

## Government Engineering College, Thrissur MA202 - PROBABILITY DISTRIBUTIONS, TRANSFORMS AND NUMERICAL METHODS Assignment Lagrange's Interpolation Formula

Date of Submission

Submitted By
Kowsik Nandagopan D
Roll No 31
TCR18CS031
GECT CSE S4

2] The population of Miscisippi during 1. Interpolate the value of function three census period was es follows Corresponding to x=4 asing Legrange's interpolation formula Interpolate the population during A from the following set of data. 1971 1961 Year 1951  $\times$   $n_0 = 2$   $n_1 = 3$   $n_2 = 5$   $n_3 = 8$   $n_4 = 12$  f(n) 10 15 25 40 60 Population 2.8 3.2 4.5 Solution X 0 22 PD = (n-np) (n-n2) (n-n3) (n-n4) f(no)
(no-n4) (no n2) (no-n3) (nonp) 45 f(n) 2.8 3.2 Be X= 1.5 1966 will  $= \underbrace{(4-3)(4-5)(4-8)(4-12)}_{(2-3)(2-5)(2-8)(2-12)}$ Po: (n-n1)(n-n2) + (no) PI = (n-no)(n-n2)(n-n3)(n-n4)(ny)
(ny-n4)(ny-n4)(ny-n4)  $= \frac{(1.5-1)(1.5-2)}{(0-1)(0-2)} 2.8 = -\frac{7}{20}$ (3-2)(4-5)(4-8)(4-12) 15 (3-2)(3-5)(3-8)(3-12) $P_1 = \frac{(n-n_0)(n-n_1)}{(n_0-n_0)(n_0-n_2)} f(n_0)$  $= \frac{(1.5-0)(1.5-2)}{(1-0)(1-2)} 3.2 = 12$ P3 = (n-no)(n-n1)(n-n3)(n-n4)f(n) (n2-n0) (n2-n1) (n2-n3) (n2-n4)  $P_2 = \frac{(n-n_0)(n-n_1)}{(n_2-n_0)(n_2-n_1)} f(n_2)$  $= \frac{(4-2)(4-8)(4-8)(4-12)}{(5-2)(5-3)(5-8)(5-12)} 25$  $= \frac{(15-0)(15-1)}{(2-0)(2-1)} + 5 = 27$ P3 - (n-no)(n-ny)(n-n2)(n-n4)f(n3) (ng-no) (ng-ny) (ng-nz) (ng-ny) f(2-1.5) = 3.7375 (3-2)(4-3)(4-5)(4-12) 40 Population in 1966 w 3.7375 P4 = (n-20)(n-2)(n-2)(n-2) f(n) ( my-no) (94-94) (74-72) (my mg) (4-2)(4-8)(4-6)(4-8) 60 = 4 (12-2)(12-8)(12-6)(12-8) f(4)= 10+ Fx+Fz+Fz+Fy= 20

Po \* 
$$(n_0 - n_1)(n - n_2)(n - n_3) - ... (n - n_6) f(n_0)$$
  
 $(n_0 - n_1)(n_0 - n_2) - ... (n_0 - n_6)$   
=  $(5 - 2)(5 - 3) - ... (5 - 10)$  2

$$(1-2)(1-3)$$
 ...  $(1-10)$ 

$$P_{1} = (n - n_{0})(n - n_{2}) \qquad (n - n_{0})$$

$$(n_{1} - n_{0})(n_{1} - n_{2}) \qquad (n_{1} - n_{0})^{(n_{0})}$$

$$= (5 - 1)(5 - 3) \qquad (5 - 10)$$

$$(2 - 1)(2 - 3) \qquad (2 - 10)^{2.5}$$

$$= \frac{25}{32}$$

$$P_{2} = \frac{(n-n_{0})(n-n_{0})}{(n_{2}-n_{0})(n_{2}-n_{0})} - \frac{(n-n_{0})}{(n_{2}-n_{0})} + \frac{(n-n_{0})}{(n_{2}-n_{0})}$$

$$= \frac{(5-1)(5-2)}{(3-1)(3-2)} - \frac{(5-10)}{(3-10)} - \frac{(5-10)}{(3-10)}$$

$$(3-1)(3-2) \cdot (3-10)$$

$$(3-1)(3-2) \cdot (3-10)$$

$$(3-10)(3-2) \cdot (3-10)$$

$$P_{3} = (n-n_{0})(n-n_{1}) \cdots (n-n_{6}) + (n_{3})$$

$$(n_{3}-n_{6})(n_{3}-n_{1}) \cdots (n_{3}-n_{6})$$

$$= (5-1)(5-2) \cdots (5-10) + 10.5$$

$$(4-1)(4-2) \cdots (4-10)$$

$$= \frac{10.5}{8}$$

$$P4 = \frac{(n-n_0)(n-n_1) - ... (n-n_6)}{(n_4-n_0)(n_4-n_1) - ... (n_4-n_6)} - f(n_4)$$

$$= \frac{(5-1)(5-2) - ... (5-10)}{(6-1)(6-2) - ... (6-10)} 12.75 = \frac{153}{32}$$

$$P_{1} = (n - n_{0})(n - n_{2})(n - n_{3}) + f(n_{1})$$

$$= (n_{1} - n_{0})(n_{1} - n_{2})(n_{1} - n_{3})$$

$$= (1 \cdot 2 - 0.969)(1 \cdot 2 - 1 \cdot 341)(1 \cdot 2 - 1 \cdot 605)$$

$$= (1 \cdot 090 - 0.969)(1 \cdot 090 - 0.969)(1 \cdot 090 - 1 \cdot 605)$$

= 
$$18.722884$$
 $P_2 = (n-n_0)(n-n_1)(n-n_3) f(n_2)$ 
 $(n_2-n_0)(n_2-n_1)(n_2-n_3)$ 
=  $(1.2-0.969)(1.2-1.090)(1.2-1.605)$ 

$$F_{3} = (n - n_{0})(n - n_{1})(n - n_{2})$$

$$(n_{3} - n_{0})(n_{3} - n_{1})(m_{0} - n_{0})$$

$$= (12 - 0.969)(1.2 - 1.090)(1.2 - 1.341)$$

$$(1605 - 0.969)(1.605 - 1.090)(1.605 - 1.341)$$

$$= -0.621 = 0.8$$

$$f(1.2) = 20.1305107$$

5] Consider the vapor - Liquid equilibrim mole fraction data selow for the binary system of methodol and water at to later

	ne ni	20.5	23	24
×	1 0.880	0.765	0.653	0.548
7	1 0 929	0.849	0.764	0 - 673
-	24	266	227	0,159
X	0-449	0.844	0 · 25	0.159
7	0.575	0.471	0.859	0.241
	ach	210		
k	0.072	0		
4	0-114	0		

Determine the vapor mole fraction of methanol (y) considering corresponding to the liquid mole fraction of methanol of x = 0.15 by lagranges interpolation x = 0.15

$$P_0 = \frac{(x - x_1)(x - x_2)}{(x_0 - x_1)} \dots (x_0 - x_{10}) f(x_0)$$

$$= 5 - 606 \times 10^{-5}$$

$$P_1 = -0.000727$$
 $P_2 = 0.0041946$ 
 $P_3 = -0.0147607$ 
 $P_4 = 0.03547577$ 
 $P_5 = -0.0615777$ 
 $P_6 = 0.0799273$ 

19= 6.0780866 19= 0.2625276 19= 0.06409761 10= 0 1(0.15) = 0.243404 Vapour processive at liquid rate faction 6:16 is 0.242464 atm