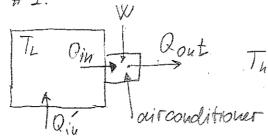
Homework # 6

PE #1.



Qin - heat removed by AC from a room
Q'un - heat entering the room through walls.

W - work done by AC.

- 1) AC efficiency $COP = \frac{Qin}{W} = \frac{Qin}{Qout} = \eta$ From 2d lane $\frac{Qin}{T_L} = \frac{Qout}{T_h} = \frac{Qin}{T_h} = \frac{T_L}{T_h} = \eta$
- Det fin be any heat flow, amount of heat per second removed by AC from the room.

 Fin = P. y, where P is electrical power consupption

 Fin = P. T.
- (3) $F_{in} = A(T_h T_L)$ heat flow into the room through walls. Steady stocte. Is when $F_{in} = F_{in}$ $P = \frac{T_L}{T_h - T_L} = A(T_h - T_L)$, we want to know T_L

$$A T_{L}^{2} - (2AT_{h} + P) T_{L} + AT_{h}^{2} = 0.$$

$$T_{L} = \frac{(2AT_{h} + P) - \sqrt{(2AT_{h} + P)^{2} - 4AT_{h}^{2}}}{2A.} = \frac{(2AT_{h} + P) - \sqrt{(2AT_{h} + P)^{2} - 4AT_{h}^{2}}}{2A.} = \frac{(T_{h} + \frac{P}{2A}) - \left[(T_{h} + \frac{P}{2A})^{2} - T_{h}^{2} \right]^{\frac{1}{2}}}{2A.}$$

Comment
"+" sign in the root
of this quadratic
equation is not
physical.

 $A = \frac{P \cdot T_L}{(T_L - T_L)^2} = \frac{2 \cdot 10^3 \cdot 290}{(20)^2} = \frac{290}{2} = 1450 \frac{\text{W}}{\text{E}}.$

HW #6 Problem #3

There were tres mistakes in the problem statement.

Pst=3kPa (not 34kPa)

L = 2260 1/g (not 25 kg/kg)

Reasoning: When air goer up water condenses. As a result of this vapor -> water phase transtoemation. heat is released and is absorbed by.

air. So we need to find out how much water is

in 1 m³ of air (initially) and make an energy balance.

(a) Partial premise of vapor $P = h \cdot 3kPa = 1.8 \cdot \times 10^{3} Pa$. $PV = \frac{M}{\mu} RT$ $M = \frac{PV\mu}{RT} = \frac{1.8 \cdot 10^{+3} \cdot 1 \cdot 18g}{8 \cdot 31 \cdot 300} = 13g$.

(b) The heat released as a result of vapor acudeusation. $Q = 13 \cdot 2260 = 29,380 \text{ J}.$

(c) Number of moles in 1 m^3 of air PV = V RT $V = \frac{PV}{RT} = \frac{10^5}{8.31 \cdot 300} = 40 \text{ moles}.$

(d) AQ=U-we assume that there is no value change.

\$ R.VOT = 29×1037 DT = 34 K.

Comments: Actual difference in temperature between Santa Cruz and Fresno (they have about the same latitude) is (12 K) Possible reasons for disagrement.:

1) Not all water condenser. (relative humidity in Fremo ~25%, in afternoon. This alone will bring our extinate down to BT= apr. (2) The air coming to Fremo not only from Sterra Newada.

3) Process is not completely adiabatic. air picks up some cold from toos of mountains.

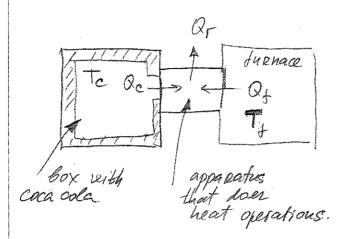
Homework # 6

PR#2

- (a) $\triangle G = 2(-237, 13 \text{ kg}) + (-394.36 \text{ kg}) (-50.72 \text{ kg}) = -817.9 \text{ kg}$ $\triangle H = 2(-285.23 \text{ kg}) + (-393.51 \text{ kg}) - (-74.81) \text{ kg} = -.890.36 \text{ kg}$
- (b) Under ideal condition all of the decrease in 6 common out as electrical work => W = 818 kg.
- (c) Wast heat Q=AH-AG=-72 kJ (negative SIGN)
 means that heat goes out of the fuel cell.
- (d) Voltage = electrical work done =

$$=\frac{818 + 5}{(8) \cdot (6.02 \times 10^{+23})(1.6 \times 10^{-19}c)} = 1.06 V$$

Home work #6 Problem #4 extra credit



(a)
$$Q_e + Q_f = Q_f$$
 $cgp = \frac{Q_e}{Q_f} = g = \frac{Q_e}{Q_r - Q_e}$

(c) 2nd lane
$$\rightarrow$$
 (deal operation \rightarrow no entropy production.

$$S_{c} + S_{f} = S_{R} \qquad \frac{Q_{c}}{T_{c}} + \frac{Q_{t}}{T_{f}} = \frac{Q_{r}}{T_{r}} = \frac{Q_{t} + Q_{c}}{T_{r}}$$

$$J \cdot \frac{1}{T_{c}} + \frac{1}{T_{f}} = \frac{1}{T_{r}} + \frac{1}{T_{r}} y$$

$$1 - 1 = T_{r} + T_{r} y$$

$$J = \frac{\frac{1}{7} - \frac{1}{7}}{\frac{1}{7} - \frac{1}{7}} = \frac{T_{e}(T_{f} - T_{f})}{T_{f}(T_{f} - T_{e})}$$

(b) Coefficient of performance can be larger than I