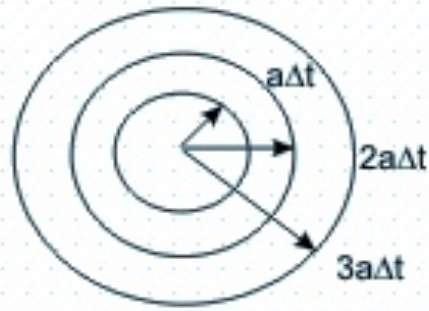
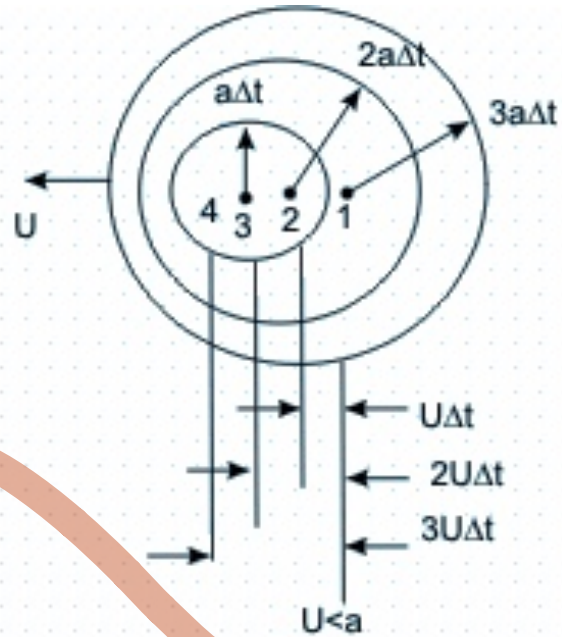


Mach angle. (μ)

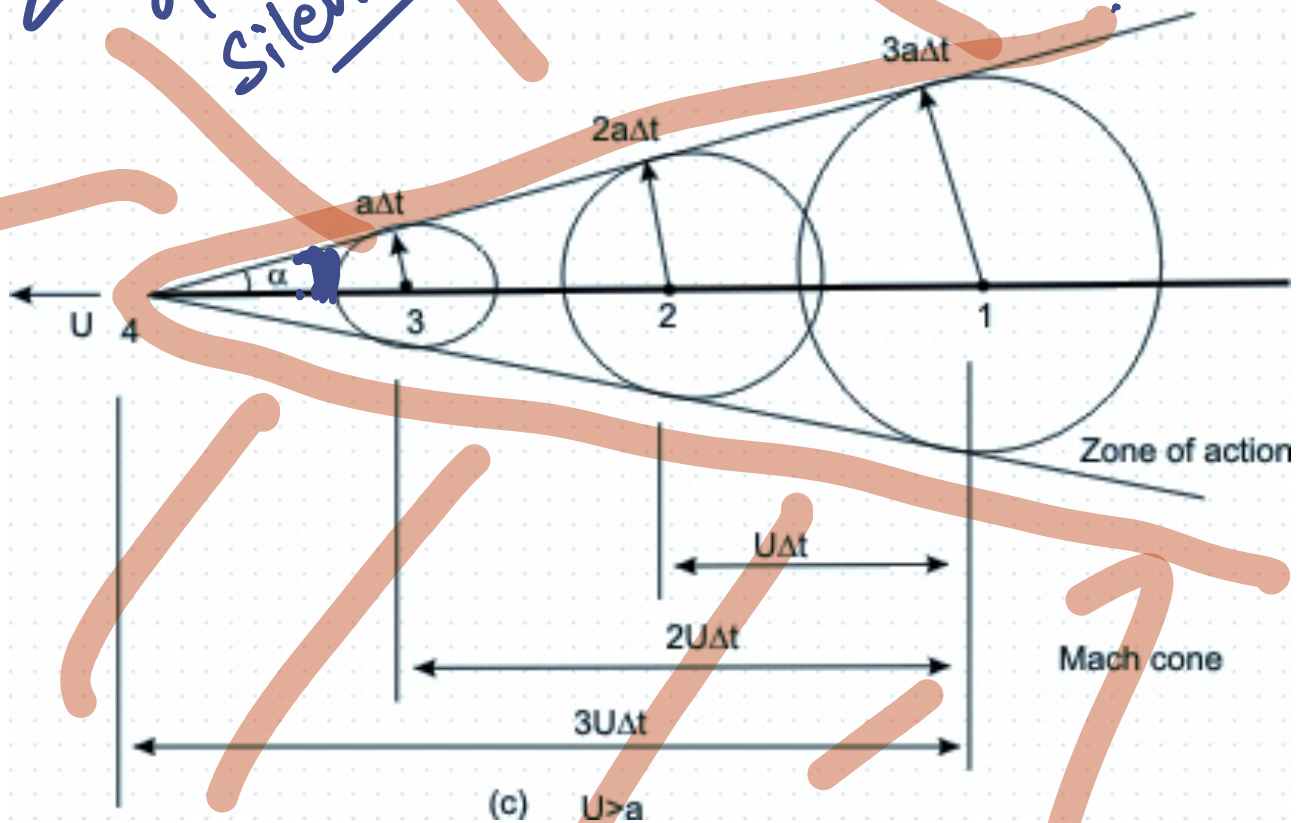


$U=0$
(a)



$U < a$

Zone of Silence

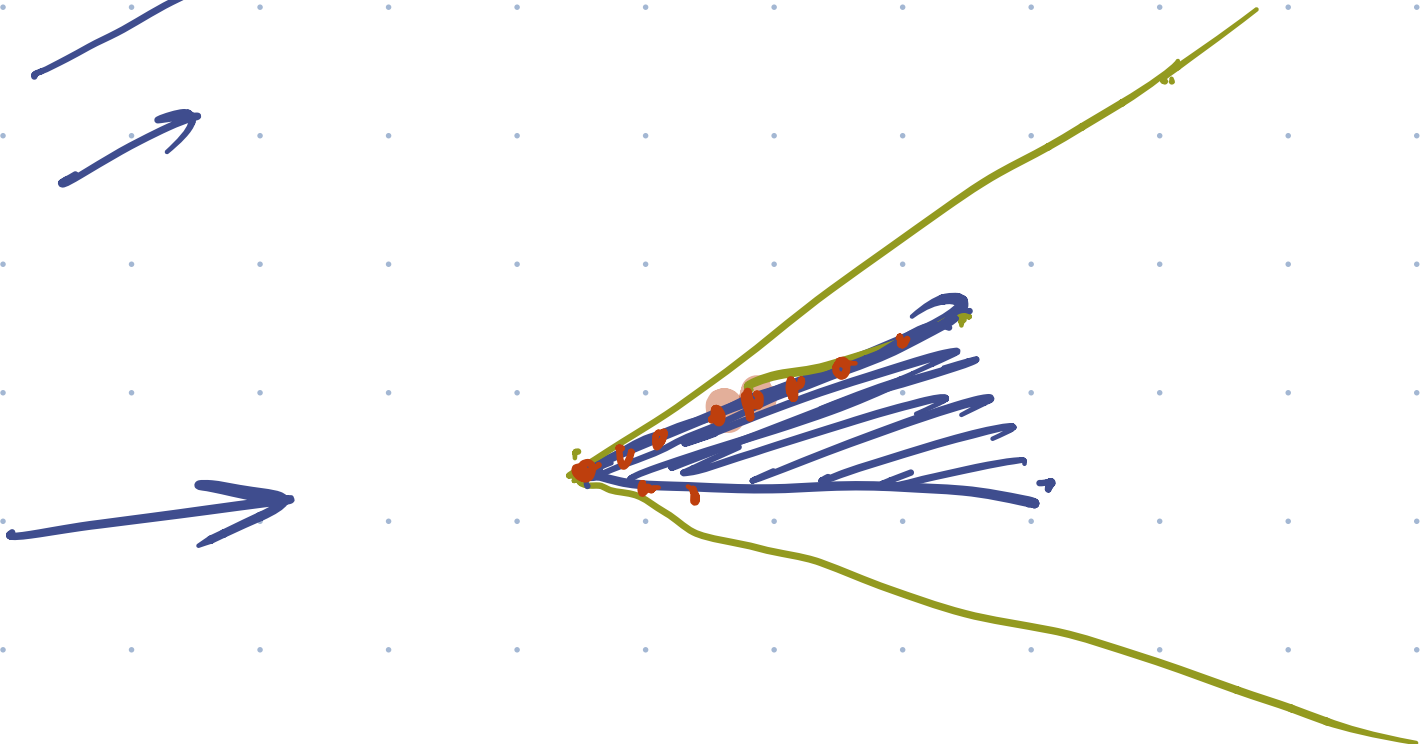
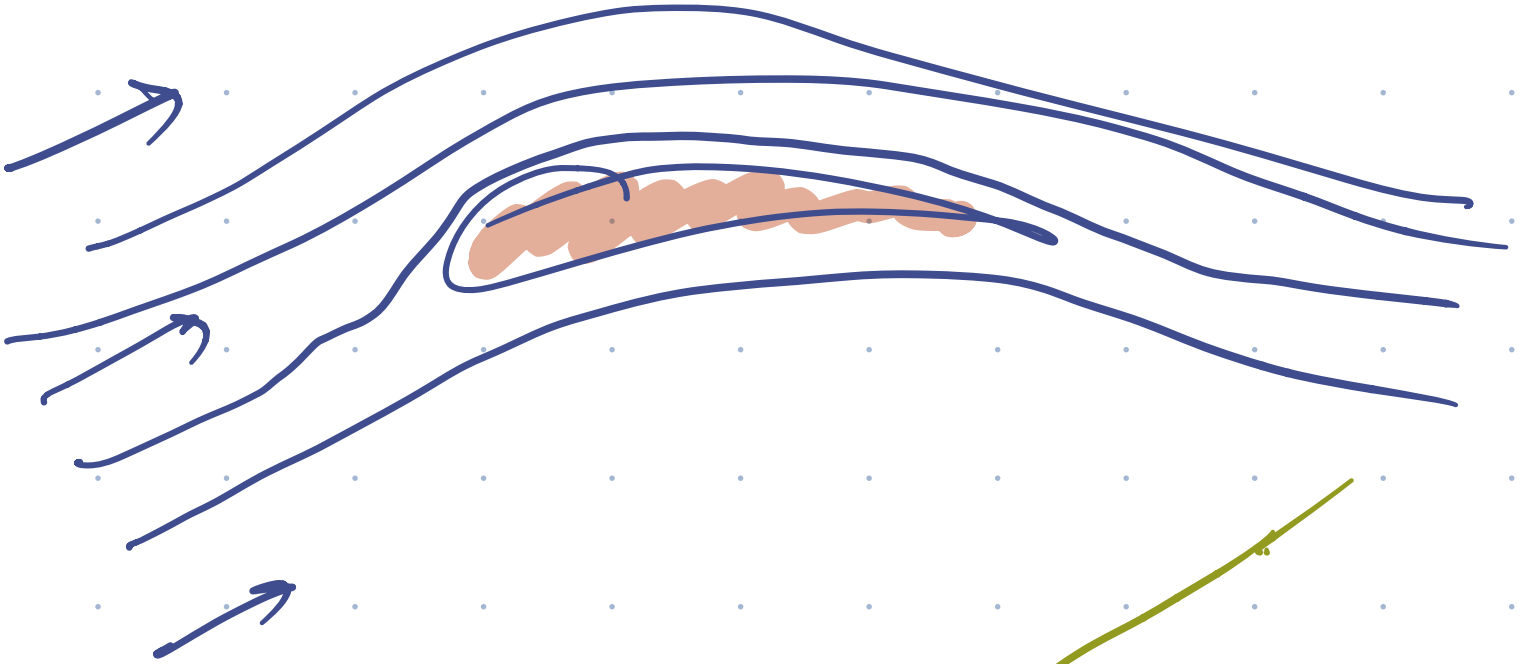
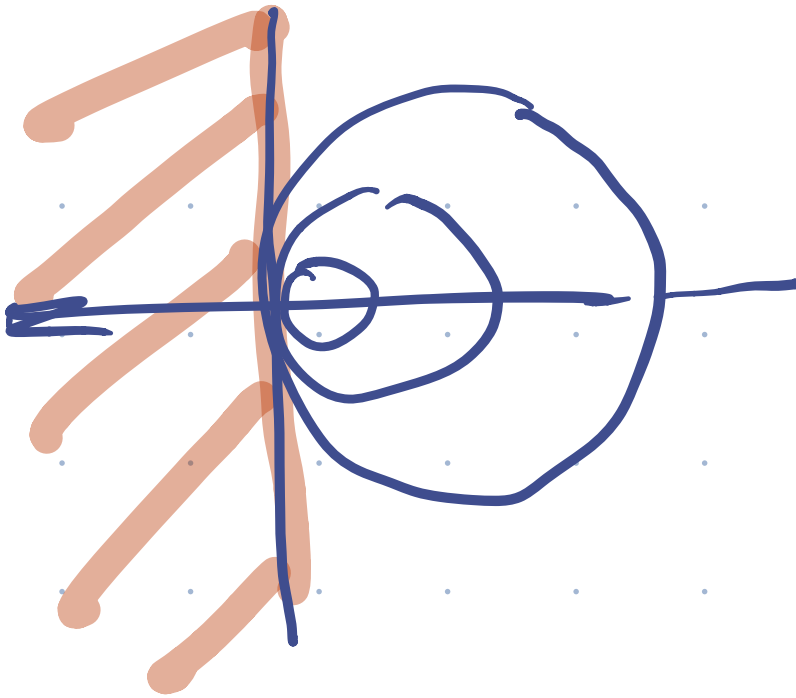


(c) $U > a$

Source: NPTEL

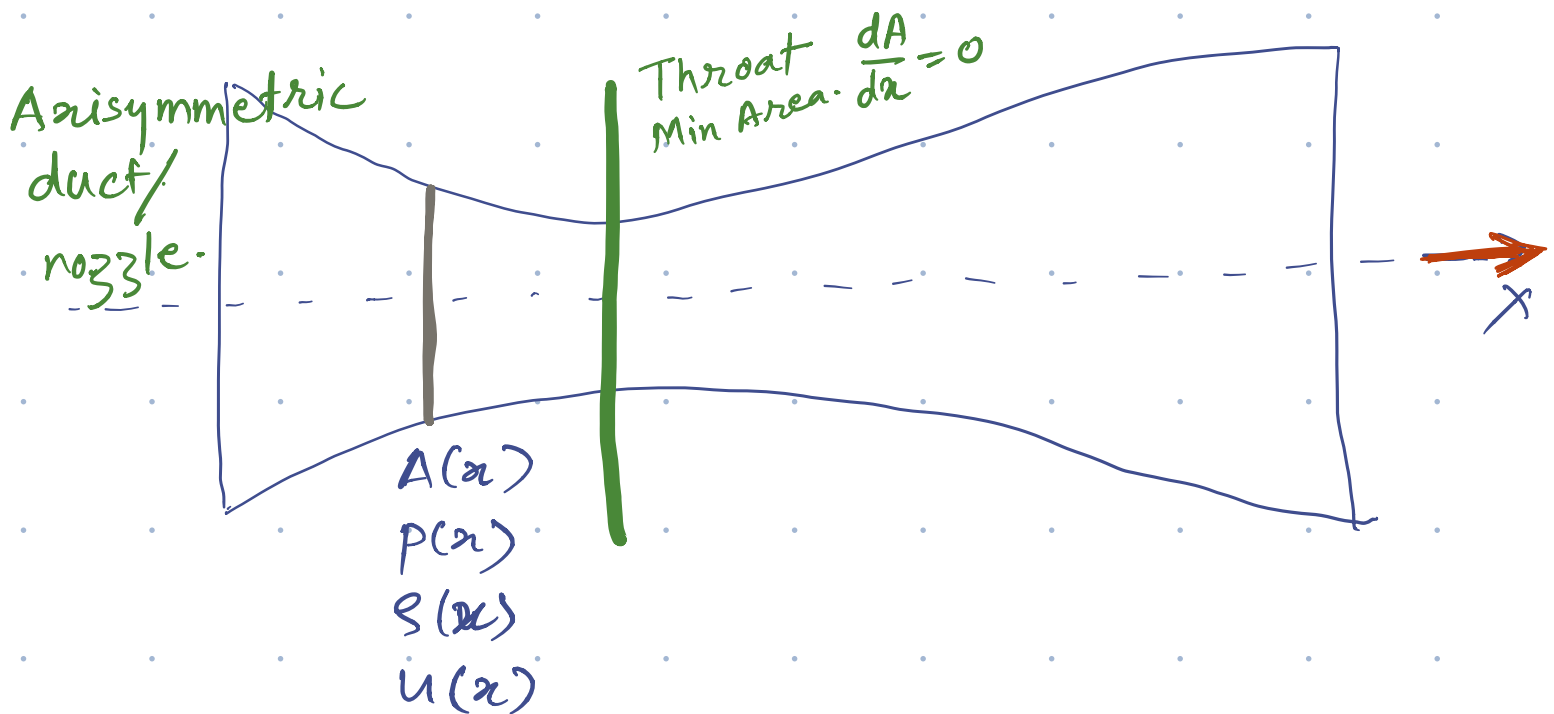
Mach Cone $\mu = \sin^{-1} \frac{1}{M}$

$M=1$



Isentropic Flow of a perfect gas

- Adiabatic $dq = 0$
 - Equilibrium flow
 - No entropy generation $ds = 0$
 - $p\bar{v} = RT$ (perfect gas)
 - Steady flow; hence $\left(\frac{\partial(\cdot)}{\partial t} = 0\right)$
- Hence
Isentropic



Conservation of mass

$$\rho A u = \dot{m} = \text{constant}$$

$$\therefore \frac{ds}{s} + \frac{dA}{A} + \frac{du}{u} = 0 \quad \text{--- (1)}$$

Momentum conservation

$$\cancel{\frac{\partial u}{\partial t}} + u \frac{\partial u}{\partial x} = -\frac{1}{\rho} \frac{\partial p}{\partial x}$$

$$\therefore \frac{dp}{dx} + \rho u \frac{du}{dx} = 0$$

— (2)

Note:- If $\rho = \text{const.}$; then this will lead to the Bernoulli's eqⁿ: $p + \rho \frac{u^2}{2} = \text{const.}$

Energy conservation

As we have seen already

$$h_0 = h'_0$$

As there is equilibrium throughout the duct;

$$dh_0 = 0 \Rightarrow dh + u du = 0$$

But we know, $dh = T ds + v dp$.

$$\therefore T ds + v dp + u du = 0$$

As $ds = 0$ (Isentropic process),

$$\frac{dp}{\rho} + u du = 0$$

$$\therefore \frac{dp}{dx} + \rho u \frac{du}{dx} = 0 \quad \text{--- (3)}$$

(3) is same as (2). Hence redundant.

So, combining (1) & (2)

$$dp + \rho u^2 \left(-\frac{ds}{s} - \frac{dA}{A} \right) = 0$$

Defining $\left. \frac{\partial p}{\partial s} \right|_s = a^2,$

We have,

$$dp + \rho u^2 \left(-\frac{dp}{\rho a^2} - \frac{dA}{A} \right) = 0$$

$$\therefore dp (1 - M^2) = \rho u^2 \frac{dA}{A}$$

where $M = u/a = \text{Mach number}$.

$$\therefore \frac{dp}{dA} = \left(\frac{\rho u^2}{1 - M^2} \right) \frac{1}{A}$$

Since, $a^2 = \gamma P / \rho$, we have

$$\frac{dp}{dA} = \left(\frac{\gamma M^2}{1 - M^2} \right) \frac{P}{A}$$

→ we note that the sign of RHS depends on $\left(\frac{1}{1 - M^2} \right)$.

→ RHS not defined for $M = 1$.

for $M < 1$,

$$\frac{dp}{dA} > 0$$

This means as $A \uparrow \Rightarrow P \uparrow \Rightarrow u \downarrow$

OR

$A \downarrow \Rightarrow P \downarrow \Rightarrow u \uparrow$

for $M > 1$,

$$\frac{dp}{dA} < 0$$

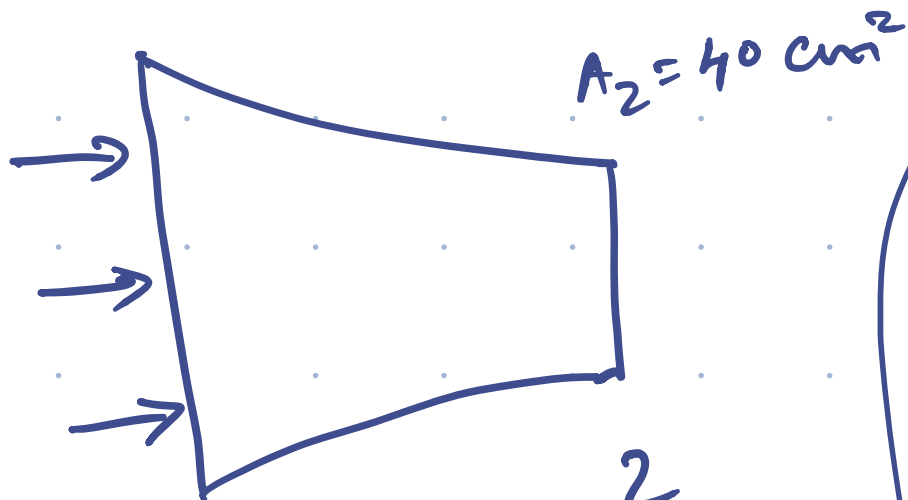
$\therefore A \uparrow \Rightarrow P \downarrow \Rightarrow u \uparrow$

OR

$A \downarrow \Rightarrow P \uparrow \Rightarrow u \downarrow$

Converging duct

$$A_1 = 50 \text{ cm}^2$$



$$T_1 = 300 \text{ K}$$

$$P_1 = 100 \text{ kPa}$$

$$V_1 = 100 \text{ m/s}$$

$$\rho = P_1 / R T_1$$

$$\rho_1 A_1 V_1 = \rho_2 A_2 V_2$$

$$M_2 = ?$$

$$P_2 = ?$$

$$T_2 = ?$$

$$T_{01} = T_{02}$$

$$P_{01} = P_{02}$$

$$\rho_{01} = \rho_{02}$$

$$\dot{m} = \rho A V$$

$$= \rho A \frac{V}{a} \cdot a$$

$$= \rho A M \cdot \sqrt{\gamma R T} \quad \text{--- (1)}$$

Also, $\frac{T_0}{T} = 1 + \frac{\gamma-1}{2} M^2 \quad \text{--- (2)}$

$$P_0/P = \left(1 + \frac{\gamma-1}{2} M^2\right)^{\gamma/\gamma-1} = \left(\frac{T_0}{T}\right)^{\gamma/\gamma-1}$$

$$\frac{\rho_0}{\rho} = \left(\frac{T_0}{T}\right)^{1/\gamma-1} = \left(1 + \frac{\gamma-1}{2} M^2\right)^{1/\gamma-1}$$

Using (1) & (2),

$$\dot{m} = \rho A M \sqrt{\gamma R} \cdot \left(\frac{\left(1 + \frac{\gamma-1}{2} M^2\right)^{1/2}}{\sqrt{T_0}} \right)^{\gamma-1}$$

$$\dot{m} = \frac{P_0}{\sqrt{RT_0}} A \sqrt{rM} \left(1 + \frac{r-1}{2} M^2\right)^{-\frac{(r+1)}{2(r-1)}}$$

$$= \frac{P_0}{\sqrt{RT_0}} A \cdot F(r, M)$$

$$\dot{m}_1 = \dot{m}_2$$

$$\frac{A_1}{A_2} = \frac{F(r, M_2)}{F(r, M_1)}$$

③

$$M_2 = \text{solving } \textcircled{3}$$

$$\rightarrow P_2 = T_0 / \left(1 + \frac{r-1}{2} M_2^2\right)$$

$f(P_0, M_2)$

$$p_2 = 1$$

$$s_2 = f(s_0, x_2)$$