

① a) Q_{aus}

E-Bilanz stat. Flussprozess

$$0 = \dot{m}(h_e - h_a) + \sum \dot{Q} - \dot{W}^0 = \dot{m}(h_e - h_a) + \dot{Q}_R - \dot{Q}_{aus}$$

$$\dot{Q}_{aus} = \dot{m}(h_e - h_a) + \dot{Q}_R$$

$$h_e = h_f(70^\circ) + x_D (h_g(200^\circ) - h_f(70^\circ)) = 364.649 \quad (A-2)$$

$$h_a = h_f(100^\circ) + x_D (h_g(100^\circ) - h_f(100^\circ)) = 409.311 \quad (A-2)$$

$$\dot{Q}_{aus} = 62.182 \text{ kW} =: A$$

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Variablen

$$A := \dot{Q}_{aus}$$

b) T_{KF}

Entropiebilanz stat.

keine druckänderung, adiabatisch \Rightarrow isentrop

$$0 = \dot{m}(s_e - s_a) + \frac{\dot{Q}}{T} + \dot{s}_{erz}$$

$$T = \frac{\dot{Q}}{\dot{m}(s_e - s_a)}$$

10/11

c) S_{erz}

$$T_{KF} = 295 \text{ K}$$

$$0 = \dot{m}(s_e - s_a) + \frac{\dot{Q}}{T} + \dot{s}_{erz}$$

$$\dot{s}_{erz} = \dot{m}(s_a - s_e) - \frac{\dot{Q}}{T} = \dot{m} c \ln\left(\frac{T_a}{T_e}\right) - \frac{\dot{Q}}{T}$$

Entropiebilanz nur Wand

$$0 = \dot{m} \dot{s}_i + \sum \frac{\dot{Q}}{T} + \dot{s}_{erz}$$

$$\dot{s}_{erz} = -\sum \frac{\dot{Q}}{T} = -\frac{\dot{Q}_{aus}}{T_{Reaktor}} + \frac{\dot{Q}_{aus}}{T_{KF}} = 0.0441 \frac{\text{kJ}}{\text{kg K}}$$

d) Δm₁₂

E-Bil.

$$\Delta E = m_2 u_2 - m_1 u_1 + \dot{W}^0 = \Delta m_{12} (h_{ein} \dot{W}^0) + \dot{Q} - \dot{W}^0$$

$$(m_1 + \Delta m_{12}) u_2 - m_1 u_1 = \Delta m_{12} h_{ein} - Q_{aus12} \Rightarrow m_1 (u_2 - u_1) + \Delta m_{12} u_2 = \Delta m_{12} h_{ein} - Q_{aus12}$$

$$h_{ein} = h_f(200^\circ) = 83.56 \quad (A-2)$$

$$u_1 = h_f(100^\circ) + x_D (h_g(100^\circ) - h_f(100^\circ)) = 409.311 \quad (A-2)$$

$$u_2 = u_f(70^\circ) = 246.9 \quad (A-2)$$

$$\Delta m_{12} = \frac{1}{u_2 - h_{ein}} (-m_1 (u_2 - u_1) - Q_{aus12}) = 3589.4 \text{ kg}$$

1/6

$$\textcircled{1} \text{ e) } \Delta S = m_2 s_2 - m_1 s_1 = m_1 (s_2 - s_1) + \Delta m s_2$$

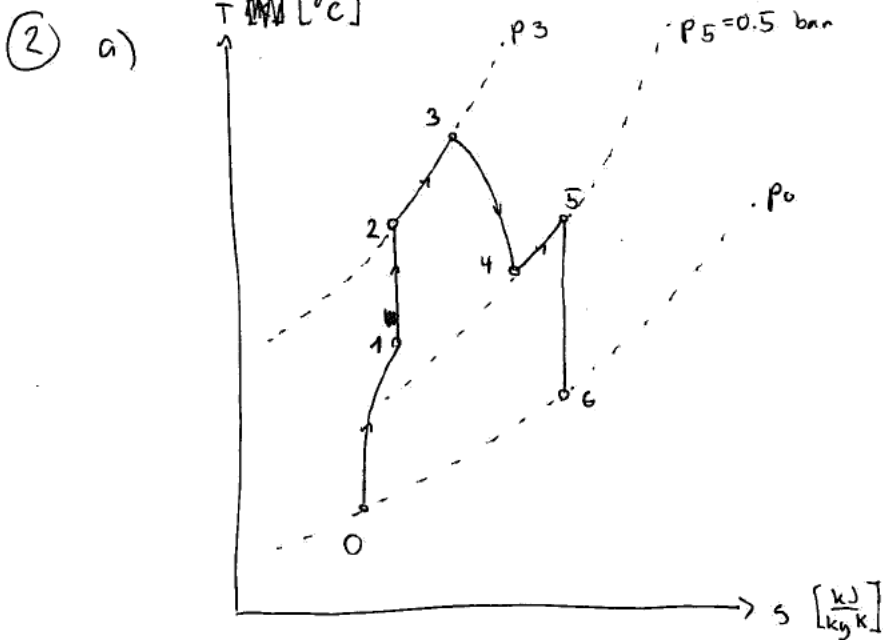
$$s_1 = s_f(100^\circ) + x_D (s_g(100^\circ) - s_f(100^\circ)) \quad (A-2)$$

$$s_2 = s_f(40^\circ)$$

$$s_1 = 1.33714 \quad \text{Btu/lb}^\circ\text{R}$$

$$s_2 = 0.9549 \quad \text{Btu/lb}^\circ\text{R}$$

$$\Delta S = -4299.4 \quad \frac{\text{Btu}}{\text{K}}$$



b) Flugzeugtriebwerk stationär und adiabatisch

~~E-Bil um gesamtes System~~

$$0 = \dot{m}_a (h_e - h_a + \frac{w_e^2 - w_a^2}{2} + \dots) + \dot{Q} - \dot{W}$$

5-7 6 isentrop

$$\frac{T_6}{T_5} = \left(\frac{p_6}{p_5} \right)^{\frac{n-1}{n}}$$

$$T_6 = T_5 \left(\frac{p_6}{p_5} \right)^{\frac{n-1}{n}} = 328.1 \text{ K} =: A$$

E-Bilanz um Schubdüse

$$0 = \dot{m} (h_e - h_a + \frac{w_e^2 - w_a^2}{2} + \dots) - \dot{W} \quad | : \dot{m}$$

$$\frac{w_e^2}{2} = h_a - h_e + \frac{w_a^2}{2}$$

$$\frac{w_e^2}{2} = h_5 - h_6 + \frac{w_5^2}{2} - w_{rev56} \quad | \cdot 2$$

$$w_e = \sqrt{2(h_5 - h_6) + w_5^2 - 2w_{rev56}} \quad \left| \begin{array}{l} h_5 - h_6 = c_p (T_5 - T_6) \\ w_{rev56} = \frac{R(T_6 - T_5)}{1-n} \end{array} \right.$$

$$w_e = \sqrt{2c_p(T_5 - T_6) + w_5^2 - 2 \cdot \frac{R(T_6 - T_5)}{1-n}}$$

$$R = \frac{\bar{R}}{M_{Luft}} = 286.99 =: B \quad (A-1)^{-1}$$

$$w_e = 329.11 \frac{\text{m}}{\text{s}} =: C$$

② c) rechnen mit $w_0 = 510 \frac{m}{s}$ $T_0 = 340 K$

$$\Delta e_{x, str} = h_6 - h_0 - T_0 (s_6 - s_0) + \frac{w_6^2 - w_0^2}{2}$$

$$\Delta e_{x, str} = - \left(c_p (T_6 - T_0) - T_0 \left(c_p \ln \left(\frac{T_6}{T_0} \right) - R \ln \left(\frac{p_6}{p_0} \right) \right) + \frac{w_6^2 - w_0^2}{2} \right)$$

$$= \cancel{-94.628} + 94.628 \frac{kJ}{kg}$$

d) rechnen mit $100 \frac{kJ}{kg}$

Energiebilanz um alles

$$e_{x, str} = \Delta e_{x, str} + \dots \overset{\substack{\uparrow \\ \text{adiab.}}}{\dot{Q}} - \dot{W}_t$$

$$\dot{W}_t = \dot{W}_{\text{Schubdrüse}}$$

$$w_{rev} = \frac{R (T_6 - T_5)}{1 - \eta} = 65.935 \frac{kJ}{kg}$$

e/wert

(3) a)

 p_{g1} ~~IG-Gleichung~~

$$p_{g1} = \frac{m R T}{V} = \frac{m \bar{R} T}{M V}$$

Kräftegleichgewicht

$$F_G + F_{p0} = F_{p1}$$

$$m_K \cdot g + p_{amb} \cdot \left(\frac{D}{2}\right)^2 \pi = \left(\frac{D}{2}\right)^2 \pi p_1$$

$$p_1 = \frac{m_K g}{\left(\frac{D}{2}\right)^2 \pi} + p_{amb} = \underline{\underline{1.40 \text{ bar}}} =: A$$

$$A := p_1 [\text{Pa}]$$

$$B := m_g [\text{kg}]$$

 m_g

IG-Gleichung

$$m_g = \frac{p_1 V}{R T_1}$$

$$R = \frac{\bar{R}}{M} = 166.28 = \frac{4157}{25}$$

$$m_g = \underline{\underline{3.419 \text{ g}}} =: B$$

- b) $p_{g2} = p_{g1} = 1.40 \text{ bar}$, da der Prozess isobar ist, weil sich das Gewicht von GW oder der aussendruck nicht geändert hat.

$$\Delta E = 0 \quad m_{EW} (u_2 - u_1) = m_g (u_2 - u_1)$$

$$m_{EW} (c (T_2 - T_{1EW})) = m_g c_v (T_2 - T_1)$$

$$m_g c_v T_1 - m_{EW} c T_{1EW} = T_2 (m_g c_v - m_{EW} c)$$

$$T_2 = \frac{m_g c_v T_1 - m_{EW} c T_{1EW}}{m_g c_v - m_{EW} c} =$$

- c) Rechnen mit $T_{g2} = 0.003^\circ \text{C}$

E-Bilanz Gas

$$\Delta E = Q - W^{10}$$

$$Q = m_g (u_2 - u_1) = m_g c_v (T_2 - T_1) = \underline{\underline{-1.082 \text{ kJ}}}$$

$$|Q| = 1.082 \text{ kJ}$$

- d) rechnen mit $|Q_{12}| = 1500 \text{ J}$

$$\Delta E = m_{EW} (u_2 - u_1) = Q_{12} + W^{20}$$

$$u_2 = u_1 + \frac{Q_{12}}{m_{EW}} \quad (\text{MAK})$$

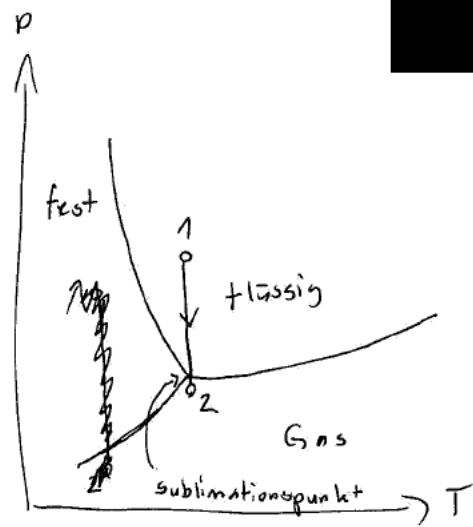
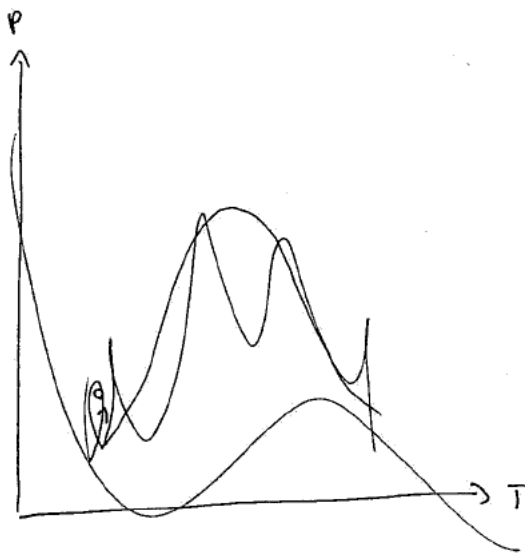
$$u_1 = u_{fe}(0^\circ \text{C}) + x_{E1} (u_{f1}(0^\circ \text{C}) - u_{fe}(0^\circ \text{C})) = 1 - 200.0928$$

$$u_2 = 238.67 - 185.0928 x_{E1} =: D$$

Interpol bei 0.003°C

$$x_{E2} = 1 - \frac{185.0928 - u_{fe}}{u_{f1} - u_{fe}} = \underline{\underline{0.555}}$$

4) a)



b) E-Bil um Verdichter

$$0 = \dot{m} (u_2 - u_3) + \dot{Q} - \dot{W}_K$$

$$\dot{W}_K = \dot{m} (u_2 - u_3)$$

$$u_2 = u_g(0^\circ\text{C}) = u_g(4^\circ\text{C}) = 229.27 \quad (\text{A-10})$$

$$T_i = 0^\circ\text{C} + 10^\circ\text{C} = 10^\circ\text{C}$$

u_3

$$s_2 = s_3 \quad (\text{isentrop})$$

$$s_2 = s_g(4^\circ\text{C}) = 0.9169$$

Interpol bei 8 bar Tab. A-12

$$x_g = \frac{s_2 - s_f(8 \text{ bar})}{s_g(8 \text{ bar}) - s_f(8 \text{ bar})} = 0.334 \quad (\text{A-12})$$

$$u_3 = u_f(8 \text{ bar}) + x_g (u_g(8 \text{ bar}) - u_f(8 \text{ bar})) =$$

$$\dot{m} = \frac{\dot{W}_K}{u_2 - u_3} =$$

d)

$$\epsilon_K = \frac{|\dot{Q}_{\text{zul}}|}{|\dot{W}_K|} = \frac{|\dot{Q}_{\text{zul}}|}{|\dot{Q}_{\text{ab}} - \dot{Q}_{\text{zul}}|}$$