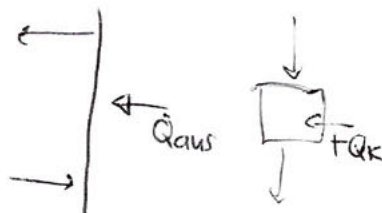
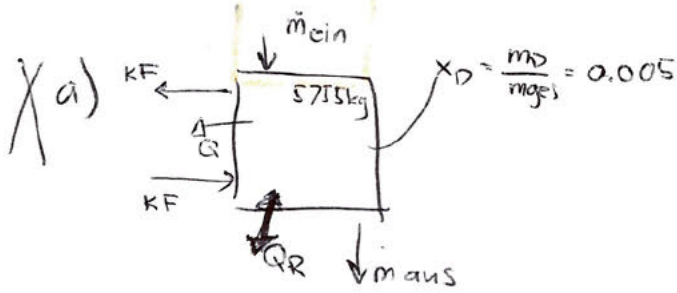


Aufgabe 1

stationär



$\approx 0 \text{ stat}$

$$\frac{dE}{dt} = \dot{m}_{in} h_1 - \dot{m}_{aus} h_2 + \dot{Q} - \dot{W}_E = 0$$

$$0 = \dot{m} (h_1 - h_2) + \dot{Q}_k + \dot{Q}_R + \dot{Q}_k$$

$$\dot{Q} = \dot{m} (h_2 - h_1) = 0.3 \frac{\text{kg}}{\text{s}} (419.04 - 292.98)$$

siedende flüssigkeit

$$h_2(100^\circ\text{C}, x_2=0) = h_g(100^\circ\text{C}) \stackrel{\text{TAB A2}}{=} 419.04 \frac{\text{kJ}}{\text{kg}}$$

$$h_1(70^\circ\text{C}, x_1=0) = 292.98 \frac{\text{kJ}}{\text{kg}} \stackrel{\text{TAB A2}}{=}$$

$$= 37.818 \text{ kW} + \underbrace{\dot{Q}_k}_{100 \text{ kW}} = 100037.818 \text{ W}$$

b)

$$\bar{T}_{KF} = \frac{\int_{S_a}^e T ds}{S_a - S_e} = \frac{\dot{Q}}{c_{if} \ln\left(\frac{T_2}{T_1}\right)} = \frac{c_{if} (T_2 - T_1)}{c_{if} \ln\left(\frac{T_2}{T_1}\right)} = \frac{T_2 - T_1}{\ln\left(\frac{T_2}{T_1}\right)} = 293.1216 \text{ K}$$

\uparrow idfalle flüssigkeit

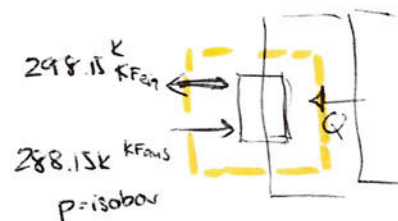
$$T_2 = 288.15 \text{ K}$$

$$T_1 = 298.15 \text{ K}$$

$$c) \dot{S}_{erz} = \dot{P} \stackrel{!}{=} 0 \text{ stat}$$

$$\frac{dS}{dt} = \dot{m}_{KF} (h_e - h_a) + \frac{\dot{Q}_{aus}}{\bar{T}_{KF}} + \dot{S}_{erz}$$

$$\dot{S}_{erz} = \dot{m} (h_a - h_e) - \frac{\dot{Q}_{aus}}{\bar{T}_{KF}}$$



$$\dot{Q}_{aus} = 65 \text{ kW}$$

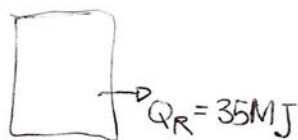
$$\bar{T}_{KF} = 295 \text{ K}$$

$$h_a(298.15 \text{ K}) = h_f(T_2) + v_f^T (p - p_{sat}(T))$$

$$h_e(288.15 \text{ K}) = h_f(T_1) + v_f^T (p - p_{sat}(T))$$

$$\left. \begin{array}{l} h_a(298.15 \text{ K}) = h_f(T_2) + v_f^T (p - p_{sat}(T)) \\ h_e(288.15 \text{ K}) = h_f(T_1) + v_f^T (p - p_{sat}(T)) \end{array} \right\} \Delta h = h_f(T_2) - h_f(T_1) = c_{if} \cdot (T_2 - T_1)$$

$$d) \Delta E = Q - \overset{\substack{v = \text{const} \\ p = \text{const}}}{W_v} = m_2 u_2 - m_1 u_1$$



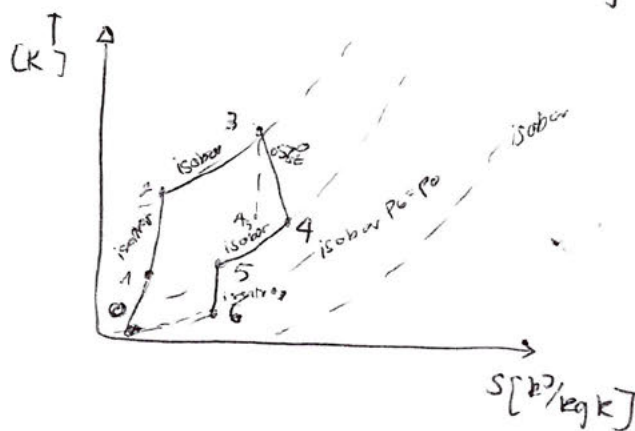
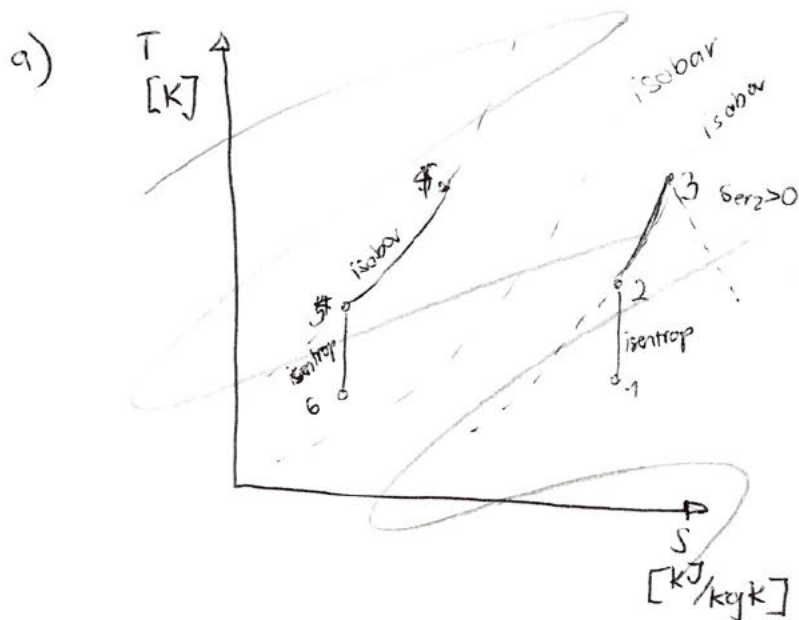
$$m_2 u_2 - m_1 u_1 = \Delta m \cdot h_f(20^\circ \text{C}) + Q_R$$

$$m_2 = m_1 + \Delta m$$

$$@ 2, x_2 = 0, 70^\circ \text{C} \rightarrow u_f(70^\circ \text{C}) = 292.95 \frac{\text{kJ}}{\text{kg}} \text{ (TAB A2)}$$

$$e) \Delta S = S_2 - S_1 = m_2 s_2 - m_1 s_1 = \Delta m s(20^\circ \text{C}) + \frac{Q}{\bar{T}_f} + \dot{S}_{erz}$$

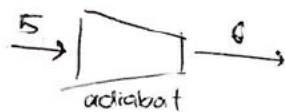
Aufgabe 2



	P	T	V
1	0.191	-30°C	
2	$P_2 = P_3$		$s_1 = s_2$
3			
4	0.5 $P_4 = P_5$		
5	0.5	431.9	$w_5 = 220 \text{ m/s}$ $s_5 = s_6$
6	0.191		

$$\dot{m}_{\text{ges}} \begin{cases} \rightarrow \dot{m}_M \\ \rightarrow \dot{m}_K \end{cases}$$

b) $w_6 = ?$, $T_6 = ?$



$$s_5 = s_6$$

$$\frac{dE}{dt} = \dot{m}_{\text{ges}} \left(h_5 - h_6 + \frac{w_5^2}{2} - \frac{w_6^2}{2} \right) + \dot{Q} - \dot{W}_e$$

i.g. $c_p \cdot (T_5 - T_6)$

$$(s_6 = s_5)$$

$$T_6 = T_5 \left(\frac{P_6}{P_5} \right)^{\frac{n-1}{n}} = 431.9 + 328.075 \text{ K}$$

$$n = 1.4$$

$$\rightarrow c_p (T_6 - T_5) - w$$

$$1006 \frac{\text{kJ}}{\text{kg K}}$$

$$c_p (T_5 - T_6) + \frac{w_5^2}{2} = \frac{w_6^2}{2} = 128647.95$$

$$\rightarrow w_6 = 507.24 \frac{\text{m}}{\text{s}}$$



$$\Delta \dot{E}_{x, str, 0,6} = \dot{m} \left[h_6 - h_0 - T_0 (s_6 - s_0) + \frac{w_6^2}{2} \right] \quad | : \dot{m}_{ges}$$

$$\Delta \dot{E}_{x, str} = 12.1586 \frac{\text{kJ}}{\text{kg}} + \frac{w_6^2}{2}$$

$$= \underline{\underline{116.487 \frac{\text{kJ}}{\text{kg}}}}$$

$$h_6 - h_0 = c_p (T_6 - T_0) + \underbrace{v^t (p_6 - p_0)}_{=0}$$

$$= 85.434 \frac{\text{kJ}}{\text{kg}}$$

$$T_6 = 328.075 \text{ K}$$

$$T_0 = -30 + 273.15 = 243.15 \text{ K}$$

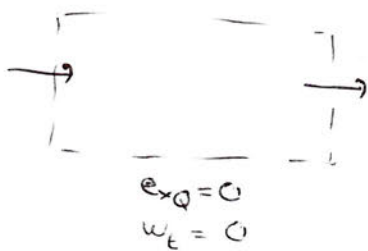
$$s_6 - s_0 = c_p \ln \left(\frac{T_6}{T_0} \right) = 0.3014 \frac{\text{kJ}}{\text{kg K}}$$

$$w_6 = 507.24 \frac{\text{m}}{\text{s}}$$

$$\frac{w_6^2}{2} = 128646$$

d) $e_{x, verl} = ?$ adiabatic

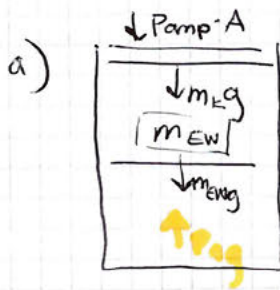
$$\frac{d\dot{E}_x}{dt} = \Delta \dot{E}_{x, str} + - e_{x, verl}$$



$$e_{x, verl} = \Delta e_{x, str} = 116.487 \frac{\text{kJ}}{\text{kg}}$$

et

Aufgabe 3



$$A = \pi \cdot \frac{D^2}{4} = 25\pi = 78.54 \text{ cm}^2$$

$$= \pi \cdot \frac{0.177^2}{4} = 0.00785 \text{ m}^2$$

$$P_{1,g} = \overbrace{P_{\text{Pump}}}^{10^5 \text{ Pa}} + \underbrace{\frac{m_K}{A} g}_{\left(9.806 \frac{\text{m}}{\text{s}^2}\right)} + \frac{m_{\text{EW}}}{A} g$$

$$\approx 140078.09 \text{ Pa}$$

$$= \underline{1.4 \text{ bar}}$$

$$V_{g,1} = V_g \cdot m_g$$

$$\rightarrow m = \frac{P_{g,1} V_{g,1}}{R T_{g,1}} = \frac{140099 \cdot V_{g,1}}{R \cdot T_{g,1}} = 0.003432 \text{ kg} = \underline{3.4 \text{ g}}$$

$$R = C_v (K - 1) = \frac{\bar{R}}{M} = \frac{8.314 \text{ J/mol K}}{50 \text{ kg/kmol}} = 166.28$$

$$\uparrow 0.633 \frac{\text{kJ}}{\text{kg}}$$

$$V_{g,1} = 3.14 \text{ L} = 3.14 \cdot 10^{-3} \text{ m}^3$$

$$T_{g,1} = 500 + 273.15$$

- b) $P_{g,2} = P_{g,1} = 1.4 \text{ bar}$, weil in der Zustandsänderung nur es keine zusätzliche Masse gegeben, die $P_{g,1}$ entgegenwirken muss (da EW konstante Masse & Kolben auch)

~~T~~ T von Eis ist auch konst weil Aggregatzustand ändert (bei konst p & T)

$$T_{g,2}$$

$$T = \frac{P V}{n R T} \quad (\text{weil } V \downarrow \text{ ist auch } T \downarrow)$$

& rest konstant

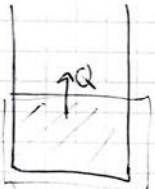
c) @ Zustand 2 GGW $\rightarrow \Delta U = 0$

i.g.

$$\Delta U = \underbrace{\Delta U_{\text{gas}}}_{c_v(T_{2g} - T_{1g})} + \underbrace{\Delta U_{\text{EW}}}_{c_{if}(T_{2w} - T_{1w})}$$

$$T_{2g} = T_{2w} = 0.003^\circ\text{C}$$

=



$$\Delta E = Q - W_v = 0$$

$$Q = W_v \Rightarrow q = w_v = \frac{R(T_2 - T_1)}{1 - \eta}$$

$$R = c_v(k - 1)$$

$$\frac{R}{c_v} + 1 = k$$

X

geschlossenes System:

$$\Delta E = m(u_2 - u_1) = Q$$

$$c_v(T_2 - T_1)$$

d) $x_{\text{Eis},2}$

$$\Delta U = Q$$

$$T_{\text{Eis}} = 0.003^\circ\text{C}$$

$$p_{\text{stat}}^2 = p_{\text{comb}} + m_{\text{E}} u$$

$$x_{\text{Eis},1} = \frac{m_{\text{Eis}}}{m_{\text{EW}}} = 0.6 \rightarrow m_{\text{Eis}} = 0.6 \cdot 0.1 \text{ kg}$$

$$@ 0^\circ\text{C} = T_{\text{Eis}}$$

$$u_2 = 334.5 \text{ zB.}$$

$$u_2 - u_1 = c_{if}(T_2 - T_1)$$

$$\rightarrow u_2 = c_{if}(T_2 - T_1) + u_1$$

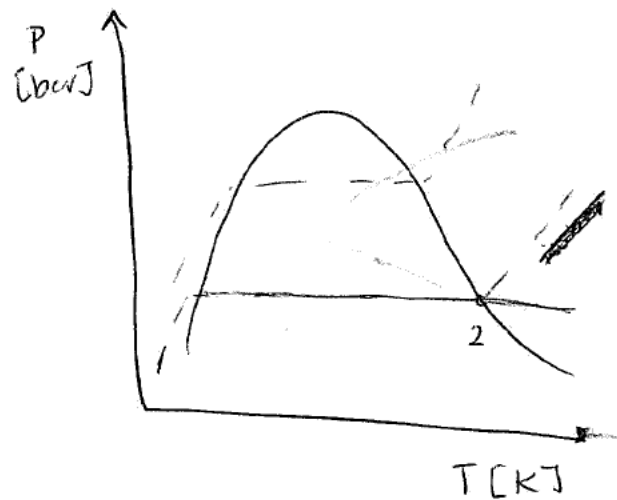
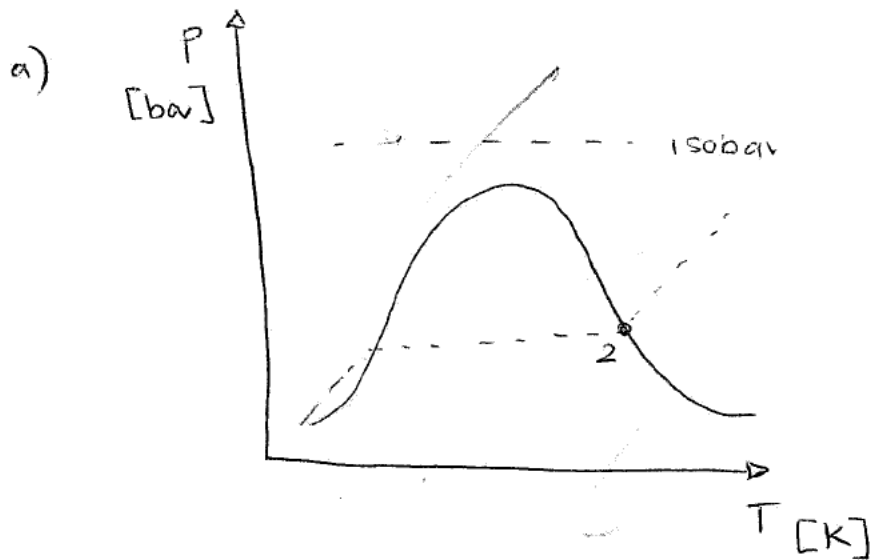
\rightarrow interpolieren

$$\rightarrow @ p = 1 \text{ bar}, T = 0.003$$

interpoliere für x

$$x = \frac{u_2 - u_f}{u_g - u_f}$$

Aufgabe 4



	P	T	v
1	p_u		
2	p_u 8 bar	-22°C	
3	8 bar		
4	8 bar		

$$q_{41} = 0$$

$$p_u = 5 \text{ bar} + p_{TP}$$

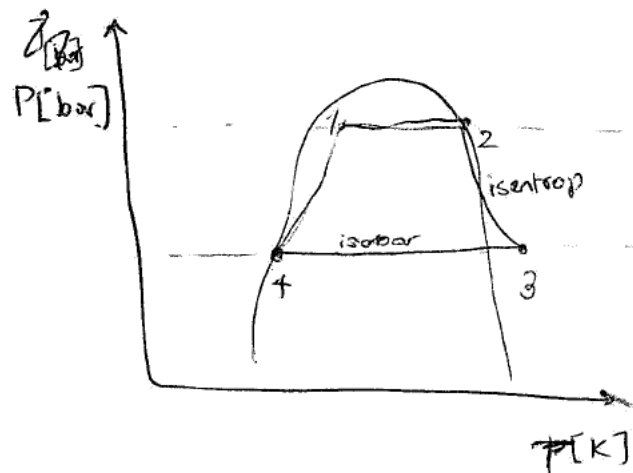
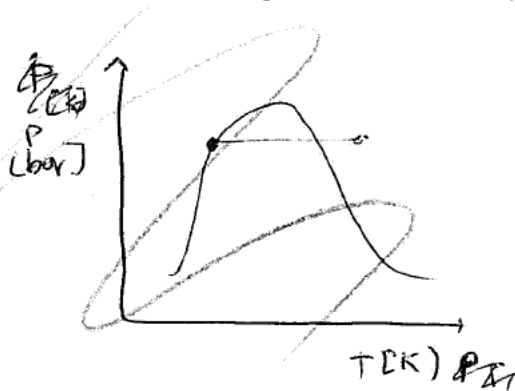
$$T_i - 10 \text{ K} = T_{\text{sublimationspunkt}}$$

$$x_2 = 1$$

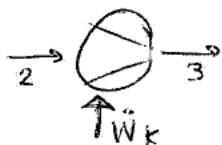
$$x_3 = 1 \quad S_3 = S_2$$

$$x_4 = 0$$

$$T_i - T_3 = 6 \text{ K}$$



b) $\dot{m}_{R134a} = ?$



$$\text{1.H.S.} \quad \frac{dE}{dt} = \dot{m}_R (h_2 - h_3) + \overset{\text{adiabatisch}}{\cancel{Q}} - \dot{W}_k$$

$$\frac{\dot{W}_k}{h_2 - h_3} = \dot{m}_{R134a}$$

$$h_2(8 \text{ bar}, x_2 = 1) = h_g(8 \text{ bar}) \stackrel{\text{TAB A11}}{=} 264.15 \frac{\text{kJ}}{\text{kg}}$$

$$h_3(8 \text{ bar}, S_2) \Rightarrow \text{interpolieren @ 8 bar mit } S_2 : h_3 = \frac{h(s_x) - h(s_y)}{s_x - s_y} (S_2 - S_y) + h_y$$

$$S_2(8 \text{ bar}, x = 1) \stackrel{\text{TAB A11}}{=} 0.9066 \frac{\text{kJ}}{\text{kg K}} = S_3$$

c) Drossel \sim isenthalp, isotherm

$$x_4 = 0 \quad p_4 = 8 \text{ bar} \quad \leadsto h_4 = 93.42 \frac{\text{kJ}}{\text{kg}}$$

$T_{AB} = 31.33$
~~34.4/11~~



$$h_1 = 92.42, \quad p_u = 6 \text{ bar}$$

\rightarrow interpolieren @ $T_{AB} = 31.33$

$$h = \frac{\phi(p_1) - \phi(p_2)}{p_1 - p_2} (p - p_2) + \phi(p_2)$$

\uparrow will das also umformen für

$$p = \frac{h - \phi(p_2)}{\phi(p_1) - \phi(p_2)} (p_1 - p_2) + p_2$$

d)

$$d) \quad \varepsilon_K = \frac{\dot{Q}_{zu}}{\underbrace{\dot{W}_t}_{\dot{W}_K}} = \dots$$

\dot{Q}_{ab}

e) $\dot{Q} = \dot{m}(T_2 - T_1) \rightarrow$ die Temp würde Abnehmen
 \swarrow Phase veränderung