

# Investigations on one-way coupling effects of particle-laden decaying isotropic turbulent flows

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## 1 Nomenclature

## **2 Introduction**

in Computational Methods for Multiphase Flow ist auf den Seiten 3-9 ein interessantes Beispiel.

### 3 Mathematical models

Sollen wir hier noch isotrope Turbulenz etc. erklären?

#### 3.1 Single-phase flow

In this section the mathematical basics for understanding and simulating turbulent flows are discussed. However, it should be pointed out that this is no complete treatise of the mathematical and physical basics. The reader can achieve further insight on this topic by looking at different books and papers, e.g. [?].

##### 3.1.1 The Navier-Stokes equations

The Navier-Stokes-Equations are of great importance for understanding turbulent phenomena. This set of equations exists in forms for compressible and incompressible fluids. For an infinitesimal small volume element  $d\tau$  and using the cartesian coordinate system, they can be written in the so-called 'divergence form':

$$\frac{\partial \mathbf{Q}}{\partial t} + \nabla \mathbf{H} = 0 \quad (3.1)$$

It should be noted by the reader that this work only contains investigations about chemically inert fluids and particles, and that the simulation results only fit under this condition. The vector  $\mathbf{Q}$  contains all the variables which are conserved, i.e. the density  $\rho$ , the velocity  $\mathbf{u}$  and the specific inner energy  $E$ :

$$\mathbf{Q} = \begin{pmatrix} \rho \\ \rho \mathbf{u} \\ \rho E \end{pmatrix} \quad (3.2)$$

$\mathbf{H}$  is the flux vector which stores all the floating variables and may be split up into two parts:

$$\mathbf{H} = \mathbf{H}^i + \mathbf{H}^v \quad (3.3)$$

The contents of the two vectors are displayed below:

$$\mathbf{H}^i = \begin{pmatrix} \rho \mathbf{u} \\ \rho \mathbf{u} \mathbf{u} + p \\ \mathbf{u}(\rho E + p) \end{pmatrix} \quad (3.4)$$

$$\mathbf{H}^v = -\frac{1}{Re} \begin{pmatrix} 0 \\ \boldsymbol{\tau} \\ \boldsymbol{\tau} \mathbf{u} + \mathbf{q} \end{pmatrix} \quad (3.5)$$

$\mathbf{H}^i$  is called inviscid flux and contains only the variables that are independent of the fluids viscosity, it describes the way a fluid with zero viscosity would behave. In contrast, the viscous flux  $\mathbf{H}^v$  represents the effects of viscosity. The Reynolds number  $Re = \frac{\rho v d}{\eta}$  is defined to be the ratio of inertia to tenacity, which makes it very valuable for understanding turbulent flows. This is also due to the fact that two familiar objects with the same Reynolds number behave similar in turbulence. One can assume that flows with  $Re \ll 1$  are laminar and

flows with  $Re \gg 1$  are turbulent. To solve the Navier-Stokes-Equations, more information regarding some variables is required. For Calculating the specific inner Energy  $E$  and the heat conduction  $\mathbf{q}$ , the following equations are used:

$$E = e \frac{1}{2} |\mathbf{u}|^2 \quad (3.6)$$

$$\mathbf{q} = -\frac{\mu}{Pr(\gamma - 1)} \nabla T \quad (3.7)$$

with

$$\gamma = \frac{c_p}{c_v} \quad (3.8)$$

and the Prandtl number

$$Pr = \frac{\mu_\infty c_p}{k_t} \quad (3.9)$$

using the specific heat capacities of the fluid  $c_v$  and  $c_p$ . If one could assume that the fluid is a newtonian fluid, the linear correlation between stress and the rate of strain results in:

$$\boldsymbol{\tau} = 2\mu \mathbf{S} - \frac{2}{3}\mu(\nabla \cdot \mathbf{u})\mathbf{I} \quad (3.10)$$

in which  $\mathbf{S} = \frac{(\nabla \mathbf{u})(\nabla \mathbf{u})^T}{2}$  denotes the rate-of-strain-tensor. Additionally, the viscosity  $\mu$  can be approximated through Sutherland's law, which is based on the ideal gas-theory:

$$\mu(T) = \mu_\infty \left(\frac{T}{t_\infty}\right)^{3/2} \frac{T_\infty + S}{T + S} \quad (3.11)$$

$S$  is in this case the Sutherland temperature. To achieve closure the caloric state equation  $e = c_v T$  and the state equation for an ideal gas  $p = \rho R T$  are used. The specific gas constant is determined by  $R = c_p - c_v$ . These equations form a set of partial differential equations, so for solving them starting values are needed. These are initialized at the first timestep of the simulation. To achieve physical solutions, 150 timesteps are computed before the particles are initialized, so the turbulence can evolve from the synthetic values to a natural flow field.

Christoph Siewert: -2.1 bis 2.6 Stephan Fritz: -Navier-Stokes-Gleichungen (Anhang B) Randbedingungen?

### 3.2 Particle dynamics

Siewert: -3.1a-3.14 (spherical particles) OHNE GRAVITATION Stokes Drag/Stokes Coefficient Filterung (Fritz) -; Viskosität durch numerischen Fehler, Smagorinsky nicht benutzen

To get a useful equation of motion for the particles in the flow, we use the Euler Lagrangian approach, as it is common in Direct Numerical Simulations (DNS) and Large Eddy Simulations (LES). In this work we deal with small and heavy particles, that have a spherical shape. Their radius  $r_p$  is even smaller than the Kolmogorov scale  $\eta$ , but also large enough to neglect the Brownian motion. The density of the particles  $\rho_p$  is much higher than that of the fluid  $\rho_f$ . In addition due to the very low particle concentration we can neglect the influence of the particles on the mean flow and on each other. This simplification is called one-way coupling. That means that the particles can cross each other without any effect. That means particle collisions are neglected. After all these simplifications we obtain a simplified version of the Maxey-Riley equations.

$$\frac{\partial \mathbf{x}_p}{\partial t} = \mathbf{v}_p \quad (3.12)$$

$$\frac{\partial \mathbf{v}_p}{\partial t} = \frac{f_D}{\tau_p} (\mathbf{u}(\mathbf{x}_p) - \mathbf{v}_p) \quad (3.13)$$

It shows that the particle motion is only depending on the hydrodynamical drag force which results out of the actual difference between the fluid velocity  $\mathbf{u}(\mathbf{x}_p)$  at particle position  $\mathbf{x}_p$  and the particle velocity  $\mathbf{v}_p$ .  $\tau_p$  is the particle response time and a factor to obtain the drag force in Stokes flow conditions. To take the case of an Reynolds number  $\mathcal{R}$  of order 1 into account the correction factor

$$f_D = 1 + 0.15 Re_p^{0.687} \quad (3.14)$$

is used. The biggest simplification of this Lagrangian approach is that the interaction of particles coming close together is neglected.

## 4 Numerical methods

To simulate flows like those described above we have two options. The direct numerical simulation (DNS) is the easier one to understand, although it is numerically very expensive. The Large-eddy simulation (LES) is numerically more capable, still we must accept certain inaccuracies. These two numerical methods are now discussed in the following chapter.

### 4.1 Direct numerical simulation

The basis of the direct numerical simulation (DNS) are the Navier-Stokes equations as described above. The idea is that the computer is very good at calculating and solves these equations completely. This provides us a very accurate result, as all scales of motion are being resolved. Still it requires an immense level of computational resources which increases rapidly with the Reynolds number. These computational resources were not available until the 1970s [?].

Pojektion (noComputationalParticles) implizite LES (Motivation fuer LES -



Pope Chapter 9, Bild 9.4), DNS

## 5 Results

Graphen (particleFree rot, Laden gruen)

## 6 Conclusion

## 7 References