

A7

a) HS:  $\dot{Q}_{aus}$

$$\Rightarrow 0 = \dot{m}_{ein} (h_e - h_i) + \dot{Q}_R - \dot{Q}_{aus}$$

$$h_e(70^\circ\text{C}, 7\text{bar}) = \cancel{h_f(70^\circ\text{C})} = 2733,8 \frac{\text{kJ}}{\text{kg}} \quad h_f(70^\circ\text{C}) = 292,98 \frac{\text{kJ}}{\text{kg}}$$

$$h_i(100^\circ\text{C}, 7\text{bar}) = \cancel{h_f(100^\circ\text{C})} = 2257,7 \frac{\text{kJ}}{\text{kg}} \quad h_f(100^\circ\text{C}) = 419,04 \frac{\text{kJ}}{\text{kg}}$$

( $\rightarrow$  ~~an offenes System  $\rightarrow$  aton Druck = 1 bar~~)

siedende flüssigkeit  $\Rightarrow$  flüssig-gastörmig Zustand

sieden  $\Rightarrow$  flüssig

$$\Leftrightarrow \underline{\dot{Q}_{aus} = \dot{m}_{ein} (h_e - h_i)} + \dot{Q}_R = \underline{\cancel{722,1\text{W}}} \quad \underline{\cancel{76,96\text{kW}}} \quad \underline{\cancel{62,78\text{kW}}}$$

b) HS:  $\bar{T}_{KF}$ ,  $\dot{Q}_{aus} = 65\text{kW}$

$$\bar{T}_{KF} = \frac{T_{KF,aus} + T_{KF,ein}}{2} = \underline{\underline{293,75\text{K}}}$$

arithmetisch

$$c) \Delta S = \cancel{s_{coz}} \frac{\dot{Q}_{aus}}{\bar{T}_{KF}} + s_{coz}$$

$$\Leftrightarrow s_{coz} = \Delta S - \frac{\dot{Q}_{aus}}{\bar{T}_{KF}}$$

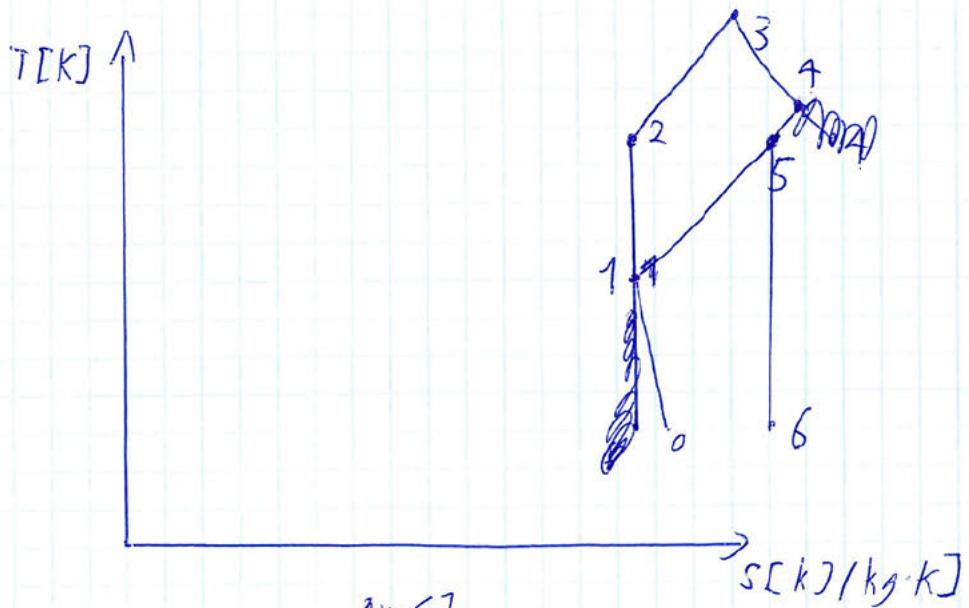
$$\Delta m_2 = m_2 - \Delta t$$

$$0 = m_n(h_e - h_a) + Q_R$$

Aus  
O

d) für  $\Delta m_2$

A 2 a) T-s Diagramm:



$0 \rightarrow 1$ : adiabat  $\rightarrow$  isentrop,  $\frac{v_1}{v_0} < 1$   
 $s_1 \leq s_0 \rightarrow p_1 \geq p_0$   
 $T_1 \geq T_0$

$1 \rightarrow 2$ : adiabat rev  $\Rightarrow$  isentrop

$$s_1 = s_2$$

$7 \rightarrow 5$ : ~~rev~~ adiabat  $\rightarrow$  isentrop,  $p_5 = p_0$  isodar

$2 \rightarrow 3$ : Isobaro

$3 \rightarrow 4$ : nicht rev

b) GS:  $w_6$ ,  $T_6$

$$\Rightarrow w_6 = \cancel{\frac{w_5}{P_5}} \quad \cancel{w_5} \quad \frac{P_5}{P_0} = 2,678$$

$$\Rightarrow \cancel{w_6} \quad \cancel{w_6 = w_5 \cdot \frac{P_0}{P_5} = 84,04 \frac{m}{s}}$$

$$\underline{\underline{w_6 = w_5 \cdot \frac{P_0}{P_0} = 575,76 \frac{m}{s}}}$$

$$\Delta_{\text{ex}} s_f = \ln(h_s - h_f) - T_0(s_s - s_f)$$

↓  
0      94      1      0

c) Ls; mgs

~~A3 d)~~  $|Q_{12}| = 1,5 \text{ kJ}$

HS:  $x_{Eis,2}$

$T_{EW,2} = T_{EW,1}$

$Q_{12} = m_2 u_2 - m_1 u_1$

$m_{EW,1} = m_{EW,2} = m_2 = m_1$

~~$u_1 = u_f + x_{Eis,1} (u_{f,1} - u_f)$~~   
 $u_1 = u_f + x_{Eis,1} (u_{f,1} - u_f)$

$\hookrightarrow$  bei  $0^\circ\text{C}$  und Druck  $p_{Eis,1} = p_{amb} + \frac{m \cdot g}{\left(\frac{D}{2}\right)^2} = 1,9 \text{ bar}$

$u_f = -0,045 \frac{\text{kJ}}{\text{kg}}$ ,  $u_{f,1} = -333,458 \frac{\text{kJ}}{\text{kg}}$

$\Rightarrow u_1 = -200,09 \frac{\text{kJ}}{\text{kg}}$

$\hookrightarrow Q_{12} = m_{EW,1} (u_2 - u_1)$

$\hookrightarrow \frac{Q_{12}}{m_{EW,1}} = u_2 - u_1 \quad \hookrightarrow \frac{Q_{12}}{m_{EW,1}} + u_1 = u_2$

$u_2 = \cancel{797,79} - 185,09 \frac{\text{kJ}}{\text{kg}}$

$\Rightarrow u_2 = u_f + x_{Eis,2} (u_{f,1} - u_f) \quad \hookrightarrow$  Bei gleichem Temp und Druck

$\hookrightarrow \frac{u_2 - u_f}{u_{f,1} - u_f} = x_{Eis,2} = \cancel{0,555} \underline{\underline{0,555}}$

$$\Delta u = \text{cv}(T_{3,2} - T_{3,1}) = 376,5 \frac{\text{K}}{\text{K}}$$

$$m_{3,2} = m_{3,1}$$

$$\Delta u = m_g \Delta u = 1,0764$$

$$\text{Es gilt: } Q = m_g \Delta u + Q_{3,2}$$

$$Q = 0,0034 \text{ kJ/K} \cdot \text{mol} \cdot \text{K}$$

~~W: Volumenänderung bei Verdampfung~~

~~W: Temperaturausgleich bei 0°C~~

~~W: Volumenänderung bei Verdampfung~~

$$T_{3,2} < T_{3,1}, \text{ da Temperaturausgleich bei } T_{3,2} \approx T_{3,1} = 0^\circ\text{C}$$

~~W: das Füllvolumen bei 0°C ist kleiner~~

$$m_g = 3,69 \text{ kg Werte eingesetzt.}$$

$$P_{3,1} = 1,5 \text{ bar und } m_g > 0$$

$$T_{3,2}, P_{3,2} \text{ und } m_g > 0$$

$$m_g = \frac{P_{3,1} V_{3,1}}{R_g T_{3,1}} = \frac{0,0034 \text{ kJ}}{166,28 \frac{\text{J}}{\text{kg K}}} = 3,49$$

$$m_g = \frac{P_{3,2} V_{3,2}}{R_g T_{3,2}} = \frac{0,0034 \text{ kJ}}{166,28 \frac{\text{J}}{\text{kg K}}} = 2,12$$

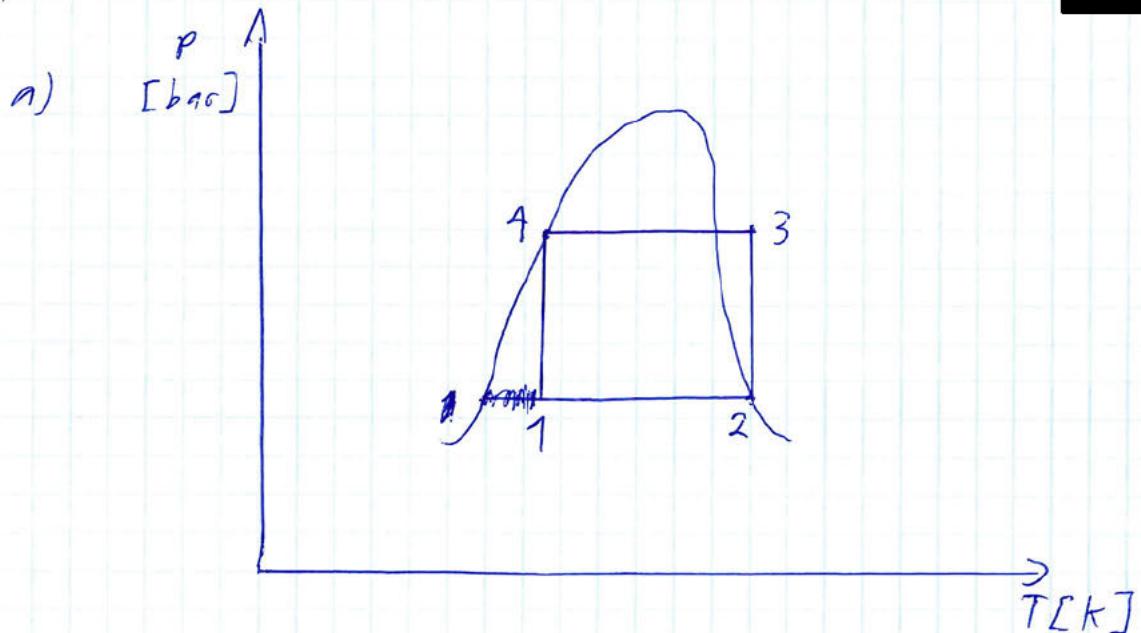
$$(P_2)^2 \pi = 0,00385 \text{ m}^2$$

$$m \cdot g = 313,92 \text{ kg/m}^2 \cdot 9,81 \text{ m/s}^2 = 3,078 \text{ N/m}$$

$$P_{3,2} = m \cdot g \cdot h + p_{\text{amb}} = 7,46 \text{ bar}$$

AS:  $P_{3,2} = m \cdot g \cdot h + p_{\text{amb}}$

AA



1  $\rightarrow$  2: isobar

2  $\rightarrow$  3: adiabat  $P \propto V \Rightarrow$  isentrope

3  $\rightarrow$  4: isobar

4  $\rightarrow$  1: isentrope

b) HS:  $\dot{m}_{R134a}$

$$\dot{Q} = \dot{m}_{R134a} (h_3 - h_1) + \dot{Q}_{ab}$$

$$0 = \dot{m}_{R134a} (h_2 - h_3) - \dot{W}_k \Leftrightarrow \dot{m}_{R134a} = \frac{\dot{W}_k}{h_2 - h_3}$$

$$\Rightarrow h_2 = h_1, s_2 = s_3$$

~~$T_2 = 6K$~~

$$h_3(8\text{ bar}, T_3)$$

$$\frac{ds - \epsilon s}{\sqrt{s} - \epsilon s} = \alpha$$

$$ds = \epsilon s$$

$$ds = \alpha s$$

$$ds : \alpha s$$

$$(1) m_{134} = 47.6, T_2 = -22^{\circ}\text{C}$$