



# Investigations of lithium–sulfur batteries using electrochemical impedance spectroscopy

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## ABSTRACT

The electrochemical behavior of lithium–sulfur (Li–S) batteries was investigated by means of electrochemical impedance spectroscopy (EIS). Measurements were performed in equidistant charge intervals at different depths of discharge and charge during the first cycle. Additionally, the degradation of the cells was analyzed for up to 50 cycles. An equivalent electrical circuit is proposed to simulate the electrochemical processes and to quantify the impedance contributions of Li–S batteries. EIS as a function of the cycle number shows an increased capacity for fading correlated with a decrease in the charge transfer resistance of the cathode. Atomic force microscopy (AFM) was also used to provide information about changes in the electrical conductivity of the cathode surface as they are related to the building of isolating films.

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## 1. Introduction

Over the last few decades, studies of new secondary cells have increased considerably. This increase is due to a demand for high energy density rechargeable batteries for various applications such as consumer electronics and electro-mobility. The Li–S battery is a promising system due to its high theoretical capacity ( $1675 \text{ mAh g}_{\text{sulfur}}^{-1}$ ), energy density ( $2500 \text{ Wh kg}^{-1}$ ), low cost and the non-toxicity of sulfur. Nevertheless, some of the drawbacks of Li–S batteries include their poor rechargeability and high self-discharge rates. Due to the low electrical conductivity of sulfur, electrically conductive material must be added to encourage an electrochemical reaction. Furthermore, polysulfides of high orders ( $\text{Li}_2\text{S}_n$  with  $2 \leq n \leq 8$ ) dissolve in the electrolyte and can diffuse to the anode and react directly with lithium metal. This so-called shuttle mechanism causes the irreversible loss of sulfur [1–3]. Insulating and insoluble polysulfide discharge product ( $\text{Li}_2\text{S}$ ) can also precipitate on the surface of electrodes, preventing further electrochemical reactions.

EIS is a powerful technique used to investigate the physical and electrochemical processes occurring in batteries during charge and discharge. This method is used in the characterization of Li–S batteries to study, amongst other topics, the influence of electrode protective layers [4–6], cathode materials [7–13] and electrolyte compositions [14–18] in the impedance of the cell. Few studies have applied EIS at different depths of charge or discharge [19–22]. In these studies, such measurements were performed using potentiostatic mode with an amplitude signal of 5 mV at different frequency ranges (100 kHz–100 mHz [19], 1 MHz–10 mHz [20], 65 kHz–1 Hz [21], 200 kHz–1 mHz [22]).

The processes described by the proposed equivalent circuits (ECs) in [19] are electrolyte resistance ( $R_e$ ), the formation of the conductive agent/electrolyte interface ( $R_{ct}/CPE_1$ ),  $\text{Li}_2\text{S}$  film formation ( $R_g/CPE_2$ ) and polysulfide diffusion (Warburg element,  $W_0$ ). The element  $R/CPE$  is defined as a resistance ( $R$ ) connected in parallel to a constant phase element (CPE). Similar ECs were applied for the fitting of the impedance spectra in [21]. The processes analyzed here were electrolyte resistance ( $R_{el}$ ), surface layer formation on lithium and sulfur electrodes ( $R_l/CPE_1$ ), the electrochemical reaction of sulfur ( $R_r/CPE_r$ ) and polysulfide diffusion ( $W$ ).

In a recent study [22], spectra obtained at high frequencies were not analyzed, and therefore, no electrolyte resistance was considered. The boundary electrode/electrolyte was also described by a  $R_{ct}/CPE_{dl}$  element, new phase formation was represented by a  $R_{ct}/CPE_f$  element, and the liquid-state diffusion of soluble polysulfides was defined by a  $CPE_1$  rather than a Warburg element.

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The models used in these studies can fit impedance spectra at high or low frequency regions. In this paper, changes in the impedance of Li–S batteries were studied by means of EIS at different depths of discharge/charge over a wide frequency range. We proposed a simple but consistent EC to quantify the impedance contributions related to each physical or electrochemical process occurring in the battery. Moreover, the impedance spectra of Li–S batteries were evaluated in discharge and charge states for up to 50 cycles. AFM measurements on the cathode provided additional information about the electrical conductivity of the cathode surface, confirming the formation of a non-conductive layer after cycling.

## 2. Experimental procedures

### 2.1. Cell preparation

The cathodes used consisted of 50 wt.% sulfur (99.5%, Alfa Aesar), 40 wt.% Super P conductive carbon black (99%, Alfa Aesar) and 10 wt.% polyvinylidene fluoride (PVDF, Alfa Aesar). The cathodes were prepared according to methods previously published [23].

The battery was built in what is known as a Swagelok cell (Fig. 1) and assembled in a glove box under an argon atmosphere. First, a cathode was placed on an aluminum disk over the spring (cathode collector). The separator, a 25  $\mu\text{m}$  thick polypropylene microporous membrane (Celgard 2500), was placed on top of the anode and soaked with 14  $\mu\text{L}$  electrolyte, 1 M  $\text{LiPF}_6$  (99.99%, Sigma–Aldrich) in tetraethylene glycol dimethyl ether (99.9%, Sigma–Aldrich). Next, a 1.5 mm thick lithium anode (99.9%, Sigma–Aldrich) was placed on the separator. To complete construction of the battery, the cell was tightened until there was no gap between the nut and body hexes. To avoid a short circuit, the diameters of the lithium foil and cathode were 10 mm, while the separator diameter was 2 mm larger.

### 2.2. Electrochemical impedance spectroscopy and cycling of the battery

The cycling performance of the battery was investigated using a Zahner® IM6 electrochemical workstation with Thales battery software (Zahner®). The charge–discharge procedure was performed galvanostatically at a current density of  $300 \text{ mA g}_{\text{sulfur}}^{-1}$  in a voltage range of 2.8–1.5 V. After reaching the charge end voltage of 2.8 V, a potentiostatic period occurred for 15 min before the next cycle began.

EIS measurements were performed at the same electrochemical workstation during cycling in equidistant charge intervals of 50 mC. Each spectrum was measured in the frequency range of 1 MHz to 60 mHz and with an excitation voltage of 5 mV. The experimental data were fitted with an EC created with Thales software.

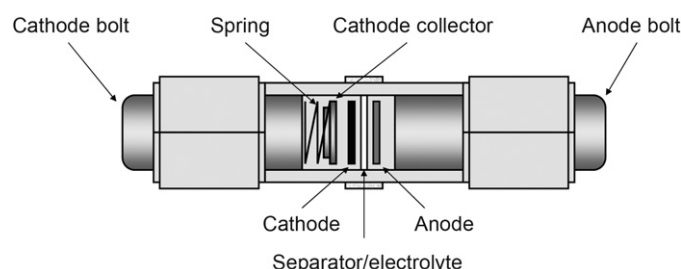


Fig. 1. Scheme of the Swagelok®-cell with an inside view of the battery components.

### 2.3. Atomic force microscopy

The electrical behavior of the cathode was investigated ex situ by means of an atomic force microscope (Multimode 8, Bruker Corp.). Each tip–sample interaction was analyzed with PeakForce–TUNA™ mode. The current was measured with a Pt-coated conductive tip working in tapping mode at a 1 kHz frequency and with a scan rate of 0.5 Hz. A voltage (100 mV) was applied between the tip and the sample holder and the averaged steady state current was measured at each tip–surface contact. The samples were analyzed in three different positions on the cathode surface and scanned over a  $9 \mu\text{m}^2$  area. More detailed information about the experimental work performed with AFM can be found in [24].

## 3. Results and discussion

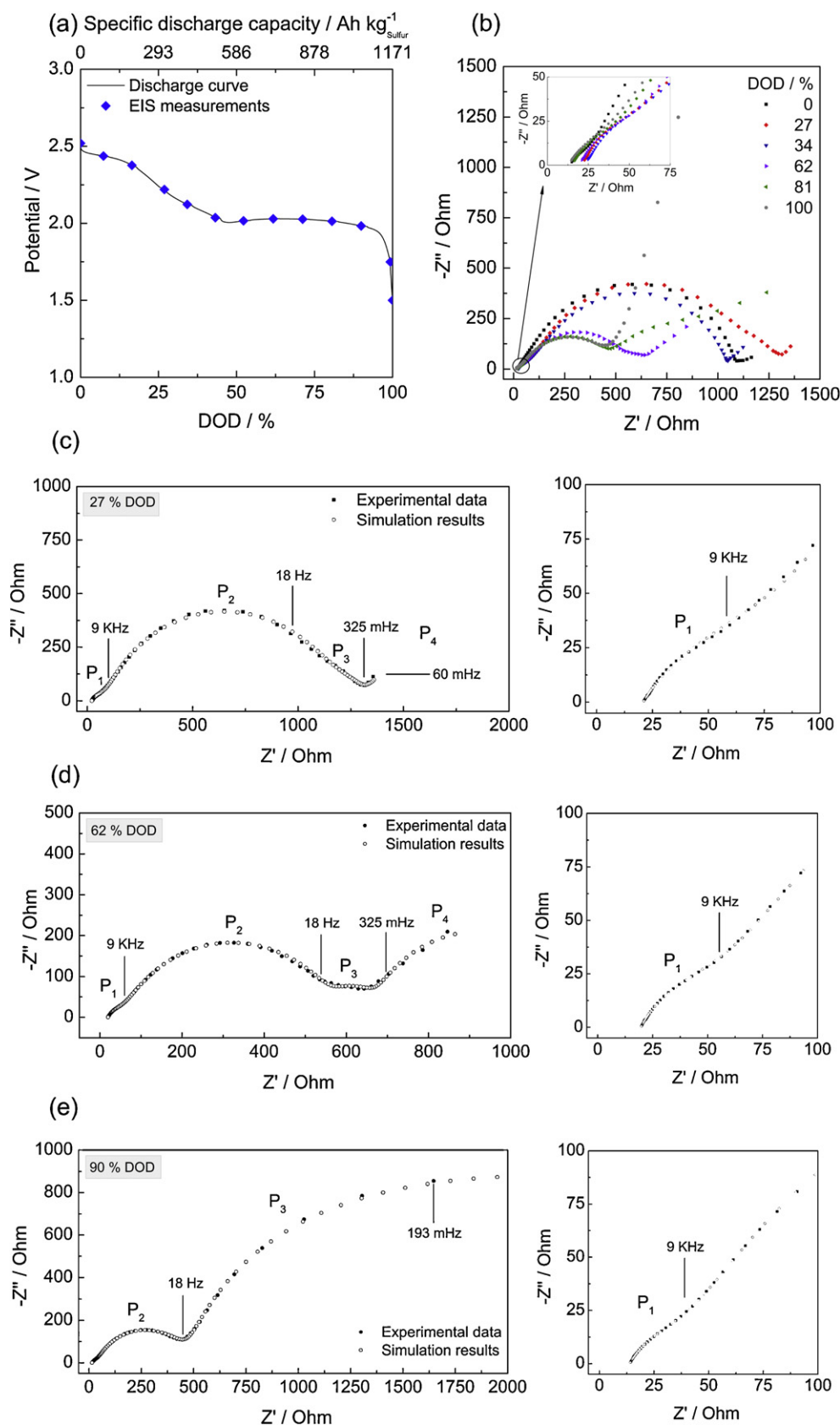
### 3.1. EIS measurements during cycling

The electrochemical reaction steps occurring during discharging are described by the reactions (1)–(9). At the anode surface, lithium oxidizes to  $\text{Li}^+$  in accordance with reaction (1). In the cathode, sulfur first dissolves into the electrolyte (reaction (2)) and then reduces to polysulfides  $\text{S}_x^{-2}$ , where  $x = 8-1$  (reactions (3)–(8)). Only the formation of solid  $\text{Li}_2\text{S}$  has been experimentally detected; for this reason, the precipitation reaction at the end of the discharge is only presented for this polysulfide (9). During charging, a reversible route is expected. This reaction mechanism is simplified, as the dissociation of polysulfides has not been described. The complete proposed sulfur reduction mechanism is discussed in [25]; the authors describe not only the irreversible electrochemical reaction but also the disproportionation of polysulfides in the electrolyte.

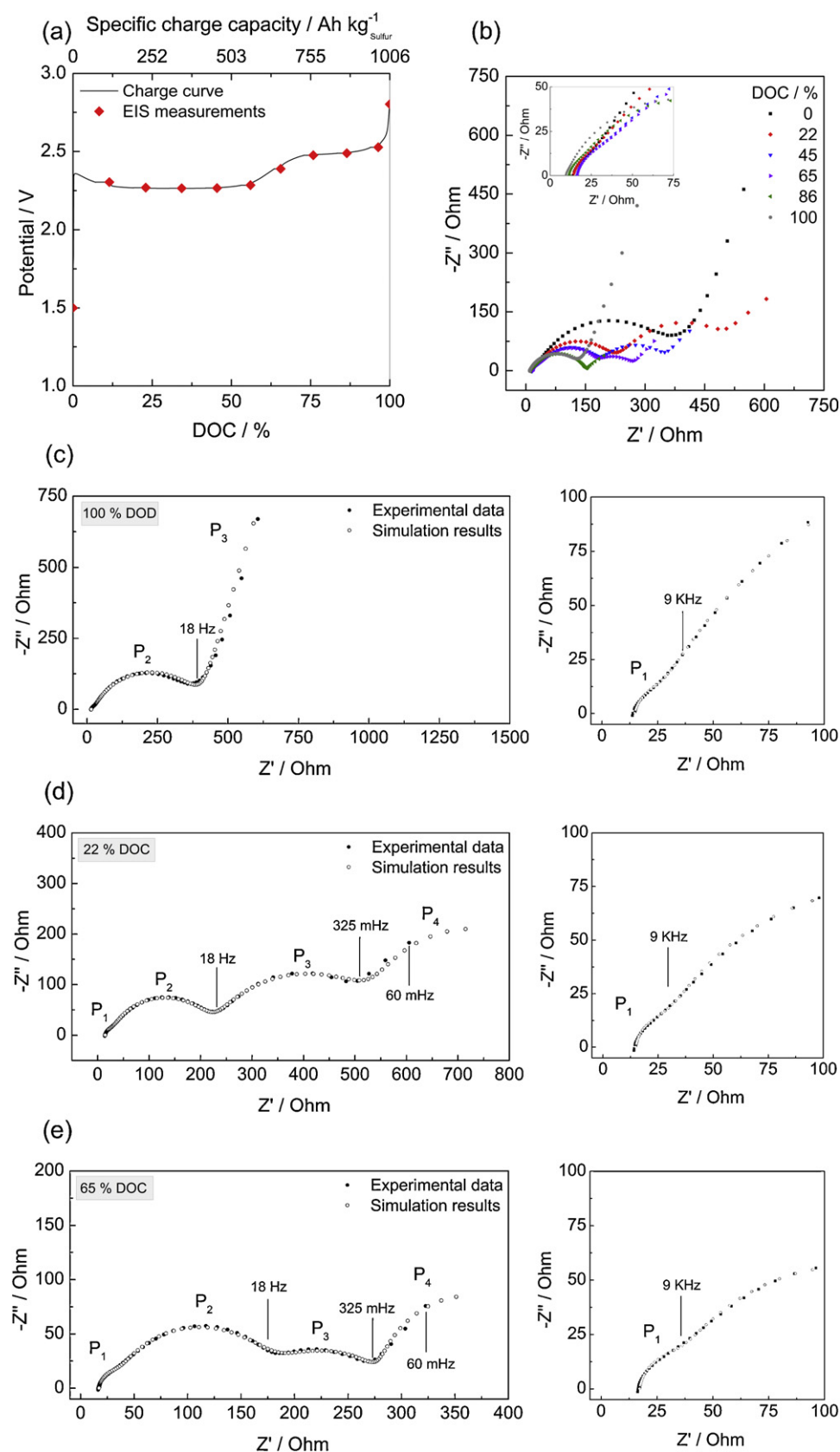


Although these reactions run in parallel during discharge, the electrochemistry of the cell may be divided into three distinct periods according to the state of aggregation of the reactants and products, as follows: (a) solid state  $\rightarrow$  dissolved in electrolyte, (b) dissolved in electrolyte  $\rightarrow$  dissolved in electrolyte and (c) dissolved in electrolyte  $\rightarrow$  solid state. During charge,  $\text{Li}_2\text{S}$  reacts reversibly to  $\text{S}_8$ . Due to the modification of the aggregate state of the reacting components, significant changes in the impedance contributions related to these processes are expected. The end products of the discharge and charge, in the case of a complete reaction, are non-conductive solid materials; this can influence the charge transfer resistance in the electrodes and enhance the formation of isolating surface layers.

Figs. 2(a) and 3(a) show the first discharge and charge curves of the Li–S battery and the points at which EIS spectra were recorded. For clarity, only certain spectra are shown (Figs. 2(b–e) and 3(b–e)). The frequency-dependent impedance of the cell represents the response of several parallel processes occurring in the battery. The impedance plots measured during cycling reveal these processes in



**Fig. 2.** (a) Discharge curve of a Li-S battery; each point represents an EIS measurement. (b) Selected Nyquist plots in the frequency range of 60 mHz–1 MHz at different depths of discharge, DOD. Experimental and fitting results of the EIS measurements at 27%, 62% and 90% DOD are shown in (c), (d) and (e), respectively. The high frequency regions of the spectra are amplified on the right.



**Fig. 3.** (a) Charge curve of a Li-S battery; each point represents an EIS measurement. (b) Selected Nyquist plots in the frequency range of 60 mHz–1 MHz at different depths of discharge, DOD. Experimental and fitting results of the EIS measurements at 100% DOD, 22% DOC and 65% DOC are shown in (c), (d) and (e), respectively. The high frequency regions of the spectra are amplified on the right.

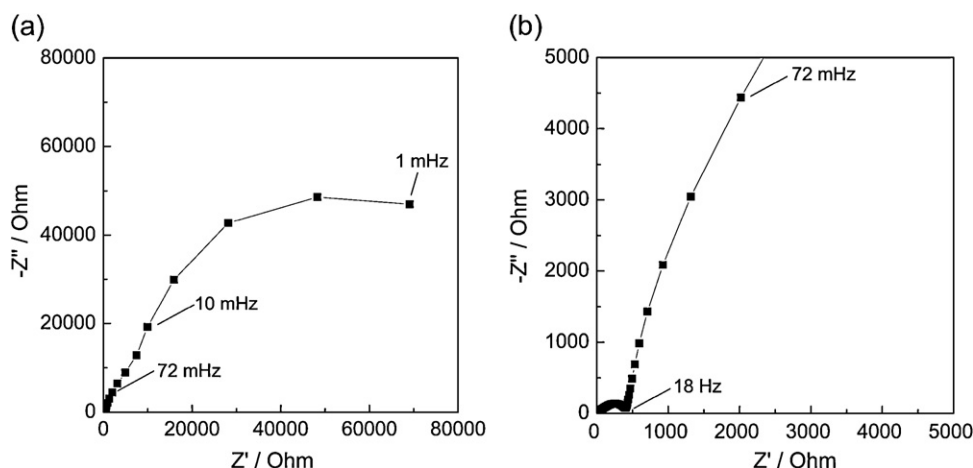


Fig. 4. Nyquist plot of a Li-S battery, frequency range: 1 mHz–1 MHz (a) with magnification in the frequency range: 72 mHz–1 MHz (b).

the form of two or three depressed semicircles. The number of semicircles that appear in the spectra is dependent on the DOD/DOC. At low frequencies, a distinct additional process is observed, which is shown by a bended slope line. To correlate this last process with a proper element of an EC, the spectrum was expanded in the lower frequency range down to 1 mHz (Fig. 4). This measurement reveals that processes at low frequencies also take the form of a semicircle. No inductance is observed in the EIS spectra at high frequencies.

At high frequencies, a semicircle with a relatively small diameter (low resistance) can be observed during discharging. We named this process  $P_1$  and found that it is present in all EIS measurements and can be seen, for example, in a magnified image in Fig. 2(c and d). In the middle frequency range, a larger depressed semicircle is observed ( $P_2$ ) during cycling. This larger semicircle is accompanied by a short bended line at low frequencies ( $P_4$ ). From a 16% depth of discharge (DOD), a new semicircle ( $P_3$ ) appears between  $P_2$  and  $P_4$ .  $P_3$  vanishes after 27% of DOD (Fig. 2(c)) and reappears at approximately 50% DOD, growing continuously, like it can be seen in Fig. 2(d and e), until the end of discharge. At higher states of discharge,  $P_3$  becomes more significant, whereas  $P_4$  (at low frequencies) is suppressed (see Fig. 2(e)).

During charging (Fig. 3), the processes  $P_1$ – $P_4$  can also be discerned.  $P_1$  is present during charging in the high frequency range and semicircle  $P_2$  decreases with increasing DOC. The semicircle corresponding to  $P_3$  diminishes continuously with an increasing depth of charge (DOC) (compare loop  $P_3$  in Fig. 3(d) and (e)). At the end of charge, a small increase is observed (see modeling results). Finally, the process  $P_4$  behaves concurrently with  $P_3$ .

The processes  $P_1$ – $P_4$  are observed at different cutoff frequencies in the MHz-, kHz-, Hz- and mHz-domains, respectively.

### 3.2. Equivalent circuit for Li-S batteries

An equivalent electrical circuit consisting of an ohmic resistance  $R_0$  in series with four  $R$ //CPE elements ( $R$  and CPE connected in parallel) was designed to model the EIS results (Fig. 5(a)). A CPE was selected instead of a capacitor because of the non-ideal behavior of the system, reflected as depressed semicircles in the Nyquist plots. In the low frequency region, neither a Warburg element nor a capacitive element could be identified (Fig. 4).

A CPE is similar to an ideal capacitive element, but has an absolute phase angle of less than  $90^\circ$ . The CPE impedance is defined as  $Z = 1/(\omega_0 V(j\omega/\omega_0))^\alpha$ , where  $\omega$  is the angular frequency,  $\omega_0$  is a

normalization factor, and  $V$  and  $\alpha$  are constants [26]. The variable  $\alpha$  is dimensionless ( $\alpha \leq 1$ ) and defines the grade of compression of the CPE semicircle. The limit value of  $\alpha = 1$  represents ideal capacitive behavior. In our measurements,  $\alpha$  varies between 0.48 and 1.

Depressed semicircles such as  $P_3$ , could be the result of the superposition of many semicircles, as several parallel reactions occur in the battery. Nevertheless, these depressed semicircles

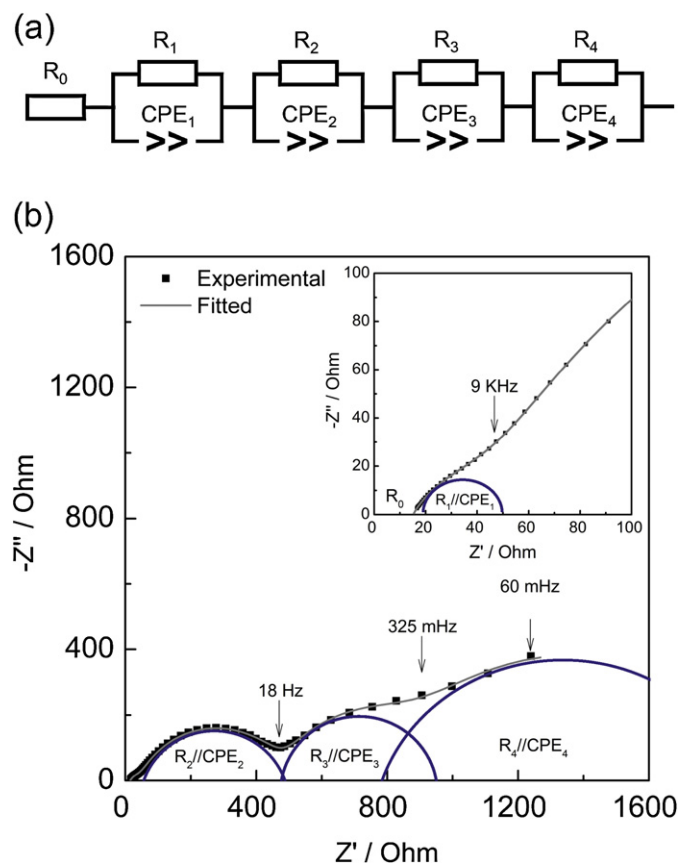
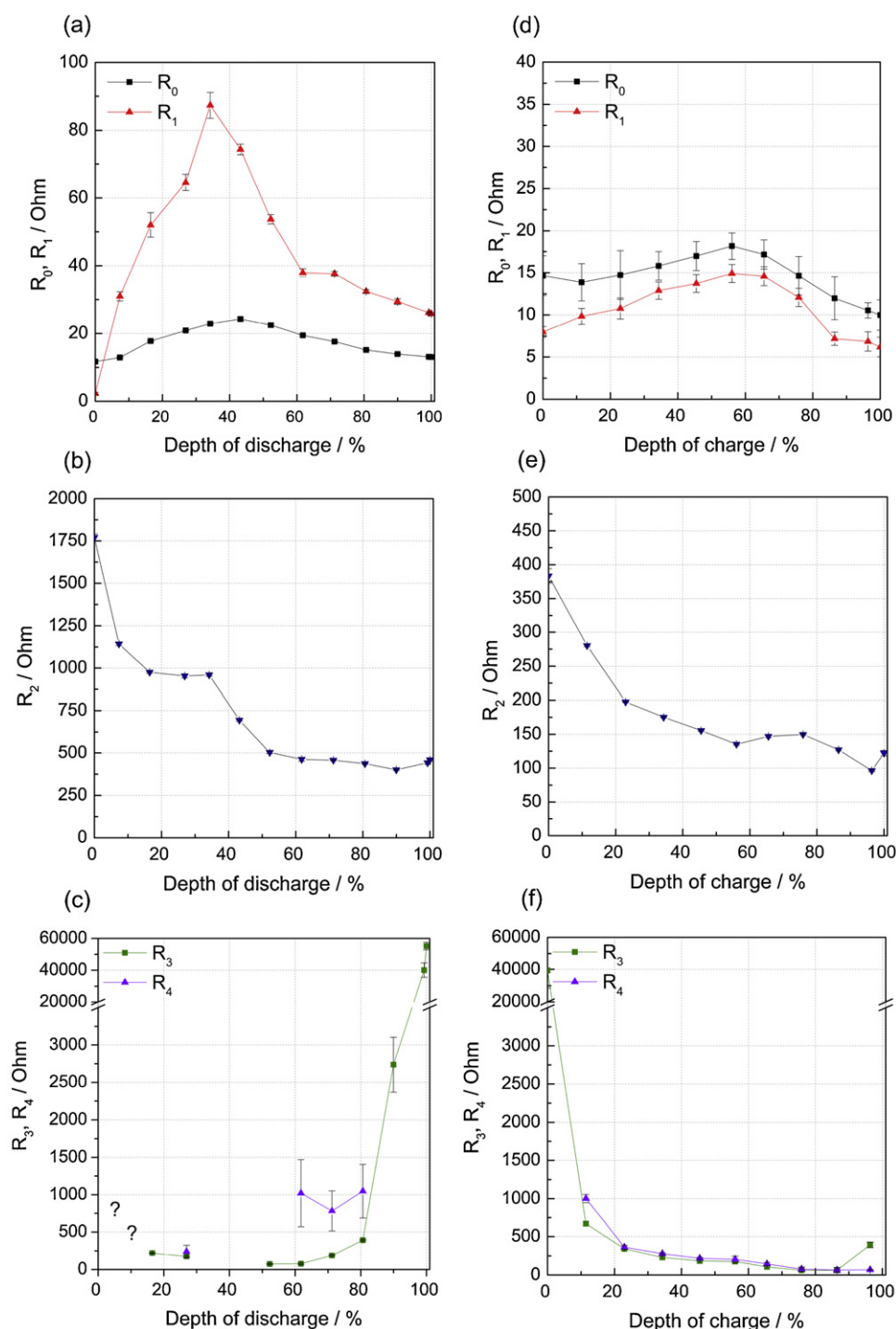


Fig. 5. (a) Equivalent electrical circuit of a Li-S battery used to fit the experimental data. (b) Nyquist plot of the impedance response of the battery at 81% DOD. The blue semicircles are schematics to clarify the domain of each EC element. The high frequency region of the spectrum is magnified at the top. (For interpretation of the references to color in this figure legend, the reader is referred to the web version of the article.)





**Fig. 6.** Charge transfer resistances calculated by modeling the impedance spectra measured during the first discharge (a–c) and charge (d–f) of the Li–S battery at DOD/DOC.

cannot be identified separately and the EC must be simplified in one depressed semicircle. Non-ideal behavior can also be explained by inhomogeneities of the electrode material, roughness and gradient concentrations.

In Fig. 5(b), an example of an EIS spectrum at 81% DOD and its fitting to the EC of Fig. 5(a) is shown. The blue semicircles in the image are only guides to the eye. As shown, the experimental points fitted well with the equivalent circuit. The different processes described previously ( $P_1$ – $P_4$ ) are now described by the corresponding  $R_i$ /CPE elements of the EC. Depending on the depth of charge or discharge,  $R_3$ /CPE<sub>3</sub> and/or  $R_4$ /CPE<sub>3</sub> may not be

present or may be indistinguishable in the frequency range of measurement.

$R_0$  represents the ohmic resistance contribution resulting from the electrolyte resistance, current collectors and cell connections. Changes observed in  $R_0$  are normally associated with variations in electrolyte properties such as chemical composition or viscosity. The electrolyte in Li–S batteries is considerably affected during cycling, because solid reaction products dissolve partially (like sulfur) and soluble polysulfides,  $\text{Li}_2\text{S}_x$  (with  $x = 3$ – $8$ ), are accumulated during charging and discharging. The dissolution of polysulfides increases the viscosity of the electrolyte and the resistance.

The first loop at high frequency,  $R_1//CPE_1$ , may be associated with the charge transfer occurring at the anode surface. This interpretation is based on analysis of the simulation results in Fig. 6. First, the clear, concurrent behavior of  $R_0$  and  $R_1$  as a function of DOD or DOC is observed. This implies that  $P_1$  is also affected by the concentration of polysulfides that can be reduced at the anode, which leads to charge transfer inhibition. Second, the resistance values of  $P_1$  are much lower than those of  $P_2$  (related to the charge transfer resistance of the cathode, see explanation below). This lower resistance of  $P_1$  is related to the lower surface area of the anode compared to the cathode.

The  $R_2//CPE_2$  element is attributable to the charge transfer of sulfur intermediates, and  $R_3//CPE_3$  is attributable to the formation and dissolution of  $S_8$  and  $Li_2S$ . The correlation of these EC-elements with specific chemical processes occurring in the battery was conceived after analysis of the simulation results. Note that  $R_2$  is highest at 0% discharge where the concentration of sulfur intermediate is minimized. On the contrary,  $R_3$  obtains its highest value at full discharge where accessible  $S_8$  is unavailable and obtains its lowest values after sulfur dissolution.  $R_3$  is visible when the formation of  $Li_2S$  starts. Both the electrochemical reactions and the resistance of each EC-element exhibit a distinct DOD/DOC dependence. This result and a comparison with other characterization techniques such as XRD and AFM [23,25], along with results from the previous literature [19–22], support our assignment of the elements in the EC.

Finally, diffusion processes are detected by means of EIS at low frequencies. In our circuit, these processes are simulated by the element  $R_4//CPE_4$ .

### 3.3. Modeling of EIS during the first cycle

The circuit elements (ohmic resistance, charge transfer resistances and associated double layer capacitance) were calculated by fitting the experimental data points with the EC. The complete results of the fitting are presented in the supplemental information. The resistance contributions as functions of DOD and DOC for the first cycle are illustrated in Fig. 6. The electrolyte resistance ( $R_0$ ) changes during discharge and is influenced by the concentration of soluble polysulfides (Fig. 6(a)). High resistances are measured from 34 to 52% DOD, indicating states with maximal concentrations of polysulfides corresponding to the end of the first plateau in the discharge curve. When the reduction of polysulfides to dilithium sulfide is complete,  $R_0$  reduces back to approximately its original values. The charge transfer resistance in the anode,  $R_1$ , shows a trajectory similar to but more pronounced than that of  $R_0$ , with a maximum at 34% DOD. The electrolyte has a high concentration of dissolved polysulfides, which can diffuse to the anode surface and hinder the charge transfer of lithium ions.

The charge transfer resistance on the cathode side, described by  $R_2$ , decreases during discharge (Fig. 6(b)). The drastic diminution of resistance  $R_2$  during the first stages of discharge may be caused by the changes in composition and morphology occurring in the cathode during this period. As a consequence of the dissolution and reaction of sulfur, the content of solid sulfur in the cathode diminishes; a more porous structure remains, with a higher surface area and greater conductivity. The charge transfer of polysulfide ions is enhanced as a result of these factors. In the interval between 16% and 34% DOD, the resistance remains constant. At this stage, process  $P_3$  can be recognized at 16% and 27% DOD (see fitting curve in Fig. 2(c)). The reason for the appearance of process  $P_3$  may be the slowing of an electrochemical step, which is seen as a new CPE element in the spectrum. The presence of this element at the first stages of discharge is related to the dissolution of the remaining sulfur in the cathode. The dissolution and progressive reaction of

sulfur was monitored by means of in situ XRD in [24]. At 0% DOD, a small loop associated with  $P_3$  can be observed between  $P_2$  and  $P_4$ . Nevertheless, the small quantity of measured points result in an imprecise quantification, and we decided to model the spectrum of the completely charged battery (0% DOD) with three  $R//CPE$ s. After sulfur dissolves and reacts,  $P_3$  cannot be observed until 52% DOD is reached. The reappearance of this process at this discharge state is now attributable to the formation of  $Li_2S$ . The resistance of this element increases continuously until the end of discharge, due to the gradual formation of this solid and low electrically conductive end product of the Li–S discharge reaction (Fig. 6(c)). Moreover,  $R_2$  stabilizes at the final stages of discharge with the progressive reduction of polysulfides.

$R_4$ , which is attributed to diffusion, could not always be determined as a result of an insufficient number of measured points at low frequencies. However, it could be observed that  $R_4$  follows the tendency of  $P_3$  (Fig. 6(c)). The dissolution or formation of solid isolating materials can influence the diffusion of species, negatively in the case of solid products formation. Diffusion is suppressed by the dominant process  $P_3$  at values higher than 81% DOD, and it is displaced out of the measured frequency range. This can be clearly observed in Fig. 2(e), at 90% DOD, where the large  $P_3$  semi-circle is present in the low frequency range.

During the charge step (Fig. 6(d–f)), an overall decrease in the absolute values of the resistance elements is observed in comparison with the discharge step. The maximum values of  $R_0$  and  $R_1$  occur at approximately 60% DOC. In contrast to the discharge process, the maximum concentration of polysulfides in the electrolyte occurs in the second half of the charging process, at the end of the first plateau. At this point, dilithium sulfide has been completely reacted to high order polysulfides.

The resistance related to the charge transfer in the cathode,  $R_2$ , decreases and stabilizes after approximately 40% DOC. The most important changes in the cathode morphology may occur during the first discharge, when the sulfur particles dissolve and leave the cathode. Afterwards, the formation of solid products may occur primarily at the surface of the cathode. For this reason, the charge transfer of the cathode during the first charge does not induce such pronounced changes as it does during the first discharge.

The reaction of  $Li_2S$  in the first stages of charging enhances the diminution of  $R_3$  considerably. The most drastic changes in  $R_3$  occur

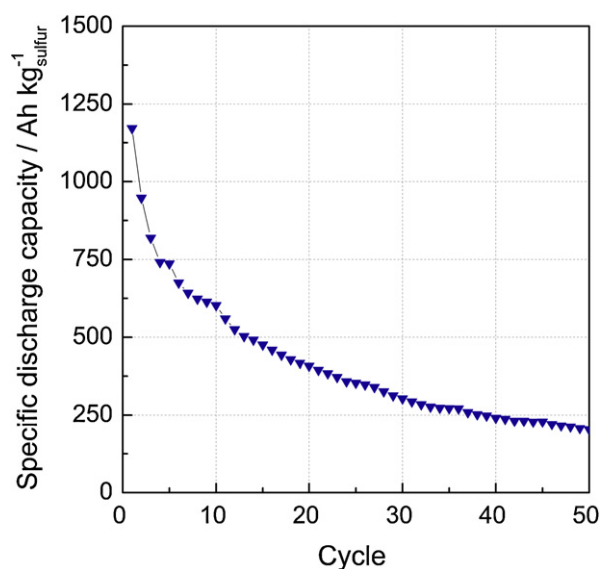
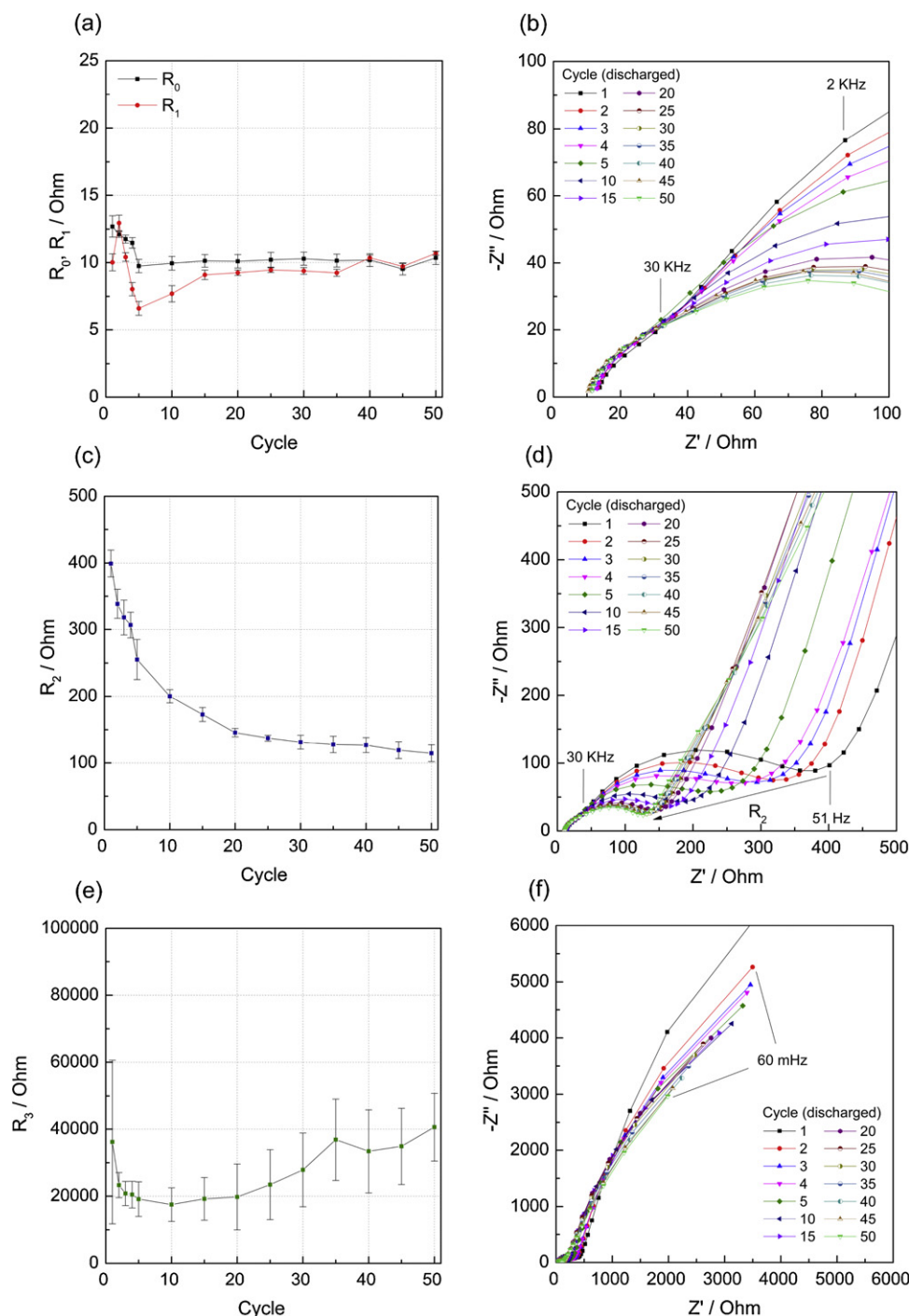


Fig. 7. Cycle performance of a Li–S battery at room temperature for up to 50 cycles.



**Fig. 8.** Charge transfer resistances calculated by modeling the impedance spectra measured in a discharge state for up to 50 cycles (a, c, and e). Selected impedance spectra are shown for each frequency domain (b, d, and f).

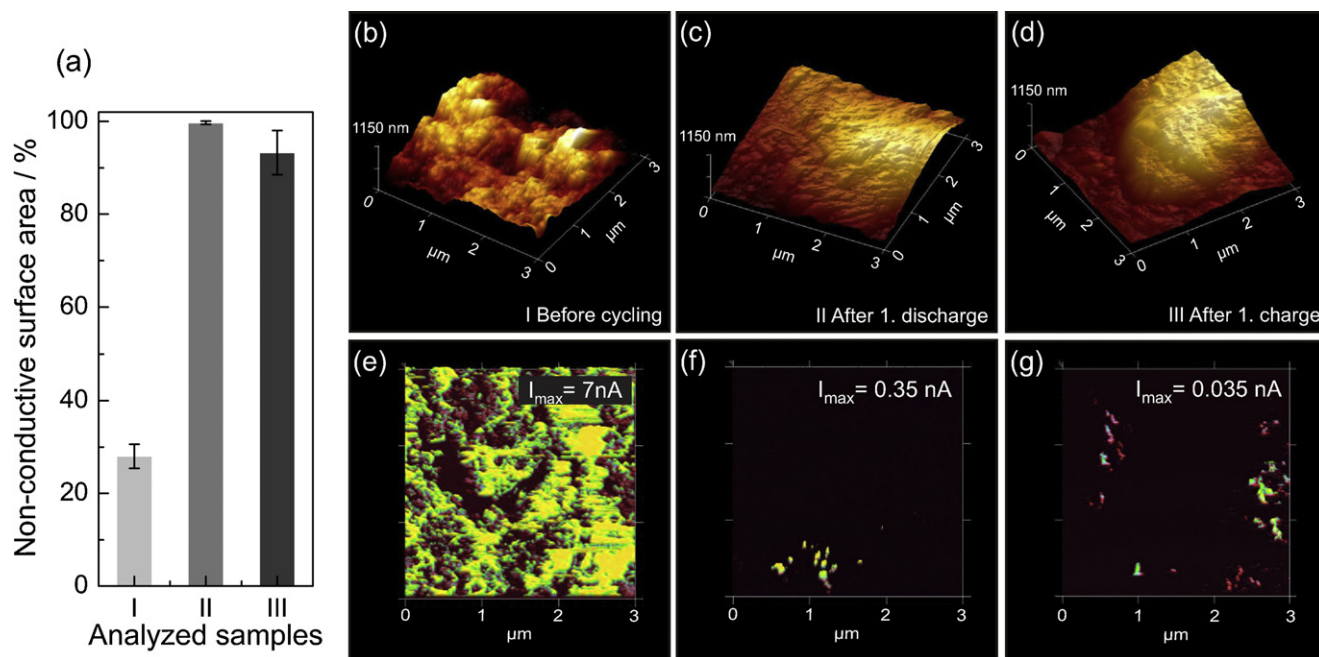
in the period between 100% DOD and 22% DOC (Fig. 6 (f)). This can be observed in Fig. 3(c and d). At the end of the charging cycle, an increase in  $R_3$  is observed due the formation of solid  $S_8$ . The resistance related to diffusion ( $R_4$ ) can be clearly linked to the dissolution of  $Li_2S$  and the formation of sulfur, with both following the same trajectory.

### 3.4. Degradation during cycling

The degradation of the battery over 50 cycles was investigated by means of EIS. The cycle performance of the battery is shown

in Fig. 7. The specific discharge capacity of the cell is high at the beginning of the cycling (approximately  $1200 \text{ mAh g}^{-1}$ ), but the battery degrades with an increasing number of cycles. Some degradation of the cell is due to the aging of the battery during testing. Although the cathode used does not present the highest constant capacity, it is still important to characterize the degradation and fading of the capacity of this cell to understand potential modifications and improvements. This simple but industrially viable cathode can be improved, for example, by the use of protective layers and electrolyte additives, as was experimentally proven in [27–32].





**Fig. 9.** (a) Non-conductive surface area (%) for the analyzed samples where I: cathode before cycling, II: cathode surface after the first discharge and III: cathode surface after the first charge. (b–d) AFM topography images of the samples. (e and f) AFM current images.

The results of fitting the battery in a discharge state with the impedance spectra are summarized in Fig. 8. In the high frequency region, the low ohmic resistance  $R_0$  and charge transfer resistance  $R_1$  do not change appreciably with an increased number of cycles (Fig. 8(a and b)).

The resistance associated with the charge transfer of the cathode ( $R_2$ ), measured in the discharge state, decreases drastically in the first few cycles, decreasing 50% between the 1st and 10th cycles (Fig. 8(c)). The rate of loss of resistance is similar to the rate of the fading of capacity (49%). The battery loses 83% of its specific discharge capacity in 50 cycles, while the major decrease (49%) occurs in the first 10 cycles. From the 10th to the 20th cycle, a more gradual diminution is observed. The loss of discharge capacity behaves concurrently with the diminution of charge transfer resistance in the cathode. The high reduction of  $R_2$  is most likely associated with the better accessibility of active material by electronic conduction; related to the less formation of non-conductive  $\text{Li}_2\text{S}$ . The charge transfer resistance in the cathode reduces; however, the degradation of the cell increases, resulting in lower discharge capacities.

The resistance  $R_3$  cannot be precisely fitted in the same manner as the other circuit elements (Fig. 8(e)). Evaluation of this element shows larger errors due to the fewer available measurement points at low frequencies. The formation of  $\text{Li}_2\text{S}$ , which is linked to this element, decreases during cycling. This decrease is reflected by the reduction of the resistance at the beginning of the cycle. Nevertheless, the resistance increases gradually after 10 cycles. This may be a result of a gradual degradation of the cathode due to the growth of an isolated film at the boundary between cathode and separator, composed of solid reaction products. On the contrary, the bulk of the cathode may consist, at the end of the 50th cycle, essentially of carbon black and some isolated sulfur particles. The concentration of non-conductive reaction products may increase in the direction of the surface of the cathode. This can be explained by the reduction of charge transfer resistance related to the reaction of soluble polysulfides,  $R_2$ , and the high resistance  $R_3$  due to the formation of a non-conductive layer on the surface.

### 3.5. AFM measurements

The electrical conductivity of the cathode was evaluated by means of conductive AFM. The measured current, directly proportional to the electrical conductivity of the path between the sample surface and the sample holder, is influenced by the composition of the sample (percentage of non-conductive material), the homogeneity of the sample, the distribution of non-conductive particles in the bulk material and the formation of non-conductive surface layers. If an isolating surface layer is present, no current can be measured and the non-conductive area can be quantified.

Each sample was analyzed in three different positions over a scan area of  $3 \mu\text{m} \times 3 \mu\text{m}$ . The results of the non-conductive surface area quantification, the AFM images of the topography of the cathode and the current distribution are shown in Fig. 9. Before cycling, the cathode has a homogeneous surface covered mainly with carbon black (28% of the non-conductive surface area). After the first discharge, the sample is covered with an isolating film, which reduces the conductive area to less than 1% of the total area. The film is accumulated during the last period of discharge and consists mainly of non-conductive  $\text{Li}_2\text{S}$ . This explains the radical increase of  $R_3$  at the end of the cycle. In air,  $\text{Li}_2\text{S}$  reacts to  $\text{LiOH}$ , which is also a non-conductive material but is stable under ex situ conditions. After charging, the cathode has a high percentage of non-conductive area (93%) with inhomogeneities in the surface. Similar tendencies toward conductivity changes on cathode surfaces were also reported from in situ AFM measurements in previous studies [33].

The AFM results confirm the formation of an isolating layer in the cathode, which increases the surface resistance on the cathode, as observed through the analysis of the impedance at low frequencies ( $R_3$ ).

## 4. Conclusions

In this work, a Li–S battery was investigated by means of EIS. An equivalent circuit is proposed for the evaluation of Li–S

batteries, which can be applied in a broad frequency domain. The elements of this circuit have been related to physical and chemical processes occurring in the anode, cathode and electrolyte. The impedance contributions associated with these processes are strongly dependent on the depths of discharge and charge of the cell. During the first cycle, the dissolution and formation of solid reaction products can be detected and evaluated through the appearance of an additional semicircle in the middle frequency region of the Nyquist impedance plot. The highest electrolyte resistance, related to the highest concentration of polysulfides, is detected at 43% DOD and 56% DOC, at the end of the first discharge and charge plateau, respectively. The study of the degradation of the cathode by means of EIS for up to 50 cycles shows that the impedance contributions related to the electrolyte and the anode side present only small changes, while the charge transfer resistance in the cathode is reduced by 71%. This diminution may be related to the rate capacity loss of the battery as a result of the lessened formation of non-conductive solid products in the cathode bulk. AFM measurements confirm the formation of a solid isolating layer after cycling, in discharge and charge states.

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## Appendix A. Supplementary data

Supplementary data associated with this article can be found, in the online version, at <http://dx.doi.org/10.1016/j.electacta.2013.02.101>.

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