

# Aufgabe 1.

1. a) stationärer Fließprozess

$$0 = \dot{m}_{E,in} (h_e - h_a) - \dot{Q}_{aus} + \dot{Q}_R$$

$$h_e = h_f^{Tab} (70^\circ\text{C}) = 292,98 \frac{\text{kJ}}{\text{kg}}$$

$$h_a = h_f (100^\circ\text{C}) = 419,04 \frac{\text{kJ}}{\text{kg}}$$

$$\begin{aligned}\dot{Q}_{aus} &= \dot{m}_{E,in} (h_e - h_a) + \dot{Q}_R \\ &= 62,182 \text{ kW}\end{aligned}$$

~~182~~

1. b)

$$\overline{T}_{AF} = \frac{\int_{s_e}^{s_a} T ds}{s_a - s_e} = \frac{\frac{T_{AFaus} + T_{AFein}}{2} (s_e - s_a)}{s_e - s_a}$$

$$= \frac{T_{AFaus} + T_{AFein}}{2} = 293,75 \text{ K}$$

1. c)

$$0 = \dot{m}_{\text{ein}} (s_e - s_a) - \frac{\dot{Q}_{\text{aus}}}{T_{KF}} + \dot{S}_{\text{erz}}$$

$$s_e = s_f(70^\circ\text{C}) = 0,9549 \frac{\text{kJ}}{\text{kg} \cdot \text{K}}$$

$$s_a = s_f(100^\circ\text{C}) = 1,3069 \frac{\text{kJ}}{\text{kg} \cdot \text{K}}$$

$$\dot{S}_{\text{erz}} = -\dot{m}_{\text{ein}} (s_e - s_a) + \frac{\dot{Q}_{\text{aus}}}{T_{KF}}$$

$$= 0,3177 \frac{\text{kJ}}{\text{K} \cdot \text{s}}$$

1. d)

$$\Delta E = \Delta m_{12} (u_2 - u_1)$$

$$\Delta E = \Delta m_{12} [h_2 - h_1] - \underbrace{\dot{Q}_{aus,12} + \dot{Q}_{R,12}}_{=0}$$

$$= m_2 u_2 - m_1 u_1 = (m_1 + \Delta m_{12}) u_2 - (m_1) u_1$$

HAHAHA

$$h_1 = h_f(20^\circ\text{C}) = 83,96 \frac{\text{kJ}}{\text{kg}}$$

$$h_2 = h_f(70^\circ\text{C}) = 419,04 \frac{\text{kJ}}{\text{kg}}$$

$$u_1 = u_f(20^\circ\text{C}) = 83,95 \frac{\text{kJ}}{\text{kg}}$$

$$u_2 = u_f(70^\circ\text{C}) = 272,95 \frac{\text{kJ}}{\text{kg}}$$

$$m_1 = 5755 \text{ kg}$$

$$\Delta m_{12} [h_2 - h_1] = m_1 u_2 + \Delta m_{12} u_2 - m_1 u_1$$

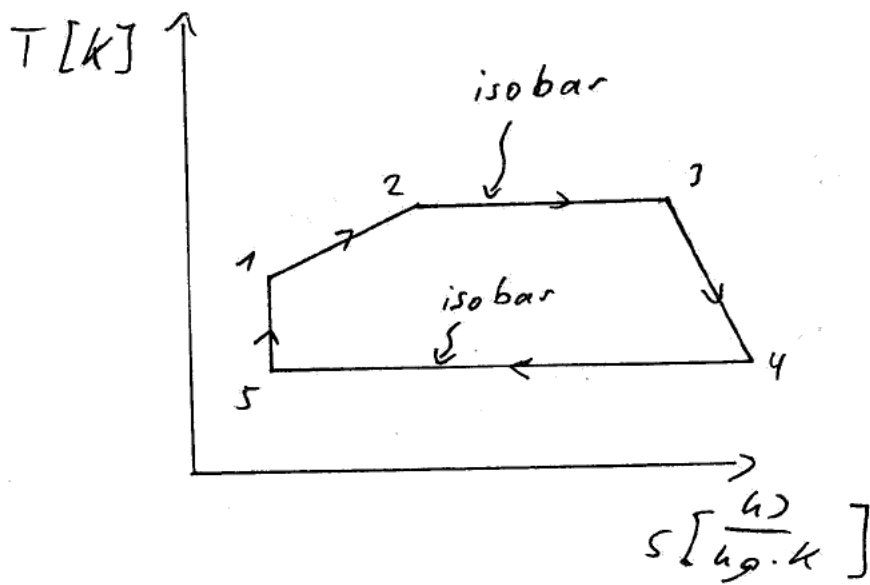
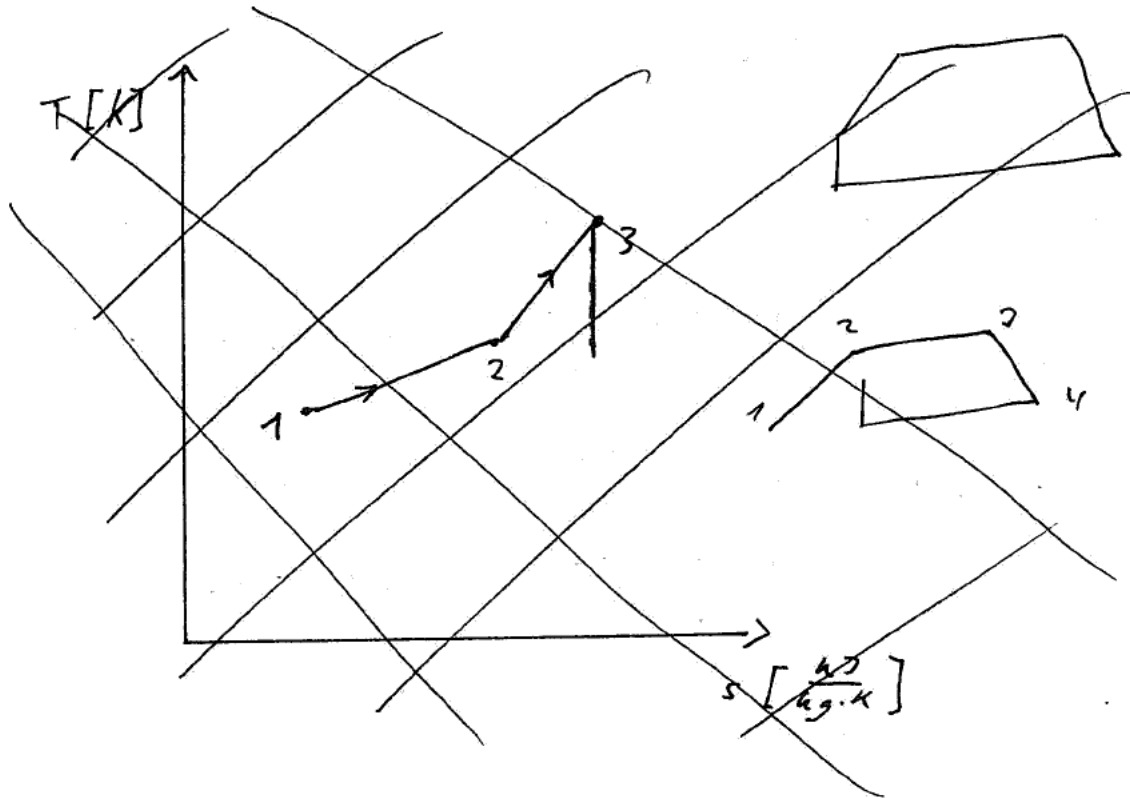
$$\Delta m_{12} = \frac{m_1 u_2 - m_1 u_1}{h_2 - h_1 - u_2}$$

$$= 28549 \text{ kg}$$

$$1. e) \quad \Delta S = m_2 s_2 - m_1 s_1 = \sum_i m_i s_i + \sum_j \frac{Q_j}{T_j} + S_{e_z}$$

# Aufgabe

2. a)



2. b) Energiebilanz (stationärer Fließprozess)

$$0 = \dot{m} \left( h_0 - h_6 + \frac{w_{\text{Lufte}}^2 - w_6^2}{2} \right) + q_B \cdot \dot{m}_K$$

$$\dot{m}_K = \cancel{8,293} \cdot \frac{1}{5,293} \cdot \dot{m}_M$$

$$h_0 = h[T_0] = h[243,15 \text{ K}]$$

$$\overset{\text{Tab.}}{A22} = h[240] + \frac{h[250] - h[240]}{250 - 240} (243,15 - 240)$$

$$= \cancel{243,18} \cdot \frac{\text{kJ}}{\text{kg}}$$

$$h_5 = h[430] + \frac{h[440] - h[430]}{440 - 430} (437,9 - 430)$$

$$= 433,37 \frac{\text{kJ}}{\text{kg}}$$

$$h_6 = h_0$$

$$\Rightarrow 0 = \dot{m} \left( \frac{w_{\text{Lufte}}^2 - w_6^2}{2} \right) + q_B \cdot \dot{m}_K$$

$$w_6 = \sqrt{\frac{2 q_B \cdot \dot{m}_K}{\dot{m}} + w_{\text{Lufte}}^2}$$

2. c)

$$e_{x, str}^m = [h - h_0 - T_0 (s - s_0) + \frac{w^2}{2}]$$

$$e_{x, str, 6} = [h_6 - h_0 - T_0 (s_6 - s_0) + \frac{v_6^2}{2}]$$

$$e_{x, str, 0} = [h_0 - h_0 - T_0 (s_0 - s_0) + \frac{v_0^2}{2}]$$

$$= \frac{w_0^2}{2} = 20000 \frac{\text{m}^2}{\text{s}^2}$$



2. d)

$$\dot{E}_{x, \text{vol}} = \dot{m} [h_e - h_a - T_0(s_e - s_a) + s h_e] + \sum_j \left(1 - \frac{T_0}{T_j}\right) \dot{Q}_j = \dot{e}_{x, \text{vol}} \cdot \dot{m}$$

$$0 = \dot{m} [h_e - h_a + s h_e] + \sum_j \dot{Q}_j$$

||

$$\begin{aligned} \dot{E}_{x, \text{vol}} &= \dot{m} [-T_0(s_e - s_a)] + \sum_j \left(1 - \frac{T_0}{T_j}\right) \dot{Q}_j - \sum_j \dot{Q}_j \\ &= \dot{e}_{x, \text{vol}} \cdot \dot{m} \end{aligned}$$

$$e_{x, \text{vol}} = -T_0(s_e - s_a) + \underbrace{\sum_j \left(1 - \frac{T_0}{T_j}\right) \dot{Q}_j}_{\dot{m}} - \sum_j \dot{Q}_j$$

# Aufgabe 3.

$$3. a) \quad p_{1,g} = \frac{m_g R T_{g,1}}{V_{g,1}}$$

$$m_g = \frac{p_{1,g} \cdot V_{g,1}}{R \cdot T_{g,1}}$$

$$R = \frac{\bar{R}}{M} \quad \bar{R} = 8,314 \frac{J}{mol \cdot K}$$

$$= 166,28 \frac{J}{kg \cdot K}$$

$$p_{1,g} = \frac{\tilde{\pi}}{4} D^2 \cdot (m_K + m_{EU}) + p_{amb}$$

$$= \cancel{1,00 bar} \quad 1,00 bar$$

$$m_g = 5,84 g$$

3. b)  $p_{g,2} = p_{g,1}$

Da festes und flüssiges Wasser hier inkompressibel ist und deswegen eine Änderung ~~mit~~ von  $x_{Ei}$  keinen Einfluss auf ~~den~~ den Druck  $p_g$  hat, kann man so wie in a) vorgehen.

$$T_{g,2} = T_{g,1}$$

Da für ideale Gase Temperatur und Druck gehoppelt sind.

2. c)  $\frac{\Delta E}{m_g} =$

3. d)

$$x = \frac{u - u_f}{u_g - u_f}$$

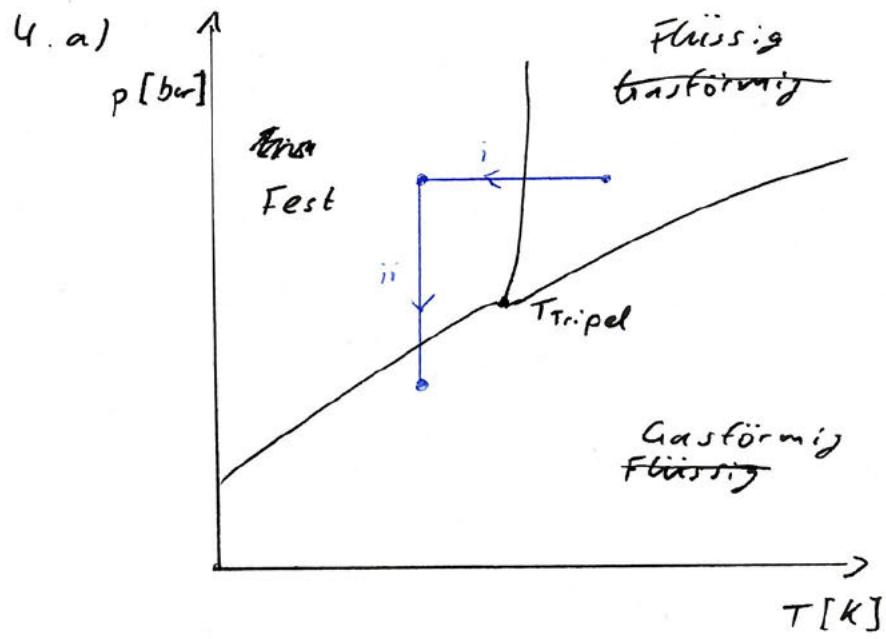
Da die Membran wärme übertragend ist:

$$T_{g,2} = T_{e,2} = 0,003^\circ\text{C}$$

$$\Delta E = -Q_{12}$$

$$\frac{\Delta E}{m_{EV}} = u = -75 \frac{\text{kJ}}{\text{kg}}$$

$$\Rightarrow x = \frac{\overset{T_{ab}}{1} \frac{75 - (-0,033)}{-333,442 + 0,033}}{=} = 0,0449$$



4. b) stationärer Fließprozess

$$0 = \dot{m}_{R134a} (h_2 - h_3) + \dot{W}_K$$

$$\dot{m}_{R134a} = - \frac{\dot{W}_K}{h_2 - h_3}$$

$$s_2 = s_3 \quad p_3 = 8 \text{ bar} \quad x_2 = 1$$

$$p_2 = p_4$$

$$T_2 = T_i - 6 \text{ K}$$

4. c)  $x_1 = \frac{\phi - \phi_f}{\phi_g - \phi_f}$

$\phi = v, u, s, j$



4.

d)

$$\epsilon_k = \frac{|\dot{Q}_{ab}|}{|\dot{W}_e|} = \frac{-\dot{Q}_{ab}}{-\dot{W}_k}$$