

What is the reaction rate model for this reversible elementary reaction?



# Rate Equation

- The determination of the rate equation follows a two-step procedure
  - the concentration dependency is found at fixed temperature
  - the temperature dependence of the rate constants is found

$$\begin{aligned}r_i &= f_1(\text{temperature}) \cdot f_2(\text{composition}) \\ &= k \cdot f_2(\text{composition})\end{aligned}$$

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# Batch Reactor

# Ideal batch reactor

Assumptions:

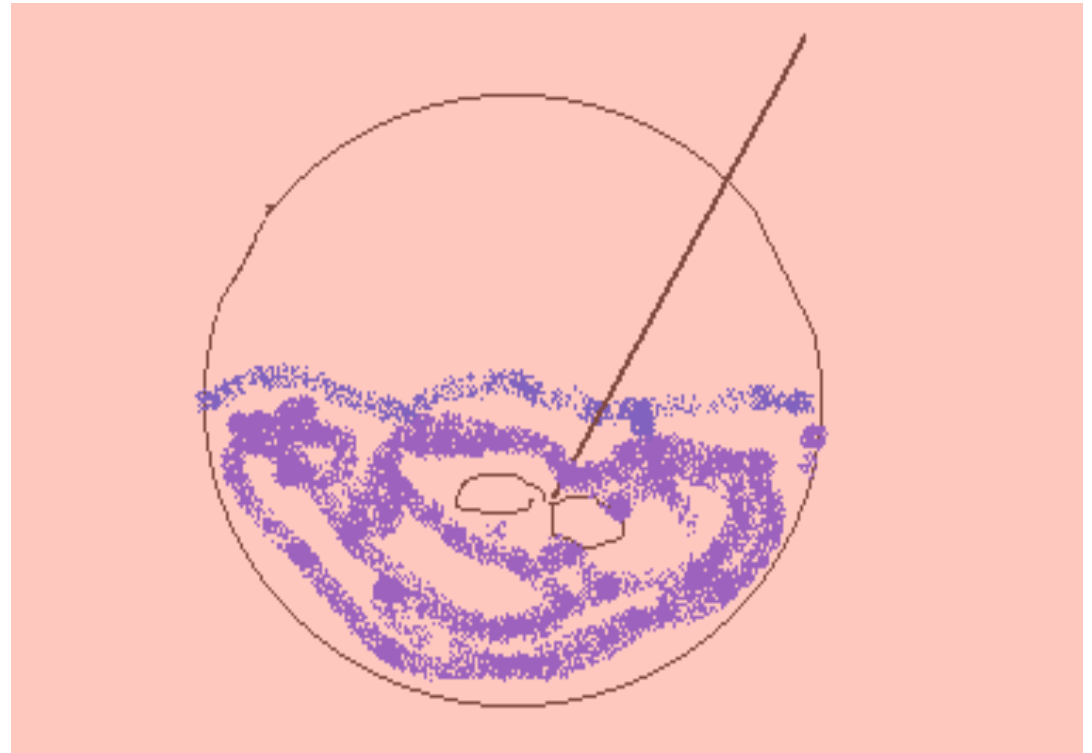
Composition varies with **time**

**Uniform** composition

Constant volume

Usually operated isothermally

- Very simple
- Need very little supporting equipment
- Ideal for small-scale experimental studies on rxn kinetics



# Constant-Volume Batch Reactor

When we mention the constant-volume batch reactor we are really referring to the volume of reaction mixture, and not the volume of reactor. Thus, this term actually means a *constant-density reaction system*. Most liquid-phase reactions as well as all gas-phase reactions occurring in a constant-volume bomb fall in this class.

In a constant-volume system the measure of reaction rate of component  $i$  becomes

$$r_i = \frac{1}{V} \frac{dN_i}{dt} = \frac{d(N_i/V)}{dt} = \frac{dC_i}{dt} \quad (1)$$

# Conversion

Suppose that  $N_{A0}$  is the initial amount of A in the reactor at time  $t = 0$ , and that  $N_A$  is the amount present at time  $t$ . Then the conversion of A in the constant volume system is given by

$$X_A = \frac{N_{A0} - N_A}{N_{A0}} = 1 - \frac{N_A/V}{N_{A0}/V} = 1 - \frac{C_A}{C_{A0}} \quad (7)$$

and

$$dX_A = -\frac{dC_A}{C_{A0}} \quad (8)$$

# Measuring how far a reaction has occurred

Concentration (C) – start at  $C_0$ , end at C

Conversion (X) – start at 0, goes up to 1

$$X = (C_0 - C)/C_0 = 1 - C/C_0$$

Extent of reaction ( $\xi$ ) – starts at 0, goes up to infinity

$$\xi = (N_i - N_{i0})/\nu_i \quad (\text{component } i)$$

# First-order Reactions

**Irreversible Unimolecular-Type First-Order Reactions.** Consider the reaction



Suppose we wish to test the first-order rate equation of the following type,

$$-r_A = -\frac{dC_A}{dt} = kC_A \quad (10)$$



Separating and integrating:

$$-\int_{C_{A0}}^{C_A} \frac{dC_A}{C_A} = k \int_0^t dt$$

or

$$-\ln \frac{C_A}{C_{A0}} = kt \quad (11)$$

In terms of conversion (see Eqs. 7 and 8), the rate equation, Eq. 10, becomes

$$\frac{dX_A}{dt} = k(1 - X_A)$$

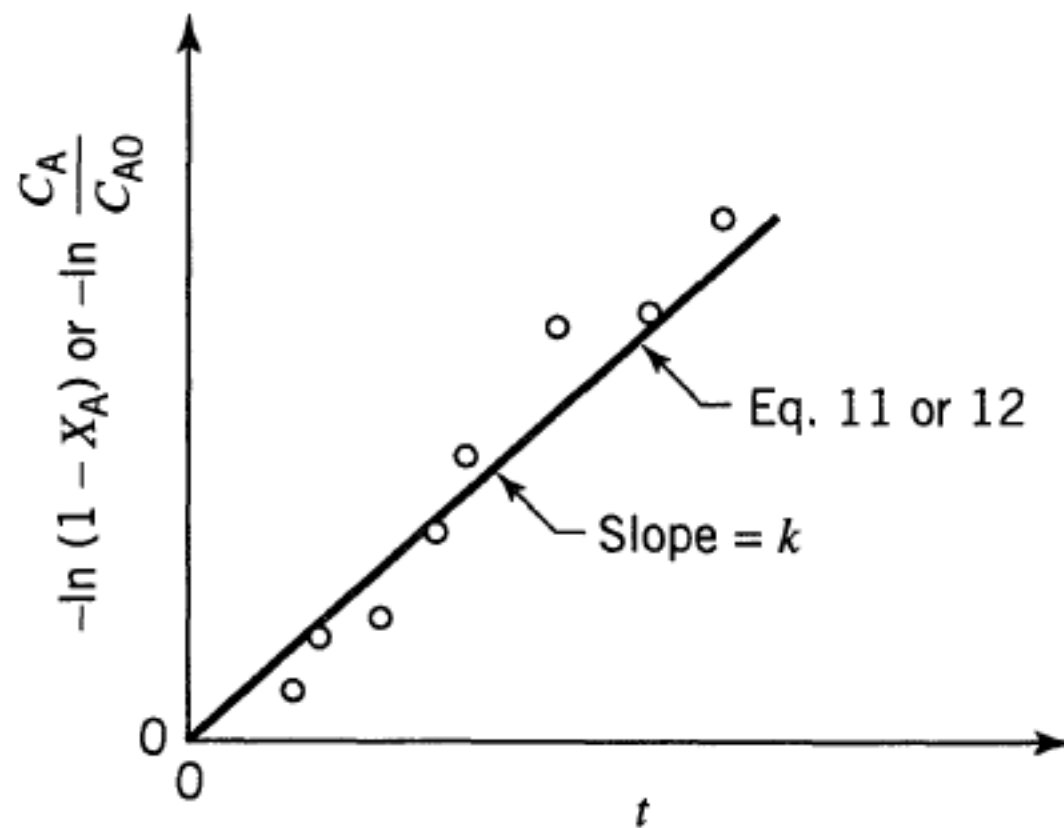
which on rearranging and integrating gives

$$\int_0^{X_A} \frac{dX_A}{1 - X_A} = k \int_0^t dt$$

or

$$\boxed{-\ln(1 - X_A) = kt}$$

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**Figure 3.1** Test for the first-order rate equation, Eq. 10.

# First order reaction solution

$$-r_i = k * C_i$$

$$-r_i = k * C_{i0} * (1-X)$$

$$-r_i = k * (C_{i0} + v_i \xi / V) \quad (V = \text{volume of reaction mixture})$$

$$C_i = C_{i0} * e^{-kt}$$

$$X = 1 - e^{-kt}$$

$$\xi = VC_{i0} / v_i * (-1 + e^{-kt})$$

What about other reaction rate equations?