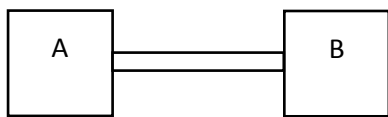


**ABE 307, Fall 2017**  
**Homework 8**  
**Assigned: 11/27/2017**  
**Due: 12/6/2017 (Wednesday)**  
**Potential Points < 70**

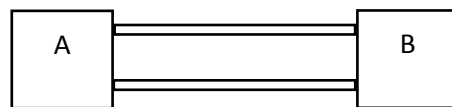
1. A glass sphere of 4 cm diameter and of density 2.63 g/cc is allowed to fall through a liquid of density 1.4 g/cc and viscosity of 1 cp. Calculate the terminal velocity of the sphere. (10)
2. A hollow sphere 5 mm in diameter, with a mass of 0.05 g, is released in a column of liquid and attains a terminal velocity of 0.5 cm/s. The liquid density is 0.9 g/cm<sup>3</sup>. The sphere is far enough from the containing walls that their effect can be neglected. (15)
  - a. Compute the drag force on the sphere in dynes.
  - b. Compute the friction factor.
  - c. Determine the viscosity of the liquid.
3. How many gal/hr of water at 68 deg F can be delivered through a 1320-ft length of smooth 6.00 in i.d. pipe under a pressure difference of 0.25 psi. Assume that the pipe is “hydraulically smooth” (10)
4. (Problem 7A.1) Pressure Rise in a Sudden Enlargement  
 An aqueous salt solution is flowing through a sudden enlargement at a rate of 450 U.S. gal/min = 0.0284 m<sup>3</sup>/s. The inside diameter of the smaller pipe is 5 in and that of the large pipe is 9 in. What is the pressure rise in pounds per square inch if the density of the solution is 63 lb<sub>m</sub>/ft<sup>3</sup>. (15)
5. Flow between two tanks. (20)  
 Case I: A fluid flows between two tanks A and B because  $P_A > P_B$ . The tanks are at the same elevation and there is no pump in the line. The connecting line has a cross-sectional area  $S_1$  and the mass rate of flow is  $w$  for a pressure drop of  $P_A - P_B$ .  
 Case II: It is desired to replace the connecting line by two lines, each with cross section  $S_{II} = \frac{1}{2} (S_1)$ . What pressure difference  $(P_A - P_B)_{II}$  is needed to give the same total mass flow rate as in Case 1 ? Assume turbulent flow and use the given Blasius formula for the friction factor. Neglect entrance and exit losses.  
 Blasius Formula for friction factor.  $f = 0.0791/(\text{Re})^{1/4}$

CASE I



Mass flow rate  $w$

CASE II



Sum of mass flow rates is  $w$