



### EXAMPLE 1

(2)

$$T_{\infty} = 200^{\circ}\text{C}$$

CONVECTION

HEAT TRANSFER BY  
CONVECTION

ROOM AIR.

$$h = 400 \frac{\text{W}}{\text{m}^2\text{K}}$$

$$t_{\text{constant}} = 1 \text{ second}$$

$$K = 20 \frac{\text{W}}{\text{m}\cdot\text{K}}$$

$$C_m = 0.4 \frac{\text{KJ}}{\text{kgK}}$$

$$\rho_{m,r} = 8500 \text{ kg/m}^3$$

$T_i$

$T(t)$  we assume that the  
temperature is  
independent of  
the position

LUMPED PARAMETER ANALYSIS

$$\frac{T(t) - T_{\infty}}{T_i - T_{\infty}} = \exp\left(-\frac{UA}{mC} t\right)$$

$$Bi = \frac{hR}{K} < 0.1$$

$$20 \frac{\text{W}}{\text{m}\cdot\text{K}}$$



Let's assume the Lumped Parameter model (3) can be used [we will need to check that later]

$$\frac{T(t) - T_{\infty}}{T_i - T_{\infty}} = \exp\left[-\frac{UA}{mc} t\right]$$

What is  $U$ ?

$U$  overall heat transfer coefficient.

$\frac{1}{U} = \text{Resistance to conduction} + \text{Resistance to convection}$

Overall resistance to heat transfer  $\quad \quad \quad \frac{1}{h}$

$U \approx h$  Because we are assuming the LUMPED PARAMETER MODEL.



$$\exp\left[-\frac{hA}{mC}t\right] = \exp\left[-\frac{t}{\frac{mC}{hA}}\right] \quad (4)$$

$$\text{Units } \frac{mC}{hA} = \frac{\cancel{\text{kg}} \times \frac{\text{J}}{\cancel{\text{kg}} \cancel{\text{K}}}}{\frac{\text{W}}{\cancel{\text{m}^2 \cancel{\text{K}}}} \times \cancel{\text{m}^2}} = \frac{\text{J}}{\text{W}} = \frac{\text{J}}{\frac{\text{J}}{\text{s}}} = \text{s}$$

$$t_{\text{constant}} = \frac{mC}{hA} = 1 \text{ s}$$

$$m = V_b \rho_m = \frac{4}{3} \pi R^3 \rho_m$$

$$A = 4\pi R^2$$

$$t_{\text{constant}} = 1 \text{ sec} = \frac{\frac{4}{3} \pi R^3 \rho_m \times C_m}{h \times 4\pi R^2}$$

$$1 \text{ sec} = \frac{\rho_m C_m R}{3h} \Rightarrow R = \frac{3h}{\rho_m C_m}$$

$$R = \frac{3 \times 400 \text{ W/m}^2 \text{K}}{8500 \frac{\text{kg}}{\text{m}^3} \times 0.4 \times 1000 \frac{\text{J}}{\text{kgK}}} = 3.5 \times 10^{-4} \text{ m}$$

$$\boxed{R = 0.35 \text{ mm}} \quad \boxed{D = 0.7 \text{ mm}}$$



$$Bi = \frac{400 \text{ W/m}^2\text{K} \times 3.5 \times 10^{-4} \text{ m}}{20 \text{ W/m.K}} = 0.007 \quad (5)$$

$$Bi = 0.007 < 0.1$$

GOOD ASSUMPTION.

We want to know time to reach  $199^\circ\text{C}$

$$\frac{T(t) - T_\infty}{T_c - T_\infty} = \exp\left(-\frac{hA}{mC} t\right)$$

$\swarrow \quad \searrow$   
 $199 \quad 200^\circ\text{C}$   
 $\swarrow \quad \searrow$   
 $25^\circ\text{C} \quad 200$

$$\ln \frac{199 - 200}{25 - 200} = -\frac{hA}{mC} t$$

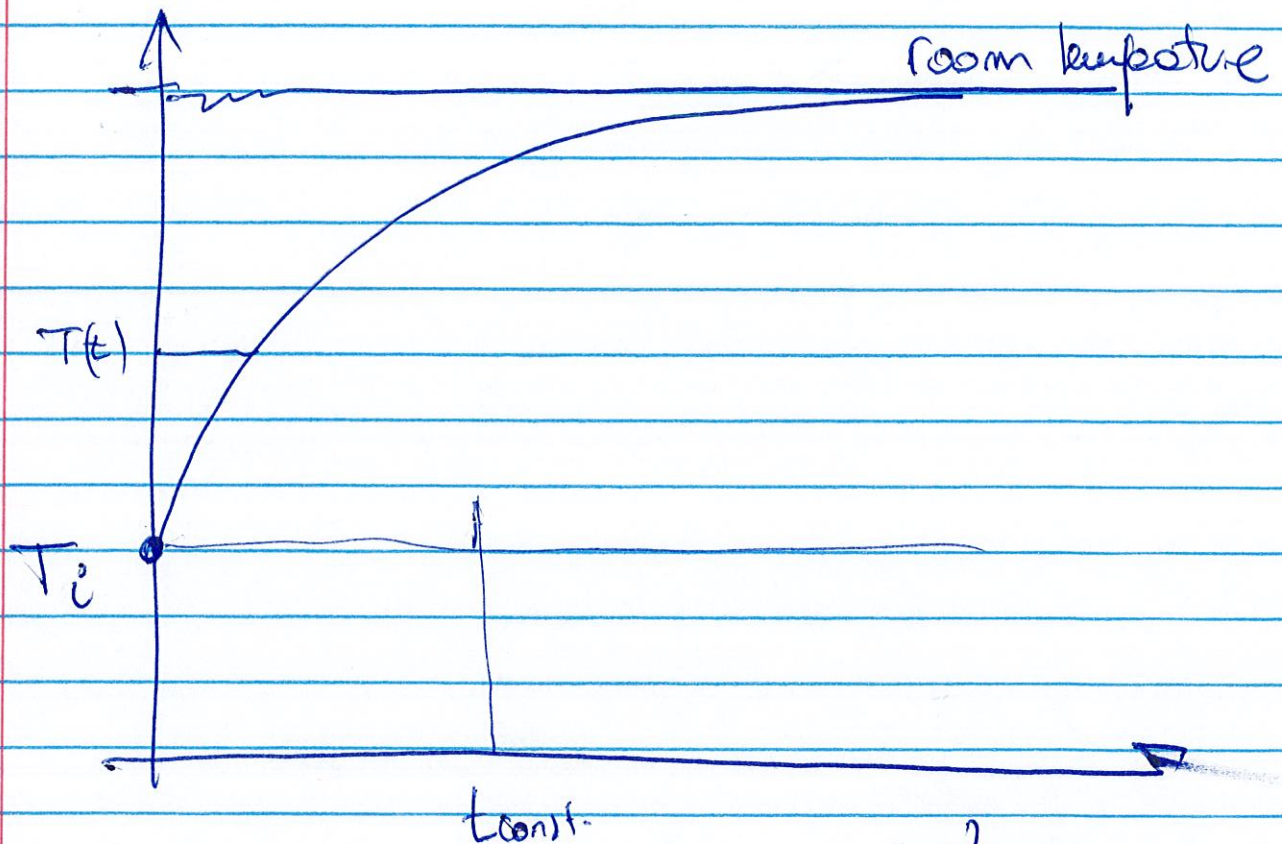
$$t = - \left( \frac{mC}{hA} \right) \ln \frac{199 - 200}{25 - 200} \approx 55$$

$t_{\text{cont}} = 1 \text{ sec.}$



What is time constant?  
Of a thermometer

(6)



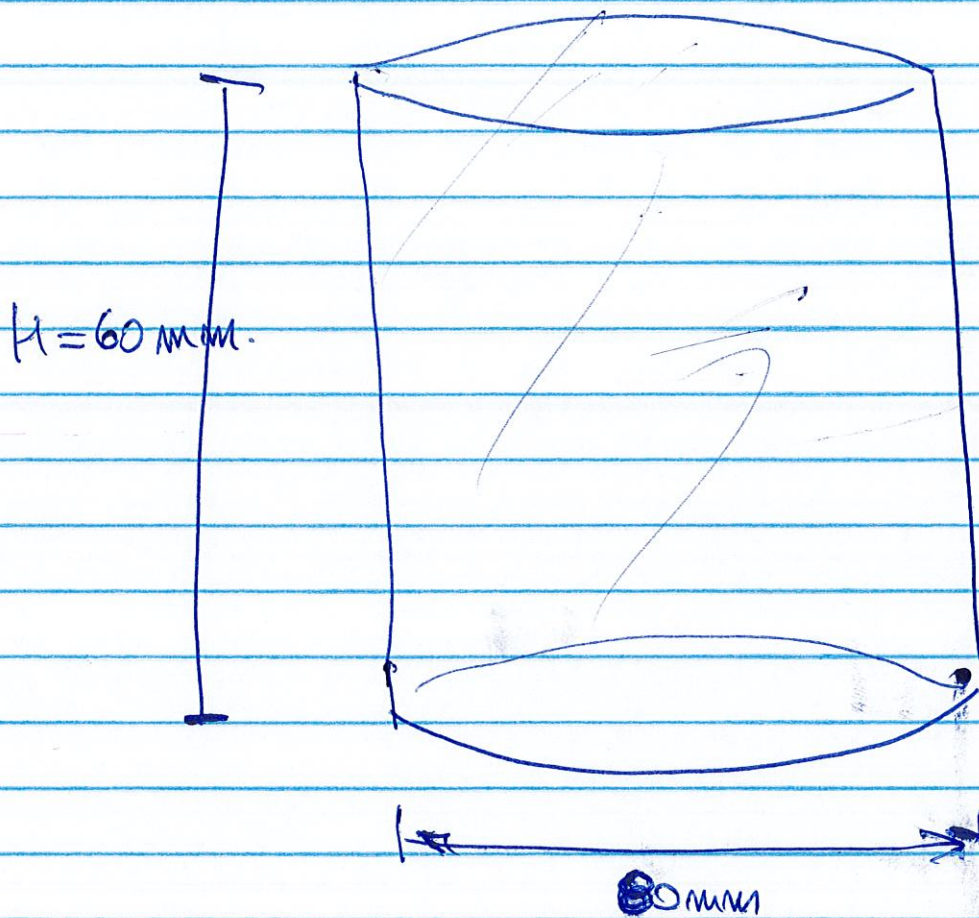
$$\text{Q61} \quad \frac{T(t) - T_{\infty}}{T_i - T_{\infty}} = e^{-\frac{t}{\frac{mc}{hA}}} = e^{-\frac{t}{t_{\text{const.}}}}$$

if  $t = t_{\text{const.}}$

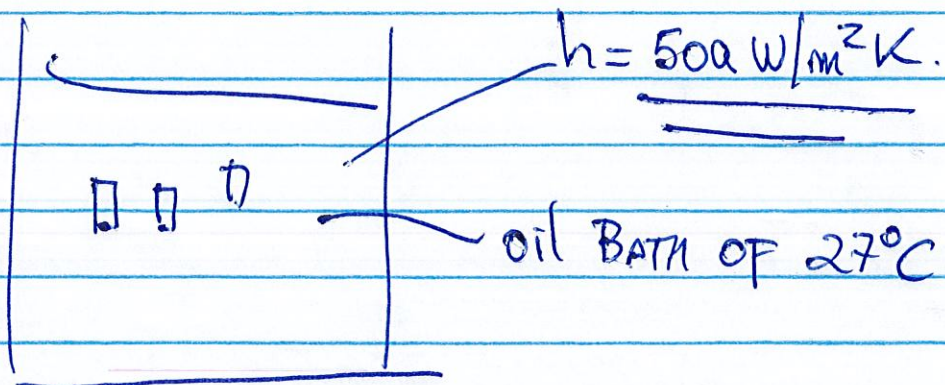
$$\frac{T_{\infty} - T(t)}{T_{\infty} - T_i} = \frac{T(t) - T_{\infty}}{T_i - T_{\infty}} = e^{-1} = 0.37$$

### Example 7

(7)



$$T_c = 327^\circ\text{C}$$



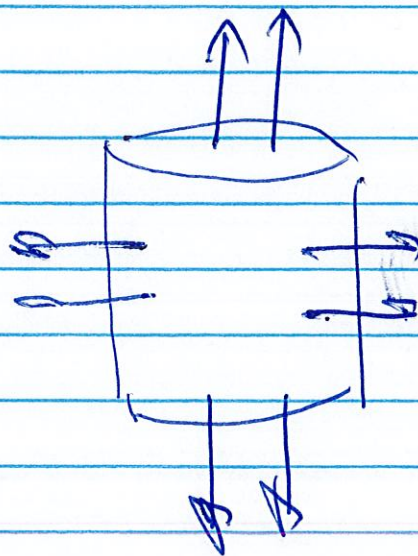
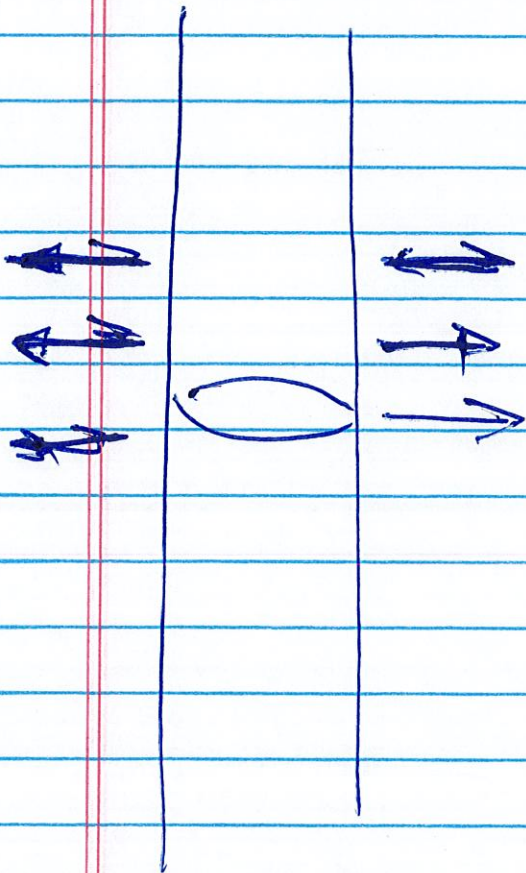


$$Bi = \frac{hR}{K} = \frac{500 \times 40 \times 10^{-3} \text{ m}}{17.4 \frac{\text{W}}{\text{m} \cdot \text{K}}} = 1.1 \quad (8)$$

$$Bi = 1.1$$

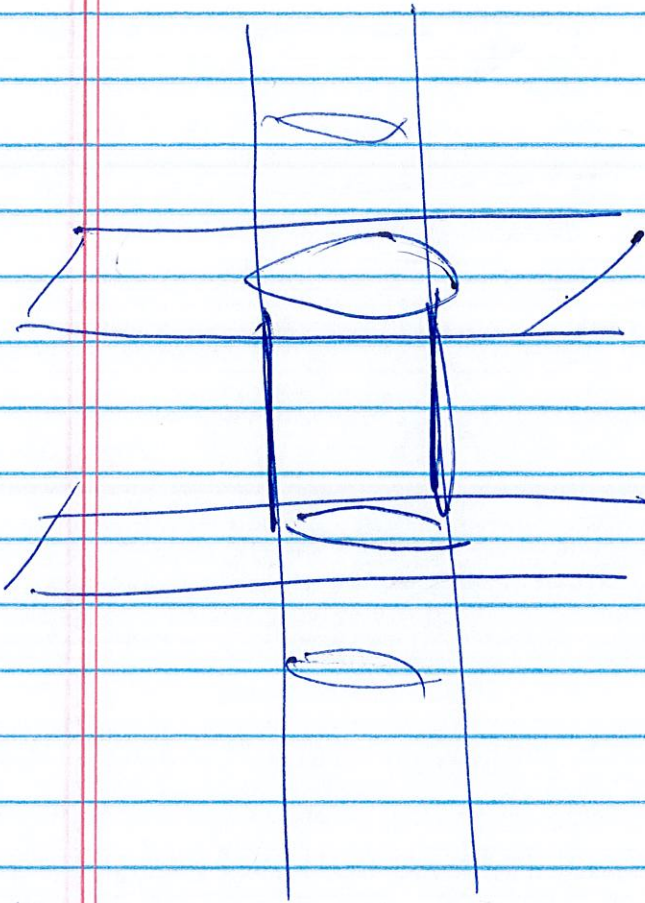
We cannot use LUMPED PARAMETER MODEL

WE HAVE TO USE CHARTS BUT THEY ARE FOR INFINITE LONG CYLINDERS





(9)



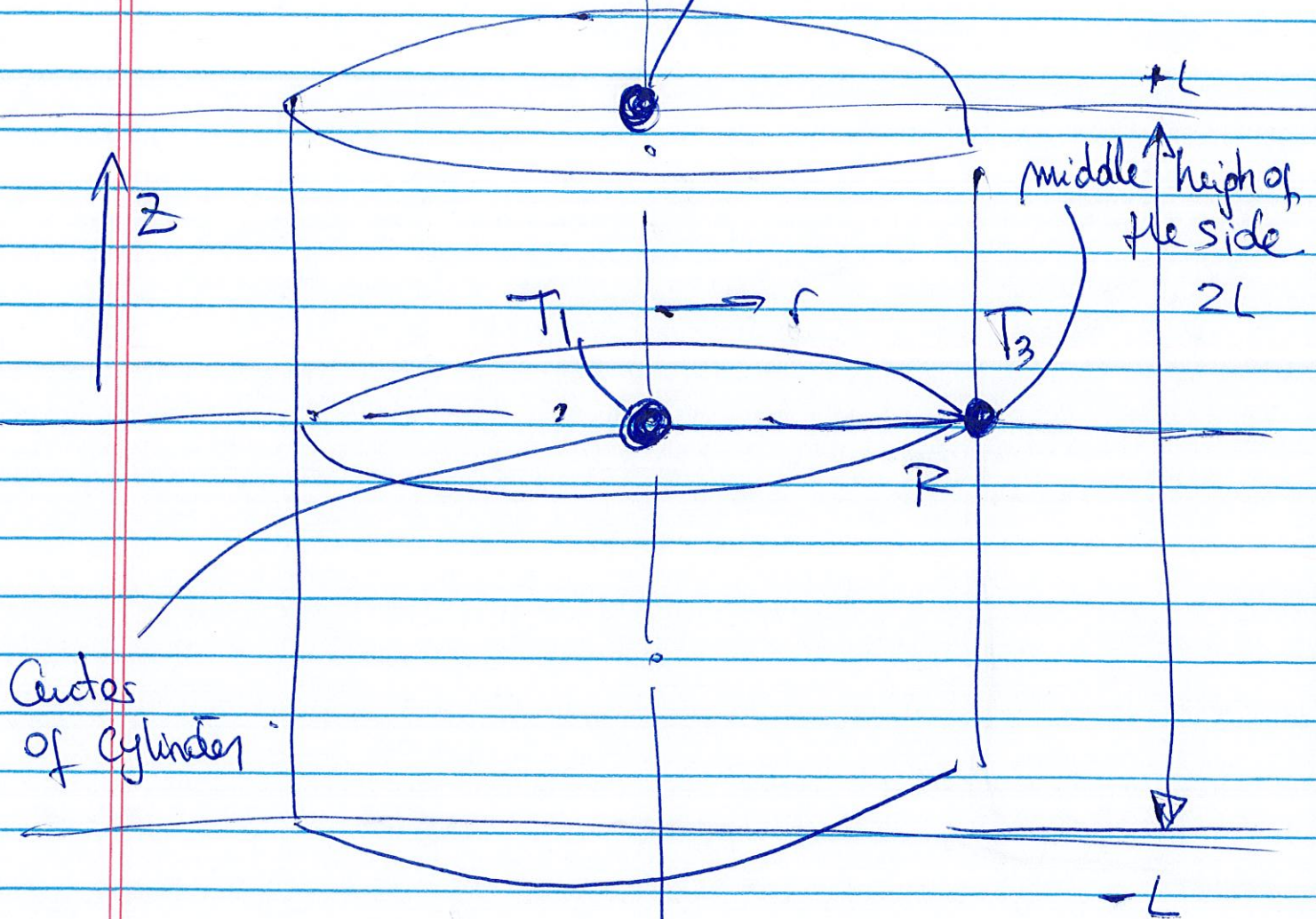
↓ solution

$$Y = Y_c \times Y_{slob.}$$



$t = 3 \text{ minutes}$

$T_2$  Center of the circular phase (19)



$$\frac{T(r, z, t) - T_s}{T_i - T_s} = \underbrace{\frac{T(r, t) - T_s}{T_i - T_s}}_{\text{CHART FOR INFINITE CYLINDER}} \times \underbrace{\frac{T(z, t) - T_s}{T_i - T_s}}_{\text{CHART FOR INFINITE SLAB}}$$

CHART  
FOR INFINITE  
CYLINDER

CHART FOR  
INFINITE SLAB