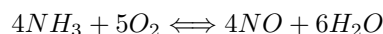
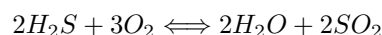


Problem 1: Develop expressions for the mole fractions of reacting species as function of the reaction coordinate, ε , for:

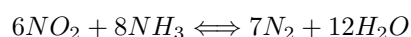
- (a) A system initially containing 2 moles of NH_3 and 5 moles of O_2 :



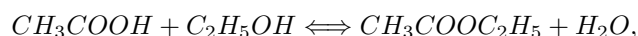
- (b) A system initially containing 3 moles of H_2S and 5 moles of O_2 :



- (c) A system initially containing 3 moles of NO_2 , 4 moles of NH_3 and 1 mole of N_2 :



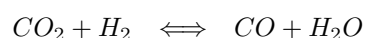
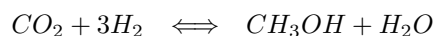
Problem 2: In the esterification reaction of acetic acid with ethanol at 100°C ,



calculate the mass fraction of ethyl acetate given that initially there was 1 mole of acetic acid and ethanol. The reaction enthalpy and Gibbs energy at standard state (25°C and 1 atm) are $\Delta H_{298}^\circ = -3640 \text{ J}$ and $\Delta G_{298}^\circ = -4650 \text{ J}$.

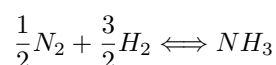
Problem 3: Give the equation for the stoichiometric combustion of 1 mole of general hydrocarbons, C_xH_y with O_2 producing CO_2 and water. Develop expressions for gas phase mole fractions of each species as a function of the reaction coordinate. Assume that initially 1 mole of hydrocarbon and the stoichiometric amount of oxygen for complete conversion are present.

Problem 4: In a reactor, 2 moles of CO_2 , 5 moles of H_2 and 1 mole of CO are mixed and start to undergo the following reactions:



Develop expressions for the mole fractions of the reacting species as functions of the reaction coordinates for the two reactions.

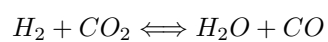
Problem 5: For the ammonia synthesis reaction,



with 0.5 mole of N_2 and 1.5 moles of H_2 as the initial amounts of reactants and with the assumption that the equilibrium mixture is an ideal gas, show that

$$\varepsilon_e = 1 \pm \left(1 + 1.299K \frac{P}{P^\circ} \right)^{-0.5}$$

Problem 6: Assuming that all species and their mixtures are ideal gases, derive an equation for the Gibbs energy as a function of the reaction coordinate for the reaction below at 1000K.



Given ΔG_f° (J.gmol⁻¹) at 1000K: (a) H₂O: -192420, (b) CO: -200240 and (c) CO₂: -395790.

Problem 01:

a) 2 moles of NH_3 + 5 moles of O_2 :



$$\nu = \sum \nu_i = -4 - 5 + 4 + 6 = 1$$

$$m_0 = \sum m_{i,0} = 2 + 5 = 7$$

↑
initial number
of moles

$$y_i = \frac{m_i}{m} = \frac{m_{i,0} + \nu_i \epsilon}{m_0 + \nu \epsilon}$$

$$y_{\text{NH}_3} = \frac{2 - 4\epsilon}{7 + \nu} ; \quad y_{\text{O}_2} = \frac{5 - 5\epsilon}{7 + \nu}$$

$$y_{\text{NO}} = \frac{4\epsilon}{7 + \nu} ; \quad y_{\text{H}_2\text{O}} = \frac{6\epsilon}{7 + \nu}$$

b) 3 moles of H_2S + 5 moles of O_2 :



$$\nu = -2 - 3 + 2 + 2 = -1 \quad m_0 = 3 + 5 = 8$$

$$y_{\text{H}_2\text{S}} = \frac{3 - 2\epsilon}{8 - \epsilon} ; \quad y_{\text{O}_2} = \frac{5 - 3\epsilon}{8 - \epsilon} ; \quad y_{\text{H}_2\text{O}} = \frac{2\epsilon}{8 - \epsilon} ; \quad y_{\text{SO}_2} = \frac{2\epsilon}{8 - \epsilon}$$

c) 3 mols of NO_2 + 4 mols of NH_3 + 1 mol of N_2



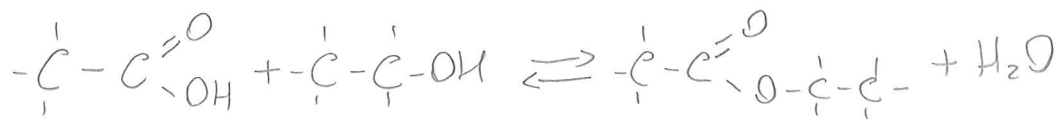
$$\nu = -16 - 8 + 7 + 12 = 5$$

$$m_0 = 3 + 4 + 1 = 8$$

$$y_{\text{NO}_2} = \frac{3 - 6\varepsilon}{8 + 5\varepsilon}; \quad y_{\text{NH}_3} = \frac{4 - 8\varepsilon}{8 + 5\varepsilon}; \quad y_{\text{N}_2} = \frac{1 + 7\varepsilon}{8 + 5\varepsilon}; \quad y_{\text{H}_2\text{O}} = \frac{12\varepsilon}{8 + 5\varepsilon}$$

Problem 02:

3



Initially: $\left\{ \begin{array}{l} 1 \text{ mol HAc} \\ 1 \text{ mol EtOH} \end{array} \right.$

$$K_{\text{EtAc}} = ?$$

$$\left\{ \begin{array}{l} \Delta H_{298}^\circ = -3640 \text{ J} \\ \Delta G_{298}^\circ = -4650 \text{ J} \end{array} \right.$$

$$K_{\text{EtAc}} = \frac{\varepsilon}{2 + 0.5\varepsilon} = \varepsilon/2 = K_{\text{H}_2\text{O}}$$

$$K_{\text{HAc}} = \frac{1 - \varepsilon}{2} = K_{\text{EtOH}}$$

Assuming ideal solution

$$\prod_{i=1}^{c=4} x_i^{\nu_i} = K = \frac{K_{\text{EtAc}} K_{\text{H}_2\text{O}}}{K_{\text{HAc}} K_{\text{EtOH}}}$$

$$K = \frac{\varepsilon^2}{4} \frac{4}{(1-\varepsilon)^2} = \frac{\varepsilon^2}{(1-\varepsilon)^2} \Rightarrow$$

By calculating K , we can obtain ε and then

$$K_{\text{EtAc}}$$

K can be calculated from

$$\ln K_{298} = - \frac{\Delta G_{298}^\circ}{RT} = \frac{4650}{8.314 \times 298.15} = 1.8759$$

K is temperature-dependent!

Now, in order to calculate K at 373.15 K (100°C) 4
we can use the van't Hoff Equation

$$\frac{d(\ln K)}{dT} = - \frac{\Delta H_{298}^\circ}{RT^2}$$
$$\int_{K_{298}}^{K_{373}} d(\ln K) = - \int_{298.15}^{373.15} \frac{\Delta H_{298}^\circ}{RT^2} dT$$

$$\ln \left(\frac{K_{373}}{K_{298}} \right) = - \frac{\Delta H_{298}^\circ}{R} \left(\frac{1}{373.15} - \frac{1}{298.15} \right) = -0.2951$$

\swarrow -3640 J

$$K_{373} = 4.8586$$

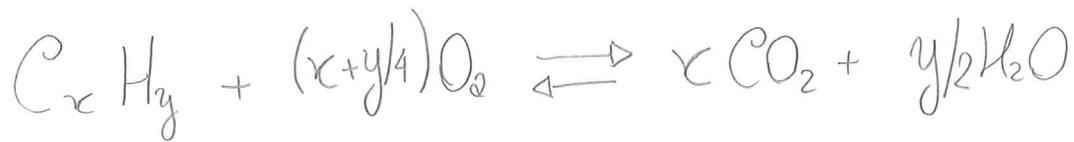
$$K_{373} = 4.8586 = \frac{\epsilon^2}{(1-\epsilon)^2} \therefore \epsilon = 0.6879$$

Now

$$\chi_{\text{EtAc}} = \frac{\epsilon}{2} = 0.34395$$

Problem 3:

5



$$\nu = -1 - \left(x + \frac{y}{4}\right) + x + \frac{y}{2} = \frac{y}{4} - 1$$

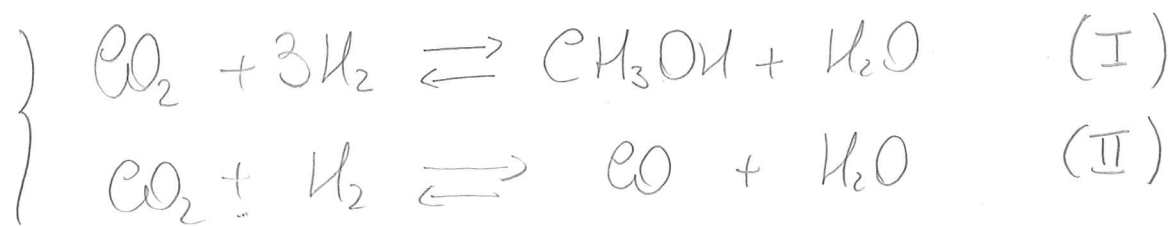
$$n_o = 1 + \left(x + \frac{y}{4}\right)$$

$$y_{C_x H_y} = \frac{1 - \varepsilon}{(1 + x + y/4) + (y/4 - 1)\varepsilon} ; \quad y_{O_2} = \frac{(x + y/4) - (x + y/4)\varepsilon}{(1 + x + y/4) + (y/4 - 1)\varepsilon}$$

$$y_{CO_2} = \frac{x\varepsilon}{(1 + x + y/4) + (y/4 - 1)\varepsilon} ; \quad y_{H_2O} = \frac{y/2 \varepsilon}{(1 + x + y/4) + (y/4 - 1)\varepsilon}$$

Problem 4

6



Initial : $\left\{ \begin{array}{l} 2 \text{ moles of } \text{CO}_2 \\ 5 \text{ moles of } \text{H}_2 \\ 1 \text{ mole of } \text{CO} \end{array} \right.$

$j \backslash i$	CO_2	H_2	CH_3OH	CO	H_2O	ν_j
I	-1	-3	1	0	1	-2
II	-1	-1	0	1	1	0

$$m_0 = 2 + 5 + 1 = 8$$

$$y_i = \frac{m_{i,0} + \sum_j \nu_{ij} \epsilon_j}{m_0 + \sum_j \nu_j \cdot \epsilon_j}$$

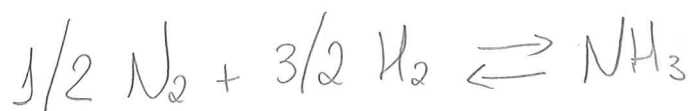
$$y_{\text{CO}_2} = \frac{2 - \epsilon_I - \epsilon_{II}}{8 - 2\epsilon_I}; \quad y_{\text{H}_2} = \frac{5 - 3\epsilon_I - \epsilon_{II}}{8 - 2\epsilon_I}$$

$$y_{\text{CH}_3\text{OH}} = \frac{\epsilon_I}{8 - 2\epsilon_I}; \quad y_{\text{CO}} = \frac{1 + \epsilon_{II}}{8 - 2\epsilon_I}$$

$$y_{\text{H}_2\text{O}} = \frac{\epsilon_I + \epsilon_{II}}{8 - 2\epsilon_I}$$

Problem 5

7



Initial: 0.5 mole N_2
1.5 moles H_2

Show: $\epsilon_e = 1 - \left(1 + 1.299 \kappa \frac{P}{P_0}\right)^{-0.5}$

$$M_0 = 0.5 + 1.5 = 2$$

$$\nu = -\frac{1}{2} - \frac{3}{2} + 1 = -1$$

$$y_i = \frac{M_{i,0} + \nu_i \epsilon}{M_0 + \nu \epsilon}$$

$$y_{\text{N}_2} = \frac{\frac{1}{2} - \frac{1}{2} \epsilon}{2 - \epsilon} = \frac{\frac{1}{2}(1 - \epsilon)}{2 - \epsilon}; \quad y_{\text{H}_2} = \frac{\frac{3}{2} - \frac{3}{2} \epsilon}{2 - \epsilon} = \frac{\frac{3}{2}(1 - \epsilon)}{2 - \epsilon}$$

$$y_{\text{NH}_3} = \frac{\epsilon}{2 - \epsilon}$$

For gas phase the equilibrium constant is defined as:

$$\prod_{i=1}^c (\bar{\phi}_i y_i)^{\nu_i} = \kappa (P/P_0)^{-\nu}$$

Assuming the mixture behaves as an ideal gas, $\bar{\phi}_i = 1$

$$\prod_{i=1}^c y_i^{\lambda_i} = K (P/P_0)^{-\nu}$$

8

$$y_{N_2}^{-1/2} y_{H_2}^{-3/2} y_{NH_3} = K \left(\frac{P}{P_0} \right)$$

$$\frac{y_{NH_3}}{y_{N_2}^{1/2} y_{H_2}^{3/2}} = \frac{\varepsilon/2-\varepsilon}{\left[\frac{1/2(1-\varepsilon)}{2-\varepsilon} \right]^{1/2} \left[\frac{3/2(1-\varepsilon)}{2-\varepsilon} \right]^{3/2}} = K \left(\frac{P}{P_0} \right)$$

$$\frac{\varepsilon(2-\varepsilon)}{(1-\varepsilon)^2 (1/2)^{1/2} (3/2)^{3/2}} = K \left(\frac{P}{P_0} \right)$$

$$\frac{\varepsilon(2-\varepsilon)}{(1-\varepsilon)^2} = \underbrace{\left(\frac{1}{2} \right)^{1/2} \left(\frac{3}{2} \right)^{3/2}}_{1.2990} K \left(\frac{P}{P_0} \right)$$

Γ

$$2\varepsilon - \varepsilon^2 = (1 - 2\varepsilon + \varepsilon^2) \Gamma = \Gamma - 2\Gamma\varepsilon + \Gamma\varepsilon^2$$

$$\varepsilon^2(1+\Gamma) + (-2\Gamma-2)\varepsilon + \Gamma = 0$$

$$\varepsilon = \frac{-(-2\Gamma-2) \pm \sqrt{(-2\Gamma-2)^2 - 4(1+\Gamma)\Gamma}}{2(1+\Gamma)}$$

$$\mathcal{E} = \frac{-(-2\Gamma+2) \pm \sqrt{4\Gamma^2+8\Gamma+4-4\Gamma-4\Gamma^2}}{2(1+\Gamma)}$$

$$\mathcal{E} = \frac{(2\Gamma+2) \pm \sqrt{4(\Gamma+1)}}{2(1+\Gamma)} = \frac{2(1+\Gamma) \pm 2\sqrt{1+\Gamma}}{2(1+\Gamma)}$$

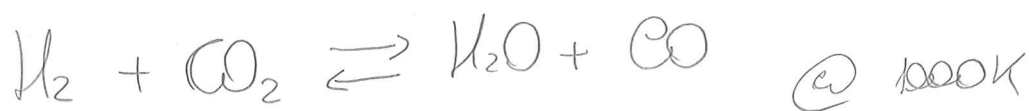
$$\mathcal{E} = \frac{(1+\Gamma) \left[1 \pm (1+\Gamma)^{-1/2} \right]}{1+\Gamma} = \underline{\underline{1 \pm (1+\Gamma)^{-1/2}}}$$

with

$$1+\Gamma = 1 + 1.299 \kappa (P/P_0)$$

Problem 6 ($T = 1000\text{ K}$)

10



$$G = \sum y_i G_i + RT \sum y_i \ln y_i$$

$$G = \sum y_i \Delta G_{f,i}^\circ + RT \sum y_i \ln y_i$$

$$\left\{ \begin{array}{l} \Delta G_{f, \text{H}_2\text{O}}^\circ = -192420 \text{ J/mol} \\ \Delta G_{f, \text{CO}}^\circ = -200240 \text{ J/mol} \\ \Delta G_{f, \text{CO}_2}^\circ = -395790 \text{ J/mol} \end{array} \right.$$

$$dG^e = d(mG) = m \frac{dG}{d\varepsilon} + G \frac{dm}{d\varepsilon} = 0$$

$$G \frac{dm}{d\varepsilon} = 0 \rightarrow dG/d\varepsilon = 0 \quad (\text{equilibrium})$$

Assuming that initially there is 1 mole of H_2 and CO_2

$$y_{\text{H}_2} = \frac{1-\varepsilon}{2} = y_{\text{CO}_2} \quad ; \quad y_{\text{H}_2\text{O}} = \frac{\varepsilon}{2} = y_{\text{CO}}$$

$$G = \left(y_{\text{H}_2} \Delta G_{f, \text{H}_2}^\circ + y_{\text{CO}_2} \Delta G_{f, \text{CO}_2}^\circ + y_{\text{H}_2\text{O}} \Delta G_{f, \text{H}_2\text{O}}^\circ + y_{\text{CO}} \Delta G_{f, \text{CO}}^\circ \right) +$$
$$RT \left(y_{\text{H}_2} \ln y_{\text{H}_2} + y_{\text{CO}_2} \ln y_{\text{CO}_2} + y_{\text{H}_2\text{O}} \ln y_{\text{H}_2\text{O}} + y_{\text{CO}} \ln y_{\text{CO}} \right)$$

$$\Delta G_{f, \text{H}_2}^\circ = 0$$

$$G = \left[\frac{1-\varepsilon}{2} \left(\frac{-395790 \text{ J}}{\text{mol}} \right) + \frac{\varepsilon}{2} \left(\frac{-192420 - 200240}{\text{mol}} \right) \right] + RT \left[(1-\varepsilon) \ln \left(\frac{1-\varepsilon}{2} \right) + \varepsilon \ln \left(\frac{\varepsilon}{2} \right) \right]$$

$$\frac{dG}{d\varepsilon} = -A + B - RT \ln \left(\frac{1-\varepsilon}{2} \right) - RT + RT \ln \left(\frac{\varepsilon}{2} \right) + RT$$

$$\frac{dG}{d\varepsilon} = B - A + RT \left[\ln \left(\frac{\varepsilon}{2} \right) - \ln \left(\frac{1-\varepsilon}{2} \right) \right] = 0$$

$$\text{where } A = \frac{-395790}{2} = -197895.0$$

$$B = \frac{-192420 - 200240}{2} = -196330.0$$

$$\ln \left[\frac{\varepsilon/2}{(1-\varepsilon)/2} \right] = -0.1882$$

$$\boxed{\varepsilon = 0.4531}$$

(@ equilibrium)

