

(2)

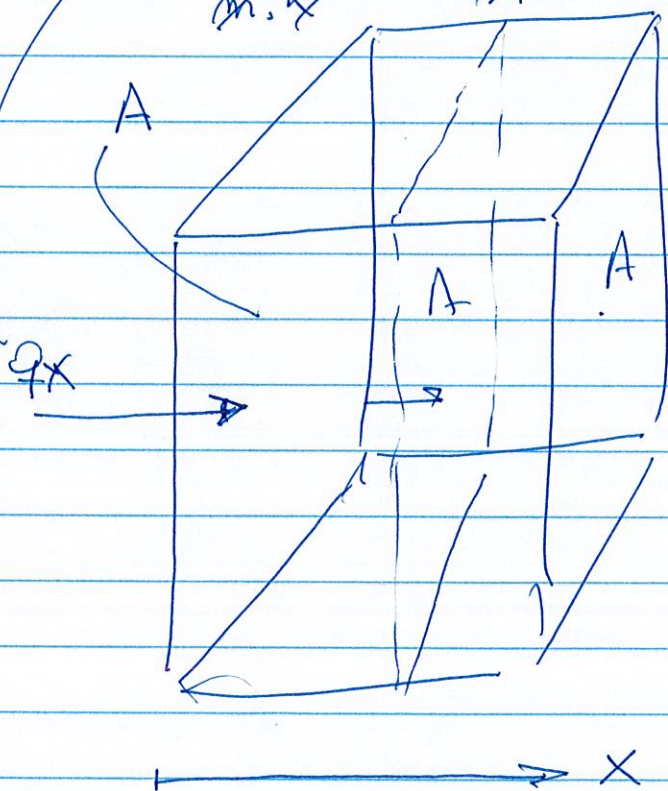
Flow [Watts]

 $[m^2]$ K

$$q_x = -KA \frac{dT}{dx} \quad [\text{FOURIER LAW}]$$

 $\leftarrow m$ thermal conductivity $\left[\frac{W}{m \cdot K} \right]$

$$\frac{W}{m \cdot K} \cdot m^2 \cdot \frac{K}{m} = \text{Watts}$$

A: cross-sectional area
to the flow

$$\text{FLUX} = \frac{\text{Flow}}{\text{Area}} = \frac{W}{m^2} = \frac{q_x}{A} = \frac{-KA \frac{dT}{dx}}{A} = q_x$$

If in your problem Area (A) is unknown
it is better to calculate the FLUX

Flow in the direction X

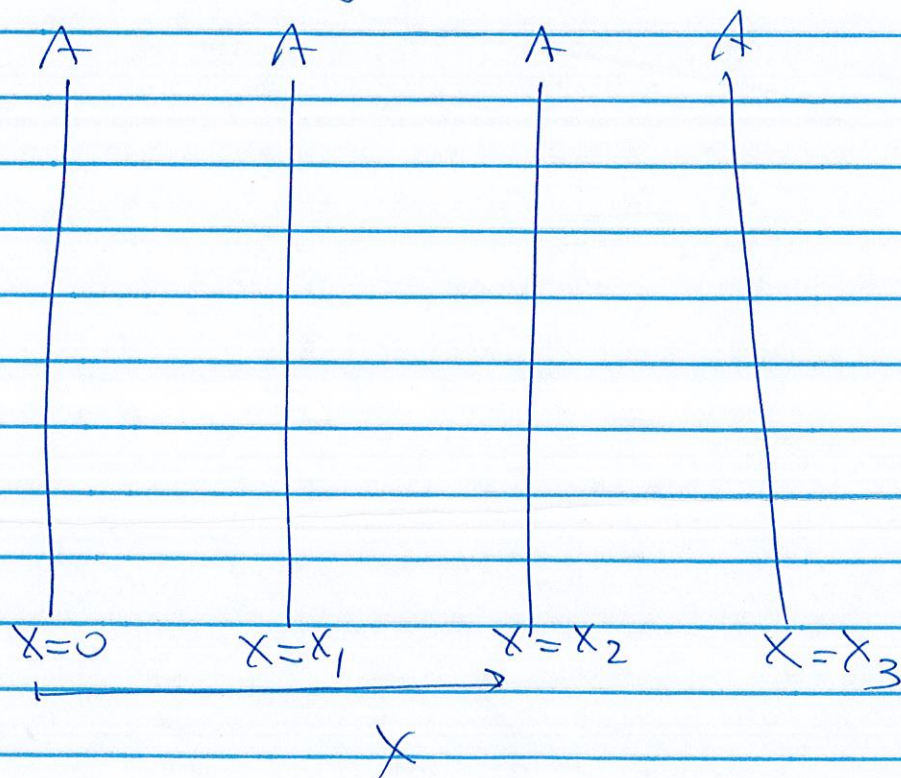
(3)
(2)

Flow $q_x = -KA \left(\frac{dT}{dx} \right)$

GRADIENT OF TEMPERATURE
IT IS ALWAYS NEGATIVE

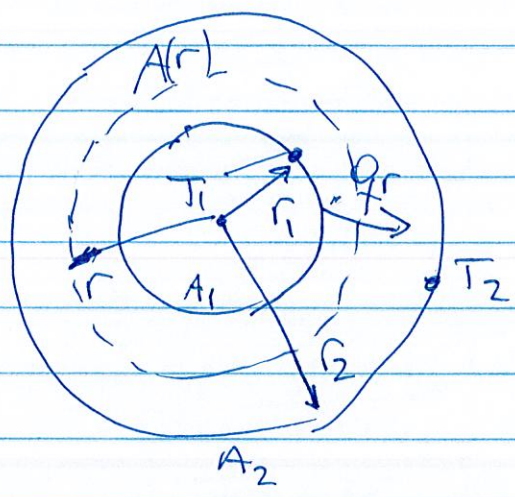
FLUX $\frac{q_x}{A} = -k \frac{dT}{dx} = q_x''$ ← Hot indicates is a flux.

CARTESIAN COORDINATES Area is the same at any location



(4)

$$T_1 > T_2$$



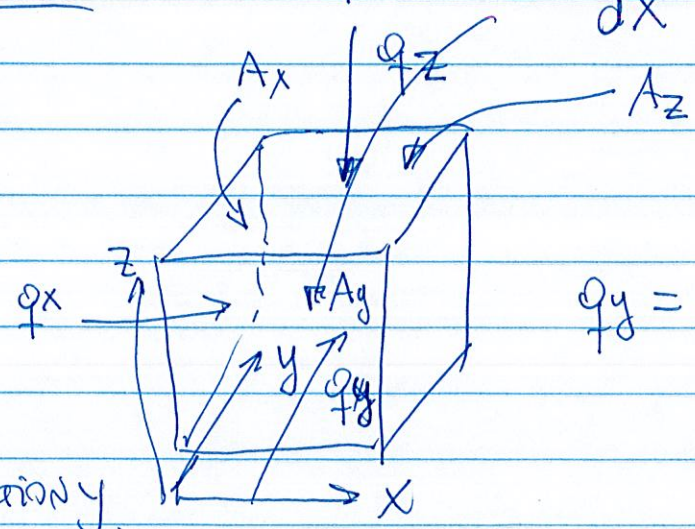
$$A_1 < A_2 > A(r)$$

For spherical \rightarrow cylindrical geometries
Areas $A(r)$ are a function of r

FOURIER LAW

DIRECTION X

$$Q_x = -K_x A_x \frac{dT}{dx}$$



$$Q_y = -K_y A_y \frac{dT}{dy}$$

DIRECTION Y

DIRECTION Z

(3)

$$q_z = -k_z A_z \frac{dT}{dz}$$

For a 3D HEAT TRANSFER PROBLEM

$$\vec{q} = \frac{\vec{Q}}{A} = -k \nabla T$$

Gradient operator

Let's assume Isotropic material $k_x = k_y = k_z = k$

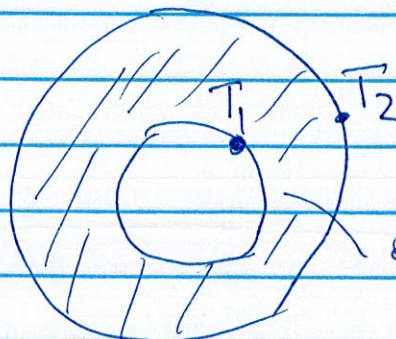
operator ∇ scalar

$$\nabla T = \frac{\partial T}{\partial x} \underline{i} + \frac{\partial T}{\partial y} \underline{j} + \frac{\partial T}{\partial z} \underline{k}$$

CONDUCTION IN A SPHERE

$$\frac{\partial T}{\partial t} = \frac{k}{\rho c} \left[\frac{1}{r^2} \frac{\partial}{\partial r} (r^2 \frac{\partial T}{\partial r}) + \frac{1}{r^2 \sin^2 \theta} \frac{\partial^2 T}{\partial \phi^2} + \frac{1}{r^2 \sin \theta} \frac{\partial}{\partial \theta} \left(\sin \theta \frac{\partial T}{\partial \theta} \right) \right]$$

CONDUCTION



GOOD AND A "REALISTIC"
ASSUMPTION IS THAT
Temperatures changes
only with r