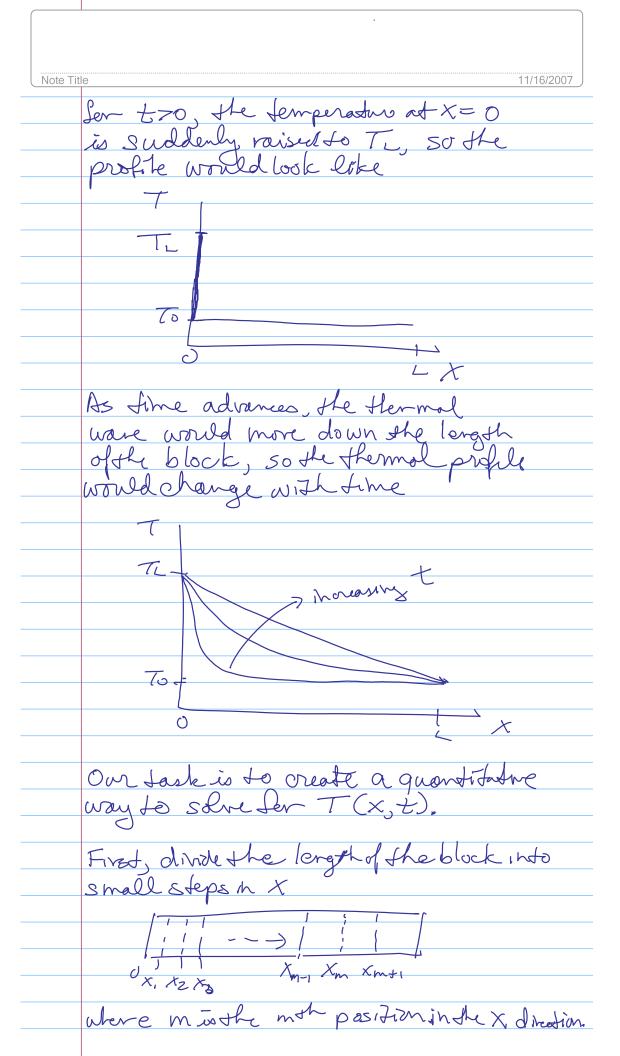
Finite Difference Numerical Solutions Many important problems in engineering & Science in volve more than I dimension. While the numerocal methods you have tearned with predictor correction mothods, these are somewhat limited when it comes to multi-dimensional and for transient system. For these, it is nort efficient to use Snite difference methods. Example 1D, transient systm, heatdransfur $L^2T = L = T$ t < 0 $T(x) = T_0$ for all $x = T_0$ t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0 t < 0(9=-K off) transferd heat in ID as a Sunction of time! Initially she system is at a unitor in temperature To, at all positions of X. At t=0, the temperature of X= 0 is suddenly raised to TL. The temperature in side the block changes as energy enters and is conducted in the Cx direction X=O X=L at t=0 the temp. Profile inste block is



dI can be approximated as
AX
dX dT = Tm+1 -Tm sx=(xm+1-xm) dx six where p refers to time, since T(x,t).
Similarly, the 2rd derivative with respect to & would be
$\frac{d}{dx}\left(\frac{d7}{dx}\right) = \frac{1}{2x}\left(\frac{1}{m+1}, \frac{1}{-m}\right)$ $= \frac{1}{2x}\left(\frac{1}{m+1}, \frac{1}{-m}\right)$ $= \frac{1}{2x}\left(\frac{1}{m+1}, \frac{1}{-m}\right)$ $= \frac{1}{2x}\left(\frac{1}{m+1}, \frac{1}{-m}\right)$
$\frac{2\times}{2\times}$
$= \frac{T_{m+1} - 2T_m^p + T_{m-1}^p}{(2x)^2}$
For the fine derivative of T = Tm ^{P+1} - Tm ^P dt = \(\text{\Delta} \tau \tau \)
Note that stush postion in orements ze and stistle time increment size.
Padding these together,
$\frac{dT}{dX^2} = 2 \frac{dT}{dA}$ $\frac{dT}{dA} = \frac{1}{2} \frac{dT}{dA}$
$\frac{\partial \mathcal{L}}{\nabla m+1} = 2Tm + Tm-1 = \alpha Tm - Tm$ $\frac{\partial \mathcal{L}}{\partial x}$

Note Tit	
	$\frac{T_{m+1}^{p}-2T_{m}^{p}+T_{m-1}^{p}}{(\Delta X)^{2}}=\frac{T_{m}^{p+1}-T_{m}^{p}}{\Delta t}$
	Re-arranging
	TPH St [TP TP]+[1-28+] TP M = 26x2 [m+1+ [m-1]+[1-2x2] [m
	now, use this egn along with initial conditions and steps izes to iterate in postim and time.
	Example calculations
	1 x = 0.1 xt= 0.1
	$\lambda = 58$
	L= 1 05t 54
	$T_0 = 350$ $T_L = 440$
	4
X	0 0.1 0.2 0.3
•	0 440 ,440 440 440
	0.) 350 → 368
	0,2 350 7
	0,3 350
	- (
	$T_{0.1} = \frac{0.1}{(5000.1)^2} \left[\frac{440 + 350}{440 + 350} \right] +$
	$\left[1-\frac{2(0.1)}{5000.10^{2}}\right]350$
	= 368
	Several calculation values are
	shown below, along with
	a graph of tus X outvarious

x 0 0.1 0.2 0.3 0.4 0.5 0 440 440 440 440 440 440 0.1 350 368 378.8 386 391.184 395.1296 0.2 350 350 350 350.72 362.096 365.8976 0.3 350 350 350 350.350.2016 353.6576 0.4 350 350 350 350 350.350.350.350 350.4996 0.5 350 350 350 350 350 350 350.0288 0.6 350 350 350 350 350 350 350 350 0.7 350 350 350 350 350 350 350 350 0.8 350 360 350 350 350 350 350 0.9 360 360 350 350 350 350 350 440 440 440 440 440 440 450 450 450 </th <th></th> <th></th> <th></th> <th></th> <th></th> <th></th> <th></th> <th></th>								
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	430 420 410 400 390 380 370 360 350	0.2	0.4		0.6	0.8	1	13
	430 420 410 400 390 380 370 360 350	0.2	0.4		0.6	0.8	1	1.3
	430 420 410 400 390 380 370 360 350	0.2	0.4		0.6	0.8	1	1.2
	430 420 410 400 390 380 370 360 350	0.2	0.4		0.6	0.8	1	1.

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Note Tit	tle 11/16/2007	
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