

MATTERIX: toward a digital twin for robotics-assisted chemistry laboratory automation

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1542 **Supplementary Section 1 Assets Description**

1543

1544 **Supplementary Section 1.1 Materials**

1545 MATTERIX supports solids and fluids using position-
1546 based-dynamics (PBD) particle simulation.

1547 **Supplementary Section 1.2 Glassware**

1548 MATTERIX has different glassware available and
1549 readily-used in our environments. These include beakers,
1550 graduated cylinders, reagent bottles, funnels, test tubes
1551 and vials.

1552 **Supplementary Section 1.2.1 Laboratory Tools**

1553 *Digital Pipette*: This can be integrated with a robot arm
1554 to facilitate the processing of pipetting fluids through its
1555 digital interface.

1556 *Spatulas*: Human scientists weigh samples (materials)
1557 using a spatula and balance. The spatula used in our
1558 environment has been demonstrated to autonomously
1559 weigh different solid materials in our previous works⁵⁹.

1560 **Supplementary Section 1.3 Laboratory Instruments**

1561 *Hot plate, stirrer, and balance*: A key instrument is a
1562 hot plate, balance, and stirrer, where for this setup we
1563 used the IKA RCT Digital hot plate and stirrer, which has
1564 been used in our previous works for solubility screening
1565 and crystallisation^{60,61}.

1566 *Syringe pump*: Syringe pumps are commonly used for
1567 precise and reliable liquid handling. In our work, we have
1568 used the Tecan Cavro pumps.

1569 **Supplementary Section 1.4 Automation Platforms**

1570 *Opentrons*: OT-2 is an open-source bench-top liquid
1571 handler.

1572 **Supplementary Section 1.4.1 Robots**

1573 *KUKA KMR iiwa*: is a mobile manipulator with a 7
1574 DoF arm that has been used in different material discov-
1575 ery experiments including the mobile robotic chemist for
1576 photocatalysis⁶ and the multi-robot system for solid-state
1577 chemistry⁷.

1578 *Franka Emika Panda*: The Franka Emika Panda arm
1579 robot, equipped with either a Franka Emika Panda Hand
1580 or a Robotiq 2F-85 gripper was used as the main ma-
1581 nipulator in the environment since it has already been
1582 demonstrated as a robotic chemist across different work-
1583 flows^{5,62}. To facilitate grasping objects from the side
1584 in tabletop scenarios and enhance constrained motion

planning in some of the environments, we positioned the
Robotiq 2F-85 end-effector parallel to the ground on the
robot's last link. This configuration was attained either
through a fixed linkage or by incorporating a Dynamixel
XM540-W150 servo motor as an additional degree of
freedom.

1591 **Supplementary Section 2 Chemistry Lab
1592 Simulated Environments**

1593 The videos of all the environment are provided on the
1594 project website at:
[https://accelerationconsortium.github.io/
1595 Matterix/](https://accelerationconsortium.github.io/Matterix/).

1596 **Beaker Placement in Fumehood with Franka Emika
1597 Panda 8 DoF robot arm and Robotiq gripper**:

1598 The Franka Emika Panda 8 DoF robot arm, equipped with a
1599 Robotiq gripper, is precisely manoeuvring a beaker within
1600 the confines of a fumehood. The robot is executing a con-
1601 trolled placement of the beaker, demonstrating its abil-
1602 ity to handle laboratory equipment in a potentially haz-
1603 ardous environment. An example reaching task using
1604 the cuRobo motion planner with collision avoidance is
1605 demonstrated as well.

1606 **Beaker Placement in OT2 with Franka Emika Panda
1607 8 DoF robot arm and Robotiq gripper**:

1608 The Franka Emika Panda robot with its Robotiq gripper is executing a
1609 precise placement of a beaker within the OT2 liquid han-
1610 dling platform's workspace.

1611 **Funnel Pick and Place with Franka Emika Panda 8
1612 DoF robot arm and Robotiq gripper**:

1613 The Franka Emika Panda with its Robotiq gripper, is performing a pick-and-
1614 place operation with a funnel. This involves grasping the
1615 funnel, transporting it, and accurately positioning it in a
1616 new location.

1617 **KUKA KMR IIWA Pick and Place Beaker**:

1618 The mobile KUKA KMR IIWA robot is autonomously transporting
1619 a beaker between different locations in a representative
1620 lab.

1621 **Liquid Dispensing Station**:

1622 The robot arm (Franka
1623 Emika Panda) sets up the OT-2 workstation by placing
1624 the dispensing rack, tips rack, and reservoir well in the
1625 tray. Following this, the OT-2 head connects the pipettes
1626 and begins the fluid dispensing process.

1627 **Franka Emika Panda (8DoF with Robotiq gripper)**

1628 **Pick and Place Beaker on Scale**: The robot arm is ac-
1629 curately placing a beaker onto the scale, for weighing its
1630 contents.

1631 **Franka Emika Panda (8DoF with Robotiq gripper)**

1632 **Pour Fluid**: The robot is precisely pouring a liquid from
1633 one container to another.

1634 **Franka Emika Panda Pick and Place Vial Rack**: The

1635 robot arm is transporting the racks of vials between dif-
1636 ferent locations.

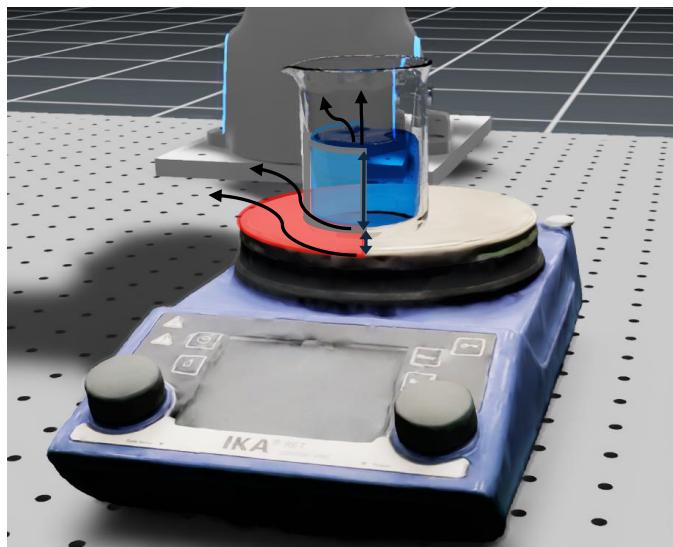
1637 **Franka Emika Panda (8DoF with Robotiq gripper)/Franka Emika Panda Vial Insertion:** The robot arm
1638 is picking up a vial and inserting it in the rack.
1639

1640 **Franka Emika Panda Wellplate Insertion in OT2:** The robot arm is picking up the wellplate and inserting
1641 it in the rack locations on the OT2.
1642

1643 Detailed instructions and tutorials for running MAT-
1644 TERIX are available on the project website and repository.
1645 We encourage readers to review them.

1646 Supplementary Section 3 Heat Transfer Se- 1647 mantics EngineExample

1648 Thermal analysis is crucial in laboratory systems to
1649 ensure experimental accuracy and optimize energy effi-
1650 ciency. Here, we develop a thermal model for a solution-
1651 beaker-heater system as an example, applying an energy
1652 balance approach to predict temperature variations in dif-
1653 ferent components over time. This approach is generic
1654 and could be applied to different laboratory components.



Supplementary Figure Supplementary Figure 1 : Heat transfer between the heater, beaker, and solution. The IKA RET control device heats the beaker through conduction, which then transfers heat to the solution. Heat exchange is bidirectional, flowing from hotter to cooler objects until equilibrium is reached. Curved arrows indicate heat dissipation to the ambient air.

1655 **System Overview** The system consists of three inter-
1656 connected thermal components:

- **IKA Heater:** A solid heating element providing heat input. 1657
1658

- **Beaker:** A glass container facilitating heat transfer 1659
1660 between the heater and the liquid.

- **Solution:** A liquid medium subjected to thermal in-
1661
1662 teractions with the beaker and ambient air.

Heat transfer in the system occurs primarily through con-
1663
1664 duction and convection.

Heat Transfer Mechanisms A uniform temperature
1665 distribution within each component is assumed in MAT-
1666 TERIX. Each component exchanges heat through differ-
1667 ent pathways, as shown in [Supplementary Figure 1](#). Dif-
1668 ferent pathways are described below:
1669

- IKA Heater
1670

- Conductive heat transfer to the Beaker: \dot{q}_{hb}
1671
- Convective heat loss to the surrounding Air: \dot{q}_{ha}
1672
- Internal heat generation: \dot{q}_{gen}
1673

- Beaker
1674

- Conductive heat transfer from the IKA Heater:
 \dot{q}_{hb}
1675
- Conductive heat transfer to the Solution: \dot{q}_{bs}
1677
- Convective heat loss to the Air: \dot{q}_{ba}
1678

- Solution
1679

- Conductive heat transfer from the Beaker: \dot{q}_{bs}
1680
- Convective heat loss to the Air: \dot{q}_{sa}
1681

Energy Balance Equations Applying the first law of
1682 thermodynamics, we obtain the governing equations:
1683

1684 IKA Heater

$$m_h C_h \frac{dT_h}{dt} = \dot{q}_{gen} - \dot{q}_{hb} - \dot{q}_{ha} \quad (7)$$

where:
1685

$$\dot{q}_{hb} = \frac{k_b A_b}{d_b} (T_h - T_b) \quad (8)$$

$$\dot{q}_{ha} = h_a A_h (T_h - T_a) \quad (9)$$

The term \dot{q}_{gen} represents the heat generated internally
1687 within the IKA heater due to electrical power input. Gen-
1688 erally, the heater can be assumed to behave as a purely
1689 resistive element, the heat generation follows Joule's Law
1690 ($V^2/R = RI^2$, where V is voltage, I is current, and R is the
1691 resistance). However, in our case, we are mainly facing
1692

1693 a temperature-controlled heating, where the heater ad-
 1694 justs its heat generation to maintain a target temperature.
 1695 Therefore, instead assuming a constant electrical power
 1696 supply, \dot{q}_{gen} depend on the heater temperature using a
 1697 proportional control system, where the heater generates
 1698 heat depending on the difference between its current tem-
 1699 perature, (T_h), and the target temperature, (T_{target}):

$$\dot{q}_{\text{gen}} = K_{\text{gen}}(T_{\text{target}} - T_h) \quad (10)$$

1700 Equation 7 describes the energy balance for the heater,
 1701 where the generated heat (\dot{q}_{gen}) is partially transferred to
 1702 the beaker via conduction (\dot{q}_{hb}) and lost to the ambient
 1703 through convection (\dot{q}_{ha}).

Beaker

$$m_b C_b \frac{dT_b}{dt} = \dot{q}_{hb} - \dot{q}_{bs} - \dot{q}_{ba} \quad (11)$$

1705 where:

$$\dot{q}_{bs} = \frac{k_b A_b}{d_b} (T_b - T_s) \quad (12)$$

$$\dot{q}_{ba} = h_b A_b (T_b - T_a) \quad (13)$$

Solution

$$m_s C_s \frac{dT_s}{dt} = \dot{q}_{bs} - \dot{q}_{sa} \quad (14)$$

1708 where:

$$\dot{q}_{sa} = h_s A_s (T_s - T_a) \quad (15)$$

Parameter Definitions

- m (kg): Mass of the component
- C (J/kg · K): Specific heat capacity
- T (K): Temperature
- T_h (K): Heater temperature
- T_b (K): Beaker temperature
- T_a (K): Ambient temperature
- k (W/m · K): Thermal conductivity
- A (m²): Heat transfer area
- d (m): Thickness of conductive medium
- h (W/m² · K): Convective heat transfer coefficient
- \dot{q} (W): Heat transfer rate
- V (V): Voltage applied across the heater
- R (Ω): Electrical resistance of the heater
- I (A): Current flowing through the heater

- K_{gen} (W/K): Proportional control gain, which deter-
 1724
 1725
 1726

- T_{target} (K): Target temperature of the IKA heater

Uniform Temperature Distribution Assumption The model employed in this work assumes a uniform temperature distribution within each component, meaning that no internal temperature gradients exist. This assumption is valid when the Biot number (Bi) is sufficiently small, indicating that internal conductive resistance is much lower than surface convective resistance⁶³. The Biot number is defined as:

$$Bi = \frac{hL_c}{k} \quad (16)$$

where, h is the convective heat transfer coefficient of the surrounding fluid (W/m² · K), k is the thermal conductivity of the material (W/m · K), and L_c is the characteristic length (m), given by:

$$L_c = \frac{\mathcal{V}}{A} \quad (17)$$

where, \mathcal{V} and A represent the volume and surface area of the object, respectively.

Although the Biot number in this study may exceed the typical threshold (0.1) depending on the object carried by the robotic system, assuming a uniform temperature distribution remains a practical simplification. This approach allows for an efficient thermal analysis that can be integrated into the MATTERIX to predict the temperature variations effectively.

In addition, it is worth mentioning that to determine whether heat transfer inside the solution is dominated by convection or conduction, we can use the Rayleigh number (Ra)^{63,64}. The Rayleigh number helps predict whether buoyancy-driven fluid motion (natural convection) occurs. It is defined as follow:

$$Ra = Gr \cdot Pr \quad (18)$$

where:

- Gr is the Grashof number, representing the ratio of buoyancy to viscous forces.
- Pr is the Prandtl number, representing the ratio of momentum diffusivity to thermal diffusivity.

The Grashof number is given by:

$$Gr = \frac{g\beta(T_{\text{hot}} - T_{\text{cold}})L^3}{v^2}$$

where:

- 1762 • g = gravitational acceleration (9.81 m/s^2),
 1763 • β = thermal expansion coefficient of the liquid ($1/K$),
 1764 • $T_{\text{hot}} - T_{\text{cold}}$ = temperature difference in the liquid,
 1765 • L = characteristic length (for example, height of the
 1766 liquid column),
 1767 • ν = kinematic viscosity of the liquid (m^2/s).

1768 The Prandtl number is given by:

$$Pr = \frac{\nu}{\alpha}$$

1769 where:

- 1770 • α = thermal diffusivity (m^2/s),
 1771 • ν = kinematic viscosity (m^2/s).

1772 The interpretation of the Rayleigh number is as follow:

- 1773 • If $Ra \gg 10^4$ (high Ra) \Rightarrow Convection dominates
 1774 (buoyancy-driven fluid motion).
 1775 • If $Ra \ll 10^4$ (low Ra) \Rightarrow Conduction dominates (the
 1776 liquid remains mostly still).
 1777 • If $Ra \approx 10^4$ \Rightarrow Transition region where both conduc-
 1778 tion and convection occur.

1779 This work establishes an energy balance framework for
 1780 multi-object systems, providing heat transfer equations
 1781 for analysis and simulation integrated with chemistry and
 1782 object manipulation. Future work may involve online iden-
 1783 tification of heat transfer constants using IoT sensors to
 1784 align simulations with real-world results.

1785 Supplementary Section 4 Physics and Se- 1786 mantics Engine Algorithm

1787 **Supplementary Algorithm 1** describes the integration of
 1788 the Physics and Semantics engines. At each simulation
 1789 step, we first pass the current physical states x_t and ac-
 1790 tions a_t to the physics engine to compute the next physics
 1791 state. Next, we iterate over all the semantics processes
 1792 and events to estimate the next semantic states s_{t+1} and
 1793 l_{t+1} . Additionally, events can influence the behaviours of
 1794 both the physics and semantics.

Algorithm Supplementary Algorithm 1

PHYSICS&SEMANTICSENGINE()

```

Input:  $x_0, s_0, l_0, a_t$ 
Output:  $x_{t+1}, s_{t+1}, l_{t+1}$ 
1: for all  $t \in \mathcal{T}$  do
2:    $x_{t+1} \leftarrow F_t(x_t, a_t)$                                  $\triangleright$  physics engine
3:    $s_{t+1} \leftarrow P_t(x_{t+1}, s_t, l_t, a_t)$                  $\triangleright$  semantic processes
4:    $l_{t+1}, F_{t+1}, P_{t+1} \leftarrow E(x_{t+1}, s_{t+1}, l_t, a_t)$      $\triangleright$  semantic events
  
```

Supplementary Section 5 Chemistry Experiment Workflows

1795 **Supplementary Figure 2** illustrates the hierarchical
 1796 state machine used to run multi-scale chemistry simula-
 1797 tions. **Supplementary Figure 2.A** shows the state ma-
 1798 chine that executes the organic chemistry experiment
 1799 presented in **Figure 5.A**, controlling both the heater and
 1800 the robot. **Supplementary Figure 2.B** shows the state
 1801 machine for the two-step reduction-oxidation chemistry
 1802 experiment presented in **Figure 5.B**. The robot begins by
 1803 pouring the solution from the first beaker into the third,
 1804 followed by the solution from the second beaker, mixing
 1805 all three solutions in the third beaker. In both workflows,
 1806 the robot's motion is calculated using inverse kinematics.
 1807

1808 **Supplementary Figure 3** presents the results of the or-
 1809 ganic chemistry experiment conducted with the IKA plate
 1810 heater set to a target temperature of 40°C . As shown
 1811 in the figure, the solution temperature remains close to
 1812 35°C , resulting in a relatively slow rate for the organic re-
 1813 action.
 1814

Supplementary Section 6 Deployment of Digital Twin Workflows to Real Setup

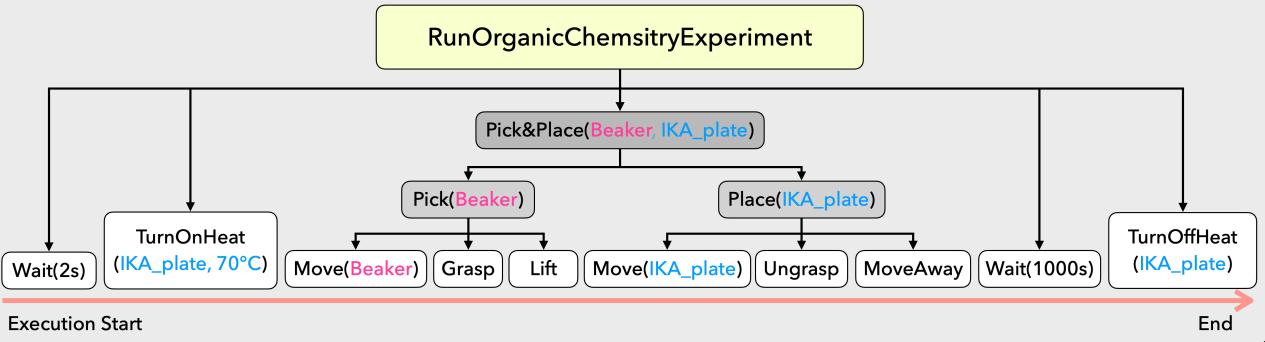
1815 The videos of the deployment of digital twin workflows
 1816 to the real setup are provided on the project website at:
 1817 [https://accelerationconsortium.github.io/
 Matterix/](https://accelerationconsortium.github.io/Matterix/).

1818 **Robot Pouring Liquid from a beaker to another:** The
 1819 Franka Emika Panda 7 DoF robot arm, equipped with a
 1820 Robotiq gripper, is transfers liquids during a pouring task
 1821 (related to **Figure 6.B**).
 1822

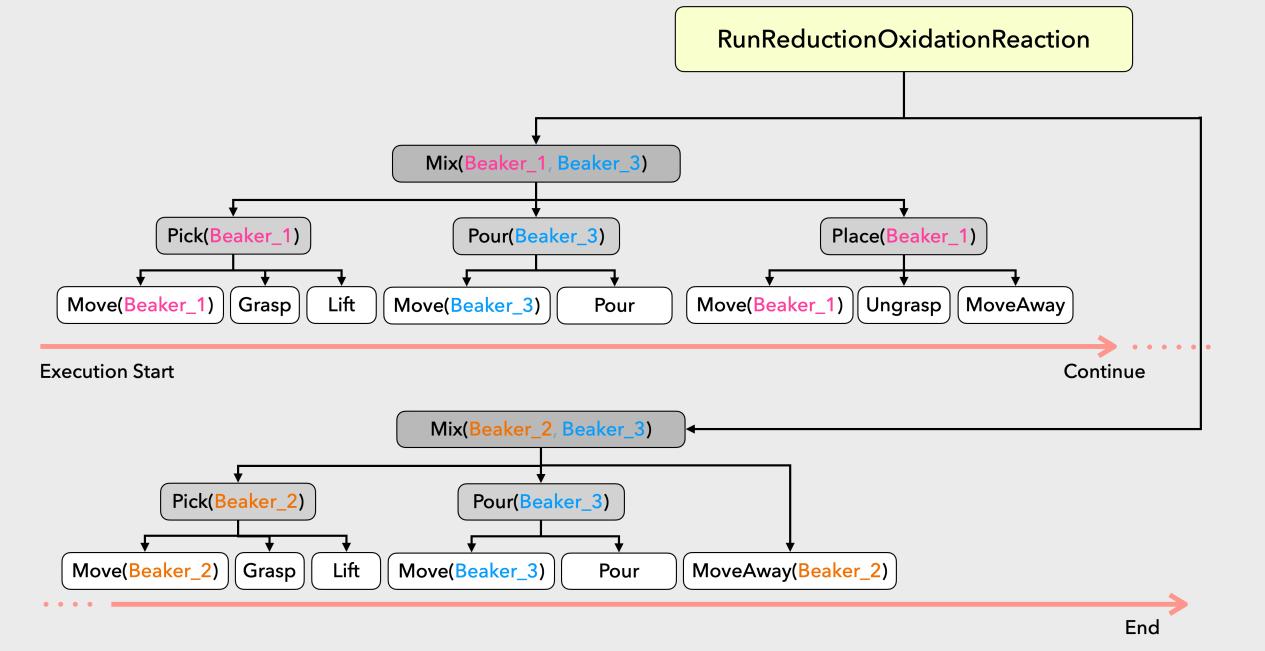
1823 **Liquid Handing Station with Opentrons and Franka
 1824 Arm:** The Franka Research 3 (FR3) robot arm setups
 1825 the Opentrons liquid hanlder in a real-world chemistry lab
 1826 (related to **Figure 6.C**).
 1827

1828 **Multi-step Reduction-Oxidation Chemistry Experi-
 1829 ment:** The Franka Panda arm (FR3) robot arm equipped
 1830 with a Robotiq gripper runs a two-step reduction-oxidation
 1831 chemistry experiment (related to **Figure 5.B**).
 1832

A. Organic Chemistry Experiment

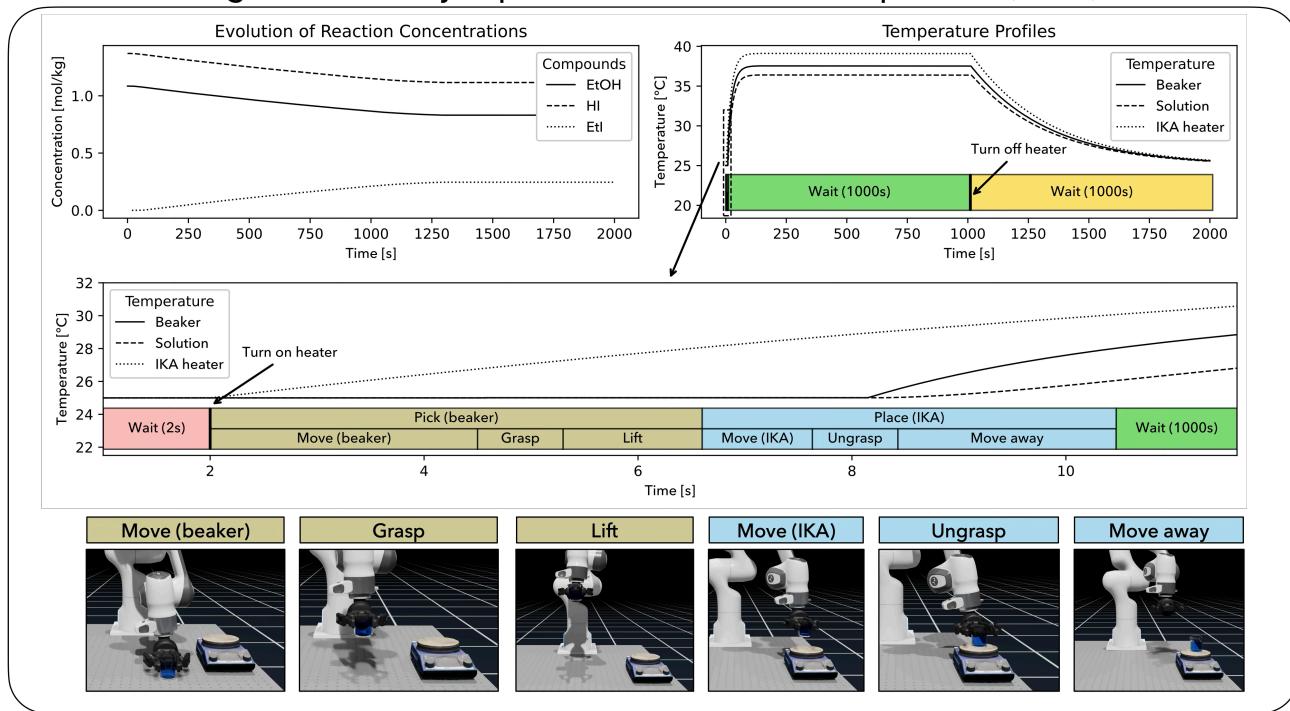


B. Multi-step Reduction-oxidation Reaction



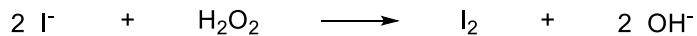
Supplementary Figure 2 : Visualization of hierarchical state machine for different chemistry experiments. (A) demonstrates the workflow of the organic chemistry experiment as shown in Figure 5.A. (B) demonstrates the workflow of the multi-step reduction-oxidation reaction as shown in Figure 5.B.

Organic Chemistry Experiment – Alternative temperature (40°C)

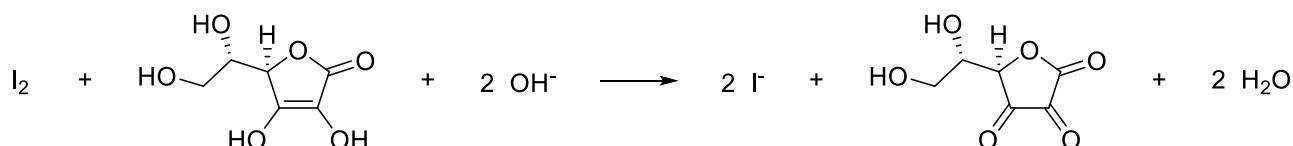


Supplementary Figure 3 : Multi-scale simulation of an organic chemistry experiment. A single-step organic chemistry experiment demonstrating the interaction of physical manipulation, heat transfer, and chemical kinetics simulation. The target temperature for the IKA plate heater is set to 40°C. Compared to Figure 5.A, the reaction proceeds at a slower rate at 40°C.

Step 1



Step 2



Supplementary Figure 4 : Reaction equations of two step organic-inorganic redox-oxidation experiment. (Step 1) Oxidation of iodide to elementary iodine with hydrogen peroxide, reflected by the dark color of the iodine-starch complex. (Step 2) Reduction of iodine with ascorbic acid (Vitamin C), reflected by the diminishing of the iodine-starch dark color.