

Aufg 1 Wasser: realer Fluid

a) Reaktor Wasser:

	p	T	
1		70°C	x=1
2		100°C	x=1

ges \dot{Q}_{aus} ~~ist das~~

 ~~$\dot{Q} = \dot{m}_w [h_{in} - h_{aus}]$~~

$$0 = \dot{m}_w [h_{in} - h_{aus}] + \dot{Q}_R - \dot{Q}_{aus}$$

wird negativ eingeführt
da es raus geht

$$\dot{Q}_{aus} = \dot{m}_w [h_{in} - h_{aus}] + \dot{Q}_R$$

$$h_{in}[70^\circ\text{C}, x=1] = 2626.8 \frac{\text{kJ}}{\text{kg}} \quad h_{aus}[100^\circ\text{C}, x=1] = 2676.1 \frac{\text{kJ}}{\text{kg}}$$

Aus ~~A13~~ A-2

$\dot{Q}_{aus} = \underline{\underline{85.2 \text{ kW}}}$ (positiv gem. Konvention)

Aufg 1

b) $0 = \dot{m}_{KF} [s_{KFe} - s_{KFu}] + \frac{\dot{Q}_{aus}}{\bar{T}_{KF}} + \dot{s}_{erz}$ 0 da kein Druckverlust

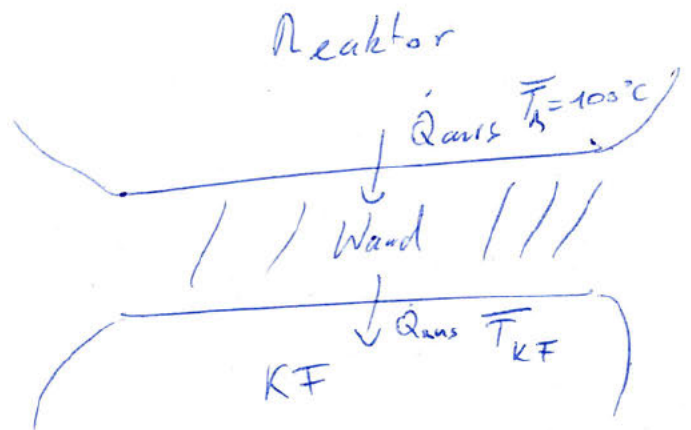
$$s_{KFe} - s_{KFu} = c_{if} \cdot \ln \left(\frac{T_{KFe}}{T_{KFu}} \right)$$

$$\bar{T}_{KF} = \frac{-\dot{m}_{KF} \cdot c_{if} \cdot \ln \left(\frac{T_{KFe}}{T_{KFu}} \right)}{\frac{\dot{Q}_{aus}}{-\dot{m}_{KF} \cdot c_{if} \cdot \ln \left(\frac{T_{KFe}}{T_{KFu}} \right)}} = \dots$$

unbekannt?

c) $\dot{s}_{erz} = -\sum \frac{\dot{Q}_{aus}}{\bar{T}} = -\frac{\dot{Q}_{aus}}{\bar{T}_{Reaktor}} + \frac{\dot{Q}_{aus}}{\bar{T}_{KF}}$

$$\dot{s}_{erz} = 0.06049 \frac{kJ}{s \cdot K}$$



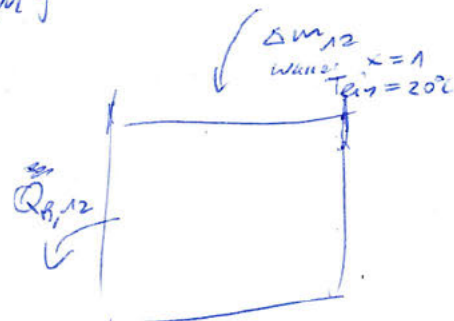
d)

	T		
1	100°C	$x_0 = 0.005$	$\dot{Q}_{2,12} = 35 MJ$
2	70°C	$x = 1$	

$m_1 = 5755 kg$

$$m_2 = m_1 + \Delta m_{12}$$

$$m_2 u_2 - m_1 u_1 = \Delta m_{12} h_{ein} + \dot{Q}_R - \dot{Q}_{12}$$



$$\Delta m_{12} h_{ein} - \Delta m_{12} \cdot u_2 = m_1 u_2 - m_1 u_1 - \dot{Q}_R$$

$$\Delta m_{12} = \frac{m_1 (u_2 - u_1) - \dot{Q}_R}{h_{ein} - u_2}$$

$$= 170.9 t$$

$$h_{ein}[20^\circ C, x=1] = 2538.1 \frac{kJ}{kg}$$

aus TAB A-2

$$u_1[100^\circ C, x=0.005] = u_f + x_0 (u_g - u_f) = 429.38 \frac{kJ}{kg}$$

$$u_2[70^\circ C, x=1] = 2469.6 \frac{kJ}{kg}$$

Afg 1

c) $\Delta S_{12} = m_2 s_2 - m_1 s_1$
 $= 64'855 \frac{\text{kJ}}{\text{kg K}}$

$m_1 = 5755 \text{ kg}$

$m_2 = m_1 + \Delta m_{12} = 9355 \text{ kg}$

$s_2 [70^\circ\text{C}, x=1] = 7.7553 \frac{\text{kJ}}{\text{kg K}}$

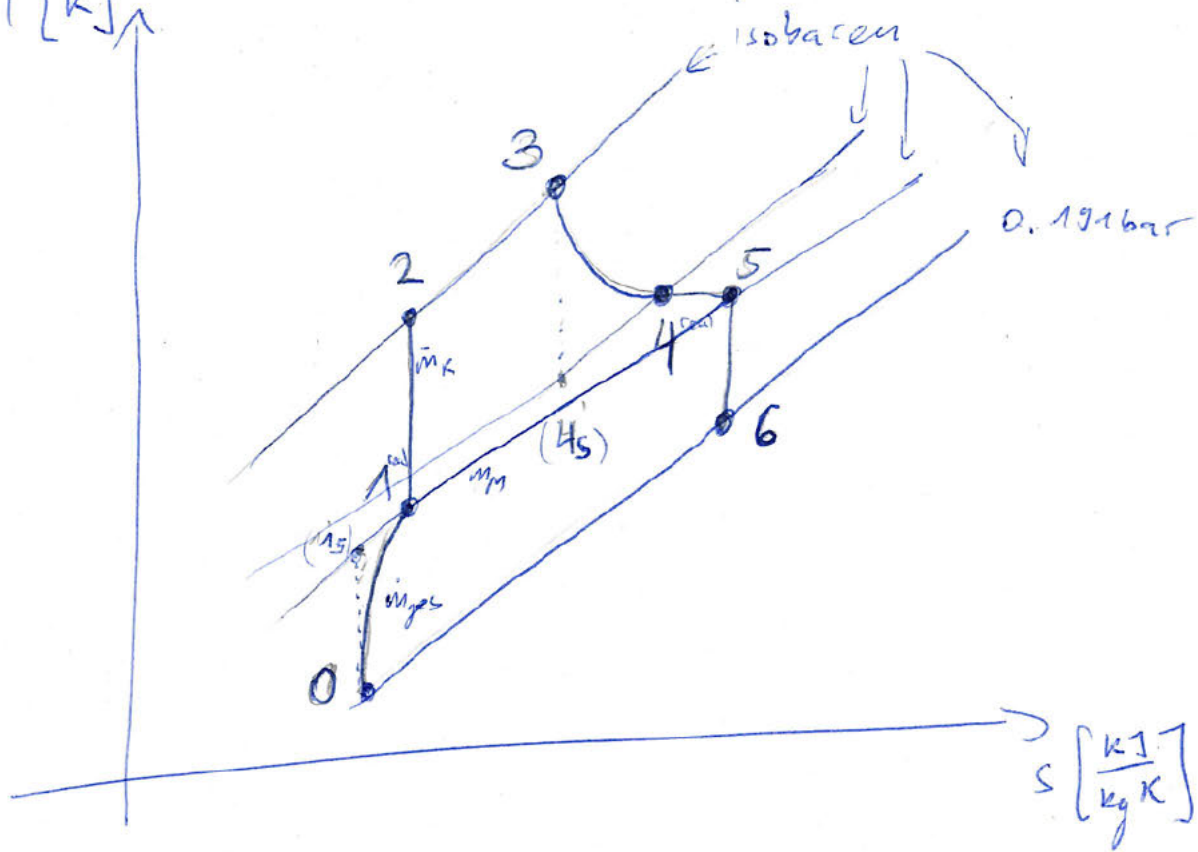
$s_1 [400^\circ\text{C}, x=0.005] = s_f + x(s_g - s_f)$

$= 1.33714 \frac{\text{kJ}}{\text{kg K}}$

Aus TAB A-2

Aufg 2

a) $T[K]$



	P	T	w	
0	0.191 bar	$= 243.15 K$ $-30^{\circ}C$	$200 m/s$	$Q_{01} = 0$
1				$\dot{m}_R = \frac{\dot{m}_M}{5.293}$
2	P_2			
3	$= P_2$			$q_B = 1195 \frac{kJ}{kg}$
4				
5	0.5 bar	$431.9 K$	$220 m/s$	$\Delta S = 0$
6	0.191 bar			

AF2

b) p_5, w_5, T_5

$$\frac{T_6}{T_5} = \left(\frac{p_6}{p_5} \right)^{\frac{0.4}{1.4}}$$

$$T_6 = T_5 \left(\frac{p_6}{p_5} \right)^{\frac{0.4}{1.4}} = \underline{\underline{328.07 \text{ K}}}$$

$$0 = \dot{m}_{\text{gas}} \left(\underbrace{h_5 - h_6}_{\text{adiabatic}} + \frac{w_5^2 - w_6^2}{2} \right) + \cancel{\dot{Q}} - \cancel{\dot{W}_{\text{esk}}}$$

$$= c_p (T_5 - T_6) \dot{m}_{\text{gas}}$$

$$\dot{W}_{\text{esk}} = \dot{m}_{\text{gas}} \left(\sqrt{2 c_p (T_5 - T_6) + w_5^2} \right) = \underline{\underline{507.25 \text{ m/s}}}$$

c) $\Delta ex_{\text{str 6}} = [h_6 - h_0]$

$$ex_{\text{str 6}} = h_6 - h_0 - T_0 (s_6 - s_0) + \frac{1}{2} w_6^2$$

$$ex_{\text{str 0}} = h_0 - h_0 - T_0 (s_0 - s_0) + \frac{1}{2} w_0^2$$

$$\Delta ex_{\text{str 06}} = ex_{\text{str 6}} - ex_{\text{str 0}} = \underbrace{h_6 - h_0}_{= c_p (T_6 - T_0)} - \underbrace{T_0 (s_6 - s_0)}_{= -T_0 (s_6 - s_0)} + \frac{1}{2} w_6^2 - \frac{1}{2} w_0^2$$

$$\Delta ex_{\text{str}} = c_p (T_6 - T_0) - T_0 \left(2 c_p \ln \left(\frac{T_6}{T_0} \right) \right) + \frac{w_6^2 - w_0^2}{2}$$

$$= \underline{\underline{120.8 \frac{\text{kJ}}{\text{kg}}}}$$

Aufg 2

$$d) 0 = \dot{m}_{\text{gas}}(s_0 - s_b) + \frac{\dot{Q}_B}{T_B} + \dot{s}_{\text{erz}} \quad | : \dot{m}_{\text{gas}}$$

$$\dot{s}_{\text{erz}} = s_b - s_0 - \frac{q_B}{T_B} = c_p \ln\left(\frac{T_b}{T_0}\right) - \frac{q_B}{T_B} = -625.73 \frac{\text{J}}{\text{kgK}} \quad \leftarrow \text{müßte positiv sein!}$$

$$l_{\text{x verl}} = s_{\text{erz}} \cdot T_0 = \underline{\underline{-152.140 \frac{\text{kJ}}{\text{kg}}}}$$

Atg 3

perf. Gas:

	p	T	V		
1	1.4 bar	500°C	0.00314 m ³		
2	1.4 bar	0°C			

EW: $m_{EW} = 0.1 \text{ kg}$

	p	T	V	
1	≈ 1.4 bar	0°C	V_1	$x_{Eis} = 0.6$
2	1.4 bar	0°C	$= V_1$	

$$p_a = \frac{N}{m^2}$$

$$p_{\text{gas}} = \frac{\overset{= m_{\text{man}} + m_{\text{Eis}}}{m_{\text{ges}} \cdot g}}{\left(\frac{D}{2}\right)^2 \cdot \pi} + p_{\text{amb}} = \underline{\underline{1.40 \text{ bar}}}$$

$$R_{\text{gas}} = \frac{\overline{R}}{M_g} = 0.166 \frac{\text{kJ}}{\text{kg} \cdot \text{K}} \quad \text{Korrekt}$$

$$m_g = \frac{p_{\text{gas}} \cdot V_1}{R_{\text{gas}} \cdot T_1} = \underline{\underline{3.419 \text{ g}}}$$

b) Da die ganze Wärme \dot{Q}_{12} in den Prozess vom Eis schmelzen einfließt und am Schluss immer noch Eis übrig ist, gilt das $T_{2,\text{Eis}} = 0^\circ\text{C}$ ist und somit auch $T_{2,\text{gas}} = 0^\circ\text{C}$ (da \leftrightarrow Therm. Gleichgewicht!). Der Druck bleibt in dieser Konstellation konstant!

$$p_{2g} = p_{1g} = 1.4 \text{ bar}$$

c) $\Delta E = \Delta U + \cancel{KE} + \cancel{PE} = \cancel{\frac{1}{2} Q_{12}} - \cancel{U_{12}}$
 $Q_{12} = \overset{\text{aus}}{c_v} (T_2 - T_1) + \cancel{p_{12} \frac{R}{1-\gamma} \ln \frac{T_2}{T_1}}$ $n = \gamma = \frac{c_p}{c_v}$
 $= -316.5 \text{ kJ}$

d) ges $x_{\text{Eis},2}$ $m_1 = m_2 = m_{\text{Eis}}$

$$\Delta U_{12} = + Q_{12} = m_2 u_2 - m_1 u_1$$

aus Tab 1.

wird
ZR von
Atz verwendet
 $|Q_{12}| = 1.5 \text{ kJ}$

$$\leftarrow \frac{Q_{12}}{m_{\text{Eis}}} + u_1 = u_2 \quad : \quad u_1 [1.4 \text{ bar}, 0^\circ\text{C}] = u_{\text{flüssig}} + x_{\text{Eis}} (u_{\text{fest}} - u_{\text{flüssig}})$$

$$= -200.09 \frac{\text{kJ}}{\text{kg}}$$

$$u_2 = -185.05 \frac{\text{kJ}}{\text{kg}}$$

$$x_{2\text{Eis}} = \frac{u_2 - u_{\text{fl}} [1.4 \text{ bar}, 0^\circ\text{C}]}{(u_{\text{fest}} - u_{\text{fl}}) [1.4 \text{ bar}, 0^\circ\text{C}]} = 0.555$$

Aufg 4

$$b) \quad 0 = \dot{m}_R [h_2 - h_3] + \overset{\substack{\nearrow \\ \text{0, adiab.}}}{\cancel{\dot{Q}}} - \dot{W}_R$$

$$h_2 [x=0]$$

$$h_3 [8 \text{ bar,}$$