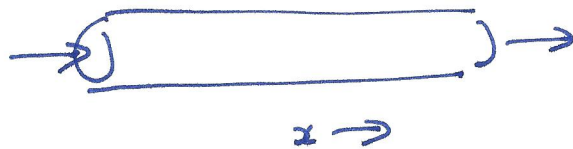


Lecture 4

(optional)

Method of characteristics for higher order PDE

Example from 1-D gas flow in a tube



ρ density, u velocity in x -direction

ρu momentum per unit volume

Conservation of mass

$$\frac{\partial}{\partial t} A \Delta x \rho = - (\text{flux of mass out} - \text{flux in})$$

$$= - [A \rho u]_{x+\Delta x} - A \rho u|_x]$$

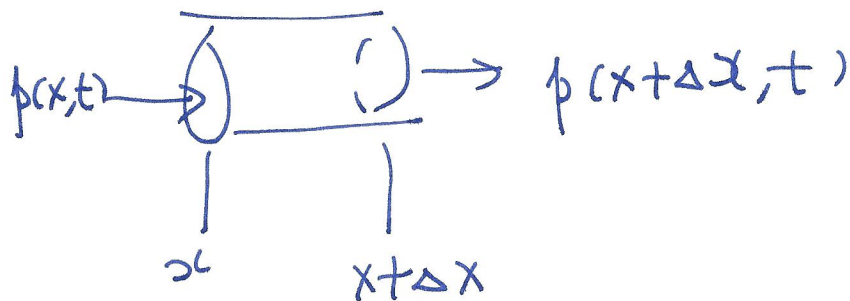
$$\Delta x \rightarrow 0, \quad \boxed{\frac{\partial}{\partial t} \rho = - \frac{\partial}{\partial x} (\rho u)}$$

Conservation of momentum

$$\frac{\partial}{\partial t} A \Delta x \rho u = - (\text{flux of momentum out} - \text{flux in}) + \text{pressure force}$$

$$\boxed{\frac{\partial}{\partial t} \rho u = - \frac{\partial}{\partial x} (\rho u u) - \frac{\partial}{\partial x} p}$$

Pressure force



Net pressure force on the volume of fluid

$$A p(x, t) - A p(x + \Delta x, t)$$

$$= A [p(x, t) - p(x + \Delta x, t)]$$

$$= A \Delta x \frac{[p(x, t) - p(x + \Delta x, t)]}{\Delta x}$$

$$= -A \frac{\partial p}{\partial x} \Delta x \quad \text{as } \Delta x \rightarrow 0$$

Equation of state

$$p = p(\rho)$$

[For isentropic flow , $p = p(\rho) = A\rho^\gamma$]

$$\text{let } c^2 \equiv \frac{dp}{d\rho}$$

$$\left[\begin{aligned} \left(\frac{\partial}{\partial t} + u \frac{\partial}{\partial x} \right) u + \frac{c^2}{\rho} \frac{\partial}{\partial x} \rho &= 0 \\ \left(\frac{\partial}{\partial t} + u \frac{\partial}{\partial x} \right) \rho + \rho \frac{\partial}{\partial x} u &= 0 \end{aligned} \right]$$

A set of two coupled nonlinear PDEs

Riemann Invariants

Chapter 7 Kevorkian

Let $\xi = \text{constant}$ be curves along which

$$\frac{dx}{dt} = u - c$$

and $\eta = \text{const}$ be curves along which

$$\frac{dx}{dt} = u + c$$

Now
$$du = dx \frac{\partial u}{\partial x} + dt \frac{\partial u}{\partial t}$$

$$dp = dx \frac{\partial p}{\partial x} + dt \frac{\partial p}{\partial t}$$

Along $\xi = \text{const}$, substitute $\frac{dx}{dt} = u - c$

$$du = dt \left[\frac{\partial}{\partial t} + (u - c) \frac{\partial}{\partial x} \right] u$$

$$dp = dt \left[\frac{\partial}{\partial t} + (u - c) \frac{\partial}{\partial x} \right] p$$

So
$$du - \frac{c}{p} dp = dt \left\{ \left(\frac{\partial}{\partial t} + u \frac{\partial}{\partial x} \right) u + \frac{c^2}{p} \frac{\partial}{\partial x} p - c \frac{\partial}{\partial x} u - \frac{c}{p} \left(\frac{\partial}{\partial t} + u \frac{\partial}{\partial x} \right) p \right\} = 0$$

More details:

$$du = dt \left[\frac{\partial}{\partial t} + (u-c) \frac{\partial}{\partial x} \right] u \text{ along } \xi = \text{const}$$

but the momentum equation is

$$\left(\frac{\partial}{\partial t} + u \frac{\partial}{\partial x} \right) u = - \frac{c^2}{\rho} \frac{\partial}{\partial x} \rho$$

$$\text{So } du = dt \left[- \frac{c^2}{\rho} \frac{\partial}{\partial x} \rho - c \frac{\partial}{\partial x} u \right]$$

$$dp = dt \left[\frac{\partial}{\partial t} + (u-c) \frac{\partial}{\partial x} \right] p$$

but the mass equation is

$$\left(\frac{\partial}{\partial t} + u \frac{\partial}{\partial x} \right) \rho = - \rho \frac{\partial}{\partial x} u$$

$$\text{So } dp = dt \left[- \rho \frac{\partial}{\partial x} u - c \frac{\partial}{\partial x} \rho \right]$$

$$\begin{aligned} du - \frac{c}{\rho} dp &= dt \left[- \frac{c^2}{\rho} \frac{\partial}{\partial x} \rho - c \frac{\partial}{\partial x} u \right. \\ &\quad \left. + \frac{c^2}{\rho} \frac{\partial}{\partial x} \rho + c \frac{\partial}{\partial x} u \right] = 0 \end{aligned}$$

$$\boxed{du - \frac{c}{\rho} d\rho = 0} \text{ along } \xi : \frac{dx}{dt} = u - c$$

Similarly

$$\boxed{du + \frac{c}{\rho} d\rho = 0} \text{ along } \eta : \frac{dx}{dt} = u + c$$

Along $\xi = \text{const}$

$$\frac{du}{d\rho} = \frac{c}{\rho} \quad \sim \quad u - \int \frac{c}{\rho} d\rho = \text{const.}$$

For isentropic fluid, $c^2 \equiv \frac{dp}{d\rho} = A r \rho^{r-1}$

$$\frac{c}{\rho} = (A r)^{1/2} \rho^{\frac{r}{2} - \frac{3}{2}}$$

$$\begin{aligned} \int \frac{c}{\rho} d\rho &= \int (A r)^{1/2} \rho^{\frac{r}{2} - \frac{3}{2}} d\rho \\ &= (A r)^{1/2} \rho^{\frac{r}{2} - \frac{1}{2}} / \left(\frac{r}{2} - \frac{1}{2} \right) \\ &= \frac{2c}{r-1} \end{aligned}$$

Along $\xi = \text{const}$

$$R_1 \equiv \frac{u}{2} - \frac{c}{\gamma-1} = \text{const}$$

Along $\eta = \text{const}$

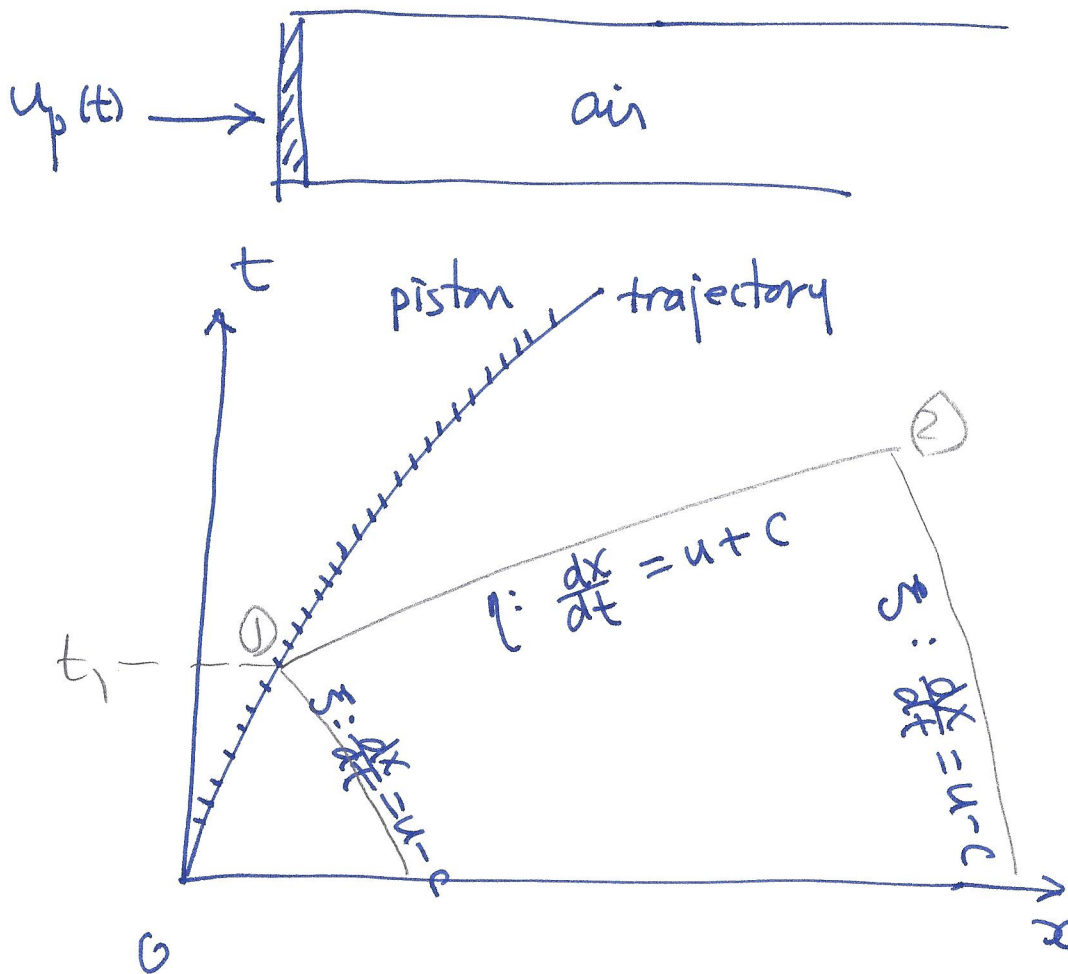
$$R_2 \equiv \frac{u}{2} + \frac{c}{\gamma-1} = \text{const}.$$

These are called the Riemann invariants.

u and c are the two unknowns

(p can be calculated once c is known)

Example shock tube driven by a piston.



Consider the characteristic $\xi = \text{const}$ intersecting $\textcircled{1}$

$$x_1 = \frac{u}{2} - \frac{c}{\gamma - 1} = \frac{u_p(t_1)}{2} - \frac{c_p(t_1)}{\gamma - 1}$$

also intersecting $t=0$: $= -\frac{c_0}{\gamma - 1}$

So. $c_p(t_1) - \frac{\gamma - 1}{2} u_p(t_1) = c_0$

At ②, along $\xi = \text{const}$

$$R_1 = \frac{u}{2} - \frac{c}{r-1} = -\frac{c_0}{r-1}$$

Also at ②, but along ①-② where $\eta = \text{const}$

$$R_2 = \frac{u}{2} + \frac{c}{r-1} = \frac{u_p(t_1)}{2} + \frac{c_p(t_1)}{r-1}$$

subtract to get rid of u

$$\frac{2c}{r-1} = \frac{c_0}{r-1} + \frac{c_p(t_1)}{r-1} + \cancel{\frac{r-1}{2}} \frac{u_p(t_1)}{2}$$

Since $c_p(t_1) = c_0 + \frac{r-1}{2} u_p(t_1)$ from previous

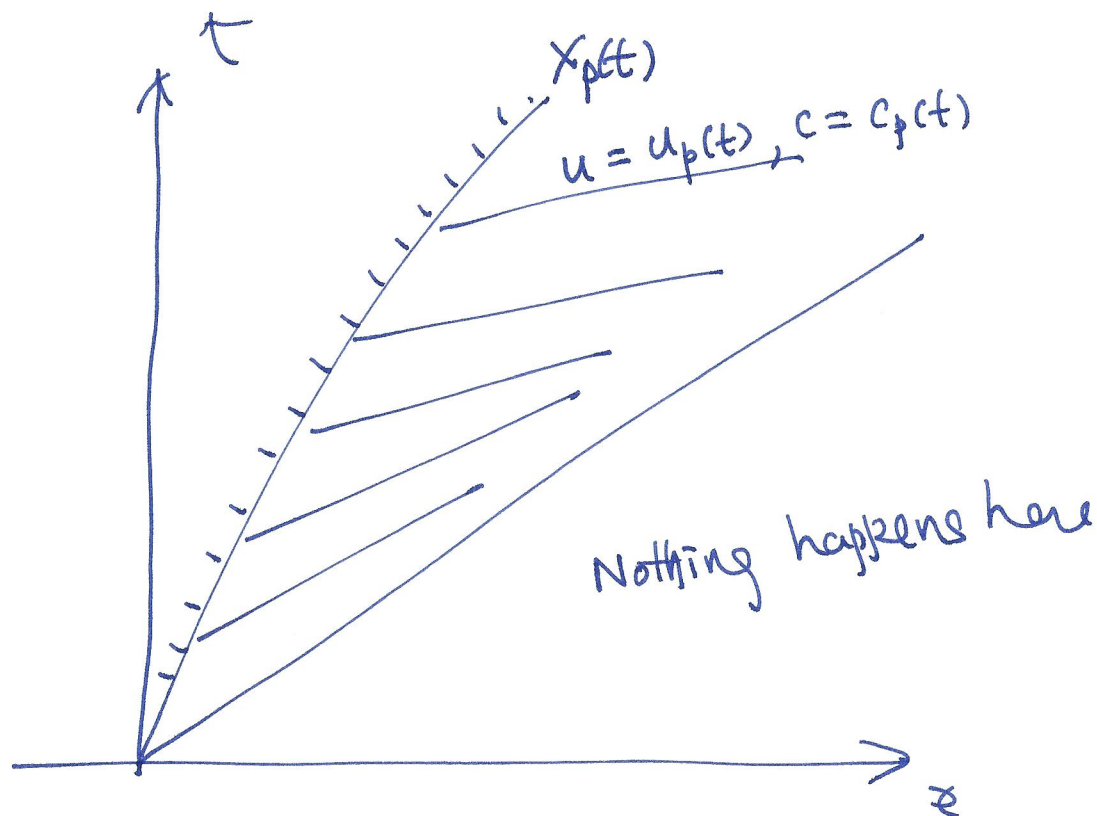
$$\frac{2c}{r-1} = \frac{2c_p(t_1)}{r-1}$$

$$\sim \boxed{\begin{array}{l} c = c_p(t_1) \\ u = u_p(t_1) \end{array}}$$

along ①-②

Therefore ①-② : $\frac{dx}{dt} = u + c = u_p(t_1) + c_p(t_1) = \text{const}.$

This characteristic is a straight line



characteristics are straight lines
but the slope may depend on $u_p(t)$.

Example :

$$u_p(t) = \bar{U} \sin \omega t$$

$$x_p = \int_0^t u_p(t) dt$$

$$= \frac{\bar{U}}{\omega} (1 - \cos \omega t)$$

