

(Q1) Roll. no.  $\rightarrow 180103097$  H  $\rightarrow 9$  I  $\rightarrow 7$

$L = 1\text{m}$   $T_L = 0^\circ\text{C}$   $T_\infty = 197^\circ\text{C}$   $h = 19.7$

general Sol.  $\rightarrow \frac{d^2 T}{dx^2} = -\frac{A}{k} (T - T_\infty)$

$$T - T_m = C_1 \cosh \sqrt{\frac{A}{k}} x + C_2 \sinh \sqrt{\frac{A}{k}} x$$

B.C.  $\rightarrow$  LHS  $\Rightarrow -T_\infty = C_1$

RHS  $\rightarrow -k \left. \frac{\partial T}{\partial x} \right|_L = \bar{h}_{RHS} (T_L - T_\infty)$

$$T_\infty \sinh \sqrt{\frac{A}{k}} L - C_2 \cosh \sqrt{\frac{A}{k}} L = \underbrace{\bar{h}_{RHS} \sqrt{\frac{k}{A}}}_{Bie} (T_\infty \cosh \sqrt{\frac{A}{k}} L + C_2 \sinh \sqrt{\frac{A}{k}} L)$$

$$\Rightarrow C_2 (Bie \sinh \sqrt{\frac{A}{k}} L + \cosh \sqrt{\frac{A}{k}} L) = Bie T_\infty \cosh \sqrt{\frac{A}{k}} L - T_\infty \sinh \sqrt{\frac{A}{k}} L$$

$$C_2 = T_\infty \left[ \frac{Bie \cosh \sqrt{\frac{A}{k}} L - \sinh \sqrt{\frac{A}{k}} L}{Bie \sinh \sqrt{\frac{A}{k}} L + \cosh \sqrt{\frac{A}{k}} L} \right]$$

$$\therefore \frac{T_\infty - T}{T_\infty} = \frac{\cosh \sqrt{\frac{A}{k}} x - Bie \cosh \sqrt{\frac{A}{k}} L - \sinh \sqrt{\frac{A}{k}} L}{Bie \sinh \sqrt{\frac{A}{k}} L + \cosh \sqrt{\frac{A}{k}} L} \sinh \sqrt{\frac{A}{k}} x$$

$h = 19.7$   $T_\infty = 197^\circ\text{C}$   $L = 1\text{m}$   $A = 10$

$$Bie = \frac{\bar{h}_{RHS}}{\sqrt{kA}} = \frac{19.7}{\sqrt{10}} = 6.2297$$

Assuming  $k = 1$

$$1 - \frac{T}{T_\infty} = \frac{\cosh(\sqrt{10}x) - 6.2297 \cosh \sqrt{10} - \sinh \sqrt{10}}{6.2297 \sinh \sqrt{10} + \cosh \sqrt{10}} \sinh(\sqrt{10}x)$$

$$\frac{T}{197} = 1 - \cosh(\sqrt{10}x) + \frac{5.5}{4.59} \sinh \sqrt{10}x$$

At  $x = 0.5 \text{ m}$ .

$$\frac{T}{197} = \frac{\cancel{25.025^\circ\text{C}}}{\cancel{n=4/5}} \quad \underline{\underline{1282.0479^\circ\text{C}}} \quad |_{n=1/2}$$

At  $x = 1 \text{ m}$   $\Rightarrow$   $\cancel{T = 50.181^\circ\text{C}} \mid_{\cancel{n=1}} \quad \underline{\underline{T = 371.547^\circ\text{C}}} \mid_{n=1}$

(Q2) Roll no.  $\rightarrow$  180103097

Assuming fin to be cylindrical,  $\frac{x}{L} = \xi$

General soln for this problem is  $\rightarrow$

$$T - T_{\infty} = C_1 e^{m\xi} + C_2 e^{-m\xi}$$
$$= C_1 e^{ML\xi} + C_2 e^{-ML\xi}$$

BC  $\rightarrow$   $q_1 = -\frac{k}{L} \frac{d(T - T_{\infty})}{d\xi} \Big|_{\xi=0} = 0$

$$q_2 = \frac{k}{L} \frac{d(T - T_{\infty})}{d\xi} \Big|_{\xi=1}$$

$$\frac{q_1}{kM} = -C_1 + C_2 \quad \xi \quad \frac{q_2}{kM} = C_1 e^{ML} - C_2 e^{-ML}$$

So,  $C_2 = \frac{q_1}{kM} + C_1 \quad \xi \quad \frac{q_2}{kM} = -\frac{q_1}{kM} e^{-ML} + C_1 2 \sinh ML$

$\therefore C_1 = \frac{q_1}{kM} \left( \frac{e^{-ML} + \frac{q_2}{q_1}}{2 \sinh ML} \right)$

$$\frac{T - T_{\infty}}{q_1/kM} = \frac{\left( e^{-ML} + \frac{q_2}{q_1} \right) e^{ML\xi} + 2 \sinh ML e^{-ML\xi} + \left( e^{-ML} + \frac{q_2}{q_1} \right) e^{-ML\xi}}{2 \sinh ML}$$
$$= \frac{\left( \frac{q_2}{q_1} \right) 2 \cosh ML \xi + e^{-ML(1-\xi)} + e^{ML(1-\xi)} - e^{-ML(1+\xi)} - e^{ML(1+\xi)}}{2 \sinh ML}$$

$\therefore \frac{T - T_{\infty}}{q_1/kM} = \frac{q_2}{q_1} \frac{\cosh ML \xi}{\sinh ML} + \frac{\cosh ML(1-\xi)}{\sinh ML}$

for  $q_2 = 0 \Rightarrow \frac{T_1 - T_{\infty}}{q_1/kM} = \frac{\cosh ML(1-\xi)}{\sinh ML} \Rightarrow$

$$\Rightarrow \frac{T - T_{\infty}}{q_1/kM} = e^{-ML\xi}$$



Roll no  $\rightarrow$  180103097  $H=9$   $J=7$   
 (Q3)  $k_s = 19.7 \text{ W/mK}$   $d_i = 3 \text{ cm}$   $t = 2 \text{ mm}$   $t_i = 6 \text{ mm}$   $k_i = 0.797 \text{ W/mK}$

$h_1 = 1597 \text{ W/m}^2\text{K}$   $h_2 = 297 \text{ W/m}^2\text{K}$

$T_i = 597 \text{ K}$   $T_o = 379 \text{ K}$

Heat transfer  $= q \Rightarrow q = 2\pi L \left( \frac{0.03}{2} \right) (1597) (597 - 379)$

$q = 2\pi L (1.5 + 2 + 0.6) \times 10^{-2} (297) (T_{a1} - 379)$

$q = -2\pi L (1.5 + x) \times 10^{-2} k \frac{dT}{dx}$

Let  $\frac{q}{2\pi L \times 10^{-2}} = Y$

$\frac{Y}{k (1.5 + x)} = -dT$

For steel,  $\frac{Y}{19.7} \ln\left(\frac{1.7}{1.5}\right) = T_{s1} - T_{s2}$  [for steel] (1)

$\frac{Y}{0.797} \ln\left(\frac{2.3}{1.7}\right) = T_{a1} - T_{a2}$  [for asbestos] (2)

Also,  $\frac{Y}{1.5 \times 1597} = 597 - T_{s1}$  (3)

$\frac{Y}{2.3 \times 297} = T_{a2} - 379$  (4)

Also  $T_{a1} = T_{s2}$  [same surface]

Adding (1), (2), (3) & (4)

$Y \left[ \frac{\ln(1.7)}{19.7(1.5)} + \frac{\ln(2.3)}{0.797(1.7)} + \frac{1}{1.5 \times 1597} + \frac{1}{2.3 \times 297} \right] = \cancel{T_{s1} - T_{s2}} + \cancel{T_{a1} - T_{a2}} + 597 - \cancel{T_{a1}} + \cancel{T_{a2}} - 379$

$Y [0.0635 + 1.7108 + 0.0004 + 0.0015] = 200$

$Y = \underline{112.5999}$

Substituting in eq (3)  $\rightarrow$

$$\frac{112.5999}{19.7} \ln\left(\frac{1.7}{1.5}\right) = \frac{112.5999}{1.5 \times 1597} = 579 - T_{s1}$$

$$T_{s1} = \underline{578.97 \text{ K}}$$

Sub. in eq (4)  $\Rightarrow$

$$\frac{112.5999}{2.3 \times 297} = T_{a2} - 379$$

$$T_{a2} = \underline{379.165 \text{ K}}$$

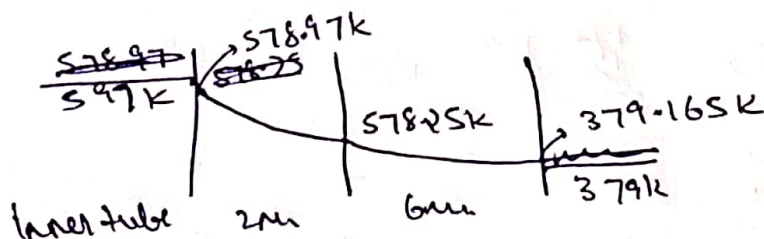
Sub. in eq (1)  $\rightarrow$

$$\frac{112.5999}{19.7} \ln\left(\frac{1.7}{1.5}\right) = 578.97 - T_{s2}$$

$$T_{s2} = T_{a1} = \underline{578.2546 \text{ K}}$$

$$\frac{q}{2\pi l \times 10^{-2}} = P$$

$$\left(\frac{q}{l}\right) = P \times 2\pi \times 10^{-2} = \underline{\underline{7.007 \text{ W/m}}}$$



(Q4)

$$H = 9 \quad I = 7$$

$$L = 0.1 \text{ m}$$

$$k = 45 \text{ W/m}^2\text{K}$$

$$\rho = 800 \text{ kg/m}^3 \quad c_p = 500 \text{ J/kgK}$$

$$T_i = 397^\circ\text{C}$$

$$T_\infty = 779^\circ\text{C}$$

$$h = 597 \text{ W/m}^2\text{K}$$

Temp. min.:- Centerline temp.  $T_0 = 559^\circ\text{C}$

$$\alpha = \frac{k}{\rho c_p} = \frac{45}{800 \times 500} = 1.125 \times 10^{-4}$$

$$Bi = \frac{hL}{k} = \frac{597 \times 0.05}{45} = 0.663$$

From Table, using linear interpolation

$$\frac{0.663 - 0.6}{0.7 - 0.6} = \frac{Z_1 - 0.7051}{0.7506 - 0.7051} \quad \Rightarrow \quad Z_1 = 1.13$$

$$\frac{0.663 - 0.6}{0.7 - 0.6} = \frac{C_1 - 1.0814}{1.0919 - 1.0814}$$

$$C_1 = 1.088$$

$$Fo = \frac{\alpha t}{L^2}$$

$$\frac{T_0 - T_\infty}{T_i - T_\infty} = C_1 e^{-Z_1^2 Fo}$$

$$\frac{559 - 779}{397 - 779} = 1.088 e^{-1.13^2 Fo}$$

$$Fo = 0.498 > 0.2 \quad (\text{OK for app. solution})$$

$$t = \frac{Fo L^2}{\alpha} = \frac{0.498 \times 0.05^2 \times 0.5}{1.125 \times 10^{-4}} = 11.066 \text{ s}$$



[Q5] Roll no.  $\rightarrow$  180103097 H=9 I=7

$$T_i = 4149.7 \text{ K} \rightarrow T_f = 0 \text{ K} \quad \kappa_{\text{SiO}_2} = 1.197 \times 10^{-6}$$

$$\frac{\partial T}{\partial x} = 27^\circ \text{C/m}$$

$$q = k \left. \frac{\partial T}{\partial x} \right|_{x=0} = k (T_i - T_\infty) \exp(-n x) \quad -1/2$$

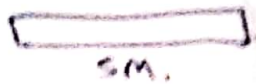
$$t = \frac{(T_i - T_\infty)^2}{(\frac{\partial T}{\partial x})^2} \cdot \frac{1}{\pi \times 1.197 \times 10^{-6}} = \frac{4.58152 \times 10^{12}}{800} \text{ sec}$$
$$= 6284.66 \times 10^6 \text{ sec}$$
$$= \underline{199 \text{ years}}$$

His estimates were wrong because  $\frac{\partial T}{\partial x} = 27^\circ \text{C/m}$  which is very very greater a huge number.

He also didn't consider internal heat generation due to radiation of <sup>radioactive</sup> material on surface.

(Q6) RAD no  $\rightarrow$  180103097  $n=9$

$$T_m = 0 = 190^\circ\text{C} \quad T|_{x=5} = 0$$



Steady state  $q_m = q_n = q_{\text{rod}}$

$$\frac{d}{dx}(q) dx = 0$$

$$\Rightarrow \frac{d}{dx} \left( -k A \frac{dT}{dx} \right) = 0$$

$$\Rightarrow \frac{dT}{dx^2} = 0$$

$$T = C_1 x + C_2$$

$$x=0 \Rightarrow T=() \rightarrow 190^\circ\text{C} = \underline{463.15}$$

$$x=L \Rightarrow T = C_1 L + C_2 = 0 \Rightarrow C_1 = \frac{-190}{L} = \frac{-463.15}{5} 190$$

$$= -92.6338$$

$$T = -92.6338 x + 463.15 \quad \text{--- (1)}$$

$$\frac{\partial T}{\partial x} = \alpha \frac{\partial^2 T}{\partial x^2}$$

Given  $\Delta x = 1\text{m}$   $\alpha = .25$   
 $\Delta t = 18.$

$$\frac{\partial T}{\partial x} \frac{T_{i+1}^n - T_i^n}{\Delta t} = \alpha \left( \frac{T_{i+1}^n - 2T_i^n + T_{i-1}^n}{\Delta x^2} \right)$$

$$\Rightarrow T_{i+1}^n - T_i^n = \alpha \left( T_{i+1}^n - 2T_i^n + T_{i-1}^n \right)$$



$$T_1^0 \quad T_2^0 \quad T_3^0 \quad T_4^0 \quad T_5^0 \quad T_6^0 \quad t=0s \quad (113) \quad (1/1)$$

$$T_1^1 \quad T_2^1 \quad T_3^1 \quad T_4^1 \quad T_5^1 \quad T_6^1 \quad t=1s$$

$$T_1^2 \quad T_2^2 \quad T_3^2 \quad T_4^2 \quad T_5^2 \quad T_6^2 \quad t=2s$$

$$T_1^3 \quad T_2^3 \quad T_3^3 \quad T_4^3 \quad T_5^3 \quad T_6^3 \quad t=3s$$

$$\text{Now, } T_1^n = 0^\circ\text{C} = \cancel{273.15\text{K}} \quad (Bl \text{ } n=0)$$

$$T_6^n = 190^\circ\text{C} = \cancel{463.15\text{K}} \quad (Bl \text{ } n=L)$$

$$T = 463.15 - 92.63m \quad T_2^0 = \cancel{372.52\text{K}} = 152^\circ\text{C}$$

$$T_3^0 = \cancel{279.89\text{K}} = 114^\circ\text{C} \quad T_4^0 = \cancel{167.76\text{K}} = 76^\circ\text{C} \quad T_5^0 = \cancel{246.3\text{K}} = 38^\circ\text{C}$$

$$\text{Now, } T_i^{nH} = \frac{T_{iH}^n + 2T_i^n + T_{i-1}^n}{4}$$

$$\cancel{T_2^1 = \frac{279.89 + 2 \times 372.52 + 273.15}{4}}$$

i =	1	2	3	4	5	6
t = 0	0	152	114	76	38	190
1	0	104.5	114	76	85.5	190
2	0	80.75	107.175	87.875	109.25	190
3	0	65.90	93.228	96.781	124.93	190