PWS/Meesterproef vloeistofdynamica

Wiebe Derksen and Daniël Visser March 9, 2022

PWS begeleiders meneer Straatman en meneer Matena, expertbegeleider Aron Van Den Bogaard

Contents

1	\mathbf{Intr}	oduction	4
2	Wha	at algorithms are feasible to implement?	5
	2.1	Introduction to differential equations	5
	2.2	The algorithms	5
		2.2.1 Finite Difference Method(FDM)	5
		2.2.2 Finite Element Method(FEM)	6
		2.2.3 Finite Volume $Method(FVM)$	6
		2.2.4 Spectral Element Method	6
		2.2.5 Lattice Boltzmann Method	7
		2.2.6 Boundary Element Method	7
		2.2.7 Turbulence methods	7
	2.3	Some Choices	8
	2.4	Neglections in the Navier Stokes Equations	8
		2.4.1 The dimension	8
		2.4.2 Compressible and incompressible Navier Stokes Equations	8
		2.4.3 Viscosity	9
		2.4.4 Laminar and Turbulent flows	9
		2.4.5 Steady and unsteady	9
	2.5	Boundary conditions	9
		2.5.1 No-slip boundary condition	9
		2.5.2 Free slip boundary condition	10
		2.5.3 Dynamic boundary condition	10
		2.010 Bynamic soundary condition	10
3	The	implementation of the finite difference method	11
	3.1	Constants	11
	3.2	Odd-even decoupling	12
	3.3	Boundary conditions and walls	13
	3.4	The sizes of the grids	14
	3.5	Discretising the convection term and implementing the grid	15
	3.6	Discretising the diffusion term	18
	3.7	Discretising the pressure	19
	3.8	Implicit and explicit methods	19
	3.9	Discretising the time	20
		The algorithm	23
		The code	24
	•	3.11.1 Programming the algorithm	24
		3.11.2 Switching grids	31
		3.11.3 Putting it all together	33
4		alisation	34
	4.1	Drawing	34
	4.2	Data capturing	34

5 Conclusion 35

1 Introduction

People have been simulating for decades using computers, for aeronautics, movies, games and more. We thought this would be an interesting subject to write our PWS about because it is a quite difficult subject, but at the same time we both have a great interest in both physics and mathematics. We thought it would be easily doable but as time progressed , we started to realize this project would take quite a bit more time than we had expected. Nevertheless, it was a really interesting project of which we learned a lot.

2 What algorithms are feasible to implement?

2.1 Introduction to differential equations

There are many algorithms to execute fluid simulations, each has its own advantages and disadvantages. In this chapter we will discuss these algorithms and their pro's and cons.

A differential equation can be solved either numerically or analytically. An analytical solution is a solution for the entire domain of the function. A numerical solution only gives an approximation for some discrete values. Many differential equations are not analytically solvable, they have to be solved numerically. A numerical solution is often obtained using computers. [2]

2.2 The algorithms

In this section we will discuss some of the most used algorithms for solving the Navier-Stokes Equations, their advantages and disadvantages.

2.2.1 Finite Difference Method(FDM)

The Finite Difference Method(FDM) approximates the derivatives of a function using a truncated Taylor series. For a Taylor series around a point x=a the following formula applies. :[4]:

$$f(x) = \sum_{i=0}^{\infty} \frac{f^{(i)}}{i!} (x-a)^i$$

A computer cannot keep computing forever. Therefore we have to use a truncated Taylor series. The truncated Taylor series unto i=3 is given by [8]

$$f(x) = f(a) + f'(a)(x - a) + \frac{f''(a)(x - a)^2}{2} + \frac{f^{(3)}(a)(x - a)^3}{6} + O(\Delta x)^4$$

 $O(\Delta x)^4$ are the truncated terms.[10]. Using the above formula, we can calculate $f(x + \Delta x)$ by taking a=x[9]

$$f(x + \Delta x) = f(x) + f'(x)\Delta x + \frac{f''(x)(\Delta x)^2}{2} + \frac{f^{(3)}(\Delta x)^3}{6} + O(\Delta x)^4$$
 (1)

In the same way we can calculate $f(x - \Delta x)$:

$$f(x - \Delta x) = f(x) - f'(x)\Delta x + \frac{f''(x)(\Delta x)^2}{2} - \frac{f^{(3)}(x) * (\Delta x)^3}{6} + O(\Delta x)^4$$
 (2)

Using equation 1 we can approximate f'(x):

$$f(x + \Delta x) - f(x) = f'(x)\Delta x + O(x)^2$$

$$f'(x) = \frac{f(x + \Delta x) - f(x)}{\Delta x} + O(\Delta x)$$

 $O(x)^2$ changes in O(x) if it is divided by Δx . The equation above is called a first order approximation, because the lowest power in the big O is 1. The lowest power of the big O of a second order approximation is 2. $O(\Delta x)^n$ decreases to zero when Δx becomes smaller, because $O(\Delta x)^n$ consists only of powers of Δx . The higher the lowest power, the fastest $O(\Delta x)^n$ declines and the better the derivative is approximated. We can calculate the second order approximation using equations 1 and 2

$$f'(x) = \frac{f(x + \Delta x) - f(x - \Delta x)}{2\Delta x} \tag{3}$$

We can also use 1 and 2 to calculate the second approximation of the second derivative.

$$f''(x) = \frac{f(x + \Delta x) - 2f(x) + f(x - \Delta x)}{(\Delta x)^2}$$
(4)

Equation 3 can be used to turn equations ?? , ?? and ?? into a set of equations without deriatives. The values of these equations can be calculated.

2.2.2 Finite Element Method(FEM)

The Finite Element Method(FEM) is a commonly used to solve differential equations. It has a lot of applications, CFD's being only one of them. Unlike the FDM the FEM does not solve the equations for only a few points, but for the entire domain. It does so by approximating the differential equation with linear subfunctions. The linear subfunctions will have unknown coefficients. These coefficients are put into a matrix.

2.2.3 Finite Volume Method(FVM)

The finite volume method calculates the movement of "fluid particles". These particles are discretized points of a certain volume.[14] Therefore the FVM gives the exact expression for the average value of the solution (over the hence described volume). For each volume there is a flow in (Diffusion), a flow out (Convection), a transient term(the disturbance of the volume) and a source term resulting in the formula below.

$$\frac{\partial \rho \phi}{\partial t} + \nabla \cdot (\rho \boldsymbol{v} \phi) = \nabla \cdot (\Gamma^{\phi} \nabla \phi) + Q^{\phi}$$

2.2.4 Spectral Element Method

The spectral element method is a solution to the partial differentiation equation derived from the finite element method.

2.2.5 Lattice Boltzmann Method

The Lattice Boltzmann Method models liquids as if the liquid exists of a n number of fictive particles. The method divides the simulation in two interchanging steps, collision and streaming. The steps change the density $\rho(\vec{x},t)$ at position \vec{x} at time t. Because the Lattice Boltzmann method works within a lattice (a grid with a n amount of points in a m number of dimensions), you can draw up a formula $f_i(\vec{x},t)$. In this formula f_i is the the influence of a neighbouring point i on \vec{x} (a point on the lattice). The total movement vector in a point then becomes:

$$P_i(\vec{x},t) = \sum_{i=0}^{a} f_i(\vec{x},t)$$

Where a is the number of adjacent points on the lattice and P the total movement of the particle.

Collision For simulating the collision of particles within the lattice, the formula is [7]:

$$f_i(\vec{x}, t + \delta_t) = f_i(\vec{x}, t) + \frac{f_i^{eq}(\vec{x}, t) - f_i(\vec{x}, t)}{\tau_f}$$

 $f_i(\vec{x}, t + \delta_t)$ is the influence at time $t + \delta_t$ with δ_t the size of the time step. A smaller δ_t leads to a more accurate simulation but also lead to more computing time required to simulate a certain situation.

 τ_f is a constant that depends on the viscosity of the simulated liquid. $f_i^{eq}(\vec{x},t)$ is the equilibrium density.

Streaming For simulating the actual movement of the particles the formula is:

$$f_i(\vec{x} + \vec{e_i}, t + \delta_t) = f_i(\vec{x}, t)$$

Here $f_i(\vec{x} + \vec{e_i}, t + \delta_t)$ is the fluid density at point \vec{x} and \vec{e} is the movement vector(the change in perceived density) of the density.

2.2.6 Boundary Element Method

The boundary element method is a method of simulating fluid dynamics with the presence of a influence of the boundary of the simulation, on the simulation. For this reason the boundary element method is quite complex and not really in the scope of this project. [12]

2.2.7 Turbulence methods

Apart from the above mentioned methods, there are also turbulence methods. These methods are able to simulate turbulent flows of liquids. These methods use a huge amount of computing power and thus are not really feasible for this paper.

2.3 Some Choices

Due to the finite difference method being relatively easy to implement, we have decided to start our simulation by implementing that method. For a programming language we have chosen (provisionally) for Rust as it is fast and reasonably easy.

2.4 Neglections in the Navier Stokes Equations

2.4.1 The dimension

It is easier for computers to solve a 2D problem than a 3D problem, because for a 2D problem the number of grid points is smaller then for a 3D problem. For example, a 10 by 10 grid contains 100 points, while a 10 by 10 by 10 grid contains 1000 points. Furthermore, 2D rendering is easier then 3D rendering. However, nowadays computers are very fast. Therefore, our computers will be able to solve 3D problems. Since we intend to simulate a container with water, we will do a 3D simulation.

2.4.2 Compressible and incompressible Navier Stokes Equations

All fluids can be compressed. Their volume gets smaller when the pressure on the gas or fluid increases. However, in many cases the change in volume is not significant, then the flows can be approximated as incompressible flows. The Navier Stokes Equations can be simplified to the incompressible Navier Stokes Equations when a fluid is not compressible. Water is not very compressible[21], so we will use the incompressible Navier Stokes Equations. The incompressible Navier Stokes equations for a Newtonian fluid, such as water, are:[18] [26]

$$\begin{split} &\frac{\partial v_{x}}{\partial x} + \frac{\partial v_{y}}{\partial y} + \frac{\partial v_{z}}{\partial z} = 0 \\ &\left(\frac{\partial v_{x}}{\partial t} + \frac{\partial v_{x}}{\partial x} v_{x} + \frac{\partial v_{x}}{\partial y} v_{y} + \frac{\partial v_{x}}{\partial z} v_{z} \right) \rho = -\frac{\partial p}{\partial x} + \eta \left(\frac{\partial^{2} v_{x}}{\partial x^{2}} + \frac{\partial^{2} v_{x}}{\partial y^{2}} + \frac{\partial^{2} v_{x}}{\partial z^{2}} \right) + \rho g_{x} \\ &\left(\frac{\partial v_{y}}{\partial t} + \frac{\partial v_{y}}{\partial x} v_{x} + \frac{\partial v_{y}}{\partial y} v_{y} + \frac{\partial v_{y}}{\partial z} v_{z} \right) \rho = -\frac{\partial p}{\partial y} + \eta \left(\frac{\partial^{2} v_{y}}{\partial x^{2}} + \frac{\partial^{2} v_{y}}{\partial y^{2}} + \frac{\partial^{2} v_{y}}{\partial z^{2}} \right) + \rho g_{y} \\ &\left(\frac{\partial v_{z}}{\partial t} + \frac{\partial v_{z}}{\partial x} v_{x} + \frac{\partial v_{z}}{\partial y} v_{y} + \frac{\partial v_{z}}{\partial z} v_{z} \right) \rho = -\frac{\partial p}{\partial z} + \eta \left(\frac{\partial^{2} v_{z}}{\partial x^{2}} + \frac{\partial^{2} v_{z}}{\partial y^{2}} + \frac{\partial^{2} v_{z}}{\partial z^{2}} \right) + \rho g_{z} \end{split}$$

$$(5)$$

The equation at the top is called the continuity equation. The others are the momentum equations. The spatial derivatives of the left hand sides are called the convection terms. The parts on the right hand sides between brackets are called the diffusion terms. The parts involving pressure are the pressure terms and ρg is the gravitational force.

2.4.3 Viscosity

All fluids have viscosity. But, like compressibility, it can be neglected sometimes. Viscosity is: $\eta = \frac{F/A}{dv_x/dz}$. Here F is the shear force, that is the force parallel to a surface. A is the surface and dv_x/dz is the change in velocity.[22]. We will not neglect viscosity, because we do intend to simulate a water container with boundaries and viscosity is important near the boundaries, because there is dissipation over there.[21] Dissipation is the conversion of some for of energy to heat energy[23]. Without viscosity the Navier Stokes Equations reduce to the Euler Equations[21].

2.4.4 Laminar and Turbulent flows

Flows can be either laminar or turbulent [21]. In laminar flows there is no disruption between adjacent layers, but in turbulent flows there is. Turbulent flows have chaotic paths and they swirl. The Navier Stokes Equations for laminar and turbulent flows are the same. But there are very small changes in pressure, velocity and temperature in turbulent flows, which should be dealt with. Although a turbulent flow can be modeled using the Navier Stokes Equations, this costs a lot of computation power due to the small changes. [24] Therefore, they are often modeled in another way. The simulation of turbulent flows is beyond the scope of this project.

2.4.5 Steady and unsteady

A flow is either steady or unsteady[21]. In a steady flow parameters, such as velocity, do not change over time. In a unsteady flow parameters can change over time. [25] We will simulate a unsteady flow, because we want that the water in the container is able to move.

2.5 Boundary conditions

To solve a partial differential equation it is necessary to enforce boundary conditions. A container with water has two types of boundaries. One type are the walls and the floor. The other is the free surface of the water. The free surface is the surface where the water and air touch each other. The boundary condition at the free surface is trickier than that at the walls and floor, since the free surface can move, while the walls and floors can not.

2.5.1 No-slip boundary condition

The no-slip boundary condition supposes the velocity of a fluid that touches a solid is equal to the velocity of the solid [16].

2.5.2 Free slip boundary condition

The free-slip boundary condition presumes the velocity of the fluid perpendicular to the wall is zero, so the fluid can not move through the wall. But, it does not restrict the velocity parallel to the wall.[17]

2.5.3 Dynamic boundary condition

The dynamic boundary condition assumes the pressure on the free surface must be constant.

3 The implementation of the finite difference method

3.1 Constants

First, we define some constants. We have not taken significance in account, because we sometimes needed to add more zeros to prevent errors. These errors happen because Rust only wants decimal numbers as f32, although they can end with .0 .

```
1 ///Physical constants
const GRIDELEMENTSCALE: f32 = 0.05;//The size of a grid
      element in meters(denoted in equations as delta x)
3 const TIMESTEPSIZE: f32 = 0.0005;//The size of a time step
      size in seconds
4 const DENSITY: f32 = 1000.0;//Density of the liquid in kg/m
      ^{3}. We simulate water.
  const EXTERNALFORCE : [f32; 3] = [0.0,0.0,-9.81];//Gravity in
6 const VISCOSITY: f32 = 0.001;//Viscosity in Pa*s.
  const ATMOSPHERIC_PRESSURE: f32=101.325;//Atmospheric pressure
       in Pa
  const MAXITERATIONSPERTIMEFRAME:i32=200;//This constant sets a
       maximum so the computer can not get in an infinite loop.
  const RELEXATION: f32=1.0;//Pressure correction is often
      underestimated, this factor should be between 1.4 and 1.8.
const ALLOWEDERROR: f32=0.000001;
  //Pressure is measured in Pascal, because it is the standard
13
      SI unit for pressure.
15 //Grid size(e.g. number of elements in each dimension)
const PRESSUREGRIDSIZE: [usize; 3] = [10,10,10];//x,y,z
```

3.2 Odd-even decoupling

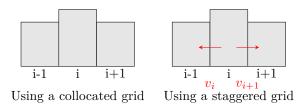


Figure 1: Collocated and staggered grids

The Finite Difference Method calculates the pressure and velocity at discrete grid points. We can choose ourselves which variables will be calculated at which points. It would be the most easy to store all variables at every point. Such a grid is called a collocated grid[27]. However, as figure 1 shows, there will be no fluid flow between cell i-1 and i and cell i and i+1 when the pressure in cells i-1 and i+1 is equal in such a grid. This phenomenon is called odd-even decoupling and happens because the derivative in cell i will be zero[27]. It is called so because information from odd and even cells are not combined properly[27]. To solve that problem we will use a staggered grid, such as in the right side of figure 1. A staggered grid consists of cells. The pressure is stored in the cell center and the velocities in the cell edges that are perpendicular to them[27]. As one can see, the derivatives will not be zero anymore, since the flow between two cells will not depend on the pressure in other cells anymore.

3.3 Boundary conditions and walls

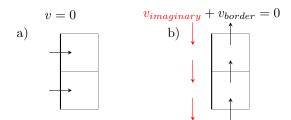


Figure 2: Wall boundary conditions

The water container is surrounded by walls on all sides. We will use a noslip boundary conditions at the walls, as discussed in paragraph 2.5.1[28]. This means the velocities of the water at the wall will be equal to the velocity of the wall. The wall velocity is always zero, so the velocity of the water is zero at points on the wall. Therefore, all velocity components should be zero for wall points[28]. Unfortunately, as can be seen in figure 2.a only the velocity perpendicular to the wall has points that are at the wall. However, by using an imaginary velocity outside the box we can obtain the velocity at the wall using the average[28]:

$$v_{wall} = \frac{v_{imaginary} + v_{border}}{2}$$

Here v is parallel to the wall(so not necessarily in the y-direction), v_{wall} is the velocity at a wall point, v_{border} is the velocity that is closest to the certain wall point and $v_{imaginary}$ is the imaginary velocity. We can modify the formula to obtain $v_{imaginary}$ quite easily:

$$\begin{split} v_{wall} &= 0 \\ &= > \frac{v_{imaginary} + v_{border}}{2} = 0 \\ &= > v_{imaginary} + v_{border} = 0 \\ &= > v_{imaginary} = -v_{border} \end{split}$$

Because of the imaginary velocity grid points, we will have to make the grid larger in some directions.

In short, we have the following boundary conditions:

- 1) The velocities on the edge of the box that are perpendicular to the box are zero.
- 2) The imaginary velocities are equal to the inverse of the velocities opposite of the wall.

3.4 The sizes of the grids

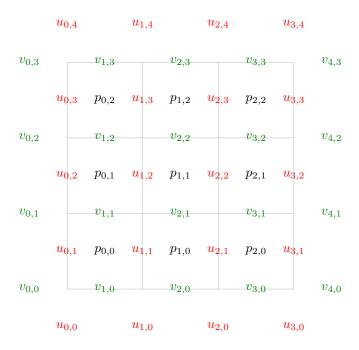


Figure 3: A 3*3 pressure grid

If we were using a collocated grid we would store our data in an array with the desired dimensions. However, we are using a staggered grid. This complicates the grid sizes a lot. We will have to use three seperate grids for velocity with different sizes and another grid for the pressure. Let u, v and w denote the velocities in respectively the x, y and z direction. In the directions that are orthogonal to the velocities of a velocity grid the size of that grid will be the size of the pressure grid plus one. We have illustrated this in figure 3. The size of the grid in the dimension that is parallel to the velocities that the grid contains is the pressure grid size plus two. The sizes in those directions are that size because of the imaginary velocities we need to store.

3.5 Discretising the convection term and implementing the grid

We will express the convection terms of equation 5 as $\partial_c[28]$.

$$\partial_{c}u = \rho(u\frac{\partial u}{\partial x} + v\frac{\partial u}{\partial y} + w\frac{\partial u}{\partial z})$$

$$\partial_{c}v = \rho(u\frac{\partial v}{\partial x} + v\frac{\partial v}{\partial y} + w\frac{\partial v}{\partial z})$$

$$\partial_{c}w = \rho(u\frac{\partial w}{\partial x} + v\frac{\partial w}{\partial y} + w\frac{\partial w}{\partial z})$$
(6)

Computers can not exactly calculate the derivatives, so we will have to approximate them to solve equation 5. We will be using Forward Time Central Space(FTCS) for approximating the derivatives[28]. This means we will use first order forward derivatives for time and second order central derivatives for space. We can calculate the convection terms $u\frac{\partial u}{\partial x}$, $v\frac{\partial v}{\partial y}$ and $w\frac{\partial w}{\partial x}$ using equation 3. In the equations below, one might notice that we have used Δx everywhere and have not used Δy or Δz . We have done this because we set $\Delta x = \Delta y = \Delta z$.

$$\begin{split} u \frac{\partial u}{\partial x} &= u_{i,j,k} \frac{u_{i+1,j,k} - u_{i-1,j,k}}{2\Delta x} \\ v \frac{\partial v}{\partial y} &= v_{i,j,k} \frac{v_{i,j+1,k} - v_{i,j-1,k}}{2\Delta x} \\ w \frac{\partial w}{\partial z} &= w_{i,j,k} \frac{w_{i,j,k+1} - w_{i,j,k-1}}{2\Delta x} \end{split}$$

However, calculating the other convection terms is more complex, because we have to estimate a velocity at point (i,j,k) of a grid which is not defined at that grid point. We can however estimate those velocities by taking the average of some nearby velocities, as in figure 4[28].

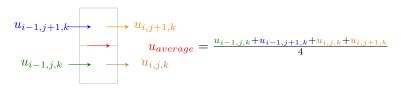


Figure 4: average of velocity

$$\begin{split} v\frac{\partial u}{\partial y} &= \frac{v_{i,j-1,k} + v_{i+1,j-1,k} + v_{i,j,k} + v_{i+1,j,k}}{4} \frac{u_{i,j+1,k} - u_{i,j-1,k}}{2\Delta x} \\ w\frac{\partial u}{\partial z} &= \frac{w_{i,j,k-1} + w_{i+1,j,k-1} + w_{i,j,k} + w_{i+1,j,k}}{4} \frac{u_{i,j,k+1} - u_{i,j,k-1}}{2\Delta x} \\ u\frac{\partial v}{\partial x} &= \frac{u_{i-1,j,k} + u_{i-1,j+1,k} + u_{i,j,k} + u_{i,j+1,k}}{4} \frac{v_{i+1,j,k} - v_{i-1,j,k}}{2\Delta x} \\ w\frac{\partial v}{\partial z} &= \frac{w_{i,j,k-1} + w_{i,j+1,k-1} + w_{i,j,k} + w_{i,j+1,k}}{4} \frac{v_{i,j,k+1} - v_{i,j,k-1}}{2\Delta x} \\ u\frac{\partial w}{\partial x} &= \frac{u_{i-1,j,k} + u_{i-1,j,k+1} + u_{i,j,k} + u_{i,j,k+1}}{4} \frac{w_{i+1,j,k} - w_{i-1,j,k}}{2\Delta x} \\ v\frac{\partial w}{\partial y} &= \frac{v_{i,j-1,k} + v_{i,j-1,k+1} + v_{i,j,k} + v_{i,j,k+1}}{4} \frac{w_{i,j+1,k} - w_{i,j-1,k}}{2\Delta x} \end{split}$$

We do not want to use these long equations in the code everywhere, since that would be a lot of work and unclear. Therefore, we will create a function that will calculate the partial derivative and a function that will calcute the average velocity at at point. To do this, we first need to create a struct that stores a velocity grid and the dimension of that grid.

```
pub struct VelocityGrid{
grid: Vec<Vec<f32>>>,
dimension: usize,
}
```

As one can see, the grid is stored in a vector (Vec means vector). In Rust, a vector is an array that can have different sizes. Furthermore, the dimension of the array is stored as a usize, which basically is an integer with a maximum length that corresponds to the maximum length of an array. The values 0,1 and 2 for dimension denote the x-, y-, and z-direction respectively. To prevent the use of a lot of if-statements, we create a function that can convert the dimension number to an array for which all elements, except the element corresponding to the dimension number are zero.

```
//Gives you the unit vector of the dimension with the given
number.
//x - 0, y - 1, z - 2
fn get_dimension(dimension_number:usize)->[usize; 3]{
let mut dim = [0,0,0];
dim[dimension_number]=1;
return dim;
}
```

Now we can create a function for the second order spatial derivative.

```
return (f.grid[x+dim[0]][y+dim[1]][z+dim[2]] - f.grid[x-
dim[0]][y-dim[1]][z-dim[2]])/(2.0*GRIDELEMENTSCALE);
}
```

Besides that, we can now also calculate the average velocity, as in figure 4.

Now we use the above two functions to write a function that calculates the convections terms $\partial_c u$, $\partial_c v$ and $\partial_c w$ from equation 6. We will write one function that is able to calculate all these terms:

```
1 fn convection_term(velocity_field_last_time_step: &
      VelocityGrid, orthogonal_velocity_field_a: &VelocityGrid,
      orthogonal_velocity_field_b: &VelocityGrid, x: usize, y:
      usize, z:usize ) -> f32{//} calculate the convection term
       return DENSITY*(velocity_field_last_time_step.grid[x][y][
      z]*second_order_spatial_derivative(&
      velocity_field_last_time_step, x, y, z,
      velocity_field_last_time_step.dimension)
                  +get_velocity_from_orthogonal_grid(&
      orthogonal_velocity_field_a, x, y, z,
      velocity_field_last_time_step.dimension)*
      second_order_spatial_derivative(
      velocity_field_last_time_step, x, y, z,
      orthogonal_velocity_field_a.dimension)
                  +get_velocity_from_orthogonal_grid(&
      orthogonal_velocity_field_b, x, y, z,
      velocity_field_last_time_step.dimension)*
      second_order_spatial_derivative(
      velocity_field_last_time_step, x, y, z,
      orthogonal_velocity_field_b.dimension));
5 }
```

3.6 Discretising the diffusion term

Like the convection term, the diffusion term contains no temporal terms. Of course it varies, since it's terms do vary over time, but we can calculate it using information from only one timestep. We will abreviate the diffusion term of u as $\partial_d u$ and the diffusion terms of v and w in a similar way[28]. The diffusion terms of equation 5 are[28]:

$$\partial_{d}u = \eta \left(\frac{\partial^{2}u}{\partial x^{2}} + \frac{\partial^{2}u}{\partial y^{2}} + \frac{\partial^{2}u}{\partial z^{2}}\right)$$

$$\partial_{d}v = \eta \left(\frac{\partial^{2}v}{\partial x^{2}} + \frac{\partial^{2}v}{\partial y^{2}} + \frac{\partial^{2}v}{\partial z^{2}}\right)$$

$$\partial_{d}w = \eta \left(\frac{\partial^{2}w}{\partial x^{2}} + \frac{\partial^{2}w}{\partial y^{2}} + \frac{\partial^{2}w}{\partial z^{2}}\right)$$
(7)

We can calculate it using equation 4:

```
fn second_order_second_spatial_derivative(f: &VelocityGrid, x:
    usize, y:usize, z:usize, dimension_number:usize) -> f32{
    let dim = get_dimension(dimension_number);
    return(f.grid[x+dim[0]][y+dim[1]][z+dim[2]]-2.0*f.grid[x][
    y][z]+f.grid[x-dim[0]][y-dim[1]][z-dim[2]])/(
    GRIDELEMENTSCALE*GRIDELEMENTSCALE);
}
```

The sum of all three second derivatives is called the laplacian. [28]

So we are now able to calculate the diffusion term using:

```
let diffusion=VISCOSITY*(laplacian(velocity_field, x, y, z));
```

We will not put this into a function already, because we do not know all the other terms yet.

3.7 Discretising the pressure

$$p_{i-1,j-1,k-1} \quad p_{i,j-1,k-1}$$

$$\bullet \quad \to \bullet$$

$$\frac{\partial p}{\partial x} = \frac{p_{i,j-1,k-1} - p_{i-1,j-1,k-1}}{\Delta x}$$

Figure 5: derivative of pressure

As in figure 5, we can calculate the derivatives $\frac{\partial p}{\partial x}$, $\frac{\partial p}{\partial y}$ and $\frac{\partial p}{\partial z}$

$$\frac{\partial p}{\partial x} = \frac{p_{i,j-1,k-1} - p_{i-1,j-1,k-1}}{\Delta x}$$

$$\frac{\partial p}{\partial y} = \frac{p_{i-1,j,k-1} - p_{i-1,j-1,k-1}}{\Delta x}$$

$$\frac{\partial p}{\partial z} = \frac{p_{i-1,j-1,k} - p_{i-1,j-1,k-1}}{\Delta x}$$
(8)

Here, (i, j, k) denotes the coordinates of the velocity in the direction we are differentiating in. We can turn these equations into code:

3.8 Implicit and explicit methods

Discretising the time can be done by using either an implicit or an explicit methods. [29] In explicit methods, all terms except for one belong to the current timestep and the remanining term that belongs to the next timestep can be calculated easily. [29] In implicit methods, more variables belong to the next timestep. At first, one variable is calculated in the same way as in the explicit methods and the values of the other variables are not changed. [29] Thereafter, the variables are corrected iteratively so that the solution will converge. [29] In the case of the incompressible Navier-Stokes equation, this means the continuity equation will converge to zero. Consequently, in explicit methods the continuity equation will always converge to zero. However, in explicit methods it is just assumed that the continuity equation holds. For the continuity equation to hold the timestep size should be very low in explicit methods. [29] The timestep size

can be higher in implicit methods, so less timesteps are needed. [29] However, explicit methods do not need multiple iterations per timestep. Therefore, they compute a timestep faster. [29]We will use an implicit method because we intend to be able to do long simulations and they are better for larger time intervals.[29]

3.9 Discretising the time

Using the formulas for $\partial_d u$ and $\partial_d c$ we can write equation 5 as [28]:

$$\rho \frac{\partial u}{\partial t} + \partial_c u = -\frac{\partial p}{\partial x} + \partial_d u + \rho g_x$$

$$\rho \frac{\partial v}{\partial t} + \partial_c v = -\frac{\partial p}{\partial y} + \partial_d v + \rho g_y$$

$$\rho \frac{\partial w}{\partial t} + \partial_c w = -\frac{\partial p}{\partial z} + \partial_d w + \rho g_z$$
(9)

We use this notation because it is a lot shorter. As discussed previously, we will use forward time for the derivatives. Let a^n denote a in the current timestep and a^{n+1} a in the next timestep, where a is a variable. As discussed in chapter 3.8, we will use an implicit method. We will rewrite the Navier Stokes Equations with the spatial pressure derivative of the next timestep. This will allow us to enforce convergence. [28]

$$\rho \frac{u^{n+1} - u^n}{\Delta t} + \partial_c u = -\frac{\partial p^{n+1}}{\partial x} + \partial_d u + \rho g_x$$

$$\rho \frac{v^{n+1} - v^n}{\Delta t} + \partial_c v = -\frac{\partial p^{n+1}}{\partial y} + \partial_d v + \rho g_y$$

$$\rho \frac{w^{n+1} - w^n}{\Delta t} + \partial_c w = -\frac{\partial p^{n+1}}{\partial z} + \partial_d w + \rho g_z$$
(10)

Unfortunately, we now have two variables for each formula: $\frac{u^{n+1}-u^n}{\Delta t}$ and $\frac{\partial p^{n+1}}{\partial x}$, for x for instance. Therefore, we can not just solve this formula. We can however set the pressure term to the current pressure term and correct the error that is created in that way later. We will denote the velocities obtained in that way \tilde{u} , \tilde{v} and $\tilde{w}[28]$.

$$\rho \frac{\tilde{u} - u^n}{\Delta t} + \partial_c u = -\frac{\partial p^n}{\partial x} + \partial_d u + \rho g_x$$

$$\rho \frac{\tilde{v} - v^n}{\Delta t} + \partial_c v = -\frac{\partial p^n}{\partial y} + \partial_d v + \rho g_y$$

$$\rho \frac{\tilde{w} - w^n}{\Delta t} + \partial_c w = -\frac{\partial p^n}{\partial z} + \partial_d w + \rho g_z$$
(11)

These equations contain only one unknown variable (per equation). We can rewrite them to calculate that variable.

$$\tilde{u} = u^n + \frac{\Delta t}{\rho} \left(-\frac{\partial p^n}{\partial x} - \partial_c u + \partial_d u + \rho g_x \right)$$

$$\tilde{v} = v^n + \frac{\Delta t}{\rho} \left(-\frac{\partial p^n}{\partial y} - \partial_c v + \partial_d v + \rho g_y \right)$$

$$\tilde{w} = w^n + \frac{\Delta t}{\rho} \left(-\frac{\partial p^n}{\partial z} - \partial_c w + \partial_d w + \rho g_z \right)$$
(12)

Now we substract equation 10 from 11.

$$\begin{split} &\rho \frac{\tilde{u} - u^{n+1}}{\Delta t} \\ &= -\frac{p_{i,j-1,k-1}^n - p_{i-1,j-1,k-1}^{n+1} - (p_{i,j-1,k-1}^{n+1} - p_{i-1,j-1,k-1}^n)}{\Delta x} \\ &= -\frac{(p_{i-1,j-1,k-1}^{n+1} - p_{i-1,j-1,k-1}^n) - (p_{i,j-1,k-1}^{n+1} - p_{i,j-1,k-1}^n)}{\Delta x} \\ &= -\frac{p_{i-1,j-1,k-1}^n - p_{i,j-1,k-1}^n}{\Delta x} \\ &= -\frac{p_{i-1,j-1,k-1}^n - p_{i,j-1,k-1}^n}{\Delta x} \\ &= -\frac{p_{i-1,j,k-1}^n - p_{i-1,j-1,k-1}^n - (p_{i-1,j,k-1}^{n+1} - p_{i-1,j-1,k-1}^n)}{\Delta x} \\ &= -\frac{(p_{i-1,j-1,k-1}^{n+1} - p_{i-1,j-1,k-1}^n) - (p_{i-1,j,k-1}^{n+1} - p_{i-1,j,k-1}^n)}{\Delta x} \\ &= -\frac{p_{i-1,j-1,k-1}^n - p_{i-1,j-1,k-1}^n}{\Delta x} \\ &= -\frac{p_{i-1,j-1,k-1}^n - p_{i-1,j-1,k-1}^n - (p_{i-1,j-1,k}^{n+1} - p_{i-1,j-1,k-1}^n)}{\Delta x} \\ &= -\frac{(p_{i-1,j-1,k-1}^{n+1} - p_{i-1,j-1,k-1}^n) - (p_{i-1,j-1,k}^{n+1} - p_{i-1,j-1,k}^n)}{\Delta x} \\ &= -\frac{p_{i-1,j-1,k-1}^n - p_{i-1,j-1,k-1}^n - (p_{i-1,j-1,k}^{n+1} - p_{i-1,j-1,k}^n)}{\Delta x} \\ &= -\frac{p_{i-1,j-1,k-1}^n - p_{i-1,j-1,k-1}^n}{\Delta x} \end{split}$$

Where $p'_{i,j-1,k-1} = p^{n+1}_{i,j-1,k-1} - p^n_{i,j-1,k-1}$ and $p'_{i-1,j-1,k-1} = p^{n+1}_{i-1,j-1,k-1} - p^n_{i-1,j-1,k-1}$. The same is valid for the other directions. The terms denoted by p' are the pressure correction terms. We can calculate the velocity at the next

timestep if we know the pressure correction:

$$u^{n+1} = \tilde{u} - \frac{\Delta t}{\rho \Delta x} (p'_{i,j-1,k-1} - p'_{i-1,j-1,k-1})$$

$$v^{n+1} = \tilde{v} - \frac{\Delta t}{\rho \Delta x} (p'_{i-1,j,k-1} - p'_{i-1,j-1,k-1})$$

$$w^{n+1} = \tilde{w} - \frac{\Delta t}{\rho \Delta x} (p'_{i-1,j-1,k} - p'_{i-1,j-1,k-1})$$
(14)

However, we still need to know the pressure to solve this equation. The velocity and pressure should satisfy the continuity equation (the upper equation in 5). We will use it to obtain the pressure. [28]

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0$$

We can discretise this equation for the timestep n+1 to obtain a formula for which the sole unknowns are the pressures. The pressure term has the coordinates (i,j,k)

$$\frac{u_{i+1,j+1,k+1}^{n+1} - u_{i,j+1,k+1}^{n+1}}{\Delta x} + \frac{v_{i+1,j+1,k+1}^{n+1} - v_{i+1,j,k+1}^{n+1}}{\Delta x} + \frac{w_{i+1,j+1,k+1}^{n+1} - w_{i+1,j+1,k}^{n+1}}{\Delta x} = 0$$
(15)

We can multiply by Δx on both sides.

$$u_{i+1,j+1,k+1}^{n+1} - u_{i,j+1,k+1}^{n+1} + v_{i+1,j+1,k+1}^{n+1} - v_{i+1,j,k+1}^{n+1} + w_{i+1,j+1,k+1}^{n+1} - w_{i+1,j+1,k}^{n+1} \\ = 0$$

Next, we fill in the velocities using equation 14.

$$\begin{split} \tilde{u}_{i+1,j+1,k+1} - \frac{\Delta t}{\rho \Delta x} (p'_{i+1,j,k} - p'_{i,j,k}) - \left(\tilde{u}_{i,j+1,k+1} - \frac{\Delta t}{\rho \Delta x} (p'_{i,j,k} - p'_{i-1,j,k}) \right) \\ + \tilde{v}_{i+1,j+1,k+1} - \frac{\Delta t}{\rho \Delta x} (p'_{i,j+1,k} - p'_{i,j,k}) - \left(\tilde{v}_{i+1,j,k+1} - \frac{\Delta t}{\rho \Delta x} (p'_{i,j,k} - p'_{i,j-1,k}) \right) \\ + \tilde{w}_{i+1,j+1,k+1} - \frac{\Delta t}{\rho \Delta x} (p'_{i,j,k+1} - p'_{i,j,k}) - \left(\tilde{w}_{i+1,j+1,k} - \frac{\Delta t}{\rho \Delta x} (p'_{i,j,k} - p'_{i,j,k-1}) \right) \\ = 0 \end{split}$$

We move all the pressure terms to the right hand side of the equation and keep the velocity terms at the left hand side.

$$\begin{split} \tilde{u}_{i+1,j+1,k+1} - \tilde{u}_{i,j+1,k+1} + \tilde{v}_{i+1,j+1,k+1} - \tilde{v}_{i+1,j,k+1} + \tilde{w}_{i+1,j+1,k+1} - \tilde{w}_{i+1,j+1,k} \\ &= \frac{\Delta t}{\rho \Delta x} (p'_{i+1,j,k} - p'_{i,j,k} - (p'_{i,j,k} - p'_{i-1,j,k}) \\ &+ p'_{i,j+1,k} - p'_{i,j,k} - (p'_{i,j,k} - p'_{i,j-1,k}) \\ &+ p'_{i,j,k+1} - p'_{i,j,k} - (p'_{i,j,k} - p'_{i,j,k-1})) \\ = > \tilde{u}_{i+1,j+1,k+1} - \tilde{u}_{i,j+1,k+1} + \tilde{v}_{i+1,j+1,k+1} - \tilde{v}_{i+1,j,k+1} + \tilde{w}_{i+1,j+1,k+1} - \tilde{w}_{i+1,j+1,k} \\ &= \frac{\Delta t}{\rho \Delta x} (p'_{i+1,j,k} + p'_{i-1,j,k} \\ &+ p'_{i,j+1,k} + p'_{i,j-1,k} \\ &+ p'_{i,j,k+1} + p'_{i,j,k-1} - 6p'_{i,j,k}) \end{split}$$

We assume that the pressure corrections for p other than (i,j,k) is zero. This will allow us to calculate the pressure correction in that point. [28]

$$\begin{split} \tilde{u}_{i+1,j+1,k+1} - \tilde{u}_{i,j+1,k+1} + \tilde{v}_{i+1,j+1,k+1} - \tilde{v}_{i+1,j,k+1} \\ + \tilde{w}_{i+1,j+1,k+1} - \tilde{w}_{i+1,j+1,k} &= -6 \frac{\Delta t}{\rho \Delta x} p'_{i,j,k} \\ = > p'_{i,j,k} &= -\frac{\rho \Delta x}{6 \Delta t} (\tilde{u}_{i+1,j+1,k+1} \\ &- \tilde{u}_{i,j+1,k+1} + \tilde{v}_{i+1,j+1,k+1} - \tilde{v}_{i+1,j,k+1} \\ &+ \tilde{w}_{i+1,j+1,k+1} - \tilde{w}_{i+1,j+1,k}) \end{split}$$

The above equation usually reaches convergence too slow, it should therefore be multiplied by a constant, ω_0 .

$$p'_{i,j,k} = -\omega_0 \frac{\rho \Delta x}{6\Delta t} (\tilde{u}_{i+1,j+1,k+1} - \tilde{u}_{i,j+1,k+1} + \tilde{v}_{i+1,j+1,k+1} - \tilde{v}_{i+1,j,k+1} + \tilde{v}_{i+1,j+1,k+1})$$

$$(16)$$

Even though we multiply by ω_0 , convergence is often not yet reached after one pressure correction. We therefore need to apply the pressure correction formula until convergence is reached. [28].

3.10 The algorithm

As we have just discussed we have to apply the pressure correction formula several times, the complete algoritm is: [28]

1) Initialize u^n , v^n , w^n and p^n The pressure will depend on the x-coordinate due to gravity, we will write a formula to determine the initial pressure.

- 2) Predict \tilde{u} , \tilde{v} and \tilde{w} Store the results of equation 12 in new arrays, we still want to keep the last timestep velocities.
- **3)** Update boundary conditions Implement the boundary conditions discussed in 3.3.
- 4) Calculate pressure correction(p') Store the pressure correction obtained from equation 16 in a new array.
- 5) Update velocities to the velocities of the next timestep Use equation 14 to calculate the next timestep velocities. The results can be stored in the grids from step 2, because the those results are not needed anymore.
- **6)** Update boundary conditions again The boundary conditions from 3.3 need to be applied on the new velocity grids.
- 7) Check convergence Check whether the continuity equatio (the upper equation of 5) is satisfied. If it is satisfied enough, set the velocity grids created in step 1 to the velocity grids of step 5. Also, add the pressure correction grid to the pressure grid. It is now possible to go to the next timestep. If it has not converged, only add the pressure correction grid to the pressure grid and go back to step 2. The continuity equation should converge to zero after doing steps 2 till 7 multiple times.

3.11 The code

3.11.1 Programming the algorithm

1) Initialize u^n , v^n , w^n and p^n u^n , v^n and w^n can be set to zero or an arbitraty value. It is important that the initial condition is realistic. If it is not the program will yield weird results or it will not even converge and yield nothing at all.

As we have explained in 3.4 the dimensions of a velocity grid are the pressure grid size plus two in the directions orthogonal to the direction of the velocities of that grid and the pressure grid size plus one in the parallel direction. The sizes of the pressure grid will of course be PRESSUREGRIDSIZES, a constant we defined in section 3.1. We will set the initial velocities to zero. So, in code:

```
let mut velocity_x = VelocityGrid{grid: vec![vec![vec!]
[0.0;PRESSUREGRIDSIZE[2]+2]; PRESSUREGRIDSIZE[1]+2];
PRESSUREGRIDSIZE[0]+1], dimension:0};// z,y,x !!!

let mut velocity_y = VelocityGrid{grid: vec![vec![vec!]
[0.0;PRESSUREGRIDSIZE[2]+2]; PRESSUREGRIDSIZE[1]+1];
PRESSUREGRIDSIZE[0]+2], dimension:1};

let mut velocity_z = VelocityGrid{grid: vec![vec![vec!]
[0.0;PRESSUREGRIDSIZE[2]+1]; PRESSUREGRIDSIZE[1]+2];
PRESSUREGRIDSIZE[0]+2], dimension:2};
```

Here the pressure is set to zero, which it should not be, since there is no vacuum. To determine the initial pressure we need to take gravity in account. The mass of fluid layers above a certain layer will exercise pressure on that layer. The pressure can be determined using the following formula:

$$p(h) = \frac{F}{A} = \frac{F_{atmospheric} + F_{g,water}}{A}$$
$$= \frac{F_{atmospheric}}{A} + \frac{\rho V_{water} g}{A}$$
$$= p_{atmospheric} + \rho h g$$

Where h is the height. z=0 is the bottom, so:

$$h = z_{max} - z$$

=> $p(z) = p_{atmospheric} + \rho g(z_{max} - z)$

We can use this function to create the desired pressure function:

```
fn initialize_pressure_grid(pressure_grid: &mut [[[f32;
      PRESSUREGRIDSIZE[2]]; PRESSUREGRIDSIZE[1]]; PRESSUREGRIDSIZE
      [0]]){
      for x in 0..(PRESSUREGRIDSIZE[0]-1){//velocty_grid has
      PRESSUREGRIDSIZE[dimension] elements, so loop from 0 to
      PRESSUREGRIDSIZE [dimension] -1.
          for y in 0..(PRESSUREGRIDSIZE[1]-1){
              for z in 0..(PRESSUREGRIDSIZE[2]-1){
                   //The pressure should be the atmosferic
      pressure(101,325Pa) plus the pressure that is exercised by
      the water above a point on the water at that point.
                   pressure_grid[x][y][z]=ATMOSPHERIC_PRESSURE+
      DENSITY*(PRESSUREGRIDSIZE[2] as f32 - z as f32)*
      GRIDELEMENTSCALE*EXTERNALFORCE[2];
          }
      }
10 }
```

2) Predict \tilde{u} , \tilde{v} and \tilde{w} We start with formula 12:

```
fn predict_velocity(provisonal_velocity_field: &mut
      VelocityGrid, velocity_field_last_time_step: &VelocityGrid,
       orthogonal_velocity_field_a: &VelocityGrid,
      orthogonal_velocity_field_b: &VelocityGrid, pressure_grid:
      [[[f32; PRESSUREGRIDSIZE[2]]; PRESSUREGRIDSIZE[1]];
      PRESSUREGRIDSIZE[0]]){
      let dim=get dimension(provisonal velocity field.dimension)
      for x in 1..(PRESSUREGRIDSIZE[0]-dim[0]+1) {
          for y in 1..(PRESSUREGRIDSIZE[1]-dim[1]+1) {
              for z in 1..(PRESSUREGRIDSIZE[2]-dim[2]+1) {
                   //Diffusion term
                  let diffusion=VISCOSITY*(laplacian(
      velocity_field_last_time_step, x, y, z));
                   //And finally, the provisional velocity
                   provisonal_velocity_field.grid[x][y][z]=
      velocity_field_last_time_step.grid[x][y][z]+TIMESTEPSIZE/
      DENSITY*(-convection_term(velocity_field_last_time_step,
      orthogonal_velocity_field_a, orthogonal_velocity_field_b, x
      , y, z)-first_order_central_spatial_pressure_derivative(
      pressure_grid, x-1, y-1, z-1, velocity_field_last_time_step
      .dimension)+diffusion+DENSITY*EXTERNALFORCE[
      velocity_field_last_time_step.dimension]);
              }
10
          }
11
      }
12
13
14 }
```

The function above stores the provisional velocities obtained from equation 12 in provisional_velocity_field, which is a seperate grid. The diffusion term is calculated as in chapter 3.6.

3) Update boundary conditions Ideally, the user can set the boundary conditions themselves. Although this is currently possible, it requires the user to program themselves quite a lot. We will create a few functions the user can use to set the boundary conditions.

We will enforce a no-slip boundary condition at the wall as we have discussed in section 3.3. We will first create a function that will enforce that boundary condition in the orthogonal direction.

This function will set the orthogonal boundary condition for a rectangular wall with given minimum and maximum coords. As one can see, we have use ..= instead of .. in the for loops. We have done this because we also want to set the boundary condition at the maximum coordinates(max_coords). This way, the boundary condition will also be set when one component of the minimum coordinates is equal to the same component of the maximum coordinates. The user can choose the variable value, so that he or she can create inflows and outflows by setting it to a nonzero value. When value is zero there is no flow.

We also have to enforce the boundary values in the directions parallel to the wall, again using the formulas from section 3.3. This is a little bit trickier, because we have to use neighboring points. The user will have to specify whether the given points are on the side of the wall with lower coordinates or higher coordinates.

```
1 //wall_is_on_lower_side=0 means the wall is on the side with
     lower coordinates seen from the dry side and
     wall_is_on_lower_side=1 means the wall is on the side with
     higher coordinates.
 //orthogonal_dimension is the dimension number(0 for x, 1 for
     y, 2 for z) of the dimension orthogonal to the wall
3 fn set parallel boundary condition at wall(
     parallel_velocity_grid: &mut VelocityGrid, min_coords: [
     usize; 3], max coords: [usize; 3], wall is on lower side:
     bool, orthogonal_dimension: usize){
      let dim=get_dimension(orthogonal_dimension);
      let transformation_in_one_dimension=1 - 2 * (
     wall_is_on_lower_side as isize);// -1 when a lower element
      is needed, +1 when a higher element is needed
      let transformation_to_neighbor:[isize; 3]=[(dim[0] as
      isize) * transformation_in_one_dimension, (dim[1] as isize)
      * transformation_in_one_dimension, (dim[2] as isize) *
     transformation_in_one_dimension];// This is the
     transformation to the neighbor opposite of the wall
      for x in min coords[0]..=max coords[0]{
          for y in min_coords[1]..=max_coords[1]{
              for z in min_coords[2]..=max_coords[2]{
```

```
//The parallel velocity should be the opposite
of the parallel velocity on the other side of the wall, so
that the average is zero.

parallel_velocity_grid.grid[x][y][z]=-
parallel_velocity_grid.grid[(x as isize +
transformation_to_neighbor[0])as usize][(y as isize +
transformation_to_neighbor[1]) as usize][(z as isize+
transformation_to_neighbor[2]) as usize];

}

}

}

}
```

To make using the program a little bit easier, we have created a function that sets the boundary conditions for two walls, it is explained in the comments.

```
fn set_boundary_conditions_of_two_parallel_walls(
      orthogonal_velocity_grid: &mut VelocityGrid,
      parallel_velocity_grid_a: &mut VelocityGrid,
      parallel_velocity_grid_b: &mut VelocityGrid,
      orthogonal_velocity_grid_value: f32){
      let dim= get_dimension(orthogonal_velocity_grid.dimension)
      //Set the max positions, the position coordinate
      orthogonal to the wall will be set to zero later
      let mut max_orthogonal_coords=[PRESSUREGRIDSIZE[0]+1,
      PRESSUREGRIDSIZE[1]+1, PRESSUREGRIDSIZE[2]+1];//max
      coordinates for orthogonal velocities
      let mut max_parallel_coords=PRESSUREGRIDSIZE;//Max
      coordinates for parallel velocities
      //The coordinates of one wall have coordinate zero in one
      dimension
      max_orthogonal_coords[orthogonal_velocity_grid.dimension
      ]=0;//Take the wall that has the 0 coordinate in one
      direction
      max_parallel_coords[orthogonal_velocity_grid.dimension]=0;
      // The sizes of the parallel grids are the same in the
      other dimensions, so we will loop through the same values.
      //Set boundary conditions for the zero wall
      set_orthogonal_boundary_condition_at_wall(
10
      orthogonal_velocity_grid, [0,0,0], max_orthogonal_coords,
      orthogonal_velocity_grid_value);
      set_parallel_boundary_condition_at_wall(
      parallel_velocity_grid_a, [0,0,0], max_parallel_coords,
      false, orthogonal_velocity_grid.dimension);
      set_parallel_boundary_condition_at_wall(
12
      parallel_velocity_grid_b, [0,0,0], max_parallel_coords,
```

```
false, orthogonal_velocity_grid.dimension);
      //The other wall has one coordinate at the maximum, so set
13
       that coordinate to the maximum
      max_orthogonal_coords[orthogonal_velocity_grid.dimension] =
14
      PRESSUREGRIDSIZE[orthogonal_velocity_grid.dimension];
      max_parallel_coords[orthogonal_velocity_grid.dimension] =
15
      PRESSUREGRIDSIZE[orthogonal_velocity_grid.dimension]+1;
      let minimum_parallel_coords=[(PRESSUREGRIDSIZE[0]+1)*dim
16
      [0], (PRESSUREGRIDSIZE[1]+1)*dim[1], (PRESSUREGRIDSIZE
      [2]+1)*dim[2];
      let minimum_orthogonal_coords=[PRESSUREGRIDSIZE[0]*dim[0],
17
      PRESSUREGRIDSIZE[1]*dim[1], PRESSUREGRIDSIZE[2]*dim[2]];
      //Set boundary conditions for the maximum wall
      set orthogonal boundary condition at wall(
19
      orthogonal_velocity_grid, minimum_orthogonal_coords,
      max_orthogonal_coords, orthogonal_velocity_grid_value);
      set_parallel_boundary_condition_at_wall(
      parallel_velocity_grid_a, minimum_parallel_coords,
      max_parallel_coords, true, orthogonal_velocity_grid.
      dimension);
      set_parallel_boundary_condition_at_wall(
      parallel_velocity_grid_b, minimum_parallel_coords,
      max_parallel_coords, true, orthogonal_velocity_grid.
      dimension);
22
23
24 }
```

We would like to implement more options for modifying boundary conditions in the future, for now it is beyond the scope of our project.

4) Calculate pressure correction(p') Next, we turn equation 16 into code.

5) Update velocities to the velocities of the next timestep We also write a function for equation 14. We do not need the provisional velocities anymore, so we will store the new velocities in the provisional velocity array for storage efficiency.

```
fn update_velocity_field(velocity_field: &mut VelocityGrid,
      pressure_correction : &[[[f32; PRESSUREGRIDSIZE[2]];
      PRESSUREGRIDSIZE[1]]; PRESSUREGRIDSIZE[0]]){
      let dim=get_dimension(velocity_field.dimension);
      let constant_term_velocity_equation=TIMESTEPSIZE/(DENSITY*
      GRIDELEMENTSCALE);
      for i in 1..PRESSUREGRIDSIZE[0]+1-dim[0]{
          for j in 1..PRESSUREGRIDSIZE[1]+1-dim[1]{
              for k in 1..PRESSUREGRIDSIZE[2]+1-dim[2]{
                  velocity_field.grid[i][j][k]=velocity_field.
      grid[i][j][k]-constant_term_velocity_equation*(
      pressure_correction[i+dim[0]-1][j+dim[1]-1][k+dim[2]-1]-
      pressure_correction[i-1][j-1][k-1]);
          }
9
      }
10
11 }
```

- **6)** Update boundary conditions again This is the same as step 3, it is important that the same boundary conditions are enforced
- 7) Check convergence The velocities should satisfy the continuity equation (the upper equation of 5). As we have seen the discretised version of the continuity equation is 15. Because we have discretised the equations, the continuity equation will not be completely satisfied. However, after each pressure correction the continuity equation should converge to zero a little more. We will stop correcting the pressure when the error is smaller than the constant ALLOWEDERROR. Calculating the error is very easy, since it is just the sum

of the derivatives of the velocities in their own direction. We will calulate the derivatives for a pressure point and use central derivatives, so that all three derivatives are calculable. So we first need to define that derivative:

```
fn first_order_central_spatial_derivative(f: &VelocityGrid, x:
    usize, y: usize, z:usize)->f32{//practically identical to
    first_order_forward_spatial_derivative, but for clarity we
    keep it.
let dim=get_dimension(f.dimension);
return (f.grid[x+dim[0]][y+dim[1]][z+dim[2]]-f.grid[x][y][
    z])/GRIDELEMENTSCALE;
}
```

Now we can create a function that determines whether the error is too big somewhere:

```
fn check_convergence(provisional_velocity_x:&VelocityGrid,
       provisional_velocity_y: &VelocityGrid,
       provisional_velocity_z: &VelocityGrid)->bool{
2
       for x in 0..PRESSUREGRIDSIZE[0]{
3
           for y in 0..PRESSUREGRIDSIZE[1]{
4
                for z in 0..PRESSUREGRIDSIZE[2]{
5
                    let error=
       first_order_central_spatial_derivative(&
       provisional_velocity_x, x, y, z)
                         +first_order_central_spatial_derivative(&
       provisional_velocity_y, x, y, z)
                         +first_order_central_spatial_derivative(&
       provisional_velocity_z, x, y, z);
                    if error.abs()>ALLOWEDERROR{
                         println!("Convergence_not_yet_reached,_
10
       error_{\sqcup}is_{\sqcup}\{\}_{\sqcup}at_{\sqcup}(\{\},_{\sqcup}\{\},_{\sqcup}\{\})\}, error, x, y, z);
                         return false;
12
                    }
13
                }
14
           }
15
       }
16
       return true;
17
```

3.11.2 Switching grids

We want to display the velocities on a collocated grid and not on a staggered grid, therefore we will create a function that calculates the velocities at pressure points:

```
fn get_velocity_at_pressure_point(velocity_grid: &VelocityGrid
    , x: usize, y: usize, z: usize)->f32{
    let dim= get_dimension(velocity_grid.dimension);
    return velocity_grid.grid[x+1][y+1][x+1]-velocity_grid.
        grid[x+1-dim[0]][y+1-dim[1]][z+1-dim[2]];//Just take the
        average
4 }
```

This function just takes the average of the two nearest velocity points. Using this function we can get all velocity components at every pressure point. However, if we will visualise all velocity components of a large grid we will show so much data that one can not interpret it well. Therefore, we want to be able to scale down the resolution. We will do that using the following function:

```
//Calculates the interval between the velocities that should
be shown in one dimension
fn calc_step_size(from_dimension: usize, to_dimension: usize)
    ->usize{
    return from_dimension/to_dimension;
}
```

The function divides a usize by a usize. A usize is an integer and thus Rust wants the answer to be an integer as well. Rust will therefore round it down when it is not an integer. We want this to happen because the array elements are all integers. Furthermore, when the answer is rounded down there will be no out-of-bounds errors.

We can use these functions to convert the velocities to a collocated grid and visualise them:

```
1 //min_coords and max_coords are the pressure coordinates of
     which we want to know the velocities (this function will
     determine those velocities by taking the average of nearby
     velocities)
2 //data grid point size is the size of the grid we want to show
      to the user
pub fn convert_velocities_to_collocated_grid_and_visualise(
     min_coords: [usize; 3], max_coords: [usize;3],
     data_grid_point_size: [usize; 3], velocity_grid_x: &
     VelocityGrid, velocity_grid_y: &VelocityGrid,
     velocity_grid_z: &VelocityGrid) -> Vec<Vec<[f32;3]>>>{
      let step_size=[calc_step_size(max_coords[0]-min_coords[0],
      data_grid_point_size[0]), calc_step_size(max_coords[1]-
     min_coords[1], data_grid_point_size[1]), calc_step_size(
     max_coords[2]-min_coords[2], data_grid_point_size[2])];
      let mut return_data: Vec<Vec<[f32; 3]>>>=vec![vec![
     vec![[0.0; 3]; data_grid_point_size[0]];
     data_grid_point_size[1]]; data_grid_point_size[0]];
```

```
for x in 0..data_grid_point_size[0]{
          for y in 0..data_grid_point_size[1]{
              for z in 0..data_grid_point_size[2]{
                   return_data[x][y][z]=[
      get_velocity_at_pressure_point(&velocity_grid_x, x*
      step_size[0], y*step_size[1], z*step_size[2]),
      get_velocity_at_pressure_point(&velocity_grid_y, x*
      step_size[0], y*step_size[1], z*step_size[2]),
      get_velocity_at_pressure_point(&velocity_grid_z, x*
      step_size[0], y*step_size[1], z*step_size[2])];
10
           }
11
      }
12
13
      return return_data;
14 }
```

3.11.3 Putting it all together

Using the functions from previous chapters, we can finally create a function for one timestep

${f Visualisation}$

4.1 Drawing

The way we decided to show the movement of the fluids is by drawing arrows in a space of three dimensions. We do this by first loading in the arrow from an OBJ file. and OBJ file is the simplest way of storing three dimensional objects. We define the center of the arrow as (0,0,0). This makes rotation and translation easier. We also make sure that by default the arrow position is up, giving us the vector $\vec{v} = (0,0,1)$. We then create multiple instances of that arrow which we multiply with a quaternion that is the cross product of the desired rotation and the neutral rotation and we set the scalar equal to the distance between the endpoints of the vectors with the origin as a starting point. finally we transform the arrow by a vector $\vec{x} = (x, y, z)$, giving us the following transformation:

the arrow by a vector
$$x=(x,y,z)$$
, giving us the following transformation:
$$\begin{bmatrix} 1 & 0 & 0 & 0 \\ 0 & 1 & 0 & 0 \\ 0 & 0 & 1 & 0 \\ x & y & z & 1 \end{bmatrix}.$$
 Due to the z-component in compute graphics being defined

as the distance from the screen and the height as the y-component, we also

need to switch the z and y-components.
$$\begin{bmatrix} 1 & 0 & 0 & 0 \\ 0 & 0 & 1 & 0 \\ 0 & 1 & 0 & 0 \\ x & y & z & 1 \end{bmatrix}$$
 The finally multiplication

as the distance from the screen and the height as the y-component, we also need to switch the z and y-components.
$$\begin{bmatrix} 1 & 0 & 0 & 0 \\ 0 & 0 & 1 & 0 \\ 0 & 1 & 0 & 0 \\ x & y & z & 1 \end{bmatrix}$$
 The finally multiplication matrix then becomes:
$$\begin{bmatrix} d & 0 & y & -x \\ 0 & d & x & y \\ -y & -x & d & 0 \\ -y & -x & d & 0 \\ xd - zy + x & yd - zx - y & 2xy + zd & -x^2 + y^2 + d \end{bmatrix}$$
 where $d = ||\vec{x} - \vec{v}||.[32]$

4.2 Data capturing

In order to actually show the data, we need to draw the arrows by defining the vertices that make up the arrows. We then multiply it with the transformation matrix from the previous chapter and finally with a standard camera matrix. [33] Then to get the final image we create a lot of instances of that arrow that are rotated and translated with the transformation matrix of the previous chapter. We finally define a grid by drawing lines with a start and endpoint multiplied with the camera matrix giving us something like this:

5 Conclusion

References

- [1] https://resources.pcb.cadence.com/blog/ 2020-cfd-simulation-types-discretization-approximation-and-algorithms
- [2] https://www.manchestercfd.co.uk/post/what-is-discretization
- [3] https://www.britannica.com/science/difference-equation
- [4] https://courses.engr.illinois.edu/cs357/fa2019/assets/lectures/Lecture8-Sept19.pdf
- [5] https://web.iit.edu/sites/web/files/departments/ academic-affairs/academic-resource-center/pdfs/Navier_Stokes. pdf
- [6] https://www.dive-solutions.de/articles/cfd-methods
- [7] https://arxiv.org/pdf/cs/0501021.pdf
- [8] https://brilliant.org/wiki/taylor-series-approximation/
- [9] https://www.quantstart.com/articles/Derivative-Approximation-via-Finite-Difference-Metho
- [10] https://math.stackexchange.com/questions/501735/why-do-we-use-big-oh-in-taylor-series
- [11] https://maxwell.ict.griffith.edu.au/jl/Chapter5.pdf
- [12] https://pure.tue.nl/ws/files/3372975/696955.pdf
- $[13] \ \mathtt{https://www.comsol.com/multiphysics/finite-element-method}$
- [14] https://link.springer.com/chapter/10.1007% 2F978-3-319-16874-6_19
- [15] http://www.fem.unicamp.br/~phoenics/SITE_PHOENICS/Apostilas/CFD-1_U%20Michigan_Hong/Lecture13.pdf
- [16] https://www.quora.com/What-is-the-physics-behind-no-slip-condition-in-fluid-mechanics
- [17] https://physics.stackexchange.com/questions/383096/understanding-free-slip-boundary-condition
- [18] https://www.tec-science.com/mechanics/gases-and-liquids/derivation-of-the-navier-stokes-equations/
- [19] https://www.paramvisions.com/2021/04/ what-is-normal-stress-shear-stress.html
- [20] http://ingforum.haninge.kth.se/armin/fluid/exer/deriv_navier_stokes.pdf

- [21] https://projects.iq.harvard.edu/files/ac274_2015/files/lecture2_3.pdf
- [22] https://physics.info/viscosity/
- [23] https://www.tec-science.com/thermodynamics/thermodynamic-processes-in-closed-systems/what-is-meant-by-dissipation-of-energy/
- [24] https://www.simscale.com/blog/2017/12/turbulence-cfd-analysis/
- [25] http://www.nzdl.org/cgi-bin/library?e= d-00000-00--off-0hdl--00-0--0-10-0--0-direct-10---4-----0-11--11-en-50---20-cl=CL1.11&d=HASH011f05bf8734d88d1a080257.12.1>=1
- [26] https://www.grc.nasa.gov/WWW/k-12/airplane/nseqs.html
- [27] https://www.youtube.com/watch?v=Kf_RHzaqFBc
- [28] https://www.youtube.com/watch?v=OqtvRjuTihY
- [29] https://enterfea.com/implicit-vs-explicit/
- [30] https://vulkan-tutorial.com/
- [31] http://thevisualroom.com/marker_and_cell_method.html
- [32] https://stackoverflow.com/questions/1171849/ finding-quaternion-representing-the-rotation-from-one-vector-to-another
- [33] https://www.youtube.com/watch?v=x_Ph2cuEWrE