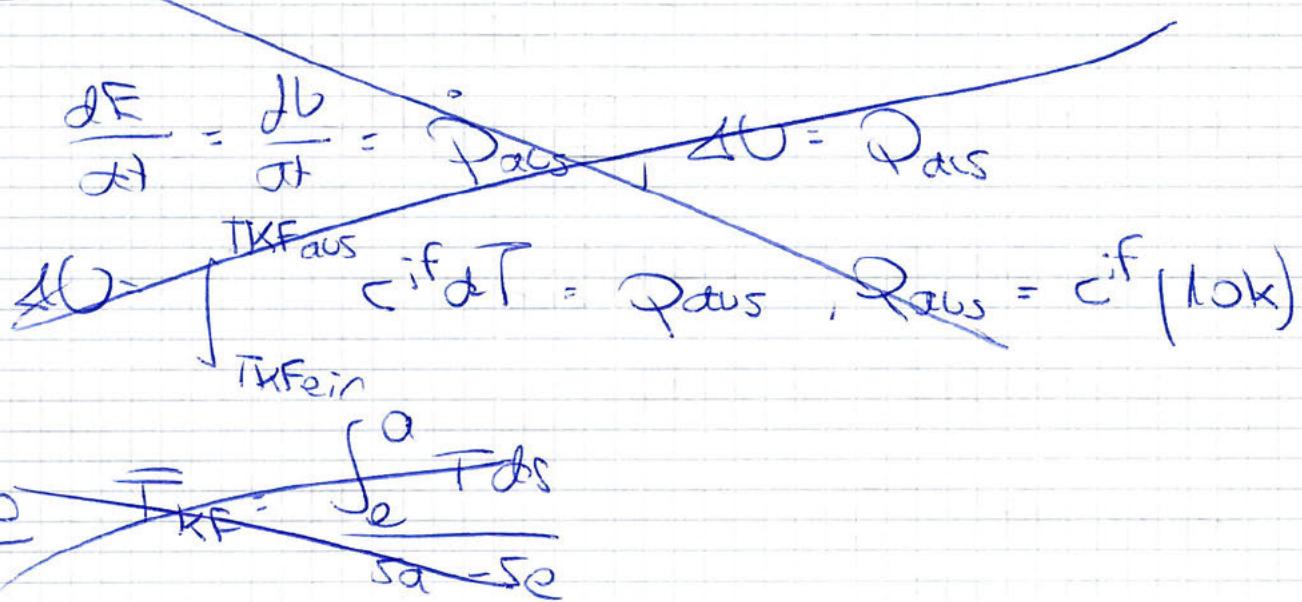


A1

la 1. HS Am Kühlmantel:



la 1. HS Um Kessel:

$$\dot{Q} = m_{ein} (h_{ein} - h_{aus}) + \dot{Q}_R - \dot{Q}_{aus}$$

$$h_{ein} (\text{TAB A2}) = 292.98 \frac{\text{kJ}}{\text{kg}}$$

$$h_{aus} (\text{TAB A2}) = 919.07 \frac{\text{kJ}}{\text{kg}}$$

$$\dot{Q}_{aus} = m_{ein} (h_{ein} - h_{aus}) + \dot{Q}_R = \underline{\underline{62.2 \text{ kJ}}}$$

Nb Hier kann das arithmetische Mittel verwendet werden:

$$\bar{T}_{KF} = \frac{T_{KF_a} + T_{KF_b}}{2} = \underline{\underline{293.15 \text{ K}}}$$

1c qgs: Sert Reaktor / XM

$$\dot{Q} = \dot{m} (s_{\text{ein}} - s_{\text{aus}}) + \frac{\dot{P}_{\text{aus}}}{T_{\text{KF}}} + \frac{\dot{Q}_R}{T_{100^\circ\text{C}}} \quad \text{Sert}$$

$$\dot{s}_{\text{ert}} = \dot{m} (s_{\text{aus}} - s_{\text{ein}}) + \frac{\dot{P}_{\text{aus}}}{T_{\text{KF}}} \cancel{+ \frac{\dot{Q}_R}{T_{100^\circ\text{C}}}} = \frac{\dot{Q}_R}{273,15\text{K}}$$

$$s_{\text{aus}} \Rightarrow T_{\text{BAC}} = 1.3069 \frac{\text{kJ}}{\text{kgK}}$$

$$s_{\text{ein}} \Rightarrow T_{\text{BAL}} = 0.9599 \frac{\text{kJ}}{\text{kgK}}$$

$$\dot{s}_{\text{ert}} = 26.9 \frac{\text{kJ}}{\text{K}}$$

1d $\Delta U = \Delta M (h_{\text{ein},12}) + 35 \text{ MJ}$

$$\Delta U = \frac{M}{g_e} (v_2 - v_1), \quad v_2 = x_D v_g + (1 - x_D) v_f$$

$$v_2 \Rightarrow T_{\text{BAC}} = 303.83 \frac{\text{kJ}}{\text{kg}}$$

$$v_1 \Rightarrow T_{\text{BAL}} = 929.39 \frac{\text{kJ}}{\text{kg}}$$

$$-693.8 \text{ MJ} = \Delta M h_{\text{ein},12} + 35 \text{ MJ}$$

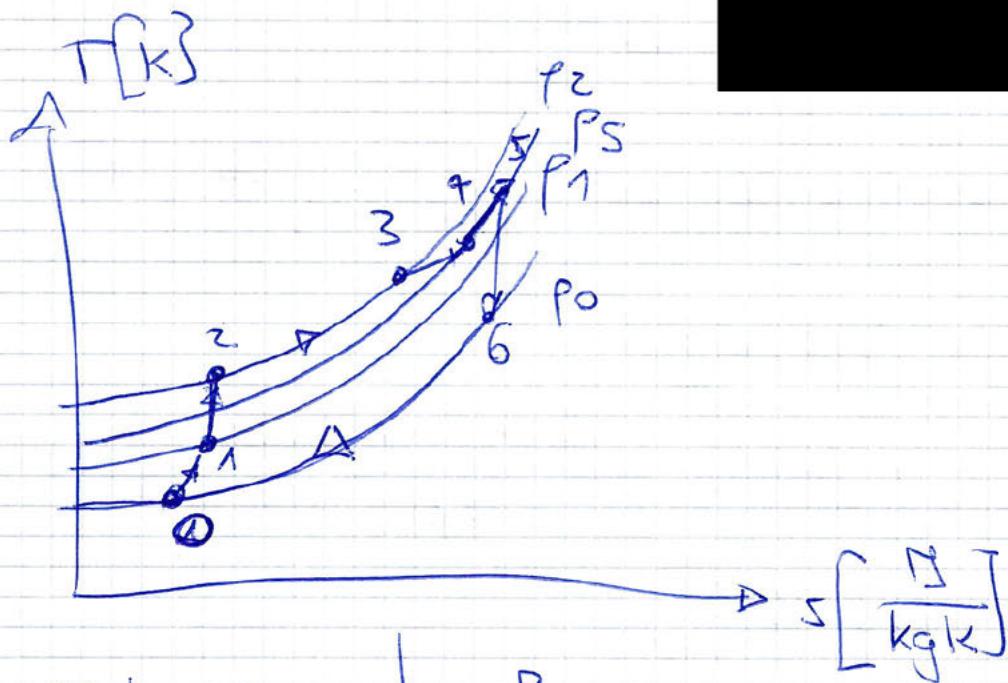
$$h_{\text{ein},12} \Rightarrow T_{\text{BAC}} = 2437.1 \frac{\text{kJ}}{\text{kg}}$$

$$(-693.8 \text{ MJ}) = 1 \text{ m} \cdot 2437.1 \frac{\text{kJ}}{\text{kg}} = 1 \text{ m} \cdot \underline{\underline{2.937 \text{ MJ}}}$$

$$\underline{\underline{\Delta M_{12} = 296.99 \text{ kg}}}$$

A2

2a



Z_{st}	T	s	P
1	-35°C	s_1	p_0
2		$s_2 = s_1$	$p_2 > p_0$
3		$s_3 > s_2$	$p_3 = p_2$
4		$s_4 > s_3$	$p_4 < p_3$
5	931.9K		$0.5 \cdot p_4 = p_7 = p_5$
6		$s_6 = s_5$	p_0

same same same same

2b ges: w_s, T_s

ISENTROPE SICHERHEIT, c_s, p_s, T_s bekannt

~~$$\dot{Q} = \dot{m} \left(h_s - h_g + \frac{c_s^2 - c_g^2}{2} \right)$$~~

~~$$\dot{m} = \dot{m}_{ges}$$~~

Exergiebilanz:

$$\dot{Q} = \dot{m}_{ges} \left(h_s - h_{6g} + \Delta ke \right), \quad \Delta ke = \frac{c_s^2 - c_g^2}{2}$$

$$h_s \rightarrow TAB A2Z = h(930K) + \frac{h(970K) - h(930K)}{10K} \cdot 1.9K$$

$$\underline{25} \quad h_5 = 953.36 \frac{\text{kJ}}{\text{kg}}$$

$$\text{Isentropic Ent. and: } T_6 = T_5 \left(\frac{P_6}{P_5} \right)^{\frac{n-1}{n}}$$

$$\underline{T_6 = 328.075 \text{K}}$$

$$\underline{h_6 = h(325 \text{K}) + \frac{h(330 \text{K}) - h(325 \text{K})}{5 \text{K}} (3.075 \text{K})}$$

$$h_6 = 333.93 \frac{\text{kJ}}{\text{kg}}$$

$$\underline{\dot{m}_{\text{ges}}^2 (h_5 - h_6) + \frac{\omega_5^2 - \omega_6^2}{2}}$$

$$\cancel{\dot{m}_{\text{ges}}^2 (h_6 - h_5) = \dot{m}_{\text{ges}} \frac{\omega_5^2 - \omega_6^2}{2}, -\omega_6^2 = 2(h_6 - h_5) - \omega_5^2}$$

$$\underline{\omega_6^2 = 2(h_5 - h_6) + \omega_5^2, \omega_6 = 998.26 \frac{\text{rad}}{\text{s}}}$$

$$\underline{\Delta ex_{\text{str}6} \approx -ex_{\text{str}0} = \dot{m}_{\text{ges}} (h_6 - h_0 - T_0 (s_6 - s_0) + \Delta ke)}$$

$$h_6 = 333.93 \frac{\text{kJ}}{\text{kg}}, h_0 = h(265.15 \text{K})$$

$$s_6 = s(T_6), s_0 = s(T_0), \Delta ke = \frac{\omega_6^2 - \omega_5^2}{2}$$

$$s(T_6) \approx 1.79 \frac{\text{kJ}}{\text{kgK}}, s_0 \approx 1.86 \frac{\text{kJ}}{\text{kgK}}$$

$$h_0 \approx 263 \frac{\text{kJ}}{\text{kg}}$$

} ENBAZ

$$\underline{4 ex_{\text{str}} = \frac{\Delta ex_{\text{str}}}{\dot{m}_{\text{ges}}} = 109.19 \frac{\text{kJ}}{\text{kg}} \quad 119.09 \frac{\text{kJ}}{\text{kg}}}$$

A3

$$\underline{3a} \quad p_{g,1} = p_{amb} + p_{EW} + p_{MK}$$

$$p_{EW} = \frac{M_{EW}}{\pi \left(\frac{D}{2}\right)^2}, \quad p_{MK} = \frac{M_{KG}}{\pi \left(\frac{R}{2}\right)^2}$$

$$p_{g,1} = 1 \text{ bar} + \cancel{12023 \text{ Pa}} + 127.91 \text{ Pa} + 39969.3 \text{ Pa}$$

$$\underline{p_{g,1} = 1.9 \text{ bar}}$$

$$\text{Mg: } p_{g,1} V_{g,1} = m_g R T_{g,1}, \quad R = \frac{\bar{R}}{M} = \frac{8.314 \frac{\text{J}}{\text{mol} \cdot \text{K}}}{30 \frac{\text{kg}}{\text{mol}}} = \frac{0.277 \frac{\text{J}}{\text{kg} \cdot \text{K}}}{\text{mol}}$$

$$m_g = \frac{p_{g,1} V_{g,1}}{R T_{g,1}} = 0.00342 \text{ kg} \quad R = 166.28 \frac{\text{N}}{\text{K} \cdot \text{kg}}$$

$$\underline{m_g = 3.42 \text{ g}}$$

$$\underline{3b} \quad \sigma_{EW,2} > 0, \text{ ges: } T_{g,2}, p_{g,2}$$

Zustand 2: Thermodyn. GGw zwischen Flüssigkeit und Gas,

heißt kein Wärmetransfer, heißt gleiche Temperatur.

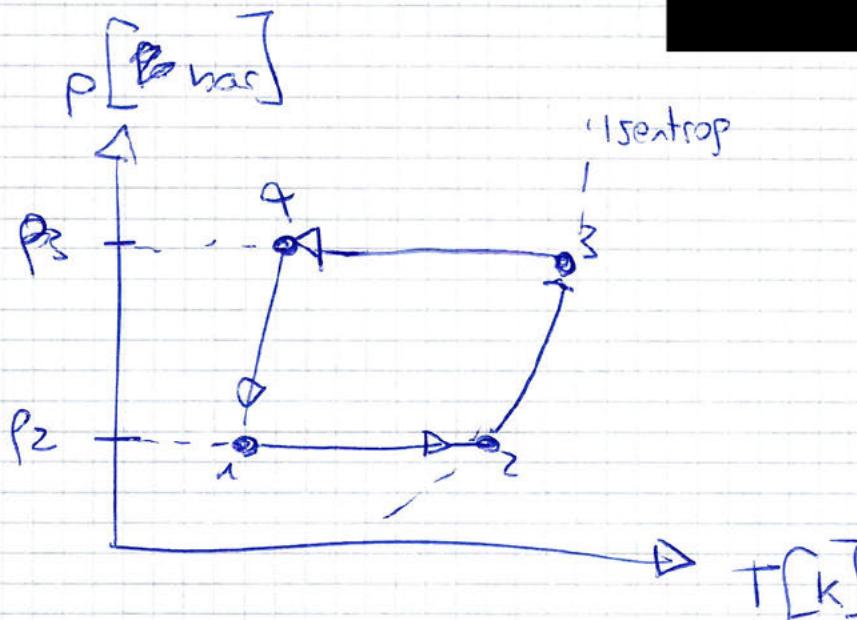
~~$$T = \frac{p_{g,1} V_{g,1}}{m_g R} = \frac{p_{EW} V_{g,1}}{M_{EW}}$$~~

$$\underline{T_{g,2} = T_{EW,2}, \quad p_{g,2} =}$$

Sc

A4

9a



9b

$$\dot{Q} = \frac{\dot{m}(h_1 - h_2)}{R_{AS_0}} + \dot{Q}_K$$

$$h_2 = T_{\text{verdampfer}} = T_i - 6K = -6K$$

$$h_1 = h_f(-6K), \quad h_2 = h_g(-6K)$$

$$x_1 = \frac{s - s_f}{s_g - s_f}$$

