Extension of the entropy viscosity method to the multi-D 7-equation two-phase flow model.

I do not know if we should have 'multi-D' in the title since we will only present 1-D results

Marc O. Delchini^a, Jean C. Ragusa^{*,a}, Ray A. Berry^b

^aDepartment of Nuclear Engineering, Texas A&M University, College Station, TX 77843, USA ^b Idaho National Laboratory, Idaho Falls, ID 83415, USA

Abstract

blabla

11

13

Key words: two-phase flow model, with variable area, entropy viscosity method, stabilization method, low Mach regime, shocks.

1 1. Introduction

- a few lines about the need for accurately resolving two-phase flows
- background on the different two-phase flow models: 5, 6 and 7-equation two-phase flow models
- then, focus on the different types of 7-equation two-phase flow models: they mostly differ because of the closure relaxations used
- discuss the different numerical solvers developed for the 7-equation twophase flow model: HLL, HLLC, and approximated Riemann solvers accounting for the source terms
 - emphasize the fact that the above numerical solvers only works on discontinuous schemes
- then, introduce the entropy viscosity method and details the organization of the paper

^{*}Corresponding author

Email addresses: delchmo@tamu.edu (Marc O. Delchini), jean.ragusa@tamu.edu (Jean C. Ragusa), ray.berry@inl.gov (Ray A. Berry)

Compressible two-phase flows are found in numerous industrial applications and are an ongoing area of research in modeling and simulation over many years. A variety of models with different levels of complexity has been developed such 16 as: five-equation model [1], six-equation model [2], and more recently the sevenequation model [3]. These models are all obtained by integrating the single-18 phase flow balance equations weighed by a characteristic or indicator function 19 for each phase. The resulting system of equations contains non-conservative 20 terms that describe the interaction between phases but also an equation for the 21 volume fraction. Once a system of equations describing the physics is derived, 22 the next challenging step is to develop a robust and accurate discretization to obtain a numerical solution. Assuming that the system of equations is hyper-24 bolic under some conditions, a Riemann solver could be used but is often ruled 25 out because of the complexity due to the number of equations involved. Further-26 more, careless approximation for the treatment of the non-conservative terms 27 can lead to failure in computing the numerical solution [4]. An alternative is to use an approximate Riemann solver, a well-established approach for single-phase 29 flows, while deriving a consistent discretization scheme for the non-conservative 30 31

This methodology was applied to the seven-equation model (SEM) introduced by Berry et al. in [3]. This model is known to be unconditionally hyperbolic which is highly desirable when working with approximate Riemann solvers and can treat a wide range of applications. Its particularity comes from the pressure and velocity relaxation terms in the volume fraction, momentum and energy equations that can bring the two phases in equilibrium when using large values of the relaxation parameters. In other words, the seven-equation model can degenerate into the six- and five-equation models. Alike for the other twophase flow models, solving for the seven-equation model requires a numerical solver and significant effort was dedicated to this task for spatially discontinuous schemes. Because each phase is assumed to obey the Euler equations, most of the numerical solvers are adapted from the single-phase approximate Riemann solvers. For example, Saurel et al. [5, 6] employed a HLL-type scheme to solve for the SEM but noted that excessive dissipation was added to the contact discontinuity. A more advanced HLLC-type scheme was developed in [7] but only for the subsonic case and then extended to supersonic flows in [8]. More recently, Ambroso et al. [9] proposed an approximate Riemann solver accounting for source terms such as gravity and drag forces, but with no interphase mass transfer.

51 2. The multi-D 7-equation two-phase flow model

33

35

36

37

38

39

41

42

44

45

46

48

50

The multi-D seven-equation two-phase model presented in this paper is obtained by assuming that each phase obeys the single-phase Euler equations (with phase-exchange terms) and by integrating over a control volume after multiplying by a characteristic function. The detailed derivation can be found in [3]. In this section, the governing multi-dimensional equations are recalled for a phase k in interaction with a phase j. Each phase obeys the following mass,

momentum and energy balance equations, supplemented by a non-conservative volume-fraction equation:

$$\frac{\partial (\alpha \rho)_k A}{\partial t} + \nabla \cdot (\alpha \rho \boldsymbol{u} A)_k = -\Gamma A_{int} A \tag{1a}$$

$$\frac{\partial (\alpha \rho \boldsymbol{u})_k A}{\partial t} + \boldsymbol{\nabla} \cdot [\alpha_k A (\rho \boldsymbol{u} \otimes \boldsymbol{u} + P \mathbb{I})_k] = P_{int} A \boldsymbol{\nabla} \alpha_k + P_k \alpha_k \boldsymbol{\nabla} A + A \lambda_u (\boldsymbol{u}_i - \boldsymbol{u}_k) - \Gamma A_{int} \boldsymbol{u}_{int} A \quad (1b)$$

$$\frac{\partial (\alpha \rho E)_k A}{\partial t} + \nabla \cdot [\alpha_k \mathbf{u}_k A (\rho E + P)_k] = P_{int} \mathbf{u}_{int} A \nabla \alpha_k - \bar{P}_{int} A \mu_P (P_k - P_j)
+ \bar{\mathbf{u}}_{int} A \lambda_u (\mathbf{u}_j - \mathbf{u}_k) + \Gamma A_{int} \left(\frac{P_{int}}{\rho_{int}} - H_{k,int} \right) A$$
(1c)

$$\frac{\partial \alpha_k A}{\partial t} + A \boldsymbol{u}_{int} \cdot \boldsymbol{\nabla} \alpha_k = A \mu_P (P_k - P_j) - \frac{\Gamma A_{int} A}{\rho_{int}}$$
 (1d)

where α_k , ρ_k , \boldsymbol{u}_k and E_k denote the volume fraction, the density, the velocity vector and the total specific energy of phase k, respectively. The phase pressure P_k is computed from an equation of state. The interfacial pressure and velocity and their corresponding average values are denoted by P_{int} , \boldsymbol{u}_{int} , \bar{P}_{int} and $\bar{\boldsymbol{u}}_{int}$, respectively, and are defined in Eq. (2).

$$P_{int} = \bar{P}_{int} + \frac{Z_k Z_j}{Z_k + Z_j} \frac{\nabla \alpha_k}{||\nabla \alpha_k||} \cdot (\boldsymbol{u}_j - \boldsymbol{u}_k)$$
 (2a)

$$\bar{P}_{int} = \frac{Z_j P_k + Z_k P_j}{Z_k + Z_j} \tag{2b}$$

$$\mathbf{u}_{int} = \bar{\mathbf{u}}_{int} + \frac{\nabla \alpha_k}{||\nabla \alpha_k||} \frac{P_j - P_k}{Z_k + Z_j}$$
 (2c)

$$\bar{\boldsymbol{u}}_{int} = \frac{Z_k \boldsymbol{u}_k + Z_j \boldsymbol{u}_j}{Z_k + Z_j}.$$
 (2d)

The interfacial specific total enthalpy of phase k, H_k , is defined as follows: $H_k = h_k + 0.5||\mathbf{u}||^2$. Following [3], the pressure and velocity relaxation coefficients, μ_P and λ_u respectively, are function of the acoustic impedance $Z_k = \rho_k c_k$ and the specific interfacial area A_{int} as shown in Eq. (3).

$$\lambda_u = \frac{1}{2} \mu_P Z_k Z_j \tag{3a}$$

$$\mu_P = \frac{A_{int}}{Z_k + Z_j} \tag{3b}$$

The specific interfacial area (i.e., the interfacial surface area per unit volume of two-phase mixture), A_{int} , must be specified from some type of flow regime

map or function under the form of a correlation. In [3], A_{int} is chosen to be a function of the liquid volume fraction:

$$A_{int} = A_{int}^{max} \left[6.75 \left(1 - \alpha_k \right)^2 \alpha_k \right], \tag{4}$$

where $A_{int}^{max} = 5100 \ m^2/m^3$. With such definition, the interfacial area is zero in the limits $\alpha_k = 0$ and $\alpha_k = 1$. Lastly, Γ is the net mass transfer rate per unit interfacial area from phase j to phase k. Its expression, given in Eq. (5), is obtained by considering a vaporization/condensation process that is dominated by heat diffusion at the interface [3, 10]:

$$\Gamma = \Gamma_{j} = \frac{h_{T,k} (T_{k} - T_{int}) + h_{T,j} (T_{j} - T_{int})}{h_{j,int} - h_{k,int}}$$

$$= \frac{h_{T,k} (T_{k} - T_{int}) + h_{T,j} (T_{j} - T_{int})}{L_{v} (T_{int})},$$
(5)

where $L_v(T_{int}) = h_{j,int} - h_{k,int}$ represents the latent heat of vaporization. The interface temperature is determined by the saturation constraint $T_{int} = T_{sat}(P)$ with the appropriate pressure $P = \bar{P}_{int}$ determined above. The interfacial heat transfer coefficients for phases k and j are denoted by $h_{T,k}$ and $h_{T,j}$, respectively, and computed from correlations [3].

The set of equations obeyed by phase j are simply obtained by substituting k by j and j by k in Eq. (1), keeping the same definition of the interfacial variables and remembering that $\Gamma_j = -\Gamma_k$. In the case of two-phase flows, the equation for the volume fraction of phase j is simply replaced by the algebraic relation

$$\alpha_i = 1 - \alpha_k$$

which reduces the number of equations from eight to seven and yields the sevenequation two-phase flow model.

The seven-equation model has interesting properties that are discussed next. A set of seven waves is present in such a model: two acoustic waves and a contact wave for each phase supplanted by a volume fraction wave propagating at the interfacial velocity u_{int} . Considering a domain of dimension \mathbb{D} , the corresponding eigenvalues are the following for each phase k:

$$\lambda_{1} = \mathbf{u}_{int} \cdot \bar{\mathbf{n}}$$

$$\lambda_{2,k} = \mathbf{u}_{k} \cdot \bar{\mathbf{n}} - c_{k}$$

$$\lambda_{3,k} = \mathbf{u}_{k} \cdot \bar{\mathbf{n}} + c_{k}$$

$$\lambda_{d+3,k} = \mathbf{u}_{k} \cdot \bar{\mathbf{n}} \text{ for } d = 1 \dots \mathbb{D},$$
(6)

where \bar{n} is an unit vector pointing to a given direction. The eigenvalues given in Eq. (6) are unconditionally real which presents an interesting property for the development of numerical methods since the system is hyperbolic and well-posed. To relax the seven-equation model to the ill-posed classical six-equation

model, only the pressures should be relaxed toward a single pressure for both phases. This is accomplished by specifying the pressure relaxation coefficient to be very large, i.e., letting it approach infinity. But if the pressure relaxation coefficient goes to infinity, so does the velocity relaxation rate also approach infinity. This then relaxes the seven-equation model not to the classical sixequation model but to the mechanical equilibrium five-equation model of Kapila [1]. This reduced five-equation model is also hyperbolic and well-posed. The five-equation model provides a very useful starting point for constructing multidimensional interface resolving methods which dynamically captures evolving and spontaneously generated interfaces [11]. Thus the seven-equation model can be relaxed locally to couple seamlessly with such a multi-dimensional, interface resolving code. Numerically, the mechanical relaxation coefficients μ_P (pressure) and λ_u (velocity) can be relaxed independently to yield solutions to useful, reduced models. It is noted, however, that relaxation of pressure only by making μ_P large without relaxing velocity will indeed give ill-posed and unstable numerical solutions, just as the classical six-equation two-phase model does, with sufficiently fine spatial resolution, as confirmed in [3, 12]. For each phase k, an entropy equation can be derived when accounting only for the pressure and velocity relaxation terms (all of the terms proportional to the net mass transfer term Γ are removed). The entropy function for a phase k is denoted by s_k and function of the density ρ_k and the internal energy e_k . The derivation is detailed in Appendix A and only the final result is recalled here:

$$(s_{e})_{k}^{-1}\alpha_{k}\rho_{k}A\frac{Ds_{k}}{Dt} = \mu_{P}\frac{Z_{k}}{Z_{k} + Z_{j}}(P_{j} - P_{k})^{2} + \lambda_{u}\frac{Z_{j}}{Z_{k} + Z_{j}}(\boldsymbol{u}_{j} - \boldsymbol{u}_{k})^{2}$$
$$\frac{Z_{k}}{(Z_{k} + Z_{j})^{2}} \left[Z_{j}(\boldsymbol{u}_{j} - \boldsymbol{u}_{k}) + \frac{\boldsymbol{\nabla}\alpha_{k}}{||\boldsymbol{\nabla}\alpha_{k}||}(P_{k} - P_{j})\right]^{2}, \quad (7)$$

The partial derivative of the entropy function s_k with respect to the internal energy e_k , $(s_e)_k$, is shown to be proportional to the inverse of the temperature of phase k, alike for the single phase Euler equations [13, 14]. The right hand-side of Eq. (7) is unconditionally positive since all terms are squared and thus, is used to demonstrate the entropy minimum principle and derive the dissipative terms. Furthermore, Eq. (7) is valid for both phases $\{k, j\}$ and ensures positivity of the total entropy equation that is obtained by summing over the phases:

$$\sum_{k} (s_e)_k^{-1} \alpha_k \rho_k A \frac{Ds_k}{Dt} = \sum_{k} (s_e)_k^{-1} \alpha_k \rho_k A (\partial_t s_k + \boldsymbol{u}_k \cdot \boldsymbol{\nabla} s_k) \ge 0.$$

Note that when one phase disappears, Eq. (8) degenerates into the single phase entropy equation [3, 14].

3. A viscous regularization for the multi-D seven-equation two-phase flow model

72

73

We now propose to derive a viscous regularization for the seven-equation model given in Eq. (1) by using the same methodology as for the multi-D Euler

equations with/without variable area [13, 15]. The method consists in adding perturbation terms to the system of equation under consideration, and re-derive 77 the entropy equation whose sign is known to be positive to ensure uniqueness 78 of the numerical solution [16]. Because of the addition of perturbation terms, 79 the entropy equation is modified and contains extra terms of unknown sign. 80 By carefully choosing a definition for each of the perturbation term, the sign 81 of the entropy equation can be determined and proved positive. For the seven-82 equation model, derivation of a viscous regularization can be achieved by consid-83 ering either the phasic entropy equation (Eq. (7)) or the total entropy equation 84 (Eq. (8)). In the later case, the entropy minimum principle is verified for the whole system which may not ensure positivity of the entropy equation for each phase. However, positivity of the total entropy equation can be also achieved 87 by assuming that the entropy minimum principle holds for each phase. This 88 stronger requirement will also ensure consistency with the single phase Euler 89 equations when one of the phase disappears in the limits $\alpha_k \to 0$ and $\alpha_k \to 1$. Thus, it is chosen to work with the phasic entropy equations. 91

For the purpose of this section, the system of equations given in Eq. (8) is considered which is obtained by simply omitting the mass source terms (terms proportional to Γ) in Eq. (1).

$$\partial_t \left(\alpha_k A \right) + A \boldsymbol{u}_{int} \cdot \boldsymbol{\nabla} \alpha_k = A \mu_P \left(P_k - P_i \right) \tag{8a}$$

$$\partial_t \left(\alpha_k \rho_k A \right) + \nabla \cdot \left(\alpha_k \rho_k \boldsymbol{u}_k A \right) = 0 \tag{8b}$$

$$\partial_{t} \left(\alpha_{k} \rho_{k} u_{k} A \right) + \nabla \cdot \left[\alpha_{k} A \left(\rho_{k} \boldsymbol{u}_{k} \otimes \boldsymbol{u}_{k} + P_{k} \mathbb{I} \right) \right] = \alpha_{k} P_{k} \nabla A + P_{int} A \nabla \alpha_{k} + A \lambda_{u} \left(\boldsymbol{u}_{j} - \boldsymbol{u}_{k} \right)$$
(8c)

$$\partial_{t} \left(\alpha_{k} \rho_{k} E_{k} A \right) + \nabla \cdot \left[\alpha_{k} A \boldsymbol{u}_{k} \left(\rho_{k} E_{k} + P_{k} \right) \right] = A P_{int} \boldsymbol{u}_{int} \cdot \nabla \alpha_{k} - \mu_{P} \bar{P}_{int} \left(P_{k} - P_{j} \right) + A \lambda_{u} \bar{\boldsymbol{u}}_{int} \cdot \left(\boldsymbol{u}_{j} - \boldsymbol{u}_{k} \right)$$
(8d)

In order to apply the entropy viscosity method, perturbation terms are added to each equation of Eq. (8), which yields:

$$\partial_t (\alpha_k A) + \boldsymbol{u}_{int} A \boldsymbol{\nabla} \alpha_k = A \mu_P (P_k - P_i) + \boldsymbol{\nabla} \cdot \boldsymbol{l}_k \tag{9a}$$

$$\partial_t \left(\alpha_k \rho_k A \right) + \nabla \cdot \left(\alpha_k \rho_k \boldsymbol{u}_k A \right) = \nabla \cdot \boldsymbol{f}_k \tag{9b}$$

$$\partial_{t} (\alpha_{k} \rho_{k} \boldsymbol{u}_{k} A) + \nabla \cdot [\alpha_{k} A (\rho_{k} \boldsymbol{u}_{k} \otimes \boldsymbol{u}_{k} + P_{k} \mathbb{I})] =$$

$$\alpha_{k} P_{k} \nabla A + P_{int} A \nabla \alpha_{k} + A \lambda_{u} (\boldsymbol{u}_{j} - \boldsymbol{u}_{k}) + \nabla \cdot \boldsymbol{g}_{k} \quad (9c)$$

$$\partial_{t} (\alpha_{k} \rho_{k} E_{k} A) + \nabla \cdot [\alpha_{k} A \boldsymbol{u}_{k} (\rho_{k} E_{k} + P_{k})] = P_{int} A \boldsymbol{u}_{int} \cdot \nabla \alpha_{k} - \mu_{P} \bar{P}_{int} (P_{k} - P_{j}) + A \lambda_{u} \bar{\boldsymbol{u}}_{int} \cdot (\boldsymbol{u}_{j} - \boldsymbol{u}_{k}) + \nabla \cdot (\boldsymbol{h}_{k} + \boldsymbol{u} \cdot \boldsymbol{g}_{k})$$
(9d)

where f_k , g_k , h_k and l_k are the phasic perturbation terms. The next step consists in deriving the entropy equation for the phase k, on the same model as what is done in Appendix A for the system of equations (Eq. (8)) that does not contain the perturbation terms.

1. derive the density and internal energy equations from Eq. (9).

96

99

100

101

102 103

104

2. assuming that the phasic entropy, s_k , is function of the density, ρ_k and the internal energy, e_k , derive the entropy equation by using the chain rule:

$$\frac{Ds_k}{Dt} = (s_\rho)_k \frac{D\rho_k}{Dt} + (s_e)_k \frac{De_k}{Dt}$$
(10)

where $\frac{D}{Dt}$ is the material derivative. The terms $(s_e)_k$ and $(s_\rho)_k$ denote the partial derivative of the entropy s_k with respect to e_k and ρ_k , respectively.

isolate the terms of interest and choose an appropriate expression for each
of the perturbation terms in order to ensure positivity of the right-hand
side.

We first derive the density equation for the primitive variable ρ_k by combining Eq. (9a) and Eq. (9b) to obtain:

$$\alpha_{k} A \left[\partial_{t} \rho_{k} + \left(\boldsymbol{u}_{k} - \underline{\underline{\boldsymbol{u}}_{int}} \right) \cdot \boldsymbol{\nabla} \rho_{k} \right] = \underline{A \rho_{k} \mu_{P} \left(P_{k} - P_{j} \right)} + \boldsymbol{\nabla} \cdot \boldsymbol{f}_{k} - \rho_{k} \boldsymbol{\nabla} \cdot \boldsymbol{l}_{k} \quad (11)$$

In order to derive the internal energy equation, the velocity equation is obtained by subtracting the density equation from the momentum equation:

$$\alpha_{k}\rho_{k}A\left[\partial_{t}\boldsymbol{u}_{k}+\boldsymbol{u}_{k}\cdot\boldsymbol{\nabla}\cdot\boldsymbol{u}_{k}\right]+\boldsymbol{\nabla}\cdot\left(\alpha_{k}\rho_{k}AP_{k}\mathbb{I}\right)=$$

$$\alpha_{k}P_{k}\boldsymbol{\nabla}A+P_{int}A\boldsymbol{\nabla}\alpha_{k}+A\lambda\left(\boldsymbol{u}_{j}-\boldsymbol{u}_{k}\right)+\boldsymbol{\nabla}\cdot\boldsymbol{g}_{k}-\boldsymbol{u}_{k}\otimes\boldsymbol{f}_{k}$$
(12)

After multiplying Eq. (12) by the velocity vector \mathbf{u}_k , the resulting kinetic energy equation is subtracted from the total energy equation to obtain the internal energy equation for phase k:

$$\alpha_{k}\rho_{k}A\left[\partial_{t}\boldsymbol{e}_{k}+\boldsymbol{u}_{k}\cdot\boldsymbol{\nabla}\cdot\boldsymbol{e}_{k}\right]+\alpha_{k}\rho_{k}AP_{k}\boldsymbol{\nabla}\boldsymbol{u}_{k}=\underbrace{\frac{P_{int}A\left(\boldsymbol{u}_{int}-\boldsymbol{u}_{k}\right)\cdot\boldsymbol{\nabla}\alpha_{k}}{-\bar{P}_{int}A\mu_{P}\left(P_{k}-P_{j}\right)}}_{+\bar{P}_{int}A\mu_{P}\left(P_{k}-P_{j}\right)}+\underbrace{\frac{\alpha_{k}P_{k}\boldsymbol{u}_{k}\boldsymbol{\nabla}A}{A\lambda_{u}\left(\boldsymbol{u}_{j}-\boldsymbol{u}_{k}\right)\cdot\left(\bar{\boldsymbol{u}}_{int}-\boldsymbol{u}_{k}\right)}}_{+\bar{P}_{int}A\mu_{P}\left(P_{k}-P_{j}\right)}+\underbrace{\frac{\alpha_{k}P_{k}\boldsymbol{u}_{k}\boldsymbol{\nabla}A}{|\boldsymbol{u}_{i}-\boldsymbol{u}_{k}|\cdot\left(\bar{\boldsymbol{u}}_{int}-\boldsymbol{u}_{k}\right)\right)}}_{|\boldsymbol{u}_{i}-\boldsymbol{u}_{k}|}$$

$$+\underline{\boldsymbol{\nabla}\cdot\boldsymbol{h}_{k}+\boldsymbol{g}_{k}:\boldsymbol{\nabla}\boldsymbol{u}_{k}+|\boldsymbol{u}_{k}|_{k}^{2}\boldsymbol{f}_{k}}}$$

$$(13)$$

The underline terms in Eq. (11) and Eq. (13) yield the positive terms in the right-hand-side of Eq. (7) and thus are ignored in the remaining of the derivation for simplicity. The entropy equation is now obtained by combining the density equation (Eq. (11)) and the internal energy equation (Eq. (13)) through the chain rule given in Eq. (10) to yield:

$$\alpha_{k}\rho_{k}A\frac{Ds_{k}}{Dt} = (\rho s_{\rho})_{k} \left[\nabla \cdot \boldsymbol{f}_{k} - \rho_{k} \nabla \cdot \boldsymbol{l}_{k} \right] + (s_{e})_{k} \left[\nabla \cdot \boldsymbol{h}_{k} + \boldsymbol{g}_{k} : \nabla \boldsymbol{u}_{k} + \left(||\boldsymbol{u}||_{k}^{2} - e_{k} \right) \nabla \cdot \boldsymbol{f}_{k} \right],$$
(14)

where it was assumed that the entropy of phase k satisfies the second thermodynamic law:

$$T_k ds_k = de_k - P_k \frac{d\rho_k}{\rho_k^2}$$
which implies $P_k(s_e)_k + \rho_k(s_\rho)_k = 0$, (15)
$$(s_e)_k = T_k^{-1} \text{ and } (s_\rho)_k = -(s_e)_k P_k \frac{d\rho_k}{\rho_k^2}.$$

Following the methodology applied in [13, 15], the right-hand side of Eq. (14) can be further simplified by using the following expression for the dissipative terms f_k , g_k and h_k :

$$\boldsymbol{f}_k = \tilde{\boldsymbol{f}}_k + \rho_k \boldsymbol{l}_k \tag{16a}$$

$$\boldsymbol{g}_k = \alpha_k \rho_k A \mu_k \mathbb{F}(\boldsymbol{u}_k) + \boldsymbol{f}_k \otimes \boldsymbol{u}_k \tag{16b}$$

$$\boldsymbol{h}_k = \tilde{\boldsymbol{h}}_k - \frac{||\boldsymbol{u}||^2}{2} \boldsymbol{f}_k + (\rho e)_k \boldsymbol{l}_k, \tag{16c}$$

where μ_k is a positive viscosity coefficient for phase k. Note the area function A in the definition of g. Substituting the expression of the dissipative term given in Eq. (16) into Eq. (14), it yields:

$$\alpha_{k}\rho_{k}A\frac{Ds_{k}}{Dt} = \underbrace{\left(s_{e}\right)_{k}\alpha_{k}\rho_{k}A\mu_{k}\mathbb{F}(\boldsymbol{u}_{k}):\boldsymbol{\nabla}\boldsymbol{u}_{k}}_{\mathcal{R}_{1}} + \underbrace{\left[\boldsymbol{\nabla}\cdot\tilde{\boldsymbol{h}}_{k} - e_{k}\boldsymbol{\nabla}\cdot\tilde{\boldsymbol{f}}_{k}\right] + (\rho s_{\rho})_{k}\boldsymbol{\nabla}\cdot\tilde{\boldsymbol{f}}_{k}}_{\mathcal{R}_{2}} + \underbrace{\left(s_{e}\right)_{k}\boldsymbol{\nabla}\cdot(\rho_{k}e_{k}\boldsymbol{l}_{k}) - (s_{e})_{k}e_{k}\boldsymbol{\nabla}\cdot(\rho_{k}\boldsymbol{l}_{k}) + \rho_{k}(s_{\rho})_{k}\boldsymbol{\nabla}\cdot(\rho_{k}\boldsymbol{l}_{k}) - \rho_{k}^{2}(s_{\rho})_{k}\boldsymbol{\nabla}\cdot\boldsymbol{l}_{k}}_{\mathcal{R}_{2}}.$$
(17)

We now split the right-hand-side of Eq. (17) into three residuals denoted by \mathcal{R}_1 , \mathcal{R}_2 and \mathcal{R}_3 and will study the sign of each of them. Since $(s_e)_k$ is defined as the inverse of the temperature and thus positive, the sign of the first term, \mathcal{R}_1 , is conditioned by the choice of the function $\mathbb{F}(\boldsymbol{u}_k)$ so that the product with the tensor $\nabla \boldsymbol{u}_k$ is positive. As in [13, 15], $\mathbb{F}(\boldsymbol{u}_k)$ is chosen proportional to the symmetric gradient of the velocity vector $\nabla^s \boldsymbol{u}_k$, whom entries are given by $((\nabla^s \boldsymbol{u})_{i,j})_k = \frac{1}{2} (\partial_{x_i} u_i + \partial_{x_j} u_j)_k$. After a few lines of algebra, the third term \mathcal{R}_3 can be recast as a function of the gradient of the entropy as follows:

$$\mathcal{R}_2 = \rho_k A \boldsymbol{l}_k \cdot \boldsymbol{\nabla} s_k. \tag{18}$$

One of the assumptions made in the entropy minimum principle is to that the entropy is at a minimum which implies that its gradient is null. Because of this, it follows that the term \mathcal{R}_3 is zero at the minimum and thus, the entropy minimum principle is verified independently of the definition of the perturbation term l_k used in the volume fraction equation Eq. (9a). It will be explained later in this section how to derive a definition for l_k .

We now focus on the term denoted by \mathcal{R}_2 , that is found identical to the right-hand-side of the single phase entropy equation obtained from the multi-D Euler equations (see [13, 15]. Thus, the term \mathcal{R}_2 is known to be positive when (i) assuming concavity of the entropy function s_k with respect to the internal energy e_k and the specific volume $1/\rho_k$ (or convexity of $-s_k$) and (ii) choosing the following definitions for the dissipative terms \tilde{h}_k and \tilde{f}_k :

$$\tilde{\boldsymbol{f}}_k = \alpha_k A \kappa_k \boldsymbol{\nabla} \rho_k \tag{19a}$$

$$\tilde{\boldsymbol{h}}_k = \alpha_k A \kappa_k \boldsymbol{\nabla} \left(\rho e \right)_k, \tag{19b}$$

where κ_k is another positive viscosity coefficient. The entropy equation can now be written in its final form:

$$\alpha_k \rho_k A \frac{Ds_k}{Dt} = \boldsymbol{f}_k \cdot \boldsymbol{\nabla} s_k + \boldsymbol{\nabla} \cdot (\alpha_k \rho_k A \boldsymbol{\nabla} s_k) - \alpha_k A \kappa_k \mathbf{Q}_k + (s_e)_k \alpha_k A \rho_k \mu_k \boldsymbol{\nabla}^s \boldsymbol{u}_k : \boldsymbol{\nabla} \boldsymbol{u}_k,$$
 (20)

where \mathbf{Q}_k is a negative semi-definite quadratic form defined as:

$$\begin{aligned} \mathbf{Q}_k &= X_k^t \Sigma_k X_k \\ \text{with } X_k &= \begin{bmatrix} \boldsymbol{\nabla} \rho_k \\ \boldsymbol{\nabla} e_k \end{bmatrix} \text{ and } \Sigma_k = \begin{bmatrix} \partial_{\rho_k} (\rho_k^2 \partial_{\rho_k} s_k) & \partial_{\rho_k, e_k} s_k \\ \partial_{\rho_k, e_k} s_k & \partial_{e_k, e_k} s_k \end{bmatrix}. \end{aligned}$$

Eq. (20) is used to prove the entropy minimum principle: assuming that s_k reaches its minimum value in $r_{min}(t)$ at each time t, the gradient, ∇s_k , and Laplacian, Δs_k , of the entropy are null and positive at this particular point, respectively. Furthermore, it is recalled that the viscosity coefficients μ_k and κ_k are positive by definition. Then, because the terms in the right-hand-side of Eq. (20) are proven either positive or null when the entropy reaches a minimum value, the entropy minimum principle holds for each phase k, independently of the definition of the dissipative term l_k , such as:

$$\alpha_k \rho_k A \partial_t s_k(\boldsymbol{r}_{min}, t) > 0 \Rightarrow \partial_t s_k(\boldsymbol{r}_{min}, t) > 0$$

Do we need to make the above statement a theorem or property?

It remains to obtain a definition for the dissipative term l_k used in the volume fraction equation Eq. (9a). A way to achieve this is to consider the volume fraction equation, by itself and notice that it is an hyperbolic equation with eigenvalue u_{int} . An entropy equation can be derived and used to prove the entropy minimum principle by properly choosing the dissipative term [16]. The objective is to ensure positivity of the volume fraction and also uniqueness of the weak solution. Following the work of Guermond et al. in [17, 18], it can be shown that a dissipative term ensuring positivity and uniqueness of the weak solution for the volume fraction equation, is of the form $l_k = \beta_k A \nabla \alpha_k$, where β_k is a positive viscosity coefficient. The dissipative term is proportional to the area A for consistency with the other terms of the volume fraction equation Eq. (9a).

All of the dissipative terms are now defined and recalled here:

$$\boldsymbol{l}_k = \beta_k A \boldsymbol{\nabla} \alpha_k \tag{21a}$$

$$\boldsymbol{f}_k = \alpha_k A \kappa_k \boldsymbol{\nabla} \rho_k + \rho_k A \boldsymbol{l}_k \tag{21b}$$

$$\boldsymbol{g}_k = \alpha_k A \mu_k \rho \boldsymbol{\nabla}^s \boldsymbol{u}_k \tag{21c}$$

$$\boldsymbol{h}_{k} = \alpha_{k} A \kappa_{k} \nabla \left(\rho e\right)_{k} + \boldsymbol{u}_{k} : \boldsymbol{g}_{k} - \frac{||\boldsymbol{u}_{k}||^{2}}{2} \boldsymbol{f}_{k} + (\rho e)_{k} \boldsymbol{l}_{k}$$
(21d)

134 At this point, some remarks are in order:

- 1. The viscous regularization given in Eq. (21) for the multi-D seven-equation model, is equivalent to the parabolic regularization [19] when assuming $\beta_k = \kappa_k = \mu_k$ and $\mathbb{F}(\boldsymbol{u}_k) = \alpha_k \rho_k \kappa_k \boldsymbol{\nabla} \boldsymbol{u}_k$. However, decoupling between the regularization on the velocity and on the density in the momentum equation is important to make the regularization rotation invariant but also to ensure well-scaled dissipative terms for a wide range of Mach number as was shown in [15] for the multi-D Euler equations.
- 2. The dissipative term l_k requires the definition of a new viscosity coefficient β_k . It was shown that this viscosity coefficient is independent of the other viscosity coefficients μ_k and κ_k . Its definition should account for the eigenvalue associated with the void fraction equation u_{int} .
- 3. The dissipative term f_k is a function of l_k . Thus, all of the other dissipative terms are also functions of l_k .
- 4. The partial derivatives $(s_e)_k$ and $(s_{\rho_k})_k$ can be computed using the definition provided in Eq. (15) and are functions of the thermodynamic variables: pressure, temperature and density.
- 5. All of the dissipative terms are chosen to be proportional to the the void fraction α_k and the cross-sectional area A, but the one in the volume fraction equation that is only proportional to A. For instance, $\alpha_k A \nabla \rho_k$ is the flux of the dissipative term in the continuity equation through the phasic area, $\alpha_k A$, seen by the phase k. When one of the phases disappears, the dissipative terms must go to zero for consistency. On the other hand, when α_k goes to one, the single-phase Euler equations with proper viscous regularization must be recovered.
- 6. Compatibility of the viscous regularization proposed in Eq. (21) with the generalized entropies identified in Harten et al. [20] has not been investigated yet. However, it is believed that the entropy inequalities still holds because of the similarities of the entropy residual for the multi-D seven-equation model with the entropy residual derived in the single phase flow case [13].

At this point in the paper, we have derived a viscous regularization for the multi-D seven-equation two-phase flow model that ensures positivity of the entropy residual, uniqueness of the numerical solution when assuming concavity of the 167 phasic entropy s_k , and is consistent with the viscous regularization derived for the multi-D Euler equations [13, 15] in the limit $\alpha_k \to 1$. The viscous 169 regularization involves a set of three viscosity coefficients for each phase, μ_k , 170 κ_k and β_k , that are assumed positive. Definition of the viscosity coefficients is 171 now required to complete the numerical stabilization method. Since the focus of this paper is the entropy viscosity method, the viscosity coefficients will be 173 defined function of the entropy residual in Section 4. However, one can also devise a definition for the viscosity coefficients μ_k and κ_k by analogy to Lapidus 175 [21, 22] or some pressure-based methods [23] used for the single-phase Euler 176 equations. On the other hand, the viscosity coefficient, β_k , for the volume 177 fraction equation should rely on artificial dissipation stabilization methods used for scalar hyperbolic equations.

Remark. Through the derivations of the viscous regularization, it was noted that another set of dissipative terms f_k and l_k would also ensures positivity of the entropy residual:

$$\boldsymbol{l}_{k} = \beta_{k} T_{k} \left[\frac{\rho_{k}}{P_{k} + \rho_{k} e_{k}} \boldsymbol{\nabla} \left(\frac{P_{k}}{\rho_{k} e_{k}} \right) - \frac{1}{P_{k}} \boldsymbol{\nabla} \rho_{k} \right]$$
(22a)

$$\boldsymbol{f}_{k} = \kappa_{k} \boldsymbol{\nabla} \rho_{k} + \frac{\rho_{k}^{2}(s_{\rho})_{k}}{(\rho s_{\rho} - e s_{e})_{k}} \boldsymbol{l}_{k}$$
(22b)

However, the definition of l_k proposed in Eq. (22a) was not considered as valid for the following reasons: positivity of the volume fraction cannot be achieved and the parabolic regularization is not retrieved when assuming equal viscosity coefficients.

4. A definition of the viscosity coefficients for all Mach flows

- non-dimensionalize the equations but use P_{∞} for the pressure instead of $(\rho c^2)_{\infty}$
- introduce a new Pechlet number for β : its behavior should be the same as the Pechlet number for κ
- two cases: zero and infinite relaxation coefficients
- derive the normalization parameters for the isentropic and non-isentropic flows
 - discussion about the

184

185

186

187

188

189

190

191

When working with artificial dissipative numerical stabilization methods, great care needs to be carried to the definition of the viscosity coefficients that will determine the accuracy of the method. Generally speaking, sufficient artificial 195 viscosity should be added into the shock and discontinuity regions to prevent spurious oscillations from forming, while little dissipation is added when the 197 numerical solution is smooth. Such requirements can be achieved by tracking 198 shocks and discontinuities in the numerical solutions. When dealing with fluid equations, the low-mach asymptotic limit also has to be accounted for in the definition of the viscosity coefficients in order to ensure well-scaled dissipative 201 terms [24, 25, 26]. The purpose of this section is to derive a definition for the phasic viscosity coefficients, μ_k , κ_k and β_k , that ensures the correct numerical 203 solution in the low-mach limit, and can accurately resolves shocks in transonic 204 and supersonic flows. 205

4.1. Definition of the viscosity coefficients

212

214

In the entropy viscosity method, each viscosity coefficient is function of an upper and a lower bound that are referred to as first-order viscosity coefficient and entropy viscosity coefficient (high-order coefficient), respectively, as shown in Eq. (23). The first-order viscosity coefficient is denoted by the subscript max and is defined proportional to the largest local eigenvalue. The entropy viscosity coefficient is set proportional to an entropy residual and jumps of quantities to determine, and denoted by the subscript e.

$$\beta_{k}(\mathbf{r},t) = \min \left(\beta_{e,k}(\mathbf{r},t), \beta_{max,k}(\mathbf{r},t) \right),$$

$$\mu_{k}(\mathbf{r},t) = \min \left(\mu_{e,k}(\mathbf{r},t), \mu_{max,k}(\mathbf{r},t) \right),$$

$$\kappa_{k}(\mathbf{r},t) = \min \left(\kappa_{e,k}(\mathbf{r},t), \kappa_{max,k}(\mathbf{r},t) \right).$$
(23)

where all of the variables are locally defined. As for the multi-D single-phase Euler equations and for the same reasons, the entropy residual for each phase k is recast as a function of the pressure, the velocity, the density and the speed of sound as follows:

$$R_k(\mathbf{r},t) := \partial_t s_k + \mathbf{u}_k \cdot \nabla s_k = \frac{\mathrm{D}s_k}{\mathrm{D}t} = \frac{(s_e)_k}{(P_e)_k} \left(\underbrace{\frac{\mathrm{D}P_k}{\mathrm{D}t} - c_k^2 \frac{\mathrm{D}\rho_k}{\mathrm{D}t}}_{\widetilde{R}_k(\mathbf{r},t)} \right), \tag{24}$$

where $\widetilde{R}_k(\mathbf{r},t)$ is the new entropy residual of phase k and will experience the same variations as $R_k(\mathbf{r},t)$.

We first choose to investigate the definitions of the high and first-order viscosity coefficients for μ_k and κ_k . It is noted that the dissipative terms function of μ_k and κ_k are the same as the ones for the single-phase Euler equation when considering $\tilde{A} = \alpha_k A$ as a pseudo cross section. Furthermore, we need to ensure consistency with the single-phase Euler equation in the limits $\alpha_k \to 1$. Thus, based on the work done in SECTION, the first order viscosity coefficients are set proportional to the local maximum eigenvalue λ_k ,

$$\kappa_{\max,k}(\boldsymbol{r},t) = \mu_{\max,k}(\boldsymbol{r},t) = \frac{h}{2} (||\boldsymbol{u}_k|| + c_k)$$
(25)

220 and the entropy viscosity viscosity coefficients are defined as

$$\mu_{e,k}(\boldsymbol{r},t) = h^{2} \frac{\max\left(|\widetilde{R}_{k}(\boldsymbol{r}_{q},t)|, ||\boldsymbol{u}_{k}(\boldsymbol{r}_{q},t)||J[P_{k}](t), ||\boldsymbol{u}_{k}(\boldsymbol{r}_{q},t)||c_{k}^{2}(\boldsymbol{r}_{q},t)J[\rho_{k}](t)\right)}{\operatorname{norm}_{P,k}^{\mu}}$$
(26a)

221 and

222

223

224

226

228

229

230

$$\kappa_{e,k}(\boldsymbol{r},t) = h^{2} \frac{\max\left(|\widetilde{R}_{k}(\boldsymbol{r}_{q},t)|, ||\boldsymbol{u}_{k}(\boldsymbol{r}_{q},t)||J[P_{k}](t), ||\boldsymbol{u}_{k}(\boldsymbol{r}_{q},t)||c_{k}^{2}(\boldsymbol{r}_{q},t)J[\rho_{k}](t)\right)}{\operatorname{norm}_{P,k}^{\kappa}}$$
(26b)

where h is the grid size and J[x](t) denotes the jump of the quantity x and was defined in SECTION. The normalization parameters $\operatorname{norm}_{P,k}^{\mu}$ and $\operatorname{norm}_{P,k}^{\kappa}$ will be determined later in this section by inspecting the non-dimensional version of the seven-equation model.

It remains to specify the viscosity coefficients β_e and β_{max} . For the purpose of this paragraph, let us consider the scalar volume fraction equation and assume that the interface velocity \boldsymbol{u}_{int} is given. Because it is a scalar hyperbolic equation, it is proposed to define the high and first-order viscosity coefficients on the same model as Burger's equation. Thus, β_{max} is set proportional to the eigenvalue that is the interface velocity \boldsymbol{u}_{int} ,

$$\beta_{max,k}(\boldsymbol{r},t) = \frac{h}{2}||\boldsymbol{u}_{int}||, \tag{27}$$

whereas the entropy viscosity viscosity coefficient β_e is function of an entropy residual, $R_{\alpha,k}$, derived from the volume fraction equation for phase k as follows:

$$\beta_{e,k}(\boldsymbol{r},t) = h^2 \frac{\max(|R_{\alpha,k}(\boldsymbol{r}_q,t)|, ||\boldsymbol{u}_{int}(\boldsymbol{r}_q,t)||J[\alpha_k](t))}{\operatorname{norm}_b^{\beta}}$$
(28)

where $\operatorname{norm}_{k}^{\beta}$ denotes a normalization parameters whom definition will be further investigated. To derive the entropy residual $R_{\alpha,k}$, we consider the volume fraction equation for phase k with its viscous regularization and assume the existence of a mathematical entropy denoted by $\eta(\alpha_k)$:

$$\partial_t (A\alpha_k) + A \boldsymbol{u}_{int} \cdot \boldsymbol{\nabla} \alpha_k = \boldsymbol{\nabla} \cdot (\beta_k A \boldsymbol{\nabla} \alpha_k) \tag{29}$$

After multiplying by $\frac{d\eta(\alpha_k)}{d\alpha_k}$ and using the chain rule, an expression for the entropy residual $R_{\alpha,k}$ is obtained:

$$R_{\alpha,k} = \partial_t \left(A \eta(\alpha_k) \right) + A \boldsymbol{u}_{int} \cdot \boldsymbol{\nabla} \eta(\alpha_k) = \frac{\mathrm{d} \eta(\alpha_k)}{\mathrm{d} \alpha_k} \boldsymbol{\nabla} \cdot (\beta_k A \boldsymbol{\nabla} \alpha_k)$$
 (30)

Because Eq. (30) is identical to Eq. (??), it is concluded that $R_{\alpha,k} \geq 0$ when assuming η convex with respect to α_k , which justifies the definition of the entropy viscosity viscosity coefficient $\beta_{e,k}$ given in Eq. (28) based on Eq. (??).

The entropy function is taken equal to $\eta(\alpha_k) = \frac{\alpha_k^2}{2}$ which is convex.

4.2. Low-Mach asymptotic limit of the seven-equation model

In order to have a complete definition for the viscosity coefficients β_k , μ_k and κ_k , the normalization parameters introduced in the definition of the entropy viscosity coefficients $\beta_{e,k}$, $\mu_{e,k}$ and $\kappa_{e,k}$ have to be determined. In SECTION, the normalization parameters were derived from the non-dimensionalized multi-D Euler equations in order to obtain well-scaled dissipative terms. Thus, it is proposed to follow the same method to derive the three normalization parameters norm $\mu_{P,k}$, norm $\mu_{P,k}$ and norm $\mu_{P,k}$ and norm $\mu_{P,k}$ are definition of the viscosity coefficients involved in the viscous regularization of the seven-equation model. For simplicity, the Ideal Gas equation of state is considered through the derivations.

For now, the definition of the viscosity coefficients is simply derived by analogy to SECTION. First, we define the far-field or stagnation coefficients for each phase as it is done in Eq. (??) by adding the subscript k to ∞ . Then, the scaled equations are derived for each phase which leads to the definition of a phasic Péclet and Reynolds numbers referred to as Pé_k and Re_k, respectively, that are tied to the far-field or stagnation quantities of the viscosity coefficients $\mu_{k,\infty}$ and $\kappa_{k,\infty}$ as shown in Eq. (31):

$$\operatorname{Re}_{k,\infty} = \frac{u_{k,\infty} L_{\infty}}{\mu_{k,\infty}} \text{ and } \operatorname{P\acute{e}}_{k,\infty} = \frac{u_{k,\infty} L_{\infty}}{\kappa_{k,\infty}}.$$
 (31)

Because the viscous regularization derived previously in SECTION requires an extra viscosity coefficient β_k for the volume fraction equation, a new Péclet number, $P\acute{e}^{\beta}_{k,\infty}$ is also defined as follows,

$$P\acute{e}_{k,\infty}^{\beta} = \frac{u_{int,\infty}L_{\infty}}{\beta_{k,\infty}}$$
 (32)

that will allow us to derive the proper scaling for $\beta_{k,\infty}$. Once the scaled equations are obtained, the scaling of the numerical numbers can be chosen in order to meet the different criteria already listed in SECTION. The scaling of the new Péclet number we defined, $P\acute{e}^{\beta}_{k,\infty}$, is derived from the scaled volume fraction equation that does not contain any term weighted by the reference Mach number M_{∞} , which yields $P\acute{e}^{\beta}_{k,\infty} = 1$ to have a well-scaled dissipative term. This scaling is the same as for $P\acute{e}_{k,\infty}$ from the continuity equation: the volume fraction and continuity equations have similar behavior since they are both advection-type equations. Thus, based on the reasoning used in SECTION, the following definitions for the viscosity coefficients is proposed in Eq. (33):

$$\mu_k(\mathbf{r},t) = \min\left(\mu_{\max,k}(\mathbf{r},t), \mu_{e,k}(\mathbf{r},t)\right) \text{ and } \kappa_k(\mathbf{r},t) = \min\left(\mu_{\max,k}(\mathbf{r},t), \kappa_{e,k}(\mathbf{r},t)\right)$$
(33a)

where the first-order viscosity is given by

$$\kappa_{\max,k}(\boldsymbol{r},t) = \mu_{\max,k}(\boldsymbol{r},t) = \frac{h}{2}(||\boldsymbol{u}_k|| + c_k)$$
(33b)

273 and the entropy viscosity coefficients by

$$\kappa_{e,k}(\boldsymbol{r},t) = \frac{h^2 \max(\widetilde{R}_k, J_k)}{\rho_k c_k^2} \text{ and } \mu_{e,k}(\boldsymbol{r},t) = \frac{h^2 \max(\widetilde{R}_k, J_k)}{\operatorname{norm}_{P,k}^{\mu}}$$
(33c)

274 with the jumps given by

$$J_k = \max\left(||\boldsymbol{u}_k||[[\boldsymbol{\nabla}P_k \cdot \boldsymbol{n}]], ||\boldsymbol{u}_k||c_k^2[[\boldsymbol{\nabla}\rho_k \cdot \boldsymbol{n}]]\right)$$
(33d)

where norm $_{P,k}^{\kappa}$ is computed from Eq. (34).

$$\operatorname{norm}_{P}^{\mu} = (1 - \sigma(M))\rho c^{2} + \sigma(M)\rho||\boldsymbol{u}||^{2}$$
(34)

where M_k is the local Mach number for phase k. The function $\sigma(M)$ is taken from Eq. (??) with the same parameters as for the single-phase flow equations: a=3 and $M^{thres}=0.05$. The jump J_k is a function of the jump of pressure and density gradients across the face with respect to its normal vector n. Then, the largest value over all faces is determined and used in the definition of the viscosity coefficients. Lastly, the viscosity coefficient for the volume fraction equation is given by:

$$\beta_k(\mathbf{r},t) = \min \left(\beta_{\max,k}(\mathbf{r},t), \beta_{e,k}(\mathbf{r},t) \right)$$
(35)

²⁸³ where the first-order viscosity is given by

$$\beta_{\max,k}(\boldsymbol{r},t) = \frac{h}{2}||\boldsymbol{u}_{int}|| \tag{36}$$

and the corresponding entropy viscosity coefficient, $\beta_{e,k}$, by

$$\beta_{e,k}(\mathbf{r},t) = \frac{h^2 \max(R_{\alpha,k}, J_{\alpha,k})}{\|\alpha_k - \bar{\alpha}_k\|_{\infty}},$$
(37)

where $\bar{\alpha}_k$ is the average value of the volume fraction over the entire computational domain, and $||\cdot||_{\infty}$ denotes the infinite norm. The definition of the $\beta_{e,k}$ is consistent with the scaling of $P\acute{e}^{\beta}_{k,\infty}=1$. The jump is given by:

$$J_{\alpha,k} = ||\boldsymbol{u}_{int}|| \cdot [[\boldsymbol{\nabla}\alpha_k \cdot \boldsymbol{n}]]. \tag{38}$$

With the definition of the viscosity coefficients μ_k and κ_k proposed in Eq. (??), 288 the low-Mach asymptotic limit is ensured for isentropic flow, and transonic flows with shocks will be correctly resolved for each phase k. Furthermore, 290 the definition of the viscosity coefficient β_k is consistent with the EVM used 291 for the scalar hyperbolic equations and thus should efficiently stabilize shocks 292 forming the in the volume fraction profile. Plus, it is noted that the viscous regularization and the definition of the viscosity coefficients proposed for the 294 seven-equation two-phase flow model degenerates into the EVM used for the 295 single-phase Euler equations. In order to validate the proposed definition of the 296 viscosity coefficients, 1-D numerical simulations are performed in SECTION. 297

5. 1-D numerical results

- simple advection problem
- shock tube with two independent fluids: exact solution and could do convergence test for this particular test
 - shock tube with infinite relaxation coefficients
- 1-D nozzle with two independent fluids
 - 1-D nozzle with infinite relaxation coefficients
 - 1-D nozzle with infinite relaxation coefficients, mass and heat transfer

306 References

299

- [1] A. K. Kapila, R. Menikoff, J. B. B. S. F. Son, D. S. Stewart, Two-phase modeling of deflagration-to-detonation transition in granular materials, Phys. Fluids (2001) 3002–3024.
- [2] I. Toumi, An upwind numerical method for two-fluids two-phases flow models, Nucl. Sci. Eng. (1996) 147–168.
- 312 [3] R. Berry, R. Saurel, O. LeMetayer, The discrete equation method (dem) 313 for fully compressible, two-phase flows in ducts of spatially varying cross-314 section, Nuclear Engineering and Design 240 (2010) 3797–3818.
- R. Abgrall, How to prevent pressure oscillations in multicomponent flow calcuations: a quasi conservative appraoch, J. Comput. Phys (2002) 125–150.
- ³¹⁸ [5] R. Saurel, R. Abgrall, A multiphase godunov method for compressible multifluid and multiphase flows, J. Comput Physics (2001) 425–267.
- ³²⁰ [6] R. Saurel, O. Lemetayer, A multiphase model for compressible flows with interfaces, shocks, detonation waves and cavitation, J. Comput Physics (2001) 239–271.
- ³²³ [7] Q. Li, H. Feng, T. Cai, C. Hu, Difference scheme for two-phase flow, Appl Math Mech (2004) 536.
- ³²⁵ [8] A. Zein, M. Hantke, G. Warnecke, Modeling phase transition for compressible two-phase flows applied to metastabe liquids, J. Comput Physics (2010) ³²⁷ 2964.
- [9] A. Ambroso, C. Chalons, P.-A. Reviart, A godunov-type method for the seven-equation model of compressible multiphase mixtures, Comput. Fluids (2012) 67–91.

- [10] R. A. Berry, M. Delchini, J. Ragusa, Relap-7 numrerical stabilization: Entropy viscosity method, Tech. Rep. INL/EXT-14-32352, Idaho National Laboratory, USA (2014).
- [11] R. Saurel, F. Petitpas, R. A. Berry, Simple and efficient relaxation methods
 for interfaces separating compressible fluids, cavitating flows and shocks in
 multiphase mixtures, J. of Computational Physics 228 (2009) 1678–1712.
- [12] J. M. Herrard, O. Hurisse, A simple method to compute standard two-fluid
 models, Int. J. of Computational Fluid Dynamics 19 (2005) 475–482.
- [13] J. L. Guermond, B. Popov, Viscous regularization of the euler equations
 and entropy principles, under review.
- [14] M. Delchini, Extension of the entropy viscosity method to multi-d euler equations and the seven-equation two-phase model, Tech. rep., Texas A& M University, USA (2014).
- [15] M. Delchini, J. Ragusa, R. Berry, Entropy-based viscosity regularization
 for the multi-dimensional euler equations in low-mach and transonic flows,
 under review.
- [16] R. Leveque, Numerical Methods for Conservation Laws, Birkhuser Basel,
 Zurich, Switzerland, 1990.
- [17] J. L. Guermond, R. Pasquetti, Entropy viscosity method for nonlinear conservation laws, Journal of Comput. Phys 230 (2011) 4248–4267.
- J. L. Guermond, R. Pasquetti, Entropy viscosity method for high-order approximations of conservation laws, Lecture Notes in Computational Science and Engineering 76 (2011) 411–418.
- ³⁵⁴ [19] B. Perthane, C. W. Shu, On positivity preserving finite volume schemes for euler equations, Numer. Math. 73 (1996) 119–130.
- [20] A. Harten, L. P. Franca, M. Mallet, Convex entropies and hyperbolicity for
 general euler equations, SIAM J Numer Anal 6 (1998) 2117–2127.
- ³⁵⁸ [21] A. Lapidus, A detached shock calculation by second order finite differences, J. Comput. Phys. 2 (1967) 154–177.
- [22] J. Donea, A. Huerta, Finite Element Methods for Flow Problems, Oxford
 University Press, 2003.
- [23] R. Lohner, Applied CFD Techniques: an Introduction based on Finite Element Methods, 2^{nd} Edition Wiley, 2003.
- ³⁶⁴ [24] H. Guillard, C. Viozat, On the behavior of upwind schemes in the low mach number limit, Computers & Fluids 28 (1999) 63–86.

- [25] E. Turkel, Preconditioned techniques in computational fluid dynamics,
 Annu. Rev. Fluid Mech. 31 (1999) 385–416.
- [26] J. S. W. D. L, Darmofal, J. Peraire, The solution of the compressible euler
 equations at low mach numbers using a stabilized finite element algorithm,
 Comput. Methods Appl. Mech. Engrg. 190 (2001) 5719–5737.

Appendix A Entropy equation for the multi-D seven equation model without viscous regularization

This appendix provides the steps that lead to the derivation of the phasic entropy equation of the seven-equation model [3]. For the purpose of this dissertation, two phases are considered and denoted by the indexes j and k. In the seven-equation model, each phase obeys to the following set of equations (Eq. (39)):

$$\partial_t \left(\alpha_k A \right) + A \boldsymbol{u}_{int} \cdot \boldsymbol{\nabla} \alpha_k = A \mu \left(P_k - P_i \right) \tag{39a}$$

$$\partial_t \left(\alpha_k \rho_k A \right) + \nabla \cdot \left(\alpha_k \rho_k \boldsymbol{u}_k A \right) = 0 \tag{39b}$$

$$\partial_{t} (\alpha_{k} \rho_{k} \boldsymbol{u}_{k} A) + \boldsymbol{\nabla} \cdot [\alpha_{k} A (\rho_{k} \boldsymbol{u}_{k} \otimes \boldsymbol{u}_{k} + P_{k} \mathbb{I})] = \alpha_{k} P_{k} \boldsymbol{\nabla} A + P_{int} A \boldsymbol{\nabla} \alpha_{k} + A \lambda (\boldsymbol{u}_{j} - \boldsymbol{u}_{k})$$
(39c)

$$\partial_{t} \left(\alpha_{k} \rho_{k} E_{k} A \right) + \nabla \cdot \left[\alpha_{k} A \boldsymbol{u}_{k} \left(\rho_{k} E_{k} + P_{k} \right) \right] = P_{int} A \boldsymbol{u}_{int} \cdot \nabla \alpha_{k} - \mu \bar{P}_{int} \left(P_{k} - P_{j} \right) + \bar{\boldsymbol{u}}_{int} A \lambda \left(\boldsymbol{u}_{j} - \boldsymbol{u}_{k} \right)$$
(39d)

where ρ_k , u_k , E_k and P_k are the density, the velocity, the specific total energy and the pressure of k^{th} phase, respectively. The pressure and velocity relaxation parameters are denoted by μ_P and λ_u , respectively. The variables with index int correspond to the interfacial variables and a definition is given in Eq. (40). The cross section A is only function of space: $\partial_t A = 0$.

$$\begin{cases}
P_{int} = \bar{P}_{int} - \frac{\nabla \alpha_k}{||\nabla \alpha_k||} \frac{Z_k Z_j}{Z_k + Z_j} \left(\boldsymbol{u}_k - \boldsymbol{u}_j \right) \\
\bar{P}_{int} = \frac{Z_k P_j + Z_j P_k}{Z_k + Z_j} \\
\boldsymbol{u}_{int} = \bar{\boldsymbol{u}}_{int} - \frac{\nabla \alpha_k}{||\nabla \alpha_k||} \frac{P_k - P_j}{Z_k + Z_j} \\
\bar{\boldsymbol{u}}_{int} = \frac{Z_k \boldsymbol{u}_k + Z_j \boldsymbol{u}_j}{Z_k + Z_j}
\end{cases}$$
(40)

where $Z_k = \rho_k c_k$ and $Z_j = \rho_j c_j$ are the impedance of the phase k and j, respectively. The speed of sound is denoted by the variable c. The function sgn(x) returns the sign of the variable x.

The first step consists of rearranging the equations given in Eq. (40) using the

primitive variables $(\alpha_k, \rho_k, \boldsymbol{u}_k, e_k)$, where e_k is the specific internal energy of k^{th} phase. We introduce the material derivative $\frac{D(\cdot)}{Dt} = \partial_t(\cdot) + \boldsymbol{u}_k \cdot \boldsymbol{\nabla}(\cdot)$ for simplicity.

The void fraction is unchanged. The continuity equation is modified as follows:

$$\alpha_k A \frac{D\rho_k}{Dt} + \rho_k A \mu \left(P_k - P_j \right) + \rho_k A \left(\boldsymbol{u}_k - \boldsymbol{u}_j \right) \cdot \boldsymbol{\nabla} \alpha_k + \rho_k \alpha_k \boldsymbol{\nabla} \cdot (A \boldsymbol{u}_k) = 0 \quad (41)$$

The momentum and continuity equations are combined to yield the velocity equation:

$$\alpha_{k}\rho_{k}A\frac{D\boldsymbol{u}_{k}}{Dt} + \partial_{x}\left(\alpha_{k}AP_{k}\right) = \alpha_{k}P_{k}\boldsymbol{\nabla}A + P_{int}A\boldsymbol{\nabla}\alpha_{k} + A\lambda_{u}\left(\boldsymbol{u}_{j} - \boldsymbol{u}_{k}\right)$$
(42)

The internal energy is obtained from the total energy and the kinetic equation $(u_k*Eq. (42))$:

$$\alpha_{k}\rho_{k}A\frac{De_{k}}{Dt} + \nabla \cdot (\alpha_{k}\boldsymbol{u}_{k}AP_{k}) - \boldsymbol{u}_{k} \cdot \nabla (\alpha_{k}AP_{k}) = P_{int}A(\boldsymbol{u}_{int} - \boldsymbol{u}_{k}) \cdot \nabla \alpha_{k}$$
$$-\alpha_{k}P_{k}\boldsymbol{u}_{k} \cdot \nabla A - \bar{P}_{int}A\mu_{P}(P_{k} - P_{j}) + A\lambda_{u}(\boldsymbol{u}_{j} - \boldsymbol{u}_{k}) \cdot (\bar{\boldsymbol{u}}_{int} - \boldsymbol{u}_{k})$$
(43)

In the next step, we assume the existence of a phase wise entropy s_k function of the density ρ_k and the internal energy e_k . Using the chain rule,

$$\frac{Ds_k}{Dt} = (s_\rho)_k \frac{D\rho_k}{Dt} + (s_e)_k \frac{De_k}{Dt},\tag{44}$$

along with the internal energy and the continuity equations, the following entropy equation is obtained:

$$\alpha_k \rho_k A \frac{Ds_k}{Dt} + \underbrace{A \left(P_k(s_e)_k + \rho_k^2(s_\rho)_k \right) \boldsymbol{u}_k \cdot \boldsymbol{\nabla} \alpha_k + \alpha_k \left(P_k(s_e)_k + \rho_k^2(s_\rho)_k \right) \boldsymbol{u}_k \cdot \boldsymbol{\nabla} A}_{\text{(a)}} =$$

$$(s_e)_k P_{int} A \left[(\boldsymbol{u}_{int} - \boldsymbol{u}_k) \cdot \boldsymbol{\nabla} \alpha_k - \bar{P}_{int} A \mu_P (P_k - P_j) + A \lambda_u (\bar{\boldsymbol{u}}_{int} - \boldsymbol{u}_k) \cdot (\boldsymbol{u}_j - \boldsymbol{u}_k) \right] - \rho^2 (s_\rho)_k \left[\mu_P A (P_k - P_j) + A (\boldsymbol{u}_k - \boldsymbol{u}_{int}) \cdot \boldsymbol{\nabla} \alpha_k \right]$$
(45)

where $(s_e)_k$ and $(s_\rho)_k$ denote the partial derivatives of the entropy s_k with respect to the internal energy e_k and the density ρ_k , respectively. The second term, (a), in the left hand side of Eq. (45) can be set to zero by assuming the following relation between the partial derivatives of the entropy s_k :

$$P_k(s_e)_k + \rho_k^2(s_\rho)_k = 0. (46)$$

The above equation is equivalent to the application of the second thermodynamic law when assuming reversibility:

$$T_k ds_k = de_k - \frac{P_k}{\rho_k^2} d\rho_k \text{ with } (s_e)_k = \frac{1}{T_k} \text{ and } (s_\rho)_k = -\frac{P_k}{\rho_k^2} (s_e)_k$$
 (47)

Thus, equation Eq. (45) can be rearranged using the relation $(s_{\rho})_k = -\frac{P_k}{\rho_L^2}(s_e)_k$:

$$((s_e)_k)^{-1}\alpha_k\rho_k\frac{Ds}{Dt} = \underbrace{[P_{int}(\boldsymbol{u}_{int} - \boldsymbol{u}_k) + P_k(\boldsymbol{u}_k - \boldsymbol{u}_{int})] \cdot \boldsymbol{\nabla}\alpha_k}_{\text{(b)}} + \underbrace{\mu(P_k - P_j)(P_k - \bar{P}_{int})}_{\text{(c)}} + \underbrace{\lambda(\boldsymbol{u}_j - \boldsymbol{u}_k) \cdot (\bar{\boldsymbol{u}}_{int} - \boldsymbol{u}_k)}_{\text{(d)}}$$
(48)

The right hand side of equation Eq. (48) is split into three terms (b), (c) and (d) that will be treated independently from each other. The terms (c) and (d) are simpler to start with and can be easily recast by using the definitions of \bar{u}_{int} and \bar{P}_{int} given in equation Eq. (40):

$$\mu(P_k - P_j)(P_k - \bar{P}_{int}) = \mu_P \frac{Z_k}{Z_k + Z_j} (P_j - P_k)^2$$

$$\lambda(\boldsymbol{u}_j - \boldsymbol{u}_k) \cdot (\bar{\boldsymbol{u}}_{int} - \boldsymbol{u}_k) = \lambda_u \frac{Z_j}{Z_k + Z_j} (\boldsymbol{u}_j - \boldsymbol{u}_k)^2$$

$$(49)$$

By definition, μ_P , λ_u and Z_k are all positive. Thus, the above terms are unconditionally positive.

It remains to look at the last term (b). Once again, by using the definition of P_{int} and u_{int} , and the following relations:

$$u_{int} - u_k = \frac{Z_j}{Z_k + Z_j} (u_j - u_k) - \frac{\nabla \alpha_k}{||\nabla \alpha_k||} \frac{Pk - P_j}{Z_k + Z_j}$$

$$P_{int} - P_k = \frac{Z_k}{Z_k + Z_j} (P_j - P_k) - \frac{\nabla \alpha_k}{||\nabla \alpha_k||} \frac{Z_k Z_j}{Z_k + Z_j} (u_k - u_j),$$

407 (b) yields:

$$[P_{int}(\boldsymbol{u}_{int} - \boldsymbol{u}_{k}) + P_{k}(\boldsymbol{u}_{k} - \boldsymbol{u}_{int})] \cdot \boldsymbol{\nabla} \alpha_{k} = (P_{int} - P_{k})(\boldsymbol{u}_{int} - \boldsymbol{u}_{k}) \cdot \boldsymbol{\nabla} \alpha_{k} = \frac{Z_{k}}{(Z_{k} + Z_{j})^{2}} \boldsymbol{\nabla} \alpha_{k} \cdot \left[Z_{j}(\boldsymbol{u}_{j} - \boldsymbol{u}_{k})(P_{j} - P_{k}) + \frac{\boldsymbol{\nabla} \alpha_{k}}{||\boldsymbol{\nabla} \alpha_{k}||} Z_{j}^{2}(\boldsymbol{u}_{j} - \boldsymbol{u}_{k})^{2} + \frac{\boldsymbol{\nabla} \alpha_{k}}{||\boldsymbol{\nabla} \alpha_{k}||} (P_{k} - P_{j})^{2} + \frac{\boldsymbol{\nabla} \alpha_{k} \cdot \boldsymbol{\nabla} \alpha_{k}}{||\boldsymbol{\nabla} \alpha_{k}||^{2}} (P_{k} - P_{j}) Z_{j}(\boldsymbol{u}_{k} - \boldsymbol{u}_{j}) \right] (50)$$

The above equation is factorized by $||\nabla \alpha_k||$ and then recast under a quadratic form when noticing that $\frac{\nabla \alpha_k \cdot \nabla \alpha_k}{||\nabla \alpha_k||^2} = 1$, which yields:

$$[(\boldsymbol{u}_{int} - \boldsymbol{u}_k)P_{int} + (\boldsymbol{u}_k - \boldsymbol{u}_{int})P_k] \boldsymbol{\nabla}\alpha_k = ||\boldsymbol{\nabla}\alpha_k|| \frac{Z_k}{(Z_k + Z_j)^2} [Z_j(\boldsymbol{u}_j - \boldsymbol{u}_k) + \frac{\boldsymbol{\nabla}\alpha_k}{||\boldsymbol{\nabla}\alpha_k||} (P_k - P_j)]^2$$
(51)

Thus, using results from Eq. (48), Eq. (49), Eq. (50) and Eq. (51), the entropy equation obtained in [3] holds and is recalled here for convenience:

$$(s_e)_k^{-1} \alpha_k \rho_k A \frac{Ds_k}{Dt} = \mu_P \frac{Z_k}{Z_k + Z_j} (P_j - P_k)^2 + \lambda_u \frac{Z_j}{Z_k + Z_j} (\boldsymbol{u}_j - \boldsymbol{u}_k)^2$$
$$\frac{Z_k}{(Z_k + Z_j)^2} \left[Z_j (\boldsymbol{u}_j - \boldsymbol{u}_k) + \frac{\boldsymbol{\nabla} \alpha_k}{||\boldsymbol{\nabla} \alpha_k||} (P_k - P_j) \right]^2.$$