

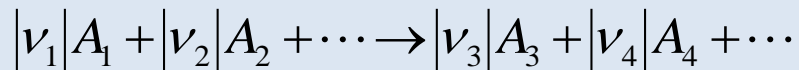
EG3029 Chemical Thermodynamics

Chemical Reaction Equilibrium

Reaction Coordinate

Single Reaction

- General chemical reaction:



ν_i stoichiometric coefficient
 A_i chemical species

- Change in quantities as reaction progresses:

$$\frac{dn_1}{\nu_1} = \frac{dn_2}{\nu_2} = \frac{dn_3}{\nu_3} = \frac{dn_4}{\nu_4} = \dots$$

- Reaction coordinate ε

$$\frac{dn_i}{\nu_i} = d\varepsilon$$

$$dn_i = \nu_i d\varepsilon$$

- Mole fractions of species

$$y_i = \frac{n_i}{n} = \frac{n_{i,0} + \nu_i \varepsilon}{n_0 + \nu \varepsilon}$$

Reaction Coordinate Multireaction

- Multireaction progress:

$$dn_i = \sum_j \nu_{i,j} d\varepsilon_j$$

- Mole fractions of species:

$$y_i = \frac{n_{i,0} + \sum_j \nu_{i,j} \varepsilon_j}{n_0 + \sum_j \nu_j \varepsilon_j}$$

j reaction index

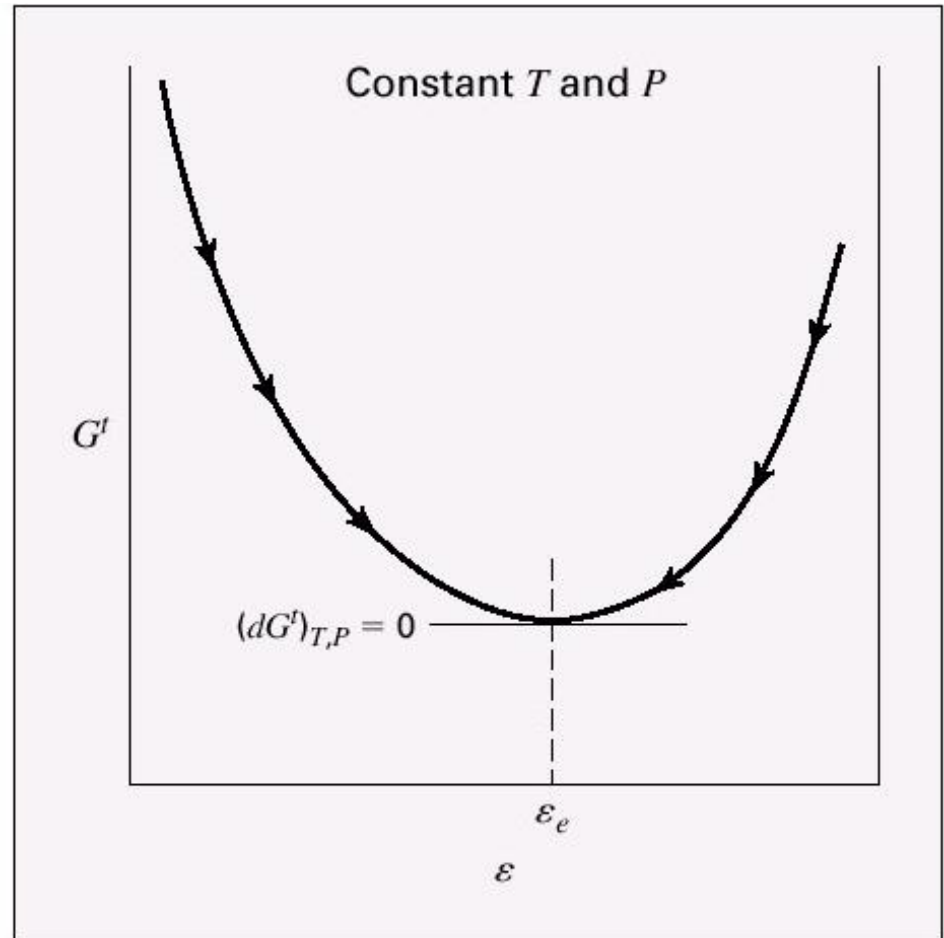
Reaktion				A[cm,mol,s]	b	E/kJ·mol ⁻¹	
----- 01. - 04. H ₂ -CO Oxidation							
----- 01. H ₂ -O ₂ -Reaktionen (HO ₂ , H ₂ O ₂ ausgeschlossen)							
O ₂	+H	=OH	+O	2.00·10 ¹⁴	0.0	70.3	
H ₂	+O	=OH	+H	5.06·10 ⁰⁴	2.67	26.3	
H ₂	+OH	=H ₂ O	+H	1.00·10 ⁰⁸	1.6	13.8	
OH	+OH	=H ₂ O	+O	1.50·10 ⁰⁹	1.14	0.42	
H	+H	+M*	=H ₂	+M*	1.80·10 ¹⁸	-1.0	0.00
O	+O	+M*	=O ₂	+M*	2.90·10 ¹⁷	-1.0	0.00
H	+OH	+M*	=H ₂ O	+M*	2.20·10 ²²	-2.0	0.00
----- 02. HO ₂ -Bildung/Verbrauch							
H	+O ₂	+M*	=HO ₂	+M*	2.30·10 ¹⁸	-0.8	0.00
HO ₂	+H		=OH	+OH	1.50·10 ¹⁴	0.0	4.20
HO ₂	+H		=H ₂	+O ₂	2.50·10 ¹³	0.0	2.90
HO ₂	+H		=H ₂ O	+O	3.00·10 ¹³	0.0	7.20
HO ₂	+O		=OH	+O ₂	1.80·10 ¹³	0.0	-1.70
HO ₂	+OH		=H ₂ O	+O ₂	6.00·10 ¹³	0.0	0.00
----- 03. H ₂ O ₂ -Bildung/Verbrauch							
HO ₂	+HO ₂		=H ₂ O ₂	+O ₂	2.50·10 ¹¹	0.0	-5.20
OH	+OH	+M*	=H ₂ O ₂	+M*	3.25·10 ²²	-2.0	0.00
H ₂ O ₂	+H		=H ₂	+HO ₂	1.70·10 ¹²	0.0	15.7
H ₂ O ₂	+H		=H ₂ O	+OH	1.00·10 ¹³	0.0	15.0
H ₂ O ₂	+O		=OH	+HO ₂	2.80·10 ¹³	0.0	26.8
H ₂ O ₂	+OH		=H ₂ O	+HO ₂	5.40·10 ¹²	0.0	4.20
----- 04. CO-Reaktionen							
CO	+OH		=CO ₂	+H	6.00·10 ⁰⁶	1.5	-3.10
CO	+HO ₂		=CO ₂	+OH	1.50·10 ¹⁴	0.0	98.7
CO	+O	+M*	=CO ₂	+M*	7.10·10 ¹³	0.0	-19.0
CO	+O ₂		=CO ₂	+O	2.50·10 ¹²	0.0	200.

Elementary reactions in methane/air combustion.
from Warnatz, Maas, Dibble, 'Combustion' (97)

Reaction Equilibrium General

- In a closed system at constant T and P , the reaction equilibrium is reached when the total Gibbs energy attains its minimum value:

$$(dG^t)_{T,P} = 0$$



Reaction Equilibrium

Equilibrium Constant

- Criterion: $\sum_i \nu_i \mu_i = 0$

- Equilibrium constant K :

$$\prod_i \left(\frac{\hat{f}_i}{f_i^\circ} \right)^{\nu_i} = K = \exp \left(\frac{-\Delta G^\circ}{RT} \right)$$

- Standard heat of reaction:

$$\Delta H^\circ = -RT^2 \frac{d \left(\Delta G^\circ / RT \right)}{dT}$$

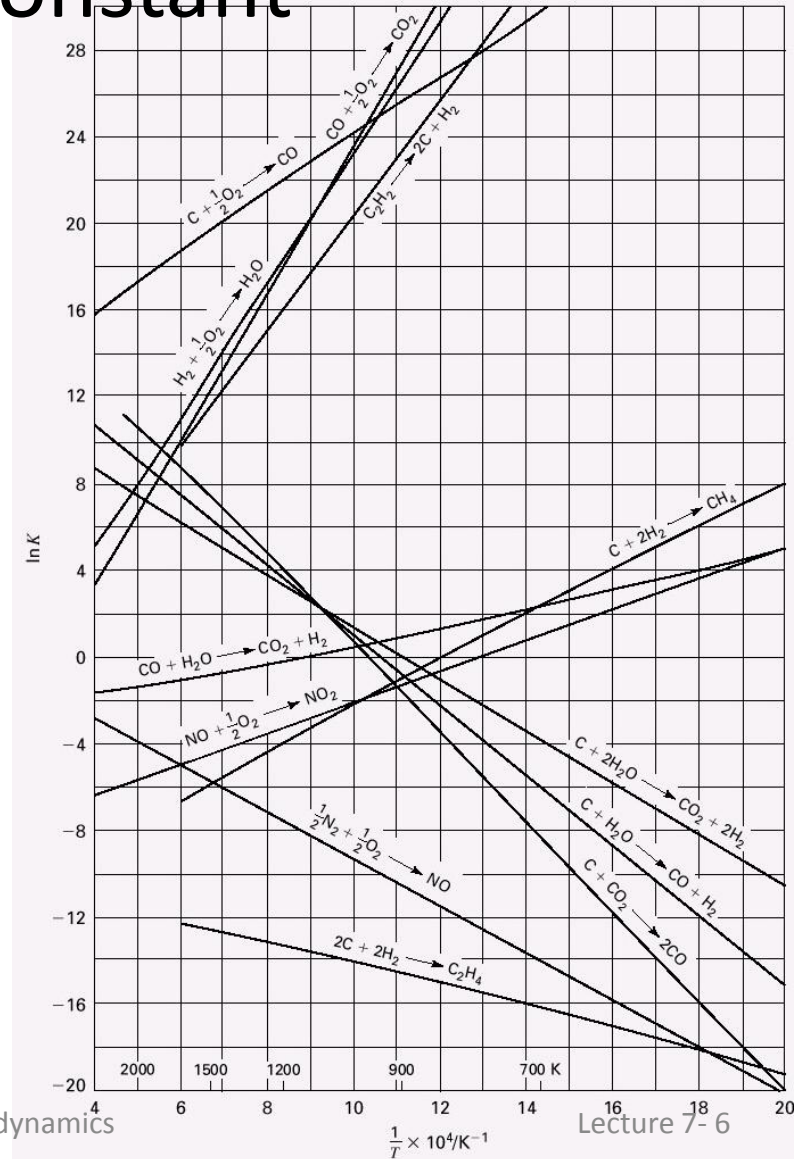
Reaction Equilibrium Equilibrium Constant

- Temperature effects...
 - on equilibrium constant

$$\frac{d \ln K}{dT} = \frac{\Delta H^\circ}{RT^2}$$

- on standard heat of reaction

$$\Delta H^\circ = \Delta H_0^\circ + R \int_{T_0}^T \frac{\Delta C_P^\circ}{R} dT$$



Reaction Equilibrium

Equilibrium Constant

- Composition effects...

- in gas-phase reactions

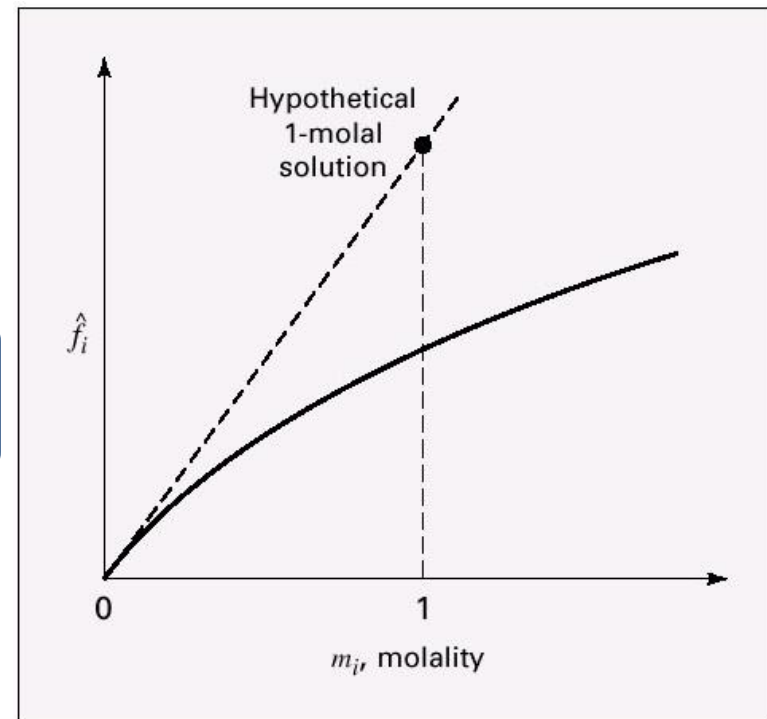
$$\prod_i (y_i \phi_i)^{v_i} = K \cdot \left(\frac{P}{P^\circ} \right)^{-\nu}$$

- in liquid-phase reactions

$$\prod_i (y_i \gamma_i)^{v_i} = K \cdot \exp \left(\frac{(P^\circ - P)}{RT} \sum_i (v_i V_i) \right)^{-\nu}$$

- Equilibrium conversion ε_e

Standard state for dilute aqueous solutions.



Phase Rule

- For a non-reacting multi-phase multi-component system:

$$F = 2 - \pi + N$$

F degrees of freedom

π number of phases

N number of chem. species

- For a multi-phase multi-component system in which r chemical reactions take place:

$$F = 2 - \pi + N - r$$

Multi-reaction Equilibrium

- For a gas-phase system (ideal gas):

$$\prod_i (y_i)^{v_{i,j}} = \left(\frac{P}{P^\circ} \right)^{-\nu_j} \cdot K_j$$

- Elemental material balance

$$\sum_i n_i a_{ik} = A_k$$

k element

i molecular species

A total number of atomic masses

a number of atoms

- Standard Gibbs energy change:

$$\Delta G_{f_i}^\circ + RT \ln \left(\frac{y_i \hat{\phi}_i P}{P^\circ} \right) + \sum_k \lambda_k a_{ik} = 0 \quad (i = 1, 2, \dots, N)$$

Multi-reaction Equilibrium

Worked example: A bed of coal (carbon) in a coal gasifier is fed with steam and air, and produces a gas stream containing H_2 , CO , O_2 , H_2O , CO_2 , and N_2 . If the feed to the gasifier consists of 1 mol of steam and 2.38 mol of air, calculate the equilibrium composition of the gas stream at $P = 20$ bar for temperatures of 1000 and 1500 K.

	$\Delta G^\circ_f / \text{J mol}^{-1}$		
T / K	H_2O	CO	CO_2
1000	-192,420	-200,240	-395,790
1500	-164,310	-243,740	-396,160

