

# Thermodynamik 1 HS23

① a) Energiebilanz Reaktor:

$$\frac{dE}{dt} \xrightarrow{\text{stationär}} = \dot{m} (h_{\text{ein}} - h_{\text{aus}}) + \dot{Q} - \dot{W} \xrightarrow{0}$$

$$\dot{Q} = \dot{m} (h_{\text{aus}} - h_{\text{ein}}) = \dot{Q}$$

$$\left. \begin{array}{l} h_{\text{aus}} = 419.04 \frac{\text{kJ}}{\text{kg}} \\ h_{\text{ein}} = 292.98 \frac{\text{kJ}}{\text{kg}} \end{array} \right\} \text{TAB A-2}$$

$$b) \frac{T}{T} = \frac{\int_1^2 T ds}{s_2 - s_1} = \frac{h_2 - h_1 + V(p_2 - p_1)}{c \ln \left( \frac{T_2}{T_1} \right)} = \frac{c (T_2 - T_1)}{c \ln \left( \frac{T_2}{T_1} \right)} = \boxed{293.12 \text{ K} = \bar{T}}$$

$$c) \frac{ds}{dt} \xrightarrow{0} = \sum \dot{m}_i h_i + \frac{\dot{Q}}{\bar{T}} + \dot{S}_{\text{erz}} \quad \text{Entropie- (Bilanz Wand)}$$

$$\dot{S}_{\text{erz}} = - \frac{\dot{Q}}{\bar{T}} = \frac{65 \text{ kW}}{293.12 \text{ K}} = \boxed{0.2218 \frac{\text{kJ}}{\text{K} \cdot \text{s}} = \dot{S}_{\text{erz}}}$$

$$d) \text{Diagramm: } E_1 \rightarrow E_2, \text{ mit } \frac{dE}{dt} = 0$$

$$0 = \dot{m}_{\text{Ges,1}} (h_{\text{ein}}(70^\circ\text{C}) - h_{\text{ein}}(100^\circ\text{C})) + \dot{m}_{12} (h(70^\circ\text{C}) - h(20^\circ\text{C}))$$

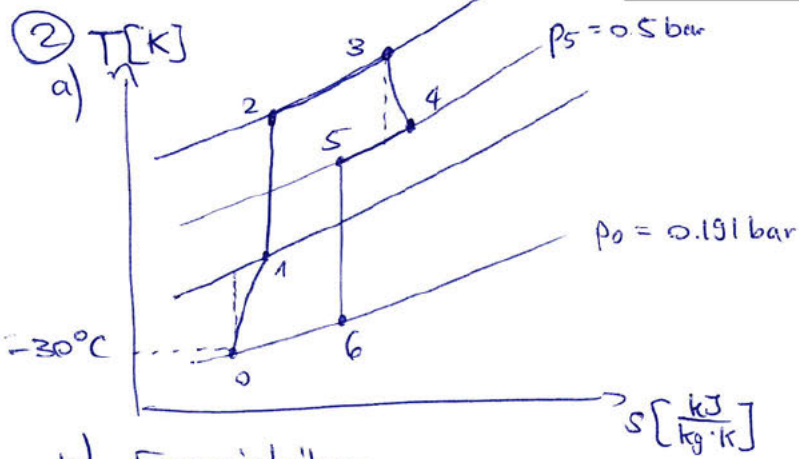
$$\dot{m}_{12} = - \dot{m}_{\text{Ges,1}} \frac{h(70^\circ\text{C}) - h(100^\circ\text{C})}{h(70^\circ\text{C}) - h(20^\circ\text{C})} = -5755 \text{ kg} \frac{292.98 \frac{\text{kJ}}{\text{kg}} - 419.04 \frac{\text{kJ}}{\text{kg}}}{292.98 \frac{\text{kJ}}{\text{kg}} - 83.96 \frac{\text{kJ}}{\text{kg}}} = \boxed{3470 \text{ kg} = \Delta \dot{m}_{12}}$$

e) Wellbaufertes System:

$$\Delta S = \dot{m}_2 s_2 - \dot{m}_1 s_1 = (\dot{m}_{\text{Ges,1}} + \Delta \dot{m}_{12}) s(70^\circ\text{C}) - \dot{m}_{\text{Ges,1}} s(100^\circ\text{C})$$

$$\begin{array}{l} s(70^\circ\text{C}) = 0.9549 \\ s(100^\circ\text{C}) = 0.13069 \end{array}$$

$$\boxed{\Delta S = 8056.8 \frac{\text{kJ}}{\text{K}}}$$



b) Energiebilanz um ganzes Triebwerk

$$\frac{dE}{dt} = \dot{m}(h_{\text{ein}} - h_{\text{aus}} + \frac{1}{2}w_0^2 - \frac{1}{2}w_6^2)$$

$$0 = c_p(T_0 - T_6) + \frac{1}{2}w_0^2 - \frac{1}{2}w_6^2$$

$$h_{\text{ein}} - h_{\text{aus}} = c_p(T_0 - T_6)$$

Energiebilanz um Schubdüse

$$0 = c_p(T_5 - T_6) + \frac{1}{2}w_5^2 - \frac{1}{2}w_6^2$$

$$c_p(T_0 - T_6) + \frac{1}{2}w_0^2 = c_p(T_5 - T_6) + \frac{1}{2}w_6^2$$

T

c)  $\Delta e_{\text{exstr}} = (h_6 - h_0 - T_0(s_6 - s_0) + \frac{1}{2}w_6^2 - \frac{1}{2}w_0^2)$

$$= c_p(T_6 - T_0) - T_0(c_p \ln(\frac{T_6}{T_0})) + \frac{1}{2}w_6^2 - \frac{1}{2}w_0^2$$

$$= 165.17 \text{ kJ/kg}$$

$$T_6 = 340 \text{ K}$$

$$w_6 = 510 \text{ m/s}$$

d)  $\frac{dE}{dt} = \dot{E}_{\text{exstr}}$

$$\frac{dE}{dt} = \dot{E}_{\text{exstr}}$$

$$\Delta e_{\text{exstr}} = e_{\text{x,a}} - e_{\text{x,verl}}$$

$$= (1 - \frac{T_0}{T}) \dot{q} - e_{\text{x,verl}}$$

$$e_{\text{x,verl}} = (1 - \frac{T_0}{T}) \dot{q} - \Delta e_{\text{x,istr}}$$

$$e_{\text{x,verl}} = 804.1 \frac{\text{kJ}}{\text{kg}}$$

$$\textcircled{3} a) p_{a,1} = p_0 + \frac{m_K g}{A} + \frac{m_{EW} g}{A}$$

$$A = \pi \left(\frac{D}{2}\right)^2 = 0.007854 \text{ m}^2$$

$$= 10^5 \text{ Pa} + \frac{32 \text{ kg} \cdot 9.81 \frac{\text{N}}{\text{m}}}{0.007854 \text{ m}^2} + \frac{0.1 \text{ kg} \cdot 9.81 \frac{\text{N}}{\text{m}}}{0.007854 \text{ m}^2}$$

$$p_{a,1} = 140.1 \text{ kPa} = 1.401 \text{ bar} = p_{a,1}$$

$$p v = R T$$

$$R = \frac{\bar{R}}{M} = \frac{8.314 \frac{\text{kJ}}{\text{kgmol} \cdot \text{K}}}{50 \frac{\text{kg}}{\text{kgmol}}} = 0.16628 \frac{\text{kJ}}{\text{kg} \cdot \text{K}}$$

$$v_{a,1} = \frac{R T_{a,1}}{p_{a,1}}$$

$$= \frac{0.16628 \cdot 773.15}{140.1} = 0.9176 \frac{\text{m}^3}{\text{kg}}$$

$$m = \frac{V_{a,1}}{v_{a,1}} = \frac{0.00314 \text{ m}^3}{0.9176 \frac{\text{m}^3}{\text{kg}}} = 0.003422 \text{ kg} = 3.422 \text{ g} = m_{a,1}$$

b)  $p_{a,2} = p_{a,1} = 140.1 \text{ kPa}$  (Masse von EW, Kolben und patm verändern sich nicht)

Thermodynamische ggW:  $T_{a,2} = T_{EW,2}$

$$p_{EW,2} = p_0 + \frac{m_K g}{A} = 139.97 \text{ kPa} = 1.3997 \text{ bar}$$

Interpolieren mit Tab. 1:  $0.00314 \text{ kg} \cdot T_{EW,2} = 0.003 + \frac{0.003}{-0.4 \text{ bar}} (0.3997 \text{ bar})$

$$\Rightarrow T_{a,2} = 0^\circ \text{C}$$

c)  $\Delta U_{a,12} = Q - W \rightarrow 0$

$$m_a (u_2 - u_1) = Q$$

$$m_a C_v^{PG} (T_2 - T_1) = 0.003422 \text{ kg} \cdot 0.633 \frac{\text{kJ}}{\text{kg} \cdot \text{K}} (500 \text{ K}) = -1.083 \text{ kJ} = Q$$

$$Q_2 = 1.083 \text{ kJ}$$

$$\Rightarrow Q_{12} = 1.083 \text{ kJ}$$

d)  $\Delta U_{w,12} = Q - W \rightarrow 0$

$$m_{EW} (u_2 - u_1) = Q$$

$$u_2 = \frac{Q}{m_{EW}} + u_1$$

$$= -189.27 \frac{\text{kJ}}{\text{kg}}$$

$$u_2 = u_{f1} + x_2 (u_{\text{fest}} - u_{f1})$$

$$x_2 = \frac{u_2 - u_{f1}}{u_{\text{fest}} - u_{f1}} = \frac{-200.1 + 0.045}{-333.458 + 0.045}$$

$$= 0.6000216 = x_{\text{Eis},2}$$

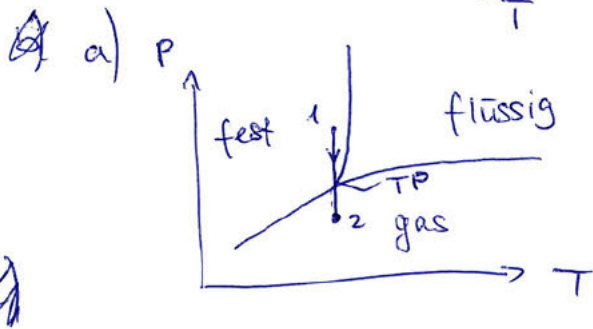
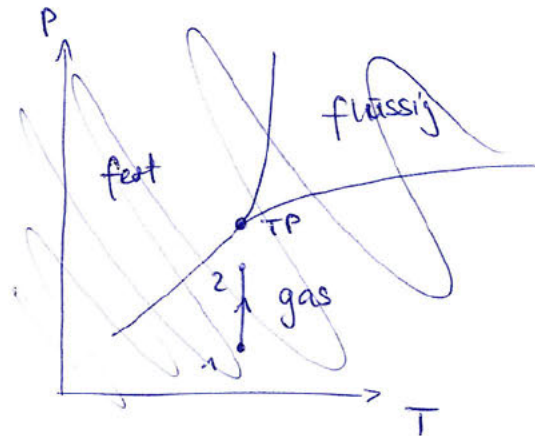
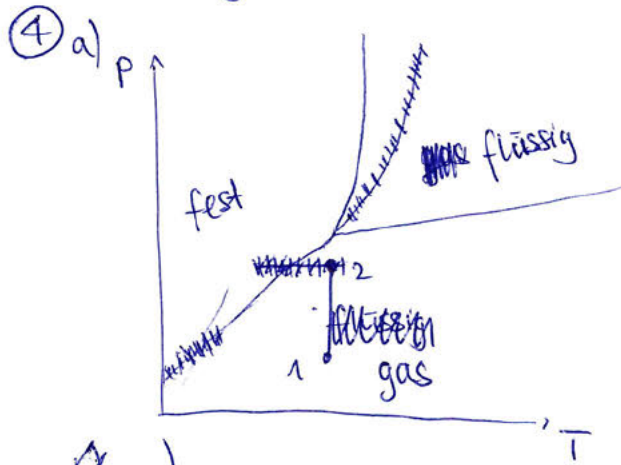
$$\Rightarrow x_{\text{Eis},2} = 0.600$$

$$u_1 = u_f(0^\circ \text{C}) + x(u_{\text{fest}}(0^\circ \text{C}) - u_f(0^\circ \text{C}))$$

$$= -0.045 + 0.6(-333.458 + 0.045)$$

$$= -200.1 \frac{\text{kJ}}{\text{kg}}$$





	Temp.	Druck
1		
2		
3		8 bar
4		8 bar

b) noch machen!

c) Annahme:  $T_2 = -22^\circ\text{C}$ ,  $\dot{m} = 4 \frac{\text{kg}}{\text{h}}$

TAB A-10:  $p_2 = 1.2192 \text{ bar} = p_1$

$S_1 = S_2$  (adiabatisch)

$S_g = 0.3459 \frac{\text{kJ}}{\text{kg K}}$  TAB A-11

$$S_1 = S_f(1.2192 \text{ bar}) + x(S_g(1.2192 \text{ bar}) - S_f(1.2192 \text{ bar}))$$

$$x = \frac{S_1 - S_f}{S_g - S_f} = \boxed{0.303 = x_1}$$

Interpolation mit TAB A-11:

$$S_f = 0.0879 + \frac{0.1055 - 0.0879}{1.4 - 1.2} (1.2192 - 1.2) = 0.08959$$

$$S_g = 0.9354 + \frac{0.9322 - 0.9359}{1.4 - 1.2} (1.2192 - 1.2) = 0.9348$$

b) Energiebilanz um Verdichter:

$$\frac{dE}{dt} = \dot{m}(h_2 - h_3) + \dot{W}$$

$$\dot{m} = \frac{+\dot{W}_K}{h_2 - h_3}$$

$$T_1 = -20^\circ\text{C}$$

$$\Rightarrow T_2 = -26^\circ\text{C}$$

$$h_2 = 231.62^\circ\text{C} \quad \text{TAB A-10}$$

$$d) \epsilon_k = \frac{|\dot{Q}_{zu}|}{|\dot{W}_t|}$$

$$\dot{W}_t = \dot{W}_K = 28 \text{ W}$$

$$|\dot{Q}_{zu}| = |\dot{Q}_K|$$

Energiebilanz ~~Kondensator~~ <sup>Verdampfer:</sup>

$$\frac{dE}{dt} \stackrel{\rightarrow 0, \text{stationär}}{=} \dot{m}(h_1 - h_2) + \dot{Q}_{Kc} - \dot{W} \stackrel{\rightarrow 0}{=}$$

$$\begin{aligned} \dot{Q}_K &= \dot{m}(h_2 - h_1) \\ &= 4 \text{ kg/h} \left( 239.08 \frac{\text{kJ}}{\text{kg}} - 93.42 \frac{\text{kJ}}{\text{kg}} \right) \\ &= 562.64 \frac{\text{kJ}}{\text{h}} \\ &= 0.156 \frac{\text{kJ}}{\text{s}} = 156 \text{ W} \end{aligned}$$

$$\Rightarrow \epsilon_k = \frac{\dot{Q}_K}{\dot{W}_K} = \frac{156 \text{ W}}{28 \text{ W}} = \boxed{5.57 = \epsilon_k}$$

$$h_1 \neq h_2$$

$$h_1 = h_g \text{ (isenthalpe Drossel)} \\ = 93.42 \frac{\text{kJ}}{\text{kg}} \quad \text{TA13 A-11}$$

$$h_2 = 239.08 \frac{\text{kJ}}{\text{kg}} \quad \text{TA13 A-10}$$

e) Temperatur würde weiter sinken, aber immer langsamer, da  $C_p$  immer grösser wird.