Chemistry question Bank

option

A) Pipole moment of molecules unat change during vibration

option

A) Reduction potential must be higher. option

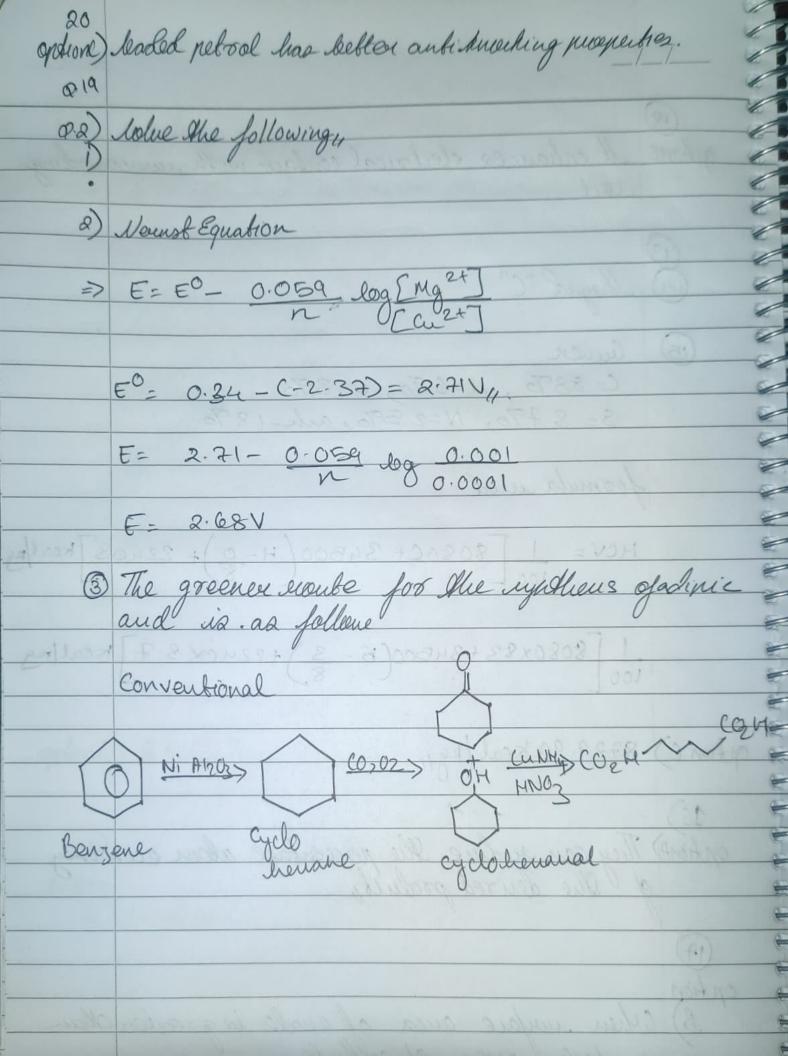
Cell can work Judefinitely ondion

O) Moderate iguation temp and high calorafic value

6) option
B) Negative. Stress corrouion.

			6
		1	-
		//	1
		Call	-
(6)	Calculate the atom economy		-
		100	-
Acodo	Co H5NH2 + CCH3 CO20 -> CO H5NHCOCK Molecular Weight of Readouts + CH3COOM [12x6+1x5+1xH+1x2]	43	6
	Moleculare Weight of Readouts + CH3COOH		-
	[12×6+1×5+1×1+1×2]	26143	1
	+ [12x1+1x3+6+16]x2+1	6 × 1	
	L		
	= 195	(E.	
	Notes law useful + al and reading	to station	5
	Molecular weight of end product	0 1	
	BOUNDAL AND ALL MAN	-122	
	12x6+1x5x+14x1+1x1+12x1+16x1+12x1+	lank a	2
	= 133	0	
		100	
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	Total moleular weight of readout	Colore	-
c valu	of reargant	10	-
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	= 133 × 100 = 68.201	TOTAL TOTAL	
	195	0	15
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	Street Cornouns.	191	(6
			-05
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options It enhances electrical contait with invulving Mayad "C" (15) C= 83%, H= 690, 0= 390 8= 3-790, N=2-590, ach=1.890 formula med HCV= 1 [8080C+ 34500 (H-0)+ 22408] kcells 1 8080x83+34500(6-3)+2240x3-7 Kcalles option E) 8729.90 Kcel/kg/ option They can reduce the percentage about economy
of the derived producty B) When myface area of ande is greater than 18) Ecell = Ecalhode - Earocle



Gereener exoube CO2H CO2H COM Polucion PLH2> HOZC 50Rsi Adipic aride. 'doean material or feed stock iliants be seenewalde" Q.4) -4 \000 x = 1 \ x 000 x \ = = -> Differential acception corrocion, it is blue corrowou that occurs when a medal is subjected to deflerent air concentration More onygenated area (Cathede) les onygenated area (Anode) -> Zusoy solution The paid while is ubmert a in the liquid organisted Therefore it is

Reaction cashade > 1 02+ H2O+ 200 -> 240 ( Reduction) -> loluble corrovion readuit, The eate is faster wince the product is an electrolyte > anodic area & alhodicarea leis corrouon ia seen -> callabie aule a 2 anodic alla More corrouten is seen, (5) Quiven formula uned. C = 80 70 = 1 [8080C+34500(H-0)+22408] H= 590 0= 190 N= 2010 8257 875 Kcal/kg/ S= 5% del = 70/0 Weight of ougen is = 0.03 kg lince air contain 2396 onygen 100 x 0. 01 = 0. 0434 kg 2x5 kg coal total amount

of cur = 2x5 x 0.0434

= 0.434 kg/l.

0.434 x 224 = 0.335 mg/

Ø.6 → SS. Cathodic coaling Coading material (0.7) dnodic coading is at lover potential is at higher potential If the coaling breaks If the coaling break is not purpleded. is itill prootected An (Sn) comprues Zn countinues so So pertect the peroteet the medal metal dell dhe cell action coaling is perfect Can be eved. Can't be end on food product Cooperane, food To protet exol confainer. 3) President of Chair makes and Con harm

(8) (DEEDE) 12 principle of green chewstry 11 3 the of non-haradern chemical Were of rafer chemicals (5) Me of catalysts (a) suoid chemical demination @ the of evenewable feedsbock (8) Mininge of Amilaly substances a) Justenie Alle efficiently 10) Product Shat degroce after use 12) dualytical medleds. 11) Minimize accidents Defler to prevent worke dran to treat or 2) Best to carry-out syndheirs by designing such a pallurery that econces by-products 3) Pisposal of Source water and con haum living organism including human beings.

O Cathodic protection.

→ Cathodic protection method of corrounce control

The metal which is to be protected is

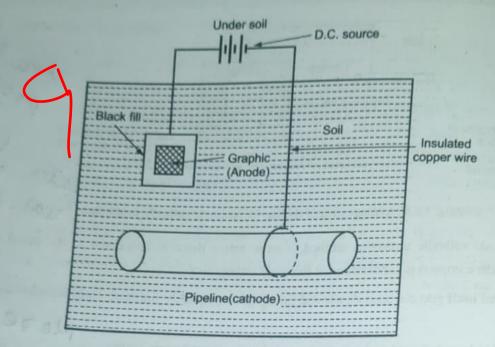
forced see art as a cathode, This is emplained by medal meation in acidic medium -> Reaction M -> M+N+NE QH++2e-> H2H -> Callodic protection is achieved by upplying entereal current to the metal deditional electron insparses the metal dessolution. (10) H= 2 x Increase in weight of water x 10 Griven

C= 0.25g = V2V1 × Normal ×1.4

CaC12=0.09g weigh of cool

KOH = 0.8g 36.5-49.5 × 0.12 × 1.4 = 5. H= 2 x 0.09 x100- 490 C= 12 x increase in weight of CO2 12 x 0.8 x100 = 87.27 90





(2D17)Fig. 4.5.5: Arrangement of the impressed current cathodic protection

- (2) In the impressed current cathodic protection method, a current is applied in the opposite direction to that of the corrosion current, thereby nullifying the effect of the corrosion current on the base metal that means converting the base metal into cathode.
- (3) The impressed current is obtained by using a d.c. source such as a wet battery or a dry cell alongwith an insoluble anode made up of platinum, stainless steel, graphite etc which is embedded underground and to this impressed current is applied.
- (4) The whole assembly is connected to the metallic structure to be protected.
- (5) The anode can be single for a small structure like water tank or there can be many series connected such anode, if the structure to be protect is big like long pipeline, oil-rig platforms on the sea etc.
- (6) The insoluble anode is kept inside back-fill made up of mostly gypsum which increases the electrical contact with the soil.
- (7) Advantage: This method can protect very large and long structures. Further, its maintenance is easy.
- (8) Disadvantage: The anode needs frequent replacement.

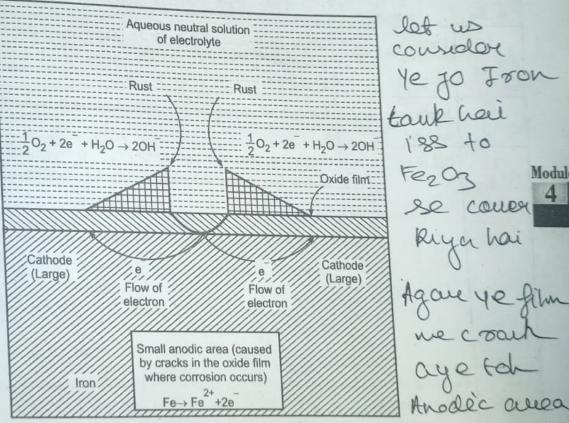
-		10000	EL ANTINO
9 4.2.2	Wet or Electrochemical Corrosion	muent &	Comp grown
10. 4.2.6	Drine electrochemical conversion.		- Q. 2(a), May 18, 1 Mark)
UQ. 4.2.	What is dectrochemical convertion?	▶ Ref. : (MU -	Q. 2(a), Dec. 14, 2 Marks)
	n and explains foll of electrochemical conversion	tal surface	1. agriculturalis
-/		constant on	Last 1 in the form
(i) (ii)	When the metal surface is in immediate contact with aqueous aci the short circuited galvanic cells. When 2 dissimilar metals or alloys are either immersed or dipped	dic/alkaline/neutral/election  of Control  partially in the agueous s	rolytic solutions forming
2) The	corrosion is due to the formation of anodic and cathodic area between the policy of the corrosion is due to the formation of anodic and cathodic area between the corrosion is due to the formation of anodic and cathodic area between the corrosion is due to the formation of anodic and cathodic area between the corrosion is due to the formation of anodic and cathodic area between the corrosion is due to the formation of anodic and cathodic area between the corrosion is due to the formation of anodic and cathodic area between the corrosion is due to the formation of anodic and cathodic area between the corrosion is due to the formation of anodic and cathodic area between the corrosion is due to the corrosion of anodic and cathodic area between the corrosion of the	ween which current flows	the unettable
	anodic reaction involves dissolution of metal as corresponding notes, at anode: $M \longrightarrow M^{n+} + ne^{-}$ According to the cathodic reaction consume electrons with either by	netallic ions with the libe	eration of free electrons.
	ending upon the nature of corrosive environment (a) and (b) are called		
pote	nen 2 different metals are in contract with a common conducting lie ential acts as an anode and it undergoes corrosion while the second chode and remains protected. Audle creater or	nd metal with lower oxid	ation potential acts as a

abroopdion of onygen occurs when the metal is in contact Ans.: (1) In the case of wet or electrochemical corrosion, absorption of oxygen occurs when the metal is in contact with aqueous acidic or alkaline/neutral or electrolytic solution and this causes corrosion. aqueous acidic

(2) Wet corrosion with oxygen absorption also takes place where two dissimilar metals or alloys are either immersed fully or dipped partially in the solutions mentioned above.

(3) Let us consider an iron tank having its inner surface coated with a thin film of iron oxide (Fe<sub>2</sub>O<sub>3</sub>) as shown in the Fig. 4.2.3.

Wet corrouin In onygen Tabli hota hai zabh Do dissimilar metal to elf south electrolyte



(2D8)Fig. 4.2.3: Schematic diagram for wet or electromechanical corrosion with absorption of oxygen

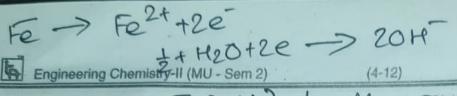
## (4) Explanation:

- (i) If this film develops some cracks, anode areas are created on the surface, while the metal acts as cathode.
- (ii) Here the anodic areas are small surfaces while rest of the surface of the metal forms large cathode.

....A SACHIN SHAH Venture

Riya hai

Module



(5) Reactions:

Fecore 2 / yellow oust,

(i) At anode: Fe  $\longrightarrow$  Fe<sup>2+</sup> + 2e<sup>-</sup>

The electrons flow to cathodic area through the metal and will be accepted by O2:

(ii) At cathode:  $\frac{1}{2}O_2 + H_2O + 2e^- \longrightarrow 2OH^-$ 

$$Fe^{2+} + 2OH^{-} \longrightarrow Fe(OH)_{2} \downarrow$$
(Ferrous hydroxide)

If enough O2 is present, ferrous hydroxide easily oxidizes to ferric hydroxide as follows:

$$2\text{Fe}(\text{OH})_2 + \frac{1}{2}O_2 + H_2O \longrightarrow \frac{2\text{Fe}(\text{OH})_3}{\text{(Ferric hydroxide) yellow rust}}$$

If O2 is limited, the corrosion product will be black anhydrous magnetite Fe2O4.

(6) Since the oxide film is porous in nature the surface of iron exposed to atmosphere acts as an anode while rest of a surface acts as a cathode.