

## Chapter 9: Introduction to Control

July 24, 2015

# Outline

- 1 Basics
  - Control Theory
  - Demo: Inverted Pendulum
- 2 Control Goals
  - Stability
  - Disturbance rejection
  - Reference tracking
  - Exercise
- 3 Closed-loop systems
  - Sensitivity
  - Robustness
  - Types of systems and Steady State Error
  - Noise- and disturbance rejection

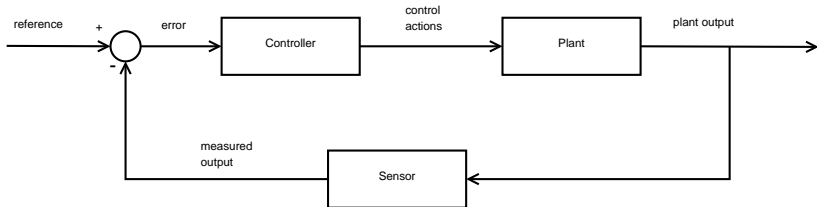
# An introduction to control

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# What is control theory?

**Control theory** is an interdisciplinary branch of engineering and mathematics that deals with the behavior of dynamical systems with inputs, and how their behavior is modified by feedback. The usual objective of control theory is to design a controller to produces inputs to the plant so its output follows a desired reference signal which may be a fixed or changing value. - wikipedia



# Controllers

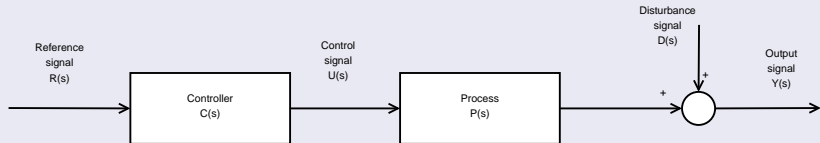
## Types of controllers

- On-off controller
  - e.g., Thermostate at home
- **PID controllers, Lead and lag compensators (this course)**
  - Cruise-control in your car
  - Temperature, level, flow, pressure, pH, ... in chemical plants.
- More advanced controllers
  - State-space feedback controllers (e.g., LQR)
  - Model Predictive Controller (MPC)
  - Fuzzy Control
  - Neuro-fuzzy Control
  - ...

# Open-loop System

## Definition

In an open loop control system the actual output signal  $Y(s)$  has no effect on the control action.



$$Y(s) = P(s)U(s) = P(s)C(s)R(s)$$

# Open-loop System

## Example

- You are pouring a glass of water, but you **cannot look at the glass**.
- The desired output is a full glass of water within a reasonable time.
- The input can have two values: on or off (assume a quite primitive tap).
- It will not be easy to do this successfully.



The solution is evident: look at the glass while pouring!

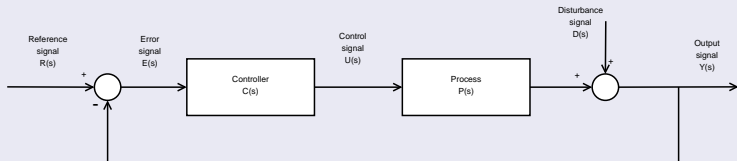


# A general set-up of a closed loop system

## Definition

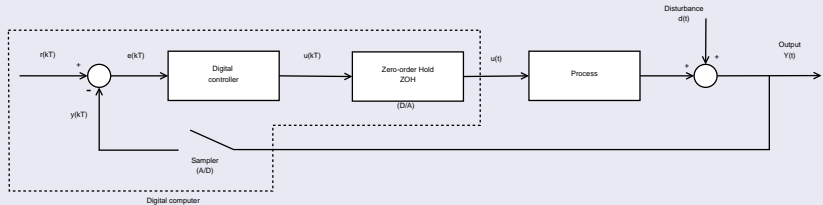
In a closed-loop system the output of the controller is influenced by the output of the system using a negative feedback loop.

## Classical control-loop



$$\frac{Y(s)}{R(s)} = \frac{P(s)C(s)}{1 + P(s)C(s)}R(s) + \frac{1}{1 + P(s)C(s)}D(s)$$

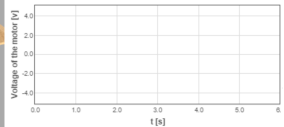
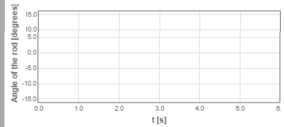
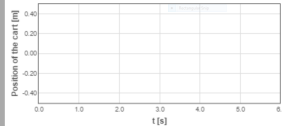
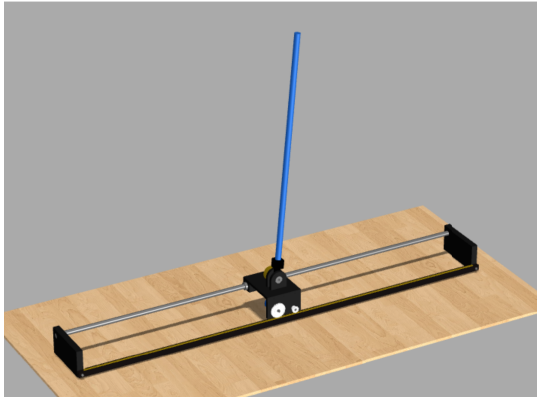
## Digital Control Loop



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### Virtual Lab: Inverted Pendulum



Simulation	Setpoint of the cart [m]	Disturbance	Initial conditions	Camera view	Controller $u(t) = -K(x(t) - x_d(t))$
<div>Start</div> <div>Stop</div> <div>Reset</div>	<input checked="" type="radio"/> Random Steps <input type="radio"/> Manual : 0	<div>Push</div> <div>Push</div> <div>&lt;</div> <div>&gt;</div>	Cart position [m]: 0 Rod angle [deg]: 5	<div>Default</div> <div>Front</div> <div>Top</div>	<div> <math>k1: -9.1287</math>  <math>k3: -14.9912</math> </div> <div> <math>k2: -52.4975</math>  <math>k4: -6.3533</math> </div> <div>Default</div>

KU Leuven/ESAT  
Oscar Mauricio Agudelo  
Bart De Moor

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# What is good control?

## Depends on the application

- Stability
- Disturbance rejection
- Reference tracking
- Sensitivity to errors in the model
- ...

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## Examples: stability



Space shuttles are like inverted pendulums. Control systems make sure they do not flip over.



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## Examples: Disturbance rejection

- Your body will try to keep your internal temperature as constant as possible, no matter how hot/cold it is outside.



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## Examples: Reference tracking



Audi has a system for automatic driving in traffic jams. The audi will follow the car in front of him at an appropriate distance.

[https://www.youtube.com/watch?v=Qa\\_ZSRj0WMO](https://www.youtube.com/watch?v=Qa_ZSRj0WMO)

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## Exercise: name the correct property

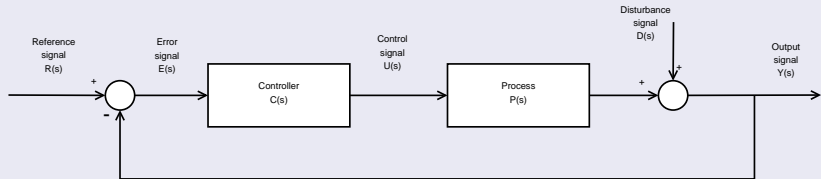


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# Transfer function of a closed-loop system

## Classical control loop



$$Y(s) - D(s) = P(s)U(s) \quad \text{with } U(s) = C(s)E(s)$$

$$Y(s) - D(s) = P(s)C(s)E(s) \quad \text{with } E(s) = R(s) - Y(s)$$



$$Y(s) - D(s) = P(s)C(s)(R(s) - Y(s))$$

$$Y(s) - D(s) = P(s)C(s)R(s) - P(s)C(s)Y(s)$$

$$Y(s) = \frac{P(s)C(s)}{1 + P(s)C(s)}R(s) + \frac{1}{1 + P(s)C(s)}D(s)$$

# Transfer function from $R(s)$ to $Y(s)$

## Definition

We define  $H$  as the transfer function from  $R(s)$  to  $Y(s)$

$$H(s) \triangleq \frac{Y(s)}{R(s)} = \frac{P(s)C(s)}{1 + P(s)C(s)} \quad \text{when } D(s) = 0$$

This transfer function  $H(s)$  will help us to evaluate tracking  
Almost perfect tracking: the output  $Y(s)$  will follow  $R(s)$  very closely  $\Rightarrow H(s) \approx 1$

# Transfer function from $D(s)$ to $Y(s)$

## Definition

We define  $M(s)$  as the transfer function from  $D(s)$  to  $Y(s)$ .

$$M(s) \triangleq \frac{Y(s)}{D(s)} = \frac{1}{1 + P(s)C(s)} \quad \text{when } R(s) = 0$$

If the disturbance rejection of the control system is very good the disturbances will have almost no effect on the output  $\Rightarrow M(s) \approx 0$

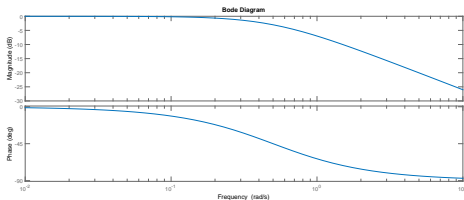
$$\begin{cases} |H(j\omega)| \cong 1 \\ |M(j\omega)| \cong 0 \end{cases}$$

$\Rightarrow |P(j\omega)C(j\omega)|$  (**open loop gain**) is very large.

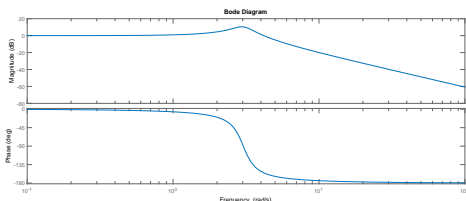
! a large open loop amplification might lead to an unstable system

# Example: Which controller do you prefer

The transfer function from  $R(s)$  to  $Y(s)$  for two different controllers for high precision surgery



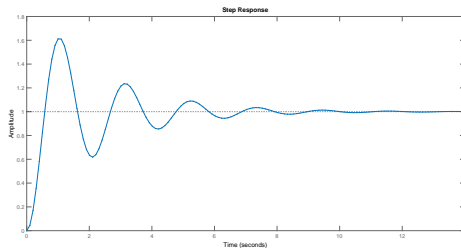
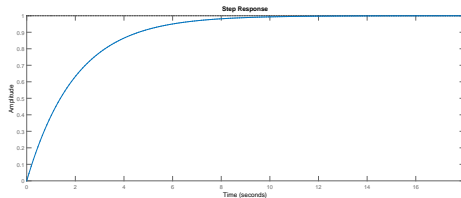
$$\frac{0.5}{s + 0.5}$$



$$\frac{10}{1.09s^2 + s + 10}$$

## Example: step response of both controllers

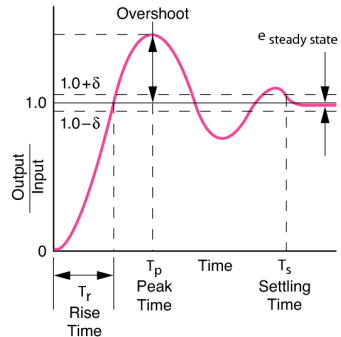
The output  $Y(s)$  when  $R(s)$  is a step function.



# Quality of reference tracking

Look at the step response of the transfer function from  $R(s)$  to  $Y(s)$ . The quality can be determined using these criteria:

- Rise-time
- Settling time
- Steady state error
- Overshoot
- ...



# Model errors

- In practice, the transfer function  $P(s)$  is often unknown. It is important to know how model errors affect the result. Sensitivity and robustness are key concepts to evaluate these effects.
- Sensitivity
  - Quantifies the effect of small model errors on the output.
- Robustness
  - Refers to bigger changes of the model. A controller is robust if it works properly over a given set of parameters.

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# Sensitivity

Sensitivity is a measure of the effect of a (small) disturbance on the model (e.g. variations in the process parameters)

$$Y(s) + \Delta Y(s) = \frac{(P(s) + \Delta P(s))C(s)}{1 + (P(s) + \Delta P(s))C(s)} R(s) + \frac{1}{1 + (P(s) + \Delta P(s))C(s)} D(s)$$

Look at the effect on the system without disturbances ( $D(s)=0$ )

$$\Delta Y(s) = \frac{(P(s) + \Delta P(s))C(s)}{1 + (P(s) + \Delta P(s))C(s)} R(s) - \frac{P(s)C(s)}{1 + P(s)C(s)} R(s)$$

# Sensitivity

$$\begin{aligned}
 &= \frac{(P(s) + \Delta P(s))C(s)(1 + P(s)C(s)) - P(s)C(s) - P(s)C(s)(P(s) + \Delta P(s))C(s)}{(1 + (P(s) + \Delta P(s))C(s))(1 + P(s)C(s))} R(s) \\
 &= \frac{\Delta P(s)C(s)}{(1 + (P(s) + \Delta P(s))C(s))(1 + P(s)C(s))} R(s) \\
 &= Y(s) \frac{\Delta P(s)}{P(s)} \frac{1}{1 + (P(s) + \Delta P(s))C(s)}
 \end{aligned}$$

# Sensitivity

Now take the relative change due to this disturbance of the model and take the limit for  $\partial x \rightarrow 0$ ; this gives the following (measure of the) sensitivity:

$$S_P^Y(s) = \frac{\frac{\partial Y}{Y}(s)}{\frac{\partial P}{P}(s)} = \frac{\partial Y}{\partial P}(s) \cdot \frac{P(s)}{Y(s)} = \frac{1}{1 + P(s)C(s)}$$

- Again, a very large  $|P(s)C(s)|$  looks like a good choice, but again there is a risk for instability!
- Note that the sensitivity can be determined for any parameter

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## Example 1: robustness

### Example

Suppose we want to stabilize the system  $P(s) = \frac{1}{(s-a)}$ . We only know that  $a \in [0.20; 0.80]$ . We propose to use a proportional controller  $C(s) = K$ . The closed loop transfer function becomes

$$S(s) = \frac{P(s)C(s)}{1 + P(s)C(s)} = \frac{\frac{1}{s-a}K}{1 + \frac{1}{s-a}K} = \frac{K}{s - a + K}$$

The controller stabilizes the system if  $-a + K > 0$ . If we choose  $K$  very large the system will be robust against changes in  $a$ .

## Example 2: robustness

### Example

Suppose we want to stabilize the system  $P(s) = \frac{s}{(s-a)}$  with  $a \in [0.20; 0.80]$ . If we choose the control law  $C(s) = \frac{K}{s}$  this results in the same transfer function.

$$S(s) = \frac{P(s)C(s)}{1 + P(s)C(s)} = \frac{\frac{s}{s-a} \frac{K}{s}}{1 + \frac{s}{s-a} \frac{K}{s}} = \frac{K}{s - a + K}$$

Again we choose  $K > a$  to ensure stability. But how does the controller perform on the slightly perturbed system  $\tilde{P}(s) = \frac{(s+\epsilon)}{(s-a)}$  ?  
The transfer function from  $R(s)$  to  $Y(s)$  becomes

$$S(s) = \frac{\frac{s+\epsilon}{s-a} \frac{K}{s}}{1 + \frac{s+\epsilon}{s-a} \frac{K}{s}} = \frac{(s+\epsilon)K}{s^2 + (K-a)s + \epsilon K}$$

## Example 2: robustness

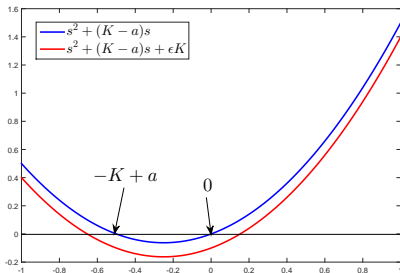
$$\tilde{S}(s) = \frac{(s + \epsilon)K}{s^2 + (K - a)s + \epsilon K}$$

The figure on the right plots

$$s^2 + (K - a)s$$

$$s^2 + (K - a)s + \epsilon K$$

For  $\epsilon$  negative the system becomes unstable. The control system is not robust and useless in practical situations. You shouldn't use control laws which rely on a pole-zero cancellation.



# Robustness of steady-state error

## Definition

The steady state error is defined as follows:

$$\begin{aligned}\lim_{t \rightarrow \infty} e(t) &= \lim_{t \rightarrow \infty} (r(t) - y(t)) \\ &= \lim_{s \rightarrow 0} s(R(s) - Y(s)) \quad (\text{final value theorem})\end{aligned}$$



A very small steady state error (preferably zero) indicates that the controller tracks the reference very well

For the open loop system with a step reference

$$e_{ol}(\infty) = \lim_{s \rightarrow 0} s(1 - C(s)P(s))R(s) = 1 - C(0)P(0)$$

- So the open loop controller can be free of a steady state error (for a step reference  $\epsilon(t)$ ) by calibrating the controller such that  $C(0)P(0) = 1$
- $\Rightarrow$  a precise calibration of the DC gain

# Steady state error

Closed loop system:

$$\begin{aligned} e_{cl}(\infty) &= \lim_{s \rightarrow 0} s \left( 1 - \frac{C(s)P(s)}{1 + C(s)P(s)} \right) R(s) \\ &= \lim_{s \rightarrow 0} \frac{s}{1 + C(s)P(s)} R(s) = \frac{1}{1 + C(0)P(0)} \end{aligned}$$

- The steady state error is small if  $C(0)P(0)$  is very large
- Again, calibrating the DC gain
- The difference is that here we only need a large gain, which is far less demanding than having to make it equal to 1

# An open loop controller is not robust

- We can now show how this results in a great advantage of the closed loop strategy over the open loop strategy:
  - If  $P$  changes slightly (for instance due to a factor that has not been taken up into the model) to  $P + \Delta P$
  - Then making  $e_{ol}(\infty)$  small would require to calibrate anew
  - Whereas  $e_{cl}(\infty)$  would remain small, as long as  $(P(0) + \Delta P(0))C(0)$  remains large
- Hence an open loop controller can not control the output **robustly** against changes in  $P$

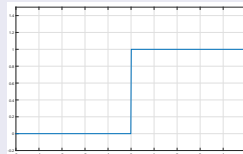
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# Steady state error: step

## Definition

$$\epsilon(t) = \begin{cases} 0, & t \leq 0 \\ \frac{1}{2}, & t = 0 \\ 1, & t \geq 0 \end{cases}$$



- For a step reference  $r(t) = A\epsilon(t) \Rightarrow R(s) = \frac{A}{s}$

$$e_{cl}(\infty) = \frac{A}{1 + C(0)P(0)}$$

So  $e_{cl}(\infty) = 0$  if  $C(s)P(s)$  has a least one pole in zero  
( $C(0)P(0) \rightarrow \infty$ )

## Steady state error: ramp

- For a ramp reference function  $r(t) = At\epsilon(t) \Rightarrow R(s) = \frac{A}{s^2}$ , we have

$$e_{cl}(\infty) = \lim_{s \rightarrow 0} \frac{s}{1 + C(s)P(s)} \frac{A}{s^2}$$

So  $e_{cl}(\infty) = 0$  if  $C(s)P(s)$  has at least two poles in zero.  
 $\left( \lim_{s \rightarrow 0} sC(s)P(s) = \infty \right)$

# Type of a system

- The type of a system is determined by the number of poles  $P(s)C(s)$  has in zero, and hence it is linked to what type of references it can track perfectly
- Write  $P(s)C(s)$  as  $\frac{K \prod_{k=1}^m (s-z_k)}{s^l \prod_{k=1}^{n-l} (s-p_k)}$  with  $l$  the amount of poles in zero
- We say this system is of type  $l$ 
  - It will be able to track references of shape  $At^0\epsilon(t)$  up to  $At^{(l-1)}\epsilon(t)$  perfectly (for  $t \rightarrow \infty$ ,  $\lim_{t \rightarrow \infty} e_{cl}(t) = 0$ )
  - A reference of shape  $At^l\epsilon(t)$  will be missed by a finite factor (for  $t \rightarrow \infty$ ,  $\lim_{t \rightarrow \infty} e_{cl}(t) = C$ )
  - A reference of shape  $At^{l+\dots}\epsilon(t)$  will be missed by infinity (for  $t \rightarrow \infty$ ,  $\lim_{t \rightarrow \infty} e_{cl}(t) = \infty$ )

## Example of a type 0 system

- Step reference  $r(t) = A\epsilon(t) \Rightarrow R(s) = \frac{A}{s}$

$$\begin{aligned} e_{cl}(\infty) &= \lim_{s \rightarrow 0} \frac{s}{1 + C(s)P(s)} \frac{A}{s} \\ &= \lim_{s \rightarrow 0} \frac{A}{1 + \frac{K \prod_{k=1}^m (-z_k)}{\prod_{k=1}^{n-l} (-p_k)}} = \frac{A}{1 + K_p} \end{aligned}$$

with  $K_p$  the static position constant

- Ramp reference  $r(t) = At\epsilon(t) \Rightarrow R(s) = \frac{A}{s^2}$

$$\begin{aligned} e_{cl}(\infty) &= \lim_{s \rightarrow 0} \frac{s}{1 + C(s)P(s)} \frac{A}{s^2} \\ &= \lim_{s \rightarrow 0} \frac{1}{1 + \frac{K \prod_{k=1}^m (-z_k)}{\prod_{k=1}^{n-l} (-p_k)}} = \infty \end{aligned}$$



# Steady state errors - type of a system

- With:

$$K_p = \lim_{s \rightarrow 0} P(s)C(s) \quad K_p = \text{Static position constant}$$

$$K_v = \lim_{s \rightarrow 0} sP(s)C(s) \quad K_v = \text{Static velocity constant}$$

$$K_a = \lim_{s \rightarrow 0} s^2 P(s)C(s) \quad K_a = \text{Static acceleration constant}$$

- And the respective steady state errors for different system types are:

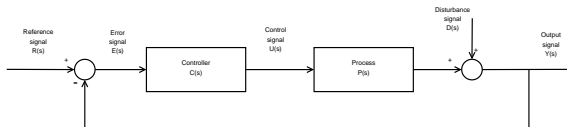
Type I	Step $A\epsilon(t)$	Ramp $At\epsilon(t)$	Parabola $\frac{At^2\epsilon(t)}{2}$
0	$\frac{A}{1+K_p}$	$\infty$	$\infty$
1	0	$\frac{A}{K_v}$	$\infty$
2	0	0	$\frac{A}{K_a}$

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# Noise rejection and disturbance rejection

- Both refer to rejection of the input  $D$  but are not the same
- Measurement noise is often modelled by white noise. (High frequency signal)
- Disturbances are actual changes to the state of the system



# Noise versus Disturbances

- Cruise control:  
Measurement errors on the speed are noise  
A change in slope is a disturbance

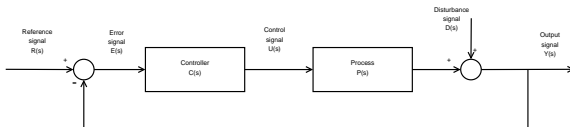


# Noise versus Disturbances

- Remember from the start of the lecture

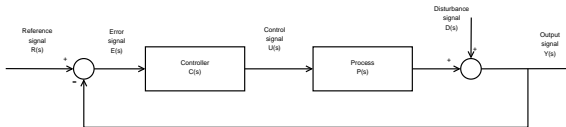
$$Y(s) = \frac{P(s)C(s)}{1 + P(s)C(s)}R(s) + \frac{1}{1 + P(s)C(s)}D(s)$$

- Choosing  $T(s) = \frac{1}{1+P(s)C(s)}$  sufficiently small results in the rejection of  $D$ . This can be achieved by choosing  $C(s)$  sufficiently high



# Disturbance vs noise

- But what happens to measurement noise
  - The amplified measurement noise will be applied to the input of the plant.
  - In reality measurement noise requires no control actions. Good noise rejection means that the controller ignores this noise.



# Disturbance versus noise rejection

- Good disturbance rejection requires fast action to bring the system back to the desired state
- Good noise rejection requires that measurement noise will be ignored
- Note that a controller can not see the difference between measurement noise and disturbances. Slow controllers will be less sensitive to measurement noise. Fast system will have better disturbance rejection

**Slow Controllers**  
Not sensitive to noise  
Small control inputs



**Fast Controllers**  
Good disturbance rejection  
Fast tracking

**Robust Controllers**  
Model errors will not  
affect the behaviour of  
the system strongly



**Aggressive Controllers:**  
Exchanges robustness for  
better performance