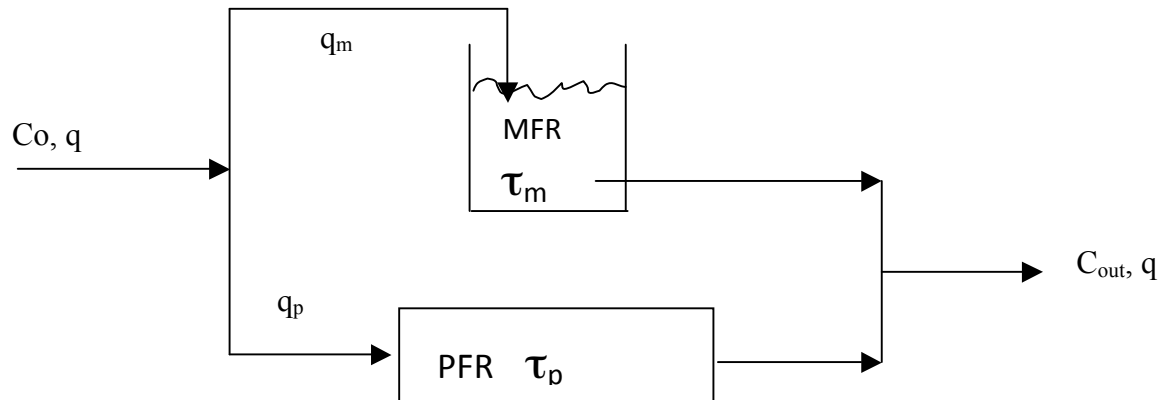


Problem 1.

Derive the equation giving  $C_{out}$  as a function of  $C_o$ ,  $q_m$ ,  $q_p$ ,  $\tau_m$ ,  $\tau_p$ , and  $k$ , assuming an zero order reaction occurs in the ideal reactors of this steady state system.



Assume outlet concentrations of each reactor are  $C_m$  and  $C_p$ , respectively.

The performance equations for each reactor are:

$$\tau_m = (C_o - C_m)/k$$

$$\tau_p = (C_o - C_p)/k$$

$$C_m = C_o - k\tau_m$$

$$C_p = C_o - k\tau_p$$

The mass balance around the mixing point gives

$$(q_m C_m + q_p C_p)/(q_m + q_p) = C_{out}$$

Re-arranging and substituting for  $C_m$  and  $C_p$  gives

$$C_{out} = [q_m(C_o - k\tau_m) + q_p(C_o - k\tau_p)]/(q_m + q_p)$$

Problem 2.

An enzymatic reaction is conducted in 2 ideal reactors in series (1 mfr, 1 pfr).

Data:

$K_m = 10 \text{ mol/L}$        $V_m = 5 \text{ mol/L-min}$        $C_0 = 100 \text{ mol/L}$        $q = 15 \text{ L/min}$   
MFR volume = 300 L      PFR volume = 150 L

- Calculate the overall conversion if the MFR is first.
- Calculate the overall conversion if the PFR is first.

m-m  
Mixed reactor  $-r_A = \frac{V_m C_A}{K_m + C_A}$

$$\tau_m = \frac{C_{A0} - C_A}{-r_A} = \frac{C_{A0} - C_A}{\frac{V_m C_A}{K_m + C_A}}$$

$$= \frac{(C_{A0} - C_A)(K_m + C_A)}{V_m C_A}$$

$$= \frac{C_{A0} K_m + (C_{A0} - K_m) C_A - C_A^2}{V_m C_A}$$

$$= \frac{C_{A0} K_m + (C_{A0} - K_m) C_{A0}(1 - X_A) - C_{A0}^2(1 - X_A)^2}{V_m C_{A0}(1 - X_A)}$$

$$= \frac{K_m}{V_m(1 - X_A)} + \frac{C_{A0} - K_m}{V_m} - \frac{C_{A0}(1 - X_A)}{V_m}$$

m-m  
PFR

$$\tau_p = \int \frac{dC_A}{r_A} = \int - \frac{dC_A (K_m + C_A)}{V_m C_A}$$

$$= - \frac{K_m}{V_m} \ln \left( \frac{C_A}{C_{A0}} \right) - \frac{1}{V_m} (C_A - C_{A0})$$

$$= \frac{K_m}{V_m} \ln \left( \frac{1}{1 - X_A} \right) + \frac{1}{V_m} C_{A0} X_A$$

Part 2 a, MFR first

$$C_{1m} = 27.016$$

$$C_{2p} = 2.181$$

$$X_1 := \frac{C_0 - C_{2p}}{C_0}$$

$$X_1 = 0.978$$

Part 2 b. PFR first

$$C_{1p} = 55.829$$

$$C_{2m} = 8.858$$

$$X_2 := \frac{C_0 - C_{2r}}{C_0}$$

$$X_2 = 0.911$$

### Problem 3.

A pulse tracer of dye is injected into the product stream of a reactor. The color of the output stream is recorded at five second intervals.

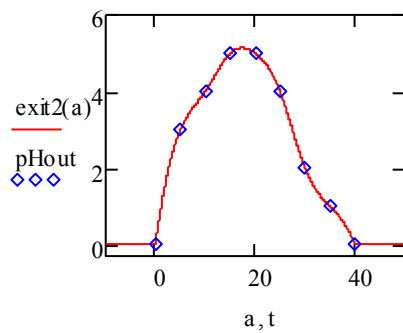
Plot the E(t) curve for this system.

Please refer to the example 11.1 in text.

$$t := \begin{pmatrix} 0 \\ 5 \\ 10 \\ 15 \\ 20 \\ 25 \\ 30 \\ 35 \\ 40 \end{pmatrix} \quad pHout := \begin{pmatrix} 0 \\ 3 \\ 4 \\ 5 \\ 5 \\ 4 \\ 2 \\ 1 \\ 0 \end{pmatrix}$$

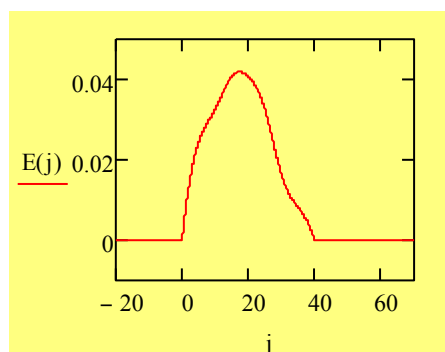
$$Area = \sum C \Delta t$$

$$\mathbf{E} = \frac{C}{area}$$



Find area under curve= 120

Normalize to get the E(t) curve to area = 1.



E curve