

$$1. a) 0 = m_{\text{ein}}(h_{\text{ein}}) - m_{\text{aus}} h_{\text{aus}} + \dot{Q} - \dot{S}^{\text{in}} = 0 + \dot{Q}_R$$

$$h_{\text{ein}} = h_f(TAB, T=270^\circ\text{C}) = 292.38 \frac{\text{kJ}}{\text{kg}}$$

$$h_{\text{aus}} = h_f(100^\circ\text{C}) = 415.04 \frac{\text{kJ}}{\text{kg}}$$

$$\dot{Q}_{\text{aus}} = m_{\text{aus}} h_{\text{aus}} - m_{\text{ein}} h_{\text{ein}} = m_{\text{aus}}(h_{\text{aus}} - h_{\text{ein}}) - \dot{Q}_R$$

$$\dot{Q}_{\text{aus}} = -62.18 \text{ kW}$$

$$b) \bar{T} = \frac{\int_a^b T ds}{s_b - s_a}$$

$$dH = T ds + \cancel{Vdp} = dH_{\text{real}} \quad \text{isobare}$$

$$\bar{T} = \frac{h_2 - h_1}{s_2 - s_1} - \frac{k(T_2 - T_1) + v(\cancel{\rho_2 - \rho_1})}{k \ln\left(\frac{T_2}{T_1}\right)} = 0$$

$$\bar{T} = \frac{T_2 - T_1}{\ln\left(\frac{T_2}{T_1}\right)} = 293.12 \text{ K}$$

$$c) \cancel{\dot{Q}_{\text{aus}}} \quad 0 = \frac{\dot{Q}_{\text{aus}}}{T_{\text{Reaktor}}} - \frac{\dot{Q}_{\text{aus}}}{\bar{T}} + \dot{S}_{\text{entz}}$$

$$\dot{S}_{\text{entz}} = \frac{\dot{Q}_{\text{aus}}}{\bar{T}} - \frac{\dot{Q}_{\text{aus}}}{T_{\text{rea}}} = 0.045 \frac{\text{kW}}{\text{K}}$$

$$d) m_2 u_2 - m_1 u_1 = \Delta m_{12} (\text{heat}) + Q_R = 0, \text{ um } \text{Enthalpiefluss gleich}$$

$$\Delta m_{12} = m_2 u_2 - m_1 u_1 - Q_R$$

$$\cancel{\underline{m_2 u_2 - m_1 u_1}} = Q_R$$

$$u_1 = u_f(100^\circ\text{C}) + x_D (u_g(100^\circ\text{C}) - u_f(100^\circ\text{C})) = 429.38 \frac{\text{kJ}}{\text{kg}}$$

$$h_{\text{air}}(20^\circ\text{C}) = \frac{h_f}{T_2}(20^\circ\text{C}) = \cancel{888.71} \frac{\text{kJ}}{\text{kg}} 83.35 \frac{\text{kJ}}{\text{kg}}$$

$$u_2(70^\circ\text{C}) = \frac{u_f}{T_2}(70^\circ\text{C}) = 292.35 \frac{\text{kJ}}{\text{kg}}$$

~~Basis~~

$$\Delta m_{12} = m_2 - m_1$$

$$m_2 u_2 - m_1 u_1 = (m_2 - m_1) h_{\text{air}} + Q_R$$

$$m_2 = \frac{m_1 u_1 - m_1 h_{\text{air}} \cancel{+ Q_R}}{u_2 - h_{\text{air}}}$$

$$m_2 = \cancel{3813.82 \text{ kg}} 3511.72 \text{ kg}$$

$$\Delta m_{12} = \cancel{4058.82 \text{ kg}} 3756.72 \text{ kg}$$

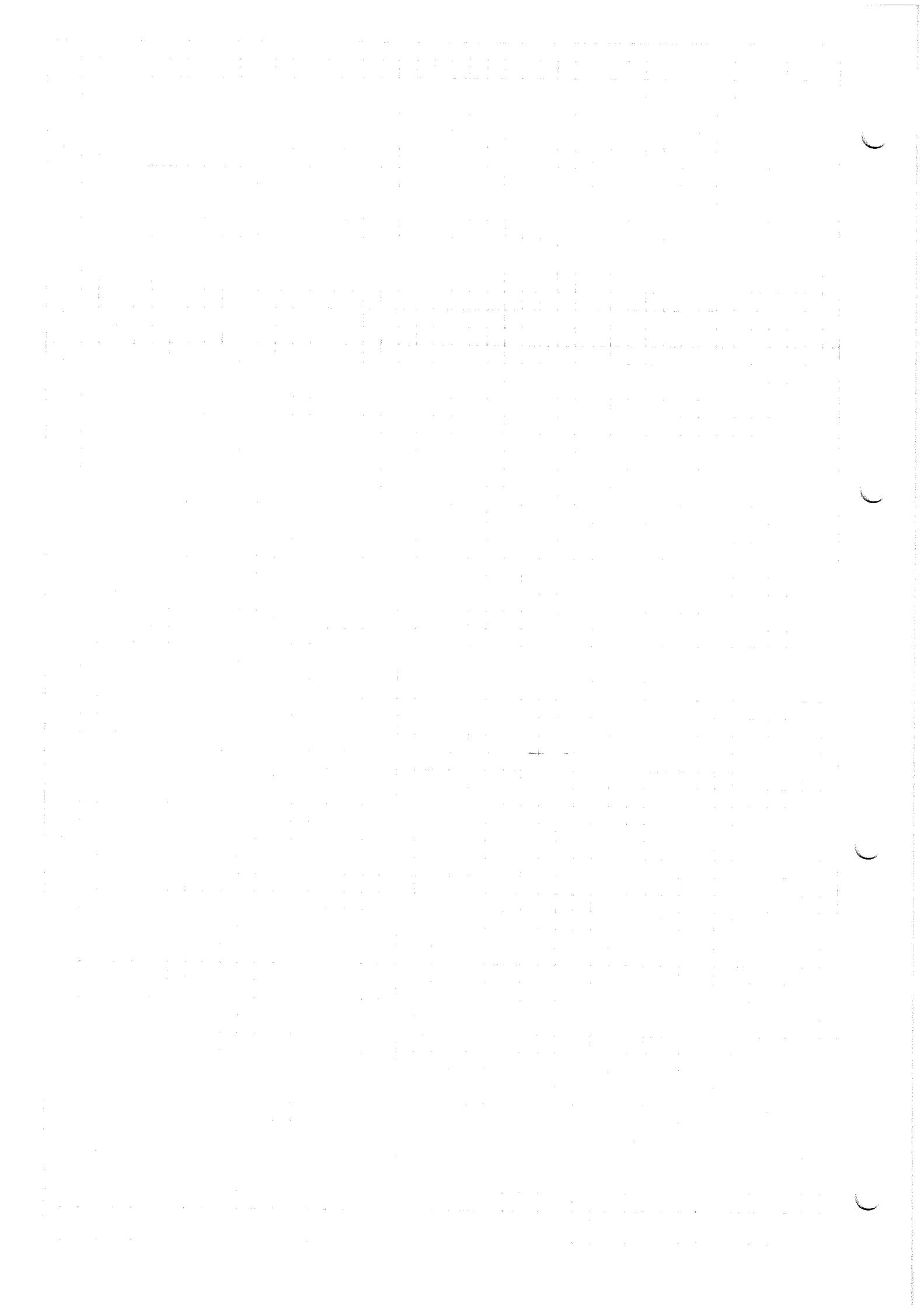
$$e) m_2 s_2 - m_1 s_1 = \Delta S_{12}$$

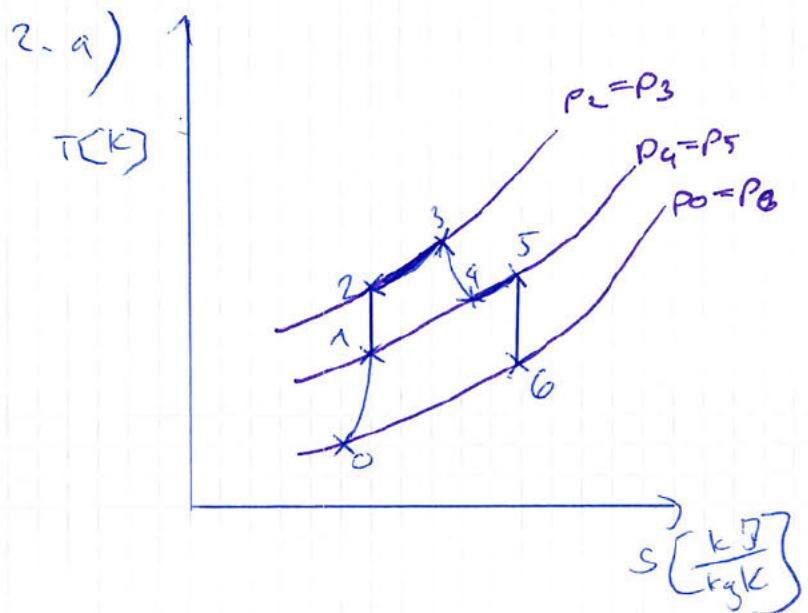
$$s_2 = \cancel{s_f(70^\circ\text{C})} 0.9549$$

$$s_1 = s_f(100^\circ\text{C}) + x_D (s_g(100^\circ\text{C}) - s_f(100^\circ\text{C})) = 1.33714$$

$$\cancel{0.52 - 3813.82 \frac{\text{J}}{\text{kg K}}} 1387.5 \frac{\text{J}}{\text{kg K}}$$

$$\Delta S = 1387.5 \frac{\text{J}}{\text{kg K}}$$





b) $5-6 \Rightarrow \text{isentrop} \Rightarrow \Delta s = 0$

~~$$0 \rightarrow \int_{T_5}^{T_6} c_v dT \Rightarrow 0 \rightarrow c_v \ln \left(\frac{T_6}{T_5} \right)$$~~

$$0 = c_p \ln \left(\frac{T_6}{T_5} \right) - R \ln \left(\frac{P_6}{P_5} \right)$$

$$\gamma = \frac{c_p}{c_v} \Rightarrow c_v = \frac{c_p}{\gamma} = 0.7186 \frac{\text{kJ}}{\text{kg} \cdot \text{K}}$$

$$R = c_p - c_v = 0.2874 \frac{\text{kJ}}{\text{kg} \cdot \text{K}}$$

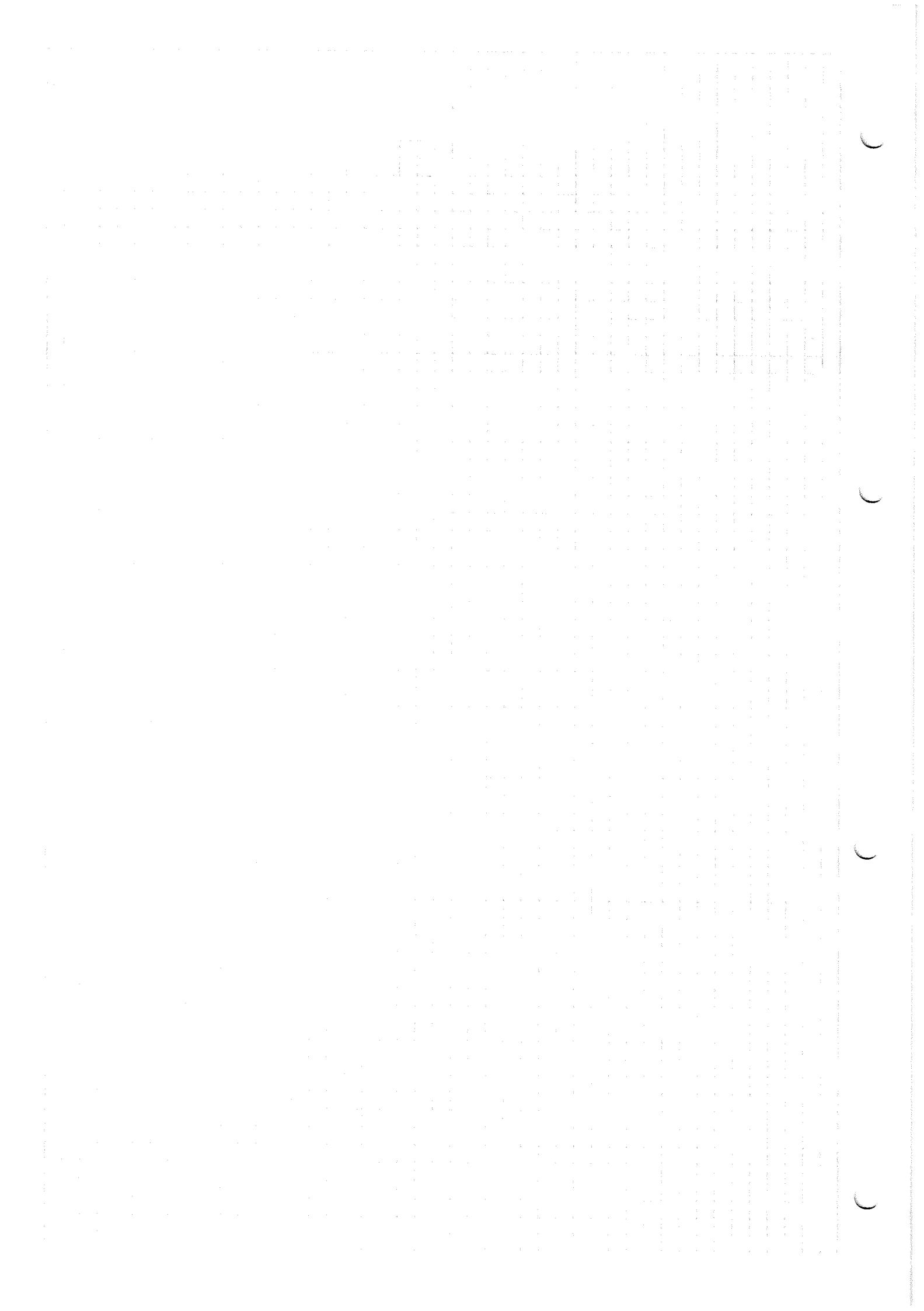
$$T_6 = T_5 e^{\frac{R}{c_p} \ln \left(\frac{P_6}{P_5} \right)}$$

$$T_6 = 328.084 \text{ K}$$

$$0 = m \left(h_5 - h_6 + \frac{(\omega_5^2 - \omega_6^2)}{2} \right) + \cancel{0} - \cancel{0} = 0$$

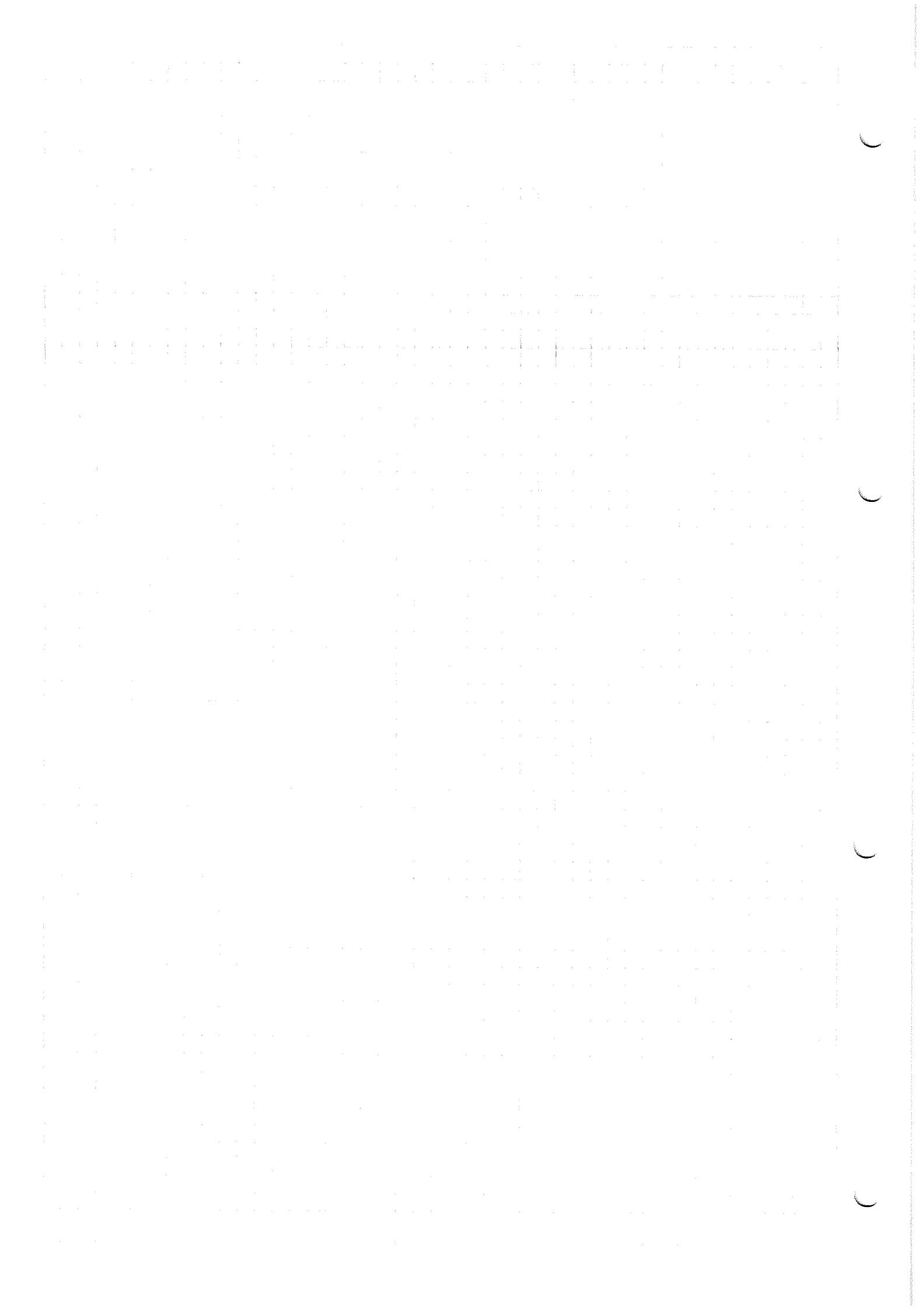
$$\omega_6 = \sqrt{2h_5 - 2h_6 + \omega_5^2} = \sqrt{2(c_p(T_5 - T_6) + \omega_5^2)}$$

$$= 507.23 \frac{\text{m}}{\text{s}}$$



$$\begin{aligned}
 c) \quad e_{\text{ext},t_0} - e_{\text{ext},t_0} &= (h_f - h_0 - T_0(s_0 - s_e) + k_e) = 0 \\
 &= c_p(T_0 - T_0) - T_0(c_p \ln\left(\frac{T_0}{T_0}\right) - R \ln\left(\frac{P_0}{P_0}\right)) + \frac{\omega_0^2 - \omega_0^2}{2} \\
 &= 120.802 \frac{\text{kJ}}{\text{kg}}
 \end{aligned}$$

$$\begin{aligned}
 d) \quad \dot{Q} &= \cancel{\Delta e_{\text{ext},t_0}} = 0 \\
 \dot{Q} &= (e_{\text{ext},t_0} + e_{\text{ext},t_0}) \cancel{\dot{m}} + \left(1 - \frac{T_0}{T_k}\right) \dot{Q} - \dot{W} - \dot{E}_{\text{ext},\text{vap}} \\
 \dot{E}_{\text{ext},\text{vap}} &= e_{\text{ext},t_0} - e_{\text{ext},t_0} + \left(1 - \frac{243.15K}{1289K}\right) 1195 \frac{\text{kJ}}{\text{kg}} \\
 \dot{E}_{\text{ext},\text{vap}} &= 840.78 \frac{\text{kJ}}{\text{kg}}
 \end{aligned}$$



$$3. a) \begin{array}{c} v_g = v_g \\ v_g \\ v_g \end{array}$$

$v_g(T_p) = v_g(T)$, weil inkompressible Flüssigkeit
 $v_f(500^\circ C) =$

$$p_1 \cdot A = p_0 \cdot A + m g$$

$$\Rightarrow p_{g,1} = p_0 + \frac{m g}{A} \quad A = \pi \cdot \frac{D^2}{4} = \frac{\pi}{400} \text{ m}^2$$

= 1.46 \text{ bar}

$$pV = mRT \quad R = \frac{R}{M} = \frac{8314 \frac{\text{J}}{\text{kmol K}}}{50 \frac{\text{kg}}{\text{kmol}}} = 166.28 \frac{\text{J}}{\text{kg K}}$$

$$m_1 = \frac{p_1 V_1}{R T_1} = 3.42 \cdot 10^{-3} \text{ kg} = 3.42 \text{ g}$$

b) $p_{g,2} = p_{g,1}$, da ~~da~~ keine zusätzliche Kraft, da Δz konst., & somit sich das Kräfteverhältnis nicht ändert

* $T_{g,2} = T_{EW,1}$, da $x_{EW,2} > 0$, muss nach EW sinken & somit kann die Temperatur nicht ansteigen, & da aus EW im thermodynamischen Gleichgewicht müssen die Temperaturen gleich sein

c) $m(u_2 - u_1) = \dot{Q} \cancel{\text{Stoffwechselrest}}$

$$0 + m(c_v(T_f - T_i)) = \dot{Q} \quad m = m_1 = m_2$$

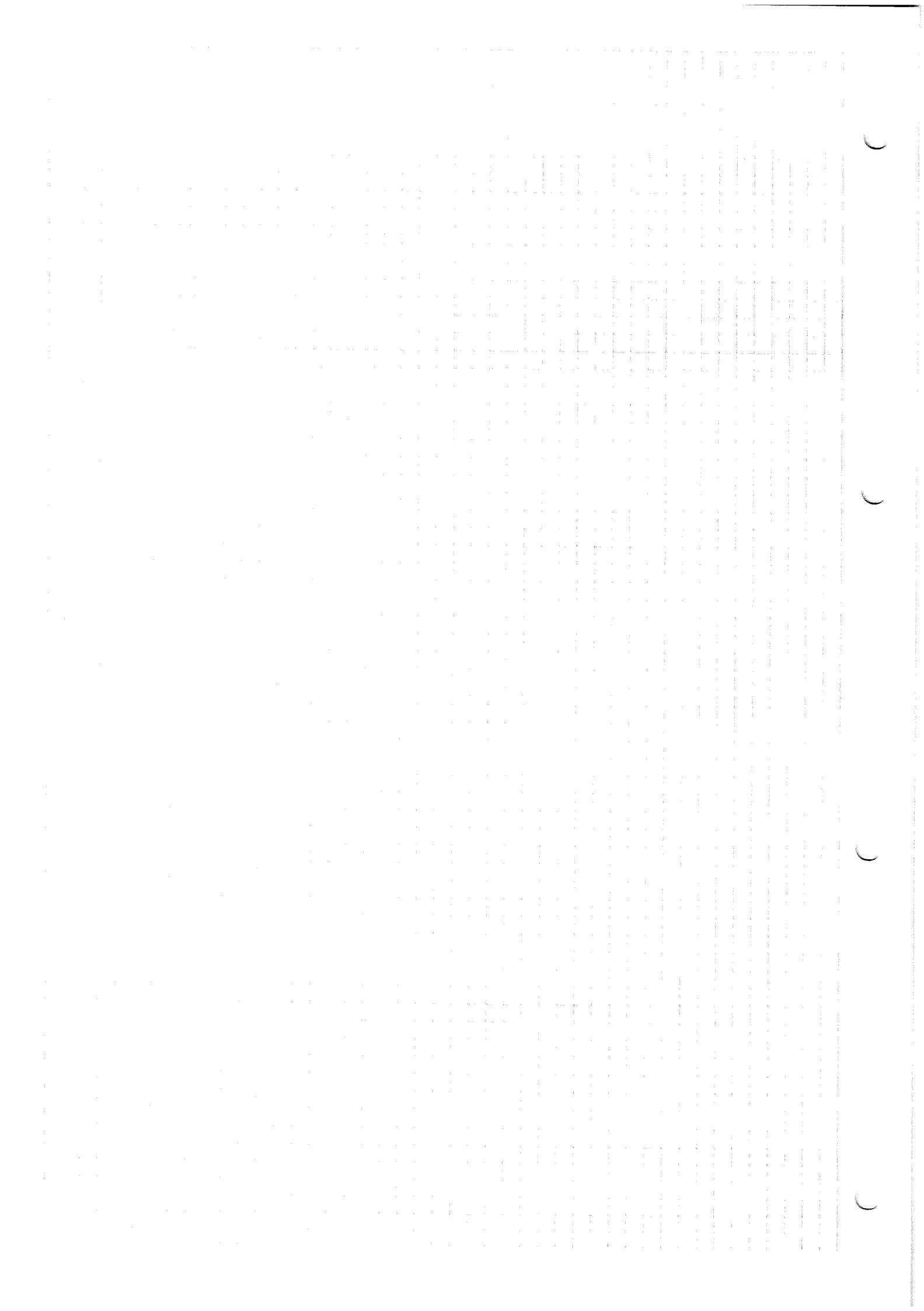
$\Rightarrow \dot{Q} = 1133.73 \text{ J}$

$$w_{EW} = p_1(v_2 - v_1) \cdot m = -3.724 \cdot 10^{-7} \text{ kJ}$$

wilreibungsfrei

$$v_1 = \frac{m R T_1}{p_1} = 3.14 \cdot 10^{-6} \frac{\text{m}^3}{\text{kg}}$$

$$v_2 = \frac{m R T_2}{p_2} = 1.109 \cdot 10^{-6} \frac{\text{m}^3}{\text{kg}}$$



$$d) m_{EW}(u_2 - u_1) + m_j(u_2 - u_1) = \cancel{d}^0 - \cancel{u}^0$$

$$\cancel{m_j(u_2 - u_1)} = \cancel{m_j}$$

$$P_g = P_{EW}$$

$$u_{1,EW} = u_1 - 333.438 \frac{kJ}{kg} + (-0.045 \frac{kJ}{kg} + 333.438 \frac{kJ}{kg}) = -133.41 \frac{kJ}{kg}$$

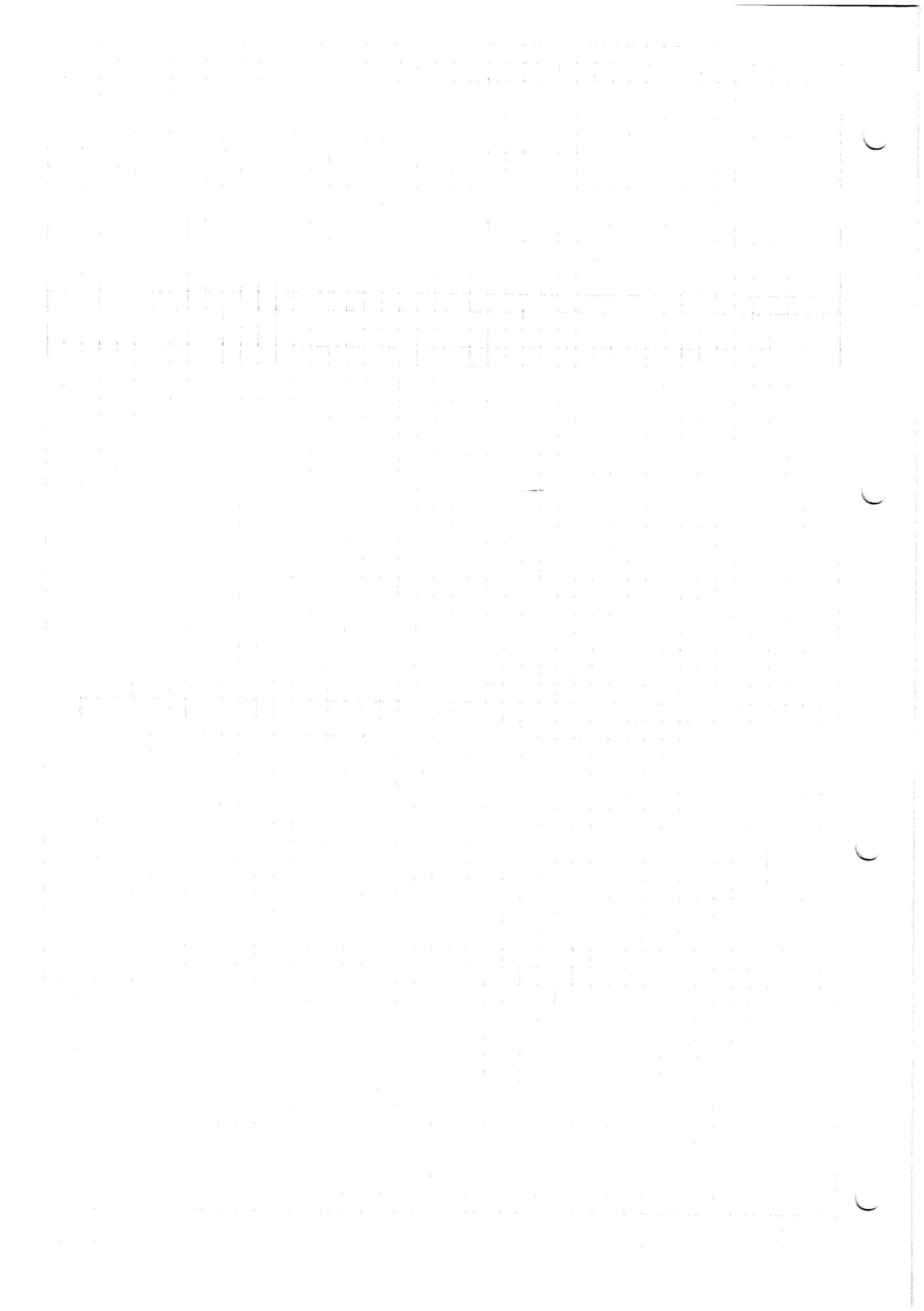
$$m_j(u_2 - u_1) = m_j c_v(T_2 - T_1) = -1.082 \text{ kJ}$$

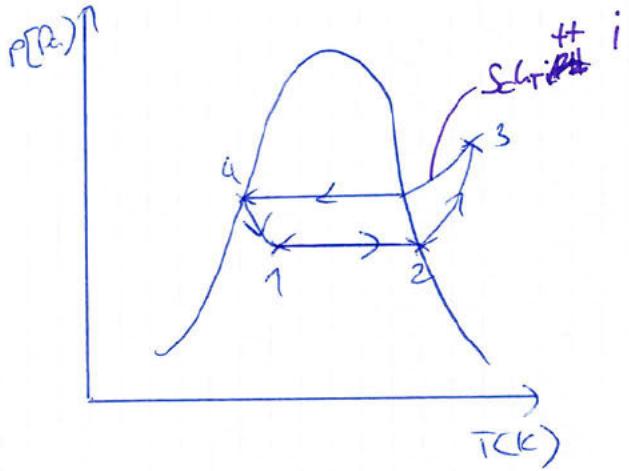
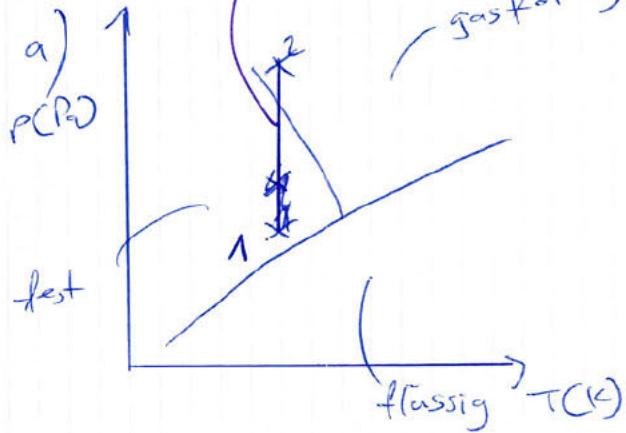
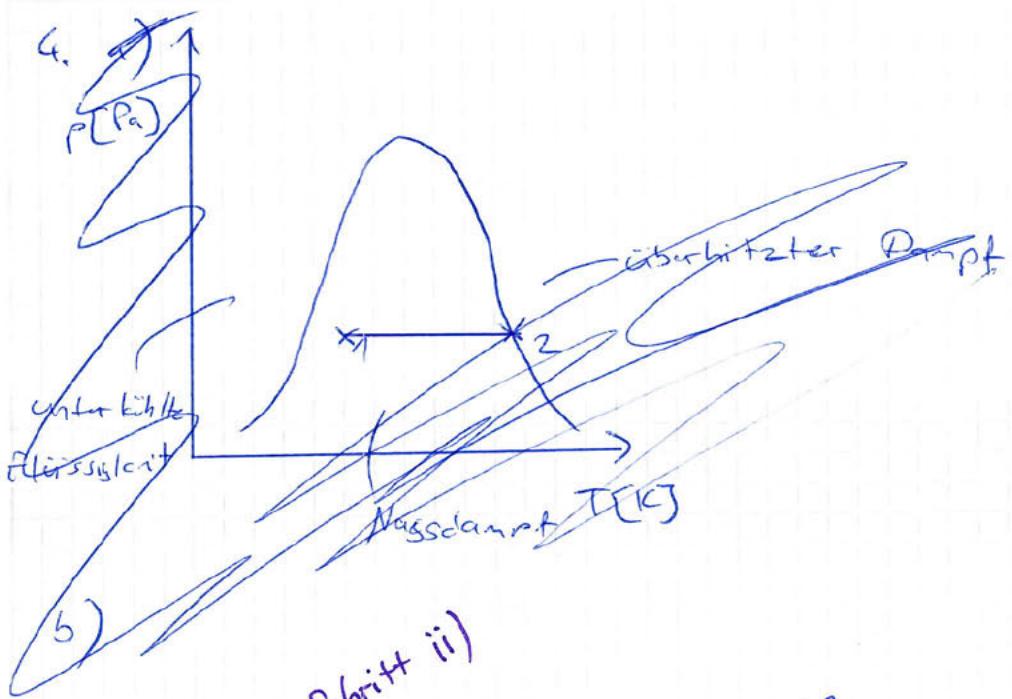
$$u_{2,EW} = u_1 + \frac{-m_j(u_2 - u_1)}{m_{EW}} = -122.52 \frac{kJ}{kg}$$

$$P_{2,EW} = P_{1,EW} = 1.45 \text{ bar}$$

$$T_{1,EW} = T_{2,EW}$$

$$x = \frac{u_{2,EW} + 333.438 \frac{kJ}{kg}}{-0.045 \frac{kJ}{kg} + 333.438 \frac{kJ}{kg}} = \frac{122.52 + 333.438}{-0.045 + 333.438} = 0.632$$





$$b) \quad 0 = m_2(h_2 - h_3) + \cancel{Q} - \cancel{i_k} \quad \stackrel{=0}{\text{---}}$$

$$h_2 = \dot{t}_{sg}(T_{2,15}) = h_g(277.15K) = 249.53 \frac{kg}{kg}$$

$$s_2 = s_3 = s_g(24^\circ C) = 0.9163 \frac{kg}{kg \cdot K}$$

$$T_1 = 10^\circ\text{C} = 283.15\text{ K}$$

$$P_{T+pre} = G_{ab} b_{at}$$

$$P_1 = 1 \text{ mbar} = P_2$$

$$T_2 = 283.15K - 6K = 277.15K$$

$$h_5(85_{\text{air}}) = s_i - s_f \quad (h_g - h_f) + h_g =$$

5) ~~Fr~~

~~Fr~~

c) $h_1 = h_4$, da adiabate Drossel

$$h_{c1} = h_f(85 \text{ bar}) = 33.42 \frac{\text{kJ}}{\text{kg}}$$

~~Fr~~ (sobald)

$$x_1 = \frac{h_1 - h_f(40^\circ\text{C})}{h_g(40^\circ\text{C}) - h_f(40^\circ\text{C})} = \overset{\text{TAB A-10}}{0.194}$$

d) $\varepsilon_k = \frac{\dot{Q}_{zu}}{\dot{w}_t} = \dot{Q}_k$
 $(= \dot{w}_k)$

mit eingesetzten Werten rechnen

$$0 = \dot{m}_R (h_1 - h_2) + \dot{Q}_k$$

$$\Rightarrow \dot{Q}_k = \dot{m}_R (h_2 - h_1) = \text{ca } 156.28 \text{ W}$$

$$h_1 = h_4$$

$$h_2 = h_g(-22^\circ\text{C}) = \overset{\text{TAB A-10}}{239.08} \frac{\text{kJ}}{\text{kg}}$$

$$\varepsilon_k = 5.58$$

e) Die Temperatur würde abnehmen, da mit im festen Bereich und f. Sonst kann Wärme abgenommen werden, sich die Temperatur senken muss.