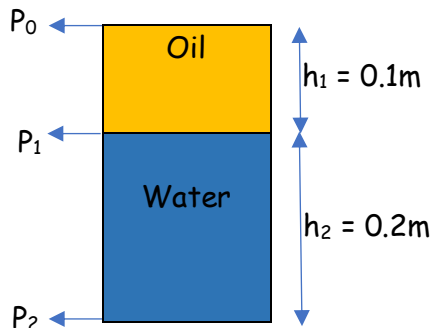


Solution 4.2019:

Problem 1:



$$\text{At the interface: } P_1 = P_0 + \rho_{\text{oil}}gh_1 \quad (1)$$

$$\text{At the bottom: } P_2 = P_1 + \rho_{\text{water}}gh_2 \quad (2)$$

(1) and (2)

$$\Rightarrow P_2 = P_1 + \rho_{\text{water}}gh_2 = P_0 + \rho_{\text{oil}}gh_1 + \rho_{\text{water}}gh_2$$

$$\Rightarrow \text{Gauge Pressure: } P_g = \rho_{\text{oil}}gh_1 + \rho_{\text{water}}gh_2$$

$$\rho_{\text{oil}} = 0.6\rho_{\text{water}} \Rightarrow P_g = (0.6h_1 + h_2) \cdot g \cdot \rho_{\text{water}}$$

$$\Rightarrow P_g = (0.6 \cdot 0.1 + 0.2) \cdot 9.8 \cdot 1000 = 2548 \text{ Pa}$$

Gauge pressure at the bottom is 2548 Pa

Problem 2:

d: diameter

$$d' = d/3 \Rightarrow r' = r/3 \Rightarrow \pi(r')^2 = \pi(r/3)^2 \Rightarrow A' = A/9 \Rightarrow \frac{A}{A'} = 9$$

$$Av = \text{const} \Rightarrow A'v' = Av \Rightarrow v' = \frac{A}{A'} \cdot v = 9v = 9 \cdot 4 = 36 \text{ m/s}$$

Flow speed at this section is 36 m/s

Problem 3:

$$\text{Heat flow rate } P = \frac{kA\Delta T}{L}$$

$$\text{Steady state} \Rightarrow P_1 = P_2 = P_3 = P_4 = P_5 \Rightarrow \frac{k_1 A_1 \Delta T_1}{L_1} = \frac{k_2 A_2 \Delta T_2}{L_2} = \frac{k_3 A_3 \Delta T_3}{L_3} = \frac{k_4 A_4 \Delta T_4}{L_4} = \frac{k_5 A_5 \Delta T_5}{L_5}$$

We have $L_1 = L_2 = L_3 = L_4 = L_5$ and $A_1 = A_2 = A_3 = A_4 = A_5$

$$\Rightarrow k_1 \Delta T_1 = k_2 \Delta T_2 = k_3 \Delta T_3 = k_4 \Delta T_4 = k_5 \Delta T_5 \Rightarrow 6k_1 = 5k_2 = 4k_3 = 7k_4 = 8k_5$$

$$\Rightarrow \text{If we let } k_1 = 1 \Rightarrow k_2 = 1.2; k_3 = 1.5; k_4 = 0.86; k_5 = 0.75 \Rightarrow k_5 \text{ is the smallest.}$$

\Rightarrow Slab 5 has the smallest thermal conductivity.

Problem 4:

Linear expansion from 7.10 m at 20°C to 7.20 m at 90°C :

$$\Delta L = L_0 \alpha \Delta T \Leftrightarrow 7.20 - 7.10 = 7.10 \cdot \alpha \cdot (90 - 20)$$

$$\Rightarrow \alpha = 2 \times 10^{-4} / ^\circ\text{C}$$

Temperature at length 7.05 after linear expansion from 7.10 m at 20°C :

$$\Delta L = L_0 \alpha \Delta T \Leftrightarrow 7.05 - 7.10 = 7.10 \cdot 2 \times 10^{-4} \cdot (T - 20)$$

$$\Rightarrow T \approx -15^\circ\text{C}$$

Temperature at length 7.05 is about -15°C .

Problem 5:

(a) Cyclic process \Rightarrow There is no change in internal energy. $\Rightarrow \Delta U = 0 \text{ J}$

(b) Work is the area within the cycle: $W = \frac{1}{2} \cdot (80 - 20) \cdot (4 - 2) = 60 \text{ J}$

From Figure 2:

Area under the line BC is smaller than area under the line AC $\Rightarrow W_{BC} < W_{CA}$

The gas expands from B to C then compresses from C to A (A to B is isobaric the volume is constant)

Therefore, the gas is compressed in one cycle.

\Rightarrow Net work done by the gas is negative $\Rightarrow W_{\text{done by gas}} = -60 \text{ J}$

(c) We have 2nd law of thermal dynamics: $\Delta U = Q - W$

Q here is heat transferred into the system, W is work done by the system.

From (a) we have $\Delta U = 0 \text{ J}$

From (b) we have W done by gas is -60 J

$\Rightarrow Q = \Delta U + W = 0 - 60 = -60 \text{ J}$.

\Rightarrow Heat transferred into the gas is -60 J. Heat

Therefore, heat transferred out of the gas is 60 J.

Answer 4.2019:

1/ 2548 Pa

2/ 36 m/s

3/ slab 5. Explain: ...

4/ about -15°C

5/ (a) $\Delta U = 0 \text{ J}$ (b) $W_{\text{done by gas}} = -60 \text{ J}$ (c) $Q_{\text{out}} = 60 \text{ J}$