

PROBLEM #1MOLE BALANCE ON A

$$\frac{dN_A}{dt} = F_{A0} - F_A + r_A V$$

$$\frac{d(c_A V)}{dt} = C_{A0} v_0 - C_A v_0 (1.5) + r_A V$$

$$-r_A = k_1 C_A^2$$

$$V \frac{dc_A}{dt} + C_A \frac{dV}{dt} = C_{A0} v_0 - 1.5 C_{A0} v_0 + r_A V$$

$$\frac{dV}{dt} = v_0 - 1.5 v_0 = -0.5 v_0$$

$$V \frac{dc_A}{dt} - 0.5 v_0 C_A = C_{A0} v_0 - 1.5 C_{A0} v_0 - k_1 C_A^2 V$$

$$\frac{dc_A}{dt} = \frac{C_{A0} v_0}{V_i - 0.5 v_0 t} - \frac{v_0 C_A}{V_i - 0.5 v_0 t} - k_1 C_A^2$$

MOLE BALANCE ON P

$$\frac{dc_P V}{dt} = 0 - c_P (1.5 v_0) + r_P V$$

$$2r_P = -r_A$$

$$V \frac{dc_p}{dt} + c_p(-0.5v_0) = -c_p(1.5v_0) + 2k_1 c_A^2 V$$

$$\frac{dc_p}{dt} = \frac{-c_p v_0}{V_i + v_0(-0.5)t} + 2k_1 c_A^2$$

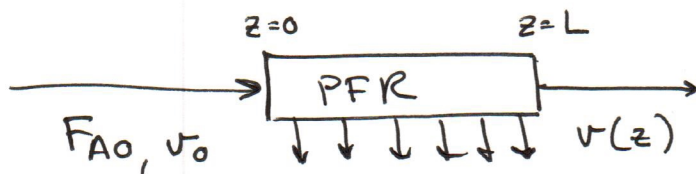
$$\frac{dc_p}{dt} = 2k_1 c_A^2 - \frac{v_0 c_p}{V_i - 0.5v_0 t}$$

INTEGRATE USING AN ODE SOLVER.

$$N_p = \int c_p(t) dt \cdot v_{out}$$

$$N_p = 10.55 \text{ mol}$$

PROBLEM #2



a. $F_{A, \text{LEAK}}|_z = C_A|_z (-v|_{z, \text{LEAK}})$

$$v|_{z, \text{LEAK}} = \frac{dv}{dz} \Delta z$$

$$F_{A, \text{LEAK}}|_z = -C_A|_z \left(\frac{dv}{dz} \Delta z \right)$$

b. $\text{IN} - \text{OUT} + \text{GEN} = \text{ACCUM.} = 0$

$$F_A|_z - (F_A|_{z+\Delta z} + F_{A, \text{LEAK}}|_z) + (-kC_A)A_c \Delta z = 0$$

$$F_A|_z - F_A|_{z+\Delta z} + C_A|_z \left(\frac{dv}{dz} \right) \Delta z = kC_A A_c \Delta z$$

c. $\text{DIVIDE BY } \Delta z$

$$\frac{-(F_A|_{z+\Delta z} - F_A|_z)}{\Delta z} + C_A \frac{dv}{dz} = kC_A A_c$$

TAKE LIMIT AS $\Delta z \rightarrow 0$

$$-\frac{dF_A}{dz} + C_A \frac{dv}{dz} = kC_A A_c$$

$$F_A = F_{A0}(1-X)$$

$$-\frac{d(F_{A0}(1-X))}{dz} + C_A \frac{dv}{dz} = kC_A A_c$$

$$F_{A0} \frac{dX}{dz} + C_A \frac{dv}{dz} = k C_A A_c$$

d. $\frac{dv}{dz} = \frac{-v_0}{L}$

$$-\frac{dF_A}{dz} - C_A \frac{v_0}{L} = k C_A A_c$$

PUT FLOW RATES & CONCENTRATIONS IN TERMS OF CONVERSIONS

$$F_A = F_{A0}(1-X) \quad C_A = \frac{F_{A0}(1-X)}{v(z)}$$

$$\cancel{F_{A0}} \frac{dX}{dz} - \frac{\cancel{F_{A0}}(1-X)}{v(z)} \frac{v_0}{L} = \frac{\cancel{k} \cancel{F_{A0}}(1-X)}{v(z)} A_c$$

$$\frac{dX}{dz} = \frac{(1-X)v_0}{v_0(1-z/L)} \frac{1}{L} = \frac{k(1-X)}{v_0(1-z/L)} A_c$$

$$\frac{dX}{dz} = \frac{(1-X)}{1-z/L} \left[\frac{k A_c}{v_0} + \frac{1}{L} \right]$$

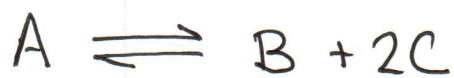
$$e. \int_0^x \frac{dx}{1-x} = \left[\frac{kAc}{v_0} + \frac{1}{L} \right] \int_0^z \frac{dz}{1-z/L}$$

$$-\ln(1-x)|_0^x = \left[\frac{kAc}{v_0} + \frac{1}{L} \right] \left[-L \ln\left(1 - \frac{z}{L}\right) \Big|_0^z \right]$$

$$\ln(1-x) = \left(\frac{LkAc}{v_0} + 1 \right) \ln\left(1 - \frac{z}{L}\right)$$

$$X = 1 - \left(1 - \frac{z}{L}\right)^{\frac{LkAc}{v_0} + 1}$$

PROBLEM #3



$$\frac{dF_A}{dV} = r_A - R_A = \frac{dF_A}{dz} \left(\frac{1}{A} \right)$$

$$\frac{dF_B}{dV} = r_B - R_B = \frac{dF_B}{dz} \left(\frac{1}{A} \right)$$

$$\frac{dF_C}{dV} = r_C = \frac{dF_C}{dz} \left(\frac{1}{A} \right)$$

IF SYSTEM IS ISOTHERMAL + ISOBARIC, THEN $C_{T0} = C_T$

$$\begin{aligned} -r_A &= k_1 \left(C_A - \frac{C_B C_C^2}{K_C} \right) = k_1 \left(\frac{C_{T0} F_A}{F_T} - \left(\frac{C_{T0}}{F_T} \right)^3 \left(\frac{F_B F_C^2}{K_C} \right) \right) \\ &= r_B = \frac{1}{2} r_C \end{aligned}$$

$$R_A = \frac{\beta_A F_A C_{T0}}{F_T}$$

$$R_B = \beta_B C_B = \frac{\beta_B F_B C_{T0}}{F_T}$$

$$\begin{aligned} \frac{dF_A}{dz} &= A (r_A - R_A) = -A \left[k_1 \left(\frac{C_{T0} F_A}{F_T} - \left(\frac{C_{T0}}{F_T} \right)^3 \left(\frac{F_B F_C^2}{K_C} \right) \right) \right. \\ &\quad \left. + \frac{\beta_A F_A C_{T0}}{F_T} \right] \end{aligned}$$

$$\frac{dF_B}{dz} = A \left[k_1 \left(\frac{C_{T0} F_A}{F_T} - \left(\frac{C_{T0}}{F_T} \right)^3 \left(\frac{F_B F_C^2}{K_C} \right) \right) - \frac{\beta_B F_B C_{T0}}{F_T} \right]$$

$$\frac{dF_C}{dz} = 2A k_1 \left(\frac{C_{T0} F_A}{F_T} - \left(\frac{C_{T0}}{F_T} \right)^3 \left(\frac{F_B F_C^2}{K_C} \right) \right)$$

In [3]:

```
from scipy.integrate import odeint
import numpy as np
import matplotlib.pyplot as plt

def myode(F,z):
    A = 2
    k1 = 10
    C_T0 = 1
    Kc = 0.01
    BetaA = 1
    BetaB = 40

    FA = F[0]
    FB = F[1]
    FC = F[2]

    rA = k1*(((C_T0*FA)/(FA+FB+FC))-((C_T0**3/((FA+FB+FC)**3))*(FB*FC**2/Kc)))
    RA = BetaA * FA * C_T0/(FA+FB+FC)
    RB = BetaB * FB * C_T0/(FA+FB+FC)

    dFAdz = -A * (rA+RA)
    dFBdz = A * (rA-RB)
    dFCdz = 2*A*rA

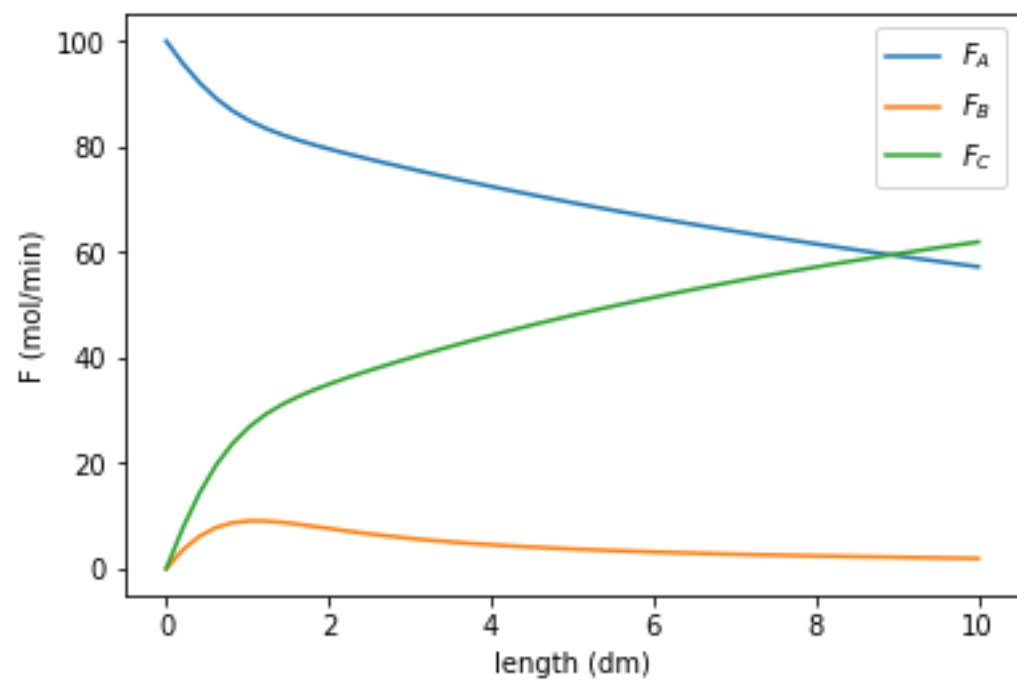
    dFdz= [dFAdz,dFBdz,dFCdz]
    return dFdz

zspan = np.linspace(0,10)

init = [100,0,0]
F = odeint(myode,init,zspan)

FA = F[:,0]
FB = F[:,1]
FC = F[:,2]

plt.plot(zspan, FA, zspan, FB, zspan, FC)
plt.xlabel('length (dm)')
plt.ylabel('F (mol/min)')
plt.legend(['$F_A$', '$F_B$', '$F_C$'])
plt.savefig('membrane.png')
```

PROBLEM #4

a. MOLE BALANCE ON "A" (NO_2)

$$\text{IN} - \text{out} + \text{gen} = \text{acc.}$$

$$F_{A0} - F_A + r_A V = 0$$

$$-r_A = \frac{F_{A0} X_A}{V}$$

b. ASSUME POWER LAW FORM OF RATE LAW

$$-r_A = k C_A^\alpha$$

$$k C_A^\alpha = \frac{F_{A0} X_A}{V}$$

$$X_A = \frac{\text{fractional decomp. of } \text{NO}_2}{100\%}$$

$$X_A = k C_A^\alpha \left(\frac{V}{F_{A0}} \right)$$

WHEN PLOTTING X_A VS. $\frac{V}{F_{A0}}$, $k C_A^\alpha$ IS THE SLOPE. AT 200°C , THE SLOPE IS THE SAME FOR ALL CONCENTRATIONS TESTED.

THE REACTION ORDER IS EQUAL TO 0.

$$c. k = A \exp\left(\frac{-E_A}{RT}\right) \Rightarrow \ln k = \ln A + \left(\frac{-E_A}{RT}\right) \left(\frac{1}{T}\right)$$

$$\text{At } 200^\circ\text{C} \quad k = \frac{X_A}{\frac{V}{F_{A0}}} \approx \frac{0.5}{4 \frac{\text{m}^3 \text{ h}}{\text{mol NO}_2}} = 0.125 \frac{\text{mol NO}_2}{\text{m}^3 \text{ h}}$$

$$\text{At } 250^{\circ}\text{C} \quad k \approx \frac{0.5}{2 \frac{\text{m}^3 \text{h}}{\text{mol NO}_2}} = 0.25 \frac{\text{mol NO}_2}{\text{m}^3 \text{h}}$$

$$\text{At } 300^{\circ}\text{C} \quad k \approx \frac{0.6}{1 \frac{\text{m}^3 \text{h}}{\text{mol NO}_2}} = 0.6 \frac{\text{mol NO}_2}{\text{m}^3 \text{h}}$$

Plot $\ln(k)$ vs. $\frac{1}{T}$

$$\text{Slope} = -4223$$

$$E_A = -4223 \left(8.314 \frac{\text{J}}{\text{mol K}} \right) = 35 \frac{\text{kJ}}{\text{mol K}}$$