

Aufgabe 1

E-Bilanz Reaktor: (stationär) (siedendes Wasser)

a)

~~$$0 = \dot{m}_{\text{ein}} (h_{\text{ein}}) + \dot{Q}_R + \dot{Q}_{\text{aus}}$$~~

$$0 = \dot{m}_{\text{ein}} (h_{\text{ein}} - h_{\text{aus}}) + \dot{Q}_R + \dot{Q}_{\text{aus}} \quad | \quad \dot{m}_{\text{ein}} = \dot{m}_{\text{aus}}$$

Tab A-2:

$$h_{\text{ein}} = h_f(70^\circ\text{C}) = 292.98$$

↑
siedende Flüssigkeit

$$h_{\text{aus}} = h_g(700^\circ\text{C}) = 479.04$$

$$\dot{Q}_{R, \text{aus}} = \dot{m}_{\text{ein}} (h_{\text{aus}} - h_{\text{ein}}) + \dot{Q}_R = \underline{137.818 \text{ kW}}$$

b)

Entropiebilanz KÜHlF:

~~$$0 = \dot{m}_{\text{KF}} (s_{\text{ein}} - s_{\text{aus}}) + \frac{\dot{Q}_{\text{aus}}}{T} + \dot{S}_{\text{erz}}$$~~

0, da Druck sich nicht ändert → reversibel

E-Bilanz KF: von KF

~~$$0 = \dot{m}_{\text{KF}} (h_{\text{ein}} - h_{\text{aus}}) + \dot{Q}_{\text{aus}}$$~~

$$\bar{T} = \frac{\int_{s_{\text{KF, ein}}}^{s_{\text{KF, aus}}} T ds}{s_{\text{KF, aus}} - s_{\text{KF, ein}}} = \frac{q_{\text{rev}}}{s_2 - s_1} = \frac{h_2 - h_1}{s_2 - s_1}$$

$$s_2 = s_{\text{KF, aus}}$$

$$s_1 = s_{\text{KF, ein}}$$

$$h_2 - h_1 = c (T_2 - T_1) + v (p_2 - p_1)$$

$$s_2 - s_1 = c \cdot \ln\left(\frac{T_2}{T_1}\right)$$

| c = Wärmekapazität des KF

$$\bar{T} = \frac{c (T_2 - T_1)}{c \cdot \ln\left(\frac{T_2}{T_1}\right)} = \frac{T_2 - T_1}{\ln\left(\frac{T_2}{T_1}\right)} = \underline{293.72 \text{ K}}$$

$$T_1 = T_{\text{KF, ein}}$$

$$T_2 = T_{\text{KF, aus}}$$

Rückseite!

aufgabe c auf separatem Blatt

d) E-Bilanz: $\Delta E = \Delta U$; $Q_{R,12} = -35 \text{ MJ}$

$$\Rightarrow U_2 - U_1 = \Delta m_{12} \cdot h(20^\circ\text{C}) + Q_{R,12}$$

$$m_{\text{ges},1} = 5755 \text{ kg} = m_1$$

$$m_{\text{ges},2} = m_{\text{ges},1} + \Delta m_{12} = m_2$$

$$\Rightarrow m_2 U_2 - m_1 U_1 = \Delta m_{12} \cdot h(20^\circ\text{C}) + Q_{R,12}$$

$$\Delta m_{12} (U_2 - h(20^\circ\text{C})) = m_1 (U_1 - U_2) + Q_{R,12}$$

$$\Delta m_{12} = \frac{m_1 (U_1 - U_2) + Q_{R,12}}{U_2 - h(20^\circ\text{C})}$$

Tab A-2:

$$h(20^\circ\text{C}) = h_f(20^\circ\text{C}) = ~~83.96~~ 83.96$$

siedende flüssigkeit
 $U_2 = U_f(70^\circ\text{C}) = 292.95$

$$~~U_2 = U_f(20^\circ\text{C}) = ~~83.96~~ 83.95~~$$

$$U_1 = U_f(100^\circ\text{C}) = 418.94$$

$$\Rightarrow ~~\Delta m_{12}~~$$

$$\Rightarrow \Delta m_{12} = 3302 \text{ kg}$$

e) S-Bilanz:

$$\Delta S_{12} = \Delta m_{12} (S(20^\circ\text{C})) + \frac{Q_{R,12}}{\bar{T}} + S_{\text{erz}} \quad \bar{T} = 295 \text{ K}$$

Tab A-2

Tab A-2:

$$S(20^\circ\text{C}) = S_f(20^\circ\text{C}) = 0.2966$$

$$\Delta S_{12} = m_2 \cdot S_2 - m_1 \cdot S_1$$

$$m_2 = m_1 + \Delta m_{12} = 9056 \text{ kg}$$

Tab A-2:

$$S_2 = S_f(70^\circ\text{C}) = 0.9549$$

$$S_1 = S_f(100^\circ\text{C}) = 1.3069$$

$$\Rightarrow \Delta S_{12} = 1126.36 \text{ kJ/K}$$

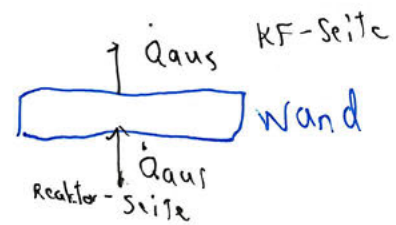
Aufgabe 1

c) * S-Bilanz ~~KW~~: Kühlwand:

$$0 = \frac{|\dot{Q}_{\text{aus}}|}{T_{\text{Reaktor},1}} + - \frac{\dot{Q}_{\text{aus}}}{\bar{T}} + \dot{S}_{\text{erz}}$$

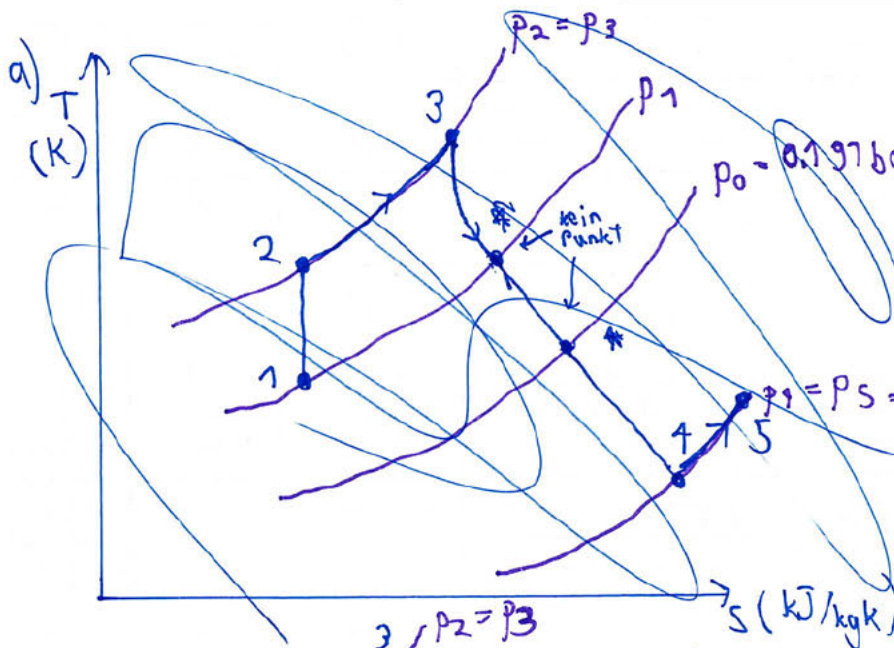
$$\Rightarrow \dot{S}_{\text{erz}} = \dot{Q}_{\text{aus}} \left(\frac{1}{\bar{T}} - \frac{1}{T_{\text{Reaktor},1}} \right)$$

$$\Rightarrow \dot{S}_{\text{erz}} = 0.1008 \text{ kW/K}$$



$$|\dot{Q}_{\text{aus}}| = 137.878 \text{ kW}$$

Aufgabe 2



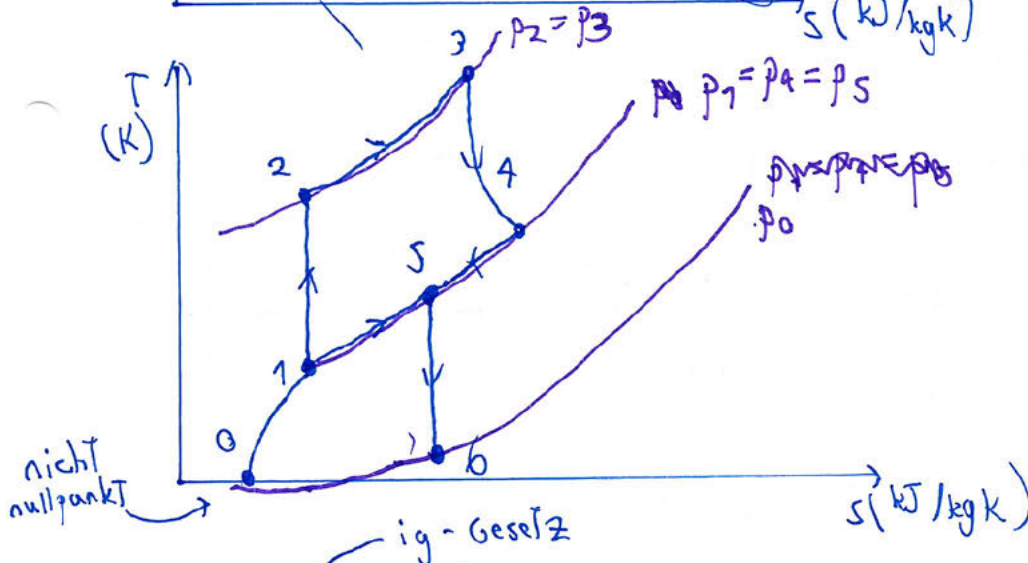
$$p_2 = p_3$$

$$s_1 = s_2$$

$$p_4 = p_5 = 0.5 \text{ bar}$$

$$p_1 = 0.5 \text{ bar}$$

$$s_5 = s_6$$



b)

$$h_5 = c_p \cdot T_5 = 434.49 \text{ kJ/kg}$$

E-Bilanz Schubdüse: adiabät $\dot{Q} = 0$; stationär

$$0 = \dot{m}_{ges} (h_5 - h_6 + \frac{1}{2} w_5^2 - \frac{1}{2} w_6^2)$$

$$\Rightarrow h_6 = h_5 + \frac{1}{2} (w_5^2 - w_6^2)$$

T_6 : $s \rightarrow 6$ isentrop $\Rightarrow \kappa = k$ $p_6 = p_0$
polytropes T-Verhältnis:

$$T_6 = T_5 \cdot \left(\frac{p_0}{p_5} \right)^{\frac{\kappa-1}{\kappa}} = 293.9 \text{ K} \quad | \quad h_6 = c_p \cdot T_6$$

$$\Rightarrow w_6 = \left(2 \cdot (h_5 - h_6) + w_5^2 \right)^{1/2} = 571 \text{ m/s}$$

Rückseite!

$$c) \Delta e_{x, str} = h_6 - h_0 - T_0 (s_6 - s_0) + p_0 (v_6 - v_0)$$

$$h_6 - h_0 = c_p (T_6 - T_0) = 57.05 \text{ kJ/kg}$$

$$s_6 - s_0 = c_p \cdot \ln\left(\frac{T_6}{T_0}\right) - R \cdot \ln\left(\frac{p_6}{p_0}\right) = 0.191 \text{ kJ/kgK}$$

$p_6 = p_0$

$$R = c_p - \frac{c_p}{\text{ig-Gas}} = 0.287 \text{ kJ/kgK}$$

$$p_6 = \dots \quad v_6 = \frac{RT_6}{p_6} = 4.416 \text{ m}^3/\text{kg}$$

$$v_0 = \frac{RT_0}{p_0} = 3.653 \text{ m}^3/\text{kg}$$

$$\Delta e_{x, str} = \underline{19.78 \text{ kJ/kg}}$$

d) keine Arbeit wird zugeführt nur die Ströme und Wärme ~~q_0~~ q_0
Energie-Bilanz Gesamtsystem: (stationär)

$$0 = \dot{m}_{ges} (-\Delta e_{x, str}) + \dot{E}_{x, Q_0} - \dot{E}_{x, verl}$$

$$\dot{E}_{x, Q_0} = \left(1 - \frac{T_0}{T_B}\right) \cdot \dot{Q}_B = \dot{m}_K \left(1 - \frac{T_0}{T_B}\right) \cdot q_B$$

$$\dot{m}_{ges} = \dot{m}_K + \dot{m}_M = \dot{m}_K + 5.293 \cdot \dot{m}_K = 6.293 \dot{m}_K$$

$$\Rightarrow \dot{m}_K = \frac{\dot{m}_{ges}}{6.293}$$

$$\Rightarrow 0 = -\Delta e_{x, str} + \frac{1}{6.293} \left(1 - \frac{T_0}{T_B}\right) \cdot q_B - e_{x, verl}$$

$$e_{x, verl} = \frac{1}{6.293} \left(1 - \frac{T_0}{T_B}\right) q_B - \Delta e_{x, str} = \underline{134.89 \text{ kJ/kg}}$$

$$| \Delta e_{x, str} = 19.78 \text{ kJ/kg}$$

Aufgabe 3

a) $R_g = \frac{\bar{R}}{M_g} = 166.28 \text{ J/kgK}$ | $A = \frac{\pi D^2}{4} = 0.0078 \text{ m}^2$

Kräfte-GGW
↓

$$p_{g,1} \cdot A = m_K \cdot g + p_{\text{amb}} \cdot A + m_{\text{EW}} \cdot g$$

~~$p_{g,1} = \frac{m_K \cdot g}{A} + p_{\text{amb}} = 1.38 \text{ bar}$~~ $p_{g,1} = \frac{(m_K + m_{\text{EW}}) \cdot g}{A} + p_{\text{amb}} = 1.4 \text{ bar}$

$$m_g = \frac{p_{g,1} \cdot V_{g,1}}{R T_{g,1}} = 3.42 \text{ g}$$

b) $p_{g,2} \stackrel{!}{=} p_{g,1} = 1.4 \text{ bar}$, da immer noch der gleiche Druck durch Atmosphäre und Gewicht wirkt.

~~reibungsfrei~~ \rightarrow reibungsfrei und adiabat \rightarrow reversibel \rightarrow ~~$n = k$~~

~~$k = \frac{R + C_V}{C_V} = 1.263$~~

~~polytropes T-Verhältnis $\Rightarrow T_{g,2} = T_{g,1} \left(\frac{p_2}{p_1} \right)^{\frac{k-1}{k}} = 773.15 \text{ K}$~~

c) ~~$T_{g,2} = 0.003 \text{ K}$~~

Rückseite!

c) $T_{g,2} = 0.003^\circ\text{C}$

E-Bilanz Gas:

$$u_2 - u_1 = Q_{12} - \int_1^2 p dV \stackrel{\text{isobar}}{\downarrow} = Q_{12} - p_1 (V_2 - V_1)$$

$$V_2 = \frac{m R T_2}{p_2} = 0.0011 \text{ m}^3$$

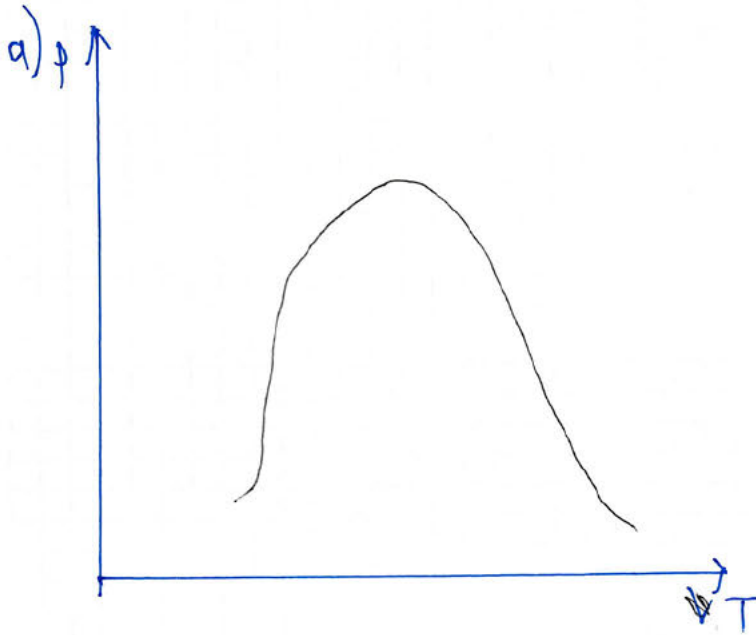
$$u_2 - u_1 = c_v (T_2 - T_1) = -316.498 \text{ kJ/kg}$$

$$Q_{12} = m_g (u_2 - u_1) + p_1 (V_2 - V_1) = -286.68 \text{ kJ} - 1398.9 \text{ kJ} = -1400 \text{ kJ}$$

d)

$$x_{\text{Eis},2} = \frac{u_{2,\text{eis}} - u_f}{u_{\text{fest}} - u_f}$$

Aufgabe 4



$$\begin{aligned}h_1 &= h_4 \\p_1 &= p_2 \\p_3 &= p_4 = 8 \text{ bar} \\s_2 &= s_3\end{aligned}$$

b) Tab A-11

$$h_4 = h_f(8 \text{ bar}) = 93.42 \text{ kJ/kg}$$

$h_1 = h_4$, da isenthalpe drossel

~~z.B. 11~~