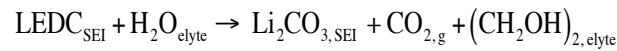
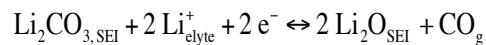
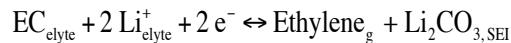
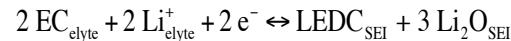
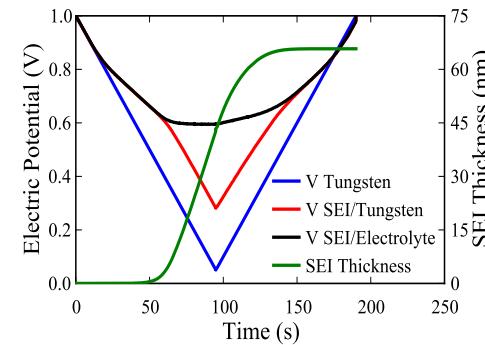


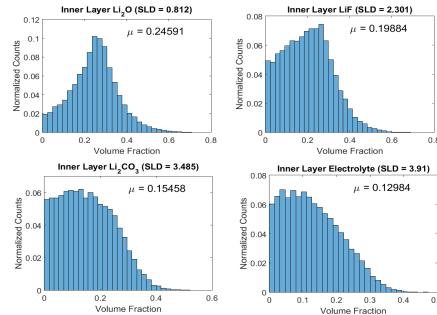
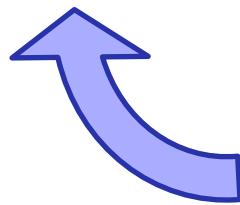
Detailed Chemistry Modeling via Cantera: A Pathway to Understand Li-ion Battery Degradation



Detailed SEI Chemistry



Numerical Simulation



SEI Chemical Composition



Steven C. DeCaluwe

Colorado School of Mines, Mechanical Engineering, Golden, CO

Presented at ECS Data Science Showcase
Monday, 01 October, 2018



Acknowledgements

Colorado School of Mines

At Colorado School of Mines:

- Christopher H. Lee (MS, 2016)
- Daniel Korff (Current PhD Student)
- Amy LeBar (Current MS Student)
- Center for High Performance Computing

At the NCNR:

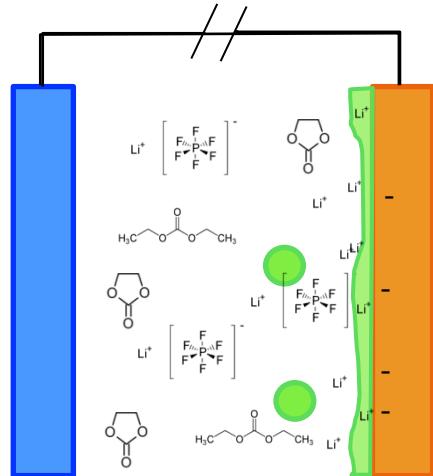
- Joseph A. Dura, Eric D. Rus – Neutron Reflectometry
- Paul Kienzle – Refl1D Fitting software

Financial Support

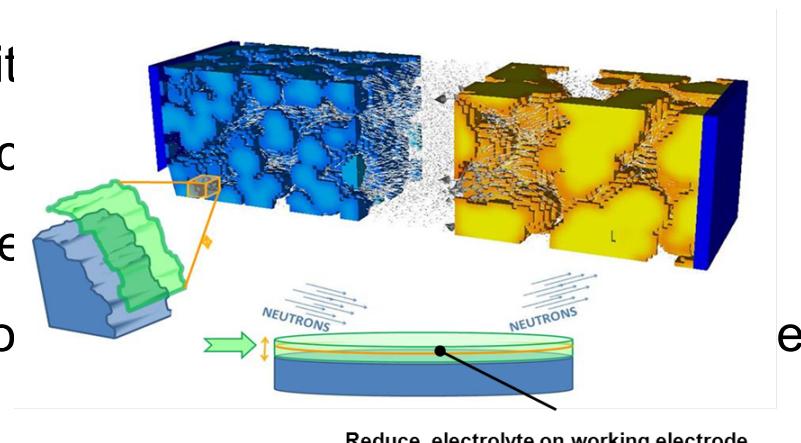
- **US Office of Naval Research, Award#: N00014-14-1-0059 (Program Manager: Dr. Michele Anderson).**
- **Dept. of Energy BES, Early Career, Award # DE-SC0018019 (Program Manager: Dr. Pappan Thiagarajan).**
- **State of Colorado Energy Research Collaboratory, Seed Grant (Program contact: Maury Dobbie)**

Lithium batteries: promise, challenges, and the SEI (2)

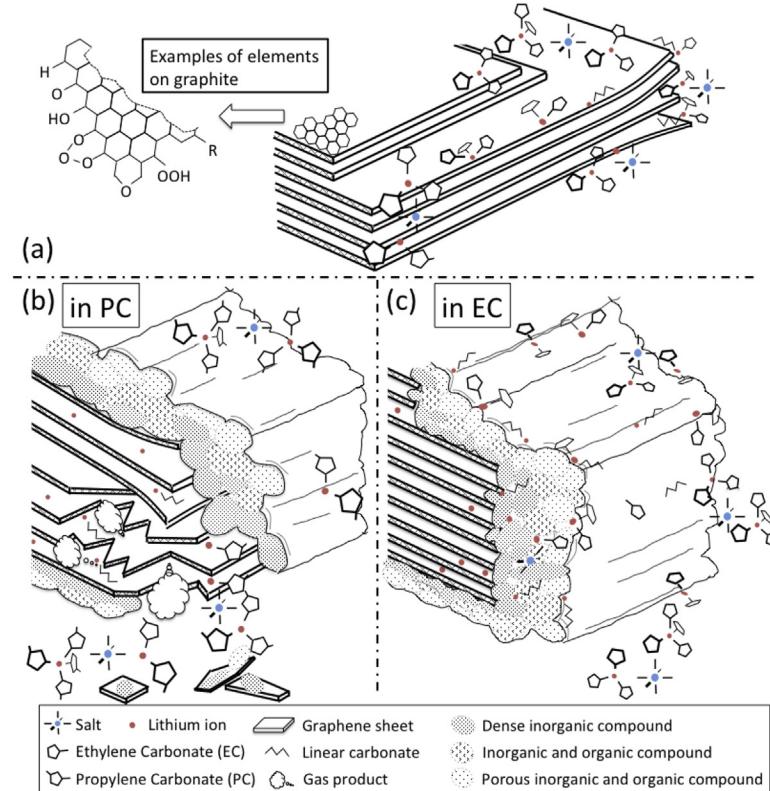
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- Because the electrolyte breaks down at the bare anode, LIBs cannot operate without a passivation layer.
 - Electrolyte formulations create a passivating film from the decomposition products: Solid Electrolyte Interphase (SEI).
 - In reality, continued SEI growth during battery operation degrades device durability and efficiency on conductivit
 - Long-term capacity fading due to Li⁺ c
 - Durability and safety issues – SEI de
 - Higher resistance, lower power – slo
- interface.



State of SEI Understanding (1)



An, et al., *Carbon* (2016)

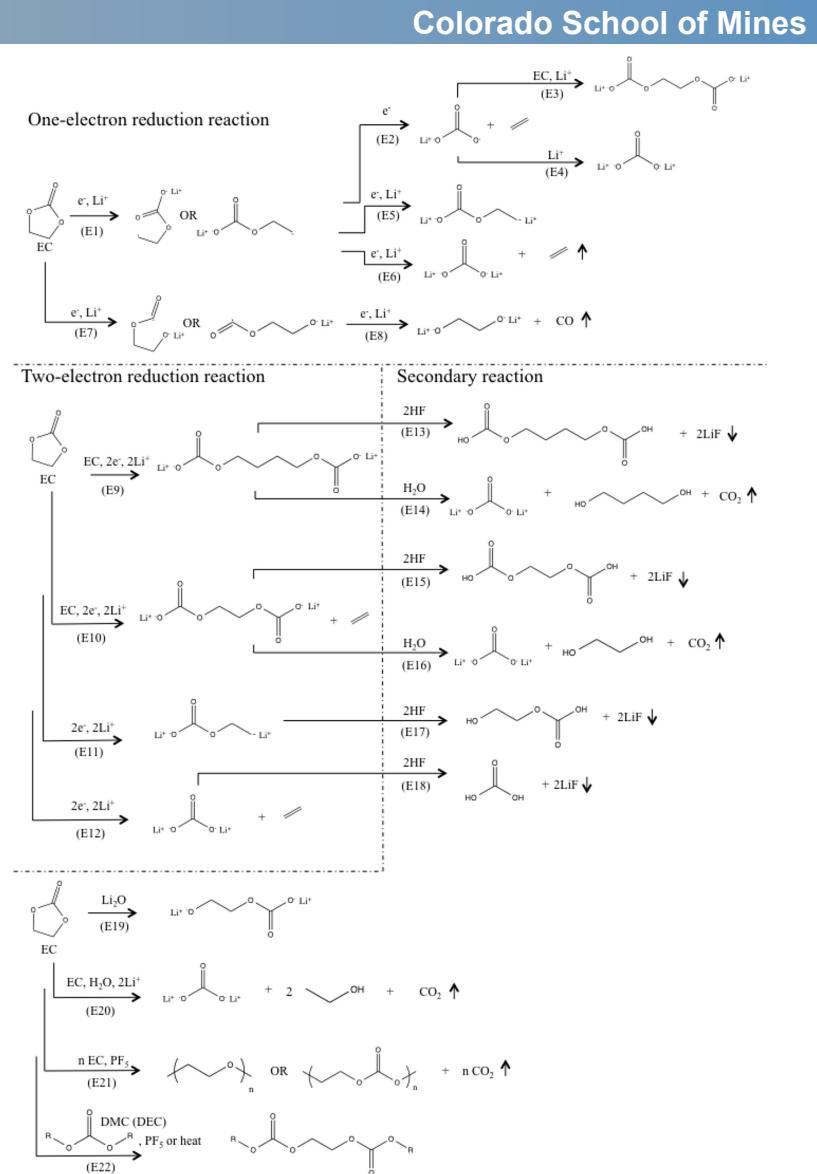
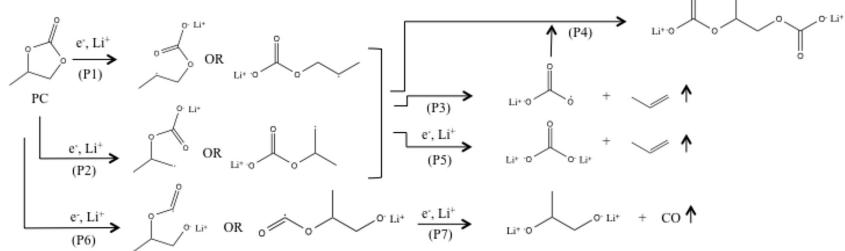


Fig. 8. Ethylene carbonate (EC) reduction process (reference groups in parentheses; details are shown in Table 2).

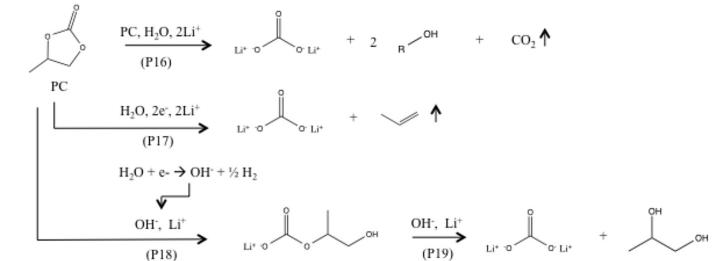
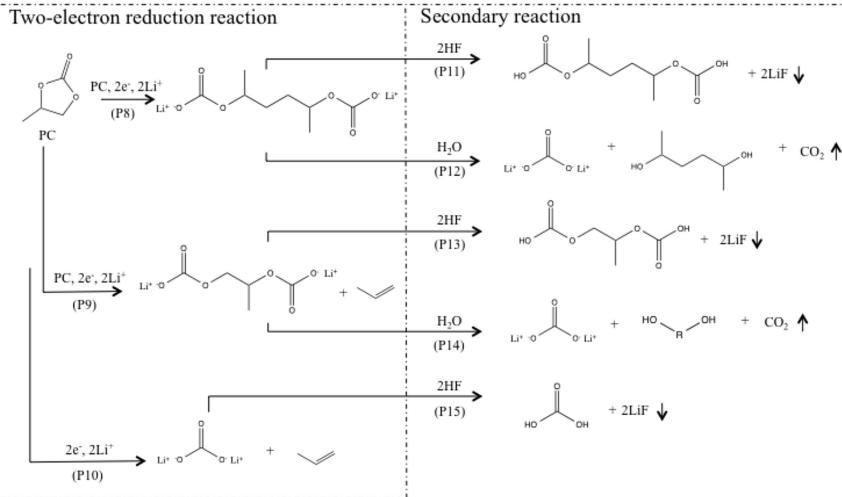
State of SEI Understanding (2)

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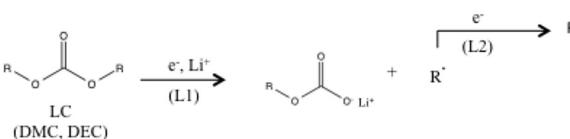
One-electron reduction reaction



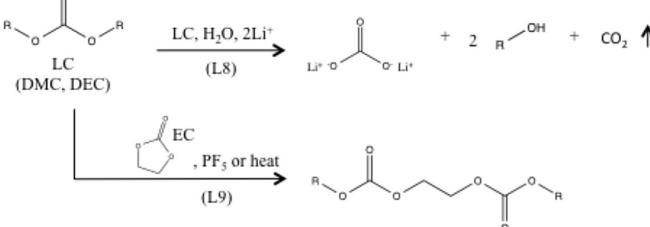
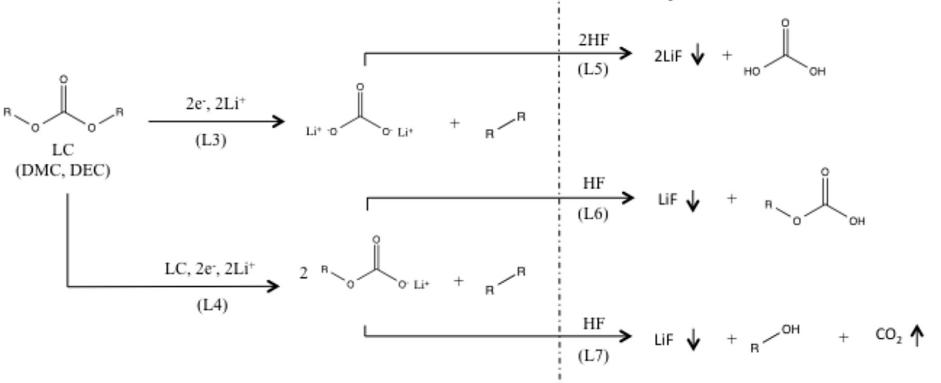
Two-electron reduction reaction



One-electron reduction reaction



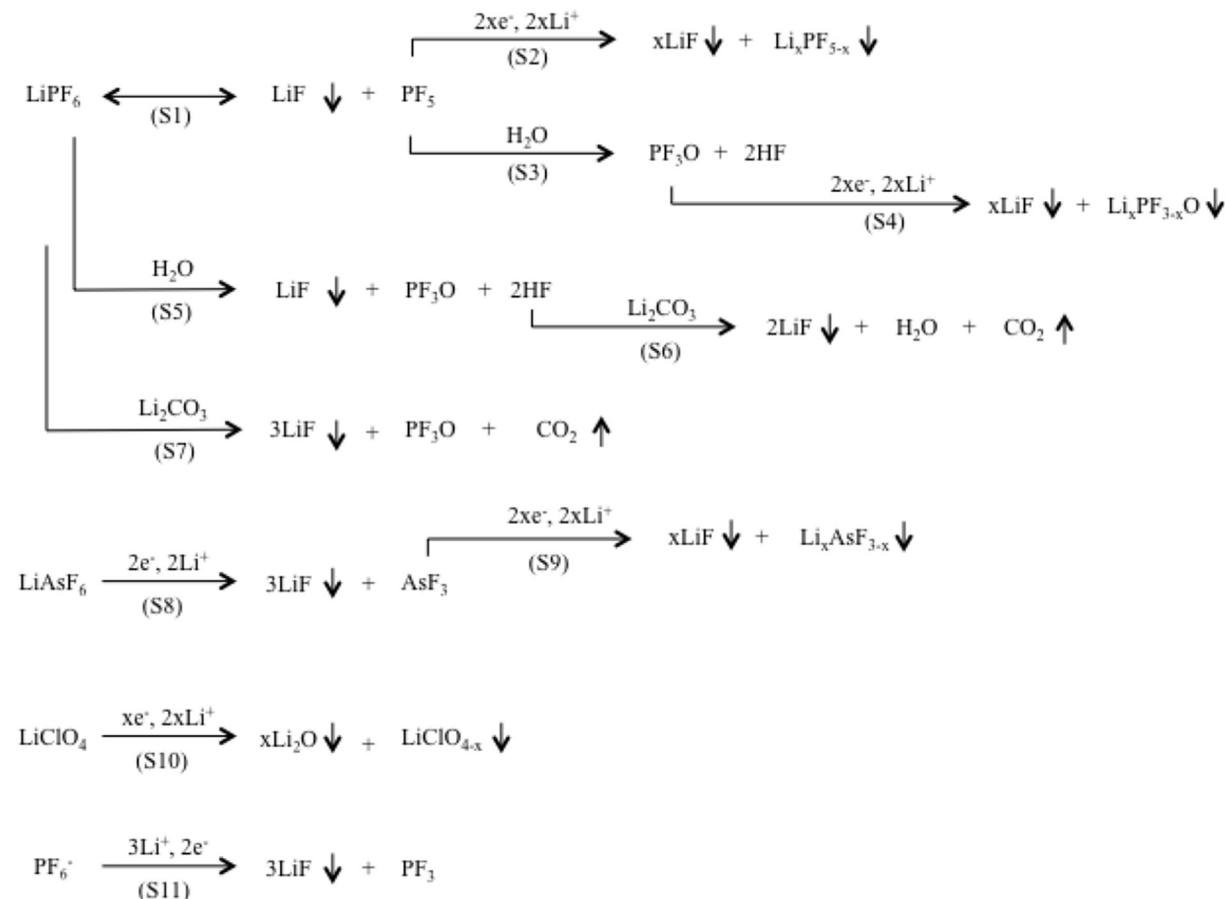
Two-electron reduction reaction



An, et al., Carbon (2016)

State of SEI Understanding (3)

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An, et al., *Carbon* (2016)

Outline

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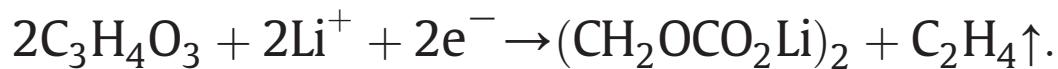
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Tanaka and Bessler

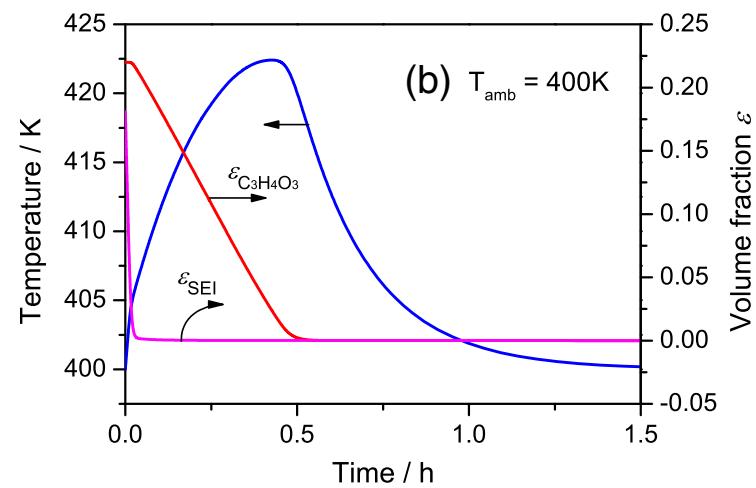
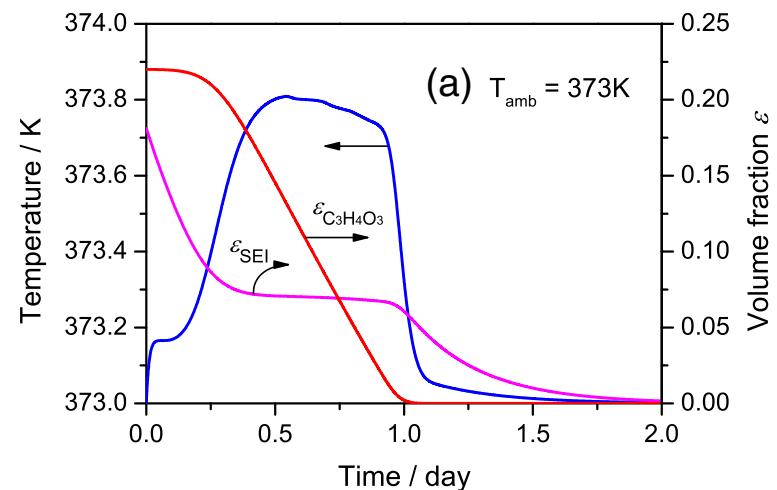
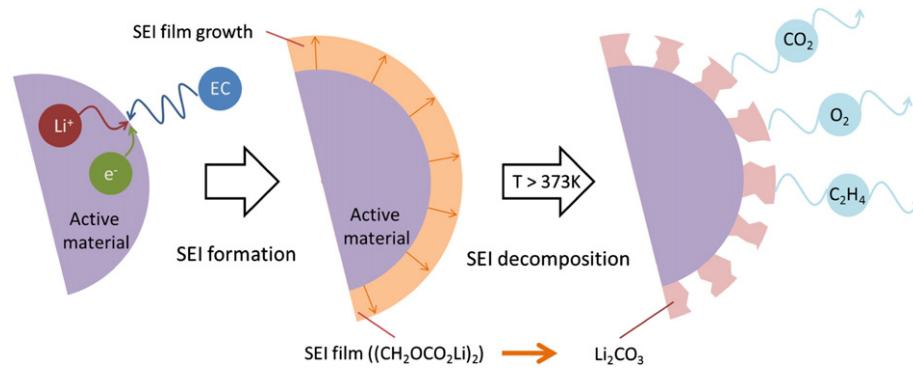
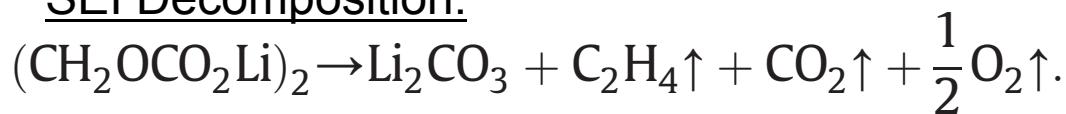
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(Solid State Ionics, 2014)

SEI Growth:

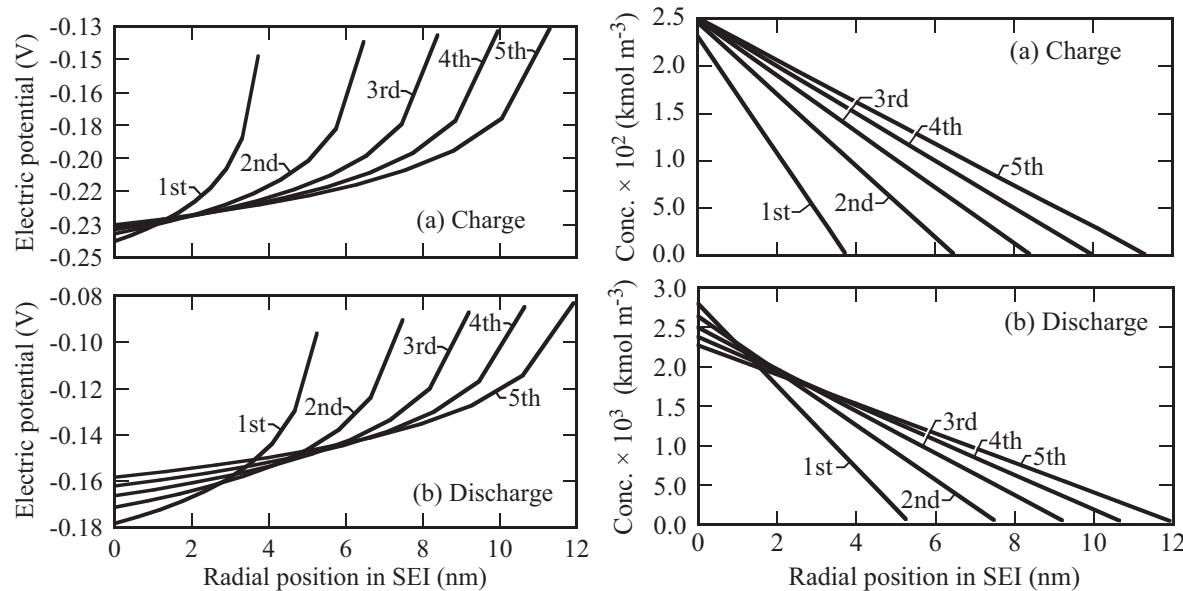


SEI Decomposition:



(Electrochmica Acta, 2011)

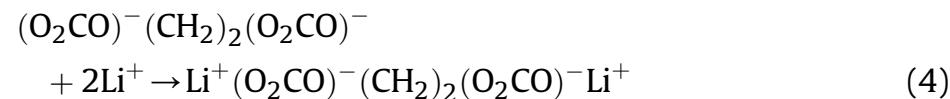
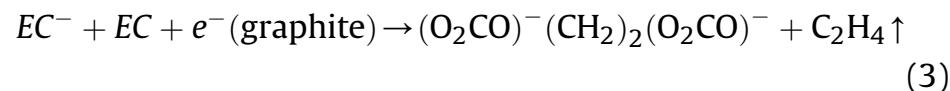
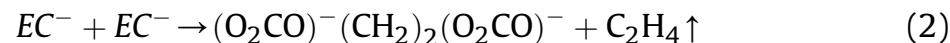
	Reaction
<i>SEI-electrolyte interface</i>	
1	$C_3H_4O_3(E) + (S^s) \rightleftharpoons C_3H_4O_3(S^s)$
2	$Li^+(S^s) \rightleftharpoons Li^+(E) + (S^s)$
3	$C_2H_4(E) + 2(S^s) \rightleftharpoons C_2H_4(S^s)$
4	$C_3H_4O_3^-(S^s) \rightleftharpoons C_3H_4O_3(S^s) + e_{S^b}^-$
5	$C_2H_4(S^s) + CO_3^{2-}(S^s) \rightleftharpoons C_3H_4O_3^-(S^s) + e_{S^b}^- + 2(S^s)$
6	$CO_3^{2-}(S^s) + 2Li^+(S^s) + (S^b) \rightleftharpoons Li_2CO_3(S^b) + 3(S^s)$
7	$Li(S^b) + (S^s) \rightleftharpoons V^-(S^b) + Li^+(S^s)$
8	$Li_{S^b}^+ + (S^s) \rightleftharpoons Li^+(S^s)$
<i>Graphite-SEI interface</i>	
9	$e_{S^b}^- \rightleftharpoons e_{C_6}^-$
10	$Li(C_6) + V^-(S^b) \rightleftharpoons Li(S^b) + e_{C_6}^- + (C_6)$
11	$Li(C_6) \rightleftharpoons Li_{S^b}^+ + e_{C_6}^- + (C_6)$



Kupper and Bessler, JECS 2017

Layer	Phase	Initial volume fraction ε	Density $\rho/\text{kg} \cdot \text{m}^{-3}$	Species (initial mole fraction X)
Cathode	Cathode active material	0.67 ¹⁰¹	1510 ¹⁰¹	Li[LFP] (0.01), V[LFP] (0.99)
	Electrolyte	0.28** ¹⁰¹	1130 ¹⁰¹	$\text{C}_3\text{H}_4\text{O}_3(\text{l})$ (0.6), $\text{C}_4\text{H}_6\text{O}_3$ (0.2), $\text{Li}^+(\text{solv})$ (0.1), PF_6^- (solv) (0.1)
	Gas phase cathode	0.05**	1.14 ¹⁰⁴	N_2 (0.999), $\text{C}_3\text{H}_4\text{O}_3(\text{g})$ ($1.0 \cdot 10^{-8}$), C_2H_4 ($1.0 \cdot 10^{-8}$), O_2 ($1.0 \cdot 10^{-8}$), CO_2 ($1.0 \cdot 10^{-8}$), H_2O ($1.0 \cdot 10^{-8}$), H_2 ($1.0 \cdot 10^{-8}$)
Separator	Separator	0.5 ¹⁰⁵	200 ¹⁰⁶	Separator (1.0)
	Electrolyte	0.5 ¹⁰⁵	1130 ¹⁰¹	$\text{C}_3\text{H}_4\text{O}_3(\text{l})$ (0.6), $\text{C}_4\text{H}_6\text{O}_3$ (0.2), $\text{Li}^+(\text{solv})$ (0.1), PF_6^- (solv) (0.1)
Anode	Anode active material	0.72 ¹⁰¹	2540 ¹⁰¹	$\text{Li}[\text{C}_6]$ (0.57), $\text{V}[\text{C}_6]$ (0.43)
	Electrolyte	0.22** ¹⁰¹	1130 ¹⁰¹	$\text{C}_3\text{H}_4\text{O}_3(\text{l})$ (0.6), $\text{C}_4\text{H}_6\text{O}_3$ (0.2), $\text{Li}^+(\text{solv})$ (0.1), PF_6^- (solv) (0.1)
	SEI	0.01*	1300 ¹⁰⁷	$(\text{CH}_2\text{OCO}_2\text{Li})_2$ (1.0)
	Gas phase anode	0.05**	1.14 ¹⁰⁴	N_2 (0.999), $\text{C}_3\text{H}_4\text{O}_3(\text{g})$ ($1.0 \cdot 10^{-8}$), C_2H_4 ($1.0 \cdot 10^{-8}$), O_2 ($1.0 \cdot 10^{-8}$), CO_2 ($1.0 \cdot 10^{-8}$), H_2O ($1.0 \cdot 10^{-8}$), H_2 ($1.0 \cdot 10^{-8}$)

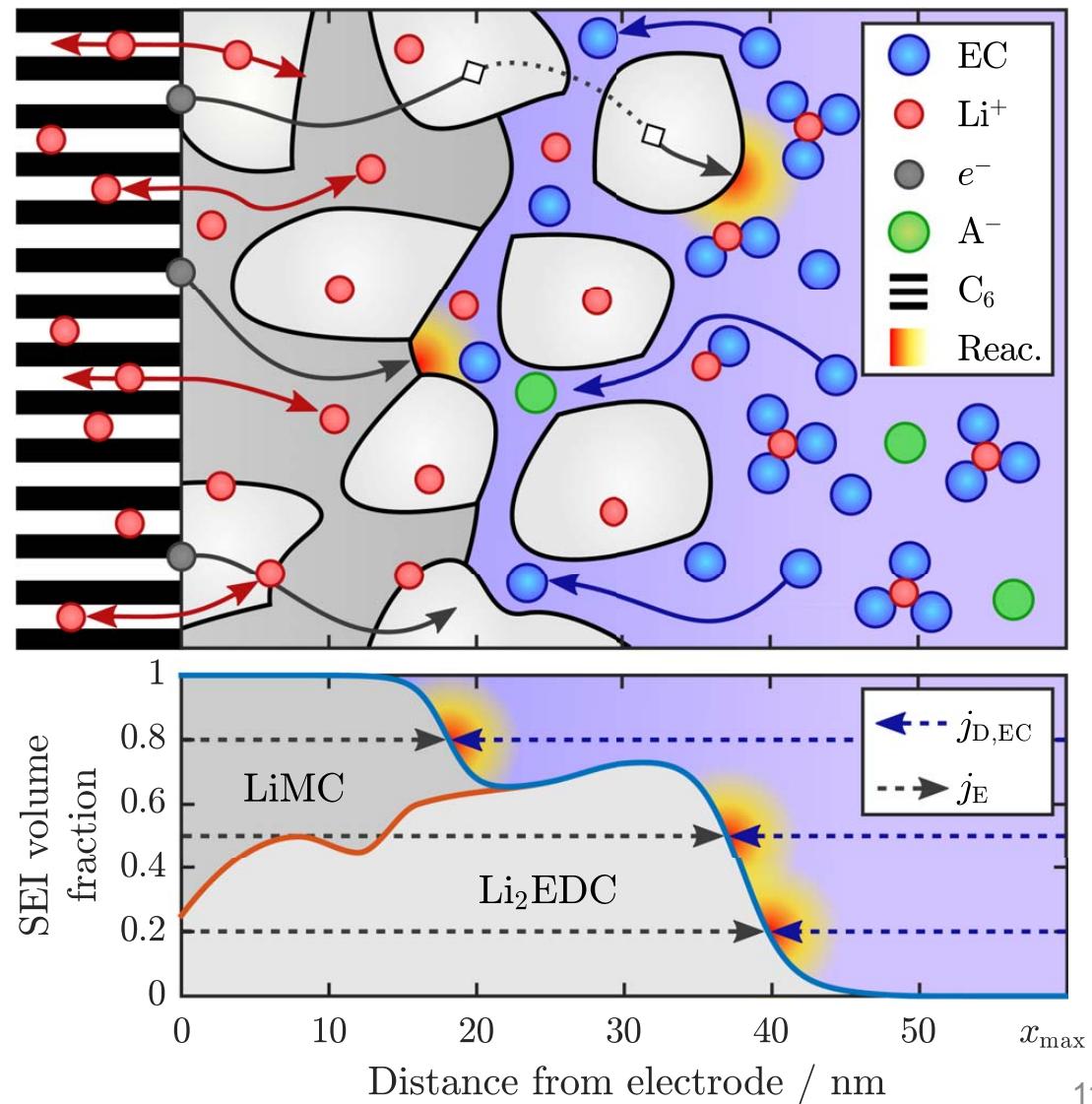
Liu, et al., J Power Sources, 2014



Single, Horstmann, Latz,

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J. Electrochem. Soc. (2017)



SEI Chemistry Models

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- Compared to other fields, “large” SEI mechanisms are small, do not yet reflect the considerable chemical, structural complexity.
- Limited development of detailed chemistry is understandable.
 - Materials constantly evolving
 - Computational tools not widely adopted; each new model must “reinvent the wheel.”
 - Limited *in situ* / *in operando* chemical data available for validation of simulation results.

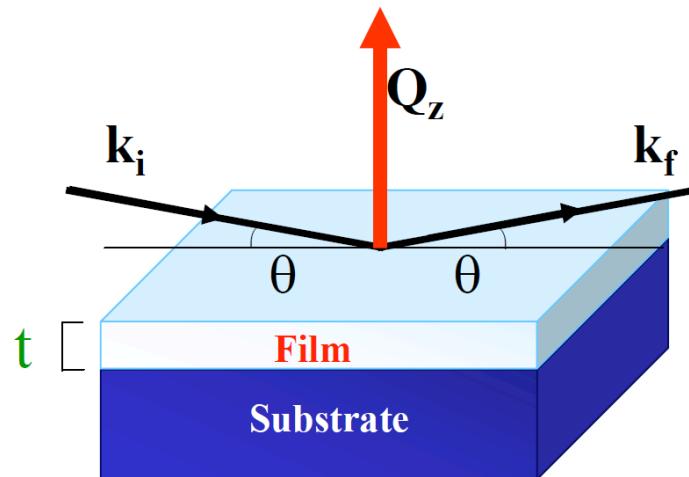
Outline

Colorado School of Mines

- Introduction: Current understanding of the SEI
- Chemical models of SEI growth
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Neutron Reflectometry Overview

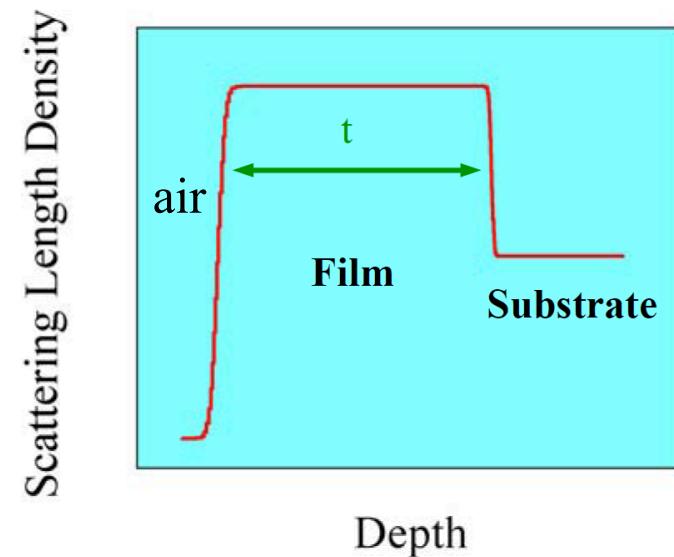
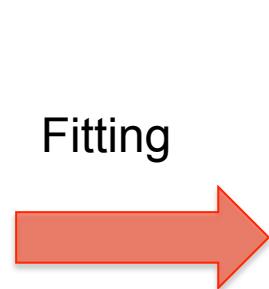
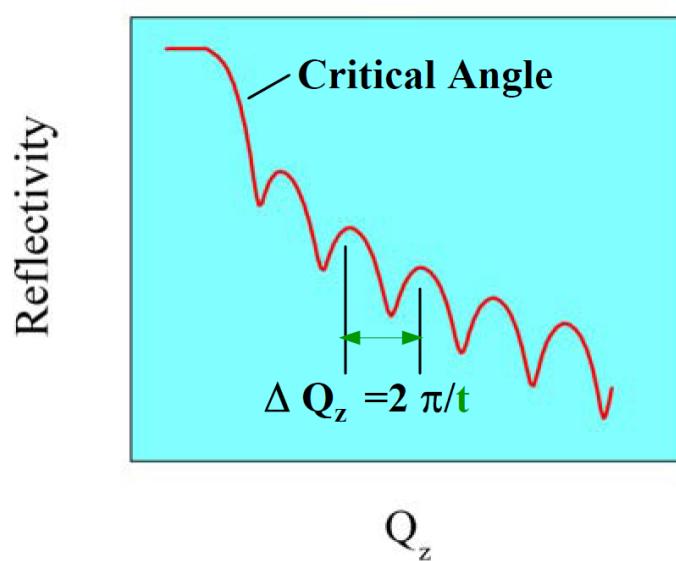
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- Measures Reflected Intensity vs. grazing angle θ
- Oscillations with period $2\pi / \text{layer thickness}$
- NR Provides Depth Profile of the SLD
- SLD related to Composition:

$$\text{SLD}(z) = \sum_j \text{SLD}_j V_j$$

$$\text{SLD}(z) = \sum_i b_i n_i$$



Cell Fabrication

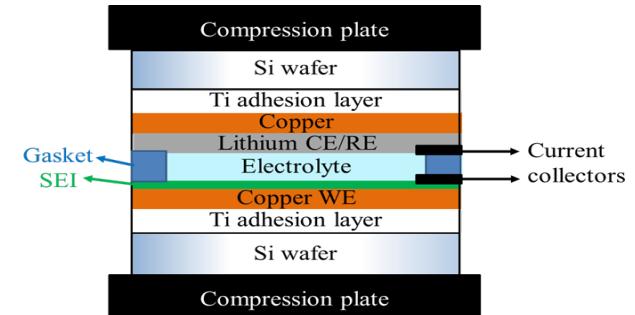
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- Non-intercalating working electrode (WE)

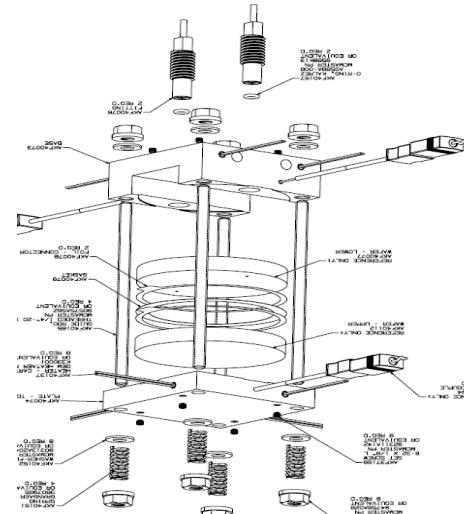
 - All charge attributed to SEI chemistry.

 - Minimal WE change during experiments.

- Li metal counter/reference electrode.



- Substrate: 5 mm thick polished Si.



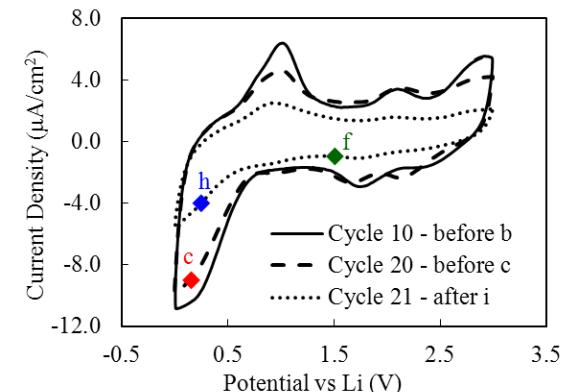
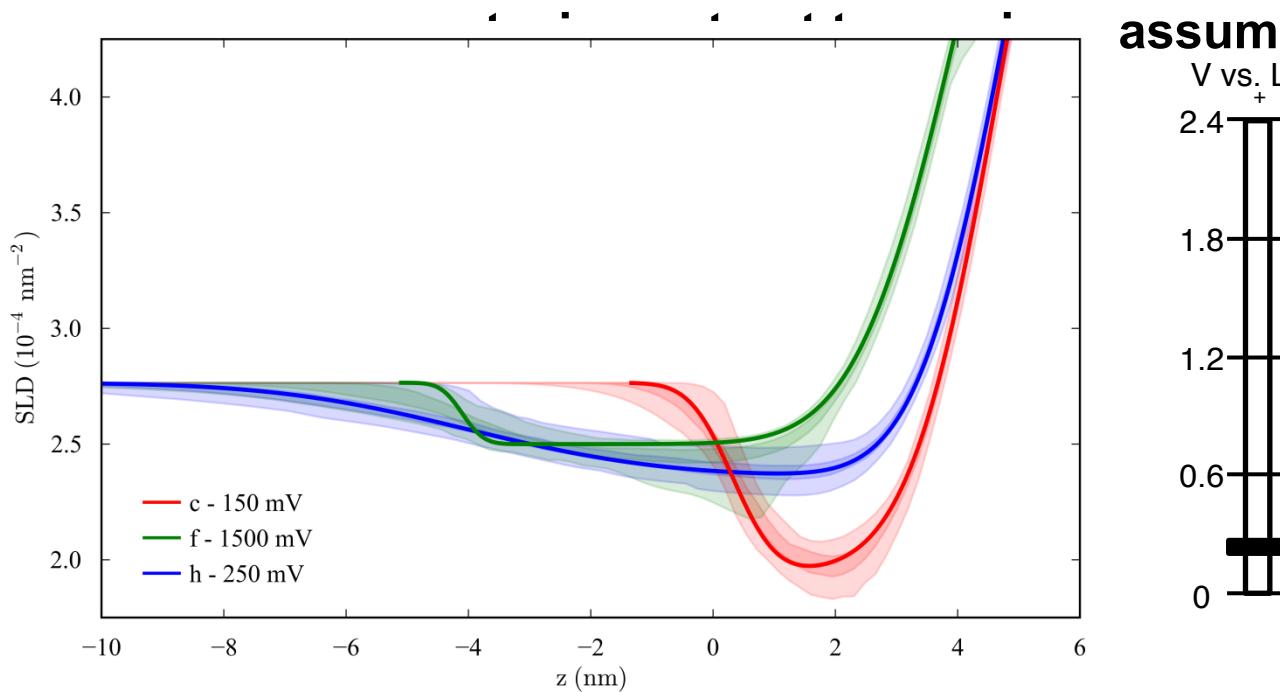
- Thick (100-500 μm) liquid electrolyte reservoir:

 - Deuteration increases SLD, better contrast with lithiated compounds in SEI.

NR of SEI on Cu at Varying Potentials

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- NR results during potentiostatic holds reveal changes to the SEI thickness, composition, and structure with cycling.
- SLD decreases (Li increases) with decreasing WE potential.
- SEI thickness continues to increase with additional processing.
- Some test points show composition gradients; others show mixing of SEI

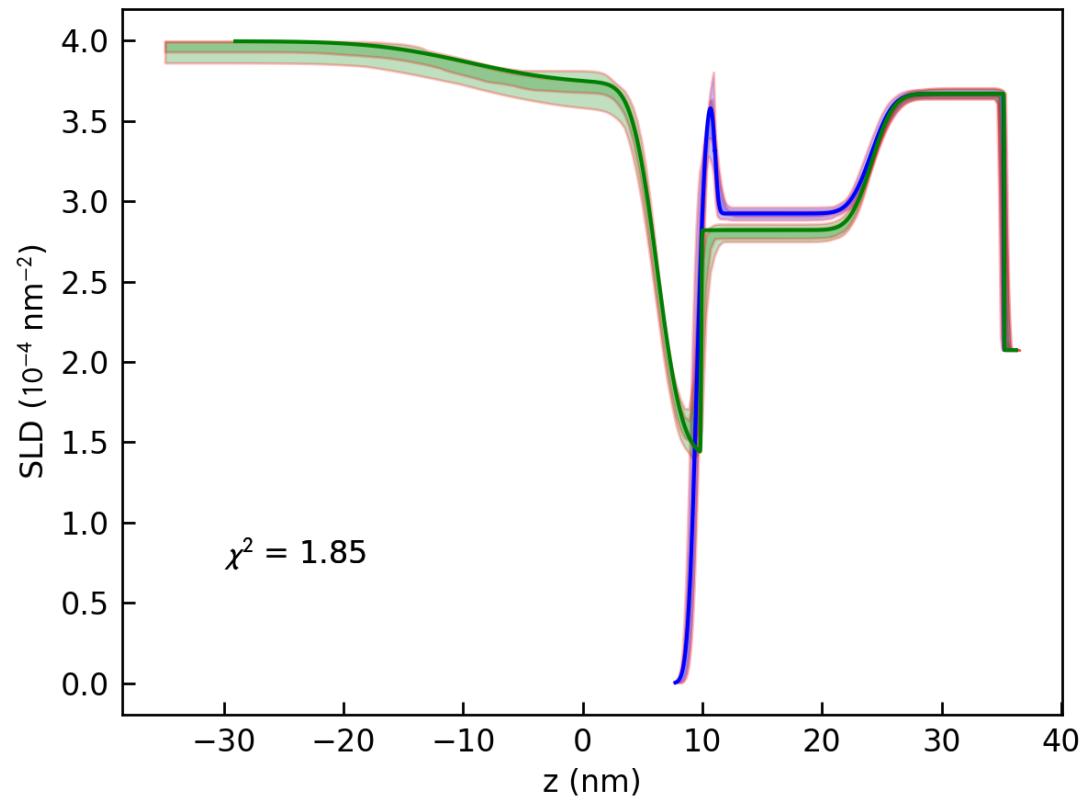
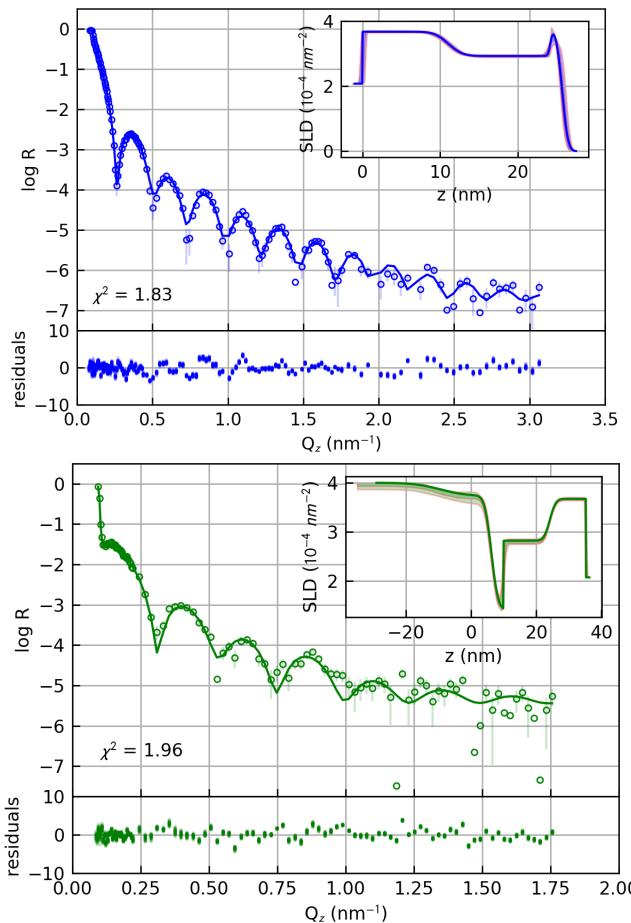


NR of SEI on Tungsten Directly Reveals Hypothesized Two-layer Structure

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■ Two layer SEI structure

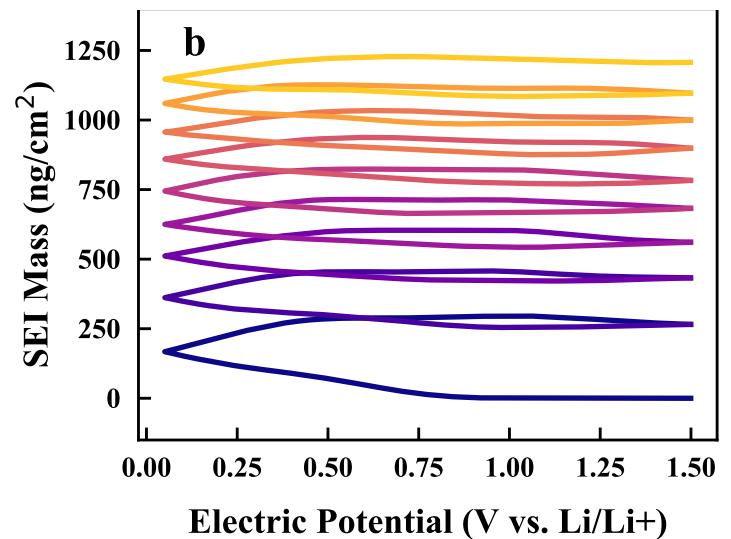
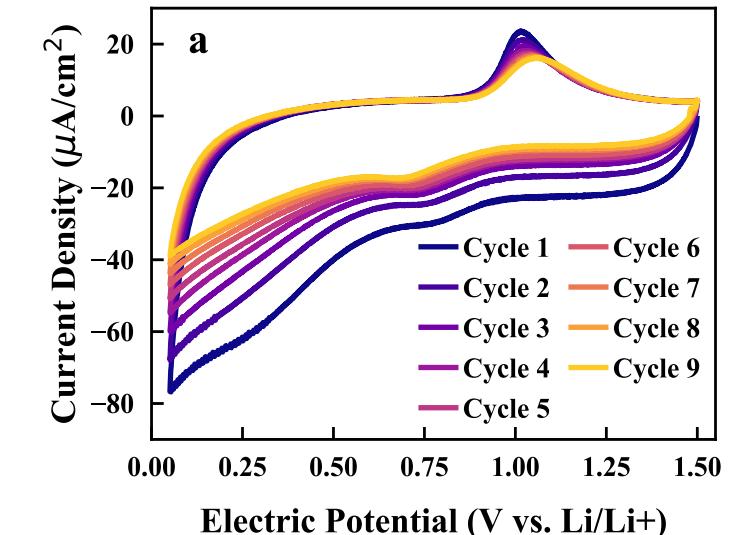
- Denser “inner” SEI – 3.7 nm
- Porous “outer” SEI – 15.3 nm



EQCM-D Shows Growth, Re-dissolution of SEI

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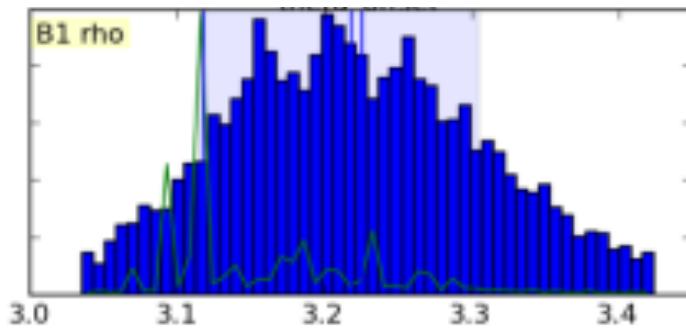
- Reduction peak at 800 mV: electrolyte decomposition
- Reduction peak at 275 mV, oxidation peak at 1.1 V: lithium underpotential deposition, stripping
- Decrease in mass gain per cycle – passivation and partial SEI dissolution



NR + QCM Provides Detailed Look at SEI Chemistry

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- NR gives thickness and SLD



- EQCM-D determines SEI mass
- Monte Carlo model of SEI chemical composition
 - Randomly generate mole fractions, choose thickness from fitted distribution
 - Calculate SLD and Mass for the generated composition and thicknesses (inner & outer layer).
 - Mass must fall within uncertainty window of QCM data
 - Compare SLD values to probability distribution function from NR, use Metropolis Algorithm to choose “likely” models.

SEI Chemistry

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Inner SEI:

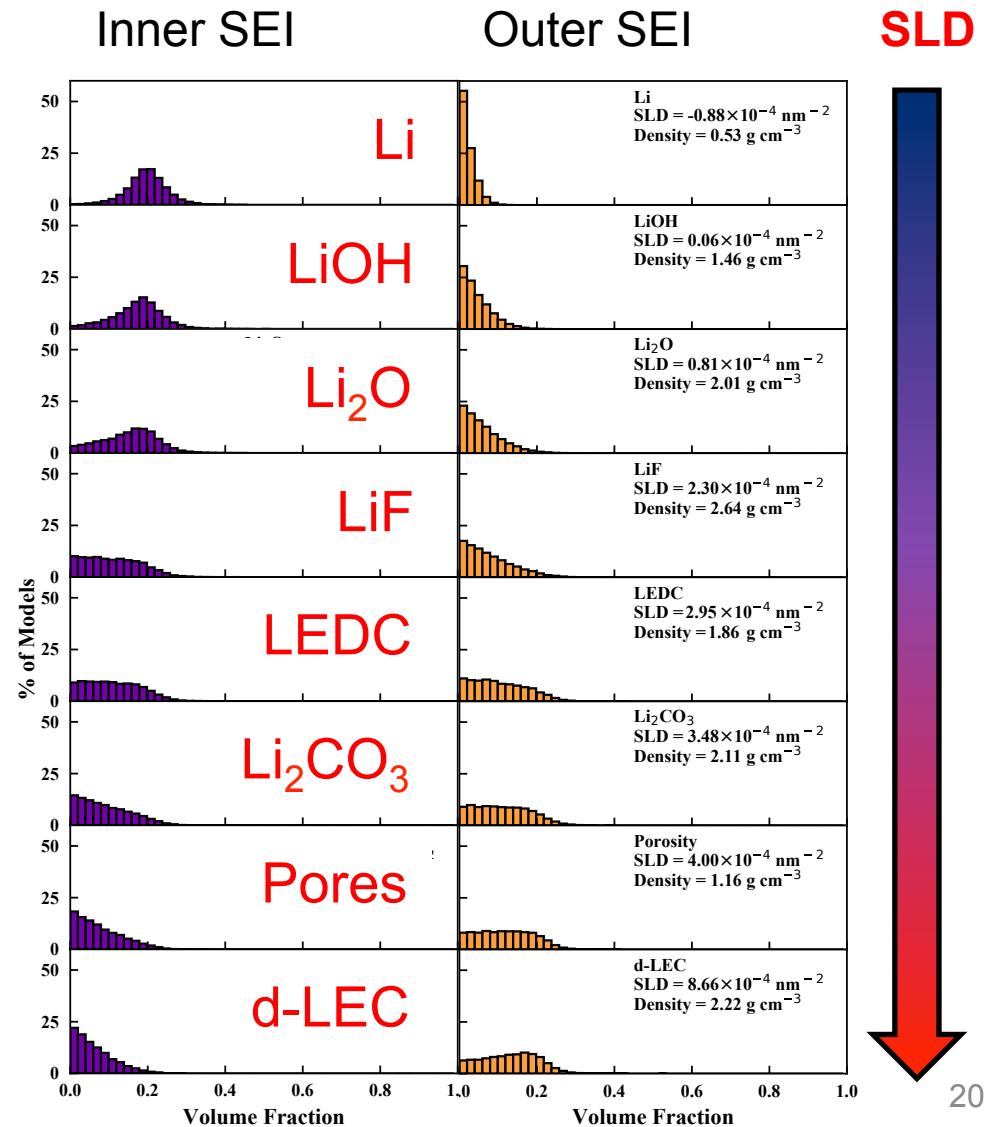
Low-SLD components most prominent
Li, LiOH, Li₂O, but all below 30%.

Outer SEI:

High-SLD components most prominent
Li Ethyl Carbonate, Electrolyte/pores

Intermediate SLD components: not really discriminated

Lower noise in QCM-D needed to determine composition with greater resolution.



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Numerical Simulation of SEI Growth

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- Growth of SEI modeled via elementary electrochemistry:

$$\dot{q}_i = k_{\text{fwd}} \prod_j a_j^{v_{j,i,\text{fwd}}} - k_{\text{rev}} \prod_j a_j^{v_{j,i,\text{rev}}}$$

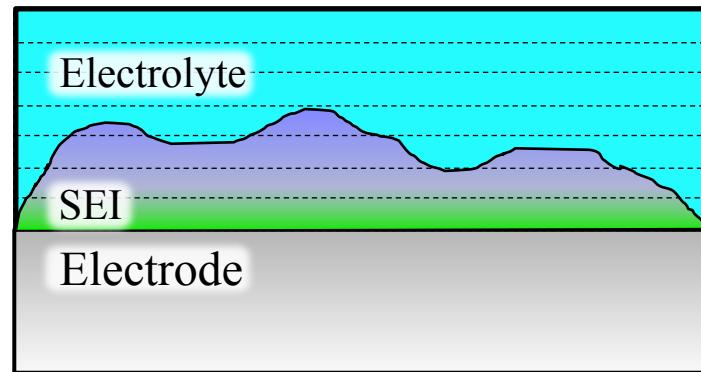
where:

$$k_{\text{fwd}} = k_{\text{fwd}}^\circ \exp\left(\frac{nF\beta\Delta\phi}{RT}\right)$$

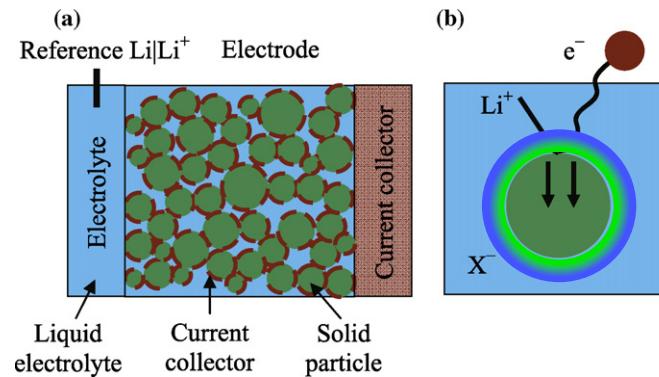
$$k_{\text{rev}} = k_{\text{rev}}^\circ \exp\left(\frac{nF(1-\beta)\Delta\phi}{RT}\right)$$

- Initial model: planar, non-intercalating “model” electrode
- Depth profiling enabled by dividing electrolyte at electrode surface into volumes.

Step 1: Model electrode



Step 2: Newman-type model

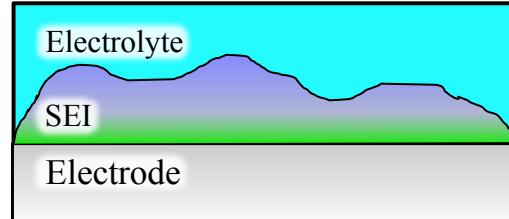
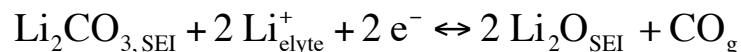
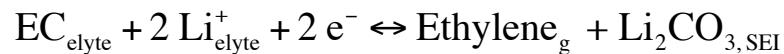
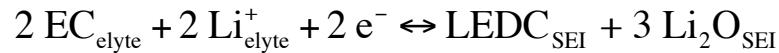


W. Lai, F. Ciucci, Electrochimica Acta, 2011

Simulation Approach

Colorado School of Mines

■ Simple SEI chemistry:



SEI Growth Rate:

$$\frac{\partial \phi_{\text{SEI}}}{\partial t} = \sum_{k,\text{SEI}} \frac{W_k}{\rho_k \Delta z} \dot{s}_k$$

Charge Transfer:

SEI / W anode:

$$\dot{q}_{\text{SEI/W}} = k_{\text{fwd}} \prod_j a_j^{v_{j,\text{SEI/W},\text{fwd}}} - k_{\text{rev}} \prod_j a_j^{v_{j,\text{SEI/W},\text{rev}}}$$

SEI / Electrolyte

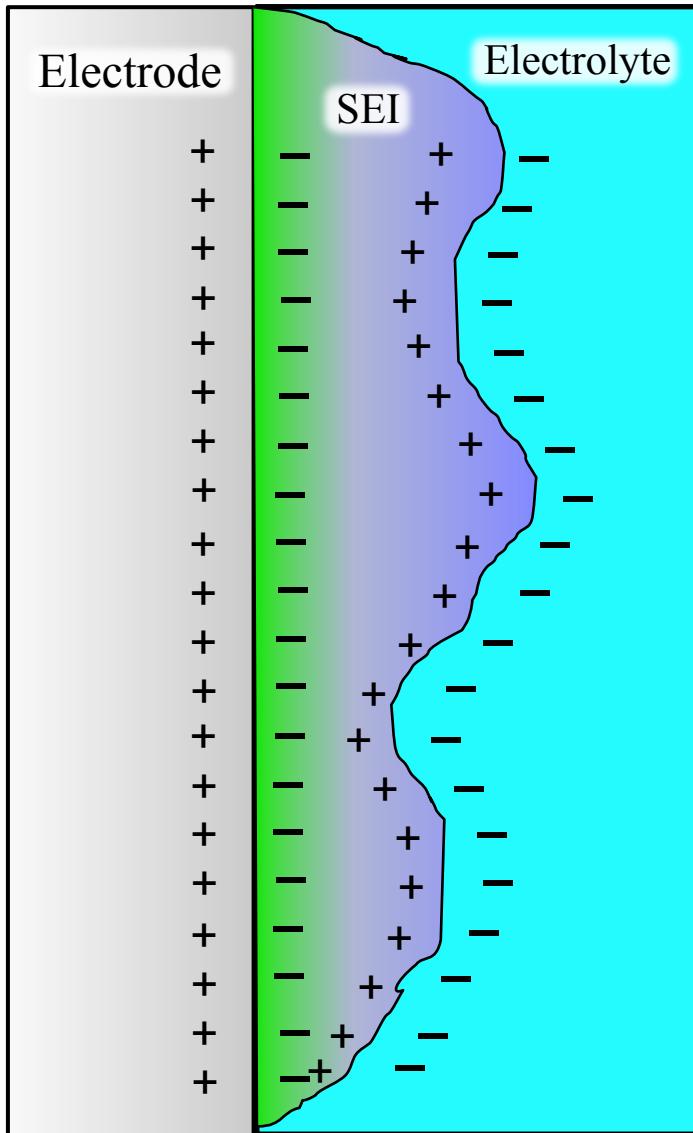
$$\dot{q}_{\text{SEI/elyte}} = k_{\text{fwd}} \prod_j a_j^{v_{j,\text{SEI/elyte},\text{fwd}}} - k_{\text{rev}} \prod_j a_j^{v_{j,\text{SEI/elyte},\text{rev}}}$$

Finite electronic conductivity.

- Charge transfer capacitance, (electro)chemical reaction rates, SEI resistance all are tunable parameters.
- Simulate a simple CV curve between 1.0 V and 0.05 V, at a scan rate of 10 mV/s.

Simulation Approach

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Charge neutrality:

$$i_{\text{SEI,elyte}} = i_{\text{SEI,cond}} = i_{\text{SEI,W}}$$

$$i_{\text{SEI,elyte}} = \sum_{k,\text{SEI}} z_k F v_{k,\text{SEI/elyte}} \dot{q}_{\text{SEI/elyte}}$$

$$i_{\text{SEI,cond}} = \frac{R_{\text{SEI}}}{\Delta\phi_{\text{SEI}}}$$

$$i_{\text{SEI,W}} = - \sum_{k,\text{SEI}} z_k F v_{k,\text{SEI/W}} \dot{q}_{\text{SEI/W}}$$

$$\phi_{\text{W}} - \phi_{\text{SEI}} = \Delta\phi_{\text{W/SEI}} + \Delta\phi_{\text{SEI}} + \Delta\phi_{\text{SEI/elyte}}$$

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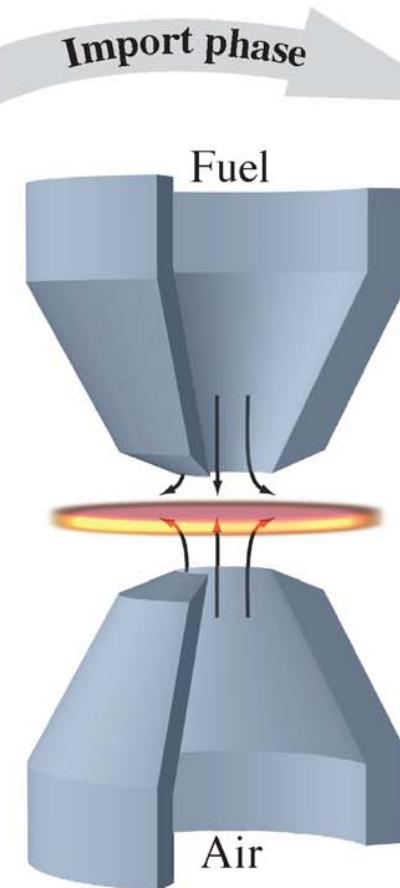
Cantera: Chemical Kinetics, Thermodynamics, Transport

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Cantera input file (CTI)

```

species(name = "H2",
       atoms = " H:2 ",
       thermo = (NASA( [200.00, 1000.00],
                      [ 2.344E+00, ... , 6.83E-01 ] ), ... ),
       transport = gas_transport (
           geom = "linear",
           diam = 2.92,
           well_depth = 38.00 ) )
species (name="CO", .....
:
reaction( "O + H2 <=> H + OH",
          [3.87000E+04, 2.7, 6260])
three_body_reaction ( "2 O + M <=> O2 + M",
                      [1.20000E+17, -1, 0],
                      efficiencies = "H2:2.4 H2O:15.4 ")
reaction( "H + O2 <=> O + OH",
          [1.0E+14, 0.0, 7700])
:
ideal_gas (name = "flamegas",
            elements = "O H C N Ar",
            species = """ H2 H O O2 OH
                        H2O HO2 H2O2 C ... """,
            transport = 'Mix',
            reactions = 'all' )
  
```



Computational model

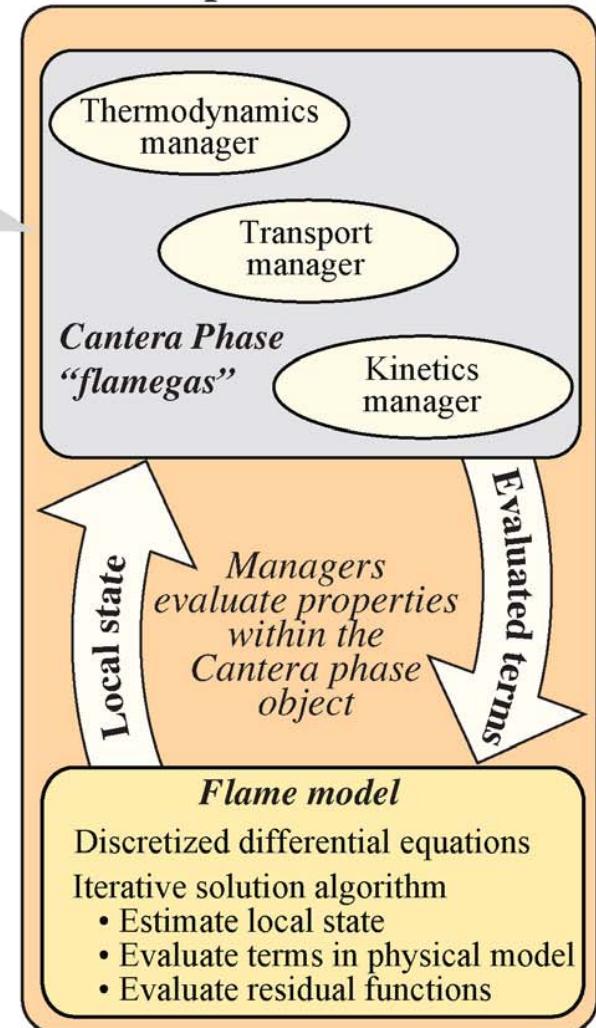


Image courtesy R. J. Kee, Colorado School of Mines

Cantera: Chemical Kinetics, Thermodynamics, Transport

Colorado School of Mines

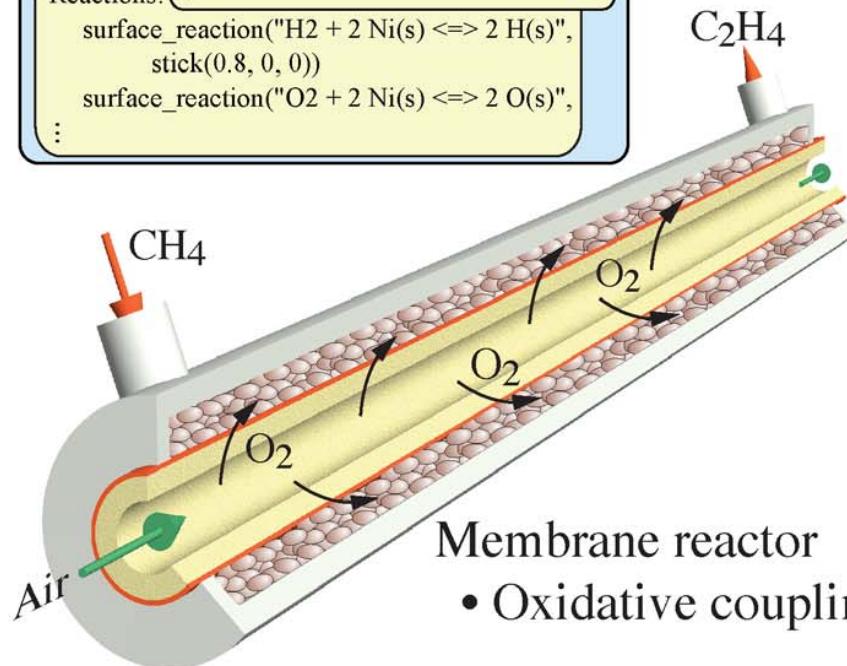
Cantera input file (CTI)

```

Gas phase object:
ideal_gas(name = 'fuelGas',
...)
:
Interface object:
ideal_interface(name='Ni_surface',
elements = "Ni H O C",
species = """"Ni(s) H(s) ... """,
phases = "fuelGas Ni_bulk",
reactions = "all",
site_density = 2.7e-9)
:
Reactions:
:
surface_reaction("H2 + 2 Ni(s) <=> 2 H(s)",
stick(0.8, 0, 0))
surface_reaction("O2 + 2 Ni(s) <=> 2 O(s)",
:

```

Import phases



Computational model

Initialize Cantera Objects:

```

Import gas and surface phases:
gas = importPhase ('OCMcat.cti', 'fuelGas');
bulk = importPhase ('OCMcat.cti', 'Ni_bulk');
surface = importInterface ('OCMcat.cti', 'Ni-surface', gas, bulk);

```

Solve Discretized ODEs:

```

Set local states for gas and surface objects:
set(gas, 'T', T_reactor, 'P', pressure, 'X', X_k)
setCoverages (surface, Theta_k)
setTemperature (surface, T_reactor)

```

Evaluate residual functions:

$$\frac{d(\phi_g \rho Y_k)}{dt} = -\nabla \cdot (\rho Y_k \mathbf{v} - D_k W_k \nabla [X_k]) + W_k (\dot{\omega}_k + a_{surf} \dot{s}_k)$$

Retrieve Diffusion Coefficients:
 $D_k = \text{mixDiffCoeffs(gas);}$

Retrieve Reaction Rates:
 $\omega_{gas} = \text{netProdRates(gas);}$
 $sdot_{surf} = \text{netProdRates(surface);}$

Cantera website: cantera.org

Repository on GitHub:
<https://github.com/cantera>

Users' Group:
<https://groups.google.com/forum/#!forum/cantera-users>

Demonstration:
[https://github.com/decaluwe/ECS_2018_materials/
blob/master/ECS_2018.ipynb](https://github.com/decaluwe/ECS_2018_materials/blob/master/ECS_2018.ipynb)

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E637



On the Fundamental and Practical Aspects of Modeling Complex Electrochemical Kinetics and Transport

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Numerous technologies, such as batteries and fuel cells, depend on electrochemical kinetics. In some cases, the responsible electrochemistry and charged-species transport is complex. However, to date, there are essentially no general-purpose modeling capabilities that facilitate the incorporation of thermodynamic, kinetic, and transport complexities into the simulation of electrochemical processes. A vast majority of the modeling literature uses only a few (often only one) global charge-transfer reactions, with the rates expressed using Butler–Volmer approximations. The objective of the present paper is to identify common aspects of electrochemistry, seeking a foundational basis for designing and implementing software with general applicability across a wide range of materials sets and applications. The development of new technologies should be accelerated and improved by enabling the incorporation of electrochemical complexity (e.g., multi-step, elementary charge-transfer reactions and as well as supporting ionic and electronic transport) into the analysis and interpretation of scientific results. The spirit of the approach is analogous to the role that Chemkin has played in homogeneous chemistry modeling, especially combustion. The Cantera software, which already has some electrochemistry capabilities, forms the foundation for future capabilities expansion.

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Outline

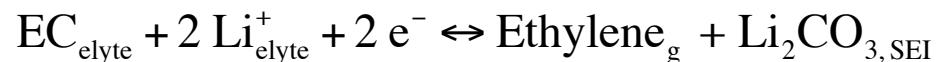
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- Introduction: Current understanding of the SEI
- Chemical models of SEI growth
- Experimental data for validation
- Numerical Simulation of SEI Chemistry (1)
- Interlude: Cantera
- Numerical Simulation of SEI Chemistry (2)
- Conclusions and Next Steps

Preliminary Simulation Results

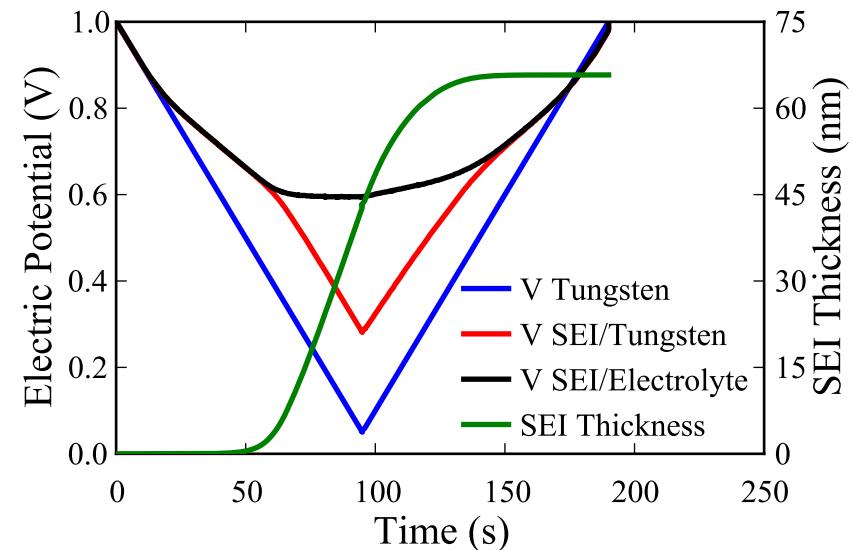
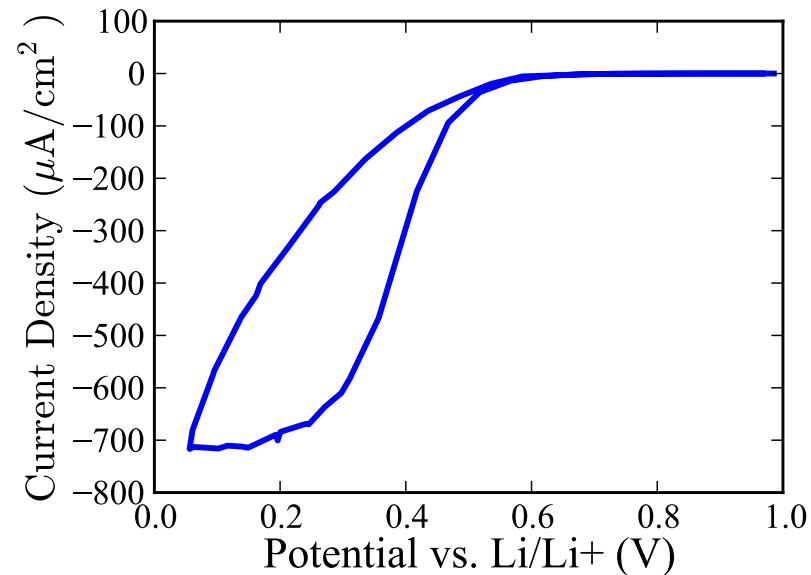
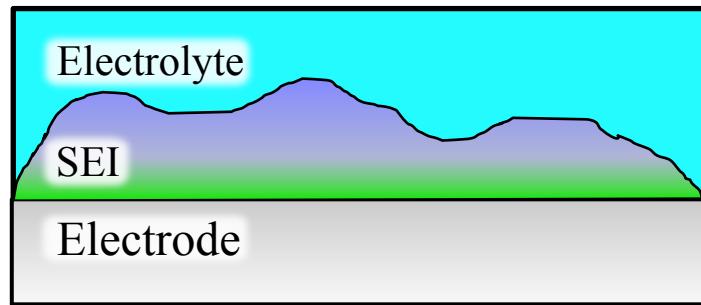
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- Simple SEI chemistry:



- Charge transfer capacitance, (electro)chemical reaction rates, SEI resistance all are tunable parameters.

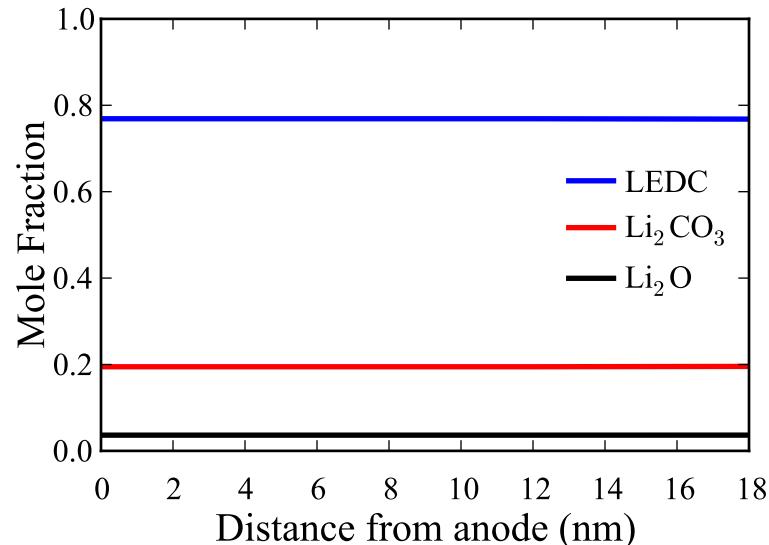
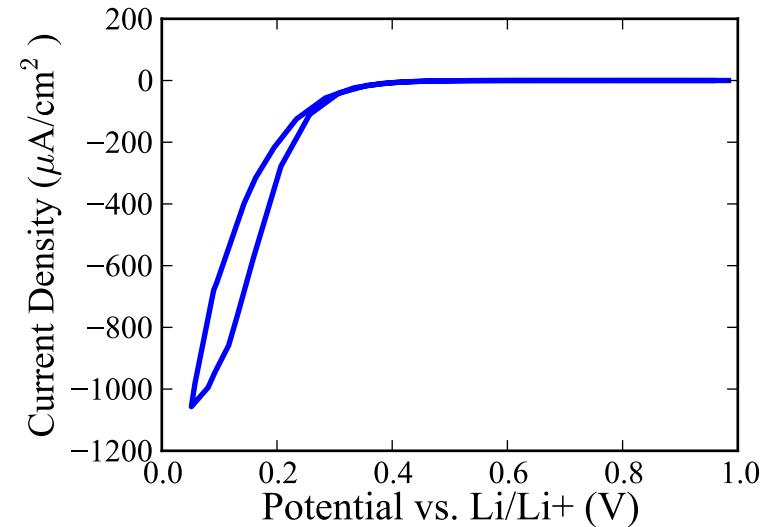
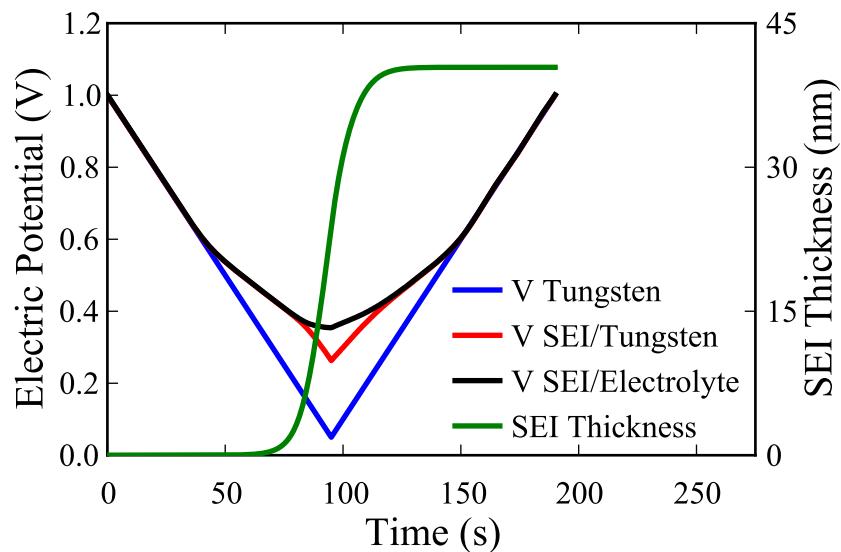
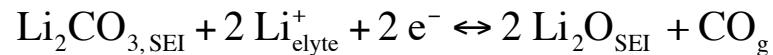
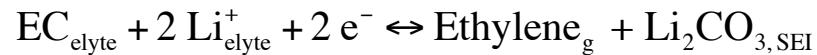
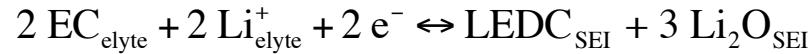
- Simulate a simple CV curve between 1.0 V and 0.05 V, at a scan rate of 10 mV/s.



Preliminary Simulation Results

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■ “Complex” SEI chemistry:



Conclusions, Outlook

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- More NR and EQCM-D
 - More realistic substrates (carbon)
 - Verify SEI mitigation / improvement strategies: additives, growth conditions.
- Additional physics for SEI growth model
 - Porosity and roughness
 - Discretized SEI electric potential
 - Local resistance function of composition
 - Ion transport in SEI – solid diffusion and diffusion in electrolyte-filled pores

Thank You.