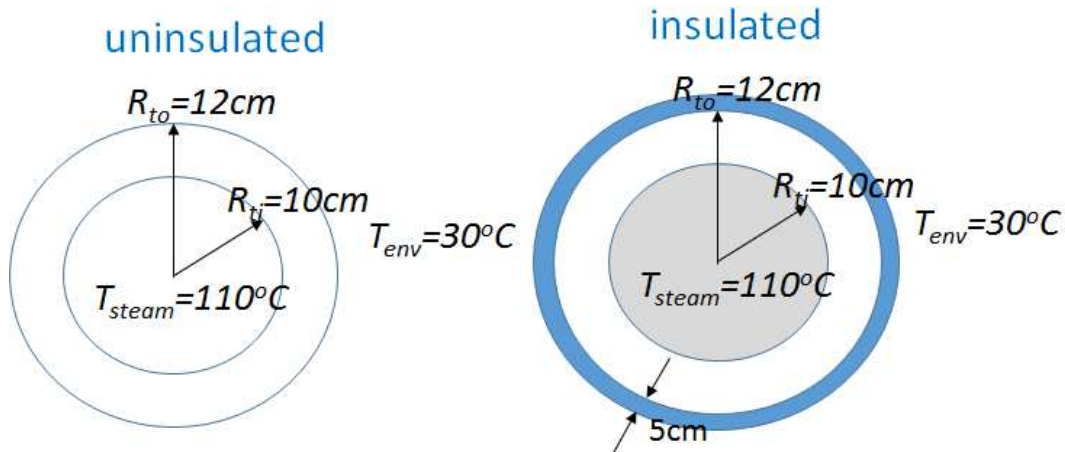


Homework 2 - Solutions

Question 1



(a)

$$R_{ti} := 10 \cdot \text{cm} \quad R_{to} := 12 \cdot \text{cm} \quad e_{ins} := 5 \cdot \text{cm}$$

$$k_{tube} := 400 \frac{\text{W}}{\text{m} \cdot \text{K}}$$

h_{steam} is very large so inner temperature is same than the temperature of the steam

$$T_{steam} := 110 \cdot \text{K} \quad T_{env} := 30 \cdot \text{K} \quad k_{ins} := 0.20 \cdot \frac{\text{W}}{\text{m} \cdot \text{K}} \quad h_{out} := 15 \cdot \frac{\text{W}}{\text{m}^2 \cdot \text{K}}$$

Uninsulated Tube

$$R_{unins} := \frac{\ln\left(\frac{R_{to}}{R_{ti}}\right)}{2\pi \cdot k_{tube}} + \frac{1}{h_{out} \cdot 2 \cdot \pi \cdot R_{to}}$$

$$R_{unins} = 0.088 \cdot \frac{\text{m} \cdot \text{K}}{\text{W}}$$

$$q_{unins_1p} := \frac{T_{steam} - T_{env}}{R_{unins}}$$

$$q_{unins_1p} = 904.037 \cdot \frac{\text{W}}{\text{m}}$$

Insulated Tube

$$R_{ext} := R_{to} + e_{ins} \quad R_{ins} := \frac{\ln\left(\frac{R_{to}}{R_{ti}}\right)}{2\pi \cdot k_{tube}} + \frac{\ln\left(\frac{R_{ext}}{R_{to}}\right)}{2\pi \cdot k_{ins}} + \frac{1}{2\pi h_{out} R_{ext}} \quad R_{ins} = 0.34 \cdot \frac{\text{m} \cdot \text{K}}{\text{W}}$$

$$q_{ins_1p} := \frac{T_{steam} - T_{env}}{R_{ins}}$$

$$q_{ins_1p} = 235.53 \cdot \frac{\text{W}}{\text{m}}$$

(b) Overall heat Transfer Coefficients

Uninsulated Tube

$$U_{i_unin} := \frac{1}{\frac{R_{ti}}{k_{tube}} \ln\left(\frac{R_{to}}{R_{ti}}\right) + \frac{R_{ti}}{R_{to}} \cdot \frac{1}{h_{out}}}$$

$$U_{i_unin} = 17.985 \cdot \frac{W}{m^2 \cdot K}$$

$$U_{o_unin} := \frac{1}{R_{to} \cdot \frac{\ln\left(\frac{R_{to}}{R_{ti}}\right)}{k_{tube}} + \frac{1}{h_{out}}}$$

$$U_{o_unin} = 14.988 \cdot \frac{W}{m^2 \cdot K}$$

However, the calculation of the heat flow is the same and independent on the area that is considered, which is demonstrated next, using values of the areas per unit of length of the inner and outer surface A_i and A_o , in m^2/m length

$$A_i := 2 \cdot \pi \cdot R_{ti} \quad q_{i_unins} := U_{i_unin} \cdot A_i \cdot (T_{steam} - T_{env})$$

$$q_{i_unins} = 904.037 \cdot \frac{W}{m}$$

$$A_{o_unins} := 2 \cdot \pi \cdot R_{to}$$

$$q_{o_unins} := U_{o_unin} \cdot A_{o_unins} \cdot (T_{steam} - T_{env})$$

$$q_{o_unins} = 904.037 \cdot \frac{W}{m}$$

Insulated Tube

$$U_{i_ins} := \frac{1}{\frac{R_{ti}}{k_{tube}} \ln\left(\frac{R_{to}}{R_{ti}}\right) + \frac{R_{ti}}{k_{ins}} \ln\left(\frac{R_{ext}}{R_{to}}\right) + \frac{R_{ti}}{R_{ext}} \cdot \frac{1}{h_{out}}}$$

$$U_{i_ins} = 4.686 \cdot \frac{W}{m^2 \cdot K}$$

$$q_{i_ins} := U_{i_ins} \cdot A_i \cdot (T_{steam} - T_{env})$$

$$q_{i_ins} = 235.53 \cdot \frac{W}{m}$$

$$U_{o_in} := \frac{1}{R_{ext} \cdot \frac{\ln\left(\frac{R_{to}}{R_{ti}}\right)}{k_{tube}} + R_{ext} \cdot \frac{\ln\left(\frac{R_{ext}}{R_{to}}\right)}{k_{ins}} + \frac{1}{h_{out}}}$$

$$U_{o_in} = 2.756 \cdot \frac{W}{m^2 \cdot K}$$

$$A_{o_ins} := 2 \pi \cdot R_{ext}$$

$$q_{o_ins} := U_{o_in} \cdot A_{o_ins} \cdot (T_{steam} - T_{env})$$

$$q_{o_ins} = 235.53 \cdot \frac{W}{m}$$

Question 2

(a) Included in a a different file

(b)

$$\begin{aligned}
 d_i &:= 2 \cdot \text{cm} & r_i &:= \frac{d_i}{2} & k_{\text{insul}} &:= 0.17 \cdot \frac{\text{W}}{\text{m} \cdot \text{K}} & h &:= 2 \cdot \frac{\text{W}}{\text{m}^2 \cdot \text{K}} \\
 r_c &:= \frac{k_{\text{insul}}}{h} & r_c &= 8.5 \cdot \text{cm} & e_{\text{crit}} &:= r_c - r_i & e_{\text{crit}} &= 7.5 \cdot \text{cm} \\
 T_i &:= 100 \cdot \text{K} & T_{\text{inf}} &:= 10 \cdot \text{K}
 \end{aligned}$$

$$R_{\text{cond}} := \frac{\ln\left(\frac{r_c}{r_i}\right)}{2 \cdot \pi \cdot k_{\text{insul}}} \quad R_{\text{cond}} = 2.004 \cdot \frac{\text{m} \cdot \text{K}}{\text{W}}$$

$$R_{\text{conv}} := \frac{1}{2 \cdot \pi \cdot h \cdot r_c} \quad R_{\text{conv}} = 0.936 \cdot \frac{\text{m} \cdot \text{K}}{\text{W}}$$

$$q_{\text{rc}} := \frac{T_i - T_{\text{inf}}}{R_{\text{cond}} + R_{\text{conv}}}$$

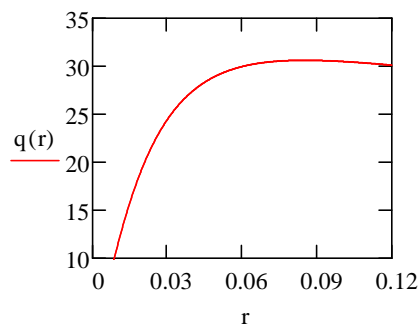
$$q_{\text{rc}} = 30.615 \cdot \frac{\text{W}}{\text{m}}$$

Plot

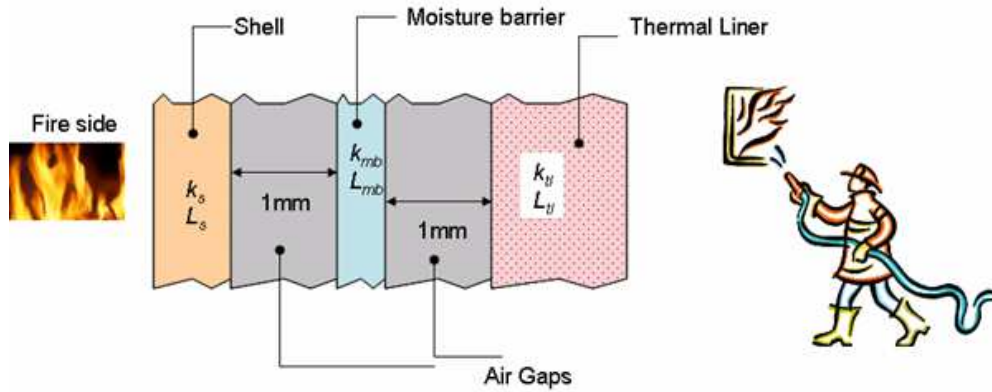
$$R_{\text{cd}}(r) := \frac{\ln\left(\frac{r}{r_i}\right)}{2 \cdot \pi \cdot k_{\text{insul}}}$$

$$R_{\text{cv}}(r) := \frac{1}{2 \cdot \pi \cdot h \cdot r}$$

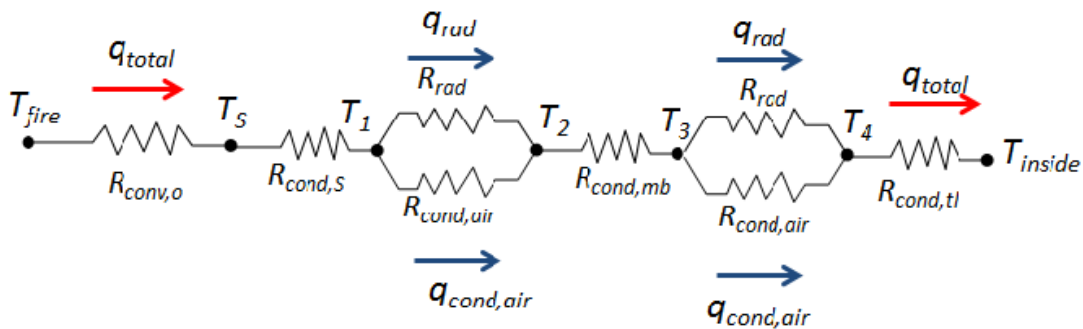
$$q(r) := \frac{T_i - T_{\text{inf}}}{R_{\text{cd}}(r) + R_{\text{cv}}(r)}$$



Question 3



(a)



(b) All the resistance calculations are straight forward except in the air gaps. It was demonstrated that for resistances in parallel, for example between the temperatures T_3 and T_4 the "equivalent" thermal resistance can be calculated as:

$$R_{equivalent} = \frac{1}{\frac{1}{R_{rad}} + \frac{1}{R_{still\ air}}}$$

Data

Shell Layer

$$L_{shell} := 1\text{mm}$$

$$k_{shell} := 0.06 \cdot \frac{\text{W}}{\text{m} \cdot \text{K}}$$

Moisture Barrier

$$L_{mb} := 0.7 \cdot \text{mm}$$

$$k_{mb} := 0.015 \cdot \frac{\text{W}}{\text{m} \cdot \text{K}}$$

Thermal Liner

$$L_{tl} := 4\text{mm}$$

$$k_{tl} := 0.045 \cdot \frac{\text{W}}{\text{m} \cdot \text{K}}$$

Let's calculate all the resistances which will be evaluated by unit of area (mainly because the area is not known). Since we do not know the convection coefficient outside (fire side), we can assume that is very large so the thermal resistance is negligible.

Resistances

Shell Layer

$$R_{\text{shell}} := \frac{L_{\text{shell}}}{k_{\text{shell}}}$$

$$R_{\text{shell}} = 0.017 \cdot \frac{\text{m}^2 \cdot \text{K}}{\text{W}}$$

Moisture Barrier

$$R_{\text{mb}} := \frac{L_{\text{mb}}}{k_{\text{mb}}}$$

$$R_{\text{mb}} = 0.047 \cdot \frac{\text{m}^2 \cdot \text{K}}{\text{W}}$$

Thermal Liner

$$R_{\text{tl}} := \frac{L_{\text{tl}}}{k_{\text{tl}}}$$

$$R_{\text{tl}} = 0.089 \cdot \frac{\text{m}^2 \cdot \text{K}}{\text{W}}$$

To estimate the resistance in the air gap it is necessary to estimate the resistance due to radiation and conduction in the air. Let's assume that the conductivity of air is $k_{\text{air}} = 0.04 \text{ W/m.K}$ taken at approximately 470K. In Appendix Table C8 from the textbook.

$$k_{\text{air}} := 0.04 \cdot \frac{\text{W}}{\text{m} \cdot \text{K}}$$

$$L_{\text{air}} := 1 \text{ mm}$$

$$R_{\text{cond_air}} := \frac{L_{\text{air}}}{k_{\text{air}}}$$

$$R_{\text{cond_air}} = 0.025 \cdot \frac{\text{m}^2 \cdot \text{K}}{\text{W}}$$

Now we have to calculate the resistance due to radiation

$$\sigma := 5.676 \cdot 10^{-8} \cdot \frac{\text{W}}{\text{m}^2 \cdot \text{K}^4}$$

$$T_{\text{avg}} := (470 + 273) \text{ K}$$

$$h_{\text{rad}} := 4 \cdot \sigma \cdot T_{\text{avg}}^3$$

$$R_{\text{radiation}} := \frac{1}{h_{\text{rad}}}$$

$$R_{\text{radiation}} = 0.011 \cdot \frac{\text{m}^2 \cdot \text{K}}{\text{W}}$$

$$R_{\text{air_gap}} := \frac{1}{\frac{1}{R_{\text{radiation}}} + \frac{1}{R_{\text{cond_air}}}}$$

$$R_{\text{air_gap}} = 7.512 \times 10^{-3} \cdot \frac{\text{m}^2 \cdot \text{K}}{\text{W}}$$

From the calculated resistances the thermal liner is what produces the highest thermal resistance.

$$q_{\text{fire}} := 2500 \cdot \frac{\text{W}}{\text{m}^2}$$

$$T_{\text{inside}} := (50 + 273) \cdot \text{K}$$

$$R_{\text{total}} := R_{\text{shell}} + R_{\text{mb}} + 2 \cdot R_{\text{air_gap}} + R_{\text{tl}}$$

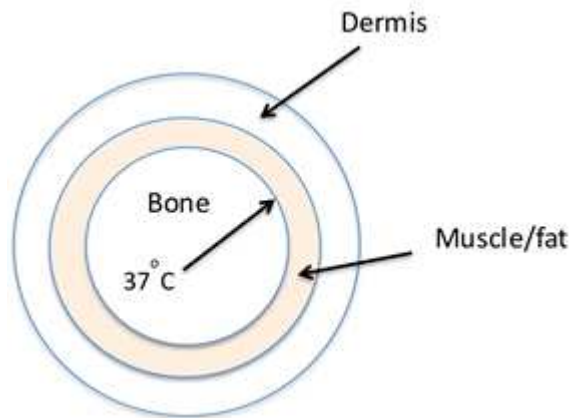
$$R_{\text{total}} = 0.167 \cdot \frac{\text{m}^2 \cdot \text{K}}{\text{W}}$$

$$T_{\text{s}} := T_{\text{inside}} + q_{\text{fire}} \cdot R_{\text{total}}$$

$$T_{\text{s}} = 741.114 \text{ K}$$

So temperature outside of the coat will be about 741.1K or 468.1C

Question 4



Data

$$D_{\text{bone}} := 25 \cdot \text{mm} \quad r_{\text{bone}} := \frac{D_{\text{bone}}}{2} \quad e_{\text{muscle}} := 2.1 \cdot \text{mm} \quad e_{\text{dermis}} := 0.4 \cdot \text{mm}$$

$$k_{\text{m_fat}} := 0.3 \cdot \frac{\text{W}}{\text{m} \cdot \text{K}} \quad k_{\text{dermis}} := 0.1 \cdot \frac{\text{W}}{\text{m} \cdot \text{K}} \quad k_{\text{glove}} := 0.02 \cdot \frac{\text{W}}{\text{m} \cdot \text{K}}$$

$$h_{\text{amb}} := 100 \cdot \frac{\text{W}}{\text{m}^2 \cdot \text{K}} \quad e_{\text{glove}} := 1.4 \cdot \text{mm}$$

$$r_{\text{m_fat}} := r_{\text{bone}} + e_{\text{muscle}}$$

$$r_{\text{dermis}} := r_{\text{m_fat}} + e_{\text{dermis}}$$

(a) The heat loss per unit length q_{prime} can be calculated from the resistances in the different layers of the finger, so the resistances need to be estimated

Without Gloves

$$R_{\text{muscle}} := \frac{1}{2\pi \cdot k_{\text{m_fat}}} \cdot \ln\left(\frac{r_{\text{m_fat}}}{r_{\text{bone}}}\right)$$

$$R_{\text{muscle}} = 0.082 \cdot \frac{\text{m} \cdot \text{K}}{\text{W}}$$

$$R_{\text{dermis}} := \frac{1}{2\pi \cdot k_{\text{dermis}}} \cdot \ln\left(\frac{r_{\text{dermis}}}{r_{\text{m_fat}}}\right)$$

$$R_{\text{dermis}} = 0.043 \cdot \frac{\text{m} \cdot \text{K}}{\text{W}}$$

$$R_{\text{conv_}} := \frac{1}{2\pi \cdot h_{\text{amb}} \cdot r_{\text{dermis}}}$$

$$R_{\text{conv_}} = 0.106 \cdot \frac{\text{m} \cdot \text{K}}{\text{W}}$$

With Gloves

If we add the glove there will be a change in the heat flux per unit length because we need to add the Resistance of the Glove. The radius after the glove is added will be:

$$r_{\text{glove}} := r_{\text{dermis}} + e_{\text{glove}}$$

$$R_{\text{glove}} := \frac{1}{2\pi \cdot k_{\text{glove}}} \cdot \ln\left(\frac{r_{\text{glove}}}{r_{\text{dermis}}}\right)$$

$$R_{\text{glove}} = 0.71 \cdot \frac{\text{m} \cdot \text{K}}{\text{W}}$$

Since the external radius changes due to the glove, convection will change and the new Resistance to Convection will be:

$$R_{\text{new_conv}} := \frac{1}{2\pi \cdot h_{\text{amb}} \cdot r_{\text{glove}}}$$

$$R_{\text{new_conv}} = 0.097 \cdot \frac{\text{m} \cdot \text{K}}{\text{W}}$$

The major resistance is due to the glove. We can calculate (no asked but needed it) the heat fluxes per unit length when you have and when you don't have gloves. I need to enter temperature please note that since I will use temperature differences I can use temperatures in degrees Kelvin

$$T_{\text{ib}} := 37 \cdot \text{K} \quad T_{\text{out}} := -25 \cdot \text{K}$$

Without Gloves

$$q_{\text{prime_wout_gloves}} := \frac{T_{\text{ib}} - T_{\text{out}}}{R_{\text{muscle}} + R_{\text{dermis}} + R_{\text{conv_}}}$$

$$q_{\text{prime_wout_gloves}} = 267.8 \cdot \frac{\text{W}}{\text{m}}$$

With Gloves

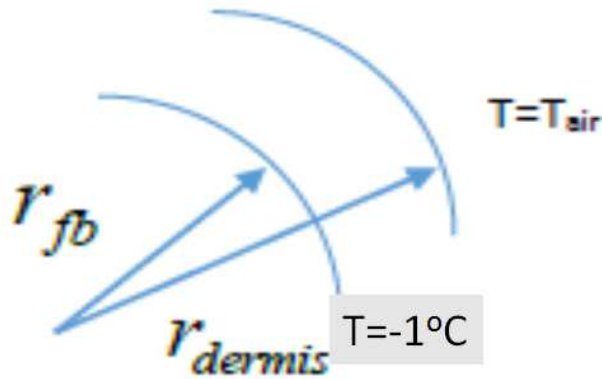
$$q_{\text{prime_with_gloves}} := \frac{T_{\text{ib}} - T_{\text{out}}}{R_{\text{muscle}} + R_{\text{dermis}} + R_{\text{glove}} + R_{\text{new_conv}}}$$

$$q_{\text{prime_with_gloves}} = 66.5 \cdot \frac{\text{W}}{\text{m}}$$

An important decrease in the heat flow per unit length

Let's assume the frostbite is within the dermis layer and can be located by the radius r_{fb} where the temperature is reaches -1C

$$T_{\text{fb}} := -1 \cdot \text{K}$$



$$r_{fb_nogv} := \frac{r_{dermis}}{\exp\left[\frac{2\pi \cdot (T_{fb} - T_{out}) \cdot k_{dermis}}{q_{prime_wout_gloves}} - \frac{k_{dermis}}{h_{amb} \cdot r_{dermis}}\right]}$$

$$r_{fb_nogv} = 15.156 \cdot \text{mm}$$

$$\text{Damaged_dermis} := r_{dermis} - r_{fb_nogv} \quad \text{Damaged_dermis} = -0.156 \cdot \text{mm}$$

The value is negative, it may indicate that all the dermis is affected and the frostbite can be even move to the muscle/fat zone. Equation to calculate the frostbite distance including that zone can be calculated using the following (it can be derived by assuming the frostbite is with the muscle/fat zone zone), which we will define as new frost bite.

$$r_{fb_nogv_new} := \frac{r_{m_fat}}{\exp\left[\frac{2\pi \cdot (T_{fb} - T_{out}) \cdot k_{m_fat}}{q_{prime_wout_gloves}} - \frac{k_{m_fat}}{k_{dermis}} \cdot \ln\left(\frac{r_{dermis}}{r_{m_fat}}\right) - \frac{k_{m_fat}}{h_{amb} \cdot r_{dermis}}\right]}$$

$$r_{fb_nogv_new} = 16.333 \text{ mm} \quad \text{NewDamaged_dermis} := r_{dermis} - r_{fb_nogv_new}$$

$$\text{NewDamaged_dermis} = -1.333 \text{ mm} \quad \text{So the frostbite is very severe and we can have temperatures of } -1^\circ\text{C} \text{ in the bone}$$

When gloves are weared,you replace in the above equation (the heat flux using gloves)

$$r_{fb_withgv} := \frac{r_{dermis}}{\exp\left[\frac{2\pi \cdot (T_{fb} - T_{out}) \cdot k_{dermis}}{q_{prime_with_gloves}} - \frac{k_{dermis}}{h_{amb} \cdot r_{dermis}}\right]}$$

$$r_{fb_withgv} = 12.78 \text{ mm} \quad \text{DamagedDermis}_{with_globe} := r_{dermis} - r_{fb_withgv}$$

$$\text{DamagedDermis}_{with_globe} = 2.22 \text{ mm}$$

Better wear gloves when temperature outside is -25°C or -13°F

Question 5

(a)

$$D_{\text{fin}} := 2.5 \text{ mm} \quad A_c := \pi \cdot \frac{D_{\text{fin}}^2}{4} \quad P := \pi \cdot D_{\text{fin}} \quad k_{\text{fin}} := 400 \cdot \frac{\text{W}}{\text{m} \cdot \text{K}}$$

$$T_{\text{fin}} := 95 \cdot \text{K} \quad T_{\text{amb_air}} := 25 \cdot \text{K} \quad h_{\text{fin_air}} := 10 \cdot \frac{\text{W}}{\text{m}^2 \cdot \text{K}}$$

$$q_{\text{fin}} := \sqrt{h_{\text{fin_air}} \cdot k_{\text{fin}} \cdot P \cdot A_c} \cdot (T_{\text{fin}} - T_{\text{amb_air}}) \quad \boxed{q_{\text{fin}} = 0.87 \text{ W}}$$

(b) For a 25mm length let's use the equation below given in the problem, but first we need to calculate the heat with no fin which is:

$$q_{\text{non_fin}} := A_c \cdot h_{\text{fin_air}} \cdot (T_{\text{fin}} - T_{\text{amb_air}})$$

$$m_p := \sqrt{\frac{h_{\text{fin_air}} \cdot P}{k_{\text{fin}} \cdot A_c}} \quad m_p = 6.325 \frac{1}{\text{m}} \quad L_{\text{fin}} := 25 \cdot \text{mm}$$

$$q_{\text{finite_fin}} := \sqrt{\frac{k_{\text{fin}} \cdot P}{h_{\text{fin_air}} \cdot A_c}} \cdot \frac{\sinh(m_p \cdot L_{\text{fin}}) + \frac{h_{\text{fin_air}}}{m_p \cdot k_{\text{fin}}} \cdot \cosh(m_p \cdot L_{\text{fin}})}{\cosh(m_p \cdot L_{\text{fin}}) + \frac{h_{\text{fin_air}}}{m_p \cdot k_{\text{fin}}} \sinh(m_p \cdot L_{\text{fin}})} \cdot q_{\text{non_fin}}$$

$$\boxed{q_{\text{finite_fin}} = 0.14 \text{ W}}$$

Very different value

(c) For the two solutions be within 5%

$$\sinh m_p L + h/m_p k * \cosh m_p L / (\cosh m_p L + (h/m_p k) \sinh(m_p L)) = 0.95$$

The root tool can be used from where a hypothetical length L_{hyp} where the infinite analytical solution (see Equation given in Lectures) can be used within a 5% error can be obtained, let's define the function from which the root L can be obtained

$$L_f := 6 \cdot \text{mm}$$

$$f(L_f) := \frac{\sinh(m_p \cdot L_f) + \frac{h_{\text{fin_air}}}{m_p \cdot k_{\text{fin}}} \cdot \cosh(m_p \cdot L_f)}{\cosh(m_p \cdot L_f) + \frac{h_{\text{fin_air}}}{m_p \cdot k_{\text{fin}}} \sinh(m_p \cdot L_f)} - 0.95$$

$$L_{\text{hyp}} := \text{root}(f(L_f), L_f)$$

$$\boxed{L_{\text{hyp}} = 28.9 \cdot \text{cm}}$$

