

**UNIVERSITY OF ABERDEEN    SESSION 2014–2015****Degree Examination in EG501J Renewable Energy: Solar and Geothermal****0<sup>th</sup> December 2014****00.00–00.00**

- Notes:*
- (i) Candidates ARE permitted to use an approved calculator.*
  - (ii) Candidates ARE permitted to use steam tables, which will be provided.*
  - (iii) Candidates ARE permitted to use refrigerant tables, which will be provided.*
  - (iv) Candidates ARE permitted to use psychrometric chart, which will be provided.*
  - (v) Data sheets are attached to the paper.*

**PLEASE NOTE THE FOLLOWING**

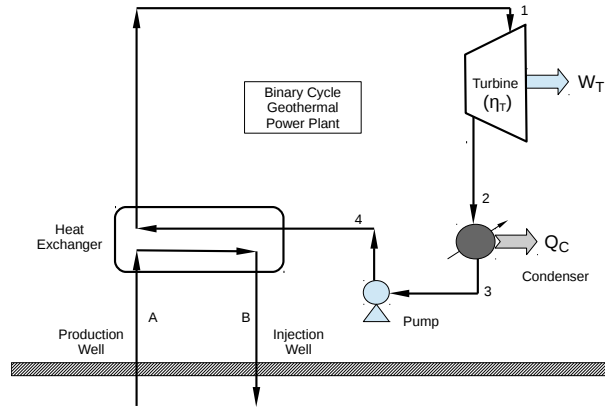
- (i) You **must not** have in your possession any material other than that expressly permitted in the rules appropriate to this examination. Where this is permitted, such material **must not** be amended, annotated or modified in any way.
- (ii) You **must not** have in your possession any material that could be determined as giving you an advantage in the examination.
- (iii) You **must not** attempt to communicate with any candidate during the exam, either orally or by passing written material, or by showing material to another candidate, nor must you attempt to view another candidate's work.

**Failure to comply with the above will be regarded as cheating and may lead to disciplinary action as indicated in the Academic Quality Handbook ([www.abdn.ac.uk/registry/quality/appendix7x1.pdf](http://www.abdn.ac.uk/registry/quality/appendix7x1.pdf)) Section 4.14 and 5.**

**Candidates must attempt *all* questions.**

### Question 1

A binary geothermal power station is operated with brine extracted at  $90^\circ\text{C}$  and reinjected at  $30^\circ\text{C}$ . Propane ( $n\text{-C}_3$ ) is used as working fluid in the Rankine cycle to produce power ( $W_T$ ) in a turbine (isentropic expansion) with efficiency ( $\eta_T$ ) of 90%. After condensed,  $n\text{-C}_3$  is driven to a heat exchanger (with thermal efficiency of 68%) and the cycle continues. The mass flow rate of  $n\text{-C}_3$  ( $\dot{m}_{C_3}$ ) is  $250 \text{ kg.s}^{-1}$  and the heat capacity ( $C_p$ ) of brine is  $3565.5 \text{ J.(kg.K)}^{-1}$ . Conditions for  $n\text{-C}_3$  and brine flows are described in Table 1.



**Table 1:** *Thermodynamic table of the geothermal binary cycle.*

| Stage | P<br>(bar) | T<br>(°C) | State       | H<br>(kJ.kg <sup>-1</sup> ) | S<br>(kJ.(kg.K) <sup>-1</sup> ) |
|-------|------------|-----------|-------------|-----------------------------|---------------------------------|
| 1     | 16         | 50        | (a)         | (b)                         | (c)                             |
| 2     | 6          | —         | wet vapour  | (d)                         | —                               |
| 3     | 6          | —         | sat. liquid | (e)                         | —                               |
| 4     | 16         | —         | (f)         | (g)                         | —                               |
| A     | —          | 90        | —           | —                           | —                               |
| B     | —          | 30        | —           | —                           | —                               |

- In Table 1, determine (a)-(g). [7 marks]
- Calculate the power produced by the turbine ( $W_T$ ) in MW. [1 marks]
- Assuming that the heat exchanger has an efficiency of 68%, calculate the mass flow rate of brine in  $\text{kg.s}^{-1}$ . [3 marks]
- Sketch the temperature  $\times$  entropy (TS) diagram for the process indicating the liquid and vapour saturated lines and each stage of the  $n\text{-C}_3$  Rankine cycle. [4 marks]
- Dry-steam, flash-steam and binary-cycle power plants are considered the three main conversion technologies in geothermal systems. Describe the flash-steam process. [4 marks]
- Temperature gradient ( $\nabla T$ ) between upper and deep layers of rocks (i.e., near the surface and at large depths) can lead to geothermal circulation. Define thermal buoyancy and its links to thermal convection. [6 marks]

To solve this problem, you should assume that the saturated liquid streams are incompressible, and therefore  $dH = VdP$  (where  $H$ ,  $V$  and  $P$  are enthalpy, volume and pressure, respectively). Quality of the vapour is expressed as

$$x_j = \frac{\Psi_j - \Psi_f}{\Psi_g - \Psi_f} \quad \text{with } \Psi = \{H, S\}$$

where  $S$  is the entropy. Efficiency of the turbine ( $\eta_{\text{Turbine}}$ ) and the heat exchanger ( $\eta_{\text{HE}}$ ) are given by,

$$\eta_{\text{Turbine}} = \frac{H_2 - H_1}{H_{2s} - H_1} \quad \text{and} \quad \eta_{\text{HE}} = \frac{\dot{Q}_{C3}}{\dot{Q}_{gf}}$$

where  $H_{2s}$  is the enthalpy of stream 2 assuming ideal turbine performance (i.e., reversible expansion).  $\dot{Q}_{C3}$  and  $\dot{Q}_{gf}$  are the heat associated with the n-C<sub>3</sub> and brine streams, respectively, at the heat exchanger.

# Appendix A: Physical Constants and Conversion Factors

## PHYSICAL CONSTANTS

Avogadro's number,  $N_A = 6.023 \times 10^{26}$  molecules/kgmole  
 Boltzmann's constant,  $k = 1.381 \times 10^{-23}$  J/(molecule·K)  
 Electron charge,  $e = 1.602 \times 10^{-19}$  C  
 Electron mass,  $m_e = 9.110 \times 10^{-31}$  kg  
 Faraday's constant,  $F = 96,487$  kC/kgmole electrons = 96,487 kJ/(V·kgmole electrons)  
 Gravitational acceleration (standard),  $g = 32.174$  ft/s<sup>2</sup> = 9.807 m/s<sup>2</sup>  
 Gravitational constant,  $k_G = 6.67 \times 10^{-11}$  m<sup>3</sup>/(kg·s<sup>2</sup>)  
 Newton's second law constant,  $g_c = 32.174$  lbm·ft/(lbf·s<sup>2</sup>) = 1.0 kg·m/(N·s<sup>2</sup>)  
 Planck's constant,  $h = 6.626 \times 10^{-34}$  J·s/molecule  
 Stefan-Boltzmann constant,  $\sigma = 0.1714 \times 10^{-8}$  Btu/(h·ft<sup>2</sup>·R<sup>4</sup>) =  $5.670 \times 10^{-8}$  W/(m<sup>2</sup>·K<sup>4</sup>)  
 Universal gas constant  $\mathfrak{R} = 1545.35$  ft·lbf/(lbmole·R) = 8314.3 J/(kgmole·K)  
     = 8.3143 kJ/(kgmole·K) = 1.9858 Btu/(lbmole·R)  
     = 1.9858 kcal/(kgmole·K) = 1.9858 cal/(gmole·K)  
     = 0.08314 bar·m<sup>3</sup>/(kgmole·K) = 82.05 L·atm/(kgmole·K)  
 Velocity of light in a vacuum,  $c = 9.836 \times 10^8$  ft/s =  $2.998 \times 10^8$  m/s

## UNIT DEFINITIONS

|                                      |                                     |
|--------------------------------------|-------------------------------------|
| 1 coulomb (C) = 1 A·s                | 1 ohm ( $\Omega$ ) = 1 V/A          |
| 1 dyne = 1 g·cm/s <sup>2</sup>       | 1 pascal (Pa) = 1 N/m <sup>2</sup>  |
| 1 erg = 1 dyne·cm                    | 1 poundal = 1 lbm·ft/s <sup>2</sup> |
| 1 farad (F) = 1 C/V                  | 1 siemens (S) = 1 A/V               |
| 1 henry (H) = 1 Wb/A                 | 1 slug = 1 lbf·s <sup>2</sup> /ft   |
| 1 hertz (Hz) = 1 cycle/s             | 1 tesla (T) = 1 Wb/m <sup>2</sup>   |
| 1 joule (J) = 1 N·m                  | 1 volt (V) = 1 W/A                  |
| 1 lumen = 1 candela·steradian        | 1 watt (W) = 1 J/s                  |
| 1 lux = 1 lumen/m <sup>2</sup>       | 1 weber (Wb) = 1 V·s                |
| 1 newton (N) = 1 kg·m/s <sup>2</sup> |                                     |

## CONVERSION FACTORS

| Length   | Energy   |
|--|--|
| 1 m = 3.2808 ft = 39.37 in = 10 <sup>2</sup> cm = 10 <sup>10</sup> Å | 1 J = 1 N·m = 1 kg·m <sup>2</sup> /s <sup>2</sup> = 9.479 × 10 <sup>-4</sup> Btu |
| 1 cm = 0.0328 ft = 0.394 in = 10 <sup>-2</sup> m = 10 <sup>8</sup> Å | 1 kJ = 1000 J = 0.9479 Btu = 238.9 cal   |
| 1 mm = 10 <sup>-3</sup> m = 10 <sup>-1</sup> cm                      | 1 Btu = 1055.0 J = 1.055 kJ = 778.16 ft·lbf = 252 cal                            |
| 1 km = 1000 m = 0.6215 miles = 3281 ft                               | 1 cal = 4.186 J = 3.968 × 10 <sup>-3</sup> Btu                                   |
| 1 in = 2.540 cm = 0.0254 m   | 1 Cal (in food value) = 1 kcal = 4186 J = 3.968 Btu                              |
| 1 ft = 12 in = 0.3048 m  | 1 erg = 1 dyne·cm = 1 g·cm <sup>2</sup> /s <sup>2</sup> = 10 <sup>-7</sup> J     |
| 1 mile = 5280 ft = 1609.36 m = 1.609 km                              | 1 eV = 1.602 × 10 <sup>-19</sup> J   |

(Continued)

**CONVERSION FACTORS** (Continued)**Area**

$$1 \text{ m}^2 = 10^4 \text{ cm}^2 = 10.76 \text{ ft}^2 = 1550 \text{ in}^2$$

$$1 \text{ ft}^2 = 144 \text{ in}^2 = 0.0929 \text{ m}^2 = 929.05 \text{ cm}^2$$

$$1 \text{ cm}^2 = 10^{-4} \text{ m}^2 = 1.0764 \times 10^{-3} \text{ ft}^2 = 0.155 \text{ in}^2$$

$$1 \text{ in}^2 = 6.944 \times 10^{-3} \text{ ft}^2 = 6.4516 \times 10^{-4} \text{ m}^2 = 6.4516 \text{ cm}^2$$

**Volume**

$$1 \text{ m}^3 = 35.313 \text{ ft}^3 = 6.1023 \times 10^4 \text{ in}^3 = 1000 \text{ L} = 264.171 \text{ gal}$$

$$1 \text{ L} = 10^{-3} \text{ m}^3 = 0.0353 \text{ ft}^3 = 61.03 \text{ in}^3 = 0.2642 \text{ gal}$$

$$1 \text{ gal} = 231 \text{ in}^3 = 0.13368 \text{ ft}^3 = 3.785 \times 10^{-3} \text{ m}^3$$

$$1 \text{ ft}^3 = 1728 \text{ in}^3 = 28.3168 \text{ L} = 0.02832 \text{ m}^3 = 7.4805 \text{ gal}$$

$$1 \text{ in}^3 = 16.387 \text{ cm}^3 = 1.6387 \times 10^{-5} \text{ m}^3 = 4.329 \times 10^{-3} \text{ gal}$$

**Mass**

$$1 \text{ kg} = 1000 \text{ g} = 2.2046 \text{ lbm} = 0.0685 \text{ slug}$$

$$1 \text{ lbm} = 453.6 \text{ g} = 0.4536 \text{ kg} = 3.108 \times 10^{-2} \text{ slug}$$

$$1 \text{ slug} = 32.174 \text{ lbm} = 1.459 \times 10^4 \text{ g} = 14.594 \text{ kg}$$

**Force**

$$1 \text{ N} = 10^5 \text{ dyne} = 1 \text{ kg} \cdot \text{m/s}^2 = 0.225 \text{ lbf}$$

$$1 \text{ lbf} = 4.448 \text{ N} = 32.174 \text{ poundals}$$

$$1 \text{ poundal} = 0.138 \text{ N} = 3.108 \times 10^{-2} \text{ lbf}$$

**Power**

$$1 \text{ W} = 1 \text{ J/s} = 1 \text{ kg} \cdot \text{m}^2/\text{s}^3 = 3.412 \text{ Btu/h} = 1.3405 \times 10^{-3} \text{ hp}$$

$$1 \text{ kW} = 1000 \text{ W} = 3412 \text{ Btu/h} = 737.3 \text{ ft} \cdot \text{lbf/s} = 1.3405 \text{ hp}$$

$$1 \text{ Btu/h} = 0.293 \text{ W} = 0.2161 \text{ ft} \cdot \text{lbf/s} = 3.9293 \times 10^{-4} \text{ hp}$$

$$1 \text{ hp} = 550 \text{ ft} \cdot \text{lbf/s} = 33000 \text{ ft} \cdot \text{lbf/min} = 2545 \text{ Btu/h} = 746 \text{ W}$$

**Pressure**

$$1 \text{ Pa} = 1 \text{ N/m}^2 = 1 \text{ kg}/(\text{m} \cdot \text{s}^2) = 1.4504 \times 10^{-4} \text{ lbf/in}^2$$

$$1 \text{ lbf/in}^2 = 6894.76 \text{ Pa} = 0.068 \text{ atm} = 2.036 \text{ in Hg}$$

$$1 \text{ atm} = 14.696 \text{ lbf/in}^2 = 1.01325 \times 10^5 \text{ Pa}$$

$$= 101.325 \text{ kPa} = 760 \text{ mm Hg}$$

$$1 \text{ bar} = 10^5 \text{ Pa} = 0.987 \text{ atm} = 14.504 \text{ lbf/in}^2$$

$$1 \text{ dyne/cm}^2 = 0.1 \text{ Pa} = 10^{-6} \text{ bar} = 145.04 \times 10^{-7} \text{ lbf/in}^2$$

$$1 \text{ in Hg} = 3376.8 \text{ Pa} = 0.491 \text{ lbf/in}^2$$

$$1 \text{ in H}_2\text{O} = 248.8 \text{ Pa} = 0.0361 \text{ lbf/in}^2$$

**MISCELLANEOUS UNIT CONVERSIONS****Specific Heat Units**

$$1 \text{ Btu}/(\text{lbm} \cdot ^\circ\text{F}) = 1 \text{ Btu}/(\text{lbm} \cdot \text{R})$$

$$1 \text{ kJ}/(\text{kg} \cdot \text{K}) = 0.23884 \text{ Btu}/(\text{lbm} \cdot \text{R}) = 185.8 \text{ ft} \cdot \text{lbf}/(\text{lbm} \cdot \text{R})$$

$$1 \text{ Btu}/(\text{lbm} \cdot \text{R}) = 778.16 \text{ ft} \cdot \text{lbf}/(\text{lbm} \cdot \text{R}) = 4.186 \text{ kJ}/(\text{kg} \cdot \text{K})$$

**Energy Density Units**

$$1 \text{ kJ/kg} = 1000 \text{ m}^2/\text{s}^2 = 0.4299 \text{ Btu/lbm}$$

$$1 \text{ Btu/lbm} = 2.326 \text{ kJ/kg} = 2326 \text{ m}^2/\text{s}^2$$

**Energy Flux**

$$1 \text{ W/m}^2 = 0.317 \text{ Btu}/(\text{h} \cdot \text{ft}^2)$$

$$1 \text{ Btu}/(\text{h} \cdot \text{ft}^2) = 3.154 \text{ W/m}^2$$

**Heat Transfer Coefficient**

$$1 \text{ W}/(\text{m}^2 \cdot \text{K}) = 0.1761 \text{ Btu}/(\text{h} \cdot \text{ft}^2 \cdot \text{R})$$

$$1 \text{ Btu}/(\text{h} \cdot \text{ft}^2 \cdot \text{R}) = 5.679 \text{ W}/(\text{m}^2 \cdot \text{K})$$

**Thermal Conductivity**

$$1 \text{ W}/(\text{m} \cdot \text{K}) = 0.5778 \text{ Btu}/(\text{h} \cdot \text{ft} \cdot \text{R})$$

$$1 \text{ Btu}/(\text{h} \cdot \text{ft} \cdot \text{R}) = 1.731 \text{ W}/(\text{m} \cdot \text{K})$$

**Temperature**

$$T(^{\circ}\text{F}) = \frac{9}{5} T(^{\circ}\text{C}) + 32 = T(\text{R}) - 459.67$$

$$T(^{\circ}\text{C}) = \frac{5}{9} [T(^{\circ}\text{F}) - 32] = T(\text{K}) - 273.15$$

$$T(\text{R}) = \frac{9}{5} T(\text{K}) = (1.8)T(\text{K}) = T(^{\circ}\text{F}) + 459.67$$

$$T(\text{K}) = \frac{5}{9} T(\text{R}) = T(\text{R})/1.8 = T(^{\circ}\text{C}) + 273.15$$

**Density**

$$1 \text{ lbm/ft}^3 = 16.0187 \text{ kg/m}^3$$

$$1 \text{ kg/m}^3 = 0.062427 \text{ lbm/ft}^3 = 10^{-3} \text{ g/cm}^3$$

$$1 \text{ g/cm}^3 = 1 \text{ kg/L} = 62.4 \text{ lbm/ft}^3 = 10^3 \text{ kg/m}^3$$

**Viscosity**

$$1 \text{ Pa} \cdot \text{s} = 1 \text{ N} \cdot \text{s}/\text{m}^2 = 1 \text{ kg}/(\text{m} \cdot \text{s}) = 10 \text{ poise}$$

$$1 \text{ poise} = 1 \text{ dyne} \cdot \text{s}/\text{cm}^2 = 1 \text{ g}/(\text{cm} \cdot \text{s}) = 0.1 \text{ Pa} \cdot \text{s}$$

$$1 \text{ poise} = 2.09 \times 10^{-3} \text{ lbf} \cdot \text{s}/\text{ft}^2 = 6.72 \times 10^{-2} \text{ lbm}/(\text{ft} \cdot \text{s})$$

$$1 \text{ centipoise} = 0.01 \text{ poise} = 10^{-3} \text{ Pa} \cdot \text{s}$$

$$1 \text{ lbf} \cdot \text{s}/\text{ft}^2 = 1 \text{ slug}/(\text{ft} \cdot \text{s}) = 47.9 \text{ Pa} \cdot \text{s} = 479 \text{ poise}$$

$$1 \text{ stoke} = 1 \text{ cm}^2/\text{s} = 10^{-4} \text{ m}^2/\text{s} = 1.076 \times 10^{-3} \text{ ft}^2/\text{s}$$

$$1 \text{ centistoke} = 0.01 \text{ stoke} = 10^{-6} \text{ m}^2/\text{s} = 1.076 \times 10^{-5} \text{ ft}^2/\text{s}$$

$$1 \text{ m}^2/\text{s} = 10^4 \text{ stoke} = 10^6 \text{ centistoke} = 10.76 \text{ ft}^2/\text{s}$$

TABLE A-17 Properties of Saturated Propane (Liquid–Vapor): Pressure Table

| Press.<br>bar | Temp.<br>°C | Specific Volume<br>m <sup>3</sup> /kg |                        | Internal Energy<br>kJ/kg |                        | Enthalpy<br>kJ/kg       |                   |                        | Entropy<br>kJ/kg · K    |                        | Press.<br>bar |
|---------------|-------------|---------------------------------------|------------------------|--------------------------|------------------------|-------------------------|-------------------|------------------------|-------------------------|------------------------|---------------|
|               |             | Sat.<br>Liquid<br>$v_f \times 10^3$   | Sat.<br>Vapor<br>$v_g$ | Sat.<br>Liquid<br>$u_f$  | Sat.<br>Vapor<br>$u_g$ | Sat.<br>Liquid<br>$h_f$ | Evap.<br>$h_{fg}$ | Sat.<br>Vapor<br>$h_g$ | Sat.<br>Liquid<br>$s_f$ | Sat.<br>Vapor<br>$s_g$ |               |
| 0.05          | −93.28      | 1.570                                 | 6.752                  | −114.6                   | 326.0                  | −114.6                  | 474.4             | 359.8                  | −0.556                  | 2.081                  | 0.05          |
| 0.10          | −83.87      | 1.594                                 | 3.542                  | −95.1                    | 335.4                  | −95.1                   | 465.9             | 370.8                  | −0.450                  | 2.011                  | 0.10          |
| 0.25          | −69.55      | 1.634                                 | 1.513                  | −64.9                    | 350.0                  | −64.9                   | 452.7             | 387.8                  | −0.297                  | 1.927                  | 0.25          |
| 0.50          | −56.93      | 1.672                                 | 0.7962                 | −37.7                    | 363.1                  | −37.6                   | 440.5             | 402.9                  | −0.167                  | 1.871                  | 0.50          |
| 0.75          | −48.68      | 1.698                                 | 0.5467                 | −19.6                    | 371.8                  | −19.5                   | 432.3             | 412.8                  | −0.085                  | 1.841                  | 0.75          |
| 1.00          | −42.38      | 1.719                                 | 0.4185                 | −5.6                     | 378.5                  | −5.4                    | 425.7             | 420.3                  | −0.023                  | 1.822                  | 1.00          |
| 2.00          | −25.43      | 1.781                                 | 0.2192                 | 33.1                     | 396.6                  | 33.5                    | 406.9             | 440.4                  | 0.139                   | 1.782                  | 2.00          |
| 3.00          | −14.16      | 1.826                                 | 0.1496                 | 59.8                     | 408.7                  | 60.3                    | 393.3             | 453.6                  | 0.244                   | 1.762                  | 3.00          |
| 4.00          | −5.46       | 1.865                                 | 0.1137                 | 80.8                     | 418.0                  | 81.5                    | 382.0             | 463.5                  | 0.324                   | 1.751                  | 4.00          |
| 5.00          | 1.74        | 1.899                                 | 0.09172                | 98.6                     | 425.7                  | 99.5                    | 372.1             | 471.6                  | 0.389                   | 1.743                  | 5.00          |
| 6.00          | 7.93        | 1.931                                 | 0.07680                | 114.2                    | 432.2                  | 115.3                   | 363.0             | 478.3                  | 0.446                   | 1.737                  | 6.00          |
| 7.00          | 13.41       | 1.960                                 | 0.06598                | 128.2                    | 438.0                  | 129.6                   | 354.6             | 484.2                  | 0.495                   | 1.733                  | 7.00          |
| 8.00          | 18.33       | 1.989                                 | 0.05776                | 141.0                    | 443.1                  | 142.6                   | 346.7             | 489.3                  | 0.540                   | 1.729                  | 8.00          |
| 9.00          | 22.82       | 2.016                                 | 0.05129                | 152.9                    | 447.6                  | 154.7                   | 339.1             | 493.8                  | 0.580                   | 1.726                  | 9.00          |
| 10.00         | 26.95       | 2.043                                 | 0.04606                | 164.0                    | 451.8                  | 166.1                   | 331.8             | 497.9                  | 0.618                   | 1.723                  | 10.00         |
| 11.00         | 30.80       | 2.070                                 | 0.04174                | 174.5                    | 455.6                  | 176.8                   | 324.7             | 501.5                  | 0.652                   | 1.721                  | 11.00         |
| 12.00         | 34.39       | 2.096                                 | 0.03810                | 184.4                    | 459.1                  | 187.0                   | 317.8             | 504.8                  | 0.685                   | 1.718                  | 12.00         |
| 13.00         | 37.77       | 2.122                                 | 0.03499                | 193.9                    | 462.2                  | 196.7                   | 311.0             | 507.7                  | 0.716                   | 1.716                  | 13.00         |
| 14.00         | 40.97       | 2.148                                 | 0.03231                | 203.0                    | 465.2                  | 206.0                   | 304.4             | 510.4                  | 0.745                   | 1.714                  | 14.00         |
| 15.00         | 44.01       | 2.174                                 | 0.02997                | 211.7                    | 467.9                  | 215.0                   | 297.9             | 512.9                  | 0.772                   | 1.712                  | 15.00         |
| 16.00         | 46.89       | 2.200                                 | 0.02790                | 220.1                    | 470.4                  | 223.6                   | 291.4             | 515.0                  | 0.799                   | 1.710                  | 16.00         |
| 17.00         | 49.65       | 2.227                                 | 0.02606                | 228.3                    | 472.7                  | 232.0                   | 285.0             | 517.0                  | 0.824                   | 1.707                  | 17.00         |
| 18.00         | 52.30       | 2.253                                 | 0.02441                | 236.2                    | 474.9                  | 240.2                   | 278.6             | 518.8                  | 0.849                   | 1.705                  | 18.00         |
| 19.00         | 54.83       | 2.280                                 | 0.02292                | 243.8                    | 476.9                  | 248.2                   | 272.2             | 520.4                  | 0.873                   | 1.703                  | 19.00         |
| 20.00         | 57.27       | 2.308                                 | 0.02157                | 251.3                    | 478.7                  | 255.9                   | 265.9             | 521.8                  | 0.896                   | 1.700                  | 20.00         |
| 22.00         | 61.90       | 2.364                                 | 0.01921                | 265.8                    | 481.7                  | 271.0                   | 253.0             | 524.0                  | 0.939                   | 1.695                  | 22.00         |
| 24.00         | 66.21       | 2.424                                 | 0.01721                | 279.7                    | 484.3                  | 285.5                   | 240.1             | 525.6                  | 0.981                   | 1.688                  | 24.00         |
| 26.00         | 70.27       | 2.487                                 | 0.01549                | 293.1                    | 486.2                  | 299.6                   | 226.9             | 526.5                  | 1.021                   | 1.681                  | 26.00         |
| 28.00         | 74.10       | 2.555                                 | 0.01398                | 306.2                    | 487.5                  | 313.4                   | 213.2             | 526.6                  | 1.060                   | 1.673                  | 28.00         |
| 30.00         | 77.72       | 2.630                                 | 0.01263                | 319.2                    | 488.1                  | 327.1                   | 198.9             | 526.0                  | 1.097                   | 1.664                  | 30.00         |
| 35.00         | 86.01       | 2.862                                 | 0.009771               | 351.4                    | 486.3                  | 361.4                   | 159.1             | 520.5                  | 1.190                   | 1.633                  | 35.00         |
| 40.00         | 93.38       | 3.279                                 | 0.007151               | 387.9                    | 474.7                  | 401.0                   | 102.3             | 503.3                  | 1.295                   | 1.574                  | 40.00         |
| 42.48         | 96.70       | 4.535                                 | 0.004535               | 434.9                    | 434.9                  | 454.2                   | 0.0               | 454.2                  | 1.437                   | 1.437                  | 42.48         |

TABLE A-18 Properties of Superheated Propane

| $T$<br>°C   | $v$<br>m <sup>3</sup> /kg | $u$<br>kJ/kg | $h$<br>kJ/kg | $s$<br>kJ/kg · K | $v$<br>m <sup>3</sup> /kg   | $u$<br>kJ/kg | $h$<br>kJ/kg | $s$<br>kJ/kg · K |
|---|---------------------------|--------------|--------------|------------------|---|--------------|--------------|------------------|
| $p = 0.05 \text{ bar} = 0.005 \text{ MPa}$<br>( $T_{\text{sat}} = -93.28^\circ\text{C}$ ) |                           |              |              |                  | $p = 0.1 \text{ bar} = 0.01 \text{ MPa}$<br>( $T_{\text{sat}} = -83.87^\circ\text{C}$ ) |              |              |                  |
| Sat.  | 6.752                     | 326.0        | 359.8        | 2.081            | 3.542   | 367.3        | 370.8        | 2.011            |
| −90   | 6.877                     | 329.4        | 363.8        | 2.103            |   |              |              |                  |
| −80   | 7.258                     | 339.8        | 376.1        | 2.169            | 3.617   | 339.5        | 375.7        | 2.037            |
| −70   | 7.639                     | 350.6        | 388.8        | 2.233            | 3.808   | 350.3        | 388.4        | 2.101            |
| −60   | 8.018                     | 361.8        | 401.9        | 2.296            | 3.999   | 361.5        | 401.5        | 2.164            |
| −50   | 8.397                     | 373.3        | 415.3        | 2.357            | 4.190   | 373.1        | 415.0        | 2.226            |
| −40   | 8.776                     | 385.1        | 429.0        | 2.418            | 4.380   | 385.0        | 428.8        | 2.286            |
| −30   | 9.155                     | 397.4        | 443.2        | 2.477            | 4.570   | 397.3        | 443.0        | 2.346            |
| −20   | 9.533                     | 410.1        | 457.8        | 2.536            | 4.760   | 410.0        | 457.6        | 2.405            |
| −10   | 9.911                     | 423.2        | 472.8        | 2.594            | 4.950   | 423.1        | 472.6        | 2.463            |
| 0   | 10.29                     | 436.8        | 488.2        | 2.652            | 5.139   | 436.7        | 488.1        | 2.520            |
| 10  | 10.67                     | 450.8        | 504.1        | 2.709            | 5.329   | 450.6        | 503.9        | 2.578            |
| 20  | 11.05                     | 270.6        | 520.4        | 2.765            | 5.518   | 465.1        | 520.3        | 2.634            |
| $p = 0.5 \text{ bar} = 0.05 \text{ MPa}$<br>( $T_{\text{sat}} = -56.93^\circ\text{C}$ )   |                           |              |              |                  | $p = 1.0 \text{ bar} = 0.1 \text{ MPa}$<br>( $T_{\text{sat}} = -42.38^\circ\text{C}$ )  |              |              |                  |
| Sat.  | 0.796                     | 363.1        | 402.9        | 1.871            | 0.4185  | 378.5        | 420.3        | 1.822            |
| −50   | 0.824                     | 371.3        | 412.5        | 1.914            |   |              |              |                  |
| −40   | 0.863                     | 383.4        | 426.6        | 1.976            | 0.4234  | 381.5        | 423.8        | 1.837            |
| −30   | 0.903                     | 396.0        | 441.1        | 2.037            | 0.4439  | 394.2        | 438.6        | 1.899            |
| −20   | 0.942                     | 408.8        | 455.9        | 2.096            | 0.4641  | 407.3        | 453.7        | 1.960            |
| −10   | 0.981                     | 422.1        | 471.1        | 2.155            | 0.4842  | 420.7        | 469.1        | 2.019            |
| 0   | 1.019                     | 435.8        | 486.7        | 2.213            | 0.5040  | 434.4        | 484.8        | 2.078            |
| 10  | 1.058                     | 449.8        | 502.7        | 2.271            | 0.5238  | 448.6        | 501.0        | 2.136            |
| 20  | 1.096                     | 464.3        | 519.1        | 2.328            | 0.5434  | 463.3        | 517.6        | 2.194            |
| 30  | 1.135                     | 479.2        | 535.9        | 2.384            | 0.5629  | 478.2        | 534.5        | 2.251            |
| 40  | 1.173                     | 494.6        | 553.2        | 2.440            | 0.5824  | 493.7        | 551.9        | 2.307            |
| 50  | 1.211                     | 510.4        | 570.9        | 2.496            | 0.6018  | 509.5        | 569.7        | 2.363            |
| 60  | 1.249                     | 526.7        | 589.1        | 2.551            | 0.6211  | 525.8        | 587.9        | 2.419            |
| $p = 2.0 \text{ bar} = 0.2 \text{ MPa}$<br>( $T_{\text{sat}} = -25.43^\circ\text{C}$ )    |                           |              |              |                  | $p = 3.0 \text{ bar} = 0.3 \text{ MPa}$<br>( $T_{\text{sat}} = -14.16^\circ\text{C}$ )  |              |              |                  |
| Sat.  | 0.2192                    | 396.6        | 440.4        | 1.782            | 0.1496  | 408.7        | 453.6        | 1.762            |
| −20   | 0.2251                    | 404.0        | 449.0        | 1.816            |   |              |              |                  |
| −10   | 0.2358                    | 417.7        | 464.9        | 1.877            | 0.1527  | 414.7        | 460.5        | 1.789            |
| 0   | 0.2463                    | 431.8        | 481.1        | 1.938            | 0.1602  | 429.0        | 477.1        | 1.851            |
| 10  | 0.2566                    | 446.3        | 497.6        | 1.997            | 0.1674  | 443.8        | 494.0        | 1.912            |
| 20  | 0.2669                    | 461.1        | 514.5        | 2.056            | 0.1746  | 458.8        | 511.2        | 1.971            |
| 30  | 0.2770                    | 476.3        | 531.7        | 2.113            | 0.1816  | 474.2        | 528.7        | 2.030            |
| 40  | 0.2871                    | 491.9        | 549.3        | 2.170            | 0.1885  | 490.1        | 546.6        | 2.088            |
| 50  | 0.2970                    | 507.9        | 567.3        | 2.227            | 0.1954  | 506.2        | 564.8        | 2.145            |
| 60  | 0.3070                    | 524.3        | 585.7        | 2.283            | 0.2022  | 522.7        | 583.4        | 2.202            |
| 70  | 0.3169                    | 541.1        | 604.5        | 2.339            | 0.2090  | 539.6        | 602.3        | 2.258            |
| 80  | 0.3267                    | 558.4        | 623.7        | 2.394            | 0.2157  | 557.0        | 621.7        | 2.314            |
| 90  | 0.3365                    | 576.1        | 643.4        | 2.449            | 0.2223  | 574.8        | 641.5        | 2.369            |

TABLE A-18 (Continued)

| $T$<br>°C   | $v$<br>m <sup>3</sup> /kg | $u$<br>kJ/kg | $h$<br>kJ/kg | $s$<br>kJ/kg · K | $v$<br>m <sup>3</sup> /kg   | $u$<br>kJ/kg | $h$<br>kJ/kg | $s$<br>kJ/kg · K |
|---|---------------------------|--------------|--------------|------------------|---|--------------|--------------|------------------|
| $p = 4.0 \text{ bar} = 0.4 \text{ MPa}$<br>( $T_{\text{sat}} = -5.46^\circ\text{C}$ ) |                           |              |              |                  | $p = 5.0 \text{ bar} = 0.5 \text{ MPa}$<br>( $T_{\text{sat}} = 1.74^\circ\text{C}$ )  |              |              |                  |
| Sat.  | 0.1137                    | 418.0        | 463.5        | 1.751            | 0.09172   | 425.7        | 471.6        | 1.743            |
| 0   | 0.1169                    | 426.1        | 472.9        | 1.786            |   |              |              |                  |
| 10  | 0.1227                    | 441.2        | 490.3        | 1.848            | 0.09577   | 438.4        | 486.3        | 1.796            |
| 20  | 0.1283                    | 456.6        | 507.9        | 1.909            | 0.1005  | 454.1        | 504.3        | 1.858            |
| 30  | 0.1338                    | 472.2        | 525.7        | 1.969            | 0.1051  | 470.0        | 522.5        | 1.919            |
| 40  | 0.1392                    | 488.1        | 543.8        | 2.027            | 0.1096  | 486.1        | 540.9        | 1.979            |
| 50  | 0.1445                    | 504.4        | 562.2        | 2.085            | 0.1140  | 502.5        | 559.5        | 2.038            |
| 60  | 0.1498                    | 521.1        | 581.0        | 2.143            | 0.1183  | 519.4        | 578.5        | 2.095            |
| 70  | 0.1550                    | 538.1        | 600.1        | 2.199            | 0.1226  | 536.6        | 597.9        | 2.153            |
| 80  | 0.1601                    | 555.7        | 619.7        | 2.255            | 0.1268  | 554.1        | 617.5        | 2.209            |
| 90  | 0.1652                    | 573.5        | 639.6        | 2.311            | 0.1310  | 572.1        | 637.6        | 2.265            |
| 100   | 0.1703                    | 591.8        | 659.9        | 2.366            | 0.1351  | 590.5        | 658.0        | 2.321            |
| 110   | 0.1754                    | 610.4        | 680.6        | 2.421            | 0.1392  | 609.3        | 678.9        | 2.376            |
| $p = 6.0 \text{ bar} = 0.6 \text{ MPa}$<br>( $T_{\text{sat}} = 7.93^\circ\text{C}$ )  |                           |              |              |                  | $p = 7.0 \text{ bar} = 0.7 \text{ MPa}$<br>( $T_{\text{sat}} = 13.41^\circ\text{C}$ ) |              |              |                  |
| Sat.  | 0.07680                   | 432.2        | 478.3        | 1.737            | 0.06598   | 438.0        | 484.2        | 1.733            |
| 10  | 0.07769                   | 435.6        | 482.2        | 1.751            |   |              |              |                  |
| 20  | 0.08187                   | 451.5        | 500.6        | 1.815            | 0.06847   | 448.8        | 496.7        | 1.776            |
| 30  | 0.08588                   | 467.7        | 519.2        | 1.877            | 0.07210   | 465.2        | 515.7        | 1.840            |
| 40  | 0.08978                   | 484.0        | 537.9        | 1.938            | 0.07558   | 481.9        | 534.8        | 1.901            |
| 50  | 0.09357                   | 500.7        | 556.8        | 1.997            | 0.07896   | 498.7        | 554.0        | 1.962            |
| 60  | 0.09729                   | 517.6        | 576.0        | 2.056            | 0.08225   | 515.9        | 573.5        | 2.021            |
| 70  | 0.1009                    | 535.0        | 595.5        | 2.113            | 0.08547   | 533.4        | 593.2        | 2.079            |
| 80  | 0.1045                    | 552.7        | 615.4        | 2.170            | 0.08863   | 551.2        | 613.2        | 2.137            |
| 90  | 0.1081                    | 570.7        | 635.6        | 2.227            | 0.09175   | 569.4        | 633.6        | 2.194            |
| 100   | 0.1116                    | 589.2        | 656.2        | 2.283            | 0.09482   | 587.9        | 654.3        | 2.250            |
| 110   | 0.1151                    | 608.0        | 677.1        | 2.338            | 0.09786   | 606.8        | 675.3        | 2.306            |
| 120   | 0.1185                    | 627.3        | 698.4        | 2.393            | 0.1009  | 626.2        | 696.8        | 2.361            |
| $p = 8.0 \text{ bar} = 0.8 \text{ MPa}$<br>( $T_{\text{sat}} = 18.33^\circ\text{C}$ ) |                           |              |              |                  | $p = 9.0 \text{ bar} = 0.9 \text{ MPa}$<br>( $T_{\text{sat}} = 22.82^\circ\text{C}$ ) |              |              |                  |
| Sat.  | 0.05776                   | 443.1        | 489.3        | 1.729            | 0.05129   | 447.2        | 493.8        | 1.726            |
| 20  | 0.05834                   | 445.9        | 492.6        | 1.740            |   |              |              |                  |
| 30  | 0.06170                   | 462.7        | 512.1        | 1.806            | 0.05355   | 460.0        | 508.2        | 1.774            |
| 40  | 0.06489                   | 479.6        | 531.5        | 1.869            | 0.05653   | 477.2        | 528.1        | 1.839            |
| 50  | 0.06796                   | 496.7        | 551.1        | 1.930            | 0.05938   | 494.7        | 548.1        | 1.901            |
| 60  | 0.07094                   | 514.0        | 570.8        | 1.990            | 0.06213   | 512.2        | 568.1        | 1.962            |
| 70  | 0.07385                   | 531.6        | 590.7        | 2.049            | 0.06479   | 530.0        | 588.3        | 2.022            |
| 80  | 0.07669                   | 549.6        | 611.0        | 2.107            | 0.06738   | 548.1        | 608.7        | 2.081            |
| 90  | 0.07948                   | 567.9        | 631.5        | 2.165            | 0.06992   | 566.5        | 629.4        | 2.138            |
| 100   | 0.08222                   | 586.5        | 652.3        | 2.221            | 0.07241   | 585.2        | 650.4        | 2.195            |
| 110   | 0.08493                   | 605.6        | 673.5        | 2.277            | 0.07487   | 604.3        | 671.7        | 2.252            |
| 120   | 0.08761                   | 625.0        | 695.1        | 2.333            | 0.07729   | 623.7        | 693.3        | 2.307            |
| 130   | 0.09026                   | 644.8        | 717.0        | 2.388            | 0.07969   | 643.6        | 715.3        | 2.363            |
| 140   | 0.09289                   | 665.0        | 739.3        | 2.442            | 0.08206   | 663.8        | 737.7        | 2.418            |



TABLE A-18 (Continued)

| $T$<br>°C  | $v$<br>m <sup>3</sup> /kg | $u$<br>kJ/kg | $h$<br>kJ/kg | $s$<br>kJ/kg · K | $v$<br>m <sup>3</sup> /kg  | $u$<br>kJ/kg | $h$<br>kJ/kg | $s$<br>kJ/kg · K |
|--|---------------------------|--------------|--------------|------------------|--|--------------|--------------|------------------|
| $p = 10.0 \text{ bar} = 1.0 \text{ MPa}$<br>( $T_{\text{sat}} = 26.95^\circ\text{C}$ ) |                           |              |              |                  | $p = 12.0 \text{ bar} = 1.2 \text{ MPa}$<br>( $T_{\text{sat}} = 34.39^\circ\text{C}$ ) |              |              |                  |
| Sat.   | 0.04606                   | 451.8        | 497.9        | 1.723            | 0.03810  | 459.1        | 504.8        | 1.718            |
| 30   | 0.04696                   | 457.1        | 504.1        | 1.744            |  |              |              |                  |
| 40   | 0.04980                   | 474.8        | 524.6        | 1.810            | 0.03957  | 469.4        | 516.9        | 1.757            |
| 50   | 0.05248                   | 492.4        | 544.9        | 1.874            | 0.04204  | 487.8        | 538.2        | 1.824            |
| 60   | 0.05505                   | 510.2        | 565.2        | 1.936            | 0.04436  | 506.1        | 559.3        | 1.889            |
| 70   | 0.05752                   | 528.2        | 585.7        | 1.997            | 0.04657  | 524.4        | 580.3        | 1.951            |
| 80   | 0.05992                   | 546.4        | 606.3        | 2.056            | 0.04869  | 543.1        | 601.5        | 2.012            |
| 90   | 0.06226                   | 564.9        | 627.2        | 2.114            | 0.05075  | 561.8        | 622.7        | 2.071            |
| 100  | 0.06456                   | 583.7        | 648.3        | 2.172            | 0.05275  | 580.9        | 644.2        | 2.129            |
| 110  | 0.06681                   | 603.0        | 669.8        | 2.228            | 0.05470  | 600.4        | 666.0        | 2.187            |
| 120  | 0.06903                   | 622.6        | 691.6        | 2.284            | 0.05662  | 620.1        | 688.0        | 2.244            |
| 130  | 0.07122                   | 642.5        | 713.7        | 2.340            | 0.05851  | 640.1        | 710.3        | 2.300            |
| 140  | 0.07338                   | 662.8        | 736.2        | 2.395            | 0.06037  | 660.6        | 733.0        | 2.355            |
| $p = 14.0 \text{ bar} = 1.4 \text{ MPa}$<br>( $T_{\text{sat}} = 40.97^\circ\text{C}$ ) |                           |              |              |                  | $p = 16.0 \text{ bar} = 1.6 \text{ MPa}$<br>( $T_{\text{sat}} = 46.89^\circ\text{C}$ ) |              |              |                  |
| Sat.   | 0.03231                   | 465.2        | 510.4        | 1.714            | 0.02790  | 470.4        | 515.0        | 1.710            |
| 50   | 0.03446                   | 482.6        | 530.8        | 1.778            | 0.02861  | 476.7        | 522.5        | 1.733            |
| 60   | 0.03664                   | 501.6        | 552.9        | 1.845            | 0.03075  | 496.6        | 545.8        | 1.804            |
| 70   | 0.03869                   | 520.4        | 574.6        | 1.909            | 0.03270  | 516.2        | 568.5        | 1.871            |
| 80   | 0.04063                   | 539.4        | 596.3        | 1.972            | 0.03453  | 535.7        | 590.9        | 1.935            |
| 90   | 0.04249                   | 558.6        | 618.1        | 2.033            | 0.03626  | 555.2        | 613.2        | 1.997            |
| 100  | 0.04429                   | 577.9        | 639.9        | 2.092            | 0.03792  | 574.8        | 635.5        | 2.058            |
| 110  | 0.04604                   | 597.5        | 662.0        | 2.150            | 0.03952  | 594.7        | 657.9        | 2.117            |
| 120  | 0.04774                   | 617.5        | 684.3        | 2.208            | 0.04107  | 614.8        | 680.5        | 2.176            |
| 130  | 0.04942                   | 637.7        | 706.9        | 2.265            | 0.04259  | 635.3        | 703.4        | 2.233            |
| 140  | 0.05106                   | 658.3        | 729.8        | 2.321            | 0.04407  | 656.0        | 726.5        | 2.290            |
| 150  | 0.05268                   | 679.2        | 753.0        | 2.376            | 0.04553  | 677.1        | 749.9        | 2.346            |
| 160  | 0.05428                   | 700.5        | 776.5        | 2.431            | 0.04696  | 698.5        | 773.6        | 2.401            |
| $p = 18.0 \text{ bar} = 1.8 \text{ MPa}$<br>( $T_{\text{sat}} = 52.30^\circ\text{C}$ ) |                           |              |              |                  | $p = 20.0 \text{ bar} = 2.0 \text{ MPa}$<br>( $T_{\text{sat}} = 57.27^\circ\text{C}$ ) |              |              |                  |
| Sat.   | 0.02441                   | 474.9        | 518.8        | 1.705            | 0.02157  | 478.7        | 521.8        | 1.700            |
| 60   | 0.02606                   | 491.1        | 538.0        | 1.763            | 0.02216  | 484.8        | 529.1        | 1.722            |
| 70   | 0.02798                   | 511.4        | 561.8        | 1.834            | 0.02412  | 506.3        | 554.5        | 1.797            |
| 80   | 0.02974                   | 531.6        | 585.1        | 1.901            | 0.02585  | 527.1        | 578.8        | 1.867            |
| 90   | 0.03138                   | 551.5        | 608.0        | 1.965            | 0.02744  | 547.6        | 602.5        | 1.933            |
| 100  | 0.03293                   | 571.5        | 630.8        | 2.027            | 0.02892  | 568.1        | 625.9        | 1.997            |
| 110  | 0.03443                   | 591.7        | 653.7        | 2.087            | 0.03033  | 588.5        | 649.2        | 2.059            |
| 120  | 0.03586                   | 612.1        | 676.6        | 2.146            | 0.03169  | 609.2        | 672.6        | 2.119            |
| 130  | 0.03726                   | 632.7        | 699.8        | 2.204            | 0.03299  | 630.0        | 696.0        | 2.178            |
| 140  | 0.03863                   | 653.6        | 723.1        | 2.262            | 0.03426  | 651.2        | 719.7        | 2.236            |
| 150  | 0.03996                   | 674.8        | 746.7        | 2.318            | 0.03550  | 672.5        | 743.5        | 2.293            |
| 160  | 0.04127                   | 696.3        | 770.6        | 2.374            | 0.03671  | 694.2        | 767.6        | 2.349            |
| 170  | 0.04256                   | 718.2        | 794.8        | 2.429            | 0.03790  | 716.2        | 792.0        | 2.404            |
| 180  | 0.04383                   | 740.4        | 819.3        | 2.484            | 0.03907  | 738.5        | 816.6        | 2.459            |