## UNIVERSITY OF ABERDEEN SESSION 2013–2014

Degree Examination in EG3521 Engineering Thermodynamics  $0^{\rm th}$  May 2014 00.00-00.00

## SAMPLE PAPER.

*Notes:* 

- (i) Candidates ARE permitted to use an approved calculator.
- (ii) Candidates ARE permitted to use steam tables, which will be provided.
- (iii) Candidates ARE permitted to use refrigerant tables, which will be provided.
- (iv) Candidates ARE permitted to use psychrometric chart, which will be provided.
- (v) Data sheets are attached to the paper.

#### PLEASE NOTE THE FOLLOWING

- (i) You **must not** have in your possession any material other than that expressly permitted in the rules appropriate to this examination. Where this is permitted, such material **must not** be amended, annotated or modified in any way.
- (ii) You **must not** have in your possession any material that could be determined as giving you an advantage in the examination.
- (iii) You **must not** attempt to communicate with any candidate during the exam, either orally or by passing written material, or by showing material to another candidate, nor must you attempt to view another candidate's work.

Failure to comply with the above will be regarded as cheating and may lead to disciplinary action as indicated in the Academic Quality Handbook (www.abdn.ac.uk/registry/quality/appendix7x1.pdf) Section 4.14 and 5.

Candidates must attempt all questions.

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An engine operates in a dual cycle with compression  $(r_c)$  and expansion  $(r_e)$  ratios of 9 and 5, respectively. The initial pressure and temperature of the air are 1 bar and 30°C. The heat liberated at constant pressure is twice the heat liberated at constant volume, i.e.,

$$C_p(T_4 - T_3) = 2C_v(T_3 - T_2).$$

The isentropic expansion and compression strokes follow  $PV^n = \text{constant}$ , with n = 1.25. The cylinder bore (diameter) is of 250 mm and the stroke length is of 400 mm.

(a) Calculate pressures and temperatures at all strokes and fill up the table below,

Stroke	P (bar)	T (K)
1	1.0	303.15
2		
3		
4		
5		

[8 Marks]

(b) Sketch the P-v diagram for this cycle, indicating the swept  $(V_s)$  and TDC  $(V_c)$  volumes.

[2 Marks]

(c) Calculate the Mean Effective Pressure (MEP) of the cycle (in bar) using the following expression:

$$MEP = \frac{1}{r_c - 1} \left[ P_3 \left( \rho - 1 \right) + \frac{P_4 \rho - P_5 r_c}{n - 1} - \frac{P_2 - P_1 r_c}{n - 1} \right]$$

[2 Marks]

(d) Calculate work done per cycle (in kJ) and the heat supplied per cycle (in kJ), given by

$$W_{\rm cycle} = MEP \times V_s \quad \text{and} \quad Q_{\rm cycle} = mQ_s = m \left[ C_p \left( T_3 - T_2 \right) + C_p \left( T_4 - T_3 \right) \right]$$
 Given:  $V_1 = V_s + V_c = \frac{r_c}{r_c - 1} V_s$ 

[2 Marks]

(e) Sketch T-S and P-V diagrams for the Otto and Diesel cycles.

[6 Marks]

Also given:

$$C_p = 1.0 \frac{\text{kJ}}{\text{kg.K}} , \quad C_v = 0.71 \frac{\text{kJ}}{\text{kg.K}} , \quad MW = 29 \frac{\text{g}}{\text{gmol}} \quad \text{(molecular weight)},$$

$$R = 8.3144621 \times 10^{-5} \frac{\text{m}^3.\text{bar}}{\text{K.gmol}} \quad \text{(gas constant)}, \quad \rho = \frac{r_c}{r_e}$$

(a) A horizontally mounted turbine is housed between circular inlet and outlet pipes of circumference 1 m and 0.6 m, respectively. Assume gas satisfying the steady flow energy conservation

$$\frac{\dot{Q} - \dot{W}_s}{\dot{m}} = \left(h_2 + \frac{u_2^2}{2}\right) - \left(h_1 + \frac{u_1^2}{2}\right),\,$$

flows through the turbine at a steady rate of 4 kg/s. At the inlet (labelled 1), the fluid has a specific enthalpy h of 70 kJ/kg and a velocity u of 30 m/s, while at the outlet (labelled 2), the fluid has a specific enthalpy of 40 kJ/kg. If the gas does work on the turbine at a rate of 30 kW and transfers heat to the surroundings at a rate of 15 kW, then find the change in gas density between the inlet and the outlet. [4 Marks]

(b) For gas flow along a duct whose length is parameterized by x and has slowly-varying cross-sectional area A(x), use equations corresponding to mass and energy conservation to show that

$$\frac{dV}{V} + \frac{dh}{u^2} - \frac{dA}{A} = 0,$$

where the specific volume is denoted V, the specific enthalpy h, and fluid velocity u. [2 Marks]

- (c) Define the speed of sound c and the Mach number Ma in a gas. State equations that are appropriate for calculating these quantities in an isentropic gas and define the variables used. [4 Marks]
- (d) For an isentropic process show that changes in specific volume are related to changes in pressure (p) through

$$dV = -\frac{V^2}{c^2}dp,$$

and explain how changes in specific enthalpy are related to changes in pressure. [3 Marks]

(e) Hence, for isentropic flow along a duct, show that

$$\frac{1}{A\left(1-Ma^{2}\right)}\frac{dA}{dx}=\frac{1}{\rho\,Ma^{2}}\frac{d\rho}{dx},$$

where the gas density is denoted  $\rho$ . [5 Marks]

(f) Explain with reasoning how the gas density changes for flow along a supersonic diffuser. [2 Marks]

(a) Define the specific humidity  $\omega$ , the saturation pressure of water vapour  $p_{v,sat}$ , and relative humidity  $\varphi$ . Assuming that dry air and water vapour behave like ideal gases show that

$$\omega = \frac{R_a \varphi p_{\text{v,sat}}}{R_v \left( p - \varphi p_{\text{g,v,sat}} \right)},$$

where  $R_a$  and  $R_v$  are the specific gas constants of dry air and water vapour, respectively.

[5 Marks]

(b) Air leaving an air-conditioning system in a building is mixed adiabatically with air from outside in a steady process. If the inlets to the mixing chamber are labelled 1 and 2 and the outlet is labelled 3, then state equations corresponding to the mass conservation of dry air, the mass conservation of water vapour and the conservation of energy. Hence show that

$$\frac{\dot{m}_{a2}}{\dot{m}_{a1}} = \frac{\omega - \omega_1}{\omega_2 - \omega_3} = \frac{h_3 - h_1}{h_2 - h_3}$$

where  $\dot{m}_a$  is a mass flux of dry air and h is an enthalpy.

[7 Marks]

- (c) Saturated air at 16°C leaves the cooling section of an air-conditioning system in a building at a rate of 1 m<sup>3</sup>/s. This air is mixed adiabatically at a constant pressure of 100 kPa, with air from outside that has temperature 30°C and specific humidity 0.0182 kg H<sub>2</sub>O/kg dry air. If the mass flux of dry air after mixing is 1.8 kg/s, then:
  - (i) Determine the mass flux through both inlets;

[3 Marks]

(ii) Calculate the specific humidity of the air leaving the cooling section of the air-conditioning system;

[1 Mark]

(iii) Calculate the specific humidity of the mixed air.

[4 Marks]

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You may assume the saturation pressure of water vapour at 16°C is 1818.747 Pa and that the specific gas constants  $R_a = 287.1 \text{ J/(kg.K)}$  and  $R_v = 461.5 \text{ J/(kg.K)}$ , respectively.

A vapour-compression refrigeration system circulates Refrigerant 134a at a rate of 6 kg/min. The refrigerant enters the compressor at -10°C, 1.4 bar and exits at 7 bar. The isentropic compressor efficiency is 67%. There are no appreciable pressure drops as the refrigerant flows through the condenser and evaporator. The refrigerant leaves the condenser at 7 bar, 24°C. Ignoring heat transfer between the compressor and its surroundings, determine:

(a)  $H_i$ ,  $i \in \{1, 2, 3, 4\}$ ;

[8 Marks]

(b) Coefficient of performance,  $\beta$ ;

$$\beta = \frac{H_1 - H_4}{H_2 - H_1}$$

[3 Marks]

(c) Refrigeration capacity,  $\dot{Q}_{\rm in}$  (in ton),

$$\dot{Q}_{\rm in} = \dot{m} \left( H_1 - H_4 \right)$$

[3 Marks]

(d) Sketch the schematics of the process and T-S diagram for this cycle.

[6 Marks]

In the expressions above for  $\beta$  and  $\dot{Q}_{\rm in}$ , assume that subscripts 1, 2, 3 and 4 represent the following flows:

- 1: Evaporator ⇒ Compressor;
- 2: Compressor  $\Rightarrow$  Condenser;
- 3: Condenser  $\Rightarrow$  Expansion Valve and;
- 4: Expansion Valve  $\Rightarrow$  Evaporator.

Also given:  $1 \text{ ton} = 1.4 \times 10^4 \frac{kJ}{h}$ 

In the secondary cooling circuit of a nuclear power plant, the steam generator (boiler / reheater) is connected to two turbines operating as a reheat Rankine cycle (Fig. 1). Primary superheated steam is at 40 bar and 370°C, with reheat to 7 bar and 370°C. The isentropic efficiencies of the first ( $\eta_{T1}$ ) and second ( $\eta_{T2}$ ) turbines and boiler feed pump ( $\eta_P$ ) are 84%, 80% and 61% respectively.

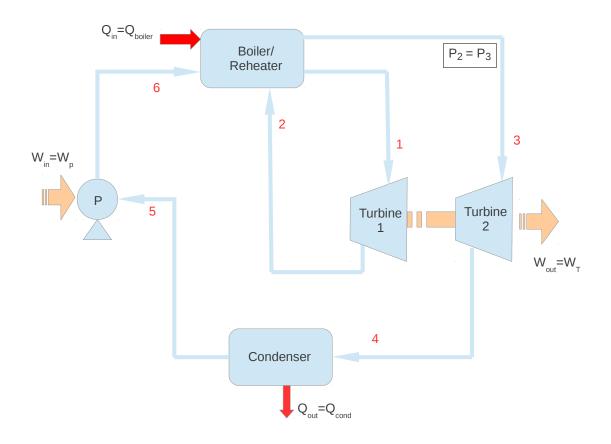


Figure 1: Reheat Rankine cycle with 2 turbines.

(a) In the Table below, determine (a)-(j). [10 Marks]

Stage	P	$\mathbf{T}$	State	H	S
	(bar)	$(^{o}\mathbf{C})$		$(\mathrm{kJ.kg^{-1}})$	$(\mathrm{kJ.(kg.K})^{-1})$
1	40	370	superheated	(a)	(b)
			steam		
2	_	_	(c)	_	_
3	7	370	superheated	(d)	(e)
			steam		
4	0.10	_	_	_	_
5	0.10	_	(f)	$(\mathbf{g})$	(h)
6	40	_	(i)	(j)	_

(b) Calculate the thermal efficiency ( $\eta_{\text{Thermal}}$ ) of the reheat Rankine cycle with 2 turbines.  $\eta_{\text{Thermal}}$  is expressed as,

$$\eta_{\text{Thermal}} = \frac{\left(H_1 - H_{2s}\right)\eta_{\text{T1}} + \left(H_3 - H_{4s}\right)\eta_{\text{T2}} - V_5\left(P_6 - P_5\right)\eta_{\text{P}}^{-1}}{\left(H_1 - H_6\right) + \left(H_3 - H_2\right)}$$

where the subscript s indicates the ideal state. [5 Marks]

(c) Sketch the T-S diagram for this cycle. [5 Marks]

#### TABLE V

#### **Conversion Factors**

Force

Pressure

 $1 \,\mathrm{bar}$  =  $750.06 \,\mathrm{mm}\,\mathrm{Hg}$ 

= 0.9869 atm=  $10^5 \text{ N/m}^2$ =  $10^3 \text{ kg/m-sec}^2$ 

 $1 \text{ N/m}^2$  = 1 pascal

=  $10^{-5}$  bar =  $10^{-2}$  kg/m-sec<sup>2</sup>

1 atm = 760 mm Hg

=  $1.03 \text{ kgf/cm}^2 = 1.01325 \text{ bar}$ =  $1.01325 \times 10^5 \text{ N/m}^2$ 

Work, Energy or Heat

1 joule = 1 newton metre

1 watt-sec

 $= 2.7778 \times 10^{-7} \, \text{kWh}$ 

0.239 cal

 $= 0.239 \times 10^{-3} \,\mathrm{kcal}$ 

1 cal = 4.184 joule

=  $1.1622 \times 10^{-6} \text{ kWh}$ 

 $1 \text{ kcal} = 4.184 \times 10^3 \text{ joule}$ 

 $427~\mathrm{kgfm}$ 

 $= 1.1622 \times 10^{-3} \text{ kWh}$ 

 $1 \text{ kWh} \qquad \qquad = \qquad 8.6 \times 10^5 \text{ cal}$ 

 $860 \, \text{kcal}$   $3.6 \times 10^6 \, \text{joule}$ 

 $1 \text{ kgfm} \qquad \qquad = \qquad \left(\frac{1}{427}\right) \text{ kcal} = 9.81 \text{ joules}$ 

Power

 $\begin{array}{lll} 1\,\mathrm{watt} & = & 1\,\mathrm{joule/sec} = 0.86\,\mathrm{kcal/h} \\ 1\,\mathrm{h.p.} & = & 75\,\mathrm{mkgf/sec} = 0.1757\,\mathrm{kcal/sec} \\ \end{array}$ 

= 735.3 watt

1 kW = 1000 watts

= 860 kcal/h

#### Specific heat

1 kcal/kg - °K = 4.18 kJ/kg-K

### Thermal conductivity

1 watt/m-K = 0.8598 kcal/h-m-°C 1 kcal/h-m-°C = 1.16123 watt/m-K = 1.16123 joules/s-m-K

#### Heat transfer co-efficient

 $\begin{array}{lll} 1 \, watt/m^2\text{-}K & = & 0.86 \, kcal/m^2\text{-}h\text{-}^\circ\text{C} \\ 1 \, kcal/m^2\text{-}h\text{-}^\circ\text{C} & = & 1.163 \, watt/m^2\text{-}K \end{array}$ 

## IMPORTANT ENGINEERING CONSTANTS AND EXPRESSIONS IN SI UNITS

	Engineering constants and expressions	M.K.S. system	S.I. units
1. 2.	Value of $g_0$ Universal gas constant	9.81 kg-m/kgf-sec <sup>2</sup> 848 kgf-m/kg mole-°K	1 kg-m/N-sec <sup>2</sup> 848 × 9.81 = 8314 J/kg-mole-°K
3.	Gas constant (R)	29.27 kgf m/kg-°K for air	( $\because$ 1 kgf-m = 9.81 joules) $\frac{8314}{29} = 287 \text{ joules/kg-K for air}$
4.	Specific heats (for air)	$c_n = 0.17 \text{ kcal/kg-}^{\circ}\text{K}$	$c_n = 0.17 \times 4.184$
	Specific flexis (tot till)	$c_p$ = 0.24 kcal/kg-°K	= $0.71128 \text{ kJ/kg-K}$ $c_p = 0.24 \times 4.184$ = $1 \text{ kJ/kg-K}$
5.	Flow through nozzle-exit velocity $(C_2)$	$91.5\mathrm{\sqrt{U}}$ where U is in kcal	44.7  subset U where U is in kJ
6.	Refrigeration 1 ton	= 50 kcal/min	= 210 kJ/min
7.	Heat transfer		
	The Stefan Boltzman Law is given by :	$\begin{aligned} &Q = \sigma T^4 \; kcal/m^2\text{-}h \\ &when \; \sigma = 4.9 \times 10^{-8} \\ &kcal/h\text{-}m^2\text{-}^\circ K^4 \end{aligned}$	$\label{eq:Q} \begin{split} Q &= \sigma T^4  watts/m^2\text{-}h \\ when  \sigma &= 5.67 \times 10^{-8} \\ W/m^2 K^4 \end{split}$

 ${\bf TABLE~II}$  Saturated Water and Steam (Pressure) Tables

Absolute Temp. Specific enthalpy Specific entropy Specific volume											
Ab solute	Temp.	Spc	•	llpy	Sp	•	рру				
pressure	(°C)		(kJ/kg)			$(kJ/kg\ K)$		$(m^3)$	kg)		
(bar)		,	7	7							
p	$t_s$	$h_f$	$h_{fg}$	$h_g$	$s_f$	$s_{\!f\!g}$	$s_g$	$v_f$	$v_g$		
0.006113	0.01	0.01	2501.3	2501.4	0.000	9.156	9.156	0.0010002	206.14		
0.010	7.0	29.3	2484.9	2514.2	0.106	8.870	8.976	0.0010000	129.21		
0.015	13.0	54.7	2470.6	2525.3	0.196	8.632	8.828	0.0010007	87.98		
0.020	17.0	73.5	2460.0	2533.5	0.261	8.463	8.724	0.001001	67.00		
0.025	21.1	88.5	2451.6	2540.1	0.312	8.331	8.643	0.001002	54.25		
0.030	24.1	101.0	2444.5	2545.5	0.355	8.223	8.578	0.001003	45.67		
0.035	26.7	111.9	2 438.4	2 550.3	0.391	8.132	8.523	0.001003	39.50		
0.040	29.0	121.5	2 432.9	2 554.4	0.423	8.052	8.475	0.001003	34.80		
0.045	31.0	130.0	2 428.2	2558.2	0.425	7.982	8.433	0.001004	31.13		
0.050	32.9	137.8	2423.7	2561.5	0.431	7.902	8.395	0.001005	28.19		
0.055	34.6	144.9	2419.6	2 565.5	0.500	7.861	8.361	0.001003	25.77		
0.000	54.0	111.0	2 415.0	2 000.0	0.500	7.001	0.001	0.001000	20.11		
0.060	36.2	151.5	2415.9	2567.4	0.521	7.809	8.330	0.001006	23.74		
0.065	37.6	157.7	2412.4	2570.1	0.541	7.761	8.302	0.001007	22.01		
0.070	39.0	163.4	2409.1	2572.5	0.559	7.717	8.276	0.001007	20.53		
0.075	40.3	168.8	2406.0	2574.8	0.576	7.675	8.251	0.001008	19.24		
0.080	41.5	173.9	2403.1	2577.0	0.593	7.636	8.229	0.001008	18.10		
0.085	42.7	178.7	2400.3	2579.0	0.608	7.599	8.207	0.001009	17.10		
0.090	43.8	183.3	2397.7	2581.0	0.622	7.565	8.187	0.001009	16.20		
0.095	44.8	187.7	2395.2	2582.9	0.636	7.532	8.168	0.001010	15.40		
0.10	45.8	191.8	2392.8	2584.7	0.649	7.501	8.150	0.001010	14.67		
0.11	47.7	199.7	2 388.3	2 588.0	0.674	7.453	8.117	0.001011	13.42		
0.12	49.4	206.9	2 384.2	2 591.1	0.696	7.390	8.086	0.001012	12.36		
0.13	51.0	213.7	2 380.2	2 593.9	0.717	7.341	8.058	0.001012	11.47		
0.14	52.6	220.0	2376.6	2 596.6	0.737	7.296	8.033	0.001013	10.69		
0.15	54.0	226.0	2373.2	2599.2	0.7549	7.2544	8.0093	0.001014	10.022		
0.16	55.3	231.6	2370.0	2 601.6	0.772 1	7.2148	7.9869	0.001015	9.433		
0.17	56.6	236.9	2366.9	2603.8	0.7883	7.1775	7.9658	0.001015	8.911		
0.18	57.8	242.0	2363.9	2605.9	0.8036	7.1424	7.9459	0.001016	8.445		
0.19	59.0	246.8	2361.1	2607.9	0.8182	7.1090	7.9272	0.001017	8.027		
0.20	60.1	251.5	2358.4	2609.9	0.8321	7.0773	7.9094	0.001017	7.650		
0.21	61.1	255.9	2355.8	2611.7	0.8453	7.0472	7.8925	0.001018	7.307		
0.22	62.2	260.1	2353.3	2613.5	0.8581	7.0184	7.8764	0.001018	6.995		
0.23	63.1	264.2	2350.9	2615.2	0.8702	6.9908	7.8611	0.001019	6.709		
0.24	64.1	268.2	2348.6	2616.8	0.8820	6.9644	7.8464	0.001019	6.447		

Absolute pressure	Temp.	Specific enthalpy (kJ/kg)		1	cific entro (kJ / kg K)	ру	Specific volume (m³/kg)		
(bar) p	$t_s$	$h_f$	$h_{f\!g}$	$h_{g}$	$s_f$	$s_{fg}$	$s_g$	$v_f$	$v_g$
0.25	65.0	272.0	2 346.4	2 618.3	0.893 2	6.939 1	7.8323	0.001020	6.205
0.26	65.9	275.7	2344.2	2619.9	0.904 1	6.9147	7.8188	0.001020	5.980
0.27	66.7	279.2	2342.1	2 621.3	0.9146	6.8912	7.8058	0.001021	5.772
0.28	67.5	282.7	2 340.0	2622.7	0.9248	6.868 5	7.7933	0.001021	5.579
0.29	68.3	286.0	2 338.1	2 624.1	0.9346	6.8466	7.7812	0.001022	5.398
0.30	69.1	289.3	2 336.1	2625.4	0.944 1	6.8254	7.7695	0.001022	5.229
0.32	70.6	295.5	2 332.4	2 628.0	0.9623	6.785 0	7.7474	0.001023	4.922
0.34	72.0	301.5	2 328.9	2630.4	0.9795	6.7470	7.7265	0.001024	4.650
0.36	73.4	307.1	2 325.5	2 632.6	0.9958	6.7111	7.7070	0.001025	4.408
0.38	74.7	312.5	2 322.3	2634.8	1.0113	6.677 1	7.688 4	0.001026	4.190
0.40	75.9	317.7	2319.2	2 636.9	1.026 1	6.6448	7.6709	0.001026	3.993
0.42	77.1	322.6	2316.3	2638.9	1.0402	6.6140	7.6542	0.001027	3.815
0.44	78.2	327.3	2 313.4	2640.7	1.0537	6.5846	7.6383	0.001028	3.652
0.46	79.3	331.9	2310.7	2642.6	1.066 7	6.5564	7.623 1	0.001029	3.503
0.48	80.3	336.3	2308.0	2 644.3	1.079 2	6.5294	7.6086	0.001029	3.367
0.50	81.3	340.6	2 305.4	2 646.0	1.0912	6.5035	7.5947	0.001030	3.240
0.55	83.7	350.6	2 299.3	2 649.9	1.1194	6.4428	7.5623	0.001032	2.964
0.60	86.0	359.9	2 293.6	2 653.6	1.1454	6.3873	7.5327	0.001033	2.732
0.65	88.0	368.6	2288.3	2656.9	1.1696	6.3360	7.5055	0.001035	2.535
0.70	90.0	376.8	2283.3	2660.1	1.1921	6.2883	7.4804	0.001036	2.369
0.75	92.0	384.5	2 278.6	2 663.0	1.213 1	6.243 9	7.4570	0.001037	2.217
0.80	93.5	391.7	2274.0	2665.8	1.2330	6.2022	7.4352	0.001039	2.087
0.85	95.1	398.6	2 269.8	2 668.4	1.2518	3.1629	7.4147	0.001040	1.972
0.90	96.7	405.2	2 265.6	2670.9	1.2696	6.1258	7.3954	0.001041	1.869
0.95	98.2	411.5	2261.7	2673.2	1.2865	6.0906	7.3771	0.001042	1.777
1.0	99.6	417.5	2 257.9	2675.4	1.3027	6.057 1	7.3598	0.001043	1.694
1.1	102.3	428.8	2 250.8	2 679.6	1.333 0	5.9947	7.327 7	0.001046	1.549
1.2	104.8	439.4	2 244.1	2 683.4	1.3609	5.9375	7.2984	0.001048	1.428
1.3	107.1	449.2	2 237.8	2 687.0	1.3868	5.8847	7.2715	0.001050	1.325
1.4	109.3	458.4	2 231.9	2 690.3	1.4109	5.8356	7.246 5	0.001051	1.236
1.5	111.3	467.1	2 226.2	2 693.4	1.4336	5.7898	7.2334	0.001053	1.159
1.6	113.3	475.4	2 220.9	2 696.2	1.455 0	5.7467	7.2017	0.001055	1.091
1.7	115.2	483.2	2 215.7	2 699.0	1.475 2	5.7061	7.1813	0.001056	1.031
1.8	116.9	490.7	2 210.8	2701.5	1.4944	5.6678	7.1622	0.001058	0.977
1.9	118.6	497.8	2 206.1	2704.0	1.5127	5.6314	7.1440	0.001060	0.929

Absolute pressure (bar)	Temp.	Sp	ecific entha	lpy	l	ecific entro (kJ/kg K)	ру	Specific v (m³/k	
p	$t_s$	$h_f$	$h_{f\!g}$	$h_g$	$s_f$	$s_{fg}$	$s_g$	$v_f$	$v_g$
2.0	120.2	504.7	2 201.6	2 706.3	1.530 1	5.5967	7.1268	0.001061	0.885
2.1	121.8	511.3	2197.2	2708.5	1.5468	5.5637	7.1105	0.001062	0.846
2.2	123.3	517.6	2193.0	2710.6	1.562 7	5.532 1	7.0949	0.001064	0.810
2.3	124.7	523.7	2188.9	2712.6	1.5781	5.5019	7.0800	0.001065	0.777
2.4	126.1	529.6	2184.9	2714.5	1.5929	5.4728	7.0657	0.001066	0.746
2.5	127.4	535.3	2 181.0	2716.4	1.607 1	5.444 9	7.0520	0.001068	0.718
2.6	128.7	540.9	2 177.3	2718.2	1.6209	5.4180	7.0389	0.001069	0.693
2.7	129.9	546.2	2 177.6	2719.9	1.6342	5.3920	7.0262	0.001000	0.668
2.8	131.2	551.4	2 170.0	2721.5	1.647 1	5.367 0	7.0202	0.001070	0.646
2.9	132.4	556.5	2 166.6	2721.3	1.6595	5.3427	7.0023	0.001071	0.625
3.0	133.5	561.4	2163.2	2724.7	1.6716	5.3193	6.9909	0.001074	0.606
3.1	134.6	566.2	2159.9	2726.1	1.6834	5.2965	6.9799	0.001075	0.587
3.2	135.7	570.9	2156.7	2727.6	1.6948	5.2744	6.9692	0.001076	0.570
3.3	136.8	575.5	2153.5	2729.0	1.7059	5.2530	6.9589	0.001077	0.554
3.4	137.8	579.9	2150.4	2730.3	1.7168	5.2322	6.9489	0.001078	0.538
3.5	138.8	584.3	2147.4	2731.6	1.7273	5.2119	6.9392	0.001079	0.524
3.6	139.8	588.5	2144.4	2732.9	1.737 6	5.1921	6.9297	0.001080	0.510
3.7	140.8	592.7	2141.4	2734.1	1.7476	5.1729	6.9205	0.001081	0.497
3.8	141.8	596.8	2138.6	2735.3	1.7574	5.1541	6.9116	0.001082	0.486
3.9	142.7	600.8	2135.7	2736.5	1.7670	5.1358	6.9028	0.001083	0.473
4.0	143.6	604.7	2 133.0	2737.6	1.7764	5.1179	6.8943	0.001084	0.462
4.2	145.4	612.3	2127.5	2739.8	1.7945	5.0834	6.8779	0.001086	0.441
4.4	147.1	619.6	2122.3	2741.9	1.8120	5.0503	6.8623	0.001088	0.423
4.6	148.7	626.7	2117.2	2743.9	1.828 7	5.0186	6.8473	0.001089	0.405
4.8	150.3	633.5	2 112.2	2745.7	1.8448	4.988 1	6.8329	0.001091	0.390
5.0	151.8	640.1	2 107.4	2747.5	1.8604	4.9588	6.8192	0.001093	0.375
5.2	153.3	646.5	2 102.7	2749.3	1.8754	4.9306	6.805 9	0.001094	0.361
5.4	154.7	652.8	2 098.1	2 750.9	1.8899	4.9033	6.793 2	0.001096	0.348
5.6	156.2	658.8	2 093.7	2 752.5	1.9040	4.8769	6.7809	0.001098	0.337
5.8	157.5	664.7	2 089.3	2 754.0	1.9176	4.8514	6.769 0	0.001099	0.326
6.0	158.8	670.4	2085.0	2755.5	1.9308	4.8267	6.7575	0.001101	0.315
6.2	160.1	676.0	2080.9	2756.9	1.943 7	4.8027	6.7464	0.001102	0.306
6.4	161.4	681.5	2076.8	2758.2	1.9562	4.7794	6.7356	0.001104	0.297
6.6	162.6	686.8	2072.7	2759.5	1.968 4	4.7568	6.7252	0.001105	0.288
6.8	163.8	692.0	2068.8	2760.8	1.980 2	4.7348	6.7150	0.001107	0.280

Absolute	Temp.	Sp	ecific entha	lpy		ecific entr	ору	Specific v	
pressure	(°C)		(kJ/kg)			$(kJ/kg\ K)$		$(m^3/k)$	g)
(bar)									
p	$t_s$	$h_f$	$h_{fg}$	$h_{g}$	$s_f$	$s_{fg}$	$s_g$	$v_f$	$v_g$
7.0	165.0	697.1	2064.9	2762.0	1.9918	4.7134	6.7052	0.001108	0.273
7.2	166.1	702.0	2061.1	2763.2	2.003 1	4.6925	6.6956	0.001110	0.265
7.4	167.2	706.9	2057.4	2764.3	2.014 1	4.6721	6.6862	0.001111	0.258
7.6	168.3	711.7	2053.7	2765.4	2.0249	4.6522	6.677 1	0.001112	0.252
7.8	169.4	716.3	2050.1	2766.4	2.035 4	4.6328	6.6683	0.001114	0.246
8.0	170.4	720.9	2046.5	2 767.5	2.045 7	4.6139	6.6596	0.001115	0.240
8.2	171.4	725.4	2043.0	2768.5	2.0558	4.5953	6.6511	0.001116	0.235
8.4	172.4	729.9	2039.6	2769.4	2.065 7	4.5772	6.6429	0.001118	0.229
8.6	173.4	734.2	2036.2	2770.4	2.0753	4.5594	6.6348	0.001119	0.224
8.8	174.4	738.5	2032.8	2771.3	2.0848	4.5421	6.6269	0.001120	0.219
9.0	175.4	742.6	2 029.5	2772.1	2.094 1	4.525 0	6.6192	0.001121	0.215
9.2	176.3	746.8	2026.2	2773.0	2.1033	4.5083	6.6116	0.001123	0.210
9.4	177.2	750.8	2023.0	2773.8	2.1122	4.4920	6.6042	0.001124	0.206
9.6	178.1	754.8	2 019.8	2774.6	2.1210	4.4759	6.5969	0.001125	0.202
9.8	179.0	758.7	2016.7	2775.4	2.1297	$4.460\ 1$	6.5898	0.001126	0.198
10.0	179.9	762.6	2 013.6	2776.2	2.1382	4.4446	6.5828	0.001127	0.194
10.5	182.0	772.0	2 005.9	2778.0	2.1588	4.407 1	6.5659	0.001127	0.185
11.0	184.1	781.1	1 998.5	2779.7	2.1786	4.3711	6.5497	0.001133	0.177
11.5	186.0	789.9	1 991.3	2781.3	2.1977	4.3366	6.5342	0.001136	0.170
12.0	188.0	798.4	1 984.3	2782.7	2.216 1	4.3033	6.5194	0.001139	0.163
12.5	189.8	806.7	1 977.4	2 784.1	2.2338	4.2712	6.5050	0.001141	0.157
13.0	191.6	814.7	1970.7	2785.4	2.2510	4.240 3	6.4913	0.001141	0.157
13.5	193.3	822.5	1964.2	2786.6	2.2676	4.2403	6.4779	0.001144	0.131
14.0	195.0	830.1	1 957.7	2787.8	2.2837	4.1814	6.4651	0.001140	0.140
14.5	196.7	837.5	1 951.4	2788.9	2.2993	4.153 3	6.4526	0.001143	0.136
15.0	100.0	0447	10450	2700.0	0.0145	4 100 1	C 440 C	0.001154	0.100
15.0	198.3	844.7	1 945.2	2789.9	2.3145	4.126 1	6.4406	0.001154	0.132
15.5	199.8	851.7	1 939.2	2790.8	2.329 2	4.0996	6.4289	0.001156	0.128
16.0	201.4	858.6	1 933.2	2791.7	2.3436	4.073 9	6.4175	0.001159	0.124
16.5	202.8	865.3	1 927.3	2792.6	2.3576	4.0489	6.4065	0.001161	0.120
17.0	204.3	871.8	1 921.5	2 793.4	2.3713	4.024 5	6.3957	0.001163	0.117
17.5	205.7	878.3	1915.9	2794.1	2.3846	4.0007	6.3853	0.001166	0.113
18.0	207.1	884.6	1910.3	2794.8	2.3976	3.9775	6.3751	0.001168	0.110
18.5	208.4	890.7	1904.7	2795.5	2.4103	3.9548	6.3651	0.001170	0.107
19.0	209.8	896.8	1899.3	2796.1	2.4228	3.9326	6.3554	0.001172	0.105
19.5	211.1	902.8	1 893.9	2796.7	2.4349	3.9110	6.3459	0.001174	0.102

Absolute	Temp.	Sp	ecific entha	ılpy	Spe	ecific entro	ру	Specific v	olume
pressure	(°C)		(kJ/kg)			$(kJ/kg\ K)$		$(m^3/k)$	rg)
(bar)									
p	$t_s$	$h_f$	$h_{f\!g}$	$h_g$	$s_f$	$s_{\it fg}$	$s_g$	$v_f$	$v_g$
20.0	212.4	908.6	1888.6	2797.2	2.4469	3.8898	6.3366	0.001177	0.0995
20.5	213.6	914.3	1883.4	2797.7	2.4585	3.8690	6.3276	0.001179	0.0971
21.0	214.8	920.0	1878.2	2798.2	2.4700	3.8487	6.3187	0.001181	0.0949
21.5	216.1	925.5	1873.1	2798.6	2.481 2	3.8288	6.3100	0.001183	0.0927
22.0	217.2	931.0	1868.1	2799.1	2.4922	3.8093	6.3015	0.001185	0.0907
22.5	218.4	936.3	1863.1	2 799.4	2.503 0	3.790 1	6.293 1	0.001187	0.0887
23.0	219.5	941.6	1858.2	2799.8	2.5136	3.7713	6.2849	0.001189	0.0868
23.5	220.7	946.8	1853.3	2800.1	2.524 1	3.7528	6.2769	0.001191	0.0849
24.0	221.8	951.9	1848.5	2800.4	2.5343	3.7347	6.2690	0.001193	0.0832
24.5	222.9	957.0	1843.7	2800.7	2.544 4	3.7168	6.2612	0.001195	0.0815
25.0	223.9	962.0	1839.0	2 800.9	2.5543	3.6993	6.2536	0.001197	0.0799
25.5	225.0	966.9	1834.3	2801.2	2.5640	3.6821	6.2461	0.001199	0.0783
26.0	226.0	971.7	1829.6	2801.4	2.573 6	3.6651	6.2387	0.001201	0.0769
26.5	227.1	976.5	1825.1	2801.6	2.583 1	3.6484	6.2315	0.001203	0.0754
27.0	228.1	981.2	1820.5	2801.7	2.5924	3.6320	6.2244	0.001205	0.0740
27.5	229.1	985.9	1816.0	2 801.9	2.6016	3.6158	6.2173	0.001207	0.0727
28.0	230.0	990.5	1811.5	2 802.0	2.6106	3.5998	6.2104	0.001209	0.0714
28.5	231.0	995.0	1807.1	2 802.1	2.619 5	3.5841	6.2036	0.001203	0.0711
29.0	232.0	999.5	1802.6	2 802.2	2.628 3	3.5686	6.1969	0.001211	0.0689
29.5	233.0	1 004.0	1798.3	2802.2	2.637 0	3.5533	6.1902	0.001213	0.0677
30.0	233.8	1 008.4	1793.9	2802.3	2.6455	3.5382	6.1837	0.001216	0.0666
30.5	234.7	1 012.7	1789.6	2802.3	2.6539	3.5233	6.1772	0.001218	0.0655
31.0	235.6	1 017.0	1785.4	2802.3	2.6623	3.5087	6.1709	0.001220	0.0645
31.5	236.5	1 021.2	1781.1	2802.3	2.6705	3.4942	6.1647	0.001222	0.0634
32.0	237.4	1 025.4	1 776.9	2802.3	2.6786	3.4799	6.1585	0.001224	0.0624
32.5	238.3	1 029.6	1 772.7	2802.3	2.6866	3.465 7	6.1523	0.001225	0.0615
33.0	239.2	1 033.7	1768.6	2802.3	2.6945	3.4518	6.1463	0.001227	0.0605
33.5	240.0	1 037.8	1764.4	2802.2	2.7023	3.4380	6.1403	0.001229	0.0596
34.0	240.9	1 041.8	1760.3	2802.1	2.7101	3.4244	6.1344	0.001231	0.0587
34.5	241.7	1 045.8	1756.3	2802.1	2.7177	3.4109	6.1286	0.001233	0.0579
35.0	242.5	1 049.8	1752.2	2 802.0	2.7253	3.3976	6.1228	0.001234	0.0570
35.5	243.3	1 053.7	1748.2	2 801.8	2.7327	3.3844	6.1171	0.001236	0.0562
36.0	244.2	1057.6	1744.2	2801.7	2.740 1	3.3714	6.1115	0.001238	0.0554
36.5	245.0	1061.4	1740.2	2801.6	2.747 4	3.3585	6.1059	0.001239	0.0534
37.0	245.7	1 065.2	1736.2	2801.4	2.7547	3.345 8	6.1004	0.001233	0.0540
J1.0	1 210.1	1 000.2	1,00.2	2001.1	2.1011	0.0100	J,100 T	0.001242	0.0000

(bar)			ecific entha (k <b>J</b> /kg)	ıpy		cific entro (kJ / kg K)	ру	$(m^3/k)$	olume eg)
1	$t_s$	$h_f$	$h_{f\!g}$	$h_g$	$s_f$	$s_{\mathit{fg}}$	$s_g$	$v_f$	$v_g$
37.5	246.5	1 069.0	1 732.3	2 801.3	2.7618	3.3332	6.0950	0.001243	0.0531
1	247.3	1072.7	1728.4	2801.1	2.7689	3.3207	6.0896	0.001245	0.0524
	248.1	1076.4	1724.5	2800.9	2.7759	3.3083	6.0842	0.001247	0.0517
1 1	248.8	1 080.1	1720.6	2800.8	2.7829	3.296 1	6.0789	0.001249	0.0511
39.5	249.6	1083.8	1716.8	2800.5	2.7897	3.2840	6.0737	0.001250	0.0504
40.0	250.3	1 087.4	1 712.9	2800.3	2.7965	3.2720	6.0685	0.001252	0.0497
	251.8	1 094.6	1712.3	2 799.9	2.7903	3.2483	6.0582	0.001252	0.0497 $0.0485$
1	253.2	1 101.6	1 697.8	2799.4	2.823 1	3.225 1	6.0482	0.001259	0.0463 $0.0473$
	254.6	1 101.6	1 690.3	2798.8	2.836 0	3.2023	6.0383	0.001259	0.0473
	256.0	1 115.4	1 690.5	2 798.3	2.848 7	3.1799	6.0286	0.001262	0.0461 $0.0451$
11.0	200.0	1110.4	1 002.0	2100.0	2.0407	0.1700	0.020 0	0.001200	0.0401
45.0	257.4	1122.1	1675.6	2797.7	2.8612	3.1579	6.0191	0.001269	0.0440
46.0	258.7	1128.8	1668.3	2797.0	2.8735	3.1362	6.0097	0.001272	0.0430
47.0	260.1	1135.3	1661.1	2796.4	2.8855	3.1149	6.0004	0.001276	0.0421
48.0	261.4	1 141.8	1653.9	2795.7	2.8974	3.0939	5.9913	0.001279	0.0412
49.0	262.6	1148.2	1646.8	2794.9	2.909 1	3.0733	5.9823	0.001282	0.0403
50.0	263.9	1 154.5	1 639.7	2 794.2	2.9206	3.0529	5.9735	0.001286	0.0394
	265.1	1 160.7	1 632.7	2793.4	2.9319	3.0328	5.9648	0.001289	0.0386
	266.4	1 166.8	1 625.7	2792.6	2.943 1	3.0130	5.9561	0.001292	0.0378
	267.6	1 172.9	1618.8	2791.7	2.954 1	2.993 5	5.9476	0.001296	0.0371
	268.7	1 178.9	1611.9	2 790.8	2.965 0	2.974 2	5.9392	0.001299	0.0363
55.0	200.0	11040	1.005.0	0.700.0	0.075.7	0.055.0	5 000 O	0.001000	0.0050
	269.9	1 184.9	1 605.0	2789.9	2.975 7	2.955 2	5.9309	0.001302	0.0356
	271.1	1 190.8	1 598.2	2789.0	2.9863	2.9364	5.9227	0.001306	0.0349
1	272.2	1 196.6	1591.4	2788.0	2.9967	2.9179	5.9146	0.001309	0.0343
	273.3 274.4	1 202.3	1584.7	2787.0	3.0071	2.8995	5.906 6	0.001312	0.0336
59.0	214.4	1 208.0	1 578.0	2 786.0	3.0172	2.8814	5.8986	0.001315	0.0330
60.0	275.5	1213.7	1571.3	2785.0	3.0273	2.8635	5.8908	0.001318	0.0324
61.0	276.6	1219.3	1564.7	2784.0	3.0372	2.8458	5.8830	0.001322	0.0319
	277.7	1224.8	1558.0	2782.9	3.0471	2.8283	5.8753	0.001325	0.0313
63.0	278.7	1230.3	1551.5	2781.8	3.0568	2.8109	5.8677	0.001328	0.0308
64.0	279.8	1235.7	1544.9	2780.6	3.0664	2.7938	5.8601	0.001332	0.0302
65.0	280.8	1 241.1	1538.4	2 779.5	3.075 9	2.7768	5.8527	0.001335	0.0297
	281.8	1 246.5	1531.9	2778.3	3.085 3	2.7600	5.8452	0.001338	0.0292
	282.8	1251.8	1525.4	2777.1	3.0946	2.7433	5.8379	0.001330	0.0287
	283.8	1 257.0	1518.9	2775.9	3.1038	2.7268	5.8306	0.001345	0.0283
1	284.8	1 262.2	1512.5	2774.7	3.1129	2.7105	5.8233	0.001348	0.0278

Absolute	Temp.	Sp	ecific entha	ulpy	_	cific entro	py	Specific v	
pressure	(°C)		(kJ/kg)		(	(kJ/kg K)		$(m^3/k)$	rg)
(bar)	$t_s$	$h_f$	$h_{f\!g}$	$h_g$	$s_f$	$s_{fg}$	$s_g$	$v_f$	$v_g$
70.0	285.8	1 267.4	1 506.0	2 773.5	3.1219	2.6943	5.8162	0.001351	0.0274
71.0	286.7	1272.5	1 499.6	2772.2	3.1308	2.678 2	5.8090	0.001355	0.0269
72.0	287.7	1277.6	1 493.3	2770.9	3.1397	2.6623	5.8020	0.001358	0.0265
73.0	288.6	1 282.7	1 486.9	2769.6	3.1484	2.646 5	5.7949	0.001361	0.0261
74.0	289.6	1 287.7	1 480.5	2768.3	3.157 1	2.6309	5.7880	0.001364	0.0257
75.0	290.5	1 292.7	1474.2	2766.9	3.165 7	2.6153	5.7810	0.001368	0.0253
76.0	291.4	1 297.6	1467.9	2765.5	3.1742	2.5999	5.7742	0.001371	0.0249
77.0	292.3	1 302.5	1461.6	2764.2	3.1827	2.5846	5.7673	0.001374	0.0246
78.0	293.2	1 307.4	1455.3	2762.8	3.1911	2.5695	5.7605	0.001378	0.0242
79.0	294.1	1 312.3	1449.1	2761.3	3.1994	2.5544	5.7538	0.001381	0.0239
80.0	294.9	1 317.1	1442.8	2759.9	3.2076	2.5395	5.7471	0.001384	0.0235
81.0	295.8	1 321.9	1436.6	2758.4	3.2158	2.5246	5.7404	0.001387	0.0232
82.0	296.7	1 326.6	1430.3	2757.0	3.2239	2.5099	5.7338	0.001391	0.0229
83.0	297.5	1 331.4	1424.1	2755.5	3.2320	2.4952	5.7272	0.001394	0.0225
84.0	298.4	1 336.1	1417.9	2754.0	3.2399	2.4807	5.7206	0.001397	0.0222
85.0	299.2	1 340.7	1411.7	2752.5	3.2479	2.4663	5.7141	0.001401	0.0219
86.0	300.1	1 345.4	1405.5	2750.9	3.2557	2.4519	5.7076	0.001404	0.0216
87.0	300.9	1 350.0	1399.3	2749.4	3.2636	2.4376	5.7012	0.001408	0.0213
88.0	301.7	1 354.6	1393.2	2747.8	3.2713	2.4235	5.6948	0.001411	0.0211
89.0	302.5	1 359.2	1387.0	2746.2	3.2790	2.4094	5.6884	0.001414	0.0208
90.0	303.3	1 363.7	1380.9	2744.6	3.2867	2.3953	5.6820	0.001418	0.0205
91.0	304.1	1 368.3	1374.7	2743.0	3.2943	2.3814	5.6757	0.001421	0.0202
92.0	304.9	1 372.8	1368.6	2741.4	3.3018	2.3676	5.6694	0.001425	0.0199
93.0	305.7	1 377.2	1362.5	2739.7	3.3093	2.3538	5.6631	0.001428	0.0197
94.0	306.4	1 381.7	1356.3	2738.0	3.3168	2.3401	5.6568	0.001432	0.0194
95.0	307.2	1 386.1	1350.2	2736.4	3.3242	2.3264	5.6506	0.001435	0.0192
96.0	308.0	1 390.6	1344.1	2734.7	3.3315	2.3129	5.6444	0.001438	0.0189
97.0	308.7	1 395.0	1338.0	2733.0	3.3388	2.2994	5.6382	0.001442	0.0187
98.0	309.4	1 399.3	1331.9	2731.2	3.346 1	2.2859	5.6321	0.001445	0.0185
99.0	310.2	1 403.7	1325.8	2729.5	3.3534	2.2726	5.6259	0.001449	0.0183
100.0	311.1	1 408.0	1319.7	2727.7	3.360 5	2.2593	5.6198	0.001452	0.0181
102.0	312.4	1 416.7	1307.5	2724.2	3.3748	2.2328	5.6076	0.001459	0.0176
104.0	313.8	1425.2	1295.3	2720.5	3.3889	2.2066	5.5955	0.001467	0.0172
106.0	315.3	1 433.7	1 283.1	2716.8	3.4029	2.1806	5.583 5	0.001474	0.0168
108.0	316.6	1 442.2	1270.9	2713.1	3.4167	2.1548	5.5715	0.001481	0.0164

Absolute pressure	Temp. (°C)	Sp	ecific entha (kJ/kg)	lpy		cific entro (kJ/kg K)	ру	Specific ve	
(bar)	$t_s$	$h_f$	$h_{f\!g}$	$h_g$	$s_f$	$s_{fg}$	$s_g$	$v_f$	$v_g$
110.0				2 709.3					
110.0	318.0	1 450.6	1 258.7		3.4304	2.129 1	5.5595	0.001488	0.0160
112.0	319.4	1 458.9	1 246.5	2705.4	3.444 0	2.1036	5.5476	0.001496	0.0157
114.0	320.7	1 467.2	1 234.3	2 701.5	3.4574	2.0783	5.5357	0.001504	0.0153
116.0	322.1	1 475.4	1 222.0	2 697.4	3.4708	2.053 1	5.5239	0.001511	0.0149
118.0	323.4	1 483.6	1 209.7	2 693.3	3.4840	2.028 0	5.5121	0.001519	0.0146
120.0	324.6	1 491.8	1 197.4	2689.2	3.4972	2.0030	5.5002	0.001527	0.0143
122.0	325.9	1 499.9	1185.0	2684.9	3.5102	1.9782	5.4884	0.001535	0.0139
124.0	327.1	1508.0	1172.6	2680.6	3.5232	1.9533	5.4765	0.001543	0.0137
126.0	328.4	1 516.0	1160.1	2676.1	3.5360	1.9286	5.4646	0.001551	0.0134
128.0	329.6	1 524.0	1147.6	2671.6	3.5488	1.9039	5.4527	0.001559	0.0131
130.0	330.8	1 532.0	1 135.0	2 667.0	3.5616	1.8792	5.4408	0.001567	0.0128
132.0	332.0	1540.0	1 122.3	2 662.3	3.5742	1.8546	5.4288	0.001507	0.0128 $0.0125$
	333.2			2662.3 $2657.4$		1.8300		0.001576	0.0123 $0.0123$
134.0		1547.9	1 109.5		3.5868		5.4168		
136.0	334.3	1 555.8	1 096.7	2 652.5	3.5993	1.8053	5.4047	0.001593	0.0120
138.0	335.5	1 563.7	1 083.8	2647.5	3.6118	1.7807	5.3925	0.001602	0.0117
140.0	336.6	1 571.6	1070.7	2642.4	3.6242	1.7560	5.3803	0.001611	0.0115
142.0	337.7	1 579.5	1057.6	2637.1	3.6366	1.7313	5.3679	0.001619	0.0112
144.0	338.8	1 587.4	1044.4	2631.8	3.6490	1.7066	5.3555	0.001629	0.0110
146.0	339.9	1 595.3	1031.0	2626.3	3.6613	1.6818	5.3431	0.001638	0.0108
148.0	341.1	1 603.1	1017.6	2620.7	3.6736	1.6569	5.3305	0.001648	0.0106
150.0	342.1	1611.0	1 004.0	2615.0	3.6859	1.632 0	5.3179	0.001658	0.0103
152.0	343.2	1611.0	990.3	2609.2	3.6981	1.607 0	5.305 1	0.001668	0.0103
154.0	344.2	1626.8	976.5	2603.3	3.7103	1.5819	5.3031 $5.2922$	0.001668	0.0101
156.0	345.3	1634.7	962.6	2597.3	3.7226	1.5567	5.2793	0.001678	0.00991
158.0	346.3	1 642.6	948.5	2591.1	3.7348	1.5314	5.2663	0.001699	0.00951
160.0	347.3	1 650.5	934.3	2584.9	3.747 1	1.5060	5.253 1	0.001710	0.00931
162.0	348.3	1658.5	920.0	2578.5	3.7594	1.4806	5.2399	0.001721	0.00911
164.0	349.3	1 666.5	905.6	2572.1	3.7717	1.4550	5.2267	0.001733	0.00893
166.0	350.3	1674.5	891.0	2 565.5	3.7842	1.4290	5.2132	0.001745	0.00874
168.0	351.3	1 683.0	875.6	2558.6	3.7974		5.1994	0.001757	0.00855
450.0	0500	1 00 -	050.0	0 851 0	0.040-	4.0=+-	- 40	0.001=00	0.0000=
170.0	352.3	1 691.7	859.9	2551.6	3.8107	1.3748	5.1855	0.001769	0.00837
172.0	353.2	1700.4	844.0	2544.4	3.8240	1.3473	5.1713	0.001783	0.00819
174.0	354.2	1709.0	828.1	2537.1	3.8372	1.3198	5.1570	0.001796	0.00801
176.0	355.1	1717.6	811.9	2529.5	3.8504	1.2922	5.1425	0.001810	0.00784
178.0	356.0	1 726.2	795.6	2521.8	3.8635	1.2643	5.1278	0.001825	0.00767

Absolute pressure (bar)	Temp.						ру	Specific v (m³/k	
p	$t_s$	$h_f$	$h_{fg}$	$h_g$	$s_f$	$s_{\it fg}$	$s_g$	$v_f$	$v_g$
180.0	356.9	1734.8	779.1	2 513.9	3.8765	1.2362	5.1128	0.001840	0.00750
182.0	357.8	1743.4	762.3	2505.8	3.8896	1.2079	5.0975	0.001856	0.00733
184.0	358.7	1752.1	745.3	2497.4	3.9028	1.1792	5.0820	0.001872	0.00717
186.0	359.6	1760.9	727.9	2488.8	3.9160	1.1501	5.0661	0.001889	0.00701
188.0	360.5	1 769.7	710.1	2479.8	3.9294	1.1205	5.0498	0.001907	0.00684
190.0	361.4	1778.7	692.0	2470.6	3.9429	1.0903	5.0332	0.001926	0.00668
192.0	362.3	1787.8	673.3	2461.1	3.9566	1.0594	5.0160	0.001946	0.00652
194.0	363.2	1 797.0	654.1	2451.1	3.9706	1.0278	4.9983	0.001967	0.00636
196.0	364.0	1806.6	634.2	2440.7	3.9849	0.9951	4.9800	0.001989	0.00620
198.0	364.8	1816.3	613.5	2429.8	3.9996	0.9614	4.9611	0.002012	0.00604
200.0	365.7	1 826.5	591.9	2 418.4	4.0149	0.9263	4.9412	0.002037	0.00588
202.0	366.5	1837.0	569.2	2 406.2	4.0308	0.8897	4.9204	0.002064	0.00571
204.0	367.3	1848.1	545.1	2 393.3	4.0474	0.8510	4.8984	0.002093	0.00555
206.0	368.2	1859.9	519.5	2 379.4	4.065 1	0.8099	4.8750	0.002125	0.00538
208.0	368.9	1872.5	491.7	2 364.2	4.084 1	0.765 7	4.8498	0.002161	0.00521
210.0	369.8	1886.3	461.3	2 347.6	4.1048	0.7175	4.8223	0.002201	0.00502
212.0	370.6	1901.5	427.4	2 328.9	4.1279	0.6639	4.7917	0.002249	0.00483
214.0	371.3	1919.0	388.4	2 307.4	4.1543	0.6026	4.7569	0.002245	0.00463
216.0	372.1	1939.9	341.6	2 281.6	4.186 1	0.5293	4.7154	0.002379	0.00439
218.0	372.9	1967.2	280.8	2 248.0	4.227 6	0.4346	4.6622	0.002483	0.00412
220.0	373.7	2011 1	184.5	2 105 6	4 904 7	0.005.0	4 570 0	0.002671	0.00373
220.0 221.2	373.7	2 011.1 2 107.4	0.0	2195.6 $2107.4$	4.294 7 4.442 9	0.2852 $0.0$	4.5799 $4.4429$	0.002671	0.00373

TABLE III
Superheated Steam at Various Pressures and Temperatures

$\begin{array}{c} \downarrow p \; (bar) \\ (t_s) \end{array}$	t (°C)	50	100	150	200	250	300	400	500
	$\rightarrow$								
	v	149.1	172.2	195.3	218.4	241.5	264.5	310.7	356.8
0.01	u	2445.4	2516.4	2588.4	2661.6	2736.9	2812.2	2969.0	3132.4
(7.0)	h	2594.5	2688.6	2783.6	2880.0	2978.4	3076.8	3279.7	3489.2
	s	9.242	9.513	9.752	9.967	10.163	10.344	10.671	10.960
	v	29.78	34.42	39.04	48.66	48.28	52.9	62.13	71.36
0.05	u	2444.8	2516.2	2588.4	2661.9	2736.6	2812.6	2969.6	3133.0
(32.9)	h	2593.7	2688.1	2783.4	2879.9	2977.6	3076.7	3279.7	3489.2
	s	8.498	8.770	9.009	9.225	9.421	9.602	9.928	10.218
	v	14.57	17.19	19.51	21.82	24.14	26.44	31.06	35.68
0.1	u	2443.9	2515.5	2587.9	2661.3	2736.0	2812.1	2968.9	3132.3
(45.8)	h	2592.6	2687.5	2783.0	2879.5	2977.3	3076.5	3279.6	3489.1
	s	8.175	8.448	8.688	8.904	9.100	9.281	9.608	9.898
	v		34.18	3.889	43.56	4.821	5.284	6.209	7.134
0.5	u		2511.6	2585.6	2659.9	2735.0	2811.3	2968.5	3132.0
(81.3)	h		2682.5	2780.1	2877.7	2976.0	3075.5	3278.9	3488.7
(81.6)	s		7.695	7.940	8.158	8.356	8.537	8.864	9.155
	v		2.27	2.587	2.900	3.211	3.520	4.138	4.755
0.75	u		2509.2	2584.2	2659.0	2734.4	2810.9	2968.2	3131.8
(92.0)	h		2679.4	2778.2	2876.5	2975.2	3074.9	3278.5	3488.4
(92.0)	s		7.501	7.749	7.969	8.167	8.349	8.677	8.967
	υ		1.696	1.936	2.172	2.406	2.639	3.103	3.565
1.0	u		2506.2	2582.8	2658.1	2733.7	2810.4	2967.9	3131.6
(99.6)	h		2676.2	2776.4	2875.3	2974.3	3074.3	3278.2	3488.1
	s		7.361	7.613	7.834	8.033	8.216	8.544	8.834
	v			1.912	2.146	2.375	2.603	3.062	3.519
1.01325	u			2582.6	2658.0	2733.6	2810.3	2967.8	3131.5
(100)	h			2776.3	2875.2	2974.2	3074.2	3278.1	3488.0
	s			7.828	7.827	8.027	8.209	8.538	8.828
	v			1.285	1.143	1.601	1.757	2.067	2.376
1.5	u			2579.8	2656.2	2732.5	2809.5	2967.3	3131.2
(111.4)	h			2772.6	2872.9	2972.7	3073.1	3277.4	3487.6
			1	1	i .	i contract of the contract of	1	1	1

	<i>t</i> (°C) →	50	100	150	200	250	300	400	500
	υ			0.960	1.080	1.199	1.316	1.549	1.781
2.0	u			2576.9	2654.4	2731.2	2808.6	2966.7	3130.8
(120.2)	h			2768.8	2870.5	2971.0	3071.8	3276.6	3487.1
	s			7.279	7.507	7.709	7.893	8.222	8.513
	υ			0.764	0.862	0.957	1.052	1.238	1.424
2.5	u			2574.7	2655.7	2734.9	2813.8	2973.9	3139.6
(127.4)	h			2764.5	2868.0	2969.6	3070.9	3275.9	3486.5
	s			7.169	7.401	7.604	7.789	8.119	8.410
	υ			0.634	0.716	0.796	0.875	1.031	1.187
3.0	u			2570.8	2650.7	2728.7	2806.7	2965.6	3130.0
(133.5)	h			2761.0	2865.6	2967.6	3069.3	3275.0	3486.1
	s			7.078	7.311	7.517	7.702	8.033	8.325
	υ			0.471	0.534	0.595	0.655	0.773	0.889
4.0	u			2564.5	2646.8	2726.1	2804.8	2964.4	3129.2
(143.6)	h			2752.8	2860.5	2964.2	3066.8	3273.4	3484.9
	s			6.930	7.171	7.379	7.566	7.899	8.191

$\downarrow_{p \; (bar)} \\ (t_s)$	<i>t</i> (°C) →	200	250	300	350	400	450	500	600
	υ	0.425	0.474	0.523	0.570	0.617	0.664	0.711	0.804
5.0	u	2642.9	2723.5	2802.9	2882.6	2963.2	3045.3	3128.4	3299.6
(151.8)	h	2855.4	2960.7	3064.2	3167.7	3271.9	3377.2	3483.9	3701.7
	s	7.059	7.271	7.460	7.633	7.794	7.945	8.087	8.353
	v	0.352	0.394	0.434	0.474	0.514	0.553	0.592	0.670
6.0	u	2638.9	2720.9	2801.0	2881.2	2962.1	3044.2	3127.6	3299.1
(158.8)	h	2850.1	2957.2	3061.6	3165.7	3270.3	3376.0	3482.8	3700.9
	s	6.967	7.182	7.372	7.546	7.708	7.859	8.002	8.267
	v	0.300	0.336	0.371	0.406	0.440	0.473	0.507	0.574
7.0	u	2634.8	2718.2	2799.1	2879.7	2960.9	3043.2	3126.8	3298.5
(165.0)	h	2844.8	2953.6	3059.1	3163.7	3268.7	3374.7	3481.7	3700.2
	s	6.886	7.105	7.298	7.473	7.635	7.787	7.930	8.196
	v	0.261	0.293	0.324	0.354	0.384	0.414	0.443	0.502
8.0	u	2630.6	2715.5	2797.2	2878.2	2959.7	3042.3	3126.0	3297.8
(170.4)	h	2839.3	2950.1	3056.5	3161.7	3267.1	3373.4	3480.6	3699.4
	s	6.816	7.038	7.233	7.409	7.572	7.724	7.867	8.133

$\downarrow p (bar)$	t (°C)	200	250	300	350	400	450	500	600
$(t_s)$	$\iota (C)$	200	250	300	550	400	450	300	600
	υ	0.230	0.260	0.287	0.314	0.341	0.367	0.394	0.446
9.0	u	2626.3	2712.7	2795.2	2876.7	2958.5	3041.3	3125.2	3297.3
(175.4)	h	2833.6	2946.3	3053.8	3159.7	3265.5	3372.1	3479.6	3698.6
	s	6.752	6.979	7.175	7.352	7.516	7.668	7.812	8.078
	v	0.206	0.233	0.258	0.282	0.307	0.330	0.354	0.401
10.0	u	2621.9	2709.9	2793.2	2875.2	2957.3	3040.3	3124.4	3296.8
(179.9)	h	2827.9	2942.6	3051.2	3157.8	3263.9	3370.7	3478.5	3697.9
	s	6.694	6.925	7.123	7.301	7.465	7.618	7.762	8.029
	v	0.132	0.152	0.169	0.187	0.203	0.219	0.235	0.267
15.0	u	2598.8	2695.3	2783.1	2867.6	2951.3	3035.3	3120.3	3293.9
(198.3)	h	2796.8	2923.3	3037.6	3147.5	3255.8	3364.2	3473.1	3694.0
	s	6.455	6.709	6.918	7.102	7.269	7.424	7.570	7.839
	v		0.111	0.125	0.139	0.151	0.163	0.176	0.200
20.0	u		2679.6	2772.6	2859.8	2945.2	3030.5	3116.2	3290.9
(212.4)	h		2902.5	3023.5	3137.0	3247.6	3357.5	3467.6	3690.1
	s		6.545	6.766	6.956	7.127	7.285	7.432	7.702
	v		0.0870	0.0989	0.109	0.120	0.130	0.140	0.159
25	u		2662.6	2761.6	2851.9	2939.1	3025.5	3112.1	3288.0
(223.9)	h		2880.1	3008.8	3126.3	3239.3	3350.8	3462.1	3686.3
	s		6.408	6.644	6.840	7.015	7.175	7.323	7.596
	v		0.0706	0.0811	0.0905	0.0994	0.108	0.116	0.132
30	u		2644.0	2750.1	2843.7	2932.8	3020.4	3108.0	3285.0
(233.8)	h		2855.8	2993.5	3115.3	3230.9	3344.0	3456.5	3682.3
	s		6.287	6.539	6.743	6.921	7.083	7.234	7.509
	v			0.0588	0.0664	0.0734	0.080	0.0864	0.0989
40	u			2725.3	2826.7	2919.9	3010.2	3099.5	3279.1
(250.4)	h			2960.7	3092.5	3213.6	3330.3	3445.3	3674.4
	s			6.362	6.582	6.769	6.936	7.090	7.369
	v			0.0453	0.0519	0.0578	0.0633	0.0686	0.0787
50	u			2698.0	2808.7	2906.6	2999.7	3091.0	3273.0
(263.9)	h			2924.5	3068.4	3195.7	3316.2	3433.8	3666.5
	s			6.208	6.449	6.646	6.819	6.976	7.259

$\downarrow p (bar)$	t (°C)	200	250	300	350	400	450	500	600
$(t_s)$	$\rightarrow$								
	υ			0.0362	0.0422	0.0474	0.0521	0.0567	0.0653
60	u			2667.2	2789.6	2892.9	2988.9	3082.2	3266.9
(275.5)	h			2884.2	3043.0	3177.2	3301.8	3422.2	3658.4
	s			6.067	6.333	6.541	6.719	6.880	7.168
	υ			0.0295	0.0352	0.0399	0.0442	0.0481	0.0557
70	u			2632.2	2769.4	2878.6	2978.0	3073.4	3260.7
(285.8)	h			2838.4	3016.0	3158.1	3287.1	3410.3	3650.3
	s			5.931	6.228	6.448	6.633	6.798	7.089
									i
$\downarrow p (bar)$	t (°C)	350	375	400	450	500	550	600	700
$(t_s)$	$\rightarrow$								
80	υ	0.02995	0.03222	0.03432	0.03817	0.04175	0.04516	0.04845	0.05481
(004.0)	,	2007.0	00001	0100.0	0050.0	00000	0501.0	00400	0000 4

$\downarrow p (bar)$	t (°C)	350	375	400	450	500	550	600	700
$(t_s)$	$\rightarrow$								
80	v	0.02995	0.03222	0.03432	0.03817	0.04175	0.04516	0.04845	0.05481
(294.9)	h	2987.3	3066.1	3138.3	3272.0	3398.3	3521.0	3642.0	3882.4
	s	6.130	6.254	6.363	6.555	6.724	6.878	7.021	7.281
90	v	0.0258	0.02796	0.02993	0.03350	0.03677	0.03987	0.04285	0.04857
(303.3)	h	2956.6	3041.3	3117.8	3256.6	3386.1	3511.0	3633.7	3876.5
	s	6.036	6.169	6.285	6.484	6.658	6.814	6.959	7.222
100	v	0.02242	0.02453	0.02641	0.02975	0.03279	0.03564	0.03837	0.04358
(311.0)	h	2923.4	3015.4	3096.5	3240.9	3373.7	3500.9	3625.3	3870.5
	s	5.944	6.089	6.212	6.419	6.597	6.756	6.903	7.169
110	v	0.01961	0.02169	0.02351	0.02668	0.02952	0.03217	0.03470	0.03950
(318.0)	h	2887.3	2988.2	3074.3	3224.7	3361.0	3490.7	3616.9	3864.5
	s	5.853	6.011	6.142	6.358	6.540	6.703	6.851	7.120
120	v	0.01721	0.01931	0.02108	0.02412	0.02680	0.02929	0.03164	0.03610
(324.6)	h	2847.7	2958.9	3051.3	3208.2	3348.2	3480.4	3608.3	3858.4
( )	s	5.760	5.935	6.075	6.300	6.487	6.653	6.804	7.075
130	v	0.01511	0.01725	0.01900	0.02194	0.0245	0.02684	0.02905	0.03322
(330.8)	h	2803.3	2927.9	3027.2	3191.3	3335.2	3469.9	3599.7	3852.3
	s	5.663	5.859	6.009	6.245	6.437	6.606	6.759	7.033
140	v	0.01322	0.01546	0.01722	0.02007	0.02252	0.02474	0.02683	0.03075
(336.6)	h	2752.6	2894.5	3001.9	3174.0	3322.0	3459.3	3591.1	3846.2
(33313)	s	5.559	5.782	5.945	6.192	6.390	6.562	6.712	6.994
150	v	0.01145	0.01388	0.01565	0.01845	0.02080	0.02293	0.02491	0.02861
(342.1)	h	2692.4	2858.4	2975.5	3156.2	3308.6	3448.6	3582.3	3840.1
(312.1)	s	5.442	5.703	5.881	6.140	6.344	6.520	6.679	6.957

$\downarrow p \ (bar) \\ (t_s)$	<i>t</i> (°C) →	350	375	400	450	500	550	600	700
160	v	0.00975	0.01245	0.01426	0.01701	0.01930	0.02134	0.02323	0.02674
(347.3)	h	2615.7	2818.9	2947.6	3138.0	3294.9	3437.8	3573.5	3833.9
	s	5.302	5.622	5.188	6.091	6.301	6.480	6.640	6.922
170	v		0.01117	0.01302	0.01575	0.01797	0.01993	0.02174	0.02509
(352.3)	h		2776.8	2918.2	3119.3	3281.1	3426.9	3564.6	3827.7
	s		5.539	5.754	6.042	6.259	6.442	6.604	6.889
180	v		0.00996	0.01190	0.01462	0.01678	0.01868	0.02042	0.02362
(356.9)	h		2727.9	2887.0	3100.1	3267.0	3415.9	3555.6	3821.5
	s		5.448	5.689	5.995	6.218	6.405	6.570	6.858
190	v		0.00881	0.01088	0.01361	0.01572	0.01756	0.01924	0.02231
(361.4)	h		2671.3	2853.8	3080.4	3252.7	3404.7	3546.6	3815.3
	s		5.346	5.622	5.948	6.179	6.369	6.537	6.828
200	v		0.00767	0.00994	0.01269	0.9477	0.01655	0.01818	0.02113
(365.7)	h		2602.5	2818.1	3060.1	3238.2	3393.5	3537.6	3809.0
	s		5.227	5.554	5.902	6.140	6.335	6.505	6.799
210	v		0.00645	0.00907	0.01186	0.01390	0.01564	0.01722	0.02006
(369.8)	h		2511.0	2779.6	3039.3	3223.5	3382.1	3528.4	3802.8
	s		5.075	5.483	5.856	6.103	6.301	6.474	6.772
220	v		0.00482	0.00825	0.01110	0.01312	0.01481	0.01634	0.01909
(373.7)	h		2345.1	2737.6	3017.9	3208.6	3370.6	3519.2	3796.5
	s		4.810	5.407	5.811	6.066	6.269	6.444	6.745

TABLE IV Supercritical Steam

					ercritica					
p(bar)	t (°C)	350	375	400	425	450	500	600	700	800
	$\rightarrow$	550	0,0	100	120	100	000	000	700	
230	υ	0.00162	0.00221	0.00748	0.00915	0.01040	0.01239	0.01554	0.01821	0.02063
250	$\begin{pmatrix} v \\ h \end{pmatrix}$	1632.8	1912.2	2691.2	2869.2	2995.8	3193.4	3510.0	3790.2	4056.2
		3.137	4.137	5.327	5.587	5.765	6.030	6.415	6.719	6.980
	s	5.157	4.157	0.521	0.001	5.765	0.050	0.410	0.719	0.900
250	υ	0.00160	0.00197	0.00600	0.00788	0.00916	0.01112	0.01414	0.01665	0.01891
	h	1623.5	1848.0	2580.2	2806.3	2949.7	3162.4	3491.4	3775.5	4047.1
	s	3.680	4.032	5.142	5.472	5.674	5.959	6.360	6.671	6.934
300	v	0.00155	0.00179	0.00279	0.00530	0.00673	0.00868	0.01145	0.01366	0.01562
	h	1608.5	1791.5	2151.1	2614.2	2821.4	3081.1	3443.9	3745.6	4024.2
	s	3.643	3.930	4.473	5.150	5.442	5.790	6.233	6.561	6.833
350	v	0.00152	0.00110	0.00210	0.00343	0.00496	0.00693	0.00953	0.01153	0.01328
	h	1597.1	1762.4	1987.6	2373.4	2672.4	2994.4	3395.5	3713.5	4001.5
	s	3.612	3.872	4.213	4.775	5.196	5.628	6.118	6.463	6.745
400	v	0.00149	0.00164	0.00191	0.00253	0.00369	0.00562	0.00809	0.00994	0.01152
	h	1588.3	1742.8	1930.9	2198.1	2512.8	2903.3	3346.4	3681.2	3978.7
	s	3.586	3.829	4.113	4.503	4.946	5.470	6.011	6.375	6.666
500	v	0.00144	0.00156	0.00173	0.00201	0.00249	0.00389	0.00611	0.00773	0.00908
	h	1575.3	1716.6	1874.6	2060.0	2284.0	2720.1	3247.6	3616.8	3933.6
	s	3.542	3.764	4.003	4.273	4.588	5.173	5.818	6.219	6.529
600		0.00140	0.00150	0.00163	0.00182	0.00209	0.00296	0.00483	0.00627	0.00746
600	$\begin{array}{c c} v \\ h \end{array}$	1566.4	1699.5	1843.4	2001.7	2179.0	2567.9	3151.2	3553.5	3889.1
		3.505	3.764	3.932	4.163	4.412	4.932	5.645	6.082	6.411
	s	5.505	5.704	5.952	4.105	4.412	4.952	0.040	0.062	0.411
700	v	0.00137	0.00146	0.00157	0.00171	0.00189	0.00247	0.00398	0.00526	0.00632
	h	1560.4	1687.7	1822.8	1967.2	2122.7	2463.2	3061.7	3492.4	3845.7
	s	3.473	3.673	3.877	4.088	4.307	4.762	5.492	5.961	6.307
800	υ	0.00135	0.00142	0.00152	0.00163	0.00177	0.00219	0.00339	0.00452	0.00548
	h	1556.4	1679.4	1808.3	1943.9	2086.9	2394.0	2982.7	3434.6	3803.8
	s	3.444	3.638	3.833	4.031	4.232	4.642	5.360	5.851	6.213
900	v	0.00133	0.00139	0.00147	0.00157	0.00169	0.00201	0.00297	0.00397	0.00484
	h	1553.9	1673.4	1797.7	1927.2	2062.0	2346.7	2915.6	3381.1	3763.8
	s	3.419	3.607	3.795	3.984	4.174	4.554	5.247	5.753	6.128
4000		0.04000	0.0010-	0.007.11	0.00170	0.001.00	0.00100		0.000	
1000	υ	0.01308	0.00137	0.00144	0.00152	0.00163	0.00189	0.00267	0.00355	0.00434
	h	1552.7	1669.4	1790.0	1914.8	2043.8	2312.8	2859.8	3332.3	3726.1
	S	3.396	3.579	3.762	3.944	4.126	4.485	5.151	5.664	6.050

## 736 Tables in SI Units

**TABLE A-10** Properties of Saturated Refrigerant 134a (Liquid–Vapor): Temperature Table

		Specific m <sup>3</sup> /l			Energy /kg		Enthalpy kJ/kg			ropy g·K	
Temp. °C	Press.	Sat. Liquid $v_{\rm f} \times 10^3$	Sat. Vapor $v_{\rm g}$	Sat. Liquid $u_{\rm f}$	Sat. Vapor u <sub>g</sub>	Sat. Liquid $h_{\rm f}$	Evap. $h_{\mathrm{fg}}$	Sat. Vapor $h_{\rm g}$	Sat. Liquid $s_{\rm f}$	Sat. Vapor	Temp.
-40	0.5164	0.7055	0.3569	-0.04	204.45	0.00	222.88	222.88	0.0000	0.9560	-40
-36	0.6332	0.7113	0.2947	4.68	206.73	4.73	220.67	225.40	0.0201	0.9506	-36
-32	0.7704	0.7172	0.2451	9.47	209.01	9.52	218.37	227.90	0.0401	0.9456	-32
-28	0.9305	0.7233	0.2052	14.31	211.29	14.37	216.01	230.38	0.0600	0.9411	-28
-26	1.0199	0.7265	0.1882	16.75	212.43	16.82	214.80	231.62	0.0699	0.9390	-26
-24	1.1160	0.7296	0.1728	19.21	213.57	19.29	213.57	232.85	0.0798	0.9370	-24
-22	1.2192	0.7328	0.1590	21.68	214.70	21.77	212.32	234.08	0.0897	0.9351	-22
-20	1.3299	0.7361	0.1464	24.17	215.84	24.26	211.05	235.31	0.0996	0.9332	-20
-18	1.4483	0.7395	0.1350	26.67	216.97	26.77	209.76	236.53	0.1094	0.9315	-18
-16	1.5748	0.7428	0.1247	29.18	218.10	29.30	208.45	237.74	0.1192	0.9298	-16
-12	1.8540	0.7498	0.1068	34.25	220.36	34.39	205.77	240.15	0.1388	0.9267	-12
-8	2.1704	0.7569	0.0919	39.38	222.60	39.54	203.00	242.54	0.1583	0.9239	-8
-4	2.5274	0.7644	0.0794	44.56	224.84	44.75	200.15	244.90	0.1777	0.9213	-4
0	2.9282	0.7721	0.0689	49.79	227.06	50.02	197.21	247.23	0.1970	0.9190	0
4	3.3765	0.7801	0.0600	55.08	229.27	55.35	194.19	249.53	0.2162	0.9169	4
8	3.8756	0.7884	0.0525	60.43	231.46	60.73	191.07	251.80	0.2354	0.9150	8
12	4.4294	0.7971	0.0460	65.83	233.63	66.18	187.85	254.03	0.2545	0.9132	12
16	5.0416	0.8062	0.0405	71.29	235.78	71.69	184.52	256.22	0.2735	0.9116	16
20	5.7160	0.8157	0.0358	76.80	237.91	77.26	181.09	258.36	0.2924	0.9102	20
24	6.4566	0.8257	0.0317	82.37	240.01	82.90	177.55	260.45	0.3113	0.9089	24
26	6.8530	0.8309	0.0298	85.18	241.05	85.75	175.73	261.48	0.3208	0.9082	26
28	7.2675	0.8362	0.0281	88.00	242.08	88.61	173.89	262.50	0.3302	0.9076	28
30	7.7006	0.8417	0.0265	90.84	243.10	91.49	172.00	263.50	0.3396	0.9070	30
32	8.1528	0.8473	0.0250	93.70	244.12	94.39	170.09	264.48	0.3490	0.9064	32
34	8.6247	0.8530	0.0236	96.58	245.12	97.31	168.14	265.45	0.3584	0.9058	34
36	9.1168	0.8590	0.0223	99.47	246.11	100.25	166.15	266.40	0.3678	0.9053	36
38	9.6298	0.8651	0.0210	102.38	247.09	103.21	164.12	267.33	0.3772	0.9047	38
40	10.164	0.8714	0.0199	105.30	248.06	106.19	162.05	268.24	0.3866	0.9041	40
42	10.720	0.8780	0.0188	108.25	249.02	109.19	159.94	269.14	0.3960	0.9035	42
44	11.299	0.8847	0.0177	111.22	249.96	112.22	157.79	270.01	0.4054	0.9030	44
48	12.526	0.8989	0.0159	117.22	251.79	118.35	153.33	271.68	0.4243	0.9017	48
52	13.851	0.9142	0.0142	123.31	253.55	124.58	148.66	273.24	0.4432	0.9004	52
56	15.278	0.9308	0.0127	129.51	255.23	130.93	143.75	274.68	0.4622	0.8990	56
60	16.813	0.9488	0.0114	135.82	256.81	137.42	138.57	275.99	0.4814	0.8973	60
70	21.162	1.0027	0.0086	152.22	260.15	154.34	124.08	278.43	0.5302	0.8918	70
80	26.324	1.0766	0.0064	169.88	262.14	172.71	106.41	279.12	0.5814	0.8827	80
90	32.435	1.1949	0.0046	189.82	261.34	193.69	82.63	276.32	0.6380	0.8655	90
100	39.742	1.5443	0.0027	218.60	248.49	224.74	34.40	259.13	0.7196	0.8117	100

Source: Tables A-10 through A-12 are calculated based on equations from D. P. Wilson and R. S. Basu, "Thermodynamic Properties of a New Stratospherically Safe Working Fluid—Refrigerant 134a," ASHRAE Trans., Vol. 94, Pt. 2, 1988, pp. 2095–2118.

 TABLE A-11
 Properties of Saturated Refrigerant 134a (Liquid–Vapor): Pressure Table

		Specific Volume m³/kg			Energy 'kg	1 /	Enthalpy kJ/kg		Enti kJ/k		
							KJ/Kg	I		- I	
		Sat.	Sat.	Sat.	Sat.	Sat.		Sat.	Sat.	Sat.	
Press.	Temp.	Liquid	Vapor	Liquid	Vapor	Liquid	Evap.	Vapor	Liquid	Vapor	Press.
bar	°C	$v_{\rm f}  imes 10^3$	$v_{\mathrm{g}}$	$u_{ m f}$	$u_{\mathrm{g}}$	$h_{ m f}$	$h_{ m fg}$	$h_{ m g}$	$s_{ m f}$	$s_{\mathrm{g}}$	bar
0.6	-37.07	0.7097	0.3100	3.41	206.12	3.46	221.27	224.72	0.0147	0.9520	0.6
0.8	-31.21	0.7184	0.2366	10.41	209.46	10.47	217.92	228.39	0.0440	0.9447	0.8
1.0	-26.43	0.7258	0.1917	16.22	212.18	16.29	215.06	231.35	0.0678	0.9395	1.0
1.2	-22.36	0.7323	0.1614	21.23	214.50	21.32	212.54	233.86	0.0879	0.9354	1.2
1.4	-18.80	0.7381	0.1395	25.66	216.52	25.77	210.27	236.04	0.1055	0.9322	1.4
1.6	-15.62	0.7435	0.1229	29.66	218.32	29.78	208.19	237.97	0.1211	0.9295	1.6
1.8	-12.73	0.7485	0.1098	33.31	219.94	33.45	206.26	239.71	0.1352	0.9273	1.8
2.0	-10.09	0.7532	0.0993	36.69	221.43	36.84	204.46	241.30	0.1481	0.9253	2.0
2.4	-5.37	0.7618	0.0834	42.77	224.07	42.95	201.14	244.09	0.1710	0.9222	2.4
2.8	-1.23	0.7697	0.0719	48.18	226.38	48.39	198.13	246.52	0.1911	0.9197	2.8
3.2	2.48	0.7770	0.0632	53.06	228.43	53.31	195.35	248.66	0.2089	0.9177	3.2
3.6	5.84	0.7839	0.0564	57.54	230.28	57.82	192.76	250.58	0.2251	0.9160	3.6
4.0	8.93	0.7904	0.0509	61.69	231.97	62.00	190.32	252.32	0.2399	0.9145	4.0
5.0	15.74	0.8056	0.0409	70.93	235.64	71.33	184.74	256.07	0.2723	0.9117	5.0
6.0	21.58	0.8196	0.0341	78.99	238.74	79.48	179.71	259.19	0.2999	0.9097	6.0
7.0	26.72	0.8328	0.0292	86.19	241.42	86.78	175.07	261.85	0.3242	0.9080	7.0
8.0	31.33	0.8454	0.0255	92.75	243.78	93.42	170.73	264.15	0.3459	0.9066	8.0
9.0	35.53	0.8576	0.0226	98.79	245.88	99.56	166.62	266.18	0.3656	0.9054	9.0
10.0	39.39	0.8695	0.0202	104.42	247.77	105.29	162.68	267.97	0.3838	0.9043	10.0
12.0	46.32	0.8928	0.0166	114.69	251.03	115.76	155.23	270.99	0.4164	0.9023	12.0
14.0	52.43	0.9159	0.0140	123.98	253.74	125.26	148.14	273.40	0.4453	0.9003	14.0
16.0	57.92	0.9392	0.0121	132.52	256.00	134.02	141.31	275.33	0.4714	0.8982	16.0
18.0	62.91	0.9631	0.0105	140.49	257.88	142.22	134.60	276.83	0.4954	0.8959	18.0
20.0	67.49	0.9878	0.0093	148.02	259.41	149.99	127.95	277.94	0.5178	0.8934	20.0
25.0	77.59	1.0562	0.0069	165.48	261.84	168.12	111.06	279.17	0.5687	0.8854	25.0
30.0	86.22	1.1416	0.0053	181.88	262.16	185.30	92.71	278.01	0.6156	0.8735	30.0

**TABLE A-12** Properties of Superheated Refrigerant 134a Vapor

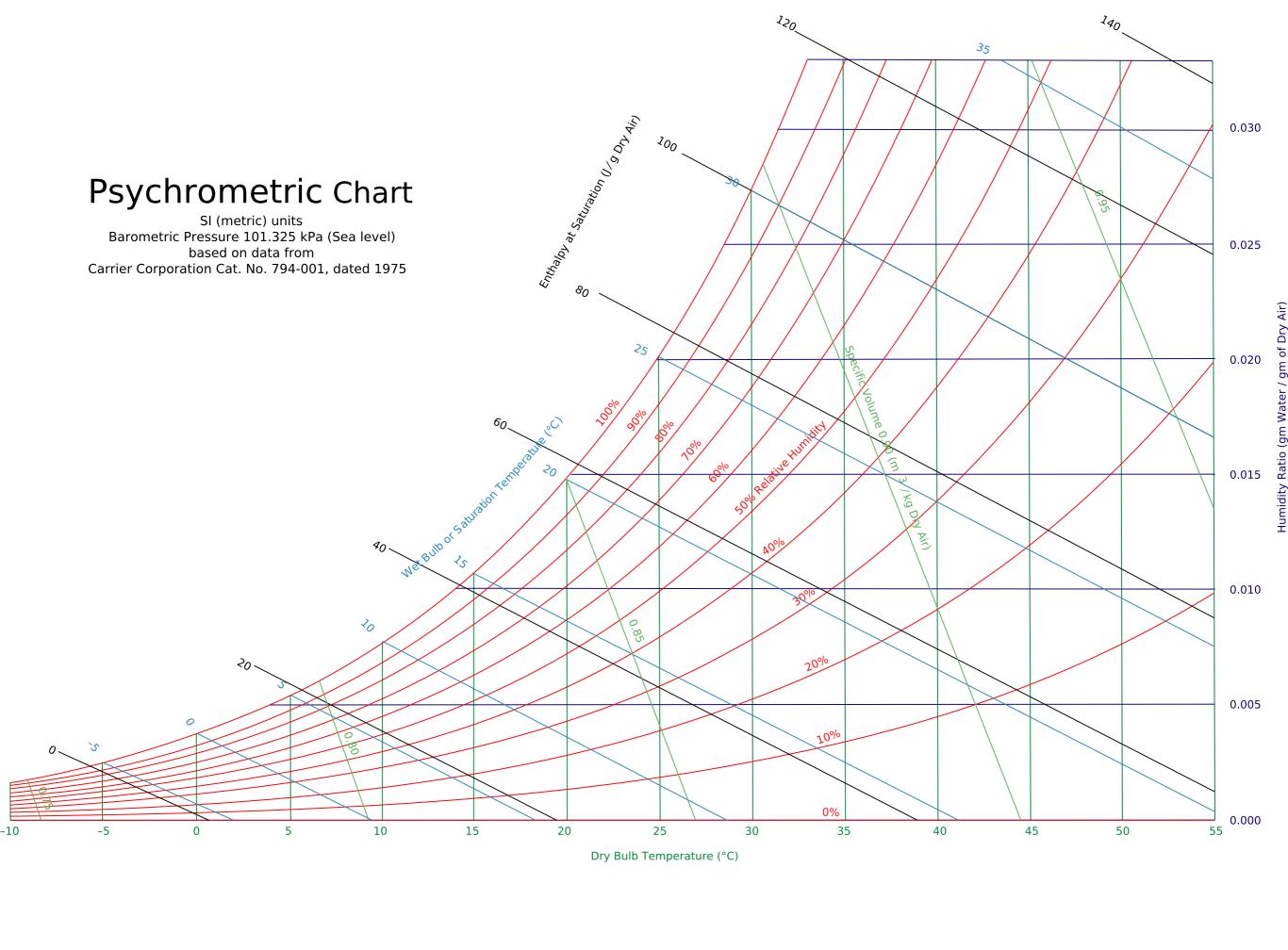
IADL	E A-12 P	roperties (	or Superin	aleu Keirig	gerant 134a	vapoi			
$^{T}_{^{\circ}\mathrm{C}}$	$\frac{v}{m^3/kg}$	и kJ/kg	<i>h</i> kJ/kg	s kJ/kg · K		$\frac{v}{m^3/kg}$	и kJ/kg	<i>h</i> kJ/kg	s kJ/kg · K
		0.6  bar = 0.6  bar = 0.6  bar		'a			$1.0 \text{ bar} = \frac{1}{r_{\text{sat}}} = -26$	0.10 MPa 5.43°C)	
Sat.	0.31003	206.12	224.72	0.9520		0.19170	212.18	231.35	0.9395
-20	0.33536	217.86	237.98	1.0062		0.19770	216.77	236.54	0.9602
-10	0.34992	224.97	245.96	1.0371		0.20686	224.01	244.70	0.9918
0	0.36433	232.24	254.10	1.0675		0.21587	231.41	252.99	1.0227
10	0.37861	239.69	262.41	1.0973		0.22473	238.96	261.43	1.0531
20	0.39279	247.32	270.89	1.1267		0.23349	246.67	270.02	1.0829
30	0.40688	255.12	279.53	1.1557		0.24216	254.54	278.76	1.1122
40	0.42091	263.10	288.35	1.1844		0.25076	262.58	287.66	1.1411
50	0.43487	271.25	297.34	1.2126		0.25930	270.79	296.72	1.1696
60	0.44879	279.58	306.51	1.2405		0.26779	279.16	305.94	1.1977
70	0.46266	288.08	315.84	1.2681		0.27623	287.70	315.32	1.2254
80	0.47650	296.75	325.34	1.2954		0.28464	296.40	324.87	1.2528
90	0.49031	305.58	335.00	1.3224		0.29302	305.27	334.57	1.2799
		1.4 bar =	- 0.14 MB				1 9 har —	0.18 MPa	
		$T_{\text{sat}} = -1$		а			$T_{\rm sat} = -12$		
Sat10 0	0.13945 0.14549 0.15219	216.52 223.03 230.55	236.04 243.40 251.86	0.9322 0.9606 0.9922		0.10983 0.11135 0.11678	219.94 222.02 229.67	239.71 242.06 250.69	0.9273 0.9362 0.9684
10	0.15875	238.21	260.43	1.0230		0.12207	237.44	259.41	0.9998
20	0.16520	246.01	269.13	1.0532		0.12723	245.33	268.23	1.0304
30	0.17155	253.96	277.97	1.0828		0.13230	253.36	277.17	1.0604
40	0.17783	262.06	286.96	1.1120		0.13730	261.53	286.24	1.0898
50	0.18404	270.32	296.09	1.1407		0.14222	269.85	295.45	1.1187
60	0.19020	278.74	305.37	1.1690		0.14710	278.31	304.79	1.1472
70	0.19633	287.32	314.80	1.1969		0.15193	286.93	314.28	1.1753
80	0.20241	296.06	324.39	1.2244		0.15672	295.71	323.92	1.2030
90	0.20846	304.95	334.14	1.2516		0.16148	304.63	333.70	1.2303
100	0.21449	314.01	344.04	1.2785		0.16622	313.72	343.63	1.2573
		$2.0 \text{ bar} = (T_{\text{sat}} = -1)$		a			$2.4 \text{ bar} = T_{\text{sat}} = -5$	0.24 MPa .37°C)	
Sat10 0	0.09933 0.09938 0.10438	221.43 221.50 229.23	241.30 241.38 250.10	0.9253 0.9256 0.9582		0.08343	224.07 228.31	244.09 248.89	0.9222
10	0.10922	237.05	258.89	0.9898		0.08993	236.26	257.84	0.9721
20	0.11394	244.99	267.78	1.0206		0.09399	244.30	266.85	1.0034
30	0.11856	253.06	276.77	1.0508		0.09794	252.45	275.95	1.0339
40	0.12311	261.26	285.88	1.0804		0.10181	260.72	285.16	1.0637
50	0.12758	269.61	295.12	1.1094		0.10562	269.12	294.47	1.0930
60	0.13201	278.10	304.50	1.1380		0.10937	277.67	303.91	1.1218
70	0.13639	286.74	314.02	1.1661		0.11307	286.35	313.49	1.1501
80	0.14073	295.53	323.68	1.1939		0.11674	295.18	323.19	1.1780
90	0.14504	304.47	333.48	1.2212		0.12037	304.15	333.04	1.2055
100	0.14932	313.57	343.43	1.2483		0.12398	313.27	343.03	1.2326

 TABLE A-12 (Continued)

IABL	E A-12 (	Continuea	)					
<i>T</i> °C	v m³/kg	u kJ/kg	<i>h</i> kJ/kg	s kJ/kg · K	v m³/kg	и kJ/kg	<i>h</i> kJ/kg	s kJ/kg · K
	p =	$= 2.8 \text{ bar} = $ $(T_{\text{sat}} = -$	= 0.28 MP 1.23°C)	a		$3.2 \text{ bar} = (T_{\text{sat}} = 2.4)$		
Sat.	0.07193	226.38	246.52	0.9197	0.06322	228.43	248.66	0.9177
0 10	0.07240 0.07613	227.37 235.44	247.64 256.76	0.9238 0.9566	0.06576	234.61	255.65	0.9427
20	0.07972	243.59	265.91	0.9883	0.06901	242.87	264.95	0.9749
30 40	0.08320 0.08660	251.83 260.17	275.12 284.42	1.0192 1.0494	0.07214 0.07518	251.19 259.61	274.28 283.67	1.0062 1.0367
50	0.08992	268.64	293.81	1.0789	0.07815	268.14	293.15	1.0665
60	0.09319	277.23	303.32	1.1079	0.08106	276.79	302.72	1.0957
70	0.09641	285.96	312.95	1.1364	0.08392	285.56	312.41	1.1243
80 90	0.09960 0.10275	294.82 303.83	322.71 332.60	1.1644 1.1920	0.08674 0.08953	294.46 303.50	322.22 332.15	1.1525 1.1802
100	0.10587	312.98	342.62	1.2193	0.09229	312.68	342.21	1.2076
110 120	0.10897 0.11205	322.27 331.71	352.78 363.08	1.2461 1.2727	0.09503 0.09774	322.00 331.45	352.40 362.73	1.2345 1.2611
		4.0 bar =	= 0.40 MF	<u>a</u>	p =	5.0 bar =	0.50 MPa	<u> </u>
		$(T_{\rm sat}=8$				$T_{\rm sat} = 15.$		
Sat.	0.05089	231.97	252.32	0.9145	0.04086	235.64	256.07	0.9117
10 20	0.05119 0.05397	232.87 241.37	253.35 262.96	0.9182 0.9515	0.04188	239.40	260.34	0.9264
30	0.05662	249.89	272.54	0.9837	0.04416	248.20	270.28	0.9597
40	0.05917	258.47	282.14	1.0148	0.04633	256.99	280.16	0.9918
50 60	0.06164 0.06405	267.13 275.89	291.79 301.51	1.0452 1.0748	0.04842 0.05043	265.83 274.73	290.04 299.95	1.0229 1.0531
70	0.06403	284.75	311.32	1.1038	0.05240	283.72	309.92	1.0331
80	0.06873	293.73	321.23	1.1322	0.05432	292.80	319.96	1.1114
90	0.07102	302.84	331.25	1.1602	0.05620	302.00	330.10	1.1397
100 110	0.07327 0.07550	312.07 321.44	341.38 351.64	1.1878 1.2149	0.05805 0.05988	311.31 320.74	340.33 350.68	1.1675 1.1949
120	0.07771	330.94	362.03	1.2417	0.06168	330.30	361.14	1.2218
130	0.07991	340.58	372.54	1.2681	0.06347	339.98	371.72	1.2484
140	0.08208	350.35	383.18	1.2941	0.06524	349.79	382.42	1.2746
		6.0 bar =	= 0.60 MF			7.0 bar =	0.70 MPa	
	Ρ	$(T_{\rm sat}=2)$		u		$T_{\rm sat} = 26.$		
Sat.	0.03408	238.74	259.19	0.9097	0.02918	241.42	261.85	0.9080
30	0.03581	246.41	267.89	0.9388	0.02979	244.51	265.37	0.9197
40 50	0.03774 0.03958	255.45 264.48	278.09 288.23	0.9719 1.0037	0.03157 0.03324	253.83 263.08	275.93 286.35	0.9539 0.9867
60	0.03938	273.54	298.35	1.0346	0.03324	272.31	296.69	1.0182
70	0.04304	282.66	308.48	1.0645	0.03634	281.57	307.01	1.0487
80 90	0.04469 0.04631	291.86 301.14	318.67 328.93	1.0938 1.1225	0.03781 0.03924	290.88 300.27	317.35 327.74	1.0784 1.1074
100	0.04631	310.53	339.27	1.1223	0.03924	309.74	338.19	1.1074
110	0.04946	320.03	349.70	1.1781	0.04201	319.31	348.71	1.1637
120	0.05099	329.64	360.24	1.2053	0.04335	328.98	359.33	1.1910
130 140	0.05251 0.05402	339.38 349.23	370.88 381.64	1.2320 1.2584	0.04468 0.04599	338.76 348.66	370.04 380.86	1.2179 1.2444
150	0.05550	359.21	392.52	1.2844	0.04399	358.68	391.79	1.2706
160	0.05698	369.32	403.51	1.3100	0.04857	368.82	402.82	1.2963

 TABLE A-12 (Continued)

IABLE A-12 (Continued)										
<i>T</i> °C	v m³/kg	и kJ/kg	<i>h</i> kJ/kg	s kJ/kg · K	$\frac{v}{\text{m}^3/\text{k}}$		u /kg	<i>h</i> kJ/kg	s kJ/kg · K	
	p =	$8.0 \text{ bar} = (T_{\text{sat}} = 3)$	= 0.80 MF 1.33°C)	p	p = 9.0  bar = 0.90  MPa $(T_{\text{sat}} = 35.53^{\circ}\text{C})$					
0-4	0.02547	1				0.9054				
Sat.	0.02547 0.02691	243.78 252.13	264.15 273.66	0.9066 0.9374	0.022 0.023		5.88	266.18 271.25	0.9054	
40 50	0.02846	261.62	284.39	0.9374	0.023		0.32	282.34	0.9217	
60	0.02992	271.04	294.98	1.0034	0.026	I	9.72	293.21	0.9897	
70	0.03131	280.45	305.50	1.0345	0.027		9.30	303.94	1.0214	
80	0.03264	289.89	316.00	1.0647	0.028		8.87	314.62	1.0521	
90	0.03393	299.37	326.52	1.0940	0.029		8.46	325.28	1.0819	
100	0.03519	308.93	337.08	1.1227	0.030		8.11	335.96	1.1109	
110	0.03642	318.57	347.71	1.1508	0.032		7.82	346.68	1.1392	
120	0.03762	328.31	358.40	1.1784	0.033	I	7.62	357.47	1.1670	
130	0.03881	338.14	369.19	1.2055	0.034		7.52	368.33	1.1943	
140	0.03997	348.09	380.07	1.2321	0.035		7.51	379.27	1.2211	
150	0.04113	358.15	391.05	1.2584	0.036		7.61	390.31	1.2475	
160	0.04227	368.32	402.14	1.2843	0.037		7.82	401.44	1.2735	
170	0.04340	378.61	413.33	1.3098	0.038		8.14	412.68	1.2992	
180	0.04452	389.02	424.63	1.3351	0.039	39   38	8.57	424.02	1.3245	
p = 10.0  bar = 1.00  MPa $p = 12.0  bar = 1.20  MPa$										
	p =	p	= 12.0	bar =	1.20 MP	a				
		$(T_{\rm sat} = 39)$	9.39°C)			-		.32°C)		
Sat.	0.02020	247.77	267.97	0.9043	0.016	63   25	1.03	270.99	0.9023	
40	0.02029	248.39	268.68	0.9066						
50	0.02171	258.48	280.19	0.9428	0.017	12   25	4.98	275.52	0.9164	
60	0.02301	268.35	291.36	0.9768	0.018	35 26	5.42	287.44	0.9527	
70	0.02423	278.11	302.34	1.0093	0.019	I	5.59	298.96	0.9868	
80	0.02538	287.82	313.20	1.0405	0.020	51   28	5.62	310.24	1.0192	
90	0.02649	297.53	324.01	1.0707	0.021	50 29.	5.59	321.39	1.0503	
100	0.02755	307.27	334.82	1.1000	0.022		5.54	332.47	1.0804	
110	0.02858	317.06	345.65	1.1286	0.023	35   31:	5.50	343.52	1.1096	
120	0.02959	326.93	356.52	1.1567	0.024	23   32	5.51	354.58	1.1381	
130	0.03058	336.88	367.46	1.1841	0.025		5.58	365.68	1.1660	
140	0.03154	346.92	378.46	1.2111	0.025	92   34	5.73	376.83	1.1933	
150	0.03250	357.06	389.56	1.2376	0.026	74   35	5.95	388.04	1.2201	
160	0.03344	367.31	400.74	1.2638	0.027		6.27	399.33	1.2465	
170	0.03436	377.66	412.02	1.2895	0.028		6.69	410.70	1.2724	
180	0.03528	388.12	423.40	1.3149	0.029	12   38	7.21	422.16	1.2980	
	p = 14.0  bar = 1.40  MPa					p = 16.0  bar = 1.60  MPa				
		$(T_{\rm sat} = 52)$		$(T_{\text{sat}} = 57.92^{\circ}\text{C})$						
Sat.	0.01405	253.74	273.40	0.9003	0.012	08 25	6.00	275.33	0.8982	
60	0.01495	262.17	283.10	0.9297	0.012		8.48	278.20	0.9069	
70	0.01603	272.87	295.31	0.9658	0.013		9.89	291.33	0.9457	
80	0.01701	283.29	307.10	0.9997	0.014		0.78	303.74	0.9813	
90	0.01792	293.55	318.63	1.0319	0.015		1.39	315.72	1.0148	
100	0.01772	303.73	330.02	1.0628	0.016		1.84	327.46	1.0467	
110	0.01960	313.88	341.32	1.0927	0.016		2.20	339.04	1.0773	
120	0.02039	324.05	352.59	1.1218	0.017		2.53	350.53	1.1069	
130	0.02115	334.25	363.86	1.1501	0.018		2.87	361.99	1.1357	
140	0.02113	344.50	375.15	1.1777	0.018		3.24	373.44	1.1638	
150	0.02169	354.82	386.49	1.2048	0.018		3.66	384.91	1.1038	
160	0.02202	365.22	397.89	1.2315	0.020		4.15	396.43	1.2181	
170	0.02333	375.71	409.36	1.2576	0.020		4.71	407.99	1.2445	
180	0.02403	386.29	420.90	1.2834	0.020		5.35	419.62	1.2443	
190	0.02472	396.96	432.53	1.3088	0.021		6.08	431.33	1.2764	
200	0.02541	407.73	444.24	1.3338	0.022		6.90	443.11	1.3212	
_50	0.02000	.0,5		1.0000	0.022	.0			1.0212	



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