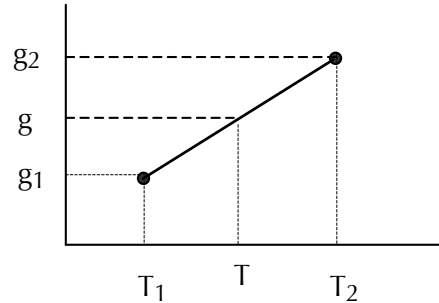


PHYS1131 HIGHER PHYSICS 1A

HOMEWORK PROBLEM SET 4

Temperatures

$$1. \quad g(T) = g_1 + \frac{g_2 - g_1}{T_2 - T_1} (T - T_1) \approx 31.2$$



2. Both the ruler (r) and the Rod (R) expand when placed in the oven
Initial is indicated by subscript i, final by subscript f

Start by working out how 1cm of ruler changes when heated:

$$\begin{aligned} \Delta L_r &= \alpha_r L_{ri} \Delta T = 1.1 \times 10^{-5} (^{\circ}C^{-1}) \times 1(cm) \times 250(^{\circ}C) \\ &= 2.75 \times 10^{-3} cm \end{aligned}$$

ie. 1cm of ruler now measures 1.00275cm

Now work out the actual final length of the rod

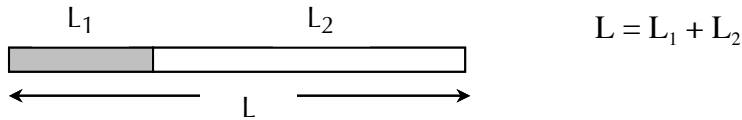
$$\begin{aligned} L_{Rf} &= 20.11cm \times 1.00275cm/cm \\ &= 20.165cm \end{aligned}$$

Now use change in length of Rod to calculate α_R

$$\begin{aligned} \Delta L_R &= L_{Rf} - L_{Ri} = 20.165 - 20.05cm \\ &= 0.115cm \end{aligned}$$

$$\alpha_R = \frac{\Delta L_R}{L_{Ri} \Delta T} = \frac{0.115cm}{20.05cm \times 250^{\circ}C} = 2.3 \times 10^{-5} (^{\circ}C^{-1}) (2sig.fig.)$$

3.



$$\begin{aligned}\frac{\delta L}{L} &= ? \quad L + \delta L = L_1(1 + \alpha_1 \Delta T) + L_2(1 + \alpha_2 \Delta T) \\ &= L_1 + L_2 + (L_1 \alpha_1 + L_2 \alpha_2) \Delta T \\ &= L \left(1 + \frac{L_1 \alpha_1 + L_2 \alpha_2}{L} \right) \Delta T \\ \delta L &= L \left(\frac{L_1 \alpha_1 + L_2 \alpha_2}{L} \right) \Delta T \\ \Rightarrow \alpha &= \frac{L_1 \alpha_1 + L_2 \alpha_2}{L}\end{aligned}$$

$$\begin{aligned}d_1 &= 11 \cdot 10^{-6} & L &= 52.4 \text{ cm} \\ \alpha_2 &= 19 \cdot 10^{-6} & d &= 13 \cdot 10^{-6} \text{ K}^{-1}\end{aligned}$$

$$\begin{aligned}\frac{L_1 \alpha_1 + L_2 \alpha_2}{L} &= \alpha & L_1 + L_2 &= L & L_1 &= L - L_2 \\ L_1 \alpha_1 + L_2 \alpha_2 &= L \alpha & (L - L_2) \alpha_1 + L_2 \alpha_2 &= L \alpha \\ L_2 &= \frac{L(\alpha - \alpha_1)}{\alpha_2 - \alpha_1} \approx 13 \text{ cm} \\ L_1 &= \frac{L(\alpha - \alpha_2)}{\alpha_1 - \alpha_2} \approx 39 \text{ cm}\end{aligned}$$

Kinetic theory and the ideal gas

$$\begin{aligned}4. \quad P_1 &= 1.00 \text{ atm} = 76.0 \text{ cm Hg} (= 1013 \times 10^2 \text{ Pa} = 1.013 \times 10^5 \text{ Pa}) \\ T_1 &= 22.0^\circ\text{C} & PV &= nRT \text{ (Ideal Gas equation, } n \# \text{ moles)} \\ V_1 &= 3.47 \text{ m}^3\end{aligned}$$

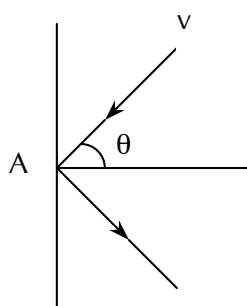
$$P_2 = 36.0 \text{ cm Hg} \quad \frac{PV}{T} = \text{const}$$

$$T_2 = -48.0^\circ\text{C}$$

$$V_2 = ? \quad \frac{P_1 V_1}{T_1} = \frac{P_2 V_2}{T_2}$$

$$T_{(k)} = T(^{\circ}\text{C}) + 273 \quad V_2 = \frac{P_1}{P_2} \cdot \frac{T_2}{T_1} \cdot V_1 \approx 5.59 \text{ m}^3$$

5.



$$\Delta p = 2 m v \cos \theta \quad F = \frac{\Delta p}{\Delta t}$$

$$\frac{N}{\Delta t} \text{ collisions/second} = 1.0 \times 10^{23} \text{ s}^{-1}$$

$$\text{pressure} = \frac{\sum F}{A} = \frac{\frac{\Delta p}{\Delta t} \cdot N}{A} = \frac{2mv \cos \theta \cdot N / \Delta t}{A} \approx 0.19 \frac{\text{N}}{\text{cm}^2}$$

$$= 1900 \text{ Pa}$$

6. (a) $m = 3.3 \times 10^{-27} \text{ kg}$
 $A = 2.0 \times 10^{-4} \text{ m}^2$
 $Q = 55^\circ$
 $v = 1.0 \times 10^3 \text{ m/s}$

$m = 0.315 \text{ kg}$
 $\text{NH}_3 \quad \mu = (14+3) \cdot 10^{-3} \text{ kg/mole} \quad [\text{Since N} + 3 \times \text{H}]$
 $P = 1.35 \times 10^6 \text{ Pa}$

$PV = nRT$ where $n = \frac{m}{\mu}$ number of moles; μ mass for 1 mole

$T = 273 + 77 = 350 \text{ K}$

$V = \frac{mRT}{\mu P} \approx 0.0399 \text{ m}^3 \quad R = 8.31 \text{ J.K}^{-1}/\text{mole}$

(b) $p_1 = 8.68 \cdot 10^5 \text{ Pa} \quad T_1 = 295 \text{ K}$

$m_1 = \frac{\mu P_1 V}{RT_1} = 0.240 \text{ kg} \quad \Rightarrow \quad \Delta m = m - m_1 = 0.075 \text{ kg} = 75 \text{ g}$

7. Mass of air in the balloon: $\rho_0 V$ in normal conditions
Archimedes principle: Upthrust = Weight of air displaced
We need: $(M + m_1)g = (\rho_0 - \rho_1)Vg$
 $\Rightarrow \rho_1 = \rho_0 - \frac{(M + m_1)}{V} \quad (1)$

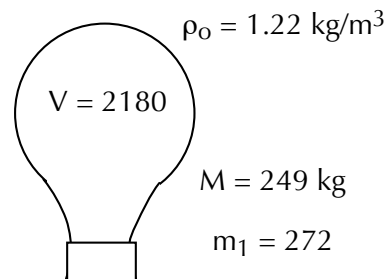
To solve for T we need a relationship between ρ and T
Start with the ideal gas law:

$PV = nRT$; $n = \frac{m}{\mu}$ where μ is the molar mass

$\frac{P\mu}{R} = \frac{m}{V}T = \rho T = \text{constant since } P, \mu \text{ and } R \text{ are constant}$
 $\Rightarrow \rho_0 T_0 = \rho_1 T_1 \quad (2)$

Substitute (2) into (1):

$\frac{\rho_0 T_0}{T_1} V = \rho_0 V - (M + m_1)$
 $\Rightarrow T_1 = \frac{\rho_0 T_0 V}{\rho_0 V - M - m_1}$
 $= \frac{1.22 \times (273 + 18) \times 2180}{1.22 \times 2180 - 249 - 272} = 362 \text{ K} = 89.0^\circ \text{C}$



Past exam question

- a) $T_o = 20^\circ\text{C}$; Power supplied P ; Water boiling $F = 0.020 \text{ L/min}$

Supply power at such a rate that amount of water neither increases or decreases; ignore other heat losses

In steady state, Energy supplied = heat to raise to boiling (i.e. ΔT) + heat to boil

ie. $P \cdot t = Mc\Delta T + ML$ c specific heat; L Latent heat; M mass

Flow Rate $F = M/t$ if amount water unchanged

Thus $P = F\rho(c\Delta T + L)$

$$= 0.020 \frac{10^{-3}}{60} 1000 \left(4200(100 - 20) + 2.3 \cdot 10^6 \right) \text{W} = 878 \text{ W}$$

$$= 880 \text{ W to 2 S. F.}$$

- b) (i) Rod A Length $L_A = (L_o + D_o)(1 + \alpha_A(T - T_o))$

Cylinder B length $L_B = L_o(1 + \alpha_B(T - T_o))$

Thus at $T = T_o$ difference is $(L_A - L_D) = D_o$, as required

$$\begin{aligned} \text{At } T \quad (L_A - L_B) &= (L_o + D_o)(1 + \alpha_A(T - T_o)) - L_o(1 + \alpha_B(T - T_o)) \\ &= D_o + L_o(T - T_o)(\alpha_A - \alpha_B) + D_o\alpha_A(T - T_o) \end{aligned}$$

$$\text{i.e.} \quad D = D_o(1 + \alpha_A\Delta T) + L_o(\alpha_A - \alpha_B)\Delta T$$

- (ii) We require that D is independent of temperature

$$\text{i.e.} \quad \Delta T [D_o\alpha_A + L_o(\alpha_A - \alpha_B)] = 0$$

$$\text{thus } D_o\alpha_A = L_o(\alpha_B - \alpha_A)$$

$$\text{or} \quad \frac{D_o}{L_o} = \left(\frac{\alpha_B - \alpha_A}{\alpha_A} \right) = \left(\frac{\alpha_B}{\alpha_A} - 1 \right)$$

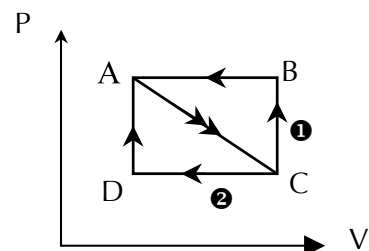
8.

Work done on gas: $dW = -pdV$

Around closed path, therefore, work done

$$W = -\oint pdV = -\text{Area enclosed by path}$$

Along path ① this is negative



Along path ② this is positive

Consider the components to the integrals, to see this

$$\text{Path 1: } \int_A^C + \int_C^B + \int_B^A$$

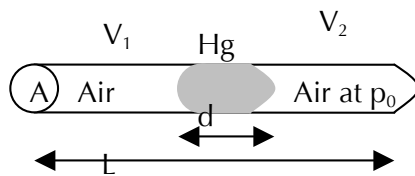
$$\text{Path 2: } \int_A^C + \int_C^D + \int_D^A$$

Area of triangle $\frac{1}{2} (8-2)(20-5) \times 1000 = 45,000$

The work done on Path 1 is - 45 kJ = 45 kJ

Work done on Path 2 is -45 kJ

9.



$L = 1.00\text{m}$, $d = 0.100\text{m}$, $p_0 = 1\text{atm} = 1013.10^2\text{Pa}$

$$V_1 = A\left(\frac{L-d}{2}\right), \quad V_2 = A\left(\frac{L-d}{2}\right)$$

$$V_1' = A\left(\frac{L-d}{2} - x\right), \quad V_2' = A\left(\frac{L-d}{2} + x\right), \quad x = \text{displacement of Hg}$$

Isothermal:

$$p_1' = \frac{p_0}{1 - \frac{x}{\frac{L-d}{2}}}, \quad p_2' = \frac{p_0}{1 + \frac{x}{\frac{L-d}{2}}} \quad \text{NOTE } \frac{1}{1-\alpha} = 1 + \alpha \quad \text{if } \alpha \ll 1 \quad \text{with } \alpha = \frac{2x}{L-d} \ll 1$$

$$p_2' - p_1' \approx p_0 \frac{2x}{\frac{L-d}{2}} = \rho g d \quad \text{where } \rho \text{ is density of mercury}$$

$$x_T = \frac{\rho g d \frac{L-d}{2}}{2p_0} \approx 2.96\text{cm}$$

For adiabatic process $PV^\gamma = \text{const}$

$$p_1' = \frac{p_0 A^\gamma \left(\frac{L-d}{2}\right)^\gamma}{A^\gamma \left(\frac{L-d}{2} - x\right)^\gamma} = \frac{p_0}{\left(1 - \frac{x}{\frac{L-d}{2}}\right)^\gamma}$$

$$p'_2 = \frac{p_0}{\left(1 + \frac{x}{L-d}\right)^\gamma}$$

$$p = \rho gh \Rightarrow p'_1 - p'_2 = \rho gd, \text{ and expand, assuming } x \ll (L-d)/2$$

$$p_0 \frac{2\gamma x}{\left(\frac{L-d}{2}\right)} = \rho gd \Rightarrow x_a = \frac{\rho gd \left(\frac{L-d}{2}\right)}{2\gamma p_0} = \frac{x_{isothermal}}{\gamma} = 2.11 \text{ cm}$$

Process is probably rapid, so an adiabatic change is initially appropriate. After a while, it will approach the isothermal result as the system thermally equilibrates.

10. As P is constant and n is constant we have:

$$\begin{aligned} \frac{V}{T} &= \text{const} \\ \Rightarrow \frac{V}{(11 + 273)} &= \frac{2V}{T_1} \\ \Rightarrow T_1 &= 568 \text{ K} \end{aligned}$$

Then calculating the heat added:

$$\begin{aligned} Q &= c_P n \Delta T \\ &= \frac{7}{2} R \times 1.35 \times (568 - 11 - 273) \\ &= 11.2 \text{ kJ} \end{aligned}$$