Chemical Reaction Engineering—Homework #3

Due: Online submission on Canvas, <u>Wednesday, February 5, 2020 at 11:59pm.</u>
No late submissions will be accepted.

Problems that require a numeric answer should have 3 significant figures. Units, where required, are shown in blue. Please use these units.

Problem 1: Condensation of product in reactor

MN Chemicals desires to run the following gas phase reaction in an isothermal, isobaric (25 deg C, 101 kPa) reactor:

$$A(g) + 2B(g) \rightarrow C(g, 1) + D(g)$$

It is determined that the rate law can be expressed as first order in both reactants. The saturation mole fraction of C in the gas phase is 0.25. Assume that A and B are fed at a stoichiometric ratio and the total volumetric flow rate is $1.5 \, \text{L/min}$. The rate constant is $0.035 \, \text{L/(mol*s)}$. Assume that all gaseous species behave as ideal gases.

- a. Is this an elementary reaction/step?
- b. Write out the stoichiometric table in terms of X_A and F_{A0} for all species.
- c. What is the vapor pressure of C? At what conversion of A does condensation of C begin? [25 kPa, 0.6]
- d. Write $(-r_A)$ both before and after condensation as a function of conversion, the rate constant, and the initial concentration of A.
- e. What volume of CSTR is required if you desire a conversion of 90% of A? [670L]

Problem 2: Production of cumene

You are going to produce cumene from propylene and benzene using the elementary, reversible gas phase reaction:

$$C_3H_6 + C_6H_6 \Leftrightarrow C_9H_{12}$$

which as forward and reverse rate constants of k_f and k_r , respectively. The research scientists at MN Chemicals have collected the following kinetic and equilibrium data for this reaction.

T(deg C) k_f (mol min ⁻¹ L ⁻¹ atm ⁻²) K_{eq} (atm ⁻¹)

30	1.75 (10 ⁻⁷)	9.09 (10²)
80	9.01 (10 ⁻⁵)	26.3
130	9.83 (10 ⁻³)	1.83
180	3.81 (10-1)	2.30 (10-1)
230	7.13	4.36 (10-2)

a. What is the activation energy and pre-exponential factor for the forward rate constant? What is the heat of reaction? [A = $2(10^{12})$, E_A = 110 kJ/mol, H_{rxn} = -63 kJ/mol]

You are synthesizing cumene using a PFR with a volume of 150L. The reactants are fed into the isothermal, isobaric reactor with a molar flow rate of 14.4 mol/min at a propylene: benzene molar ratio of 2:1 and a total volumetric flow rate of 100 L/min. Hint: Use the partial pressures of the gases instead of the molar concentrations in your rate expressions.

- b. What conversion do you achieve if the reactor is operated at 100°C? [0.1]
- c. What conversion do you achieve if the reactor is operated at 150°C? [0.68]
- d. Determine the equilibrium conversions at 100° C and 150° C as a function of concentrations of various species? [at 100° C, X = 0.95; at 150° C, X = 0.68]

Problem 3: Gas phase batch reactor

A second order gas phase reaction, $A \rightarrow 3B$ occurs in an isothermal batch reactor. The volume of the reactor is 10L. Initially the reactor as 50 mol of gas with 50% A and 50% inert gas. The rate constant is 0.45 s⁻¹ M⁻¹. Assume ideal gas behavior in the reactor. Calculate the conversion for this reaction after 1 minute if the reactor is operated isobarically. [0.97]

Problem 4: Equilibrium conversions

The reversible reaction $2A \Leftrightarrow B$ is carried out in a flow reactor where pure A is fed at a concentration of 4 mol/L. The equilibrium conversion is found to be 60%. Assume that the reactor is isothermal and isobaric.

- a. What is the equilibrium constant, K_C , if the reaction is a gas phase reaction? [0.33]
- b. What is K_C if it is a liquid phase reaction? [0.47]

The gas phase reaction A \Leftrightarrow 3C is carried out in a flow reactor with no pressure drop. Pure A enters at a temperature of 400K and a pressure of 10 atm. At this temperature, $K_C = 0.25 \text{ M}^2$.

- c. What is the equilibrium conversion if the reaction is carried out in a constant volume batch reactor? Assume isothermal operation. [0.4]
- d. What is the equilibrium conversion if the reaction is carried out in a constant pressure batch reactor? Assume isothermal operation. [0.6]