

Aufgabe 1

-stationär

1.1
Aufgabe 1: Sich zur jeweiligen Aufgabe

$$\dot{m}_{\text{in}} = 0.3 \frac{\text{kg}}{\text{s}}, T_{\text{in}} = 70^\circ\text{C}$$

Erläuterung

| Kitt | in | T _{in} | Phase | aus | Phase | reiner Wärmetauscher |
|---------|----------|-----------------|-------------------------|-----|-------|----------------------|
| Eing | 0.3 kg/s | 70°C | flüssige Flüssigkeit | r | | |
| Ausgang | 0.3 kg/s | 100°C | seichtwärme Flüssigkeit | r | | |

~~Raum~~

$$\text{Rakktor: } m = 5755 \text{ kg}$$

$$x_D = 0.005$$

$$T = 100^\circ\text{C} = \text{const.}$$

$$Q_E = 100 \text{ kW}$$

$$Q_{\text{aus}} = ?$$

$$\text{Kühlkreislauf: } T_{\text{refin}} = 288.15 \text{ K} \\ T_{\text{r,aus}} = 298.15 \text{ K} \quad \left. \right\} \text{IF!}$$

Aufgabe 1 : 1. 2

Aufgabe Seite zur jew. Aufgabe

EB um Reaktor ~~abflusswärme~~ Reaktor

"Siedeblender Flüssigkeit"
= aufsteigende Punkttemperatur

$$\dot{Q} = \dot{m}_{\text{min}} (h_{\text{in}} - h_{\text{as}}) + \dot{Q}_{\text{aus}}$$

$$\dot{Q}_{\text{aus}} = \dot{m}_{\text{min}} (h_{\text{as}} - h_{\text{in}})$$

$$= 0.3 \text{ kg/s} (419.04 \text{ kJ/kg} - 292.98 \text{ kJ/kg}) =$$

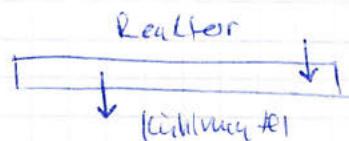
$$\dot{Q} = \dot{m}_{\text{min}} (h_{\text{in}} - h_{\text{as}}) + \dot{Q}_{\text{ab}}$$

$$\dot{Q}_{\text{ab}} = \dot{m}_{\text{min}} (h_{\text{as}} - h_{\text{out}})$$

$$= 0.3 \text{ kg/s} (419.04 \text{ kJ/kg} - 292.98 \text{ kJ/kg}) = \underline{\underline{37.818 \text{ kW}}}$$

TAB A2

c)



$$\dot{Q} = \frac{\dot{Q}_{\text{aus}}}{T_{\text{Reaktor}}} - \frac{\dot{Q}_{\text{aus}}}{T_{\text{KW}}} + \dot{S}_{\text{ext}} \Rightarrow \dot{S}_{\text{ext}} = \frac{65 \text{ kW}}{295 \text{ K}} - \frac{65 \text{ kW}}{373.15 \text{ K}} = \underline{\underline{0.046 \frac{\text{W}}{\text{K}}}}$$

d.) $T_{\text{Reaktor}} = 70^\circ\text{C} = 343.15\text{K}$

$$\Delta u_{12} \stackrel{!}{=} \text{Siedend}, T_{\text{ein}} = 20^\circ\text{C}$$

$$m_2 u_2 - m_1 u_1 = \Delta u_{12} h_{\text{ein}} + Q_{R,12}$$

$$\begin{aligned}\Delta u_{12} &= \frac{m_2 u_2 - m_1 u_1}{Q_{R,12}} \quad \cancel{\text{Zurückrechnung}} \\ &= \frac{(m_1 + \Delta u_{12}) u_2 - m_1 u_1}{Q_{R,12}}\end{aligned}$$

$$Q_{R,12} \Delta u_{12} = (m_1 + \Delta u_{12}) u_2 - m_1 u_1$$

$$\Delta u_{12} (Q_{R,12} - \cancel{u_2}) = u_2 m_1 - m_1 u_2$$

$$\Delta u_{12} = \frac{\cancel{m_1} (u_2 - u_1)}{Q_{R,12} - u_2} = \cancel{\text{Endgült}}$$

e.) $\Delta S = \cancel{m_2} \cancel{m_1} m_2 s_2 - m_1 s_1$

W08 Aufgabe 2

Aufgabe: 2. A

| | m | T | V | P | w | Q | w | Notiz |
|----|------------|-------|---|-----------|-------------------|---|---|------------------------------|
| Z0 | Präzession | -30°C | | 0.191 bar | | - | | $n_{vs} < 1$ |
| Z1 | | | | | | | | $1 \rightarrow 2$: isentrop |
| Z2 | | | | | | | | $2 \rightarrow 3$: isobar |
| Z3 | | | | | | | | $3 \rightarrow 4$: adiabat |
| Z4 | | | | | | | | |
| Z5 | 431.9 K | | | 0.5 bar | 220 $\frac{m}{s}$ | | | $5 \rightarrow 6$: isentrop |
| Z6 | | | | | | | | |

$$\text{W}_{\text{Luft}} = 200 \frac{W}{s}$$

$$p_0 = 0.191 \text{ bar}$$

$$T_0 = -30^\circ\text{C}$$

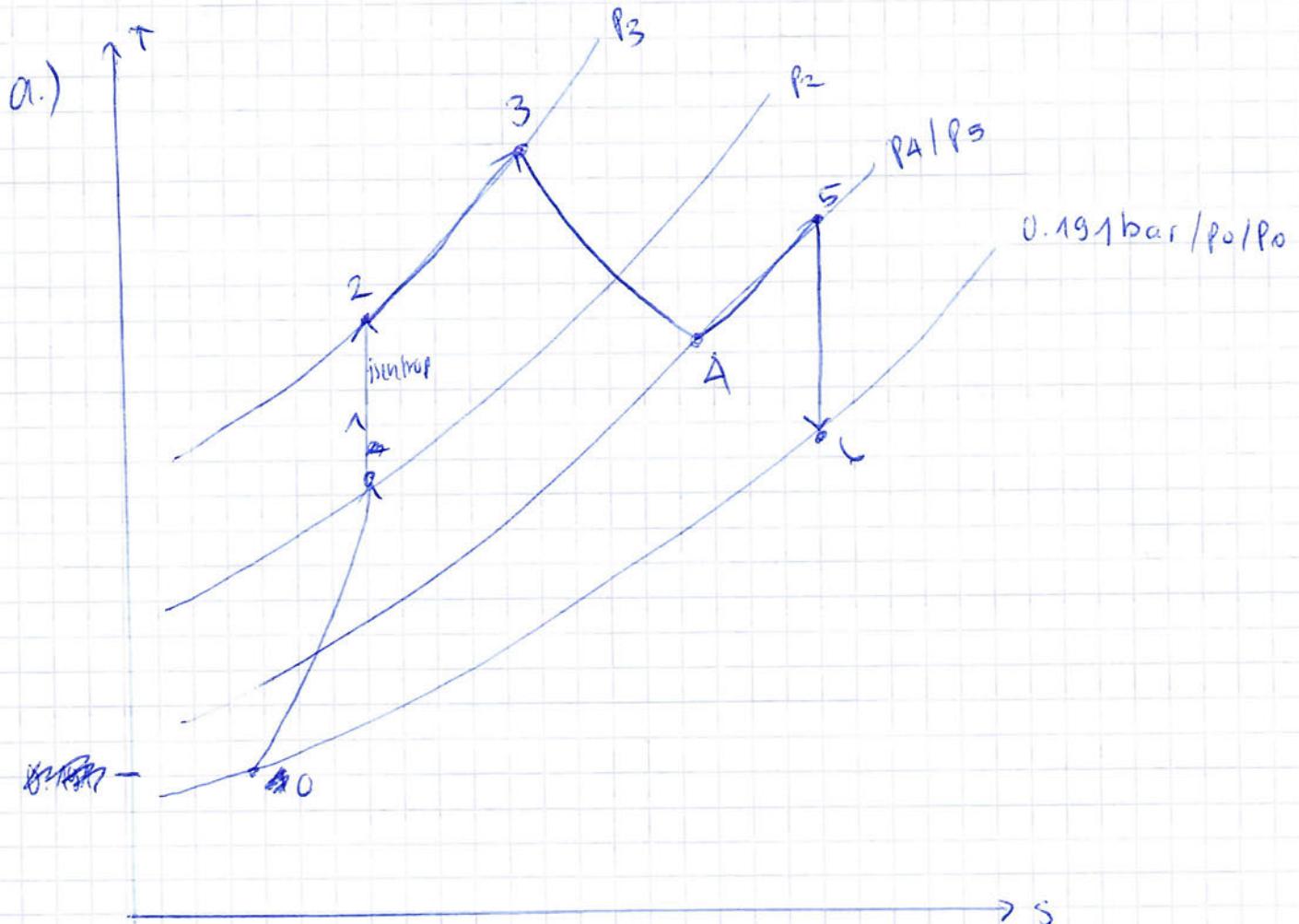
$$\frac{\bar{m}_M}{\bar{m}_K} = 5.293$$

~~(P)~~ Luft: $\kappa = 1.6$

$$c_p^{\text{is}} = 1.006 \frac{\text{kJ}}{\text{kgK}}$$

$$\kappa = \gamma = 1.4$$

Aufgabe 2: 2.2



$$b) T_b = T_5 \cdot \left(\frac{P_5}{P_b} \right)^{\frac{n-1}{n}} = 431.9 \text{ K} \cdot \left(\frac{0.3 \text{ bar}}{0.191 \text{ bar}} \right)^{\frac{1.4-1}{1.4}}$$

$$= \underline{\underline{568.58 \text{ K}}}$$

EB um Schubdüse

$$0 = \cancel{h_5 + h_6 - P_6} \quad \cancel{\text{Volumen} (h_5 - h_6 + \frac{1}{2} w_5^2 - w_6^2)}$$

~~h5 + h6 - P6~~

$$\frac{1}{2} w_6^2 = h_5 - h_6 + \frac{1}{2} w_5^2 = c_p^{ig} (T_5 - T_b) + \frac{1}{2} w_5^2$$

$$= 1.006 \frac{\text{kJ}}{\text{kg K}} (431.9 \text{ K} - 340 \text{ K}) + \frac{1}{2} 220 \frac{\text{m}^2}{\text{s}^2}$$

$$= 24298.2 \cdot 45.14 \frac{\text{m}^2}{\text{s}^2} = 311.72 \frac{\text{m}}{\text{s}}$$

$$w_6^2 = \sqrt{2 \cdot (24298.2 \cdot 45.14 \frac{\text{m}^2}{\text{s}^2})} = \cancel{222241.98}$$

Aufgabe 2: 2.3

$$c.) \Delta e_{x,15\%} = h_b - h_0 - T_0 (s_b - s_0) + \frac{1}{2} w_b^2 - \frac{1}{2} w_0^2 \\ = (T_b - T_0) c_p^{(g)} - T_0 \left(\cancel{T_0} c_p^{(g)} \ln \left(\frac{T_0}{T_b} \right) - R \cdot \ln \left(\frac{P_b}{P_0} \right) \right) + \frac{1}{2} w_b^2 + \frac{1}{2} w_0^2$$

$$R = c_p^{(g)} - c_v^{(g)}$$

$$= c_p^{(g)} - \frac{c_p^{(g)}}{n} = c_p^{(g)} \left(1 - \frac{1}{n} \right) = 1.006 \frac{\text{kJ}}{\text{kgK}} \left(1 - \frac{1}{1.4} \right) = 0.287 \frac{\text{kJ}}{\text{kgK}}$$

$$\Delta e_{x,15\%} = (340\text{K} - 243.15\text{K}) 1.006 \frac{\text{kJ}}{\text{kgK}} - 243.15\text{K} \left(1.006 \frac{\text{kJ}}{\text{kgK}} \cdot \ln \left(\frac{340\text{K}}{243.15\text{K}} \right) - 0.287 \frac{\text{kJ}}{\text{kgK}} \cdot \ln(1) \right) + \frac{1}{2} (200 \frac{\text{m}}{\text{s}})^2 + \frac{1}{2} (510 \frac{\text{m}}{\text{s}})^2$$

=

$$d.) e_{x,\text{vert}} = T_0 \cdot \cancel{s_{0,24}} \quad \text{sic!}$$

$$0 = -\frac{q_B}{T_B} + \cancel{s_{0,24}} \quad \text{sic!}$$

$$s_{\text{sic!}} = \frac{q_B}{T_B} = \frac{1195 \frac{\text{kJ}}{\text{kg}}}{1289 \text{K}} = 0.927 \frac{\text{kJ}}{\text{kgK}}$$

$$e_{x,\text{vert}} = 303.15\text{K} \cdot 0.927 \frac{\text{kJ}}{\text{kgK}} = \underline{\underline{281 \text{ kW}}}$$

Aufgabe 3

Oberes Abteil

| | T | V | m | Phase | |
|----|-----|-------|-------|---|--|
| z1 | 0°C | V_1 | 0.1kg | $x = \frac{m_{\text{wiss}}}{m_{\text{EW}}} = 0.6$ | |
| z2 | | V_2 | | | |

3.1
Aufgabe
Blatt

$$1L = 10^{-3} m^3$$

$$3.14L \approx 0.00314 m^3$$

- EW ausrechnen

~~ist das
perfekt~~

Unteres Abteil

| | T | $V_{g,1}$ |
|----|---------|------------|
| z1 | 500°C | 0.00314 m³ |
| z2 | 0.003°C | |

perf Gas, $c_v = \cancel{0.633} \quad 0.633 \frac{J}{kg \cdot K} \quad M_g = 30 \frac{kg}{mol}$

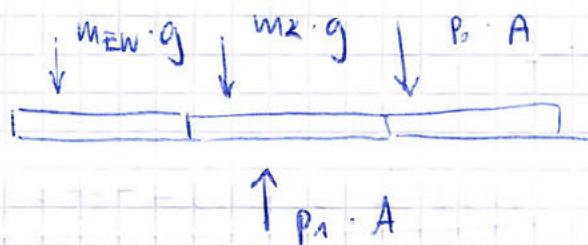
Körper $m_k = 32 \text{ kg}$, $\rho = 10 \text{ cm} = 0.1 \text{ m}$

$P_{\text{amb}} = 1 \text{ bar}$

Q fließt

Aufgabe 3 : 3.2

$$a) p_1 \overset{\checkmark}{V_1} = m_1 R \overset{\checkmark}{T_1} \quad p = \frac{F}{A}$$



$$A = \pi r^2 = \pi \cdot \left(\frac{0.1}{2} \text{m}\right)^2 \\ = 0.007854 \text{m}^2$$

KGLW: $m_{EW} \cdot g + m_K \cdot g + p_0 \cdot A = p_1 \cdot A$

$$p_1 = \frac{0.1 \text{kg} \cdot 9.81 \text{m/s}^2}{0.007854 \text{m}^2} + \frac{32 \text{kg} \cdot 9.81 \text{m/s}^2}{0.007854 \text{m}^2} + 10^5 \text{Pa} = \underline{\underline{1.4 \text{ bar}}}$$

~~$p_{g1} = p_{g1} \cdot R \cdot T_1$~~ $m_{g1} = \frac{p_{g1} V_{1g}}{R \cdot T_1} = \frac{1.4 \cdot 10^5 \text{ Pa} \cdot 0.00314 \text{ m}^3}{166.28 \frac{\text{kg}}{\text{mol K}} \cdot (500 + 273.15) \text{ K}}$

$$R = \frac{D}{M} = \frac{8.314 \frac{\text{J}}{\text{K mol}}} {50 \frac{\text{kg}}{\text{mol}}} \cdot 10^3 = 166.28 \frac{\text{kg}}{\text{mol K}} \quad = \cancel{\cancel{3.419 \text{ g}}} \quad \underline{\underline{3.419 \text{ g}}}$$

b.) Der Druck ist derselbe wie im Zustand 1, da sich die auf den Kolben wirkenden Kräfte nicht verändert haben. $p_{g2} = p_{g1} = 1.4 \text{ bar}$. Die Temperatur hat sich verändert, da Energie aufgenommen wurde und das Eiswasser zu Schmelzen

~~W287~~

$$C_V = 0.633 \frac{\text{J}}{\text{kg K}}$$

$$C_P = R + C_V = 166.28 \frac{\text{J}}{\text{kg K}} + 0.633 \frac{\text{J}}{\text{kg K}} = 179.928 \frac{\text{J}}{\text{kg K}}$$

~~Zg = Zg AB~~

c)

$$\Delta E = \dot{Q}_{12} - \dot{W}_{12}$$

$$m_{g2} \cdot u_2 - m_{g1} \cdot u_1 = \dot{Q}_{12} - \dot{W}_{12}$$

$$W_{12} = \int_{p_1}^{p_2} pdV = \frac{R \cdot (T_{2g} - T_{1g})}{n-1} = \frac{106.28 \frac{J}{kgK} (273.153K - 773.15K)}{1 - 1.263} = 316.12 \text{ kJ}$$

$$n = \frac{C_p}{C_v} = \frac{0.79928}{0.633} = 1.263$$

$$+ 316.12 \text{ kJ}$$

$$\dot{Q}_{12} = \Delta E + W_{12} = m_g (T_{2g} - T_{1g}) C_V V = 0.003149 \text{ kg} (273.153K - 773.15K) \\ \cdot 0.633 \frac{\text{kJ}}{\text{kgK}} + 316.12 \text{ kJ} \\ = \underline{\underline{315.12 \text{ kJ}}}$$

d) im Zustand 2:

$$\cancel{m_{us}} (u_2 - u_1) = 0$$

~~aus = rezip~~~~Stoffz. Z. ADs~~

$$u_2 = u_1$$

$$u_1 = u_{fi} + 0.6 \cdot (u_{g_{Fe}} - u_{fi}) = -0.045 \frac{\text{kJ}}{\text{kg}} + 0.6 (-333.458 \frac{\text{kJ}}{\text{kg}} \\ + 0.045 \frac{\text{kJ}}{\text{kg}})$$

Tub 1

$$= 0.002 \frac{\text{kJ}}{\text{kg}}$$

$$r_1 = r_2$$

$$u_{1,us} = m_{ew} \cdot 0.6 = 0.1 \text{ kg} \cdot 0.6 = 0.06 \text{ kJ}$$

$$\cancel{x_1} \quad x = \frac{u_{Fe}}{u_{Fe} + u_{Fl}}$$

$$m_{2,us} = 0.04 \text{ kg}$$

Aufgabe 4

Aufgabe: 4.1

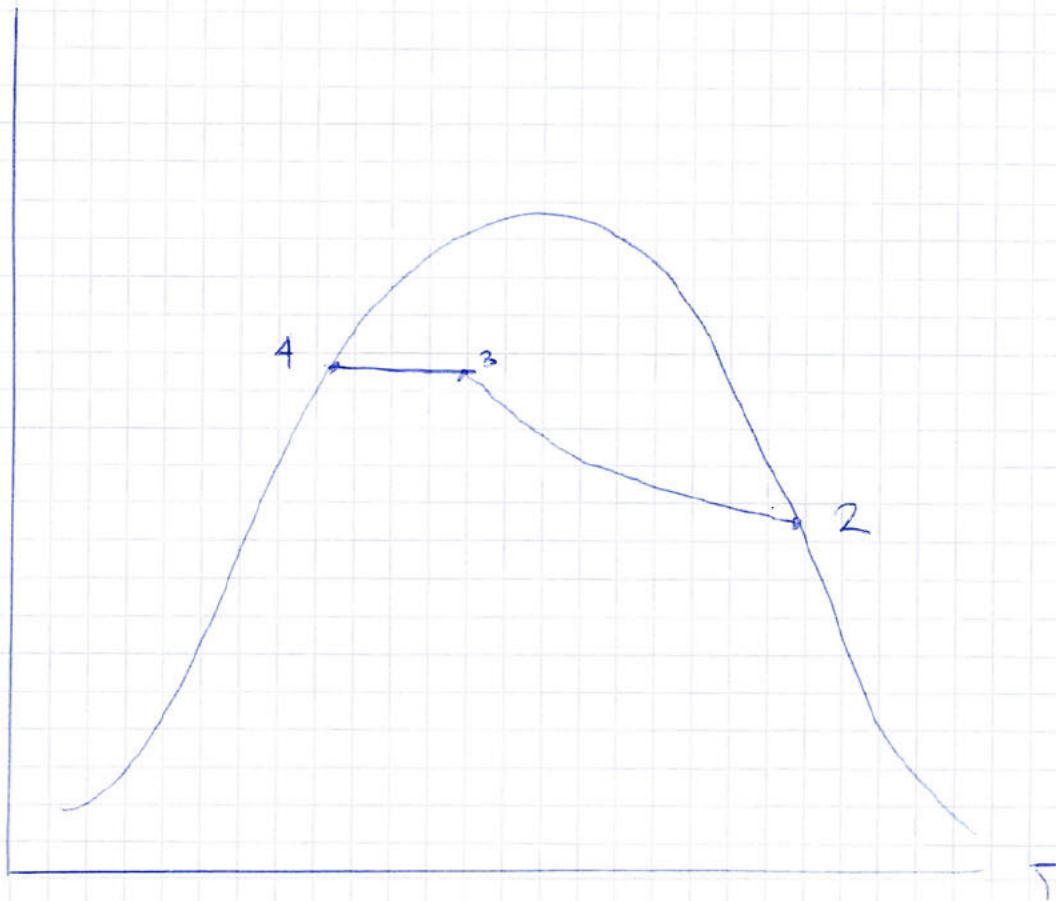
| | M | V | P | T | Q | W | Notiz |
|----|---|---|---|-------|---|---------------|---|
| z1 | | | | p_1 | | Q_{12} | |
| z2 | | | | p_2 | | $\lambda 28W$ | geöffneter Dampf 2 → 3: isochor |
| z3 | | | | 8 bar | | | |
| z4 | | | | 8 bar | | | Cycloidal Fließzyklus 4 → 1: adiabate Druck 1 (nicht p) |

$$\text{Im Verdampfer} = T_i - 6K$$

Im Kondensator: Im Isoterm, Sub var unter Trippelpunkt

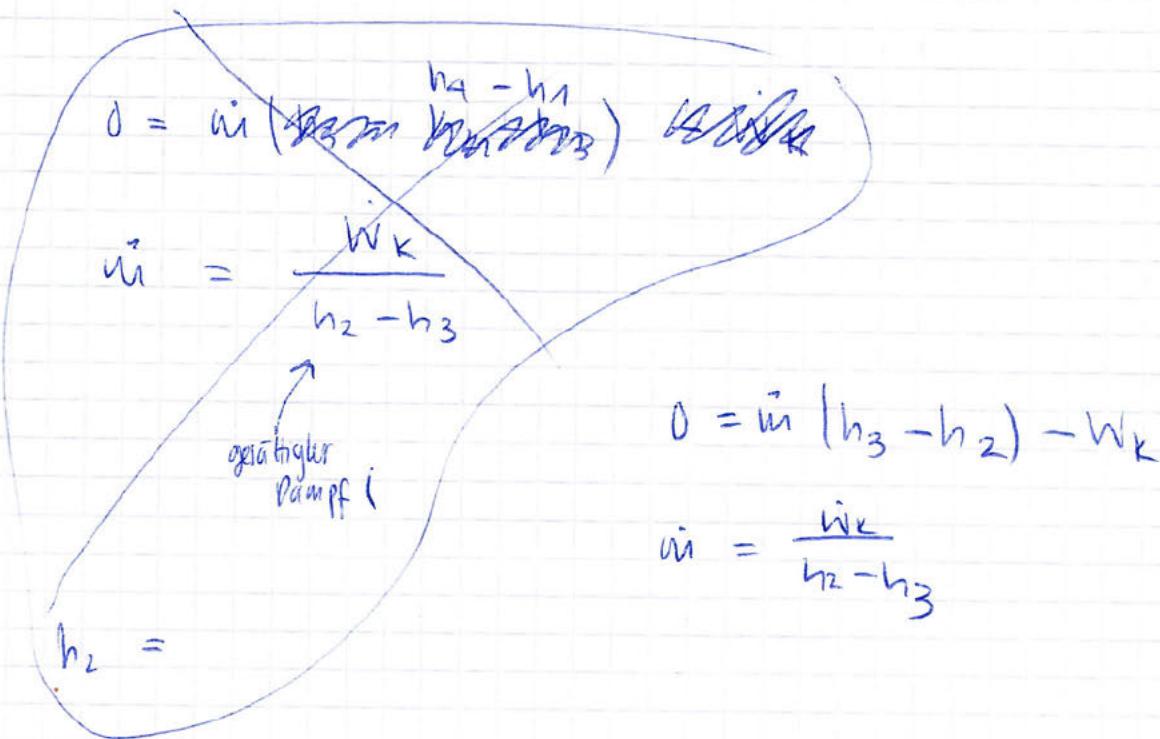
$T_i = 10K$ unter Subpunkt

a.)



Anlyse : 4.2

b.) EB um ~~TAB A1~~ 2+3



c.) $h_4 = h_1$ (isenthalpe Drossel)

$$h_4 = 93.42 \frac{10}{\log} = h_1$$

TAB A11

d.) $\varepsilon_e = \frac{\dot{E}_{exakt}}{\dot{E}_{zu}} = \frac{\dot{w}_k}{\dot{w}_{vakuum}}$