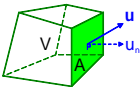


4. The Scalar-Transport Equation

Generic Scalar-Transport Equation

Conservation:



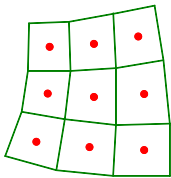
$$\left(\begin{matrix} \text{RATE OF CHANGE} \\ \text{inside } V \end{matrix} \right) + \left(\begin{matrix} \text{FLUX} \\ \text{through boundary of } V \end{matrix} \right) = \left(\begin{matrix} \text{SOURCE} \\ \text{inside } V \end{matrix} \right)$$

ϕ = concentration (amount per unit mass)

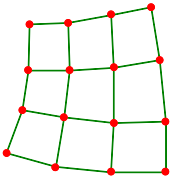
$$\frac{d}{dt}(\text{mass} \times \phi) + \sum_{\text{faces}} (\text{mass flux} \times \phi - \Gamma \frac{\partial \phi}{\partial n} A) = S$$

rate of change advection diffusion source

Location of Storage Nodes

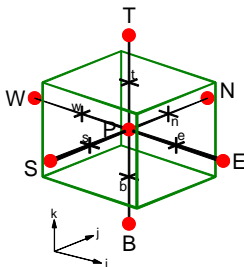


Cell-centred



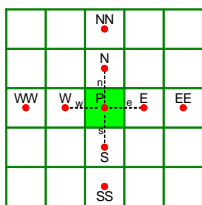
Cell-vertex

Cell Indexing (Structured Meshes)

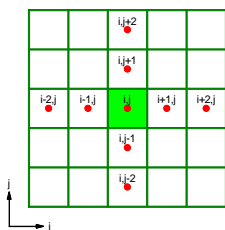


Cell Indexing (Structured Meshes)

Local



Global



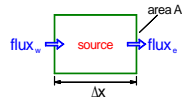
1-d Advection-Diffusion Equation

- Simple analysis
- Hand solution
- Straightforward generalisation to 2-d/3-d
- Coordinatewise discretisation in practice
- Many important theoretical problems are 1-d

Steady 1-d Advection-Diffusion Equation

Conservation:

$$\text{flux}_w - \text{flux}_e = \text{source}$$



Fluxes:

Advection: $(\rho u A) \phi$ (mass flux \times concentration)

Diffusion: $-\Gamma A \frac{d\phi}{dx}$ (diffusivity \times area \times gradient)

Differential form:

$$\frac{d}{dx}(\text{flux}) = \text{source per unit length}$$

$$\frac{d}{dx}(\rho u A \phi - \Gamma A \frac{d\phi}{dx}) = s$$

Discretising Diffusion and Source

Example

A thin rod has length 1 m and cross-section $1 \text{ cm} \times 1 \text{ cm}$. The left-hand end is kept at 100°C , whilst the right-hand end is insulated.

The heat flux across any section of area A is given by

$$-kA \frac{dT}{dx}$$

where the conductivity $k = 1000 \text{ W m}^{-1} \text{ K}^{-1}$.

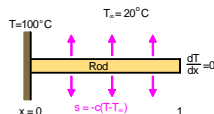
The rod is allowed to cool along its length at a rate proportional to its difference from the ambient temperature (Newton's law of cooling); i.e. the heat source per unit length is:

$$s = -c(T - T_\infty)$$

where the ambient temperature $T_\infty = 20^\circ \text{C}$ and the coefficient $c = 2.5 \text{ W m}^{-1} \text{ K}^{-1}$.

(a) Write down and solve the differential equation satisfied by the temperature.

(b) Divide the rod into 5 control sections with nodes at the centre of each section and carry out a finite-volume analysis to find the temperature along the rod.



Differential Equation and Exact Solution

$$\text{flux}_e - \text{flux}_w = \text{source}$$



$$\left(-kA \frac{dT}{dx}\right)_e - \left(-kA \frac{dT}{dx}\right)_w = -c(T - T_\infty)\Delta x$$

$$\frac{\left(-kA \frac{dT}{dx}\right)_e - \left(-kA \frac{dT}{dx}\right)_w}{\Delta x} = -c(T - T_\infty)$$

$$\frac{d}{dx} \left(-kA \frac{dT}{dx}\right) = -c(T - T_\infty)$$

$$T(0) = 100, \quad T'(l) = 0$$

$$\frac{d^2 T}{dx^2} - \frac{c}{kA} T = -\frac{c}{kA} T_\infty$$

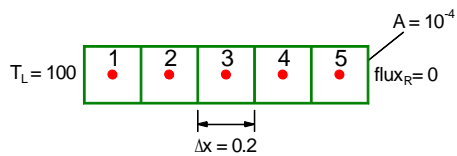
$$\frac{d^2 T}{dx^2} - 25T = -500$$

$$T = Ae^{5x} + Be^{-5x} + \frac{20}{25}$$

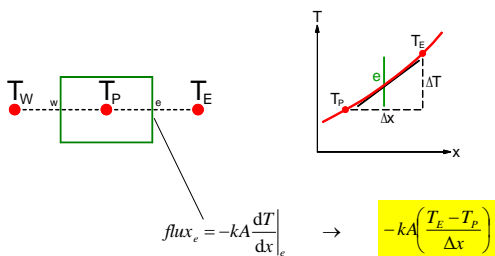
complementary function particular integral

$$A = 0.0036, \quad B = 79.9964$$

Finite-Volume Decomposition



Discretisation of Fluxes



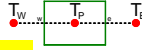
Finite-Volume Discretisation

Conservation: $flux_e - flux_w = source$



Fluxes:

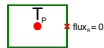
interior faces: $flux_e = -kA \frac{dT}{dx} \Big|_e \rightarrow -kA \left(\frac{T_e - T_p}{\Delta x} \right)$
 $\rightarrow -D(T_e - T_p)$ $D = \frac{kA}{\Delta x} = 0.5$



left boundary: $flux_e = -kA \frac{dT}{dx} \Big|_L \rightarrow -kA \left(\frac{T_p - T_L}{\frac{1}{2}\Delta x} \right)$
 $\rightarrow -2D(T_p - T_L)$



right boundary: $flux_e = 0$

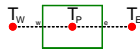


Source: $source = -c(T_p - T_\infty)\Delta x \rightarrow b_p + s_p T_p$

$b_p = cT_\infty\Delta x = 10$, $s_p = -c\Delta x = -0.5$

Finite-Volume Discretisation

$flux_e - flux_w = source$

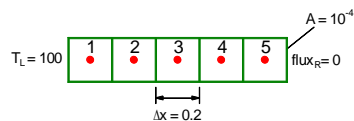


Interior cells: $-0.5(T_e - T_p) + 0.5(T_p - T_w) = 10 - 0.5T_p$
 $-0.5T_w + 1.5T_p - 0.5T_e = 10$

Left boundary: $-0.5(T_e - T_p) + 1.0(T_p - 100) = 10 - 0.5T_p$
 $2.0T_p - 0.5T_e = 110$

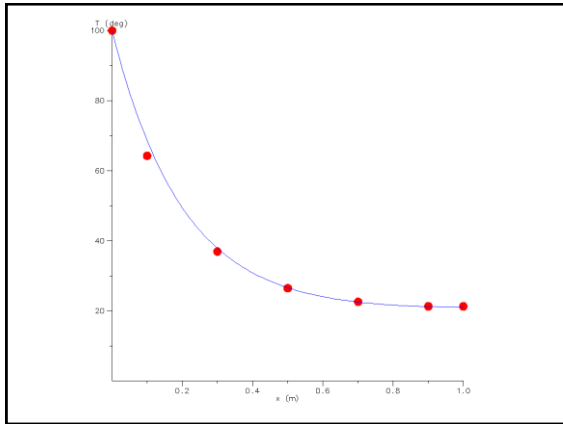
Right boundary: $0 + 0.5(T_p - T_w) = 10 - 0.5T_p$
 $-0.5T_w + 1.0T_p = 10$

Assembled Equations



$$\begin{pmatrix} 2 & -0.5 & 0 & 0 & 0 \\ -0.5 & 1.5 & -0.5 & 0 & 0 \\ 0 & -0.5 & 1.5 & -0.5 & 0 \\ 0 & 0 & -0.5 & 1.5 & -0.5 \\ 0 & 0 & 0 & -0.5 & 1 \end{pmatrix} \begin{pmatrix} T_1 \\ T_2 \\ T_3 \\ T_4 \\ T_5 \end{pmatrix} = \begin{pmatrix} 110 \\ 10 \\ 10 \\ 10 \\ 10 \end{pmatrix}$$





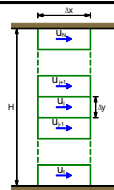
Points to Note

- Each control volume gives one equation
- Each equation is a linear equation connecting the central node and nodes on either side
- Boundary values are incorporated into the source term
- The resulting matrix is tri-diagonal

$$\begin{pmatrix} \text{---} \\ \text{---} \\ \text{---} \\ \text{---} \\ \text{---} \end{pmatrix} \Phi = \mathbf{b}$$

Example

A 2-d finite-volume calculation is to be undertaken for fully-developed, laminar flow between stationary, plane, parallel walls. A streamwise pressure gradient $dp/dx = -G$ is imposed and the fluid viscosity is μ . The depth of the channel, H , is divided into N equally-sized cells of dimension $\Delta x \times \Delta y \times 1$ as shown, with the velocity u stored at cell centres.



- What are the boundary conditions on velocity?
- What is the net pressure force on a single cell?
- Using a finite-difference approximation for velocity gradient, find expressions for the viscous forces on upper and lower faces of the j^{th} cell in terms of the nodal velocities $\{u_j\}$. (You will need to deal separately with interior cells and the boundary cells $j = 1$ and $j = N$.)
- By balancing pressure and viscous forces set up the finite-volume equations for velocity.
- Solve for the nodal velocities in the case $N = 6$, leaving your answers as multiples of $U_0 = GH^2/4\mu$. (You are advised to note the symmetry of the problem.)
- Using your numerical solution, find the volume flow rate (per unit span) Q in terms of U_0 and H .
- Find the wall shear stress, τ_w .
- Compare your answers to (e), (f), (g) with the exact solution for plane Poiseuille flow.

Discretising Advection (Part 1)

Example



A pipe of cross-section $A = 0.01 \text{ m}^2$ and length $L = 1 \text{ m}$ carries water (density $\rho = 1000 \text{ kg m}^{-3}$) at velocity $u = 0.1 \text{ m s}^{-1}$.

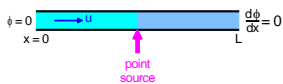
A faulty valve introduces a reactive chemical into the pipe half-way along its length at a rate of 0.01 kg s^{-1} . The diffusivity of the chemical in water is $\Gamma = 0.1 \text{ kg m}^{-1} \text{ s}^{-1}$. The chemical is subsequently broken down at a rate proportional to its concentration ϕ (mass of chemical per unit mass of water), this rate amounting to $-\gamma\phi$ per metre, where $\gamma = 0.5 \text{ kg m}^{-1} \text{ s}^{-1}$.

Assuming that the downstream boundary condition is $d\phi/dx = 0$, set up a finite-volume calculation with 7 cells to estimate the concentration along the pipe using:

- Central
- Upwind

differencing schemes for advection.

Fluxes and Sources



Concentration ϕ (= mass of chemical per mass of water)

Flux (= rate of transport across a surface)

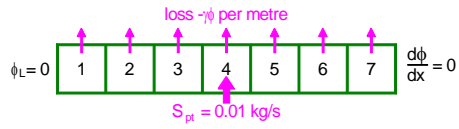
advection: $C\phi$ $C = \rho u A$

diffusion: $-\Gamma A \frac{d\phi}{dx}$

Source

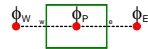
- point source S_{pt} at $x = 0.5 \text{ m}$
- loss by chemical breakdown $-\gamma\phi$ per unit length

Finite-Volume Decomposition



Finite-Volume Discretisation

$$\text{flux}_e - \text{flux}_w = \text{source}$$



$$\text{flux} = C\phi - \Gamma A \frac{d\phi}{dx}$$

$$\text{flux}_e = C\phi_e - D(\phi_e - \phi_P)$$

$$\text{flux}_w = C\phi_w - D(\phi_P - \phi_w)$$

$$C = \rho u A = 1.0$$

$$D = \frac{\Gamma A}{\Delta x} = 0.007$$

$$\text{source} = \underbrace{S_{pt}}_{\text{cell 4 only}} - \gamma\phi_P \Delta x$$

$$\text{source} = b_P + s_P \phi_P$$

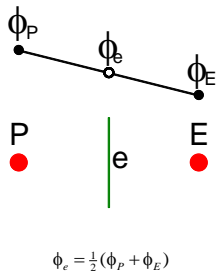
$$b_P = 0.01 \text{ (cell 4)}$$

$$s_P = -0.071$$

$$\underbrace{C\phi_e - C\phi_w}_{\text{advection}} - \underbrace{D\phi_w + 2D\phi_P - D\phi_E}_{\text{diffusion}} = \underbrace{b_P + s_P \phi_P}_{\text{source}}$$

An approximation for cell-face values ϕ_e and ϕ_w is called an **advection scheme** or **advection-differencing scheme**

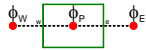
Central Differencing



Finite-Volume Discretisation:

Central Differencing For Advection

$$\underbrace{C\phi_e - C\phi_w}_{\text{advection}} - \underbrace{D\phi_w + 2D\phi_P - D\phi_E}_{\text{diffusion}} = \underbrace{b_P + s_P\phi_P}_{\text{source}}$$



Central differencing: $C\phi_e - C\phi_w = C\frac{1}{2}(\phi_P + \phi_E) - C\frac{1}{2}(\phi_W + \phi_P)$

$$= \frac{C}{2}(\phi_E - \phi_W)$$

$$-\left(\frac{C}{2} + D\right)\phi_W + (2D - s_P)\phi_P - \left(-\frac{C}{2} + D\right)\phi_E = b_P$$

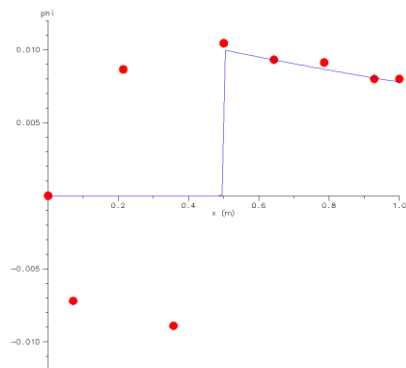
$$-0.507\phi_W + 0.085\phi_P + 0.493\phi_E = \frac{0.01}{\text{cell 4 only}}$$

Assembled Equations

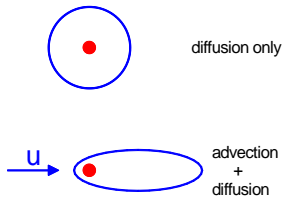
Central Advection Scheme

$$\begin{pmatrix} 0.592 & 0.493 & 0 & 0 & 0 & 0 & 0 \\ -0.507 & 0.085 & 0.493 & 0 & 0 & 0 & 0 \\ 0 & -0.507 & 0.085 & 0.493 & 0 & 0 & 0 \\ 0 & 0 & -0.507 & 0.085 & 0.493 & 0 & 0 \\ 0 & 0 & 0 & -0.507 & 0.085 & 0.493 & 0 \\ 0 & 0 & 0 & 0 & -0.507 & 0.085 & 0.493 \\ 0 & 0 & 0 & 0 & 0 & -0.507 & 0.578 \end{pmatrix} \begin{pmatrix} \phi_1 \\ \phi_2 \\ \phi_3 \\ \phi_4 \\ \phi_5 \\ \phi_6 \\ \phi_7 \end{pmatrix} = \begin{pmatrix} 0 \\ 0 \\ 0 \\ 0.01 \\ 0 \\ 0 \\ 0 \end{pmatrix}$$

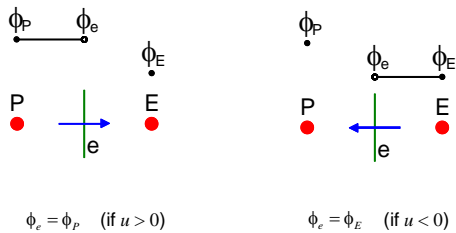




Directional Bias

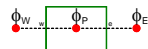


Upwind Differencing



Upwind Differencing

$$\underbrace{C\phi_e - C\phi_w}_{\text{advection}} - \underbrace{D\phi_w + 2D\phi_P - D\phi_E}_{\text{diffusion}} = \underbrace{b_P + s_P\phi_P}_{\text{source}}$$



Upwind differencing: $C\phi_e - C\phi_w = C(\phi_P - \phi_W)$

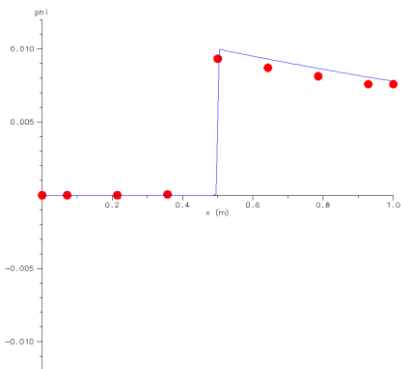
$$-(C + D)\phi_W + (C + 2D - s_P)\phi_P - D\phi_E = b_P$$

$$-1.007\phi_W + 1.085\phi_P - 0.007\phi_E = \frac{0.01}{\text{cell 4 only}}$$

Assembled Equations

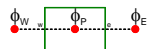
- Upwind Advection Scheme

$$\begin{pmatrix} 1.092 & -0.007 & 0 & 0 & 0 & 0 & 0 \\ -1.007 & 1.085 & -0.007 & 0 & 0 & 0 & 0 \\ 0 & -1.007 & 1.085 & -0.007 & 0 & 0 & 0 \\ 0 & 0 & -1.007 & 1.085 & -0.007 & 0 & 0 \\ 0 & 0 & 0 & -1.007 & 1.085 & -0.007 & 0 \\ 0 & 0 & 0 & 0 & -1.007 & 1.085 & -0.007 \\ 0 & 0 & 0 & 0 & 0 & -1.007 & 1.078 \end{pmatrix} \begin{pmatrix} \phi_1 \\ \phi_2 \\ \phi_3 \\ \phi_4 \\ \phi_5 \\ \phi_6 \\ \phi_7 \end{pmatrix} = \begin{pmatrix} 0 \\ 0 \\ 0 \\ 0.01 \\ 0 \\ 0 \\ 0 \end{pmatrix}$$



Simple Advection Schemes Compared

$$-a_w \phi_w + a_p \phi_p - a_e \phi_e = b_p$$



Central differencing

$$\begin{aligned} a_w &= \frac{1}{2}C + D \\ a_e &= -\frac{1}{2}C + D \\ a_p &= 2D - s_p \end{aligned}$$

OK \Leftrightarrow $Pe \leq 2$

$$Pe = \frac{C}{D} = \frac{\rho u \Delta x}{\Gamma} \quad \text{Peclet number}$$

Theoretically, high accuracy ...
... but unphysical "wiggles"

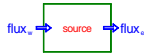
Upwind differencing

$$\begin{aligned} a_w &= C + D \\ a_e &= D \\ a_p &= C + 2D - s_p \quad (\text{if } C > 0) \end{aligned}$$

Lower accuracy ...
... but no "wiggles"

Finite-Volume Analysis: 1-d

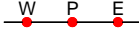
Conservation:



$$flux_e - flux_w = source$$

$$flux = C\phi - \Gamma A \frac{d\phi}{dx}$$

Discretisation:



$$-a_w\phi_w + a_P\phi_P - a_E\phi_E = b_P$$

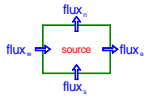
Assembled matrix equation:

$$\begin{pmatrix} \text{---} \\ \text{---} \\ \text{---} \end{pmatrix} \Phi = \mathbf{b}$$

$$\mathbf{A}\Phi = \mathbf{b}$$

Finite-Volume Analysis: 2-d

Conservation:

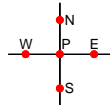


$$flux_e - flux_w + flux_n - flux_s = source$$

$$flux_{e,w} = (\rho u A \phi - \Gamma A \frac{\partial \phi}{\partial x})_{e,w}$$

$$flux_{s,n} = (\rho v A \phi - \Gamma A \frac{\partial \phi}{\partial y})_{s,n}$$

Discretisation:



$$-a_s\phi_s - a_w\phi_w + a_P\phi_P - a_E\phi_E - a_N\phi_N = b_P$$

$$a_P\phi_P - \sum a_f\phi_f = b_P$$

Assembled matrix equation:

$$\begin{pmatrix} \text{---} \\ \text{---} \\ \text{---} \end{pmatrix} \Phi = \mathbf{b}$$

$$\mathbf{A}\Phi = \mathbf{b}$$

General Discretisation Properties

Discretisation Properties

- Consistency
- Conservativeness
- Transportiveness
- Boundedness
- Stability
- Accuracy ("order")

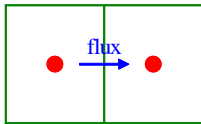
Consistent

Definition: an algebraic approximation is **consistent** if it tends to the exact governing equation as the mesh size tends to zero

e.g. $\frac{\phi_E - \phi_P}{\Delta x} \leftarrow \frac{d\phi}{dx}$

Conservativeness

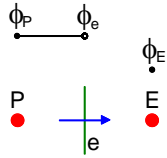
Definition: flux **out** of one cell = flux **into** adjacent cell



- **Fluxes** are worked out by **face**, not by cell
- Automatically built into the finite-volume method

Transportiveness

Definition: upstream-biased

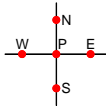


Boundedness

Definition: for advection-diffusion **without sources**:

- (1) ϕ_P must lie between minimum and maximum values at surrounding nodes
- (2) $\phi = \text{constant}$ must be a possible solution

$$a_P \phi_P - \sum a_F \phi_F = 0$$



Requirements:

- (1) Positive coefficients: $a_P, a_F \geq 0$
- (2) Sum of neighbouring coefficients: $a_P = \sum a_F$

Stability

Definition:

- small errors do not grow in the course of the calculation

Requirement:

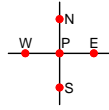
- negative-slope linearisation of the source term ("negative feedback")

$$\text{source} = b_P + s_P \phi_P, \quad s_P \leq 0$$

Summary of Conditions on Matrix Coefficients

$$\text{source} = b_P + s_P \phi_P$$

$$a_P \phi_P - \sum a_F \phi_F = b_P$$



Positive coefficients:

$$a_F \geq 0 \text{ for all } F$$

Negative-slope linearisation of the source term:

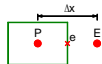
$$s_P \leq 0$$

Sum of neighbouring coefficients:

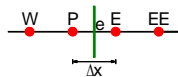
$$a_P = \sum a_F - s_P$$

Accuracy ("Order")

- General definition:
 $\text{order } n \Leftrightarrow \text{error} \propto (\Delta x)^n \quad (\text{as } \Delta x \rightarrow 0)$
- Determined by Taylor-series expansion (about a cell face)
- Common advection schemes:
 - upwind: 1st order
 - central: 2nd order
 - QUICK: 3rd order



Example



Consider the uniform, one-dimensional arrangement of nodes shown. Face e lies half way between P and E nodes.

(a) Show that the central-differencing schemes

$$\phi_e \approx \frac{1}{2}(\phi_P + \phi_E) \quad \left. \frac{d\phi}{dx} \right|_e \approx \frac{\phi_E - \phi_P}{\Delta x}$$

are second-order accurate approximations for ϕ_e and $(d\phi/dx)_e$ respectively.

(b) Making use of the W and EE nodes also, find symmetric fourth-order-accurate approximations for ϕ_e and $(d\phi/dx)_e$.

Discretising Advection (Part 2)

Exponential Scheme

Exact solution of the 1-d advection-diffusion equation
(with constant coefficients and without sources)

$$\text{flux} = C\phi - \Gamma A \frac{d\phi}{dx} = \text{constant}$$



$$\text{flux}_e = C \left(\frac{e^{Pe} \phi_P - \phi_E}{e^{Pe} - 1} \right)$$

$$C = \rho u A, \quad D = \frac{\Gamma A}{\Delta x}, \quad Pe = \frac{C}{D}$$

$$\text{flux}_e - \text{flux}_w = a_P \phi_P - \sum a_F \phi_F$$

$$a_w = \frac{C e^{Pe}}{e^{Pe} - 1}, \quad a_E = \frac{C}{e^{Pe} - 1}$$

$$a_P = a_E + a_w$$

Hybrid Scheme

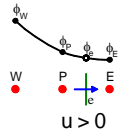
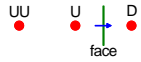
More computationally-efficient approximation to the exponential scheme.

Amounts to:

- Central differencing if $|Pe| \leq 2$
- Upwind differencing (with no diffusion) if $|Pe| > 2$

QUICK

- 3-point, upwind-biased scheme

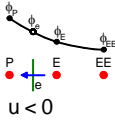


$u > 0$

- Fits a quadratic through 3 nodes

$$\phi_{face} = -\frac{1}{8}\phi_{UU} + \frac{3}{4}\phi_U + \frac{3}{8}\phi_D$$

- 3rd-order accurate ... but not bounded

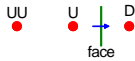


$u < 0$

Flux-Limited Schemes

- 3-point, upwind-biased schemes, with solution-dependent limiters

$$\phi_{face} = \text{function}(\phi_{UU}, \phi_U, \phi_D)$$

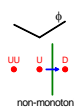


- General form: $\phi_{face} = \begin{cases} \phi_U + \frac{1}{2}\psi(r)(\phi_D - \phi_U) & \text{if monotonic} \\ \phi_U & \text{otherwise} \end{cases}$

$$r = \frac{\phi_U - \phi_{UU}}{\phi_D - \phi_U}$$



monotonic



non-monotonic

- Non-linear (\Rightarrow iteration necessary)

- Total-Variation-Diminishing

Scheme	$\psi(r)$ (for $r > 0$)	
UMIST	$\min\{2, 2r, \frac{1}{4}(1+3r), \frac{1}{4}(3+r)\}$	Upstream Monotonic Interpolation for Scalar Transport (Lien and Leschziner, 1993)
Harmonic	$\frac{2r}{1+r}$	Van Leer (1974)
Min-mod	$\min\{r, 1\}$	Roe (1985)
Van Albada et al.	$\frac{r+r^2}{1+r^2}$	Van Albada et al., (1982)

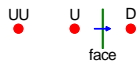
In all cases $\psi(r)$ is taken as 0 if non-monotonic ($r < 0$)

Example

The Van Leer harmonic advection scheme is given by

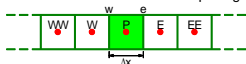
$$\phi_{face} = \phi_U + \frac{1}{2} \psi(r) (\phi_D - \phi_U)$$

$$\psi(r) = \begin{cases} \frac{2r}{1+r} & \text{if } r > 0 \\ 0 & \text{otherwise} \end{cases} \quad r = \frac{\phi_U - \phi_{UU}}{\phi_D - \phi_U}$$



where nodes UU, U and D are determined by flow direction as shown.

A local arrangement of nodes and faces in a 1-d finite-volume mesh with standard geographical notation and uniform mesh spacing Δx is shown below.



The values of a scalar ϕ at these nodes are:

$$\phi_{WW} = 2, \quad \phi_W = 4, \quad \phi_P = 6, \quad \phi_E = 7, \quad \phi_{EE} = 6.$$

Using the Van Leer harmonic advection scheme, calculate the value of ϕ on the west (w) and east (e) cell faces if the velocity throughout the domain is:

- (a) positive;
- (b) negative.

Implementation of Higher-Order Schemes

$$\sum_{faces} (\text{mass flux} \times \phi - \Gamma \frac{\partial \phi}{\partial n} A) = S$$

advection diffusion source

$$\sum_{faces} [C_f \phi_f + D_f (\phi_P - \phi_P)] = b_P + s_P \phi_P$$

$$\sum_{faces} C_f = 0$$

$$\sum_{faces} [C_f (\phi_f - \phi_P) + D_f (\phi_P - \phi_P)] = b_P + s_P \phi_P$$



Write the cell-face value as **upwind + correction**: $\phi_f = \underbrace{\phi_U}_{\text{upwind}} + \underbrace{(\phi_f - \phi_U)}_{\text{deferred correction}}$

The **upwind** part always gives positive coefficients and diagonal dominance

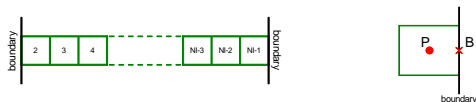
$$C_f (\phi_f - \phi_P) = \underbrace{C_f (\phi_U - \phi_P)}_{\text{upwind}} + \underbrace{C_f (\phi_f - \phi_U)}_{\text{correction}}$$

$$= \max(-C_f, 0) (\phi_P - \phi_f) + C_f (\phi_f - \phi_U)$$

The **deferred correction** is transferred to the source term and treated explicitly (i.e. not updated until the next iteration):

$$\sum_f a_f (\phi_P - \phi_f) = b_P + s_P \phi_P - \underbrace{\sum_{faces} C_f (\phi_f - \phi_U)}_{\text{deferred correction}} \quad a_f = \max(-C_f, 0) + D_f$$

Implementation of Boundary Conditions



Boundary fluxes are transferred to the **source** term:

$$\sum_{\text{nat boundary}} \text{flux} + \text{flux}_{\text{boundary}} = \text{source}$$



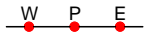
$$a_P \phi_P - \sum_{\text{nat boundary}} a_f \phi_f = b_P - \text{flux}_{\text{boundary}}$$

Matrix Solution Algorithms

Form of the Matrix Equations

$$a_P \phi_P - \sum_F a_F \phi_F = b_P$$

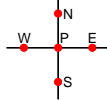
1-d



$$-a_W \phi_W + a_P \phi_P - a_E \phi_E = b_P$$

$$\begin{pmatrix} \text{diagonal lines} \end{pmatrix} \Phi = b$$

2-d



$$-a_S \phi_S - a_W \phi_W + a_P \phi_P - a_E \phi_E - a_N \phi_N = b_P$$

$$\begin{pmatrix} \text{diagonal lines} \end{pmatrix} \Phi = b$$

Characteristics of the Equations

- **Fluid-flow equations:**
 - non-linear
 - Coupled
- **Matrix equations:**
 - sparse
 - Banded
- **Solution methods:**
 - iterative

Common Solution Methods

- Gaussian elimination
- Gauss-Seidel
- Line Gauss-Seidel

Gaussian Elimination

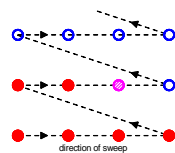
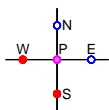
- **Direct**, not iterative
- Sequence of **row operations** aiming to produce an **upper-triangular matrix**
- Tends to “**fill in**” sparse matrices
- Important exception: tri-diagonal systems (basis of the **tri-diagonal matrix algorithm**)

$$\begin{pmatrix} \text{---} \\ \text{---} \\ \text{---} \end{pmatrix} \Phi = \mathbf{b}$$

Gauss-Seidel

$$-a_S\phi_S - a_W\phi_W + a_P\phi_P - a_E\phi_E - a_N\phi_N = b_P$$

$$\phi_P = \frac{1}{a_P} (b_P + a_S\phi_S^* + a_W\phi_W^* + a_E\phi_E^* + a_N\phi_N^*)$$



- being updated
- already updated
- not yet updated

Gauss-Seidel Example (i)

$$\begin{pmatrix} 4 & -1 & 0 & 0 \\ -1 & 4 & -1 & 0 \\ 0 & -1 & 4 & -1 \\ 0 & 0 & -1 & 4 \end{pmatrix} \begin{pmatrix} A \\ B \\ C \\ D \end{pmatrix} = \begin{pmatrix} 2 \\ 4 \\ 6 \\ 13 \end{pmatrix}$$



Gauss-Seidel Example (ii)

$$\begin{pmatrix} 1 & -4 & 0 & 0 \\ -4 & 1 & -4 & 0 \\ 0 & -4 & 1 & -4 \\ 0 & 0 & -4 & 1 \end{pmatrix} \begin{pmatrix} A \\ B \\ C \\ D \end{pmatrix} = \begin{pmatrix} -7 \\ -14 \\ -21 \\ -8 \end{pmatrix}$$



Gauss-Seidel Overview

- **Iterative**
- **Simple** to code
- Minimal **storage** requirements
- **Convergence slow** for large matrices
- Constraints on matrix elements (e.g. **diagonal dominance**)

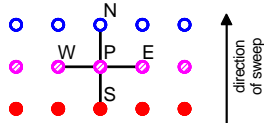
$$\sum_{j \neq i} |a_{ij}| \leq a_{ii}$$

Line Gauss-Seidel (Line-Iterative Procedures, LIP)

$$-a_S\phi_S - a_W\phi_W + a_P\phi_P - a_E\phi_E - a_N\phi_N = b_P$$

$$-a_W\phi_W + a_P\phi_P - a_E\phi_E = b_P + a_S\phi_S^* + a_N\phi_N^*$$

$$\begin{pmatrix} \text{---} \end{pmatrix} \phi = \mathbf{b} - \begin{pmatrix} \text{---} \end{pmatrix} \phi^*$$



Line Gauss-Seidel - Overview

- Iterative
- Repeated use of **tri-diagonal solver**:
 - **whole line** updated in one go
 - rapid propagation across domain
- Applicable to **structured meshes** only
- Basis of many research codes

Convergence Criteria

$$a_P\phi_P - \sum_F a_F\phi_F = b_P$$

Single-cell error:

residual: $res = a_P\phi_P - \sum_F a_F\phi_F - b_P$

Global error:

sum of absolute residuals: $\sum_{cells} |res|$

root-mean-square error: $\sqrt{\frac{1}{N} \sum_{cells} (res)^2}$

Convergence criteria:

error < tolerance
or
error < fraction of initial error

Under-Relaxation

- The governing equations are coupled and non-linear
- Matrix coefficients change at every iteration
- The iterative solution method may be numerically unstable
- **Under-relaxation** tries to stabilise an iterative procedure by **reducing the change** in variables at each iteration

Under-Relaxation in CFD

Standard linearised equation:

$$a_P \phi_P - \sum_F a_F \phi_F = b_P$$

Rearrange as the **change** in ϕ :

$$\phi_P = \frac{\sum_F a_F \phi_F + b_P}{a_P}$$

$$\phi_P = \phi_P^{prev} + \left(\frac{\sum_F a_F \phi_F + b_P}{a_P} - \phi_P^{prev} \right)$$

Under-relax the change:

$$\phi_P = \phi_P^{prev} + \alpha \left(\frac{\sum_F a_F \phi_F + b_P}{a_P} - \phi_P^{prev} \right)$$

Rearrange back:

$$a_P \phi_P - \sum_F a_F \phi_F = \alpha b_P + (1 - \alpha) a_P \phi_P^{prev}$$

Incorporate by **modifying coefficients**:

$$a_F \rightarrow \alpha a_F$$

$$b_P \rightarrow \alpha b_P + (1 - \alpha) a_P \phi_P^{prev}$$

Summary (1)

- The generic scalar-transport equation for a particular control volume has the form **rate of change + net outward flux = source**
- **Flux** \equiv rate of transport through a surface and consists of:
 - advection**: transport with the flow (other authors prefer *convection*)
 - diffusion**: net transport by random molecular or turbulent fluctuations
- Discretisation of the (steady) scalar-transport equation yields an equation of form

$$a_P \phi_P - \sum_F a_F \phi_F = b_P$$
 for each control volume, where the summation is over adjacent nodes
- The collection of these simultaneous equations on a structured mesh yields a **matrix equation** with limited bandwidth (i.e. few non-zero diagonals), typically solved by iterative methods such as Gauss-Seidel or line-Gauss-Seidel

Summary (2)

- **Source** terms are linearised as

$$b_p + s_p \phi_p, \quad s_p \leq 0$$

- **Diffusive** fluxes are usually discretised by central differencing; e.g.

$$-\Gamma \frac{\partial \phi}{\partial x} \Big|_e A \rightarrow -\frac{\Gamma A}{\Delta x} (\phi_E - \phi_P)$$

- **Advection** schemes are means of approximating ϕ on cell faces in order to compute advective fluxes. They include Upwind, Central, Exponential, Hybrid, QUICK, and various flux-limited schemes
- General desirable properties for a numerical scheme:
 - consistency
 - conservativeness
 - transportiveness
 - boundedness
 - stability
 - accuracy / high order

Summary (3)

- **Boundedness** and **stability** impose certain constraints on the discretisation:

$$a_p \geq 0 \quad (\text{"positive coefficients"})$$

$$s_p \leq 0 \quad (\text{"negative feedback in the source term"})$$

$$a_p = \sum_F a_F - s_p \quad (\text{"sum of the neighbouring coefficients"})$$

- To ensure positive coefficients (and implement non-linear schemes), advective fluxes are often decomposed into **Upwind + deferred correction** with the latter being transferred to the source term and treated explicitly (i.e. fixed for this iteration)
- **Boundary conditions** can be implemented by transferring boundary fluxes to the source terms
- **Under-relaxation** is usually required to solve coupled and/or non-linear equations
