

①

$$\dot{Q}_{\text{aus}} = ?$$

$$\dot{Q}_{\text{aus}} = \dot{m}_w (h_{\text{aus}} - h_{\text{ein}}) + \dot{Q}_{\text{KFW}}$$

$$\dot{Q}_{\text{KFW}} = \dot{m}_w (h_{\text{KFW}} - h_{\text{ein}})$$

im Reaktor

$$s_{\text{ein}} = s_f(70^\circ\text{C})$$

$$s_{\text{aus}} = s_f(101^\circ\text{C})$$

$$\dot{m}_d = \dot{m}_{\text{ges}} \cdot x = 28.775 \text{ kg}$$

$$\dot{m}_f = \dot{m}_{\text{ges}} (1 - x) = 5726.23 \text{ kg}$$

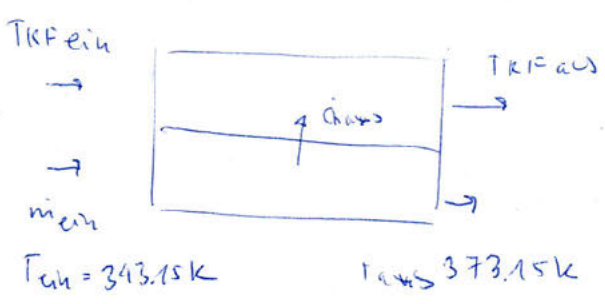
$$h_{\text{KFWein}} - h_{\text{KFWaus}} = c_{\text{KF}} (T_{\text{KFWein}} - T_{\text{KFWaus}})$$

$$\int_e^a T ds = h_{\text{aus}} - h_{\text{ein}} = \frac{\dot{Q}}{\dot{m}} = 216.6$$

$$b) \quad \bar{T} = \frac{\int_e^a T ds}{s_e - s_a} = \frac{T_{\text{KFWaus}} - T_{\text{KFWein}}}{\ln \left(\frac{T_{\text{KFWaus}}}{T_{\text{KFWein}}} \right)} = \underline{\underline{293.12 \text{ K}}}$$

1

c) $\dot{S}_{erz} = ?$



$$\dot{Q} = m \left(s_{\text{aus}} - s_{\text{ein}} \right) = \frac{\dot{Q}}{\bar{T}} + \dot{S}_{erz}$$

$$\left[\begin{aligned} s(70^\circ\text{C}) : s_f(70^\circ) &= 0.9549 \text{ kJ/kgK} \\ s_g(70^\circ) &= 7.7553 \text{ kJ/kgK} \end{aligned} \right]$$

$$\left[\begin{aligned} s(100^\circ\text{C}) : s_f(100^\circ\text{C}) &= 1.3069 \text{ kJ/kgK} \\ s_g(100^\circ\text{C}) &= 7.3599 \text{ kJ/kgK} \end{aligned} \right]$$

(@ 100°C)

$$s = s_f + x(s_g - s_f) = 1.33719 \text{ kJ/kgK}$$

$$\dot{S}_{erz} = \left(\frac{\dot{Q}_{\text{aus}}}{\bar{T}_{K12}} - \frac{\dot{Q}_{\text{aus}}}{\bar{T}_W} \right)$$

$$\bar{T}_W = 100^\circ\text{C}$$

$$= 0.046 \frac{\text{kJ}}{\text{kgK}}$$

d) $T_1 = 100^\circ\text{C} = 373.15 \text{ K}$ $T_2 = 343.15 \text{ K}$

$\Delta m = ?$ $T_{\text{in}} = 20^\circ\text{C} = 293.15 \text{ K}$ $Q_{\text{aus}} = 35'000 \text{ kJ}$

siedende Flüssigkeit $\Rightarrow x = 0$

$m_1 = 5755 \text{ kg}$ $\Delta E = m_2 u_2 - m_1 u_1 = \Delta m (h_f) + Q_{\text{aus}}$ $m_2 = (m_1 + \Delta m)$

$$(m_1 + \Delta m) u_f(70^\circ\text{C}) - m_1 (u_f(100^\circ\text{C})) = \Delta m (h_f(20^\circ\text{C})) + Q_{\text{aus}}$$

$$= \Delta m (h_f - u_f(70^\circ\text{C}))$$

$$\begin{cases} u_f(70^\circ\text{C}) = 292.95 \frac{\text{kJ}}{\text{kg}} \\ u_f(100^\circ\text{C}) = 418.94 \frac{\text{kJ}}{\text{kg}} \\ h_f(20^\circ\text{C}) = 83.96 \frac{\text{kJ}}{\text{kg}} \end{cases}$$

$$\Delta m = \frac{m_1 (u_f(70^\circ) - u_f(100^\circ)) - Q_{\text{aus}}}{h_f - u_f(20^\circ)} = 3637.9 \text{ kg}$$

(1)

e) $\Delta S_{12} = ?$

~~$$\Delta S_{12} = m_2 s_2 - m_1 s_1 = \Delta m \cdot s_f(20^\circ\text{C}) + \frac{Q}{T} + S_{\text{erz}}$$~~

$$\Delta S_{12} = m(s_2 - s_1) = \frac{Q}{T} + S_{\text{erz}}$$

$$S_{\text{erz}} =$$

$$s_2 = s_f(70^\circ\text{C}) = 0.5899 \frac{\text{kJ}}{\text{kgK}}$$

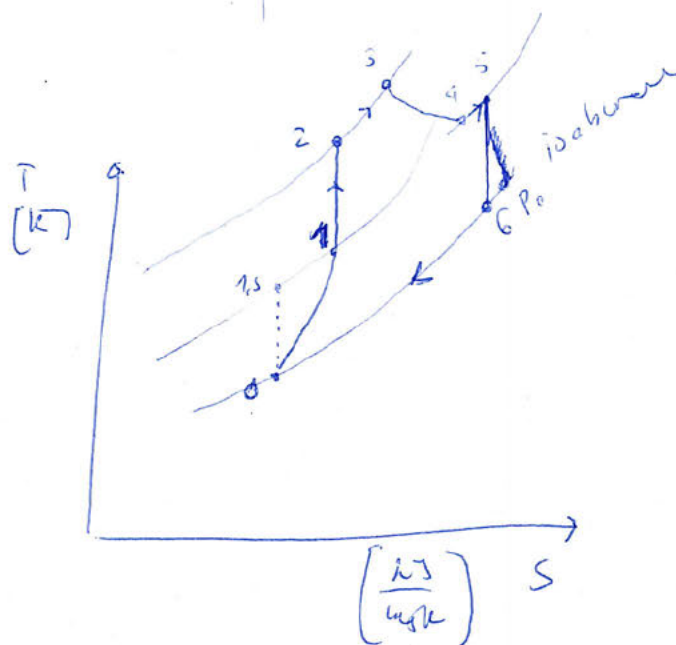
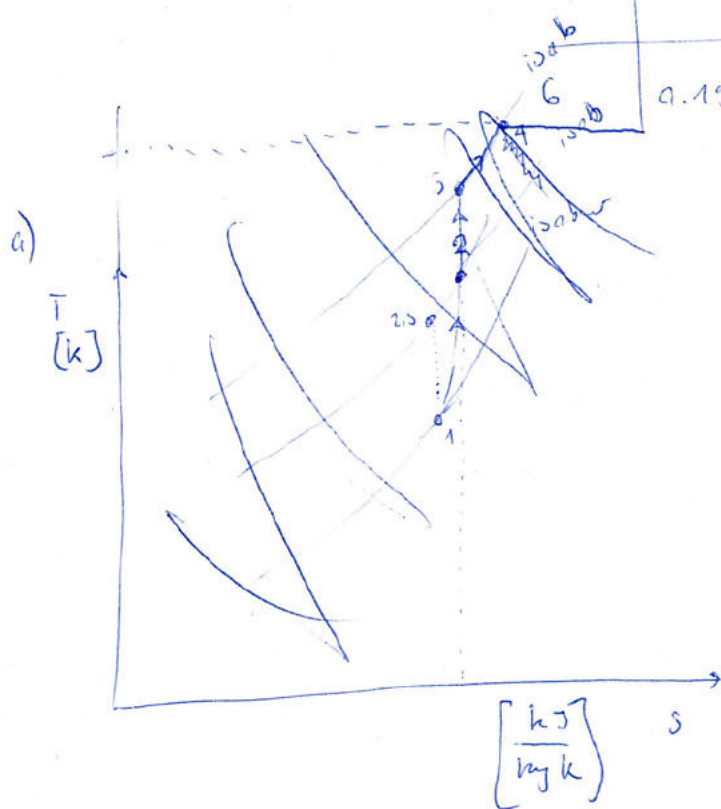
$$s_1 = s_f(100^\circ\text{C}) = 1.3069$$

2

$$\kappa = 1.4$$

$$c_p = 1006 \frac{\text{kJ}}{\text{kg K}}$$

	P	T	w
0	0.191 bar	293.15 K	
1			
2			
3			
4			
5	0.5 bar	431.9 K	220 m/s
6	0.191 bar		



(2)

b) ω_6 T_6 $\omega_5 = 220 \text{ m/s}$

(-q) $S \rightarrow G$

$$Q = m \left[h_5 - h_6 + \frac{\omega_5^2 - \omega_6^2}{2} \right] - \dot{W}_{\text{dise}} \rightarrow \omega_6 = \dots$$

$$\dot{W}_{\text{dise}} = - \dot{m} \left(\frac{V^2}{2} \right)$$

$$\frac{T_6}{T_5} = \left(\frac{p_6}{p_5} \right)^{\frac{k-1}{k}} \Rightarrow T_6 = T_5 \left(\frac{p_6}{p_5} \right)^{\frac{k-1}{k}} = \underline{\underline{328.07 \text{ K}}}$$

Ex B $S \rightarrow G$

$$Q = m [h_5 - h_6 - T_0 (s_5 - s_6)] + \dot{Q} = \dot{W}_{\text{dise}}$$

$$\dot{W}_{\text{dise}} = m \left[c_p (T_5 - T_6) - T_0 \left(c_p \ln \left(\frac{T_5}{T_6} \right) - R \ln \left(\frac{p_5}{p_6} \right) \right) \right]$$

c) $w_6 = 512 \text{ m/s}$ $T_6 = 342 \text{ K}$

(2)

niges

$$\Delta \text{exstr.} = \text{exstr.}_6 - \text{exstr.}_0$$

$$\Delta \text{exstr.} = m \left[h_6 - h_0 - T_0 (s_6 - s_0) + (w_6 - w_0) \right] + \dots$$

$$\Delta \text{exstr.} = c_p (T_6 - T_1) - T_0 \left(c_p \ln \left(\frac{T_6}{T_0} \right) \right) + w_6 - w_0$$

$$= 335.42 \text{ kJ/kg}$$

d) $\text{exverl} = ?$

$$\eta = \frac{\text{exstr.} - \dot{W}}{\dot{W}} = \text{exverl}$$

3)

a) $p_{g,1} = ?$

$m_g = ?$

$A = \left(\frac{D}{2}\right)^2 \pi = 0.00785 \text{ m}^2$

~~Pg~~

~~F~~ $p = \frac{F}{A}$

$p_{g,1} = \frac{F + p_{amb}}{A} = \frac{90114.8 \text{ Pa}}{1}$

$F = (m_k + m_{Gew})g = 314.9 \text{ N}$

$140114.8 \text{ Pa} = 1.4 \text{ bar}$

$m = \frac{p_1 V_1}{R T_1}$

$R = \frac{\bar{R}}{M} = \frac{8.314 \frac{\text{kJ}}{\text{kmol K}}}{50 \frac{\text{kg}}{\text{kmol}}} = 0.16628 \frac{\text{kJ}}{\text{kg K}}$

3.4 g

$p_{g,2} = 1.5 \text{ bar}$

$p_{g,2} = \text{gleich wie } p_{g,1}$

da Massen von Gas

nicht ändert

(p0 auch nicht)

b) $T_{\text{eis},2} = T_{\text{gas},2}$

$T_{\text{eis},2} = \frac{p_{g,2} V_1}{m R}$

~~$T_{\text{gas},2} = \frac{p_{g,2} V_2}{m R T_{\text{gas},2}}$~~

c) $\Delta E = E_2 - E_1 = Q - W_{V,1}$

$W_v + m(u_2 - u_1) = Q$

$W_v =$

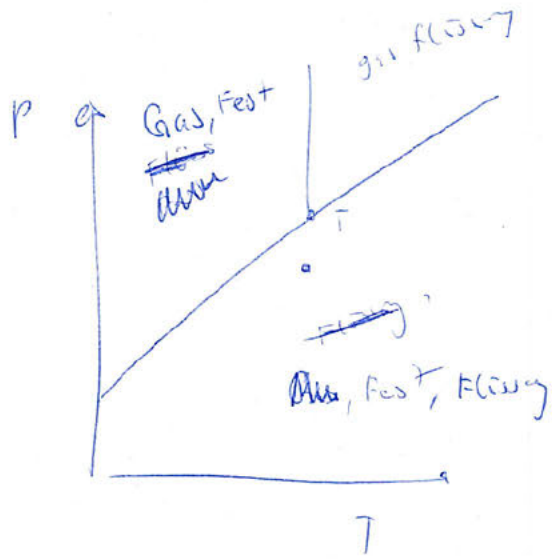
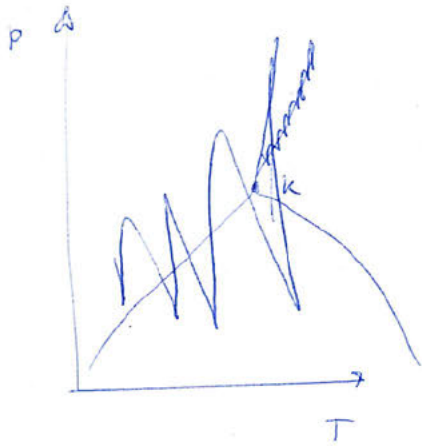
$$d) \quad u = u_{f2} + x(u_{g2} - u_{f2}) \quad -m_g(u_2 - u_1) + Q = W_v$$

$$u(0.003^\circ\text{C}) \Rightarrow u_{fe} = -333.492 \quad u_{fe} = -0.033$$

$$x_{ej} = \frac{u_{tnt_2} - u_{f2}}{u_{g2} - u_{f2}}$$

a)

e)



Temp condensing = -16°C

$\bar{T}_i \rightarrow P_{r,i} = \underline{1 \text{ mbar}}$

$\bar{T}_i = \underline{-10^{\circ}\text{C}}$

EB 1 \rightarrow 2

b) ~~$Q = \dot{m} [h_1 - h_2]$~~ $Q = \dot{m} [h_1 - h_2] + \dot{Q}_k$
 $= h_2 = h_g(-22) = \underline{234.28 \text{ kJ/kg}}$

EB 2 \rightarrow 3

$Q = \dot{m} [h_2 - h_3] - \dot{W}_k$
 ~~$Q = \dot{m} [h_2 - h_3]$~~

c) $h_1 = h_g$ $h_g = h_f(86\text{bar}) = \underline{93.42 \text{ kJ/kg}}$

$h_f(\dots)$
 $h_g(\dots)$
 $x = \frac{h_g - h_f}{h_g - h_f}$

d)

$$\epsilon_k = \frac{\dot{W}_{\text{nutz}}}{\dot{Q}_{\text{zu}}}$$

e) und ~~Wärmer~~ ^{Wärmer} da die Lebensmittel
alle Wärme beibringen