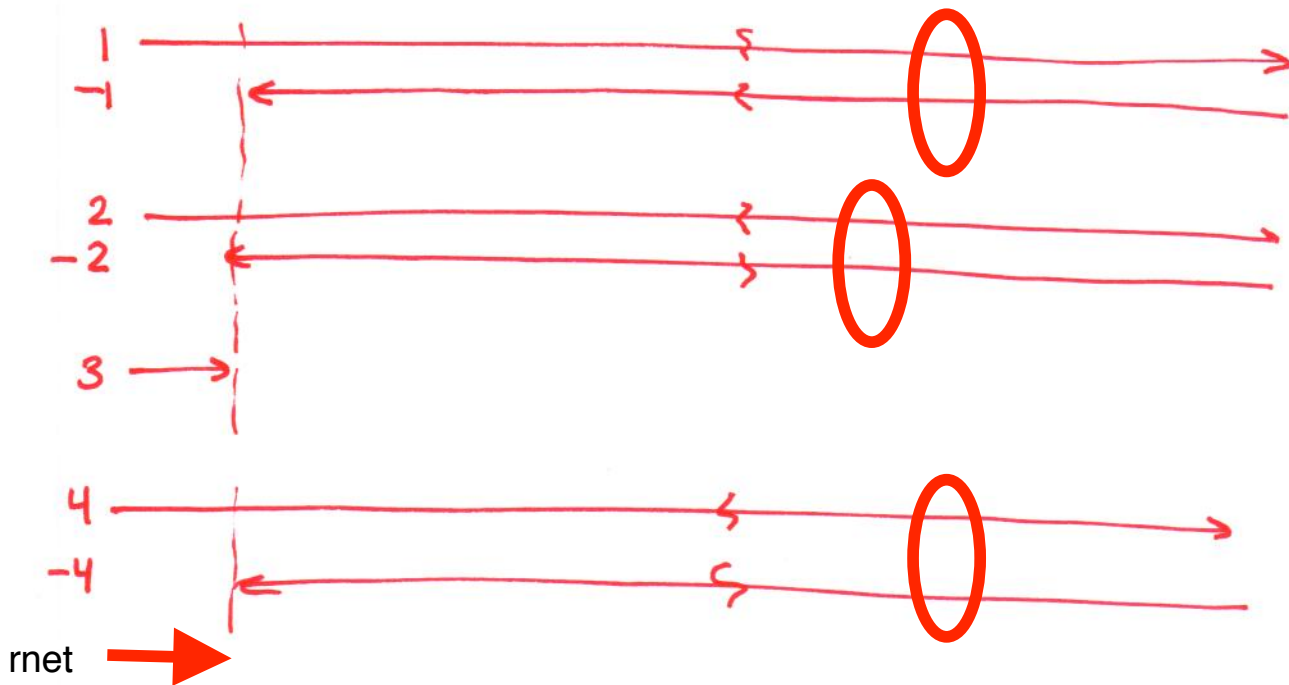


a.

Step



$$b. \quad r = r_3 = \frac{k_r (D^*) (W^*)}{C_T}$$

$$(D^*) = K_D (D) (*)$$

$$(W^*) = K_W (W) (*)$$

$$r = \frac{k_r K_D K_W (D) (W) (*)^2}{C_T}$$

$$C_T = (*) + (D^*) + (W^*) + (C^*)$$

$$C^* = \frac{(C) (*)}{K_C}$$

$$C_T = (*) + (D^*) + (W^*) + \frac{(C) (*)}{K_C}$$

$$C_T = (*) + K_D (D) (*) + K_W (W) (*) + \frac{(C) (*)}{K_C}$$

$$(*) = \frac{C_T}{1 + K_D(D) + K_W(W) + \frac{(C)}{K_C}}$$

$$r = \frac{k_r K_D K_W (D)(W) C_T}{\left(1 + K_D(D) + K_W(W) + \frac{(C)}{K_C}\right)^2}$$

c. If  $(*)$  is MASI  $C_T = (*)$

$$r = k_r K_D K_W (D)(W) C_T$$

d.  $\psi = \frac{C_A}{C_{AS}} = \frac{1}{\lambda} \left( \frac{\sinh \phi_1 \lambda}{\sinh \phi_1} \right)$

$$0.1 = \frac{1}{0.8} \left( \frac{\sinh[\phi_1 (0.8)]}{\sinh \phi_1} \right)$$

Solve for  $\phi_1$

$$\phi_1 = 12.6$$

$$\eta_1 = \frac{3}{\phi_1^2} (\phi_1 - 1) = 0.22$$

e. PFR DESIGN EQN.

$$F_{D0} \frac{dX}{dV} = -r_A = k(D)$$

$$(D)_0 v \frac{dX}{dV} = \frac{k(D)_0(1-X)}{1+\varepsilon X}$$

$$\varepsilon = \delta y_{D0} = (1+0.2-1)(1) = 0.2$$

$$v \left( \frac{dX}{dV} \right) = \frac{k(1-X)}{1+0.2X}$$

$$\int \frac{(1+0.2X)dX}{1-X} = \frac{k}{v} \int dV$$

$$\int \frac{(1+0.2X)dX}{1-X} = k\tau$$

$$\int_0^{0.6} \frac{(1+0.2X)dX}{1-X} = k\tau$$

$$0.98 = \frac{0.10}{s} \tau$$

$$\tau = 9.8s$$

$$\tau = \frac{V}{v} = 9.8s \quad v = 49L$$

f. This conversion is the same as with the segregation model, as mixing is not important in 1st order reaction

g.

$$K = \frac{(C)(CO)^{0.2}}{(D)}$$

$$(D) = \frac{(D)_0 (1-X)}{1 + 0.2X}$$

$$(C) = \frac{(D)_0 X}{1 + 0.2X}$$

$$(CO) = \frac{(D)_0 (0.2X)}{1 + 0.2X}$$

$$(D)_0 = \frac{1.01 \text{ E } 6 \text{ Pa}}{8.31 \frac{\text{J}}{\text{mol K}} (700 \text{ K})} = 173 \frac{\text{mol}}{\text{m}^3}$$

$$= 0.173 \frac{\text{mol}}{\text{L}}$$

$$8 = \frac{\left[ \frac{(D)_0 X}{1 + 0.2X} \right] \left[ \frac{(D)_0 (0.2X)}{1 + 0.2X} \right]^{0.2}}{\frac{(D)_0 (1-X)}{1 + 0.2X}}$$

Solve for X

$$X = 0.94$$

h.

$$Q = -(\Delta H_R) F_{D0} X_D$$

$$Q = -(-5000 \text{ J/mol}) (0.173 \frac{\text{mol}}{\text{L}}) (5 \frac{\text{L}}{\text{s}}) (0.6)$$

$$\boxed{Q = 2.60 \text{ kW}}$$

or 4.07 kW if  $X = 0.94$ 

i.

$$F_{D0} \frac{dX}{dV} = -r_A = k(D)$$

$$(D) = \frac{(D)_0 (1-X)}{1 + 0.2X} \frac{T_0}{T}$$

$$T = \frac{X(-\Delta H_R) + \sum \Theta_i c_{pi} T_0 + X \Delta c_p T_R}{\sum \Theta_i c_{pi} + X \Delta c_p}$$

$$\Delta c_p = 0.2 c_p$$

$$T = \frac{X(-\Delta H_R) + c_p T_0 + 0.2 c_p X T_R}{c_p + X(0.2 c_p)}$$

$$k = k(T_0) \exp \left[ \frac{E}{R} \left( \frac{1}{T_0} - \frac{1}{T} \right) \right]$$

Substitute  $T$  INTO EQNS FOR  $k + (D)$ 

$$\frac{dX}{dV} = \frac{k(D)}{F_{D0}}$$



INTEGRATE FROM  $V=0$  TO  $49L$   
USING COMPUTATIONAL SOFTWARE.

WHEN  $V = 49L$        $X = 0.596$        $T = 776K$

WHEN  $X = 0.75$        $V = 76.8L$

j. 
$$0.2 = \frac{F_C}{F_C + F_D + F_{CO}} = \frac{F_{D0} X}{F_{D0} X + F_{D0} (1-X) + 0.2 F_{D0} X_D}$$

$$\boxed{X = 0.208}$$