

$$1. a) \dot{Q}_{aus} : 1. HS : 0 = \dot{m}(h_{ein} - h_{aus}) + \dot{Q}_{aus} + \dot{Q}_R$$

$$\begin{aligned} \text{TAB A-2} \left\{ \begin{aligned} h_{ein}(70^\circ\text{C, siedend}) &= 292.98 \text{ kJ/kg} \\ h_{aus}(100^\circ\text{C, siedend}) &= 419.04 \text{ kJ/kg} \\ h_{ein}(70^\circ\text{C, gesättigt}) &= 292.98 \text{ kJ/kg} \\ h_{aus}(100^\circ\text{C, gesättigt}) &= 419.04 \text{ kJ/kg} \end{aligned} \right. \end{aligned}$$

$$\begin{aligned} \dot{Q}_{aus} &= -\dot{m}(h_{aus} - h_{ein}) + \dot{Q}_R \\ &= 62.182 \text{ kW} // \end{aligned}$$

$$b) \bar{T}_{KF} = \frac{\int_{s_a}^s T ds}{s_a - s_c} = \frac{1}{s_a - s_c} \cdot \left( \frac{T_a^2}{2} - \frac{T_c^2}{2} \right)$$

$$s_a - s_c = c_p \ln\left(\frac{T_a}{T_c}\right) =$$

$$c) \dot{s}_{crz} = \dot{m}[s_a - s_c] - \frac{\dot{Q}_{aus}}{\bar{T}_{KF}} =$$

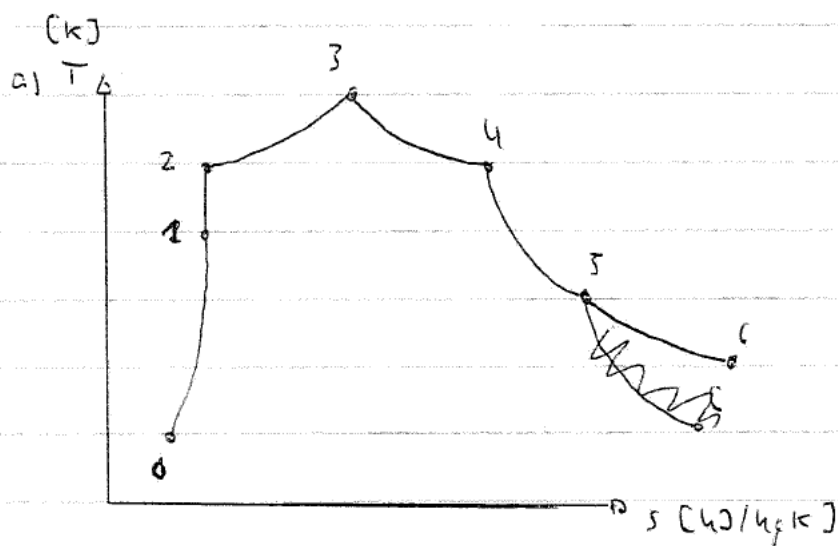
$$d) \dot{Q}_{R,12} = \dot{Q}_{aus,12} = 35 \text{ MW}$$

$$0 = \dot{m}_{ges,1} ($$

	[°C]	[bar]	
	T	P	
2.	0	0.191	
	293.15 -30		
1			isobar $\eta_{vis} < 1$
2			isobar
3			$Q_B = 1195 \text{ kJ/kg}$ , $\bar{T}_B = 1289 \text{ K}$
4		0.5	isobar
5	421.9 K	0.5	$w_5 = 220 \text{ m/s}$
6	328.075 K	0.191	isobar

$$w_{\text{eff}} = 200 \text{ m/s}$$

Verdicht



b)  $w_c$  &  $T_c$ :  $T_c = \left(\frac{P_2}{P_1}\right)^{\frac{n-1}{n}} T_5 = 328.075 \text{ K} //$

→ isobar

$$w_c = \frac{v_6}{v_5} \cdot w_5 = 437.427 \text{ m/s} //$$

$$v_5 = \frac{RT_5}{P_5} = 248.2823 \text{ m}^3/\text{kg}, 0.00248$$

$$R = c_p - c_v = 0.2874$$

$$k = \frac{c_p}{c_v} \rightarrow c_v = \frac{c_p}{k} = 0.719$$

$$v_6 = \frac{RT_c}{P_6} = 0.0049 \text{ kg/m}^3$$

$$c) \Delta c_{x, str} = c_{x, str6} - c_{x, str0}$$

$$\Delta c_{x, str} = m[h_a - h_c - T_0(s_a - s_c) + \Delta h_c] = 87.829 \text{ kJ/kg}$$

$$h_a - h_c = c_p(T_6 - T_0) = 85.436 \text{ kJ/kg}$$

$$T_0 = 243.15 \text{ K}$$

$$s_a - s_c = c_p \ln\left(\frac{T_6}{T_0}\right) - R \ln\left(\frac{p_6}{p_0}\right) = 0.30136 \text{ kJ/kgK}$$

$$\Delta h_c = \frac{w_6^2}{2} - \frac{w_0^2}{2} = 75'671.19 \text{ J} = 75.671 \text{ kJ/kg}$$

d)  $c_{x, verl}$  auf  $w_{ges}$  bezogen

$$Ex_{verl} = T_0 \dot{s}_{erz} \xrightarrow{\text{auf } w_{ges} \text{ bezogen}} c_{x, verl} = T_0 \dot{s}_{erz}$$

$$T_0 = 243.15 \text{ K}$$

$$\dot{s}_{erz} = (s_a - s_c) + \frac{q_j}{T_j} = (s_6 - s_0) + \frac{q_B}{T_B} = 1.2284$$

$$s_6 - s_0 = c_p \ln\left(\frac{T_6}{T_0}\right) = 0.30136 \text{ kJ/kgK}$$

$$\frac{q_B}{T_B} = 0.927 \text{ kJ/kgK}$$

$$\dot{c}_{x, verl} = T_0 \dot{s}_{erz} = 298.69 \text{ kJ/kg} //$$

3. a)  $P_{G,1}$  &  $m_g$ :

$$P_{G,1} = P_{\text{atm}} + \left( \frac{3241 \text{ g}}{A_{241}} \right) \cdot 10^{-5} + \left( \frac{0.141 \text{ g}}{A_{241}} \right) \cdot 10^{-5} = 1400,140159 \text{ //}$$

$$A_{241 \text{ Zylinder}} = 0.05 \text{ m}^2 \cdot \pi = 0.00785 \text{ m}^2$$

$$m_g: \text{ ~~Wasser~~ } n = \frac{P_1 V_1}{RT_1} = 0.0684 \text{ mol}$$

$$V_1 = 3.14 \cdot 10^{-3} \text{ m}^3$$

$$M_G = 50 \text{ g/mol}$$

$$m_G = n \cdot M_G = 3.4194 \text{ g //}$$

↳  $P_{G,2} = P_{G,1} \Rightarrow$  Masse steigt nicht, somit steigt der Druck  
konstant  $P_{G,2} = 1.40159 \text{ //}$

$$c) \text{ ~~Wasser~~ } \Delta u m_G = Q_{12} = -1082.23 \text{ kJ //}$$

$$\Delta u = u(T_2) - u(T_1) = c_v(T_2 - T_1) = -316.4984 \text{ J/kg}$$

$$\text{mit } T_2 = 0.003^\circ\text{C}$$

$$d) u_1 = u_{\text{Fest,ref}} + x_{\text{Fe}}(u_{\text{Fe,ref}} - u_{\text{Fe,ref}}) = -200.0928 \text{ kJ/kg}$$

$$u_{\text{Fe,ref}}(0^\circ\text{C}) = -333.45 \text{ kJ/kg}$$

$$u_{\text{Fe,ref}}(0^\circ\text{C}) = -0.0454 \text{ J/kg}$$

$$u_1 = u_1 m = \text{~~220.09 kJ~~ } -20.009 \text{ kJ}$$

$$u_1 = -20.0092842 \text{ kJ}$$

$$W_1 + Q_{12} = -21091.51 \text{ J}$$

$$u_2 = \frac{W_1 + Q_{12}}{m} = -220.914749 \text{ kJ/kg} \quad -220.915142149$$

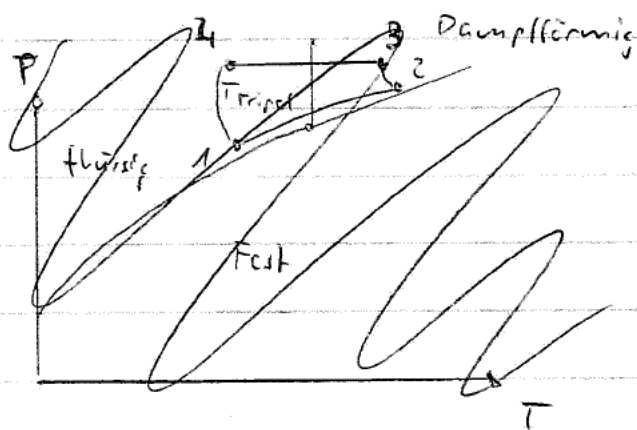
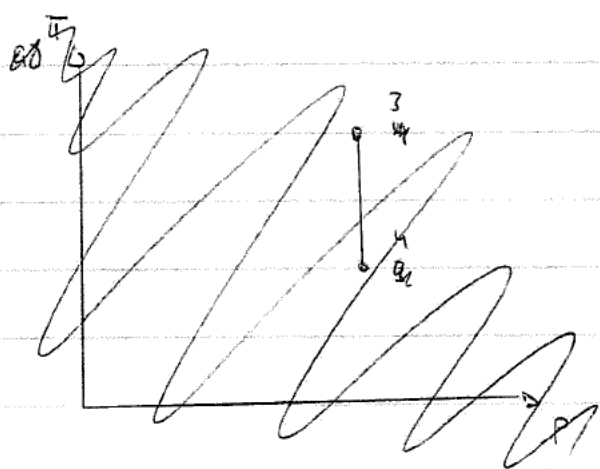
$$x_{2, \text{Eis}} = \frac{u_2 - u_{2\text{Fest}}}{u_{2\text{Fest}} - u_{2\text{flüssig}}} = 0.63250 = 0.633 //$$

$$u_{2\text{Fest}} = -332.442 \text{ kJ/kg}$$

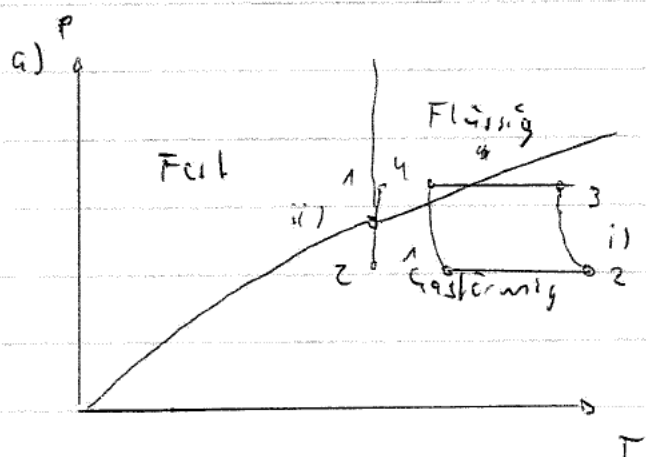
$$u_{2\text{flüssig}} = -0.0334 \text{ kJ/kg}$$

4.

	[kJ]	$P$ [bar]	$x$	
1	$-C$			$\rightarrow -6K$ zu $T_i$ $\rightarrow \dot{Q}_K$
2			1	isentrope $s = \text{const}$
3		8	<del>8</del>	$\dot{W}_K = 2P\dot{W}$
4		8	0	$\rightarrow \dot{Q}_{K2}$



WZ 143



b)  $\dot{W}_{R,174g} \rightarrow 2 \Rightarrow 3$  isentrope  $\rightarrow s = \text{const}$

$2 \rightarrow$  gesättigter Nüchmitteldampf

$4 \Rightarrow 1$  isentrope isochale

1. HS über  $2 \rightarrow 3$   $0 = \dot{m}(h_2 - h_3) - \dot{W}_K$

Wärme

$$1) \text{ in } T_2 = -10^\circ\text{C} - 6\text{K} = -16^\circ\text{C}$$

$$0 =$$

$$S_2 = 0.9525 \text{ kJ/K} = S_3$$

$$S_3 \rightarrow \text{in TIR A-9}$$

$$241,4 \text{ W} \quad 30/35^\circ\text{C}$$

$$\text{in int: } T_3 = 30 + \frac{0.9525 - 0.9444}{0.9574 - 0.9444} (35 - 30) = 30^\circ\text{C}$$