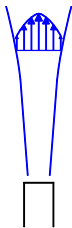


7. Turbulence

Turbulent Jet

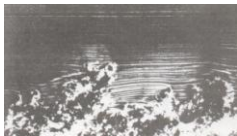


Instantaneous

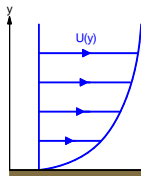


Mean

Turbulent Boundary Layer



Instantaneous



Mean

What is Turbulence?

- A “random”, 3-d, time-dependent eddying motion with many scales, superposed on an often drastically simpler **mean** flow
- A solution of the Navier-Stokes equations
- The natural state at **high Reynolds numbers**
- An efficient transporter and **mixer**
- A major source of **energy loss**
- A significant influence on **drag**:
 - **increases frictional drag** in non-separated flow
 - delays, or sometimes prevents, boundary-layer separation on curved surfaces, so **reducing pressure drag**.
- “The last great unsolved problem of classical physics”

Flow Regimes

- **Laminar:**
 - smooth
 - **no mixing** of fluid
 - momentum transfer by **viscous forces**
- **Turbulent:**
 - chaotic
 - **mixing** of fluid
 - momentum transfer mainly by **net effect of intermingling**



Regime determined by **Reynolds number**: $Re = \frac{\rho UL}{\mu} = \frac{UL}{\nu}$

‘Low’ Re \Rightarrow laminar; ‘high’ Re \Rightarrow turbulent

‘High’ or ‘low’ depends on the flow and the choice of U and L

Reynolds’ Decomposition

mean fluctuation

$$u = \bar{u} + u'$$
$$v = \bar{v} + v'$$
$$p = \bar{p} + p'$$

Alternative Notations

- **Overbar** for mean, **prime** for fluctuation:
 $\bar{u} + u'$ $-\rho \bar{u}'v'$
- **Upper case** for mean, **lower case** for fluctuation:
 $U + u$ $-\rho uv$

Reynolds Averaging

$u = \bar{u} + u'$ $\bar{u}' = 0$

Variance: $\overline{u^2} = \bar{u}^2 + \overline{u'^2}$

Covariance: $\overline{uv} = \bar{u} \bar{v} + \overline{u'v'}$

Effect of Turbulence on the Mean Flow

(i) Mass

Mass flux: $\rho v A$



Average mass flux: $\rho \bar{v} A$

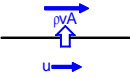
The **mean** velocity satisfies the same continuity equation as the **instantaneous** velocity

Effect of Turbulence on the Mean Flow

(ii) Momentum

(*) momentum flux:

$$(\rho v A)u = \rho(uv)A$$



Average momentum flux :

$$\overline{(\rho v A)u} = \rho(\overline{u \bar{v}} + \overline{u'v'})A$$

extra term

Net rate of transport of momentum $\rho \overline{u'v'}A$ from LOWER to UPPER ...

... is equivalent to $-\rho \overline{u'v'}A$ from UPPER to LOWER ...

... has the same **dynamic** effect as a **stress** $-\rho \overline{u'v'}$

The **mean** velocity satisfies the same momentum equation as the **instantaneous** velocity, except for additional **apparent** stresses; e.g.

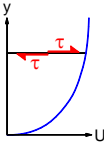
$$-\rho \overline{u'v'} \quad -\rho \overline{u'u'}$$

These are called the **Reynolds stresses**

Total Stress

In simple shear:

$$\tau = \underbrace{\mu \frac{\partial u}{\partial y}}_{\text{viscous stress}} + \underbrace{-\rho \overline{u'v'}}_{\text{turbulent stress}}$$

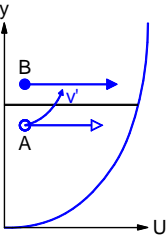


τ may be regarded as EITHER:

- the **force** per unit area exerted by upper on lower fluid
- OR
- the **rate of transport of momentum** per unit area from upper to lower fluid

The **dynamic** effect (average rate of transfer of momentum) is the same

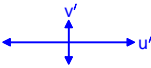
Turbulent Transport



Velocity Fluctuations

Normal stresses:

$$\overline{u'^2}, \overline{v'^2}, \overline{w'^2}$$



Shear stresses:

$$\overline{v'u'}, \overline{w'u'}, \overline{u'v'}$$

Turbulent kinetic energy: $k = \frac{1}{2}(\overline{u'^2} + \overline{v'^2} + \overline{w'^2})$

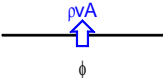
Turbulence intensity: $\frac{\text{root-mean-square fluctuation}}{\text{mean velocity}} = \frac{u'_{rms}}{U} = \frac{\sqrt{\frac{2}{3}k}}{U}$

Effect of Turbulence on the Mean Flow

(iii) General Scalar

Scalar flux:

$$(\rho v A) \phi = \rho(\bar{v} \phi) A$$



Average scalar flux:

$$(\rho v A) \phi = \rho(\bar{v} \bar{\phi} + \overline{v' \phi'}) A$$

extra term

The **mean** concentration satisfies the same transport equation as the **instantaneous** concentration, except for the addition of **turbulent fluxes**

$$\rho \overline{v' \phi'}$$

The Closure Problem

- To close the **mean** flow equations one must specify the **Reynolds stresses**

$$-\rho \overline{u'^2}, -\rho \overline{u'v'}, \dots$$

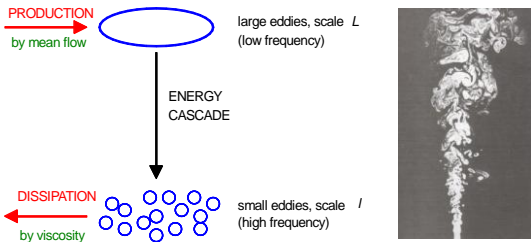
and other turbulent fluxes

- A means of doing so is called a **turbulence model** or **turbulence closure**
- The simplest model assumes that the turbulent stress can be modelled similarly to the viscous stress. In simple shear:

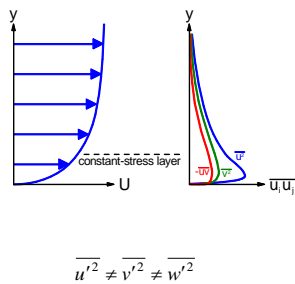
$$-\rho \overline{u'v'} = \mu_r \frac{\partial U}{\partial y}$$

This is called an **eddy-viscosity model**

Turbulence Energy

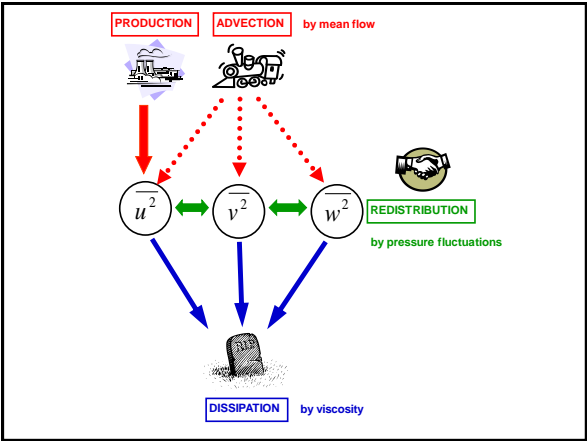


Anisotropy



Turbulence Transport

- Turbulence is transported by the flow
- Each individual Reynolds stress satisfies its own scalar-transport equation
- The “source” term is a balance between:
 - **production** by mean-velocity gradients
 - **dissipation** by viscosity
 - **redistribution** by pressure fluctuations
- Turbulence **anisotropy** is a result of:
 - anisotropic production by particular velocity gradients
 - selective damping of wall-normal fluctuations



Production of Turbulence Energy

$$P_{11} = -2(\overline{uu} \frac{\partial U}{\partial x} + \overline{uv} \frac{\partial U}{\partial y} + \overline{uw} \frac{\partial U}{\partial z})$$
$$P_{12} = -(\overline{uu} \frac{\partial V}{\partial x} + \overline{uv} \frac{\partial V}{\partial y} + \overline{uw} \frac{\partial V}{\partial z}) - (\overline{vu} \frac{\partial U}{\partial x} + \overline{vv} \frac{\partial U}{\partial y} + \overline{vw} \frac{\partial U}{\partial z})$$

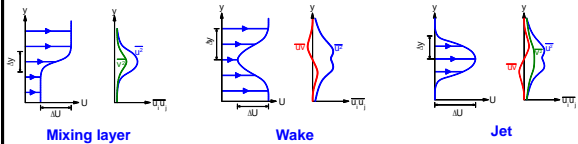
$$P_{ij} = -(\overline{u_i u_j} \frac{\partial U_j}{\partial x_i} + \overline{u_j u_i} \frac{\partial U_i}{\partial x_j})$$

$$P^{(k)} = \frac{1}{2}(P_{11} + P_{22} + P_{33})$$

In **simple shear**: $P_{11} = -2\overline{uv} \frac{\partial U}{\partial y}$, $P_{22} = P_{33} = 0$ Energy is preferentially supplied to the streamwise normal stress \overline{uu}

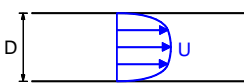
$$P^{(k)} = -\overline{uv} \frac{\partial U}{\partial y}$$

Free Shear Flows

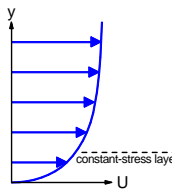


- Maximum turbulence where $|\partial U / \partial y|$ largest
- \overline{uv} has the opposite sign to $\partial U / \partial y$ and vanishes where this is zero
- Turbulence is anisotropic: $\overline{u^2} > \overline{v^2}$

Wall-Bounded Flows



Pipe flow

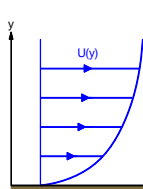


Flat-plate boundary layer

Parameters in Wall-Bounded Flows

Wall shear stress: τ_w

Friction velocity: $u_\tau = \sqrt{\tau_w/\rho}$



Non-dimensional height: $y^+ = \frac{y u_\tau}{\nu}$

Non-dimensional velocity: $U^+ = \frac{U}{u_\tau}$

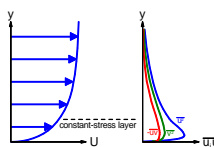
} wall units

Key Regions of a Turbulent Boundary Layer

Viscous sublayer ($y^+ < 5$):

- viscous stress dominant

$$\tau_w = \mu \frac{\partial U}{\partial y} \Rightarrow U = \frac{\tau_w}{\mu} y$$



Log layer ($30 < y^+ < 500$):

- direct effect of viscosity negligible

$$\frac{\partial U}{\partial y} \propto \frac{u_\tau}{y} \Rightarrow U = u_\tau \left(\frac{1}{\kappa} \ln \frac{y u_\tau}{\nu} + B \right)$$

In wall units:

$U^+ = \frac{U}{u_\tau}, \quad y^+ = \frac{y u_\tau}{\nu}$

(viscous sublayer) $U^+ = y^+$

(log layer) $U^+ = \frac{1}{\kappa} \ln y^+ + B$

8

Summary (1)

- Turbulence is a 3-d, time-dependent eddying motion with many scales, causing continuous mixing
- Any instantaneous flow variable can be decomposed as **mean + fluctuation**
- The process of averaging turbulent variables is called **Reynolds averaging** and leads to the **Reynolds-averaged Navier-Stokes (RANS) equations**
- The **product** of turbulent fluctuations makes a net contribution to the transport of momentum and other quantities via **Reynolds stresses** and **turbulent fluxes**

Summary (2)

- A **turbulence model** is a means of specifying turbulent fluxes in order to close the mean-flow equations
- Turbulent energy is:
 - **generated** (anisotropically, at large scale) by mean-velocity gradients
 - **redistributed** amongst components by pressure fluctuations
 - **dissipated** (at small scale) by viscosity
- Turbulence modelling is guided by theory and experiments for fundamental **free** and **wall-bounded** flows: in particular, by the **log law**
