Problem 1

Part 1

[illegible]

Therefore

[illegible]

Since $Deg(B)$ is clearly 0, [illegible]

[illegible]

In order for minimum phase to be achieved, the following conditions on the degrees of the polynomials making up the system must be met and will ultimately guide the desing.

[illegible]

Since $Deg(B^-) = 0$ then $Deg(B^+) = 1$ and therfore

[illegible]

Additionally, considering the polynomial degrees derived above, we know that

[illegible]

The Diophantine equation in terms of control parameters is given by

[illegible]

Grouping the coefficients of the same ordered z terms and solving for the control parameters yields

[illegible]

Part 2

ODE of Plant

[illegible]

The ODE of 2nd order describing the process is given by

[illegible]

where p is the time shifting operator. The reliance of the RHS of the equation on derivatives can be changed to integrals by filtering the input u(t) and output y(t) of the plant by a filter whose denominator polynomial is of a greater order than the highest derivative term. The above equation becomes

[illegible]

For simplicity, let $(d+1) = a$. The ODE then becomes

[illegible]

This equation can be further simplified as

[illegible]

This equation will be used for the measurement model i.e.

[illegible]

Bilinear Transformation of Filtered ODE

[illegible]

The filter $H_f(p)$ is given to be

[illegible]

This filter, and the ODE above, are however, in terms of p and are therefore, in continuous time domain. To convert the filter to discrete time (q), a bilinear transformation will be performed i.e.

[illegible]

The ODE can now be represented in the discrete time domain by

[illegible]

[illegible]

The equations for the filtered output and input y_{f1}, y_{f2} and u_{f1} equations are

[illegible]

An equation for $y(kT)$ can be obtained by isolating the $y(kT)$ term in the $y_{f1}(kT)$ equation. The $y_{f1}(kT)$ equation is

[illegible]

Isolating $y(kT)$ gives

[illegible]

The above equation depends only on present and past values of $y_{f1}(kT)$, in which the present value can be obtained via the measurment model $\phi^T(t)\theta$ and past values of $y_{f1}(kT)$.

Bilinear Transformation of Control Signal u(t)

[illegible]

The control signal of the system is given by

[illegible]

This however, must also be converted to the discrete time domain with a bilinear transformation as well. This will be done by directly performing the transformation on $\frac{T}{R}$ and $\frac{S}{R}$ (no filtering) and using the α and β coefficients to derive difference equations for $u_c(kT)$ and $y(kT)$ respectively.

The bilinear transformations of $\frac{T}{R}$ and $\frac{S}{R}$ are

[illegible]

For $\frac{T}{R}$, the coefficients of the numerator and denominator are

[illegible]

while the coefficients of the numerator and denominator for $\frac{S}{R}$ are

[illegible]

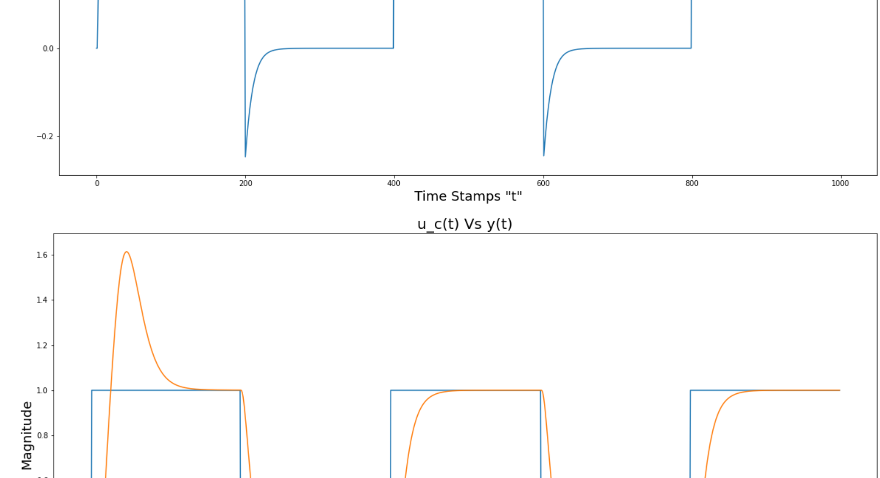
The difference equation representing the control signal becomes

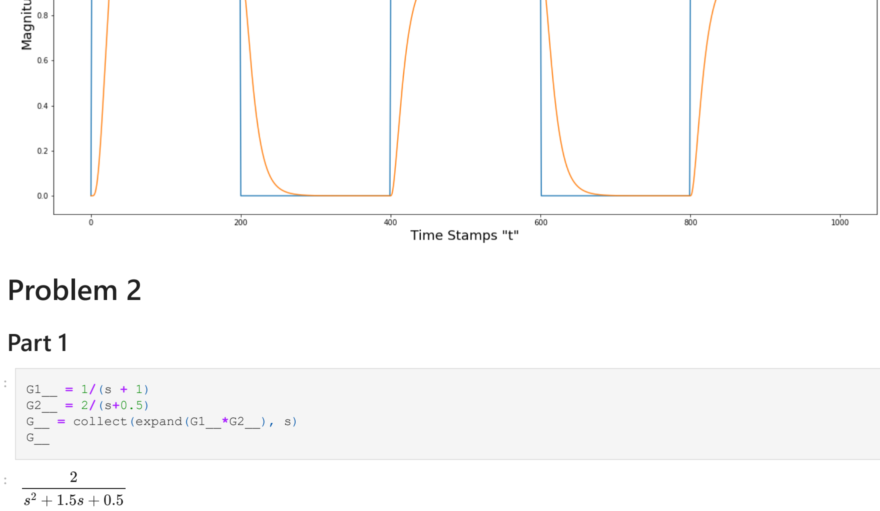
[illegible]

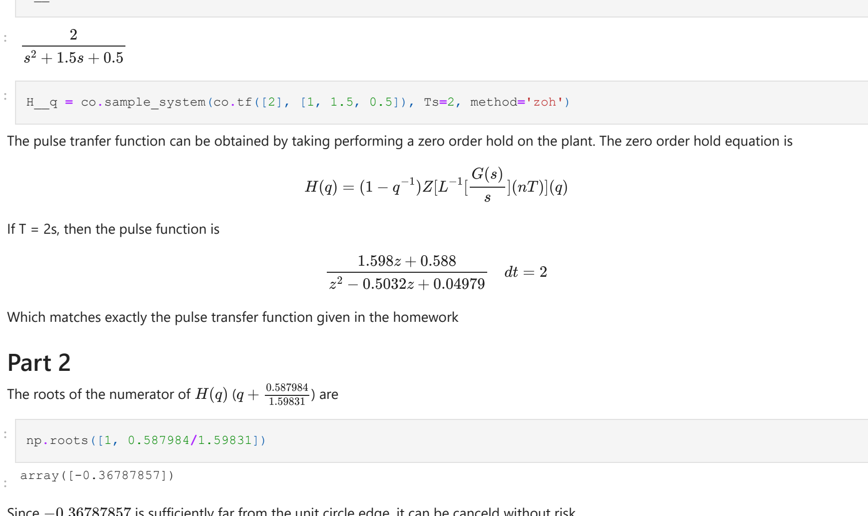
Part 3

[illegible]

[illegible]







Problem 2

Part 1

[illegible]

Part 2

[illegible]

```
A = q**2 + a1*q + a2
B = b0*q + b1

A_pol = sp.Poly(A)
B_pol = sp.Poly(B)

B_minus = b0
B_plus = simplify(B/B_minus)
H = B/A
```

$B = B^-B^+ = (b_0)(q + \frac{b_1}{b_0})$

Therfore,

$$Deg(B^-) = 0$$

and

$$Deg(B^+) = Deg(B) = Deg(B_m) = 1$$

Additionally

$$Deg(A) = Deg(A_m) = 2$$

$$Deg(S) = Deg(R) = Deg(A) - 1 = 2 - 1 = 1$$

$$Deg(R^{'}) = Deg(R) - Deg(B^+) = 1 - 1 = 0$$

$$Deg(A_0) = Deg(A) + Deg(R^{'}) - Deg(A_m) = 2 + 0 - 2 = 0$$

In [22]:
```
A0 = 1
S = s0*q + s1
R = q + r1
R_prime = 1
Am = q**2 + am1*q + am2
Bm = Am.subs(q,1)*q**B_pol.degree()
# T = simplify(A0*Bm/B_minus)
T = q*t0
```

The control polynomials become

$A_0 = 1$

$S = qs_0 + s_1$

$R = q + r_1$

$R^{'} = 1 \quad \Rightarrow \quad R = B^+R^{'} = B^+ = q + \frac{b_1}{b_0}$

$A_m = a_{m1}q + a_{m2} + q^2$

Additionally, to achive unity gain, the final value theorem can implemented on A_m to obtain the value of B_m. This is achived by the equation $B_m = A_m(1)q^m$.This way, when k goes to infinity ($q \rightarrow 1$), $G_m = 1$ and $Deg(B_m) = Deg(B)$. Therfore,

$B_m = q\left(a_{m1} + a_{m2} + 1\right)$

From this result, T can be calculated

$T = A_0\frac{B_m}{B^-} = \frac{q\left(a_{m1} + a_{m2} + 1\right)}{b_0} = qt_0$

In [23]:
```
LHS_coeffs = sp.Poly(A*R_prime + B_minus*S, q).coeffs()[::-1]
RHS_coeffs = sp.Poly(A0*Am, q).coeffs()[::-1]

r_1 = b1/b0
s_0 = sp.solve(sp.Eq(LHS_coeffs[1], RHS_coeffs[1]), s0)[0]
s_1 = sp.solve(sp.Eq(LHS_coeffs[0], RHS_coeffs[0]), s1)[0]
t_0 = (am1 + am2 + 1)/b0
```

We can see that

$r_1 = \frac{b_1}{b_0}$

and

$t_0 = \frac{a_{m1} + a_{m2} + 1}{b_0}$

Solving the diophantine equation

$AR^{'} + B^-S = A_0A_m \quad \Rightarrow \quad a_1q + a_2 + q^2 \ + b_0qs_0 + s_1 = a_{m1}q + a_{m2} + q^2$

yeilds the following control paramters

$s_0 = \frac{-a_1 + a_{m1}}{b_0}$

$s_1 = \frac{-a_2 + a_{m2}}{b_0}$

In [24]:
```
S_ = S.subs([(s0, s_0), (s1, s_1)])
R_ = R.subs(r1, r_1)
T_ = T.subs(t0, t_0)
```

The control polynomials in terms of control parameters are

$R = q + \frac{b_1}{b_0}$

$S = \frac{q\left(-a_1 + a_{m1}\right)}{b_0} + \frac{-a_2 + a_{m2}}{b_0}$

$T = \frac{q\left(a_{m1} + a_{m2} + 1\right)}{b_0}$

Part 3

We know that the pulse transfer function is of the form

$H(q) = \frac{b_0q + b_1}{a_1q + a_2 + q^2}$

Therefore, the measurment model can be found to be

$y(t+2) = -a_1y(t+1) - a_2y(t) + b_0u(t+1) + b_1u(t)$

$\Rightarrow y(t) = -a_1y(t-1) - a_2y(t-2) + b_0u(t-1) + b_1u(t-2)$

Therfore

$y(t) = \phi^T(t)\theta = [-y(t-1) \ \ -y(t-2) \ \ u(t-1) \ \ u(t-2)][a_1 \ a_2 \ b_0 \ b_1]^T$

Control equation u(t)

In [25]:
```
TR = simplify(T_/R_)
SR = simplify(S_/R_)

obj_TR = numden_coeff(TR, q)
obj_SR = numden_coeff(SR, q)

aTR = obj_TR.lst_denum_coeff
bTR = obj_TR.lst_num_coeff

aSR = obj_SR.lst_denum_coeff
bSR = obj_SR.lst_num_coeff
```

For $\frac{T}{R}$, the coefficients of the numerator and denominator are

$\alpha\frac{T}{R} = \left[1, \ \frac{b_1}{b_0}\right]$

and

$\beta\frac{T}{R} = \left[\frac{a_{m1} + a_{m2} + 1}{b_0}, \ 0\right]$

while the coefficients of the numerator and denominator for $\frac{S}{R}$ are

$\alpha\frac{S}{R} = \left[1, \ \frac{b_1}{b_0}\right]$

and

$\beta\frac{S}{R} = \left[\frac{-a_1 + a_{m1}}{b_0}, \ \frac{-a_2 + a_{m2}}{b_0}\right]$

In [26]:
```
u_k, u_k_1, uc_k, y_k, y_k_1, y_k_2 = sp.symbols('u(k) u(k-1) u_{c}(k) y(k) y(k-1) y(k-2)')

uk = -u_k_1*aTR[1] + uc_k*bTR[0] - y_k*bSR[0] - y_k_1*bSR[1]
```

The control equation in terms of the plant and model parameters is

$u(t) = -\frac{b_1u(k-1)}{b_0} + \frac{u_c(k)\left(a_{m1} + a_{m2} + 1\right)}{b_0} - \frac{y(k)\left(-a_1 + a_{m1}\right)}{b_0} - \frac{y(k-1)\left(-a_2 + a_{m2}\right)}{b_0}$

In [27]:
```
co.sample_system(co.tf([1], [1, 2, 1]), Ts=2, method='zoh') # pulse transfer function of model
```

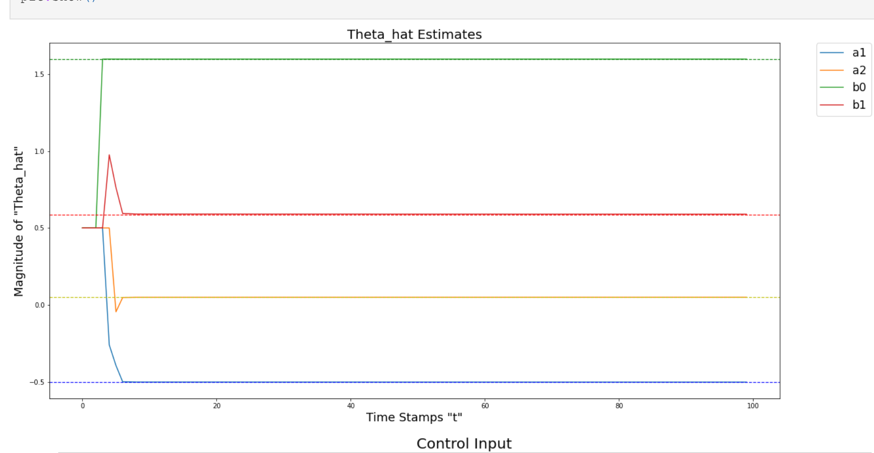
Out[27]:

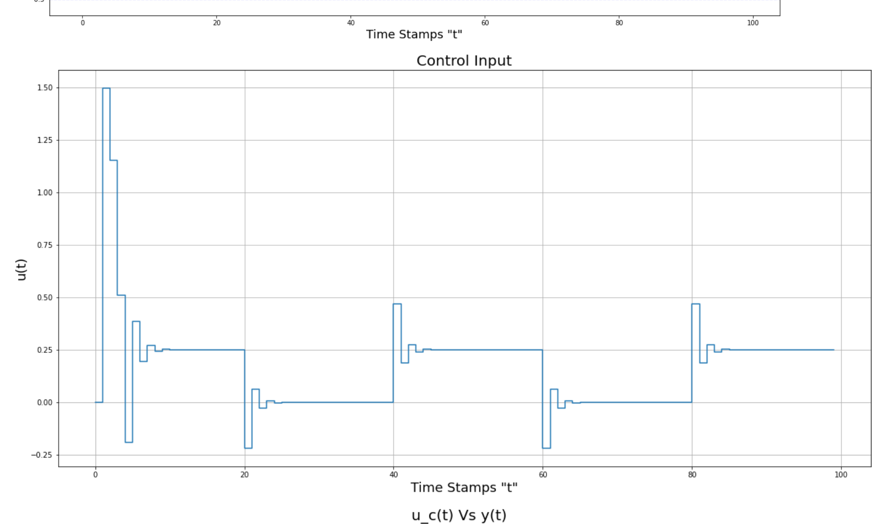
$$\frac{0.594z + 0.1537}{z^2 - 0.2707z + 0.01832} \quad dt = 2$$

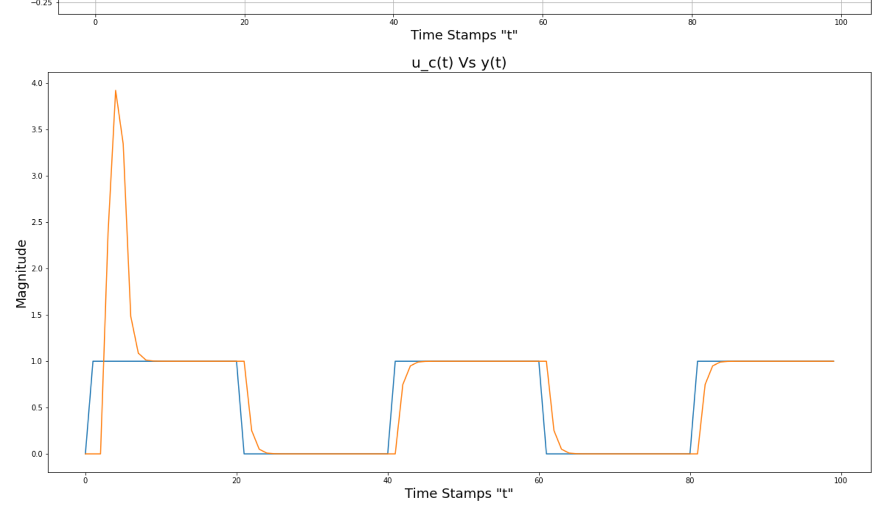
We can see from the pulse transfer function of model above that $a_{m1} = -0.2707$ and $a_{m2} = 0.01832$

Part 4

In [28]:
```
# Tunable components vvvvvvvvvvvvvvvvvvvvvvvvvvvvvvvvvv
sample_depth = 100
starting_samples = 2

# starting estimate for plant parameters
est = 0.5

lam = 1 # forgeting factor lambda

# true plant parameters
a_1 = -0.503215
a_2 = 0.0497871
b_0 = 1.59831
b_1 = 0.587984
theta0 = np.array([a_1, a_2, b_0, b_1]).reshape(-1,1)

# Tunable components ^^^^^^^^^^^^^^^^^^^^^^^^^^^^^^^^^^

theta_hat = [np.array([est]*len(theta0)).reshape(-1,1) for _ in range(starting_samples)]

# model parameters
a_m1 = -0.2707
a_m2 = 0.01832

# Convert control equation derived above symbolically into numeric function
uk_subd = uk.subs([(am1, a_m1), (am2, a_m2)]) # subing in true values for am1 and am2 into control input funct
uk_func = sp.lambdify([u_k_1, uc_k, y_k, y_k_1, a1, a2, b0, b1], uk_subd)

# System input
sample_range = range(sample_depth)
t = [i for i in sample_range]
u_c = np.ones(sample_depth)
u_c[np.where([m.sin(t[i]*m.pi/20)<=0 for i in sample_range])] = 0

y = [0]*starting_samples
u = [0]*starting_samples

I = np.identity(len(theta0))
p = 1000*I

for k in range(starting_samples ,sample_depth):
    phi = np.array([-y[-1], -y[-2], u[-1], u[-2]]).reshape(-1,1)

    y.append(np.reshape(phi.T@theta0, ()))
    K = p@phi@inv(lam + phi.T@p@phi)
    p = (I - K@phi.T)@p/lam
    theta_hat.append(theta_hat[-1] + K*(y[k] - phi.T@theta_hat[-1]))

    u.append(np.reshape(uk_func(u[k-1], u_c[k], y[k], y[k-1],
                                theta_hat[-1][0], theta_hat[-1][1],
                                theta_hat[-1][2], theta_hat[-1][3]), ()))

# ploting of estimated parameters
df_theta = pd.DataFrame(np.asarray(theta_hat).reshape(-1,4,), columns=['a1', 'a2', 'b0', 'b1'])
theta_hat_ploter(df_theta, theta0, 'Theta_hat Estimates')

# ploting of control sig
plt.step(t,u)
plt.title('Control Input', fontsize=20)
plt.ylabel('u(t)', fontsize=18)
plt.xlabel('Time Stamps "t"', fontsize=18)
plt.grid()
plt.show()

# ploting of input vs output
plt.plot(t,u_c)
plt.plot(t,y)
plt.title('u_c(t) Vs y(t)', fontsize=20)
plt.ylabel('Magnitude', fontsize=18)
plt.xlabel('Time Stamps "t"', fontsize=18)
plt.show()
```







Part 5

In [29]:
```
x0, y0, r01, s00, s01 = sp.symbols('x_0 y_0 r_{01} s_{00} s_{01}')

Ad = q - 1 # Disturbance filter

# original Control Polynomials
R0 = q + r01
S0 = s00*q + s01
T = q*t0

X = q + x0
Y = y0

X_ = q
Y_ = (-X_*R0/B).subs(q,1)

R = collect(expand(X_*R0 + Y*B),q)
S = collect(expand(X_*S0 - Y*A), q)

r_01 = r_1
s_00 = s_0
s_01 = s_1

b_0 = sp.solve(sp.Eq(Y_, y0), b0)[0]
R_prime = simplify((R/Ad).subs(b0, b_0))
```

x_0 will be chosen to be equal to 0. This introduces a pole at the origin. Since the new R is given by

$A_d\bar{R} = R_0X + YB \Rightarrow (q-1)\bar{R} = (q+r_{01})(q+x_0) + Y(b_0q+b_1)$ Y must be a scalar value to maintain the order of R. This is done by finding the steady state of the above equation and solving for y_0. This gives

$$Y = y_0 = -\frac{r_{01}+1}{b_0+b_1}$$

Pluging this result back into the equation for R gives

$$R = (q(q+r_{01}) + (-\frac{r_{01}+1}{b_0+b_1})(b_0q+b_1) = b_1y_0 + q^2 + q(b_0y_0 + r_{01})$$

Similarly,

$$S = XS_0 - YA = -a_2y_0 + q^2(s_{00}-y_0) + q(-a_1y_0 + s_{01})$$

Derivations of Equations of Filtered System

Filtered Output Equation y_f(t)

$$A_d(q)A(q)y(t) = A_d(q)B(q)(u(t)+v(t))$$

$$\Rightarrow q(1-q^{-1})A(q)y(t) = q(1-q^{-1})B(q)(u(t)+v(t))$$

$$\Rightarrow (1-q^{-1})A(q)y(t) = (1-q^{-1})B(q)(u(t)+v(t))$$

$$\Rightarrow A(q)y_f(t) = B(q)u_f(t) + e(t)$$

$$\Rightarrow (a_1q + a_2 + q^2)y_f(t) = (b_0q+b_1)u_f(t) + e(t)$$

Therefore

$$y_f(t+2) = -a_1y_f(t+1) - a_2y_f(t) + b_0u_f(t+1) + b_1u_f(t)$$

$$\Rightarrow y_f(t) = -a_1y_f(t-1) - a_2y_f(t-2) + b_0u_f(t-1) + b_1u_f(t-2)$$

This means that the measurment model is

$$y_f(t) = \phi^T\theta = [-y_f(t-1)\ -y_f(t-2)\ u_f(t-1)\ u_f(t-2)]\,[a_1\ a_2\ b_0\ b_1]^T$$

Output Equation y(t)

We know that

$$y_f(t) = A_d(q^{-1})y(t)$$

$$\Rightarrow y_f(t) = (1-q^{-1})y(t)$$

$$\Rightarrow y_f(t) = y(t) - y(t-1)$$

$$\Rightarrow y(t) = y_f(t) + y(t-1)$$

Filtered Control Input Equation u_f(t)

Similarly

$$u_f(t) = A_d(q^{-1})u(t)$$

$$\Rightarrow u_f(t) = u(t) - u(t-1)$$

Control Equation u(t)

In [30]:
```
TR = simplify(T/R)
SR = simplify(S/R)

obj_TR = numden_coeff(TR, q)
obj_SR = numden_coeff(SR, q)

aTR = obj_TR.lst_denum_coeff
bTR = obj_TR.lst_num_coeff

aSR = obj_SR.lst_denum_coeff
bSR = obj_SR.lst_num_coeff
```

For $\frac{T}{R}$, the coefficients of the numerator and denominator are

$$\alpha\frac{T}{R} = [1,\ b_0y_0 + r_{01},\ b_1y_0]$$

and

$$\beta\frac{T}{R} = [t_0,\ 0]$$

while the coefficients of the numerator and denominator for $\frac{S}{R}$ are

$$\alpha\frac{S}{R} = [1,\ b_0y_0+r_{01},\ b_1y_0]$$

and

$$\beta\frac{S}{R} = [s_{00}-y_0,\ -a_1y_0+s_{01},\ -a_2y_0]$$

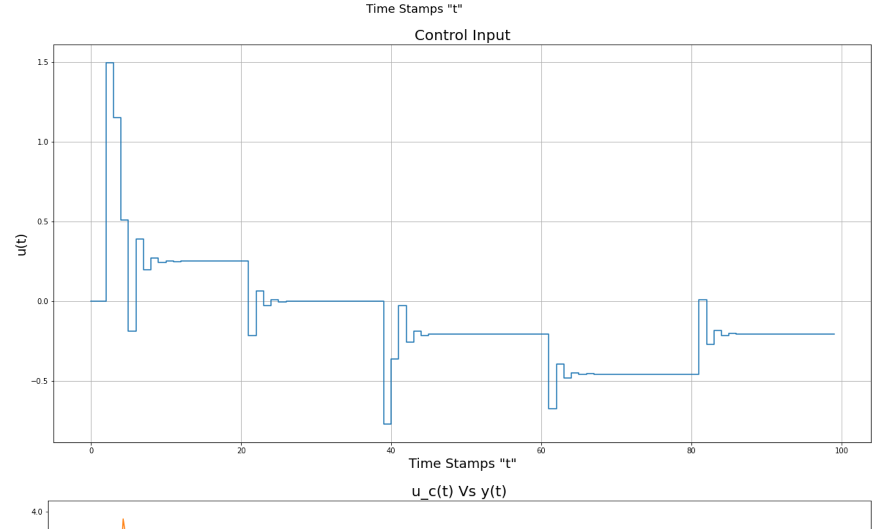
In [31]:
```
u_k_1, u_k_2, uc_k_1, y_k, y_k_1, y_k_2 = sp.symbols('u(k-1) u(k-2) u_{c}(k-1) y(k) y(k-1) y(k-2)')

uk_ = -u_k_1*aTR[1] -u_k_2*aTR[2] + uc_k_1*bTR[0] - y_k*bSR[0] - y_k_1*bSR[1] - y_k_2*bSR[2]
uk = simplify(uk_.subs([(t0, t_0), (y0, Y_), (r01, r_01), (s00, s_00), (s01, s_01)]))
```

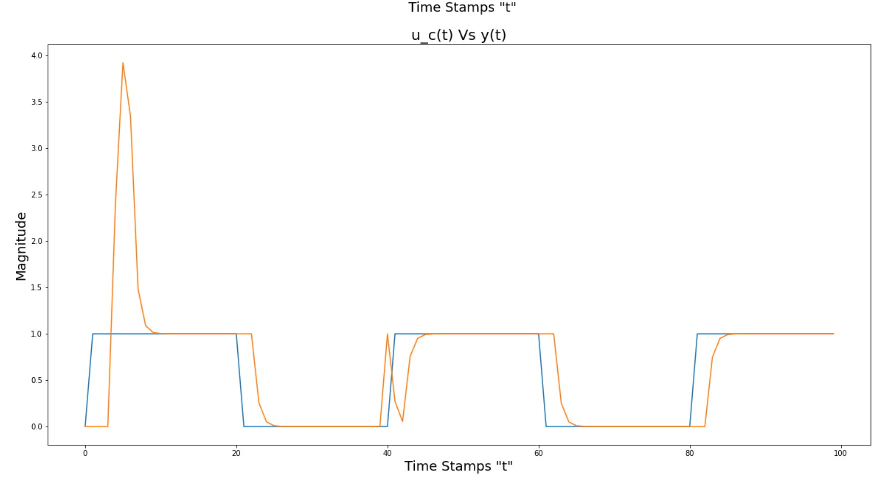
The control equation becomes

$$u(t) = a_2y(k-2)y_0 - b_1u(k-2)y_0 + t_0u_c(k-1) - u(k-1)(b_0y_0+r_{01}) - y(k)(s_{00}-y_0) - y(k-1)(-a_1y_0+s_{01})$$

$$\Rightarrow u(t) = \frac{-a_2y(k-2) + b_1u(k-2) + u(k-1)(b_0-b_1) + u_c(k-1)(a_{m1}+a_{m2}+1) - y(k)(-a_1+a_{m1}+1) - y(k-1)(a_1-a_2+a_{m2})}{b_0}$$

In [32]:
```
# Tunable components vvvvvvvvvvvvvvvvvvvvvvvvvvvvvvvvvv
sample_depth = 100
starting_samples = 3

# starting estimate for plant parameters
est = 0.5

lam = 1 # forgeting factor lambda

# true plant parameters
a_1 = -0.503215
a_2 = 0.0497871
b_0 = 1.59831
b_1 = 0.587984
theta0 = np.array([a_1, a_2, b_0, b_1]).reshape(-1,1)

# Tunable components ^^^^^^^^^^^^^^^^^^^^^^^^^^^^^^^^^^

theta_hat = [np.array([est]*len(theta0)).reshape(-1,1)]

# model parameters
a_m1 = -0.2707
a_m2 = 0.01832

# Convert control equation derived above symbolically into numeric function
uk_subd = uk.subs([(am1, a_m1), (am2, a_m2)])
uk_func = sp.lambdify([u_k_1, u_k_2, uc_k_1, y_k, y_k_1, y_k_2,
                       a1, a2, b0, b1], uk_subd)

sample_range = range(sample_depth)

# system input
t = [i for i in sample_range]
u_c = np.ones(sample_depth)
u_c[np.where([m.sin(t[i]*m.pi/20)<=0 for i in sample_range])] = 0

# system disturbance starting at t=40
dist = np.zeros(sample_depth)
dist[np.where([t[i]>= 40 for i in sample_range])] = 1

y = [0]*starting_samples
u = [0]*starting_samples

yf = [0]*starting_samples
uf = [0]*starting_samples

I = np.identity(len(theta0))
p = 1000*I

for k in range(starting_samples ,sample_depth):
    phi = np.array([-yf[-1], -yf[-2], uf[-1], uf[-2]]).reshape(-1,1)
    yf.append(np.reshape(phi.T@theta0 + dist[k] - dist[k-1], ()))

    K = p@phi@inv(lam + phi.T@p@phi)
    p = (I - K@phi.T)@p/lam

    theta_hat.append(theta_hat[-1] + K*(yf[k] - phi.T@theta_hat[-1]))

    y.append(yf[k] + y[k-1])

    u.append(np.reshape(uk_func(u[k-1], u[k-2], u_c[k-1], y[k], y[k-1], y[k-2],
                        theta_hat[-1][0], theta_hat[-1][1],
                        theta_hat[-1][2], theta_hat[-1][3]), ()))

    uf.append(u[k] - u[k-1])

# ploting of estimated parameters
df_theta = pd.DataFrame(np.asarray(theta_hat).reshape(-1,4,), columns=['a1', 'a2', 'b0', 'b1'])
theta_hat_ploter(df_theta, theta0, 'Theta_hat Estimates')

# ploting of control sig
plt.step(t,u)
plt.title('Control Input', fontsize=20)
plt.ylabel('u(t)', fontsize=18)
plt.xlabel('Time Stamps "t"', fontsize=18)
plt.grid()
plt.show()

# ploting of input vs output
plt.plot(t,u_c)
plt.plot(t,y)
plt.title('u_c(t) Vs y(t)', fontsize=20)
plt.ylabel('Magnitude', fontsize=18)
plt.xlabel('Time Stamps "t"', fontsize=18)
plt.show()
```





Problem 3

In [33]:
```
z1, z0 = sp.symbols('z_1 z_0')

A = q**2 + a1*q + a2
B = b0*q + b1
B_minus = b0
B_plus = simplify(B/B_minus)
[illegible]
A1 = 1

S = q*s0 + s1
R = q + r1
R_prime = 1
T = q*t0 # t0 = (am1 + am2 + 1)/b0
```

Part 1

$$H = \frac{b_0q + b_1}{a_1q + a_2 + q^2}$$

$$B = B^+B^- = (b_0)(q + \frac{b_1}{b_0})$$

Therefore,

$$Deg(B^-) = 0$$

and

$$Deg(B^+) = Deg(B) = Deg(B_m) = 1$$

Additionally

$$Deg(A) = Deg(A_m) = 2$$

$$Deg(S) = Deg(R) = Deg(A) - 1 = 2 - 1 = 1$$

$$Deg(R') = Deg(R) - Deg(B^+) = 1 - 1 = 0$$

$$Deg(A_o) = Deg(A) + Deg(R') - Deg(A_m) = 2 + 0 - 2 = 0$$

The control polynomials become

$A_o = 1$

$S = qs_0 + s_1$

$R = q + r_1$

$R' = 1$

$A_m = a_{m1}q + a_{m2} + q^2$

Additionally, to achive unity gain, the final value theorem can implemented on A_m to obtain the value of B_m. This is achived by the equation $B_m = A_m(1)q^n$ This way, when k goes to infinity ($q \to 1$), $G_m = 1$ and $Deg(B_m) = Deg(B)$. Therefore,

$B_m = q(a_{m1} + a_{m2} + 1)$

From this result, T can be calculated

$T = qt_0$

Output Equation

In [34]:
```
coef_1 = S*B_minus/Am
coef_2 = R*B_minus/Am

coef_1_ = (S*B_minus).subs(q, q**(-1))
coef_2_ = (R*B_minus).subs(q, q**(-1))
```

The diophantine equation can be manipulated to give a formula for the output and subsequently, the measurment model.

$$AR + B^-S = A_oA_m$$

Multiplying both sides of the equation gives

$$ARy(t) + B^-Sy(t) = A_oA_my(t)$$

Since $Ay(t) = Bu(t)$ the above equation becomes

$$R'Bu(t) + B^-Sy(t) = A_oA_my(t)$$

Isolating $y(t)$ on the right hand side of the equation gives

$$y(t) = \frac{1}{A_oA_m}[R'Bu(t) + B^-Sy(t)]$$

Since $R'B = R'B^+B^- = RB^-$ the above equation becomes

$$y(t) = \frac{1}{A_oA_m}[RB^-u(t) + B^-Sy(t)]$$

Substituting A_o, A_m, R, B^- and S with their polynomilas gives

$$y(t) = \frac{b_0(q+r_1)}{a_{m1}q + a_{m2} + q^2}u(t) + \frac{b_0(qs_0 + s_1)}{a_{m1}q+a_{m2}+q^2}y(t)$$

Noting that the numerator of both coefficients will have to be shifted by 2, considering the order of the denominator, we can rewrite the above equation as

$$y(t) = b_0(q^{-1} + r_1q^{-2})u_f(t) + b_0(s_0q^{-1} + s_1q^{-2})y_f(t)$$

Where $u_f(t)$ and $y_f(t)$ are the filtered input and output respectively. Expanding the above equation gives

$$y(t) = b_0u_f(t-1) + b_0r_1u_f(t-2) + b_0s_0y_f(t-1) + b_0s_1y_f(t-2)$$

For simplicity, let $b_0r_1 = r_1'$, $b_0s_0 = s_0'$ and $b_0s_1 = s_1'$. The above equation becomes

$$y(t) = b_0u_f(t-1) + r_1'u_f(t-2) + s_0'y_f(t-1) + s_1'y_f(t-2)$$

Therefore,

$$y(t) = \phi^T\theta = [u_f(t-1),\ u_f(t-2),\ y_f(t-1),\ y_f(t-2)][b_0,\ r_1',\ s_0',\ s_1']^T$$

The equation for $u_f(t)$ is given by

$$u_f(t) = \frac{1}{a_{m2}q^{-2} + a_{m1}q^{-1} + 1}u(t) = \frac{1}{1 + a_{m1}q^{-1} + a_{m2}q^{-2}}u(t)$$

This can then be rearranged to give

$$u_f(t) = -a_{m1}u_f(t-1) - a_{m2}u_f(t-2) + u(t)$$

Similarly, the difference equation for the filtered output $y_f(t)$ is given by

$$y_f(t) = \frac{1}{1+a_{m1}q^{-1}+a_{m2}q^{-2}}y(t) = -a_{m1}y_f(t-1) - a_{m2}y_f(t-2) + y(t)$$

Control Law Equation

In [35]:
```
TR = simplify(T/R)
SR = simplify(S/R)

obj_TR = numden_coeff(TR, q)
obj_SR = numden_coeff(SR, q)

aTR = obj_TR.lst_denum_coeff
bTR = obj_TR.lst_num_coeff

aSR = obj_SR.lst_denum_coeff
bSR = obj_SR.lst_num_coeff
```

For $\frac{T}{R}$, the coefficients of the numerator and denominator are

$$\alpha\frac{T}{R} = [1,\ r_1]$$

and

$$\beta\frac{T}{R} = [t_0,\ 0]$$

while the coefficients of the numerator and denominator for $\frac{S}{R}$ are

$$\alpha\frac{S}{R} = [1,\ r_1]$$

and

$$\beta\frac{S}{R} = [s_0,\ s_1]$$

In [36]:
```
u_k, u_k_1, uc_k, y_k, y_k_1, y_k_2 = sp.symbols('u(k) u(k-1) u_{c}(k) y(k) y(k-1) y(k-2)')

uk = -u_k_1*aTR[1] + uc_k*bTR[0] - y_k*bSR[0] - y_k_1*bSR[1]
```

The control equation becomes

$$u(t) = -r_1u(k-1) - s_0y(k) - s_1y(k-1) + t_0u_c(k)$$

Part 2

In [37]:
```
# Tunable components vvvvvvvvvvvvvvvvvvvvvvvvvvvvvvvvvv
sample_depth = 100
starting_samples = 2

# starting estimate for plant parameters
est = 0.1
est_offset = 0

lam = 1 # forgeting factor lambda

# model parameters
a_m1 = -0.2707
a_m2 = 0.01832

# true plant parameters
a_1 = -0.503215
a_2 = 0.0497871
b_0 = 1.59831
b_1 = 0.587984

# true control parameters (pseudo version)
[illegible]

theta0 = np.array([b_0, r_1_p, s_0_p, s_1_p]).reshape(-1,1)

# Tunable components ^^^^^^^^^^^^^^^^^^^^^^^^^^^^^^^^^^

theta_hat = [np.array([est]*len(theta0)).reshape(-1,1)]
theta_hat[0][0] = est*est_offset

# Convert control equation derived above symbolically into numeric function
uk_subd = uk.subs([(am1, a_m1), (am2, a_m2)])
uk_func = sp.lambdify([u_k_1, uc_k, y_k, y_k_1, r1, s0, s1, t0], uk_subd)

# system input
sample_range = range(sample_depth)
t = [i for i in sample_range]
u_c = np.ones(sample_depth)
u_c[np.where([m.sin(t[i]*m.pi/20)<=0 for i in sample_range])] = 0

y = [0]*starting_samples
u = [0]*starting_samples

yf = [0]*starting_samples
uf = [0]*starting_samples

I = np.eye(len(theta0))
p = 100*I

for k in range(starting_samples ,sample_depth):
    [illegible]

# ploting of estimated parameters
[illegible]

theta_hat_ploter(df_theta, theta0[[0,3]], 'Theta_hat Estimates')

# ploting of control sig
plt.step(t,u)
plt.title('Control Input', fontsize=20)
plt.ylabel('u(t)', fontsize=18)
plt.xlabel('Time Stamps "t"', fontsize=18)
plt.grid()
plt.show()

# ploting of input vs output
plt.plot(t,u_c)
plt.plot(t,y)
plt.title('u_c(t) Vs y(t)', fontsize=20)
plt.ylabel('Magnitude', fontsize=18)
plt.xlabel('Time Stamps "t"', fontsize=18)
plt.show()
```