

第十三章 热力学基础 090410102 方尧

13-1 (B) 13-2 (B) 13-3 (C) 13-4 (B) 13-5 (B) 13-6 (A) 13-7 (D)

$$13-11 \quad W = p \cdot \Delta V = 1 \times 10^5 \times (1.5 \times 10^{-2} - 1 \times 10^{-2}) \text{ J} = 5 \times 10^2 \text{ J}$$

$$\Delta E = Q - W = 1.2 \times 10^3 \text{ J}$$

$$13-12 \quad \nu = \frac{m}{M} = \frac{50}{9} \text{ mol}$$

$$1) Q_V = \nu C_{V,m} \cdot \Delta T = 3091.1 \text{ J} \quad 2) Q_P = \nu C_{P,m} \Delta T = 4023.3 \text{ J}$$

$$13-14 \quad C_{V,m} = \frac{5}{2} R = 20.775 \text{ J} \cdot \text{mol}^{-1} \cdot \text{K}^{-1} \quad C_{P,m} = C_{V,m} + R = 29.085 \text{ J} \cdot \text{mol}^{-1} \cdot \text{K}^{-1}$$

$$1) \nu = \frac{pV}{RT} = 4.41 \times 10^{-2} \text{ mol}$$

$$2) Q_P = \nu C_{P,m} \Delta T = 128.21 \text{ J} \quad Q_V = \nu C_{V,m} \Delta T = 91.58 \text{ J}$$

$$3) \text{ 知等体 } \Delta E = Q_V + W_V, \Delta E = Q_V \text{ 故 } W_V = 0.$$

$$\text{等压 } \Delta E = Q_P - W_P = Q_V \text{ 故 } W_P = 36.62 \text{ J}$$

$$13-15 \text{ 有 } \Delta E_{ABC} = Q_1 - W_1 \text{ 得 } \Delta E_{ABC} = 200 \text{ J}$$

$$C \rightarrow A \text{ 过程 } \Delta E_{CA} = Q_2 - W_2 = -\Delta E_{ABC} \text{ 得 } Q_2 = -252 \text{ J 即放出热量 } 252 \text{ J}$$

$$13-19 \quad 1) \text{ 等温过程 } Q_T = \nu RT_A \ln \frac{V_2}{V_1} \quad \text{其中 } p_A V_A = \nu RT_A \text{ 得 } Q_T = 2.773 \times 10^3 \text{ J},$$

$$\text{有 } \Delta E = Q_T - W_T = 0 \text{ 得 } W_T = 2.773 \times 10^3 \text{ J, 吸收 } 2.773 \times 10^3 \text{ J, 做功 } 2.773 \times 10^3 \text{ J}$$

$$2) \text{ 等体过程 + 等压过程 } ACB,$$

$$W_2 = p_C (V_B - V_C) = 2 \times 10^3 \text{ J}$$

$$\Delta E = Q' - W_2 = 0 \text{ 故 } Q' = 2 \times 10^3 \text{ J, 吸收 } 2 \times 10^3 \text{ J, 做功 } 2 \times 10^3 \text{ J}$$

$$13-20 \text{ 有 } p_1 V_1^\gamma = p_2 V_2^\gamma \text{ 得 } p_2 = 9.77 \times 10^5 \text{ Pa}$$

$$W = \frac{p_1 V_1 - p_2 V_2}{\gamma - 1} = -23.024 \text{ J}$$

$$13-22 \text{ 由 } pV = \nu RT \text{ 得 } p = 9.972 \times 10^4 \text{ Pa} \quad C_{V,m} = \frac{5}{2} R = 20.775 \text{ J} \cdot \text{mol}^{-1} \cdot \text{K}^{-1}, C_{P,m} = 29.085 \text{ J} \cdot \text{mol}^{-1} \cdot \text{K}^{-1}$$

$$1) \text{ 等压, } W = p \cdot \Delta V = p \cdot V = 2.49 \times 10^3 \text{ J} \quad Q_P = \nu C_{P,m} \cdot \Delta T = \nu C_{P,m} \cdot T = 8.73 \times 10^3 \text{ J}$$

$$2) \text{ 等温 } W = \nu RT \ln \frac{V_2}{V_1} = 1.73 \times 10^3 \text{ J} \quad \Delta E = Q_T - W = 0 \text{ 得 } Q_T = 1.73 \times 10^3 \text{ J}$$

$$3) \text{ 绝热 } pV^\gamma = p'V'^\gamma \text{ 其中 } V' = 2V \quad \gamma = \frac{7}{5} \text{ 得 } p' = 3.778 \times 10^4 \text{ Pa}$$

$$W = \frac{p_1 V_1 - p_2 V_2}{\gamma - 1} = 1510 \text{ J}$$

$$13-24 \quad \nu = \frac{m}{M} = 10 \text{ mol}$$

$$\text{对外做功 } W = W_{AB} + W_{CD} = \nu RT_1 \ln \frac{V_2}{V_1} + \nu RT_2 \ln \frac{V_1}{V_2} = \nu R(T_1 - T_2) \ln \frac{V_2}{V_1} = 5.76 \times 10^3 \text{ J}$$

吸收的热量仅在 AB, DA 段吸热.

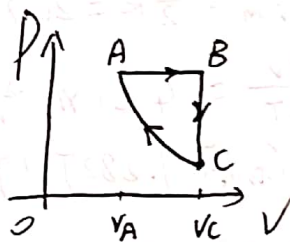
$$\text{AB 段 等温 } \Delta E = Q_{AB} - W_{AB} = 0 \quad \text{得 } Q_{AB} = W_{AB} = 1.728 \times 10^4 \text{ J}$$

$$\text{DA 段 等体则 } \Delta E = Q_{DA} - W_{DA} = Q_{DA} \quad Q_{DA} = \Delta E = \nu \cdot \frac{5}{2} R(T_1 - T_2) = 2.077 \times 10^4 \text{ J}$$

$$\text{则 } Q_{\Sigma} = Q_{AB} + Q_{DA} = 3.81 \times 10^4 \text{ J}$$

$$\eta = \frac{W}{Q_{\Sigma}} = 15.12\%$$

13-26 (1) 对应 P-V 图如右
正循环, 当热机循环.



$$12) \text{ 做功 } W = P_A(V_C - V_A) + \nu RT \ln \frac{V_A}{V_C}$$

$$= P_A V_A (1 - \ln 2)$$

$$Q_{AB} = C_{p,m} \cdot \nu \cdot (T_B - T_A) = \frac{5}{2} R \nu (T_B - T_A)$$

$$\eta = \frac{W}{Q_{AB}} = \frac{1 - \ln 2}{\frac{5}{2}} = 12.3\%$$

13-28 (1) 知仅在 AB 吸热, CD 放热

$$\text{则有 } Q_{CD} = \nu C_{p,m} (T_C - T_D) \quad Q_{AB} = \nu C_{p,m} (T_B - T_A)$$

$$\text{有 } P_A^{1-\gamma} T_A^{\gamma} = P_D^{1-\gamma} T_D^{\gamma} \quad \text{得 } T_D = \sqrt[\gamma]{\frac{P_A}{P_D}} \cdot T_A$$

$$\text{同理 } T_C = \sqrt[\gamma]{\frac{P_B}{P_C}} \cdot T_B$$

$$\eta = 1 - \frac{Q_{CD}}{Q_{AB}} = 1 - \frac{T_C - T_D}{T_B - T_A} = 1 - \frac{T_C}{T_B} \left(1 - \frac{T_D}{T_C} \right) / \left(1 - \frac{T_A}{T_B} \right) = 1 - \frac{T_C}{T_B}$$

(2) 卡诺循环为等温等绝热过程组成, 此循环非卡诺循环.

13-30.

证明: B-C 放热 有 $Q_{BC} = \nu C_{p,m} (T_B - T_C)$

(-A 吸热) $Q_{AB} = \nu C_{p,m} (T_A - T_C)$

$$\eta = 1 - \frac{Q_{BC}}{Q_{AB}} = 1 - \gamma \frac{T_B - T_C}{T_A - T_C} = 1 - \gamma \frac{\frac{T_B}{T_C} - 1}{\frac{T_A}{T_C} - 1} = 1 - \gamma \frac{\frac{V_1}{V_2} - 1}{P_1/P_2 - 1} \quad \text{得证}$$

$$13-31 \text{ 热机循环效率 } \eta = \frac{W}{Q_1} = \frac{Q_1 - Q_2}{Q_1} = 1 - \frac{Q_2}{Q_1}$$

$$(1) \eta_1 = 1 - \frac{T_2}{T_1} = 1 - \frac{27+273}{227+273} = 40\% \quad W_1 = 2000 \text{ J} \quad \text{得 } Q_1 = 5 \text{ kJ}, Q_2 = 3 \text{ kJ}$$

知在低温热源温度不变, Q_2 不变即 $Q_2' = Q_2 = 3 \text{ kJ}$

$$W' = Q_1' - Q_2' \quad \text{得 } Q_1' = 6 \text{ kJ} \quad \text{得 } \eta_2 = 1 - \frac{Q_2}{Q_1'} = 50\%$$

$$(2) \eta_2 = 1 - \frac{T_2'}{T_1'} = 0.5 \quad \text{故 } T_2' = 600 \text{ K}$$

13-3) ab等温吸热 bc等容降压, 放热 ca无热交换.

$$Q_{ab} = \nu R T_A \ln \frac{V_B}{V_A} \quad Q_{bc} = \nu C_{V,m} (T_B - T_C)$$

其中 $T_A \cdot V_A^{\gamma-1} = T_C \cdot V_C^{\gamma-1}$

$$1) \eta = 1 - \frac{Q_{bc}}{Q_{ab}} = 1 - \frac{V \cdot \sum R (T_B - T_C)}{\nu R T_A \ln 3} = 1 - \frac{5}{2 \ln 3} \left(1 - \frac{1}{3}\right)^{0.67} = 19.08\%$$

$$2) \Delta S = \int_b^c \frac{dQ}{T} = \int_b^c \frac{\nu C_{V,m}}{T} dT = \nu C_{V,m} \ln \frac{T_C}{T_B} = -0.913 \text{ J} \cdot \text{K}^{-1}$$

13-38 根据 $S = k \ln W$

$$\Delta S = k \ln \frac{W_2}{W_1} = k \ln \left(\frac{V_2}{V_1} \right)^N = k N \ln \frac{V_2}{V_1} = \nu R \ln \frac{V_2}{V_1} = 11.52 \text{ J} \cdot \text{K}^{-1}$$