

Extension of the entropy viscosity method to the
multi-D 7-equation two-phase flow model.
I do not know if we should have 'multi-D' in the title
since we will only present 1-D results

Marc O. Delchini^a, Jean C. Ragusa^{*,a}, Ray A. Berry^b

^a*Department of Nuclear Engineering, Texas A&M University, College Station, TX 77843,
USA*

^b*Idaho National Laboratory, Idaho Falls, ID 83415, USA*

Abstract

blabla

Key words: two-phase flow model, with variable area, entropy viscosity method, stabilization method, low Mach regime, shocks.

1. Introduction

- a few lines about the need for accurately resolving two-phase flows
- background on the different two-phase flow models: 5, 6 and 7-equation two-phase flow models
- then, focus on the different types of 7-equation two-phase flow models: they mostly differ because of the closure relaxations used
- discuss the different numerical solvers developed for the 7-equation two-phase flow model: HLL, HLLC, and approximated Riemann solvers accounting for the source terms
- emphasize the fact that the above numerical solvers only works on discontinuous schemes
- then, introduce the entropy viscosity method and details the organization of the paper

*Corresponding author

Email addresses: `delchmo@tamu.edu` (Marc O. Delchini), `jean.ragusa@tamu.edu` (Jean C. Ragusa), `ray.berry@inl.gov` (Ray A. Berry)

Compressible two-phase flows are found in numerous industrial applications and are an ongoing area of research in modeling and simulation over many years. A variety of models with different levels of complexity has been developed such as: five-equation model [1], six-equation model [2], and more recently the seven-equation model [3]. These models are all obtained by integrating the single-phase flow balance equations weighed by a characteristic or indicator function for each phase. The resulting system of equations contains non-conservative terms that describe the interaction between phases but also an equation for the volume fraction. Once a system of equations describing the physics is derived, the next challenging step is to develop a robust and accurate discretization to obtain a numerical solution. Assuming that the system of equations is hyperbolic under some conditions, a Riemann solver could be used but is often ruled out because of the complexity due to the number of equations involved. Furthermore, careless approximation for the treatment of the non-conservative terms can lead to failure in computing the numerical solution [4]. An alternative is to use an approximate Riemann solver, a well-established approach for single-phase flows, while deriving a consistent discretization scheme for the non-conservative terms.

This methodology was applied to the seven-equation model (SEM) introduced by Berry et al. in [3]. This model is known to be unconditionally hyperbolic which is highly desirable when working with approximate Riemann solvers and can treat a wide range of applications. Its particularity comes from the pressure and velocity relaxation terms in the volume fraction, momentum and energy equations that can bring the two phases in equilibrium when using large values of the relaxation parameters. In other words, the seven-equation model can degenerate into the six- and five-equation models. Alike for the other two-phase flow models, solving for the seven-equation model requires a numerical solver and significant effort was dedicated to this task for spatially discontinuous schemes. Because each phase is assumed to obey the Euler equations, most of the numerical solvers are adapted from the single-phase approximate Riemann solvers. For example, Saurel et al. [5, 6] employed a HLL-type scheme to solve for the SEM but noted that excessive dissipation was added to the contact discontinuity. A more advanced HLLC-type scheme was developed in [7] but only for the subsonic case and then extended to supersonic flows in [8]. More recently, Ambroso et al. [9] proposed an approximate Riemann solver accounting for source terms such as gravity and drag forces, but with no interphase mass transfer.

2. The multi-D 7-equation two-phase flow model

The multi-D seven-equation two-phase model presented in this paper is obtained by assuming that each phase obeys the single-phase Euler equations (with phase-exchange terms) and by integrating over a control volume after multiplying by a characteristic function. The detailed derivation can be found in [3]. In this section, the governing multi-dimensional equations are recalled for a phase k in interaction with a phase j . Each phase obeys the following mass,

momentum and energy balance equations, supplemented by a non-conservative volume-fraction equation:

$$\frac{\partial (\alpha \rho)_k A}{\partial t} + \nabla \cdot (\alpha \rho \mathbf{u} A)_k = -\Gamma A_{int} A \quad (1a)$$

$$\begin{aligned} \frac{\partial (\alpha \rho \mathbf{u})_k A}{\partial t} + \nabla \cdot [\alpha_k A (\rho \mathbf{u} \otimes \mathbf{u} + P \mathbb{I})_k] &= P_{int} A \nabla \alpha_k + P_k \alpha_k \nabla A \\ &+ A \lambda_u (\mathbf{u}_j - \mathbf{u}_k) - \Gamma A_{int} \mathbf{u}_{int} A \end{aligned} \quad (1b)$$

$$\begin{aligned} \frac{\partial (\alpha \rho E)_k A}{\partial t} + \nabla \cdot [\alpha_k \mathbf{u}_k A (\rho E + P)_k] &= P_{int} \mathbf{u}_{int} A \nabla \alpha_k - \bar{P}_{int} A \mu_P (P_k - P_j) \\ &+ \bar{\mathbf{u}}_{int} A \lambda_u (\mathbf{u}_j - \mathbf{u}_k) + \Gamma A_{int} \left(\frac{P_{int}}{\rho_{int}} - H_{k,int} \right) A \end{aligned} \quad (1c)$$

$$\frac{\partial \alpha_k A}{\partial t} + A \mathbf{u}_{int} \cdot \nabla \alpha_k = A \mu_P (P_k - P_j) - \frac{\Gamma A_{int} A}{\rho_{int}} \quad (1d)$$

where α_k , ρ_k , \mathbf{u}_k and E_k denote the volume fraction, the density, the velocity vector and the total specific energy of phase k , respectively. The phase pressure P_k is computed from an equation of state. The interfacial pressure and velocity and their corresponding average values are denoted by P_{int} , \mathbf{u}_{int} , \bar{P}_{int} and $\bar{\mathbf{u}}_{int}$, respectively, and are defined in Eq. (2).

$$P_{int} = \bar{P}_{int} + \frac{Z_k Z_j}{Z_k + Z_j} \frac{\nabla \alpha_k}{\|\nabla \alpha_k\|} \cdot (\mathbf{u}_j - \mathbf{u}_k) \quad (2a)$$

$$\bar{P}_{int} = \frac{Z_j P_k + Z_k P_j}{Z_k + Z_j} \quad (2b)$$

$$\mathbf{u}_{int} = \bar{\mathbf{u}}_{int} + \frac{\nabla \alpha_k}{\|\nabla \alpha_k\|} \frac{P_j - P_k}{Z_k + Z_j} \quad (2c)$$

$$\bar{\mathbf{u}}_{int} = \frac{Z_k \mathbf{u}_k + Z_j \mathbf{u}_j}{Z_k + Z_j}. \quad (2d)$$

The interfacial specific total enthalpy of phase k , H_k , is defined as follows: $H_k = h_k + 0.5 \|\mathbf{u}\|^2$. Following [3], the pressure and velocity relaxation coefficients, μ_P and λ_u respectively, are function of the acoustic impedance $Z_k = \rho_k c_k$ and the specific interfacial area A_{int} as shown in Eq. (3).

$$\lambda_u = \frac{1}{2} \mu_P Z_k Z_j \quad (3a)$$

$$\mu_P = \frac{A_{int}}{Z_k + Z_j} \quad (3b)$$

⁵² The specific interfacial area (i.e., the interfacial surface area per unit volume
⁵³ of two-phase mixture), A_{int} , must be specified from some type of flow regime

map or function under the form of a correlation. In [3], A_{int} is chosen to be a function of the liquid volume fraction:

$$A_{int} = A_{int}^{max} \left[6.75 (1 - \alpha_k)^2 \alpha_k \right], \quad (4)$$

where $A_{int}^{max} = 5100 \text{ m}^2/\text{m}^3$. With such definition, the interfacial area is zero in the limits $\alpha_k = 0$ and $\alpha_k = 1$. Lastly, Γ is the net mass transfer rate per unit interfacial area from phase j to phase k . Its expression, given in Eq. (5), is obtained by considering a vaporization/condensation process that is dominated by heat diffusion at the interface [3, 10]:

$$\begin{aligned} \Gamma = \Gamma_j &= \frac{h_{T,k} (T_k - T_{int}) + h_{T,j} (T_j - T_{int})}{h_{j,int} - h_{k,int}} \\ &= \frac{h_{T,k} (T_k - T_{int}) + h_{T,j} (T_j - T_{int})}{L_v (T_{int})}, \end{aligned} \quad (5)$$

where $L_v (T_{int}) = h_{j,int} - h_{k,int}$ represents the latent heat of vaporization. The interface temperature is determined by the saturation constraint $T_{int} = T_{sat}(P)$ with the appropriate pressure $P = \bar{P}_{int}$ determined above. The interfacial heat transfer coefficients for phases k and j are denoted by $h_{T,k}$ and $h_{T,j}$, respectively, and computed from correlations [3].

The set of equations obeyed by phase j are simply obtained by substituting k by j and j by k in Eq. (1), keeping the same definition of the interfacial variables and remembering that $\Gamma_j = -\Gamma_k$. In the case of two-phase flows, the equation for the volume fraction of phase j is simply replaced by the algebraic relation

$$\alpha_j = 1 - \alpha_k,$$

which reduces the number of equations from eight to seven and yields the seven-equation two-phase flow model.

The seven-equation model has interesting properties that are discussed next. A set of seven waves is present in such a model: two acoustic waves and a contact wave for each phase supplanted by a volume fraction wave propagating at the interfacial velocity \mathbf{u}_{int} . Considering a domain of dimension \mathbb{D} , the corresponding eigenvalues are the following for each phase k :

$$\begin{aligned} \lambda_1 &= \mathbf{u}_{int} \cdot \bar{\mathbf{n}} \\ \lambda_{2,k} &= \mathbf{u}_k \cdot \bar{\mathbf{n}} - c_k \\ \lambda_{3,k} &= \mathbf{u}_k \cdot \bar{\mathbf{n}} + c_k \\ \lambda_{d+3,k} &= \mathbf{u}_k \cdot \bar{\mathbf{n}} \text{ for } d = 1 \dots \mathbb{D}, \end{aligned} \quad (6)$$

where $\bar{\mathbf{n}}$ is an unit vector pointing to a given direction. The eigenvalues given in Eq. (6) are unconditionally real which presents an interesting property for the development of numerical methods since the system is hyperbolic and well-posed. To relax the seven-equation model to the ill-posed classical six-equation

model, only the pressures should be relaxed toward a single pressure for both phases. This is accomplished by specifying the pressure relaxation coefficient to be very large, i.e., letting it approach infinity. But if the pressure relaxation coefficient goes to infinity, so does the velocity relaxation rate also approach infinity. This then relaxes the seven-equation model not to the classical six-equation model but to the mechanical equilibrium five-equation model of Kapila [1]. This reduced five-equation model is also hyperbolic and well-posed. The five-equation model provides a very useful starting point for constructing multi-dimensional interface resolving methods which dynamically captures evolving and spontaneously generated interfaces [11]. Thus the seven-equation model can be relaxed locally to couple seamlessly with such a multi-dimensional, interface resolving code. Numerically, the mechanical relaxation coefficients μ_P (pressure) and λ_u (velocity) can be relaxed independently to yield solutions to useful, reduced models. It is noted, however, that relaxation of pressure only by making μ_P large without relaxing velocity will indeed give ill-posed and unstable numerical solutions, just as the classical six-equation two-phase model does, with sufficiently fine spatial resolution, as confirmed in [3, 12]. For each phase k , an entropy equation can be derived when accounting only for the pressure and velocity relaxation terms (all of the terms proportional to the net mass transfer term Γ are removed). The entropy function for a phase k is denoted by s_k and function of the density ρ_k and the internal energy e_k . The derivation is detailed in APPENDIX and only the final result is recalled here:

$$(s_e)_k^{-1} \alpha_k \rho_k A \frac{Ds_k}{Dt} = \mu_P \frac{Z_k}{Z_k + Z_j} (P_j - P_k)^2 + \lambda_u \frac{Z_j}{Z_k + Z_j} (\mathbf{u}_j - \mathbf{u}_k)^2 \\ \frac{Z_k}{(Z_k + Z_j)^2} \left[Z_j (\mathbf{u}_j - \mathbf{u}_k) + \frac{\nabla \alpha_k}{\|\nabla \alpha_k\|} (P_k - P_j) \right]^2, \quad (7)$$

63 The partial derivative of the entropy function s_k with respect to the internal
64 energy e_k , $(s_e)_k$, is shown to be proportional to the inverse of the temperature of
65 phase k , alike for the single phase Euler equations [13, 14]. The right hand-side
66 of Eq. (7) is unconditionally positive since all terms are squared and thus, is used
67 to demonstrate the entropy minimum principle and derive the dissipative terms.
68 Furthermore, Eq. (7) is valid for both phases $\{k, j\}$ and ensures positivity of
69 the total entropy equation that is obtained by summing over the phases:

$$\sum_k (s_e)_k^{-1} \alpha_k \rho_k A \frac{Ds_k}{Dt} = \sum_k (s_e)_k^{-1} \alpha_k \rho_k A (\partial_t s_k + \mathbf{u}_k \cdot \nabla s_k) \geq 0.$$

70 Note that when one phase disappears, Eq. (8) degenerates into the single phase
71 entropy equation [3, 14].

72 **3. A viscous regularization for the multi-D seven-equation two-phase** 73 **flow model**

- 74 • explain why we work with the phase entropy equation instead of consid-
75 ering the total entropy residual by summing over the two phases

- 76 • viscous regularization must be consistent with single-phase flow equation
- 77 • recall the notion of entropy condition and entropy inequality \rightarrow require
- 78 dissipative terms in order to get a sign
- 79 • give the system of equations with the dissipative terms
- 80 • guide the reader through the derivation of the dissipative terms
- 81 • give the entropy residual with all terms in the right hand-side
- 82 • make the link with the single-phase flow equations
- 83 • explain how to derive the dissipative term for the volume fraction equation
- 84 • emphasizes the fact that the regularization is valid for any EOS with
- 85 convex entropy
- 86 • a few words about the parabolic regularization

87 We now propose to derive a viscous regularization for the seven-equation model
 88 given in Eq. (1) by using the same methodology as for the multi-D Euler equa-
 89 tions with/without variable area [13, 15]. The method consists in adding per-
 90 turbation terms to the system of equation under consideration, and re-derive
 91 the entropy equation whose sign is known to be positive to ensure unique-
 92 ness of the numerical solution [16]. Because of the addition of perturbation
 93 terms, the entropy equation is modified and contains extra terms of unknown
 94 sign. By carefully choosing a definition for each of the perturbation term, the
 95 sign of the entropy equation can be determined and proved positive. For the
 96 seven-equation model, derivation of a viscous regularization can be achieved by
 97 considering either the phasic entropy equation (Eq. (7)) or the total entropy
 98 equation (Eq. (8)). In the later case, the entropy minimum principle is verified
 99 for the whole system which may not ensure positivity of the entropy equation
 100 for each phase. However, positivity of the total entropy equation can be also
 101 achieved by assuming that the entropy minimum principle holds for each phase.
 102 This stronger requirement will also ensure consistency with the single phase
 103 Euler equations when one of the phase disappears in the limits $\alpha_k \rightarrow 0$ and
 104 $\alpha_k \rightarrow 1$. Thus, it is chosen to work with the phasic entropy equations.

For the purpose of this section, the system of equations given in Eq. (8) is considered which is obtained by simply omitting the mass source terms (terms proportional to Γ) in Eq. (1).

$$\partial_t (\alpha_k A) + A \mathbf{u}_{int} \cdot \nabla \alpha_k = A \mu_P (P_k - P_j) \quad (8a)$$

$$\partial_t (\alpha_k \rho_k A) + \nabla \cdot (\alpha_k \rho_k \mathbf{u}_k A) = 0 \quad (8b)$$

$$\begin{aligned} \partial_t (\alpha_k \rho_k u_k A) + \nabla \cdot [\alpha_k A (\rho_k \mathbf{u}_k \otimes \mathbf{u}_k + P_k \mathbb{I})] = \\ \alpha_k P_k \nabla A + P_{int} A \nabla \alpha_k + A \lambda_u (\mathbf{u}_j - \mathbf{u}_k) \end{aligned} \quad (8c)$$

$$\begin{aligned} \partial_t (\alpha_k \rho_k E_k A) + \nabla \cdot [\alpha_k A \mathbf{u}_k (\rho_k E_k + P_k)] = \\ AP_{int} \mathbf{u}_{int} \cdot \nabla \alpha_k - \mu_P \bar{P}_{int} (P_k - P_j) + A \lambda_u \bar{\mathbf{u}}_{int} \cdot (\mathbf{u}_j - \mathbf{u}_k) \end{aligned} \quad (8d)$$

In order to apply the entropy viscosity method, perturbation terms are added to each equation of Eq. (8), which yields:

$$\partial_t (\alpha_k A) + \mathbf{u}_{int} A \nabla \alpha_k = A \mu_P (P_k - P_j) + \nabla \cdot \mathbf{l}_k \quad (9a)$$

$$\partial_t (\alpha_k \rho_k A) + \nabla \cdot (\alpha_k \rho_k \mathbf{u}_k A) = \nabla \cdot \mathbf{f}_k \quad (9b)$$

$$\begin{aligned} \partial_t (\alpha_k \rho_k \mathbf{u}_k A) + \nabla \cdot [\alpha_k A (\rho_k \mathbf{u}_k \otimes \mathbf{u}_k + P_k \mathbb{I})] = \\ \alpha_k P_k \nabla A + P_{int} A \nabla \alpha_k + A \lambda_u (\mathbf{u}_j - \mathbf{u}_k) + \nabla \cdot \mathbf{g}_k \end{aligned} \quad (9c)$$

$$\begin{aligned} \partial_t (\alpha_k \rho_k E_k A) + \nabla \cdot [\alpha_k A \mathbf{u}_k (\rho_k E_k + P_k)] = \\ P_{int} A \mathbf{u}_{int} \cdot \nabla \alpha_k - \mu_P \bar{P}_{int} (P_k - P_j) + A \lambda_u \bar{\mathbf{u}}_{int} \cdot (\mathbf{u}_j - \mathbf{u}_k) \\ + \nabla \cdot (\mathbf{h}_k + \mathbf{u} \cdot \mathbf{g}_k) \end{aligned} \quad (9d)$$

where \mathbf{f}_k , \mathbf{g}_k , \mathbf{h}_k and \mathbf{l}_k are the phasic perturbation terms. The next step consists in deriving the entropy equation for the phase k , on the same model as what is done in Appendix A:

1. derive the density and internal energy equations from Eq. (9).
2. assuming that the phasic entropy, s_k , is function of the density, ρ_k and the internal energy, e_k , derive the entropy equation by using the chain rule:

$$\frac{Ds_k}{Dt} = (s_\rho)_k \frac{D\rho_k}{Dt} + (s_e)_k \frac{De_k}{Dt} \quad (10)$$

- where $\frac{D}{Dt}$ is the material derivative. The terms $(s_e)_k$ and $(s_\rho)_k$ denote the partial derivative of the entropy s_k with respect to e_k and ρ_k , respectively.
3. isolate the terms of interest and choose an appropriate expression for each of the perturbation terms in order to ensure positivity of the right-hand side.

We first derive the density equation for the primitive variable ρ_k by combining Eq. (9a) and Eq. (9b) to obtain:

$$\alpha_k A \left[\partial_t \rho_k + (\mathbf{u}_k - \underline{\mathbf{u}_{int}}) \cdot \nabla \rho_k \right] = \underline{\underline{A \rho_k \mu_P (P_k - P_j)}} + \nabla \cdot \mathbf{f}_k - \rho_k \nabla \cdot \mathbf{l}_k \quad (11)$$

In order to derive the internal energy equation, the velocity equation is obtained by subtracting the density equation from the momentum equation:

$$\begin{aligned} \alpha_k \rho_k A [\partial_t \mathbf{u}_k + \mathbf{u}_k \cdot \nabla \mathbf{u}_k] + \nabla \cdot (\alpha_k \rho_k A P_k \mathbb{I}) = \\ \underline{\underline{\alpha_k P_k \nabla A + P_{int} A \nabla \alpha_k + A \lambda (\mathbf{u}_j - \mathbf{u}_k)}} + \nabla \cdot \mathbf{g}_k - \mathbf{u}_k \otimes \mathbf{f}_k \end{aligned} \quad (12)$$

After multiplying Eq. (12) by the velocity vector \mathbf{u}_k , the resulting kinetic energy equation is subtracted from the total energy equation to obtain the internal energy equation for phase k :

$$\begin{aligned} \alpha_k \rho_k A [\partial_t \mathbf{e}_k + \mathbf{u}_k \cdot \nabla \cdot \mathbf{e}_k] + \alpha_k \rho_k A P_k \nabla \mathbf{u}_k = \\ \underline{\underline{P_{int} A (\mathbf{u}_{int} - \mathbf{u}_k) \cdot \nabla \alpha_k - \alpha_k P_k \mathbf{u}_k \nabla A}} \\ \underline{\underline{-\bar{P}_{int} A \mu_P (P_k - P_j) + A \lambda_u (\mathbf{u}_j - \mathbf{u}_k) \cdot (\bar{\mathbf{u}}_{int} - \mathbf{u}_k)}} \\ + \nabla \cdot \mathbf{h}_k + \mathbf{g}_k : \nabla \mathbf{u}_k + \|\mathbf{u}\|_k^2 \mathbf{f}_k \end{aligned} \quad (13)$$

The underline terms in Eq. (11) and Eq. (13) yield the positive terms in the right-hand-side of Eq. (7) and thus are ignored in the remaining of the derivation for simplicity. The entropy equation is now obtained by combining the density equation (Eq. (11)) and the internal energy equation (Eq. (13)) through the chain rule given in Eq. (10) to yield:

$$\begin{aligned} \alpha_k \rho_k A \frac{Ds_k}{Dt} = (\rho s_\rho)_k [\nabla \cdot \mathbf{f}_k - \rho_k \nabla \cdot \mathbf{l}_k] + \\ (s_e)_k [\nabla \cdot \mathbf{h}_k + \mathbf{g}_k : \nabla \mathbf{u}_k + (\|\mathbf{u}\|_k^2 - e_k) \nabla \cdot \mathbf{f}_k], \end{aligned} \quad (14)$$

where it was assumed that the entropy of phase k satisfies the second thermodynamic law:

$$\begin{aligned} T_k ds_k = de_k - P_k \frac{d\rho_k}{\rho_k^2} \\ \text{which implies } P_k (s_e)_k + \rho_k (s_\rho)_k = 0, \\ (s_e)_k = T_k^{-1} \text{ and } (s_\rho)_k = -(s_e)_k P_k \frac{d\rho_k}{\rho_k^2}. \end{aligned} \quad (15)$$

Following the methodology applied in [13, 15], the right-hand side of Eq. (14) can be further simplified by using the following expression for the dissipative terms \mathbf{f}_k , \mathbf{g}_k and \mathbf{h}_k :

$$\mathbf{f}_k = \tilde{\mathbf{f}}_k + \rho_k \mathbf{l}_k \quad (16a)$$

$$\mathbf{g}_k = \alpha_k \rho_k A \mu_k \mathbb{F}(\mathbf{u}_k) + \mathbf{f}_k \otimes \mathbf{u}_k \quad (16b)$$

$$\mathbf{h}_k = \tilde{\mathbf{h}}_k - \frac{\|\mathbf{u}\|^2}{2} \mathbf{f}_k + (\rho e)_k \mathbf{l}_k, \quad (16c)$$

where μ_k is a positive viscosity coefficient for phase k . Note the area function A in the definition of \mathbf{g} . Substituting the expression of the dissipative term given in Eq. (16) into Eq. (14), it yields:

$$\begin{aligned} \alpha_k \rho_k A \frac{Ds_k}{Dt} = \\ \underbrace{(s_e)_k \alpha_k \rho_k A \mu_k \mathbb{F}(\mathbf{u}_k) : \nabla \mathbf{u}_k}_{\mathcal{R}_1} + \underbrace{[\nabla \cdot \tilde{\mathbf{h}}_k - e_k \nabla \cdot \tilde{\mathbf{f}}_k]}_{\mathcal{R}_2} + (\rho s_\rho)_k \nabla \cdot \tilde{\mathbf{f}}_k + \\ \underbrace{(s_e)_k \nabla \cdot (\rho_k e_k \mathbf{l}_k) - (s_e)_k e_k \nabla \cdot (\rho_k \mathbf{l}_k) + \rho_k (s_\rho)_k \nabla \cdot (\rho_k \mathbf{l}_k) - \rho_k^2 (s_\rho)_k \nabla \cdot \mathbf{l}_k}_{\mathcal{R}_3}. \end{aligned} \quad (17)$$

We now split the right-hand-side of Eq. (17) into three residuals denoted by \mathcal{R}_1 , \mathcal{R}_2 and \mathcal{R}_3 and will study the sign of each of them. Since $(s_e)_k$ is defined as the inverse of the temperature and thus positive, the sign of the first term, \mathcal{R}_1 , is conditioned by the choice of the function $\mathbb{F}(\mathbf{u}_k)$ so that the product with the tensor $\nabla \mathbf{u}_k$ is positive. As in [13, 15], $\mathbb{F}(\mathbf{u}_k)$ is chosen proportional to the symmetric gradient of the velocity vector $\nabla^s \mathbf{u}_k$, whose entries are given by $((\nabla^s \mathbf{u})_{i,j})_k = \frac{1}{2} (\partial_{x_i} u_j + \partial_{x_j} u_i)_k$. After a few lines of algebra, the third term \mathcal{R}_3 can be recast as a function of the gradient of the entropy as follows:

$$\mathcal{R}_2 = \rho_k A l_k \cdot \nabla s_k. \quad (18)$$

118 One of the assumptions made in the entropy minimum principle is that the
 119 entropy is at a minimum which implies that its gradient is null. Because of
 120 this, it follows that the term \mathcal{R}_3 is zero at the minimum and thus, the entropy
 121 minimum principle is verified independently of the definition of the perturbation
 122 term l_k used in the volume fraction equation Eq. (9a). It will be explained later
 123 in this section how to derive a definition for l_k .

We now focus on the term denoted by \mathcal{R}_2 , that is found identical to the right-hand-side of the single phase entropy equation obtained from the multi-D Euler equations (see [13, 15]). Thus, the term \mathcal{R}_2 is known to be positive when (i) assuming concavity of the entropy function s_k with respect to the internal energy e_k and the specific volume $1/\rho_k$ (or convexity of $-s_k$) and (ii) choosing the following definitions for the dissipative terms \tilde{h}_k and \tilde{f}_k :

$$\tilde{f}_k = \alpha_k A \kappa_k \nabla \rho_k \quad (19a)$$

$$\tilde{h}_k = \alpha_k A \kappa_k \nabla (\rho e)_k, \quad (19b)$$

where κ_k is another positive viscosity coefficient. The entropy equation can now be written in its final form:

$$\begin{aligned} \alpha_k \rho_k A \frac{Ds_k}{Dt} &= \tilde{f}_k \cdot \nabla s_k + \nabla \cdot (\alpha_k \rho_k A \nabla s_k) \\ &\quad - \alpha_k A \kappa_k \mathbf{Q}_k + (s_e)_k \alpha_k A \rho_k \mu_k \nabla^s \mathbf{u}_k : \nabla \mathbf{u}_k, \end{aligned} \quad (20)$$

124 where \mathbf{Q}_k is a negative semi-definite quadratic form defined as:

$$\begin{aligned} \mathbf{Q}_k &= X_k^t \Sigma_k X_k \\ \text{with } X_k &= \begin{bmatrix} \nabla \rho_k \\ \nabla e_k \end{bmatrix} \text{ and } \Sigma_k = \begin{bmatrix} \partial_{\rho_k} (\rho_k^2 \partial_{\rho_k} s_k) & \partial_{\rho_k, e_k} s_k \\ \partial_{\rho_k, e_k} s_k & \partial_{e_k, e_k} s_k \end{bmatrix}. \end{aligned}$$

125 Eq. (20) is used to prove the entropy minimum principle: assuming that s_k
 126 reaches its minimum value in $\mathbf{r}_{min}(t)$ at each time t , the gradient, ∇s_k , and
 127 Laplacian, Δs_k , of the entropy are null and positive at this particular point,
 128 respectively. Furthermore, it is recalled that the viscosity coefficients μ_k and
 129 κ_k are positive by definition. Then, because the terms in the right-hand-side of
 130 Eq. (20) are proven either positive or null when the entropy reaches a minimum

value, the entropy minimum principle holds for each phase k , **independently of the definition of the dissipative term \mathbf{l}_k** , such as:

$$\alpha_k \rho_k A \partial_t s_k(\mathbf{r}_{min}, t) \geq 0 \Rightarrow \partial_t s_k(\mathbf{r}_{min}, t) \geq 0$$

Do we need to make the above statement a theorem or property?

It remains to obtain a definition for the dissipative term \mathbf{l}_k used in the volume fraction equation Eq. (9a). A way to achieve this is to consider the volume fraction equation, by itself and notice that it is an hyperbolic equation with eigenvalue \mathbf{u}_{int} . An entropy equation can be derived and used to prove the entropy minimum principle by properly choosing the dissipative term [16]. The objective is to ensure positivity of the volume fraction and also uniqueness of the weak solution. Following the work of Guermond et al. in [17, 18], it can be shown that a dissipative term ensuring positivity and uniqueness of the weak solution for the volume fraction equation, is of the form $\mathbf{l}_k = \beta_k A \nabla \alpha_k$, where β_k is a positive viscosity coefficient. The dissipative term is proportional to the area A for consistency with the other terms of the volume fraction equation Eq. (9a).

All of the dissipative terms are now defined and recalled here:

$$\mathbf{l}_k = \beta_k A \nabla \alpha_k \quad (21a)$$

$$\mathbf{f}_k = \alpha_k A \kappa_k \nabla \rho_k + \rho_k A \mathbf{l}_k \quad (21b)$$

$$\mathbf{g}_k = \alpha_k A \mu_k \rho \nabla^s \mathbf{u}_k \quad (21c)$$

$$\mathbf{h}_k = \alpha_k A \kappa_k \nabla (\rho e)_k + \mathbf{u}_k : \mathbf{g}_k - \frac{\|\mathbf{u}_k\|^2}{2} \mathbf{f}_k + (\rho e)_k \mathbf{l}_k \quad (21d)$$

At this point, some remarks are in order:

1. The viscous regularization given in Eq. (21) for the multi-D seven-equation model, is equivalent to the parabolic regularization [19] when assuming $\beta_k = \kappa_k = \mu_k$ and $\mathbb{F}(\mathbf{u}_k) = \alpha_k \rho_k \kappa_k \nabla \mathbf{u}_k$. However, decoupling between the regularization on the velocity and on the density in the momentum equation is important to make the regularization rotation invariant but also to ensure well-scaled dissipative terms for a wide range of Mach number as was shown in [15] for the multi-D Euler equations.
2. The dissipative term \mathbf{l}_k requires the definition of a new viscosity coefficient β_k . It was shown that this viscosity coefficient is independent of the other viscosity coefficients μ_k and κ_k . Its definition should account for the eigenvalue associated with the void fraction equation \mathbf{u}_{int} .
3. The dissipative term \mathbf{f}_k is a function of \mathbf{l}_k . Thus, all of the other dissipative terms are also functions of \mathbf{l}_k .
4. The partial derivatives $(s_e)_k$ and $(s_{\rho_k})_k$ can be computed using the definition provided in Eq. (15) and are functions of the thermodynamic variables: pressure, temperature and density.

- 163 5. All of the dissipative terms are chosen to be proportional to the the void
 164 fraction α_k and the cross-sectional area A , but the one in the volume
 165 fraction equation that is only proportional to A . For instance, $\alpha_k A \nabla \rho_k$
 166 is the flux of the dissipative term in the continuity equation through the
 167 phasic area, $\alpha_k A$, seen by the phase k . When one of the phases disappears,
 168 the dissipative terms must go to zero for consistency. On the other hand,
 169 when α_k goes to one, the single-phase Euler equations with proper viscous
 170 regularization must be recovered.
- 171 6. Compatibility of the viscous regularization proposed in Eq. (21) with the
 172 generalized entropies identified in Harten et al. [20] has not been investi-
 173 gated yet. However, it is believed that the entropy inequalities still holds
 174 because of the similarities of the entropy residual for the multi-D seven-
 175 equation model with the entropy residual derived in the single phase flow
 176 case [13].

177 At this point in the paper, we have derived a viscous regularization for the multi-
 178 D seven-equation two-phase flow model that ensures positivity of the entropy
 179 residual and also uniqueness of the numerical solution when assuming concavity
 180 of the phasic entropy s_k . The viscous regularization involves a set of three
 181 viscosity coefficients for each phase, μ_k , κ_k and β_k , that are assumed positive.
 182 Definition of the viscosity coefficients is now required to complete the numerical
 183 stabilization method. Since the focus of this paper is the entropy viscosity
 184 method, the viscosity coefficients are defined function of the entropy residual
 185 as it will be shown in Section 4. However, one can also devise a definition
 186 for the viscosity coefficients μ_k and κ_k by analogy to Lapidus [21, 22] or some
 187 pressure-based methods [23] used for the single-phase Euler equations. The
 188 viscosity coefficient, β_k , for the volume fraction equation should rely on artificial
 189 dissipation stabilization method used for scalar hyperbolic equations.

Remark. *Through the derivations of the viscous regularization, it was noted that another set of dissipative terms \mathbf{f}_k and \mathbf{l}_k would also ensures positivity of the entropy residual:*

$$\mathbf{l}_k = \beta_k T_k \left[\frac{\rho_k}{P_k + \rho_k e_k} \nabla \left(\frac{P_k}{\rho_k e_k} \right) - \frac{1}{P_k} \nabla \rho_k \right] \quad (22a)$$

$$\mathbf{f}_k = \kappa_k \nabla \rho_k + \frac{\rho_k^2 (s_\rho)_k}{(\rho s_\rho - e s_e)_k} \mathbf{l}_k \quad (22b)$$

190 *However, the definition of \mathbf{l}_k proposed in Eq. (22a) was not considered as valid*
 191 *for the following reasons: positivity of the volume fraction cannot be achieved*
 192 *and the parabolic regularization is not retrieved.*

193 4. A definition of the viscosity coefficients for all Mach flows

- 194 • non-dimensionalize the equations but use P_∞ for the pressure instead of
 195 $(\rho c^2)_\infty$

- 196 • introduce a new Pechlet number for β : its behavior should be the same
197 as the Pechlet number for κ
- 198 • two cases: zero and infinite relaxation coefficients
- 199 • derive the normalization parameters for the isentropic and non-isentropic
200 flows
- 201 • discussion about the

202 This section aims at deriving a definition of the viscosity coefficients involved in
203 the viscous regularization for the multi-D seven-equation model. We propose to
204 follow the same methodology as in SECTION for the multi-D Euler equations:
205 after obtaining the non-dimensional equations, a definition for the viscosity
206 coefficients is derived based on the entropy residual and consistent with the
207 low-Mach asymptotic limit. Particular attention is paid to the definition of the
208 viscosity coefficient β_k used in the volume fraction equation.

209 Using the EVM to define the viscosity coefficients is not the unique option
210 here. Other numerical methods initially developed for single-phase flows, such
211 as pressure-based and Lapidus viscosity methods, could be used as a starting
212 point and adapted to the seven-equation model. Such a reasoning is motivated
213 by one of the initial assumptions of the seven-equation model that assumes each
214 phase verifies the Euler equations.

215 4.1. Definition of the viscosity coefficients

The viscous regularization derived in SECTION for the multi-D SEM re-
quires three viscosity coefficients for each phase k denoted by β_k , μ_k and κ_k .
Following the methodology detailed in SECTION, for each viscosity coefficient
an upper bound, denoted by the subscript *max*, is defined and referred to as the
first-order viscosity coefficient, along with a entropy viscosity coefficient that is
set proportional to an entropy residual and denoted by the subscript *e*:

$$\begin{aligned}\beta_k(\mathbf{r}, t) &= \min(\beta_{e,k}(\mathbf{r}, t), \beta_{max,k}(\mathbf{r}, t)), \\ \mu_k(\mathbf{r}, t) &= \min(\mu_{e,k}(\mathbf{r}, t), \mu_{max,k}(\mathbf{r}, t)), \\ \kappa_k(\mathbf{r}, t) &= \min(\kappa_{e,k}(\mathbf{r}, t), \kappa_{max,k}(\mathbf{r}, t)).\end{aligned}$$

216 where all of the variables are locally defined. As for the multi-D single-phase
217 Euler equations and for the same reasons, the entropy residual for each phase
218 k is recast as a function of the pressure, the velocity, the density and the speed
219 of sound as follows:

$$R_k(\mathbf{r}, t) := \partial_t s_k + \mathbf{u}_k \cdot \nabla s_k = \frac{Ds_k}{Dt} = \frac{(s_e)_k}{(P_e)_k} \underbrace{\left(\frac{DP_k}{Dt} - c_k^2 \frac{D\rho_k}{Dt} \right)}_{\tilde{R}_k(\mathbf{r}, t)}, \quad (23)$$

220 where $\tilde{R}_k(\mathbf{r}, t)$ is the new entropy residual of phase k and will experience the
221 same variations as $R_k(\mathbf{r}, t)$.

222 We first choose to investigate the definitions of the high and first-order vis-
 223 cosity coefficients for μ_k and κ_k . It is noted that the dissipative terms function
 224 of μ_k and κ_k are the same as the ones for the single-phase Euler equation when
 225 considering $\tilde{A} = \alpha_k A$ as a pseudo cross section. Furthermore, we need to ensure
 226 consistency with the single-phase Euler equation in the limits $\alpha_k \rightarrow 1$. Thus,
 227 based on the work done in SECTION, the first order viscosity coefficients are
 228 set proportional to the local maximum eigenvalue λ_k ,

$$\kappa_{max,k}(\mathbf{r}, t) = \mu_{max,k}(\mathbf{r}, t) = \frac{h}{2} (||\mathbf{u}_k|| + c_k) \quad (24)$$

229 and the entropy viscosity viscosity coefficients are defined as

$$\mu_{e,k}(\mathbf{r}, t) = h^2 \frac{\max \left(|\tilde{R}_k(\mathbf{r}_q, t)|, ||\mathbf{u}_k(\mathbf{r}_q, t)|| J[P_k](t), ||\mathbf{u}_k(\mathbf{r}_q, t)|| c_k^2(\mathbf{r}_q, t) J[\rho_k](t) \right)}{\text{norm}_{P,k}^\mu}, \quad (25a)$$

230 and

$$\kappa_{e,k}(\mathbf{r}, t) = h^2 \frac{\max \left(|\tilde{R}_k(\mathbf{r}_q, t)|, ||\mathbf{u}_k(\mathbf{r}_q, t)|| J[P_k](t), ||\mathbf{u}_k(\mathbf{r}_q, t)|| c_k^2(\mathbf{r}_q, t) J[\rho_k](t) \right)}{\text{norm}_{P,k}^\kappa}. \quad (25b)$$

231 where h is the grid size and $J[x](t)$ denotes the jump of the quantity x and was
 232 defined in SECTION. The normalization parameters $\text{norm}_{P,k}^\mu$ and $\text{norm}_{P,k}^\kappa$ will
 233 be determined later in this section by inspecting the non-dimensional version of
 234 the seven-equation model.

235 It remains to specify the viscosity coefficients β_e and β_{max} . For the purpose
 236 of this paragraph, let us consider the scalar volume fraction equation and as-
 237 sume that the interface velocity \mathbf{u}_{int} is given. Because it is a scalar hyperbolic
 238 equation, it is proposed to define the high and first-order viscosity coefficients
 239 on the same model as Burger's equation. Thus, β_{max} is set proportional to the
 240 eigenvalue that is the interface velocity \mathbf{u}_{int} ,

$$\beta_{max,k}(\mathbf{r}, t) = \frac{h}{2} ||\mathbf{u}_{int}||, \quad (26)$$

whereas the entropy viscosity viscosity coefficient β_e is function of an entropy
 residual, $R_{\alpha,k}$, derived from the volume fraction equation for phase k as follows:

$$\beta_{e,k}(\mathbf{r}, t) = h^2 \frac{\max (|R_{\alpha,k}(\mathbf{r}_q, t)|, ||\mathbf{u}_{int}(\mathbf{r}_q, t)|| J[\alpha_k](t))}{\text{norm}_k^\beta} \quad (27)$$

241 where norm_k^β denotes a normalization parameters whom definition will be fur-
 242 ther investigated. To derive the entropy residual $R_{\alpha,k}$, we consider the volume
 243 fraction equation for phase k with its viscous regularization and assume the
 244 existence of a mathematical entropy denoted by $\eta(\alpha_k)$:

$$\partial_t (A\alpha_k) + A\mathbf{u}_{int} \cdot \nabla \alpha_k = \nabla \cdot (\beta_k A \nabla \alpha_k) \quad (28)$$

245 After multiplying by $\frac{d\eta(\alpha_k)}{d\alpha_k}$ and using the chain rule, an expression for the
 246 entropy residual $R_{\alpha,k}$ is obtained:

$$R_{\alpha,k} = \partial_t (A\eta(\alpha_k)) + A\mathbf{u}_{int} \cdot \nabla \eta(\alpha_k) = \frac{d\eta(\alpha_k)}{d\alpha_k} \nabla \cdot (\beta_k A \nabla \alpha_k) \quad (29)$$

247 Because Eq. (29) is identical to Eq. (??), it is concluded that $R_{\alpha,k} \geq 0$ when
 248 assuming η convex with respect to α_k , which justifies the definition of the en-
 249 tropy viscosity coefficient $\beta_{e,k}$ given in Eq. (27) based on Eq. (??).
 250 The entropy function is taken equal to $\eta(\alpha_k) = \frac{\alpha_k^2}{2}$ which is convex.

251 4.2. Low-Mach asymptotic limit of the seven-equation model

252 In order to have a complete definition for the viscosity coefficients β_k , μ_k and
 253 κ_k , the normalization parameters introduced in the definition of the entropy vis-
 254 cosity coefficients $\beta_{e,k}$, $\mu_{e,k}$ and $\kappa_{e,k}$ have to be determined. In SECTION, the
 255 normalization parameters were derived from the non-dimensionalized multi-D
 256 Euler equations in order to obtain well-scaled dissipative terms. Thus, it is pro-
 257 posed to follow the same method to derive the three normalization parameters
 258 $\text{norm}_{P,k}^\mu$, $\text{norm}_{P,k}^\kappa$ and $\text{norm}_{P,k}^\beta$ used in the definition of the viscosity coefficients
 259 involved in the viscous regularization of the seven-equation model. For simplic-
 260 ity, the Ideal Gas equation of state is considered through the derivations.

261 For now, the definition of the viscosity coefficients is simply derived by anal-
 262 ogy to SECTION. First, we define the far-field or stagnation coefficients for
 263 each phase as it is done in Eq. (??) by adding the subscript k to ∞ . Then, the
 264 scaled equations are derived for each phase which leads to the definition of a
 265 phasic Péclet and Reynolds numbers referred to as Pé_k and Re_k , respectively,
 266 that are tied to the far-field or stagnation quantities of the viscosity coefficients
 267 $\mu_{k,\infty}$ and $\kappa_{k,\infty}$ as shown in Eq. (30):

$$\text{Re}_{k,\infty} = \frac{u_{k,\infty} L_\infty}{\mu_{k,\infty}} \text{ and } \text{Pé}_{k,\infty} = \frac{u_{k,\infty} L_\infty}{\kappa_{k,\infty}}. \quad (30)$$

268 Because the viscous regularization derived previously in SECTION requires an
 269 extra viscosity coefficient β_k for the volume fraction equation, a new Péclet
 270 number, $\text{Pé}_{k,\infty}^\beta$ is also defined as follows,

$$\text{Pé}_{k,\infty}^\beta = \frac{u_{int,\infty} L_\infty}{\beta_{k,\infty}} \quad (31)$$

271 that will allow us to derive the proper scaling for $\beta_{k,\infty}$. Once the scaled equa-
 272 tions are obtained, the scaling of the numerical numbers can be chosen in order
 273 to meet the different criteria already listed in SECTION. The scaling of the
 274 new Péclet number we defined, $\text{Pé}_{k,\infty}^\beta$, is derived from the scaled volume frac-
 275 tion equation that does not contain any term weighted by the reference Mach
 276 number M_∞ , which yields $\text{Pé}_{k,\infty}^\beta = 1$ to have a well-scaled dissipative term.
 277 This scaling is the same as for $\text{Pé}_{k,\infty}$ from the continuity equation: the vol-
 278 ume fraction and continuity equations have similar behavior since they are both

279 advection-type equations. Thus, based on the reasoning used in SECTION, the
 280 following definitions for the viscosity coefficients is proposed in Eq. (32):

$$\mu_k(\mathbf{r}, t) = \min \left(\mu_{\max,k}(\mathbf{r}, t), \mu_{e,k}(\mathbf{r}, t) \right) \text{ and } \kappa_k(\mathbf{r}, t) = \min \left(\mu_{\max,k}(\mathbf{r}, t), \kappa_{e,k}(\mathbf{r}, t) \right) \quad (32a)$$

281 where the first-order viscosity is given by

$$\kappa_{\max,k}(\mathbf{r}, t) = \mu_{\max,k}(\mathbf{r}, t) = \frac{h}{2} \left(\|\mathbf{u}_k\| + c_k \right) \quad (32b)$$

282 and the entropy viscosity coefficients by

$$\kappa_{e,k}(\mathbf{r}, t) = \frac{h^2 \max(\tilde{R}_k, J_k)}{\rho_k c_k^2} \text{ and } \mu_{e,k}(\mathbf{r}, t) = \frac{h^2 \max(\tilde{R}_k, J_k)}{\text{norm}_{P,k}^\mu} \quad (32c)$$

283 with the jumps given by

$$J_k = \max \left(\|\mathbf{u}_k\| [[\nabla P_k \cdot \mathbf{n}]], \|\mathbf{u}_k\| c_k^2 [[\nabla \rho_k \cdot \mathbf{n}]] \right) \quad (32d)$$

284 where $\text{norm}_{P,k}^\kappa$ is computed from Eq. (33).

$$\text{norm}_P^\mu = (1 - \sigma(M)) \rho c^2 + \sigma(M) \rho \|\mathbf{u}\|^2 \quad (33)$$

285 where M_k is the local Mach number for phase k . The function $\sigma(M)$ is taken
 286 from Eq. (??) with the same parameters as for the single-phase flow equations:
 287 $a = 3$ and $M^{thres} = 0.05$. The jump J_k is a function of the jump of pressure
 288 and density gradients across the face with respect to its normal vector \mathbf{n} . Then,
 289 the largest value over all faces is determined and used in the definition of the
 290 viscosity coefficients. Lastly, the viscosity coefficient for the volume fraction
 291 equation is given by:

$$\beta_k(\mathbf{r}, t) = \min \left(\beta_{\max,k}(\mathbf{r}, t), \beta_{e,k}(\mathbf{r}, t) \right) \quad (34)$$

292 where the first-order viscosity is given by

$$\beta_{\max,k}(\mathbf{r}, t) = \frac{h}{2} \|\mathbf{u}_{int}\| \quad (35)$$

293 and the corresponding entropy viscosity coefficient, $\beta_{e,k}$, by

$$\beta_{e,k}(\mathbf{r}, t) = \frac{h^2 \max(R_{\alpha,k}, J_{\alpha,k})}{\|\alpha_k - \bar{\alpha}_k\|_\infty}, \quad (36)$$

294 where $\bar{\alpha}_k$ is the average value of the volume fraction over the entire computa-
 295 tional domain, and $\|\cdot\|_\infty$ denotes the infinite norm. The definition of the $\beta_{e,k}$
 296 is consistent with the scaling of $\text{Pé}_{k,\infty}^\beta = 1$. The jump is given by:

$$J_{\alpha,k} = \|\mathbf{u}_{int}\| \cdot [[\nabla \alpha_k \cdot \mathbf{n}]]. \quad (37)$$

297 With the definition of the viscosity coefficients μ_k and κ_k proposed in Eq. (??),
 298 the low-Mach asymptotic limit is ensured for isentropic flow, and transonic
 299 flows with shocks will be correctly resolved for each phase k . Furthermore,
 300 the definition of the viscosity coefficient β_k is consistent with the EVM used
 301 for the scalar hyperbolic equations and thus should efficiently stabilize shocks
 302 forming the in the volume fraction profile. Plus, it is noted that the viscous
 303 regularization and the definition of the viscosity coefficients proposed for the
 304 seven-equation two-phase flow model degenerates into the EVM used for the
 305 single-phase Euler equations. In order to validate the proposed definition of the
 306 viscosity coefficients, 1-D numerical simulations are performed in SECTION.

307 5. 1-D numerical results

- 308 • simple advection problem
- 309 • shock tube with two independent fluids: exact solution and could do con-
 310 vergence test for this particular test
- 311 • shock tube with infinite relaxation coefficients
- 312 • 1-D nozzle with two independent fluids
- 313 • 1-D nozzle with infinite relaxation coefficients
- 314 • 1-D nozzle with infinite relaxation coefficients, mass and heat transfer

315 References

- 316 [1] A. K. Kapila, R. Menikoff, J. B. B. S. F. Son, D. S. Stewart, Two-phase
 317 modeling of deflagration-to-detonation transition in granular materials,
 318 Phys. Fluids (2001) 3002–3024.
- 319 [2] I. Toumi, An upwind numerical method for two-fluids two-phases flow mod-
 320 els, Nucl. Sci. Eng. (1996) 147–168.
- 321 [3] R. Berry, R. Saurel, O. LeMetayer, The discrete equation method (dem)
 322 for fully compressible, two-phase flows in ducts of spatially varying cross-
 323 section, Nuclear Engineering and Design 240 (2010) 3797–3818.
- 324 [4] R. Abgrall, How to prevent pressure oscillations in multicomponent flow
 325 calcuations: a quasi conservative appraoch, J. Comput. Phys (2002) 125–
 326 150.
- 327 [5] R. Saurel, R. Abgrall, A multiphase godunov method for compressible mul-
 328 tifluid and multiphase flows, J. Comput Physics (2001) 425–267.
- 329 [6] R. Saurel, O. Lemetayer, A multiphase model for compressible flows with
 330 interfaces, shocks, detonation waves and cavitation, J. Comput Physics
 331 (2001) 239–271.

- 332 [7] Q. Li, H. Feng, T. Cai, C. Hu, Difference scheme for two-phase flow, Appl
333 Math Mech (2004) 536.
- 334 [8] A. Zein, M. Hantke, G. Warnecke, Modeling phase transition for compress-
335 ible two-phase flows applied to metastable liquids, J. Comput Physics (2010)
336 2964.
- 337 [9] A. Ambroso, C. Chalons, P.-A. Raviart, A godunov-type method for the
338 seven-equation model of compressible multiphase mixtures, Comput. Fluids
339 (2012) 67–91.
- 340 [10] R. A. Berry, M. Delchini, J. Ragusa, Relap-7 numerical stabilization: En-
341 tropy viscosity method, Tech. Rep. INL/EXT-14-32352, Idaho National
342 Laboratory, USA (2014).
- 343 [11] R. Saurel, F. Petitpas, R. A. Berry, Simple and efficient relaxation methods
344 for interfaces separating compressible fluids, cavitating flows and shocks in
345 multiphase mixtures, J. of Computational Physics 228 (2009) 1678–1712.
- 346 [12] J. M. Herrard, O. Hurisse, A simple method to compute standard two-fluid
347 models, Int. J. of Computational Fluid Dynamics 19 (2005) 475–482.
- 348 [13] J. L. Guermond, B. Popov, Viscous regularization of the euler equations
349 and entropy principles, under review.
- 350 [14] M. Delchini, Extension of the entropy viscosity method to multi-d euler
351 equations and the seven-equation two-phase model, Tech. rep., Texas A&
352 M University, USA (2014).
- 353 [15] M. Delchini, J. Ragusa, R. Berry, Entropy-based viscosity regularization
354 for the multi-dimensional euler equations in low-mach and transonic flows,
355 under review.
- 356 [16] R. Leveque, Numerical Methods for Conservation Laws, Birkhuser Basel,
357 Zurich, Switzerland, 1990.
- 358 [17] J. L. Guermond, R. Pasquetti, Entropy viscosity method for nonlinear con-
359 servation laws, Journal of Comput. Phys 230 (2011) 4248–4267.
- 360 [18] J. L. Guermond, R. Pasquetti, Entropy viscosity method for high-order ap-
361 proximations of conservation laws, Lecture Notes in Computational Science
362 and Engineering 76 (2011) 411–418.
- 363 [19] B. Perthame, C. W. Shu, On positivity preserving finite volume schemes for
364 euler equations, Numer. Math. 73 (1996) 119–130.
- 365 [20] A. Harten, L. P. Franca, M. Mallet, Convex entropies and hyperbolicity for
366 general euler equations, SIAM J Numer Anal 6 (1998) 2117–2127.
- 367 [21] A. Lapidus, A detached shock calculation by second order finite differences,
368 J. Comput. Phys. 2 (1967) 154–177.

- 369 [22] J. Donea, A. Huerta, Finite Element Methods for Flow Problems, Oxford
370 University Press, 2003.
- 371 [23] R. Lohner, Applied CFD Techniques: an Introduction based on Finite
372 Element Methods, 2nd Edition Wiley, 2003.

373 **Appendix A Entropy equation for the multi-D seven equation model**
 374 **without viscous regularization**

This appendix provides the steps that lead to the derivation of the phasic entropy equation of the seven-equation model [3]. For the purpose of this dissertation, two phases are considered and denoted by the indexes j and k . In the seven-equation model, each phase obeys to the following set of equations (Eq. (38)):

$$\partial_t (\alpha_k A) + A \mathbf{u}_{int} \cdot \nabla \alpha_k = A \mu (P_k - P_j) \quad (38a)$$

$$\partial_t (\alpha_k \rho_k A) + \nabla \cdot (\alpha_k \rho_k \mathbf{u}_k A) = 0 \quad (38b)$$

$$\begin{aligned} \partial_t (\alpha_k \rho_k \mathbf{u}_k A) + \nabla \cdot [\alpha_k A (\rho_k \mathbf{u}_k \otimes \mathbf{u}_k + P_k \mathbb{I})] = \\ \alpha_k P_k \nabla A + P_{int} A \nabla \alpha_k + A \lambda (\mathbf{u}_j - \mathbf{u}_k) \end{aligned} \quad (38c)$$

$$\begin{aligned} \partial_t (\alpha_k \rho_k E_k A) + \nabla \cdot [\alpha_k A \mathbf{u}_k (\rho_k E_k + P_k)] = \\ P_{int} A \mathbf{u}_{int} \cdot \nabla \alpha_k - \mu \bar{P}_{int} (P_k - P_j) + \bar{\mathbf{u}}_{int} A \lambda (\mathbf{u}_j - \mathbf{u}_k) \end{aligned} \quad (38d)$$

375 where ρ_k , \mathbf{u}_k , E_k and P_k are the density, the velocity, the specific total energy
 376 and the pressure of k^{th} phase, respectively. The pressure and velocity relaxation
 377 parameters are denoted by μ_P and λ_u , respectively. The variables with index
 378 $_{int}$ correspond to the interfacial variables and a definition is given in Eq. (39).
 379 The cross section A is only function of space: $\partial_t A = 0$.

$$\left\{ \begin{array}{l} P_{int} = \bar{P}_{int} - \frac{\nabla \alpha_k}{\|\nabla \alpha_k\|} \frac{Z_k Z_j}{Z_k + Z_j} (\mathbf{u}_k - \mathbf{u}_j) \\ \bar{P}_{int} = \frac{Z_k P_j + Z_j P_k}{Z_k + Z_j} \\ \mathbf{u}_{int} = \bar{\mathbf{u}}_{int} - \frac{\nabla \alpha_k}{\|\nabla \alpha_k\|} \frac{P_k - P_j}{Z_k + Z_j} \\ \bar{\mathbf{u}}_{int} = \frac{Z_k \mathbf{u}_k + Z_j \mathbf{u}_j}{Z_k + Z_j} \end{array} \right. \quad (39)$$

380 where $Z_k = \rho_k c_k$ and $Z_j = \rho_j c_j$ are the impedance of the phase k and j ,
 381 respectively. The speed of sound is denoted by the variable c . The function
 382 $sgn(x)$ returns the sign of the variable x .

383 The first step consists of rearranging the equations given in Eq. (39) using the
 384 primitive variables $(\alpha_k, \rho_k, \mathbf{u}_k, e_k)$, where e_k is the specific internal energy of
 385 k^{th} phase. We introduce the material derivative $\frac{D(\cdot)}{Dt} = \partial_t(\cdot) + \mathbf{u}_k \cdot \nabla(\cdot)$ for
 386 simplicity.

387 The void fraction is unchanged. The continuity equation is modified as follows:

$$\alpha_k A \frac{D\rho_k}{Dt} + \rho_k A \mu (P_k - P_j) + \rho_k A (\mathbf{u}_k - \mathbf{u}_j) \cdot \nabla \alpha_k + \rho_k \alpha_k \nabla \cdot (A \mathbf{u}_k) = 0 \quad (40)$$

388 The momentum and continuity equations are combined to yield the velocity
389 equation:

$$\alpha_k \rho_k A \frac{D\mathbf{u}_k}{Dt} + \partial_x (\alpha_k A P_k) = \alpha_k P_k \nabla A + P_{int} A \nabla \alpha_k + A \lambda_u (\mathbf{u}_j - \mathbf{u}_k) \quad (41)$$

The internal energy is obtained from the total energy and the kinetic equation (\mathbf{u}_k *Eq. (41)):

$$\begin{aligned} \alpha_k \rho_k A \frac{De_k}{Dt} + \nabla \cdot (\alpha_k \mathbf{u}_k A P_k) - \mathbf{u}_k \cdot \nabla (\alpha_k A P_k) &= P_{int} A (\mathbf{u}_{int} - \mathbf{u}_k) \cdot \nabla \alpha_k \\ &\quad - \alpha_k P_k \mathbf{u}_k \cdot \nabla A - \bar{P}_{int} A \mu_P (P_k - P_j) + A \lambda_u (\mathbf{u}_j - \mathbf{u}_k) \cdot (\bar{\mathbf{u}}_{int} - \mathbf{u}_k) \end{aligned} \quad (42)$$

390 In the next step, we assume the existence of a phase wise entropy s_k function
391 of the density ρ_k and the internal energy e_k . Using the chain rule,

$$\frac{Ds_k}{Dt} = (s_\rho)_k \frac{D\rho_k}{Dt} + (s_e)_k \frac{De_k}{Dt}, \quad (43)$$

392 along with the internal energy and the continuity equations, the following en-
393 tropy equation is obtained:

$$\begin{aligned} \alpha_k \rho_k A \frac{Ds_k}{Dt} + \underbrace{A (P_k (s_e)_k + \rho_k^2 (s_\rho)_k) \mathbf{u}_k \cdot \nabla \alpha_k + \alpha_k (P_k (s_e)_k + \rho_k^2 (s_\rho)_k) \mathbf{u}_k \cdot \nabla A}_{(a)} &= \\ (s_e)_k P_{int} A [(\mathbf{u}_{int} - \mathbf{u}_k) \cdot \nabla \alpha_k - \bar{P}_{int} A \mu_P (P_k - P_j) + A \lambda_u (\bar{\mathbf{u}}_{int} - \mathbf{u}_k) \cdot (\mathbf{u}_j - \mathbf{u}_k)] &- \\ \rho_k^2 (s_\rho)_k [\mu_P A (P_k - P_j) + A (\mathbf{u}_k - \mathbf{u}_{int}) \cdot \nabla \alpha_k] &\quad (44) \end{aligned}$$

394 where $(s_e)_k$ and $(s_\rho)_k$ denote the partial derivatives of the entropy s_k with
395 respect to the internal energy e_k and the density ρ_k , respectively. The second
396 term, (a), in the left hand side of Eq. (44) can be set to zero by assuming the
397 following relation between the partial derivatives of the entropy s_k :

$$P_k (s_e)_k + \rho_k^2 (s_\rho)_k = 0. \quad (45)$$

398 The above equation is equivalent to the application of the second thermody-
399 namic law when assuming reversibility:

$$T_k ds_k = de_k - \frac{P_k}{\rho_k^2} d\rho_k \text{ with } (s_e)_k = \frac{1}{T_k} \text{ and } (s_\rho)_k = -\frac{P_k}{\rho_k^2} (s_e)_k \quad (46)$$

400 Thus, equation Eq. (44) can be rearranged using the relation $(s_\rho)_k = -\frac{P_k}{\rho_k^2} (s_e)_k$:

$$\begin{aligned} ((s_e)_k)^{-1} \alpha_k \rho_k \frac{Ds}{Dt} &= \underbrace{[P_{int} (\mathbf{u}_{int} - \mathbf{u}_k) + P_k (\mathbf{u}_k - \mathbf{u}_{int})] \cdot \nabla \alpha_k}_{(b)} + \\ &\quad \underbrace{\mu (P_k - P_j) (P_k - \bar{P}_{int})}_{(c)} + \underbrace{\lambda (\mathbf{u}_j - \mathbf{u}_k) \cdot (\bar{\mathbf{u}}_{int} - \mathbf{u}_k)}_{(d)} \end{aligned} \quad (47)$$

401 The right hand side of equation Eq. (47) is split into three terms (b), (c) and
 402 (d) that will be treated independently from each other. The terms (c) and (d)
 403 are simpler to start with and can be easily recast by using the definitions of $\bar{\mathbf{u}}_{int}$
 404 and \bar{P}_{int} given in equation Eq. (39):

$$\begin{aligned}\mu(P_k - P_j)(P_k - \bar{P}_{int}) &= \mu_P \frac{Z_k}{Z_k + Z_j} (P_j - P_k)^2 \\ \lambda(\mathbf{u}_j - \mathbf{u}_k) \cdot (\bar{\mathbf{u}}_{int} - \mathbf{u}_k) &= \lambda_u \frac{Z_j}{Z_k + Z_j} (\mathbf{u}_j - \mathbf{u}_k)^2\end{aligned}\quad (48)$$

405 By definition, μ_P , λ_u and Z_k are all positive. Thus, the above terms are uncon-
 406 ditionally positive.
 407 It remains to look at the last term (b). Once again, by using the definition of
 408 P_{int} and \mathbf{u}_{int} , and the following relations:

$$\begin{aligned}\mathbf{u}_{int} - \mathbf{u}_k &= \frac{Z_j}{Z_k + Z_j} (\mathbf{u}_j - \mathbf{u}_k) - \frac{\nabla \alpha_k}{\|\nabla \alpha_k\|} \frac{P_k - P_j}{Z_k + Z_j} \\ P_{int} - P_k &= \frac{Z_k}{Z_k + Z_j} (P_j - P_k) - \frac{\nabla \alpha_k}{\|\nabla \alpha_k\|} \frac{Z_k Z_j}{Z_k + Z_j} (\mathbf{u}_k - \mathbf{u}_j),\end{aligned}$$

409 (b) yields:

$$\begin{aligned}[P_{int}(\mathbf{u}_{int} - \mathbf{u}_k) + P_k(\mathbf{u}_k - \mathbf{u}_{int})] \cdot \nabla \alpha_k &= (P_{int} - P_k)(\mathbf{u}_{int} - \mathbf{u}_k) \cdot \nabla \alpha_k = \\ &= \frac{Z_k}{(Z_k + Z_j)^2} \nabla \alpha_k \cdot \left[Z_j(\mathbf{u}_j - \mathbf{u}_k)(P_j - P_k) + \frac{\nabla \alpha_k}{\|\nabla \alpha_k\|} Z_j^2 (\mathbf{u}_j - \mathbf{u}_k)^2 + \right. \\ &\quad \left. \frac{\nabla \alpha_k}{\|\nabla \alpha_k\|} (P_k - P_j)^2 + \frac{\nabla \alpha_k \cdot \nabla \alpha_k}{\|\nabla \alpha_k\|^2} (P_k - P_j) Z_j (\mathbf{u}_k - \mathbf{u}_j) \right]\end{aligned}\quad (49)$$

The above equation is factorized by $\|\nabla \alpha_k\|$ and then recast under a quadratic form when noticing that $\frac{\nabla \alpha_k \cdot \nabla \alpha_k}{\|\nabla \alpha_k\|^2} = 1$, which yields:

$$\begin{aligned}[(\mathbf{u}_{int} - \mathbf{u}_k)P_{int} + (\mathbf{u}_k - \mathbf{u}_{int})P_k] \cdot \nabla \alpha_k &= \\ \|\nabla \alpha_k\| \frac{Z_k}{(Z_k + Z_j)^2} \left[Z_j(\mathbf{u}_j - \mathbf{u}_k) + \frac{\nabla \alpha_k}{\|\nabla \alpha_k\|} (P_k - P_j) \right]^2\end{aligned}\quad (50)$$

Thus, using results from Eq. (47), Eq. (48), Eq. (49) and Eq. (50), the entropy equation obtained in [3] holds and is recalled here for convenience:

$$\begin{aligned}(s_e)_k^{-1} \alpha_k \rho_k A \frac{Ds_k}{Dt} &= \mu_P \frac{Z_k}{Z_k + Z_j} (P_j - P_k)^2 + \lambda_u \frac{Z_j}{Z_k + Z_j} (\mathbf{u}_j - \mathbf{u}_k)^2 \\ &\quad + \frac{Z_k}{(Z_k + Z_j)^2} \left[Z_j(\mathbf{u}_j - \mathbf{u}_k) + \frac{\nabla \alpha_k}{\|\nabla \alpha_k\|} (P_k - P_j) \right]^2.\end{aligned}$$

410