Indian Institute of Technology, Guwahati.

ME 670 Advanced Computational Fluid Dynamies

Assignment - 1 (Dept. of Mechanical Engg.)

(Solve Lid-driven Cavity problem using

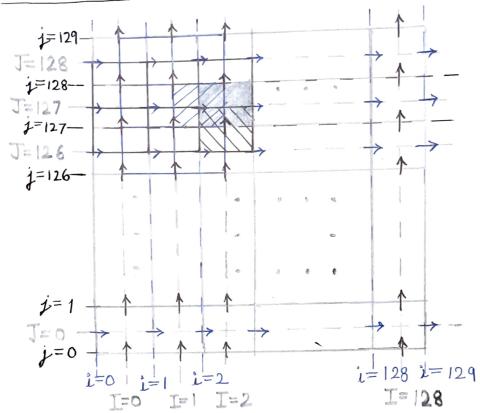
SIMPLE Algorithm)

Submitted ley:

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Gid Detail:



PI, J - denotes centre of p-control volume Pi, J - denotes centre of u-control volume PI, j - denotes centre of v-control volume

- for V- control volume

Discretized Equation detail.

The given problem requires us to solve two dimensional, incompressible, steady and isothermal flow inside a lid-driven; carrity.

We start by writing the non-dimensional steady Navier stakes equations:

$$\frac{\partial U^*}{\partial x^*} + \frac{\partial V^*}{\partial y^*} + \frac{\partial \omega^*}{\partial z^*} = 0 \quad (\text{continuity equation})$$

$$\Rightarrow \quad \underline{\nabla}^{*}, \quad \underline{U}^{*} = 0 \quad (compact form)$$

; where $\underline{\nabla}^* = \underline{L}\underline{\nabla}$ $\underline{u}^* = \underline{u}$ \underline{U}

$$(\underline{u} = \underline{u}\underline{b} + \underline{V}\underline{j} + \underline{\omega}\underline{k})$$

$$(\underline{u}^*, \underline{\nabla}^*)\underline{v}^* = -\underline{\nabla}^* \rho^* + \underline{1} \underline{\nabla}^* \underline{u}^*$$
 (Momentum equation)

can be rewritten as: The term on LHS

$$(\overrightarrow{n}_{\star}, \overrightarrow{\Delta}_{\downarrow} \overrightarrow{n}_{\star} = \overrightarrow{\Delta}_{\star}, (\overrightarrow{n}_{\star} \overrightarrow{n}_{\star})$$

 $\underline{\nabla}^{\star}.\left(\underline{\upsilon}^{\star}\underline{\upsilon}^{\star}\right) = -\underline{\nabla}^{\star}P^{\star} + \underline{1}_{Re}\nabla^{\star}.\left(\underline{\nabla}^{\star}\underline{\upsilon}^{\star}\right)$ Therefore, we can write:

In order to discretize this equation, we will use the finite volume method. The first step is to divide the flow domain into a finite no of control volumes.

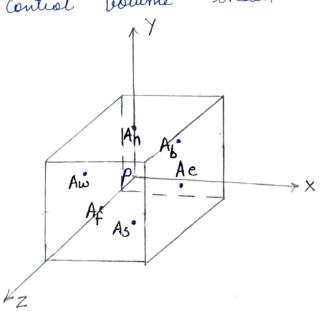
The Navier stokes equations are then integrated over the control volume as follows -

$$\int_{CV} \nabla^* \cdot (\underline{U}^* \underline{U}^*) dV = \int_{CV} \nabla^* \rho^* dV + \int_{Re} \underline{V}^* \cdot (\underline{V}^* \underline{U}^*) dV$$

Using the Gauss divergence theorem, $\int_{CV} \nabla \cdot F dV = \oint_{CS} F \cdot \hat{n} dS$ we can rewrite the 1st and 3rd term in the above equation as follows:

$$\oint_{CS} (U * U *) \cdot n \, ds = - \nabla * P * \Delta + \frac{1}{Re} \oint_{CS} (\nabla * U *) \cdot n \, ds$$

Now, in order to proceed, we must split the integral into the constituent control surfaces which enclose the control volume and integrate over each of these surfaces individually. Consider the control volume shows below -



The integral containing the connective turn on the LHS can be split as:

$$(\underline{u}^*\underline{u}^*) \cdot \underline{i} A_c + (\underline{u}^*\underline{u}^*) \cdot (\underline{-i}) A_w + (\underline{u}^*\underline{u}^*) \cdot \underline{i} A_n$$

+ $(\underline{v}^*\underline{u}^*) \cdot (\underline{-j}) A_s + (\underline{v}^*\underline{u}^*) \cdot \underline{k} A_F + (\underline{v}^*\underline{u}^*) \cdot (\underline{-k}) A_b$

Here, we introduce a variable + to represent the convective mass flux per unit area:

$$\neq$$
 Also, since we have a uniform grid,
 $Ae = Aw = An = As = Ap = Ab = A$

Now,
$$U^* = U^* L + V^* J + \omega^* K$$

$$F_0 = U^* \omega$$

$$F_0 = V^* \omega$$

$$F_0 = V^* \omega$$

$$F_1 = V^* \omega$$

$$F_2 = V^* \omega$$

$$F_3 = V^* \omega$$

$$F_4 = \omega^* \omega$$

$$F_6 = \omega^* \omega$$

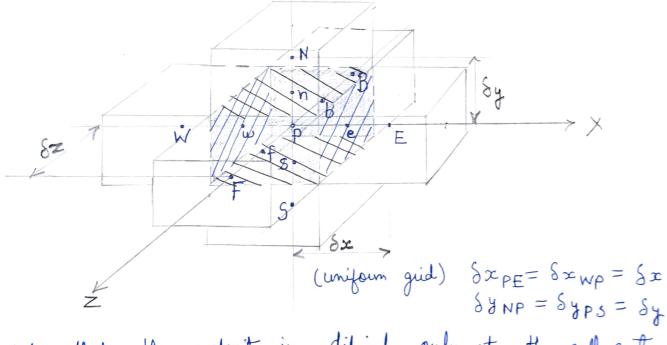
substitutions, un get Applying these

The integral containing the diffusion lum on the right hand side of the egin can be split as !

$$\frac{1}{Re} \left(\frac{\partial u^{*}}{\partial x} \Big|_{e} A_{e} - \frac{\partial u^{*}}{\partial x} \Big|_{w} A_{w} + \frac{\partial u^{*}}{\partial y} \Big|_{n} A_{n} - \frac{\partial u^{*}}{\partial y} \Big|_{s} A_{s} \right)$$

$$+ \frac{\partial u^{*}}{\partial z} \Big|_{f} A_{t} - \frac{\partial u^{*}}{\partial z} \Big|_{b} A_{b}$$

Here, we assume that U* varies linearly over the Control volume



Note that the velocity is difined only at the cell centers P, E, N, S, etc. but not at the face centres e, w, n

Assuming linear interpolation, we can now unite - $\frac{\partial v^*}{\partial x}|_e = \frac{v^*_E - v^*_P}{8x}$, $\frac{\partial v^*}{\partial x}|_w = \frac{v^*_F - v^*_W}{8x}$

$$\frac{\partial u^*}{\partial y}\Big|_{n} = \frac{u^* N - u^* p}{\delta y}, \quad \frac{\partial u^*}{\partial y}\Big|_{s} = \frac{u^* p - u^* s}{\delta y}$$

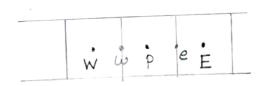
This is a vector equation in V^* and P^* . We can split this equation into its component form as follows— X- momentum equation: $(U^* = u^*) = P^* - P^*$ $(Fu^*) = -(Fu^*) + (Fu^*) - (Fu^*) = ($

 $\begin{aligned} |Fu^*\rangle_{e} - (Fu^*)_{w} + (Fu^*)_{n} - (Fu^*)_{5} + (Fu^*)_{f} - (Fu^*)_{b} = \\ (u_{E}^* - u_{P}^*)_{De} + (u_{P}^* - u_{W}^*)_{Dw} + (u_{N}^* - u_{P}^*)_{Dn} - (u_{P}^* - u_{S}^*)_{Ds} \\ + (u_{F}^* - u_{P}^*)_{Df} - (u_{P}^* - u_{B}^*)_{Db} - (P_{P}^* - P_{W}^*) \end{aligned}$

Now, u* is defined only at cell centres. So, we need to write U*e, U*w, etc. in terms of velocities at cell centres. For this we employ the Hybrid differencing Scheme.

Consider the east face of the control volume, we first evaluate the Peclet no. $Pe = \frac{Fe}{De}$

Fe u*e = Fe u*E + 0 · u*p ; $P_e \ge 2$ Fe u*e = Fe u*P + 0 · u*E ; $P_e \le -2$ Fe u*e = $\left(\frac{Fe}{2} + De\right) \cup p^* + \left(\frac{Fe}{2} - De\right) \cup E^*$; $-2 < P_e < 2$



The above relations can be written in a compact form as:

$$Fe \stackrel{*}{ve} = - \max \left[-Fe, 0, \left(-\frac{Fe}{2} + De \right) \right] \stackrel{*}{UE} + \max \left[Fe, 0, \left(Det \underline{Fe} \right) \stackrel{*}{Up} \right]$$

$$= - \alpha_{E} \stackrel{*}{UE} + \left(\max \left[0, -Fe, \left(De - \frac{Fe}{2} \right) \right] + Fe \right) \stackrel{*}{Up}$$

Similarly,
$$(F \cup^*)_W = \max \left[0, F_W, \left(\frac{F_W}{2} + D_W \right) \right] \bigcup_{W}^* + \max \left[0, F_W, \left(\frac{F_W}{2} + D_W \right) \right] \bigcup_{V_P}^* + \max \left[0, F_W, \left(\frac{F_W}{2} + D_W \right) \right] \bigcup_{V_P}^* + \max \left[0, F_W, \left(\frac{F_W}{2} + D_W \right) \right] \bigcup_{V_P}^* + \max \left[0, F_W, \left(\frac{F_W}{2} + D_W \right) \right] \bigcup_{V_P}^* + \max \left[0, F_W, \left(\frac{F_W}{2} + D_W \right) \right] \bigcup_{V_P}^* + \sum_{W_P}^* + \sum_{W_P}$$

Y-momentum equation: (U* = V* & <u>AP</u>* = Pp*-Ps*) (Fr*)e-(Fr*)w+(Fr*)n-(Fr*)s+(Fr*)f-(Fr*)b= (VE-Up) Det (Vp-Ux) Dw+ (VN-Up) Dn- (Vp-Ux) Ds $+ (v_F^* - v_P^*)D_f - (v_P^* - v_B^*)D_b - (P_P^* - P_S^*)$ Again to compute v'e, v'w, v'n, etc. we use the hybrid differencing scheme, just like the case for x-momentum equation. equation. Substituting the hybrid differencing convecture terms in the equation and rearranging to get v'p on LHS (setting diffusion terms equal to zero): Vp aE+awtan+as+aF+aB + Fe-Fw+ Fn-Fs +Ff-Fb] = all tetaw vw + an vn + as vs + af vf + abvb + ps * - Pp* The discretized y-nomentum equation is: ap $V_p^{\star} = \sum_{a_{nb}} V_{nb}^{\star} + P_s^{\star} - P_p^{\star}$; $a_p = \sum_{a_{nb}} F_e - F_w + F_n - F_s + F_f - F_b$ Z- momentum equation: (U* = w* & <u>AP</u>* = PBP - PB*) $(F\omega^*)e - (F\omega^*)\omega + (F\omega^*)_n - (F\omega^*)_s + (F\omega^*)_f - (F\omega^*)_b =$ (ω=*- ωp*) De+ (ωp*- ω*) Dω+ (ω*, - ω*) Dn- (ω*, - ω*) Ds + (w=-w=)D+- (wp-w=B)Db - (Pp*-PB*)

Similar to the previous cases we approximate the velocities at face centres using the hybrid differencing scheme.

Substituting the hybrid difference convective terms in the

Substituting the hybrid difference convective terms in the Equation and rearranging to get wp on LHS (setting diffusion terms equal to zero) we get,

Wp [a Etaw+ an+ast af+ aB + Fe-Fw+Fn-Fs+Ff-Fb]

= a E WE + a WWW + a N WI + a S WS + A F WF + a B WB + PB* - PP

The discretized z-momentum equation is:

apwp* = Eanbwh + PB*-Pp*; ap = Eanbt Fe-Fw+ Fn-Fstff-Fb

Next, we need to find the discretized continuity eq. The this, we again use the finite volume method and integrate the continuity equation over the control volume as follows-

 $\int_{CV} \underline{\nabla}^* \cdot \underline{\upsilon}^* = 0 = \oint_{CS} \underline{\upsilon}^* \cdot \underline{n} \, ds$

[Using Gauss dureyence theorem]

To proceed, we split the integral into the constituent control surfaces which enclose the control volume just like done before and integrate over each of these surfaces individually

<u>u</u>*: i Ae + <u>u</u>*. (-i) Aw + <u>u</u>*. j An + <u>u</u>*. (-j) As

 $+ v^{*} \times A_{f} + v^{*} \cdot (-k) A_{b} = 0$

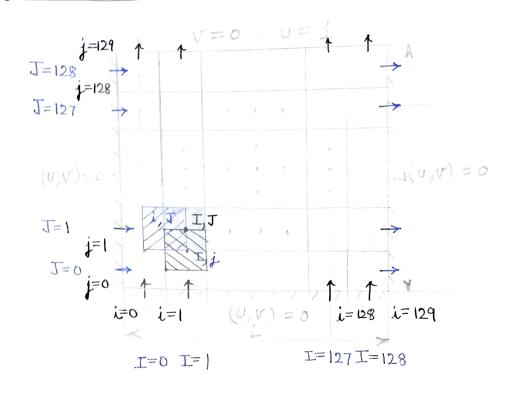
$$U^*(Ae - Aw) + V^*(An - As) + w^*(Af - Ab) = 0$$
Assuming $Fe = U^*e$, $Fw = U^*w$, $Fn = V^*n$

$$Fs = V^*s, Ff = w^*f, Fb = w^*b$$
Also, $Ae = Aw = An = As = Af = Ab = A$ (for uniform grid)

$$\Rightarrow (F_e - F_w + F_n - F_s + F_f - F_b) A = 0$$

$$F_e - F_w + F_n - F_s + F_f - F_b = 0$$

Boundary Condition Implementation Detail



For the given problem, we have discretized the control volume into a grid size of 129 x 129 such that the edges of the pressure control volume coincide with the walls of the given problem.

The boundary conditions at the four walls are:

Left wall: Given u = 0, v = 0since U is defined explicitly at the bottom wall, we can write

 $n^{0^{1}} = 0$

Now, I is not defined explicitly at left wall, V-control volume has its edge coinciding with the wall, it experiences a Shear force from the wall which can be modelled as:

$$F_{L} = -T_{L} A$$

$$= -\frac{1}{Re} \frac{(V_{0}, j-0)}{\frac{5}{x}} A = -\frac{2}{Re} \frac{V_{0}, j}{Re} A$$

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$$\therefore S_{p} = -\frac{2}{Re} \sum_{Re} \frac{S_{in}C_{e}}{Res_{in}C_{e}} \text{ we divided discretized } V_{p} - \frac{1}{Re} \frac{V_{p}}{Re} A$$

$$= -\frac{1}{Re} \frac{V_{0}, j-0}{\frac{5}{x}} A = -\frac{2}{Re} \frac{V_{0}, j}{Re} A$$

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$$= -\frac{2}{Re} \frac{V_{0}, j-0}{\frac{5}{x}} A = -\frac{2}{Re} \frac{V_{0}, j-0}$$

Also,
$$aW=0$$
; [since V at $I=-1$ is not defined]

Right Wall: guien u=0, v=0

Since U is defined explicitly at the right wall, we can write

U 129, J = 0

Now, v is not defined explicitly at right wall best, the v-control volume has its right edge coinciding with the wall and experiences a shear force which can be modelled as:

$$F_{R} = -T_{R}A$$

$$= -\frac{1}{Re} \left(\frac{V_{128,j} - 0}{\frac{5x}{2}} \right) A = -\frac{2}{Re} S_{x} V_{128,j} A$$
[Here $V_{p} = V_{128,j}$

$$S_p = \frac{2}{Re \delta x} \left[Since, we divided discretized egh throughout $yA \right]$$$

Also, $\alpha E = 0$ [Since V at I = 129 is not defined defined for $[0, 128] \rightarrow total$ 129 points]

i. aP = aW+ aN+aS+ Fe+Fn - Fw -Fs - Sp

Bottom Wall: given u=0, v=0

since, v is defined explicitly at the bottom wall we can write,

Now, u is not defined explicitly at the bottom wall, the v-control volume has its bottom edge coincident with the wall, it experiences a shear force which can be modelled as -

$$F_B = - T_B A$$

$$= -\frac{1}{Re} \left(\frac{u_{i,0}-0}{5y} \right) A = -\frac{2}{Re} \underbrace{u_{i,0}A}_{Re}$$
[Here $u_{i,0} = v_p$]

is
$$Sp = -\frac{2}{ReSy}$$
 [Since we divided the discretized V-momentum

Also, aS=0; [since u at J=-1 is not defined]

iap = aW+ aE+ aN + Fe+ Fm - Fw - Fs - Sp

Top Wall: Given u = 1, v = 0

since v is defined explicitly at the top wall, we can write $V_{\rm I}, 129 = 0$

Now, u is not defined explicitly at the top wall, the U-control volume has its top-edge
coinciding with the wall and experiences a show force
which can be modelled as:

$$F_{T} = -T_{T}A$$

$$= -\frac{1}{Re} \left(u_{i,128} - 1 \right) A$$

$$\frac{\delta y}{2}$$

$$= \left(-\frac{2}{Re} \frac{U\rho}{8\gamma} + \frac{2}{Re} \frac{2}{8\gamma}\right) A$$
[Here $\psi_p = V_{1,128}$]

$$5p = -\frac{2}{\text{Re Sy}}$$
 8 Su = $\frac{2}{\text{Re Sy}}$

[Since, we divided the discretized U-momentum equation throughout by A]

Also, aN=0 [Since u at J=129 is not defined u defined for [0,128] -> total 129 points]

8 Finally,
$$U_p^* = (aW U_W^* + a_E U_E^* + a_S U_S^* + P_E^* W - P_P^* + S_U)$$