



$$P_{tank}^{max} = 1.1 \cdot 2.5 \text{ bara} = 2.75 \text{ bara}$$

- ① Vent vapor/gas
- ② Vent liquid

$$Ma = \min \left( 1, \sqrt{\frac{P_{tank}}{P_{atm}}} \right)$$

$$\dot{m} = M_w \cdot P_0 \cdot A \cdot \sqrt{\frac{\gamma}{R T M_w}} \cdot 1 \cdot \left[ 1 + \frac{(\gamma-1)}{2} Ma^2 \right]^{\frac{\gamma+1}{2-\gamma}}$$

$\dot{m} = 5 \frac{kg}{sec}$

$P_0 = 2.75 \text{ bara}$

$A = ?$

$\gamma = 1.4$

$R = 8.314$

$T = 298K$

$M_w = 18$

= soup # but what is A? or what  $\dot{m}$ ?

Next step? to get A?

What is  $\dot{m}_{gas}$ ? or how is the volume changing?

$$\dot{m}_{H_2O} = 5 \frac{kg}{sec}$$

$$\dot{V}_{water} = \frac{\dot{m}_{water}}{\rho_{water}} = \dot{V}_{gas}$$

$$P_{gas} \dot{V}_{gas} = \dot{m}_{out, gas}$$

not constant

$$P_{gas} (@ P = P_{tank}^{max})$$

venty condition

2.75 bara

Will  $A_{gas}$  sufficient for liquid?

$$\dot{m} = A C_d \sqrt{2 \rho (P_{tank} - P_{atm})}$$

$C_d = 0.65$

liquid density

$$\dot{m} = 5 \frac{kg}{sec}$$

$$[=] \frac{m^2}{s} \sqrt{\frac{kg}{m^3} \cdot \frac{Pa}{N/m^2}} [=] \frac{m^2}{s} \cdot \frac{kg}{m^3}$$

$$A = \frac{\dot{m}}{C_d \sqrt{2 \rho (P_{tank} - P_{atm})}}$$