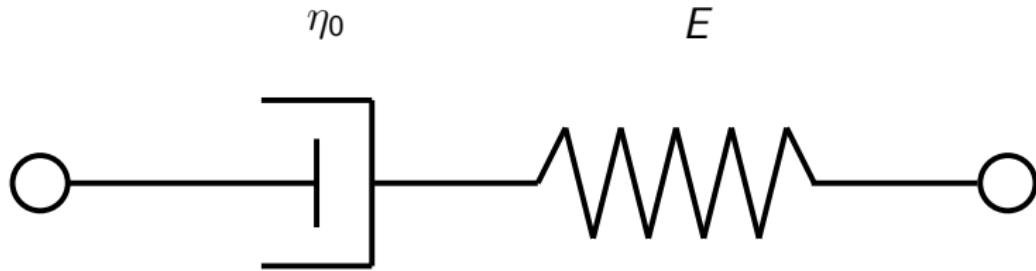


- Build models by combining these elements!

# Maxwell Model

## Maxwell Material

The simplest construction we can make is

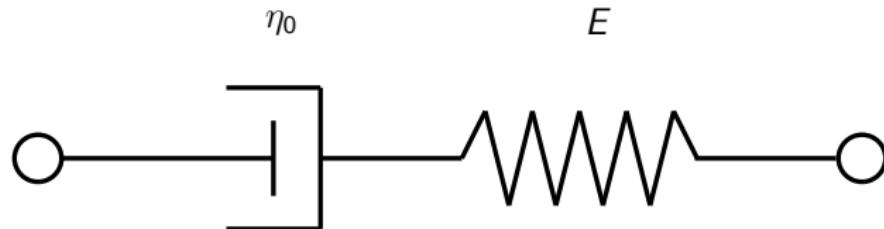


We need to relate the stress  $T$  to the strain  $\epsilon$ .

$$\epsilon = \frac{\text{change in length}}{\text{original length}}.$$

# Maxwell Model

## Maxwell Equation



## Components

Spring:  $T_S = E\epsilon_S$  (Hooke's Law)

Dashpot:  $T_D = \eta_0 \frac{\partial \epsilon_D}{\partial t}$  (Newton's Law of Viscosity)

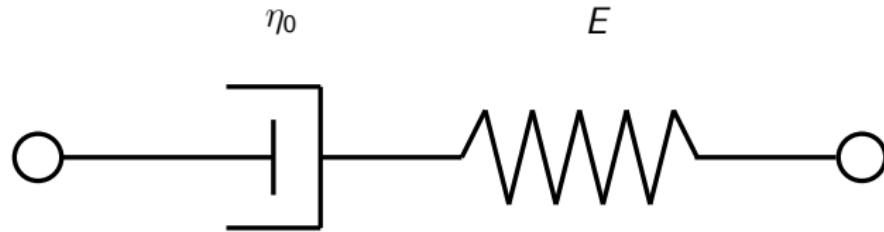
## Total

Stress:  $T = T_S = T_D$ .

Strain:  $\epsilon = \epsilon_S + \epsilon_D$ .

# Maxwell Model

## Maxwell Equation



Differentiating total strain yields:

$$T + \lambda \frac{\partial T}{\partial t} = \eta_0 \frac{\partial \epsilon}{\partial t},$$

with relaxation time  $\lambda = \frac{\eta_0}{E}$ .

This is the Maxwell equation!

Maxwell, J. C. 1867.

# Maxwell Model

Is this any good?

In three dimensions:

$$\boldsymbol{T} + \lambda \frac{\partial \boldsymbol{T}}{\partial t} = 2\eta_0 \boldsymbol{D}.$$

Predictions:

- Viscous and elastic limits!
- Stress relaxation — for a step strain ( $2\boldsymbol{D} = \boldsymbol{\epsilon}_0 \delta(t)$ ),

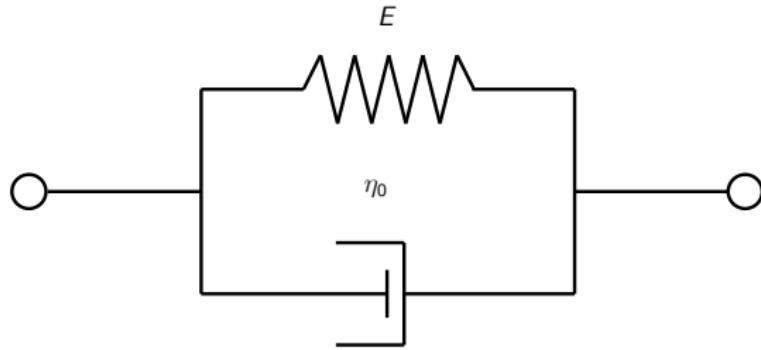
$$\boldsymbol{T} = \boldsymbol{\epsilon}_0 \frac{\eta_0}{\lambda} e^{-t/\lambda} H(t).$$

- Creep — response to step stress is linear.
- Shear — no shear thinning ( $\eta_s = \eta_0$ ).
- Elongation — no strain hardening ( $\eta_e = 3\eta_0$ ).

# Further Spring and Dashpot Models

How else can we relate strain ( $\epsilon$ ) and stress ( $T$ )?

## 1. Kelvin-Voigt



$$T = E\epsilon + \eta_0 \frac{\partial \epsilon}{\partial t}.$$

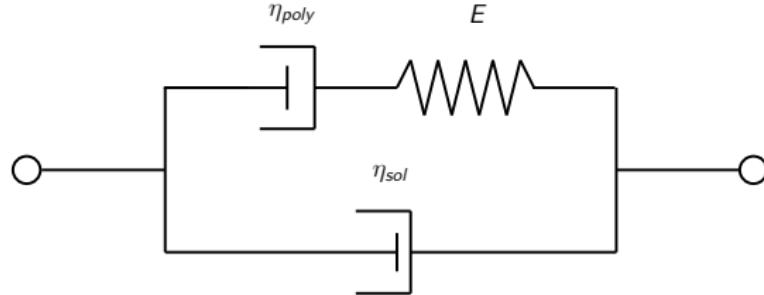
Captures creep behaviour better at expense of stress relaxation.

Thompson, W. 1878.

# Further Spring and Dashpot Models

How else can we relate strain ( $\epsilon$ ) and stress ( $T$ )?

2. Jeffreys'



$$T + \lambda \frac{\partial T}{\partial t} = \eta_0 \left( \frac{\partial \epsilon}{\partial t} + \lambda_r \frac{\partial^2 \epsilon}{\partial t^2} \right).$$

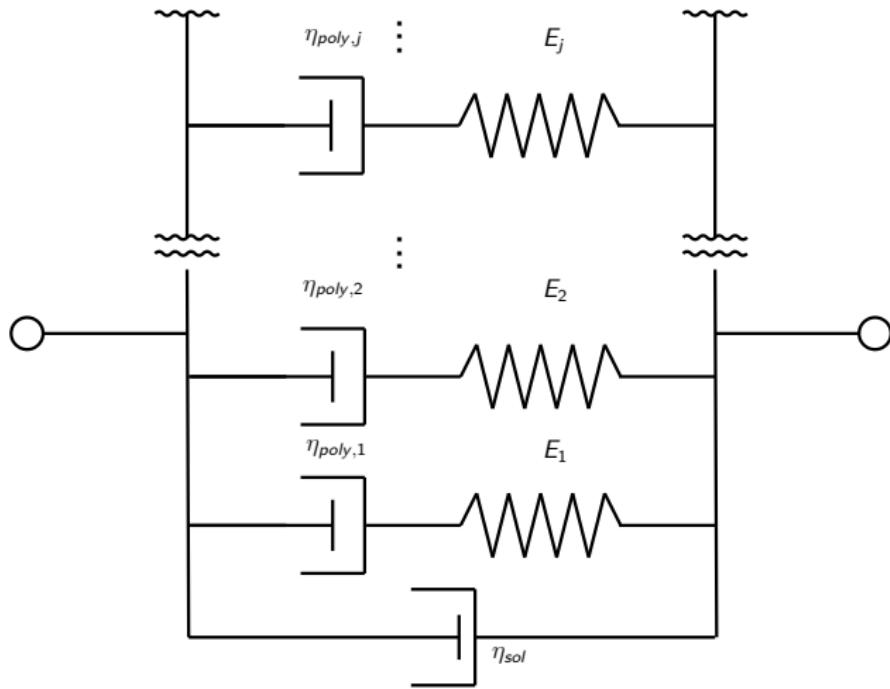
- Relaxation time:  $\lambda = \frac{\eta_{poly}}{E}$
- Zero-shear viscosity:  $\eta_0 = \eta_{poly} + \eta_{sol}$
- Retardation time:  $\lambda_r = \frac{\eta_{sol}\eta_{poly}}{E\eta_0}$

Jeffreys, H., 1929.

# Further Spring and Dashpot Models

How else can we relate strain ( $\epsilon$ ) and stress ( $T$ )?

## 3. Maxwell-Wiechert (equation omitted!)



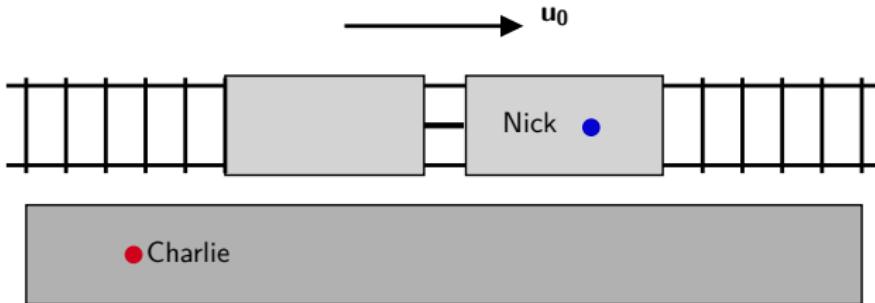
# A Major Problem!

- None of these models hold for large deformations!
- Why? They are not *frame invariant*.
  - Relation between stress and strain needs to be independent of the frame of reference.
- Return to the Maxwell equation:

$$\boldsymbol{\tau} + \lambda \frac{\partial \boldsymbol{\tau}}{\partial t} = 2\eta_0 \boldsymbol{D}.$$

- Note this depends only on stresses ( $\boldsymbol{\tau}$ ) and velocity gradients ( $\boldsymbol{D}$ ).

# A Major Problem!

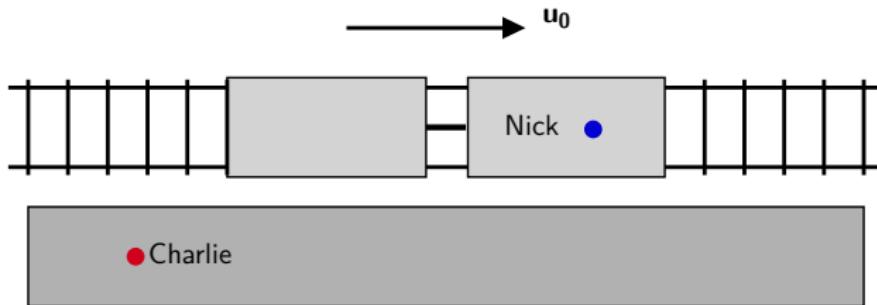


Example:

- Two identical fluids: one in a stationary frame (Charlie); one on a train with constant velocity  $\mathbf{u}_0$  (Nick).
- Both fluids should be described by the same Maxwell equation.
- However, Charlie sees Nick's change in stress as

$$\frac{\partial}{\partial t} T_{ij}(\mathbf{x} + \mathbf{u}_0 t, t) = \frac{\partial}{\partial t} T_{ij} + \mathbf{u}_0 \cdot \nabla T_{ij}.$$

# A Major Solution!



- Fix: replace  $\frac{\partial}{\partial t}$  with a new time derivative!
- Choose an *upper convected derivative*:

$$\overset{\nabla}{S} := \frac{\partial S}{\partial t} + (\mathbf{u} \cdot \nabla) S - (\nabla \mathbf{u}) S - S(\nabla \mathbf{u})^T.$$

- This is now frame invariant!

# A Major Solution!

New equations!

- Maxwell → Upper Convected Maxwell (UCM)

$$\boldsymbol{T} + \lambda \overset{\nabla}{\boldsymbol{T}} = 2\eta_0 \boldsymbol{D}.$$

- Jeffreys' → Oldroyd-B

$$\boldsymbol{T} + \lambda \overset{\nabla}{\boldsymbol{T}} = 2\eta_0 (\boldsymbol{D} + \lambda_r \overset{\nabla}{\boldsymbol{D}}).$$

Note that setting  $\lambda_r = 0$  gives UCM; setting  $\lambda_r = \lambda$  gives the Newtonian stress tensor.

Oldroyd, J. G., 1950.

# UCM/Oldroyd-B

$$\boldsymbol{T} + \lambda \overset{\nabla}{\boldsymbol{T}} = 2\eta_0(\boldsymbol{D} + \lambda_r \overset{\nabla}{\boldsymbol{D}})$$

Predictions:

- Stress relaxation/creep inherited from Maxwell model.
- Shear:

$$\eta_s = \eta_0, \quad T_{11} - T_{22} = 2\eta_0(\lambda - \lambda_r)\dot{\gamma}^2, \quad T_{22} - T_{33} = 0.$$

- Extension:

$$\eta_e = \eta_0 \left[ \frac{2(1 - \lambda_r \dot{\epsilon})}{1 - 2\lambda \dot{\epsilon}} + \frac{1 + \lambda_r \dot{\epsilon}}{1 + \lambda \dot{\epsilon}} \right]$$

We obtain strain hardening (with a vengeance!)

# Going Further

We can improve on this... but the equations become unwieldy!

- White-Metzner:  
Viscosity and relaxation time shear rate dependent.
- Extended White-Metzner:  
Viscosity and relaxation time dependent on trace of stress tensor.
- Corotational UCM:  
Swap  $\overset{\nabla}{T}$  with a *Jaumann* time derivative.

Does moving beyond continuum mechanics help?

White, J. L. and Metzner, A. B., 1960/Souvaliotis, A. and Beris, A. N. 1992/Jaumann, G., 1911

# A Dumbbell Model

- Polymers aren't points!
- Suppose they are subject to *direction dependent drag*.
- In absence of solvent ( $\eta_{sol} = 0$ ,  $\eta_p = \eta_0$ ), modify UCM equation as

$$\lambda \overset{\nabla}{\mathbf{T}} + \mathbf{M}\mathbf{T} = 2\eta_0 \mathbf{D}.$$

- Choosing  $\mathbf{M} = \mathbf{I} + \frac{\alpha\lambda}{\eta_0} \mathbf{T}$  gives the *Giesekus model*:

$$\lambda \overset{\nabla}{\mathbf{T}} + \mathbf{T} + \frac{\alpha\lambda}{\eta_0} \mathbf{T}^2 = 2\eta_0 \mathbf{D}, \quad \alpha \in (0, 1).$$

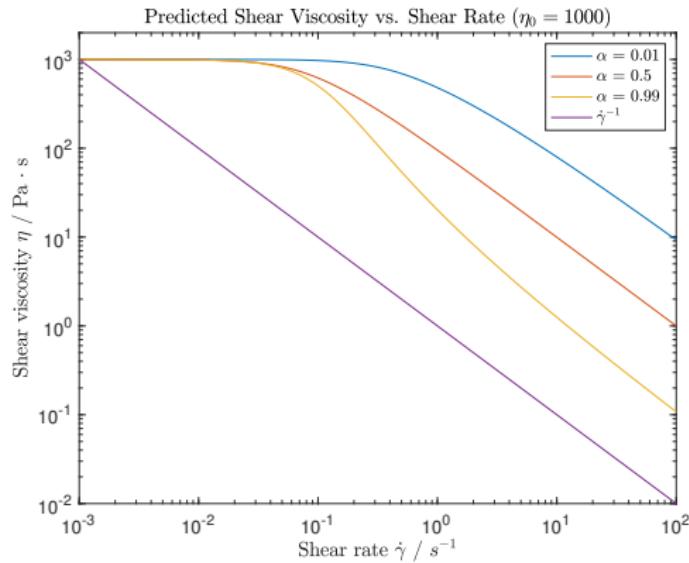
- This is no longer linear in stress!

Giesekus, H., 1966.

# Giesekus Predictions

## Shear Viscosity

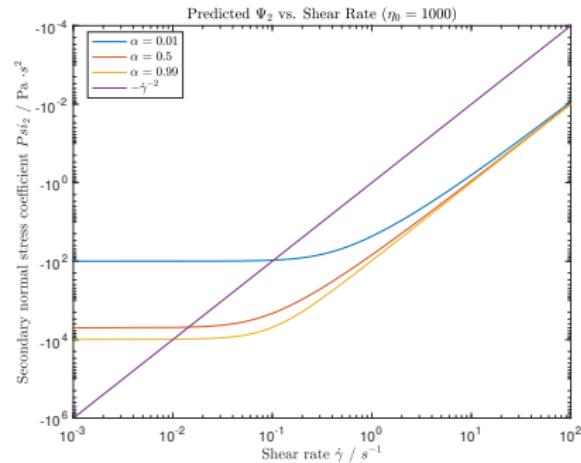
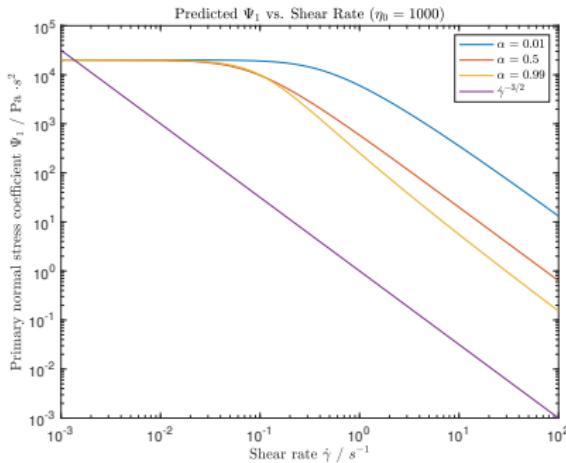
We actually predict shear thinning!



# Giesekus Predictions

## Shear Normal Stress Coefficients

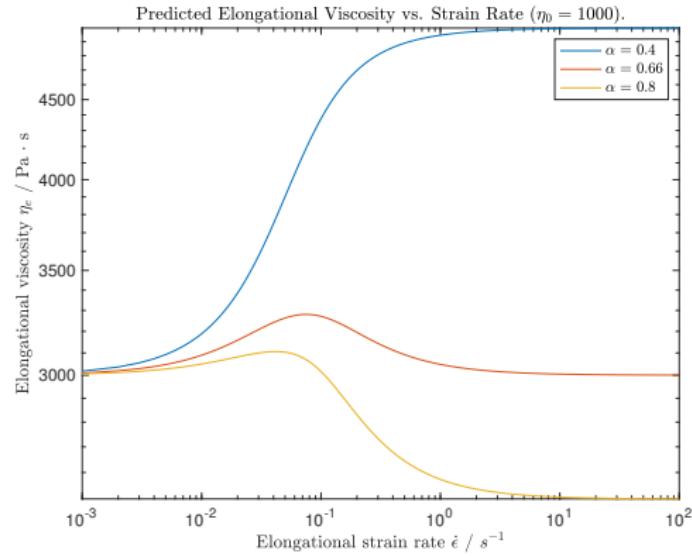
*Positive primary normal stresses; negative secondary normal stresses.*



# Giesekus Predictions

## Elongational Viscosity

Strain *hardening* for  $\alpha < 2/3$ ; strain *softening* for  $\alpha \geq 2/3$ .



Bird et. al.: ( $\alpha < 1/2$ ) (1987)

# Giesekus Predictions

In fact...

Constitutive model	Steady viscometric									Remark
	Small-strain	$\eta$	$N_1$	$N_2$	Steady elongation	Start/stop in shearing flow	Elongational start/recoil	Single shear step	Double-step shear	
Newtonian, eqn (1.7)	P	M	U	U	M	P	U	U	U	Infinite stresses in step strains.
Generalized Newtonian, e.g. eqns (4.4, 4.11)	P	E	U	U	M	P	U	U	U	Infinite stresses in step strains.
Lodge-Maxwell, (UCM) eqns (4.25, 5.150)	E	M	M	U	P	M	M	M	M	Useful for illustrative purposes.
Giesekus eqn (5.111)	E	E	E	G-E	G	G	G	M	M	

...Giesekus can have fairly good predictions in many situations!

Tanner, R. I., 2000.

# Summary

So far, we have

- Discussed the basics of viscoelastic modelling.
- Looked at some mechanical-based continuum models and motivated the UCM model.
- Discussed a more complicated model which can make more useful predictions.

One final question...

# Summary

So far, we have

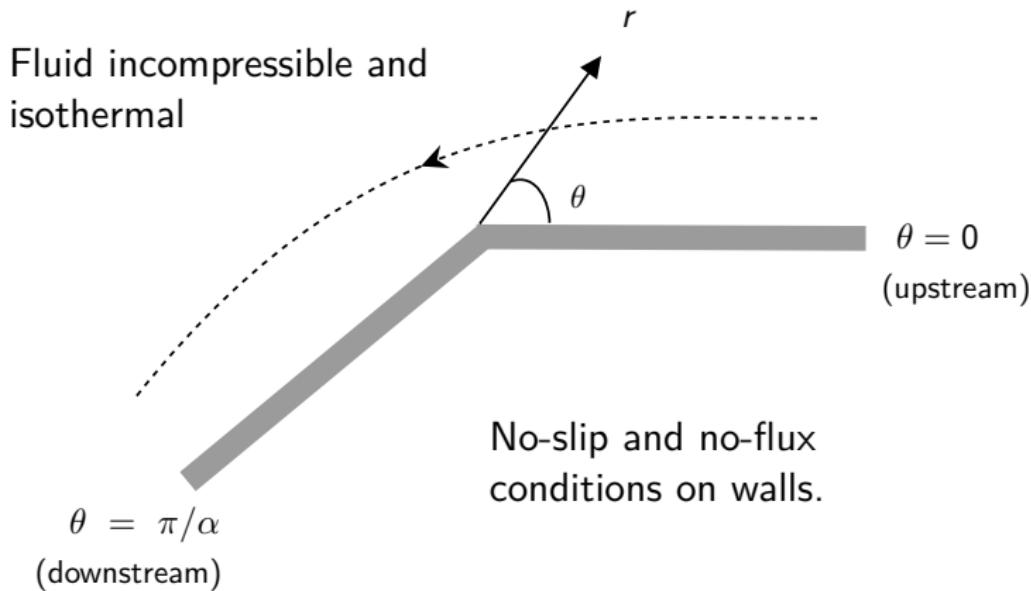
- Discussed the basics of viscoelastic modelling.
- Looked at some mechanical-based continuum models and motivated the UCM model.
- Discussed a more complicated model which can make more useful predictions.

One final question...

Why am I here!?

# What About a More Complex Flow?

Planar, steady flow around corner of angle  $\theta = \pi/\alpha$ . ( $1/2 \leq \alpha < 1$ )



PhD aim: *Apply asymptotic techniques to study White-Metzner fluids.*

# White-Metzner?

Dimensionless equations:

$$\nabla \cdot \mathbf{u} = 0,$$

$$\text{Re}(\mathbf{u} \cdot \nabla) \mathbf{u} = -\nabla p + \nabla \cdot \boldsymbol{\mathcal{T}},$$

$$\boldsymbol{\mathcal{T}} + \text{Wi} \dot{\gamma}^{n-1} \overset{\nabla}{\boldsymbol{\mathcal{T}}} = 2\dot{\gamma}^{n-1} \boldsymbol{\mathcal{D}}.$$

Obtain Reynolds (Re) and Weissenberg (Wi) numbers:

$$\text{Re} = \frac{[\text{inertial forces}]}{[\text{viscous forces}]}; \quad \text{Wi} = \frac{[\text{elastic forces}]}{[\text{viscous forces}]}.$$

These equations are complicated...

# White-Metzner?

...and I've gone through a lot of A3 paper this year!



# What Does 500+ Sheets of A3 Give You?

White-Metzner Equations:

$$\begin{aligned} 2Winf''|f''|^{n-1}t_{uw} &= [n - 2Wif'|f''|^{n-1}((3 - 2\alpha)n + \alpha - 1)](f')^2 t_{uu} \\ &\quad - (2(2 - \alpha)n + \alpha - 1)Wif(f')^2 |f''|^{n-1}t'_{uu}. \end{aligned}$$

Momentum equation:

# What Does 500+ Sheets of A3 Give You?

White-Metzner Equations:

$$2\text{Wi}f''|f''|^{n-1}t_{uw} = [n - 2\text{Wi}f'|f''|^{n-1}((3 - 2\alpha)n + \alpha - 1)](f')^2 t_{uu} \\ - (2(2 - \alpha)n + \alpha - 1)\text{Wi}f(f')^2 |f''|^{n-1}t'_{uu}.$$

$$n\text{Wi}f''|f''|^{n-1}t_{ww} = [n + \text{Wi}(\alpha - 1)nf'|f''|^{n-1}](f')^2 t_{uw} \\ - (2(2 - \alpha)n + \alpha - 1)\text{Wi}f(f')^2 |f''|^{n-1}t'_{uw}.$$

Momentum equation:

# What Does 500+ Sheets of A3 Give You?

White-Metzner Equations:

$$2\text{Wi}f''|f''|^{n-1}t_{uw} = [n - 2\text{Wi}f'|f''|^{n-1}((3 - 2\alpha)n + \alpha - 1)](f')^2 t_{uu} \\ - (2(2 - \alpha)n + \alpha - 1)\text{Wi}f(f')^2 |f''|^{n-1}t'_{uu}.$$

$$n\text{Wi}f''|f''|^{n-1}t_{ww} = [n + \text{Wi}(\alpha - 1)nf'|f''|^{n-1}](f')^2 t_{uw} \\ - (2(2 - \alpha)n + \alpha - 1)\text{Wi}f(f')^2 |f''|^{n-1}t'_{uw}.$$

$$n(f')^2 = nt_{ww} + 2((2 - \alpha)n + (\alpha - 1))\text{Wi}f'|f''|^{n-1}t_{ww} \\ - (2(2 - \alpha)n + \alpha - 1)f|f''|^{n-1}t'_{ww}$$

Momentum equation:

# What Does 500+ Sheets of A3 Give You?

White-Metzner Equations:

$$2\text{Wi}f''|f''|^{n-1}t_{uw} = [n - 2\text{Wi}f'|f''|^{n-1}((3 - 2\alpha)n + \alpha - 1)](f')^2 t_{uu} \\ - (2(2 - \alpha)n + \alpha - 1)\text{Wi}f(f')^2 |f''|^{n-1}t'_{uu}.$$

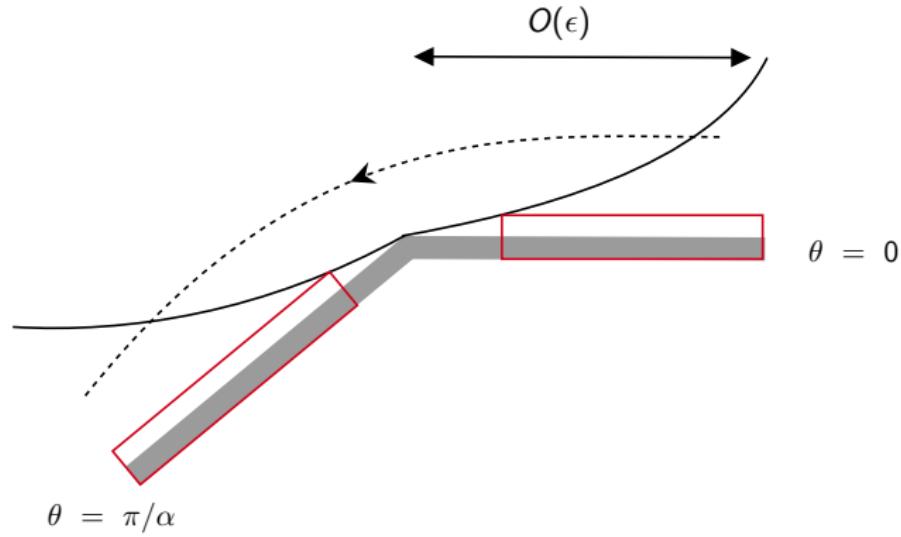
$$n\text{Wi}f''|f''|^{n-1}t_{ww} = [n + \text{Wi}(\alpha - 1)nf'|f''|^{n-1}](f')^2 t_{uw} \\ - (2(2 - \alpha)n + \alpha - 1)\text{Wi}f(f')^2 |f''|^{n-1}t'_{uw}.$$

$$n(f')^2 = nt_{ww} + 2((2 - \alpha)n + (\alpha - 1))\text{Wi}f'|f''|^{n-1}t_{ww} \\ - (2(2 - \alpha)n + \alpha - 1)f|f''|^{n-1}t'_{ww}$$

Momentum equation:

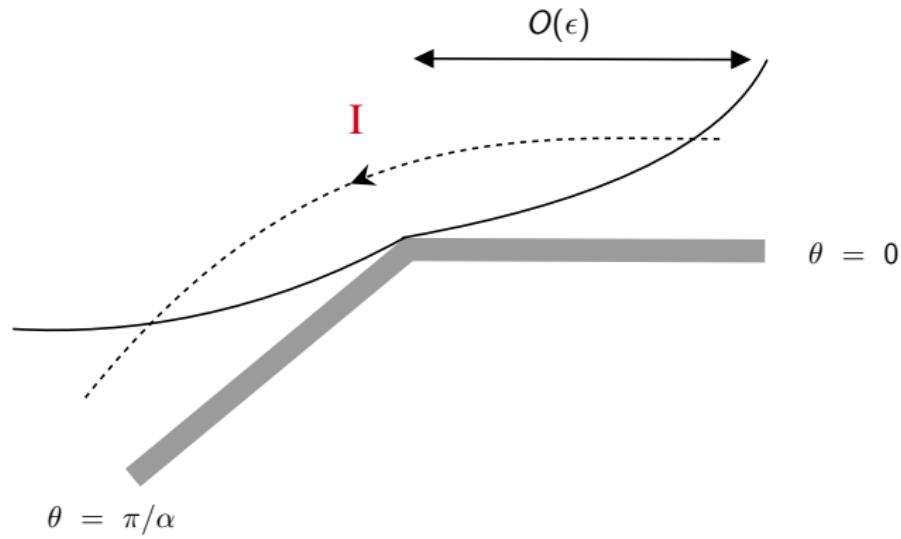
$$nt'_{uw} = 2n(\alpha - 1)\text{Wi}p_0 + [(4 - 2\alpha)n + \alpha - 1]ff't'_{uu} \\ + [(4 - 3\alpha)n + (\alpha - 1)](f')^2 t_{uu} \\ + [2(2 - \alpha)n + \alpha - 1]ff''t_{uu}.$$

# So What Can I Tell You?



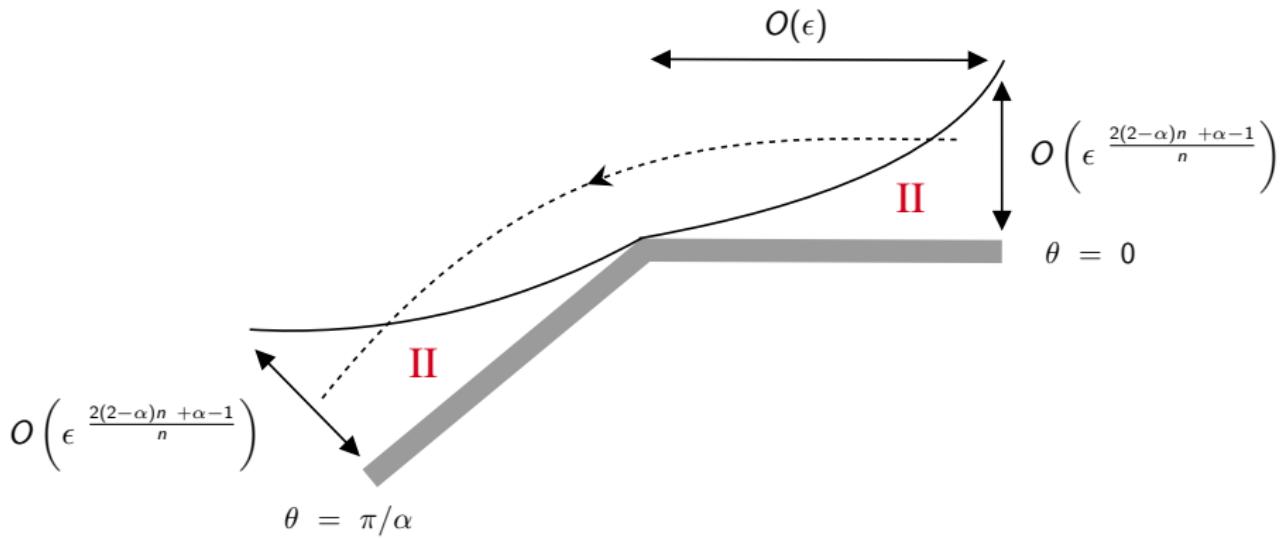
1. Flow near walls is (to leading order) simple shear.

# So What Can I Tell You?



2. Fluid behaves elastically as it flows round the corner (Region I).

# So What Can I Tell You?



- 3. Viscous effects remain important in Regions II. Similarity equations tell us the velocity/stresses in the fluid!

# A Final Thought

Complex fluids are complex...

## A Final Thought

Complex fluids are complex...but they aren't scary!

Thank you for listening!



Diolch yn fawr i wrando!

# References

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iStock, 2021 '*Why Do Dogs Drool?*' [Online]. East Sacramento Veterinary Center. Available from: <https://www.eastsacvet.com/blog/why-do-dogs-drool/> [Accessed 03-10-23]

## Tendons:

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