

# Numerical solution of the advection diffusion equation

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## Introduction

The steady state advection diffusion equation is solved using the finite volume method. Central differencing is applied to the diffusion terms and the upwind differencing scheme is applied to the convection terms. The resulting linear system is solved using the Gauss-Seidel method.

## Model equations

From a component balance at an arbitrary location in the domain it follows that the advection diffusion equation is given by:

$$\frac{D_a}{U} \frac{d^2 C_a}{dz^2} - \frac{dC_a}{dz} + \frac{r_a}{U} = 0 \quad (1)$$

Where  $D_a$  is the diffusion coefficient,  $U$  is the fluid velocity,  $C_a$  the concentration of component  $a$ ,  $z$  the axial coordinate and  $r_a$  the reaction rate law of component  $a$ .

## Verification

When Danckwerts boundary conditions for a closed-closed system apply and the reaction rate law is first order an analytical solution to (1) can be obtained:

$$\frac{C_{al}}{C_{a0}} = \frac{4q \exp(Pe/2)}{(1+q)^2 \exp(Pe \cdot q/2) - (1-q)^2 \exp(-Pe \cdot q/2)} \quad (2)$$

Where  $C_{al}$  is the concentration of component  $a$  at the reactor outlet,  $C_{a0}$  is the concentration of component  $a$  at the reactor inlet,  $Pe$  is the Peclet number  $Pe = UL/D_a$  with  $L$  the length of the reactor and  $q$  is a quantity that depends on the Peclet and Damkohler numbers:

$$q = \sqrt{1 + 4Da/Pe} \quad (3)$$

Where  $Da$  is the Damkohler number  $Da = kL/U$  with  $k$  the reaction rate constant.

Numerical solutions to equation (1) are compared with (2). Results are given in table 1. Results show that analytical and numerical solutions agree well and that discrepancies are within 1 %.

Table 1: Exit concentration vs Peclet number		
$Pe$	Concentration analytical	Concentration numerical
0.1	0.909	0.907
0.2	0.832	0.832
0.4	0.709	0.709
0.8	0.534	0.534
1.6	0.319	0.320
3.2	0.118	0.120