## **OP 06**

# Controlling the CO<sub>2</sub>-lipid liquid phase separation via process tuning and lipid structural design

Authors and affiliation

Ying-Chieh Hung<sup>1</sup>, Yuna Tatsumi<sup>1</sup>, Chieh-Ming Hsieh<sup>2</sup>, Shiang-Tai Lin<sup>3</sup>, and Yusuke Shimoyama\*<sup>1</sup>

- <sup>1</sup> Department of Chemical Science and Engineering, Tokyo Institute of Technology, S1-33 2-12-1 Ookayama, Meguro-ku, Tokyo, 1528550, Japan
- <sup>2</sup> Department of Chemical and Materials Engineering, National Central University, Taoyuan 32001, Taiwan
- <sup>3</sup> Department of Chemical Engineering, National Taiwan University, Taipei 10617, Taiwan
- \*E-mail: yshimo@chemeng.titech.ac.jp

### Key Word

Volume expansion, Supercritical CO<sub>2</sub>, Thermodynamics modeling

#### Abstract

The volume expansion of organic solvent at near critical and supercritical CO<sub>2</sub> (ScCO<sub>2</sub>) is a critical property for designing and optimizing ScCO<sub>2</sub>-mediated process. The lipid expansion behavior in the ScCO<sub>2</sub> is found to be a dominant factor toward ScCO<sub>2</sub> ani-solvent precipitation process, liposome capsule production using ScCO<sub>2</sub>, and ScCO<sub>2</sub> assisted lipid extraction process[1-5]. In this work, the oleic acid, linoleic acid, and 1-octadecene are selected to perform measurement of liquid volume expansion during CO<sub>2</sub> pressurization at a pressure–volume–temperature (PVT) cell with visible window, to investigate the role of carboxyl group and double bond to CO<sub>2</sub> dispersion behavior in the lipid at pressure range of 5 MPa to 20 MPa, temperature range of 308 K to 338 K.

It is found that the dispersion behavior of  $CO_2$  in the liquid phase is dominated by the carboxyl group on the lipid. The temperature and pressure dependent liquid expansion in  $CO_2$  environment is reasonably fitted by Peng-Robinson equation of state combining with Wong-Sandler mixing. From analysis of molecular  $\sigma$ -profile, carboxyl group and double bond shows strong and weak hydrophilic character, respectively. Both functional groups are disadvantage of  $CO_2$  dispersion into liquid lipid, leading to  $CO_2$ -lipid phase separation at high pressure region (P > 15MPa).

## References

- [1] C. Dejoye, M.A. Vian, G. Lumia, C. Bouscarle, F. Charton, F. Chemat, Combined Extraction Processes of Lipid from Chlorella vulgaris Microalgae: Microwave Prior to Supercritical Carbon Dioxide Extraction, International Journal of Molecular Sciences, 12 (2011) 9332-9341.
- [2] C. Pando, A. Cabañas, I.A. Cuadra, Preparation of pharmaceutical co-crystals through sustainable processes using supercritical carbon dioxide: a review, RSC Advances, 6 (2016) 71134-71150.
- [3] C. Brandenbusch, B. Bühler, P. Hoffmann, G. Sadowski, A. Schmid, Efficient phase separation and product recovery in organic-aqueous bioprocessing using supercritical carbon dioxide, Biotechnology and Bioengineering, 107 (2010) 642-651.
- [4] A. Tabernero, E.M. Martín del Valle, M.A. Galán, Supercritical fluids for pharmaceutical particle engineering: Methods, basic fundamentals and modelling, Chemical Engineering and Processing: Process Intensification, 60

(2012) 9-25.

[5] I. Pasquali, R. Bettini, F. Giordano, Supercritical fluid technologies: An innovative approach for manipulating the solid-state of pharmaceuticals, Advanced Drug Delivery Reviews, 60 (2008) 399-410.

MTMS '21