

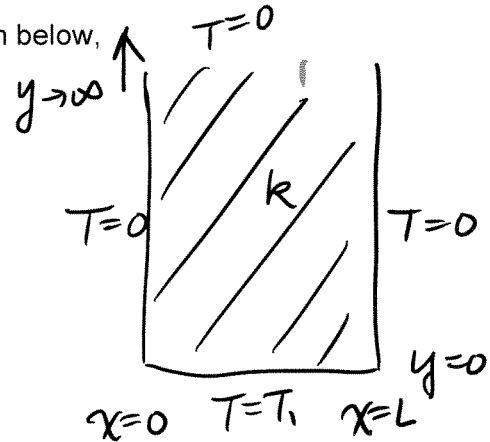
Problem I. Short answer questions. (20 points) For true/false questions, please correct the incorrect part(s) or explain why it is wrong. For multiple choice questions, circle the correct answer.

1. (3 pts) For a semi-infinite 2-D slab at steady state as shown below, simplify the heat transfer equation.

$$\nabla \cdot k \nabla T + \dot{q} = \rho C_v \frac{DT}{Dt} \quad \text{s.s.} \\ \text{no gen.} \quad \text{solid}$$

$$k \nabla^2 T = 0 \Rightarrow \nabla^2 T = 0$$

$$\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} = 0$$



2. (7 pts) The solution for problem 1 is

$$T(x, y) = (A \cos \lambda x + B \sin \lambda x) (C e^{\lambda y} + D e^{-\lambda y})$$

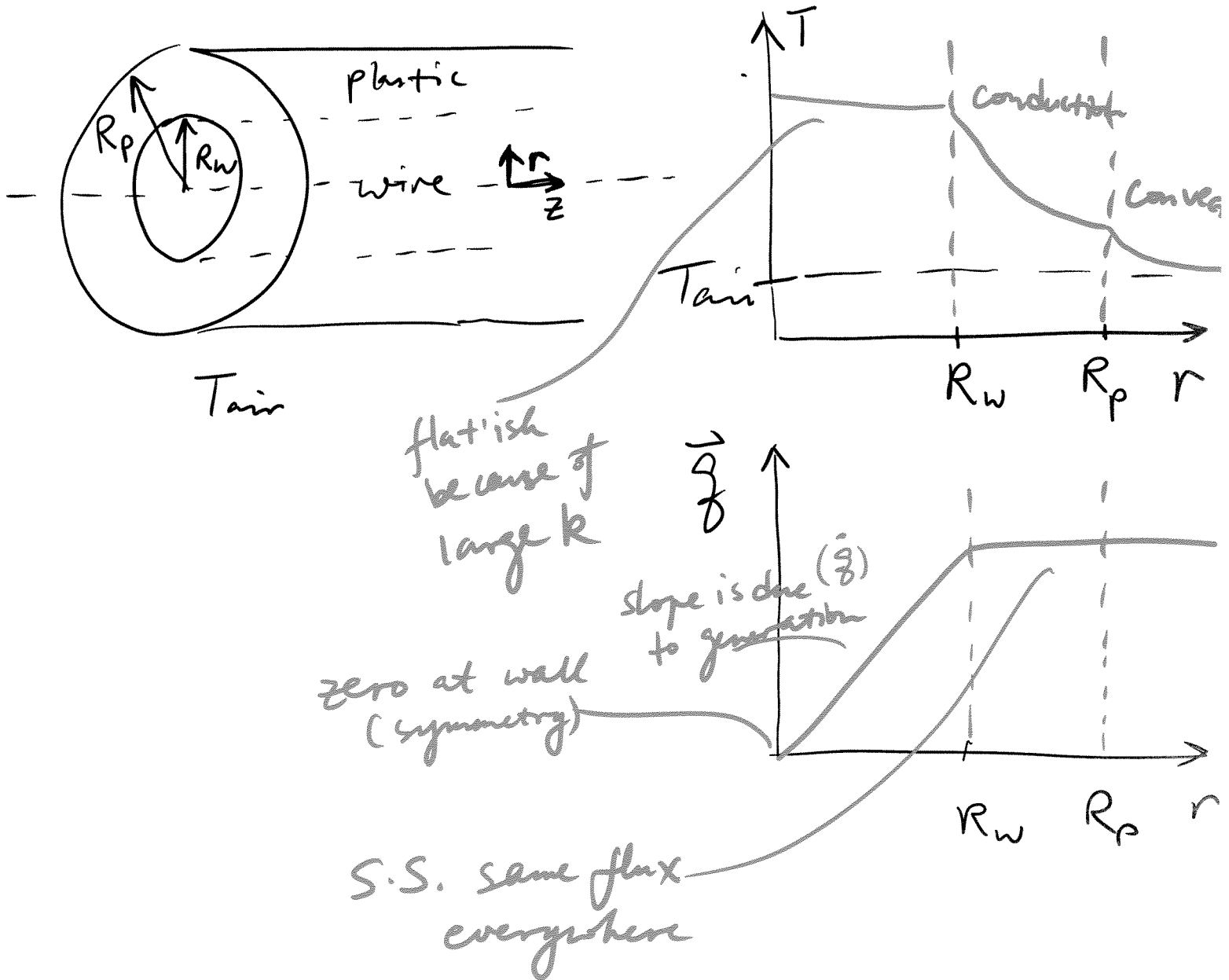
Use the boundary conditions and determine A and C.

- B.C.
- ① $x=0 \quad y>0 \quad T=0$
 - ② $x=L \quad y>0 \quad T=0$
 - ③ $0 < x < L \quad y=0 \quad T=T_1$
 - ④ $0 < x < L \quad y \rightarrow \infty \quad T=0$

use ④ $T=0$ for all x , so $C e^{\lambda y} + D e^{-\lambda y} = 0$
 when $y \rightarrow \infty$, $C e^{\lambda y} = 0 \Rightarrow C = 0$

use ①, $T=0$ for all $y>0$, so $A \cos \lambda x + B \sin \lambda x = 0$
 when $x=0$ $A \cos \lambda x = 0 \Rightarrow A = 0$

3. (10 pts) For a thin and long electrical wire that is resistively heated up (by applying a voltage across), assume the thermal conductivity of the wire to be much higher than that of the plastic. Draw the T profile and the heat flux profile as a function of radius, and give some reasons for the features of these curves.



2.

$$q = \frac{(T_{\text{oo, inner}} - T_{\text{oo, out}})}{\sum R} = \frac{(90^\circ\text{C} - 25^\circ\text{C})}{\sum R} = \frac{65}{\sum R}$$

$$q = \frac{65}{R_{\text{conv. H}_2\text{O}} + R_{\text{cond}} + R_{\text{conv. air}}}$$

$$R_{\text{cond}} = \frac{\ln(r_2/r_1)}{2\pi r} = \frac{\ln(.016\text{m}/.013\text{m})}{(2\pi)(20\text{W/mK})} = 1.65 \times 10^{-3} \text{ mK/W}$$

↙ conduction thru inner pipe

$$R_{\text{conv. H}_2\text{O}} = (hA)^{-1} = (h2\pi R)^{-1} = [(5000\text{W/m}^2\text{K})(2\pi)(.013\text{m})]^{-1} = 2.45 \times 10^{-3} \text{ mK/W}$$

$$R_{\text{conv. air}} = (h_{\text{air}} [A_o + \eta_f A_f])^{-1}$$

$$h_{\text{air}} = 200 \text{ W/m}^2\text{K}$$

$$A_o = 2\pi(.016\text{m}) \cdot (4\text{ fins})(.003\text{m}) = .6885 \text{ m}$$

$$A_f = \underset{\substack{\uparrow \\ \text{top} + \\ \text{bottom}}}{2} (.024\text{m})(4\text{ fins}) = .192 \text{ m}$$

$$L \sqrt{\frac{h}{kt}} = (.024) \left[\frac{200}{20 \times .0015\text{m}} \right]^{\frac{1}{2}} = 1.95$$

↑
"t" not "2t"

From chart

$$\eta_f \approx .50$$

$$R_{\text{conv. air}} = \left[200 \frac{\text{W}}{\text{m}^2\text{K}} (.6885 + (.5)(.192)) \right]^{-1} = 27.103 \times 10^{-3} \frac{\text{mK}}{\text{W}}$$

$$q_{\text{TOTAL}} = \frac{65}{(2.45 \times 10^{-3} \text{ mK/W}) + (1.65 \times 10^{-3} \text{ mK/W}) + (27.103 \times 10^{-3} \text{ mK/W})}$$

$q_{\text{TOTAL}} = 2083 \text{ W/m}$

3.

Known: $D_p = 0.27 \text{ mm} = 2.7 \times 10^{-4} \text{ m}$
 $\rho = 2400 \text{ kg/m}^3$
 $\epsilon_{p.b.} = 0.4$
 $\epsilon_{mf} = 0.45$
 $D = 0.2 \text{ m}$ $L_{p.b.} = 0.1 \text{ m}$
 $\rho_a = 1.275 \text{ kg/m}^3$
 $\mu = 1.9 \times 10^{-5} \text{ Pa}\cdot\text{s}$

(1) Min. fluidization

$$\frac{1.75}{\epsilon_{mf}^3} R_{mf}^2 + \frac{150(1-\epsilon_{mf})}{\epsilon_{mf}^3} R_{mf} - \frac{D_p^3 \rho_s \rho_g}{\mu} = 0 \quad \rho_p \gg \rho_f$$

Plug in #'s,

$$\frac{1.75}{0.45^3} R_{mf}^2 + \frac{150(1-0.45)}{0.45^3} R_{mf} - \frac{(2.7 \times 10^{-4})^3 (1.275)(2400)(98)}{(1.9 \times 10^{-5})^2} = 0$$

$$19.2 R_{mf}^2 + 905.3 R_{mf} - 1630 = 0$$

Solve quadratic eqn., take (+) root

$$R_{mf} = 1.74$$

$$R_{mf} = \frac{D_p \rho v'}{\mu} \Rightarrow v' = \frac{(1.74)(1.9 \times 10^{-5})}{(2.7 \times 10^{-4})(1.275)}$$

$$= 0.096 \text{ m/s}$$

$$= \boxed{9.6 \text{ cm/s}}$$

$$(2) \quad L_1 (1 - \epsilon_1) = L_2 (1 - \epsilon_2)$$

packed min. fluidized

$$(0.11)(1 - 0.4) = L_{mf} (1 - 0.45)$$

$$\Rightarrow L_{mf} = 0.109 \text{ m} = 10.9 \text{ cm}$$

$$\begin{aligned} \Delta P &= L_{mf} (1 - \epsilon_{mf}) (\rho_r - \rho_f) g \\ &= (0.109)(1 - 0.45)(2400 - 1.275)(9.8) \\ &= \boxed{1409 \text{ Pa}} \end{aligned}$$

(3) Because $50 \text{ Pa} < 1409 \text{ Pa}$,
the bed is not fluidized

$$\Rightarrow L = 10 \text{ cm}, \quad \epsilon = 0.4$$