

BENCHMARK SYSTEMS FOR PID CONTROL

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Abstract This paper describes a collection of systems that are suitable for testing PID controllers. The systems are collected from a wide range of sources.
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INTRODUCTION

When evaluating PID controllers it is of interest to have a batch of test examples so that different schemes can be evaluated. Over the years we have collected a large number of test examples which we have used for research and for evaluation of commercial systems. This paper describes a collection of systems that we have found useful. The material is based on many different sources. The systems 1-5 are standard systems that are well suited to parametric studies. Their properties can easily be changed by varying a parameter. The systems 6-10 are more specialized. They illustrate systems with various difficulties of control. PID control is not well suited for all of them. Parameters for PID controllers for many of these systems are found in (Åström and Hägglund (1995)), (Åström *et al.* (1998)) (Panagopoulos *et al.* (1999)).

1. MULTIPLE EQUAL POLES

Transfer function

$$G(s) = \frac{1}{(s+1)^n} \quad n = 1, 2, 3, 4, 8 \quad (1)$$

These systems are very common. For $n = 1$ and 2 anything can be achieved by PI or PID control respectively. For large values of n the system behaves like systems with long dead times. The systems have been used by controller manufacturers as test cases for a long time. We have obtained this information from Eurotherm and Foxboro.

2. FOURTH ORDER SYSTEM

Transfer function

$$G(s) = \frac{1}{(s+1)(1+\alpha s)(1+\alpha^2 s)(1+\alpha^3 s)} \quad (2)$$

$$\alpha = 0.1, 0.2, 0.5, 1.0$$

This system has four poles whose spacing is determined by parameter α . For small values there are drastic improvements when going from PI to PID control. For $\alpha = 1$ the system is identical to the system (1) for $n=4$.

3. RIGHT HALF PLANE ZERO

Transfer function

$$G(s) = \frac{1-\alpha s}{(s+1)^3} \quad (3)$$

$$\alpha = 0.1, 0.2, 0.5, 1, 2, 5$$

This system has three equal poles and a right half plane zero. The achievable performance is determined by parameter α . The difficulty of control increases with increasing α .

4. TIME DELAY AND LAG

Transfer function

$$G(s) = \frac{1}{1+sT} e^{-s} \quad (4)$$

$$T = 0, 0.1, 0.2, 0.5, 2, 5, 10$$

This is the classic system which has been used in many investigations of PID control. The

system reduces to a pure time delay for $T = 0$ and represents lag dominated systems for large T . Many of the early tuning rules were derived based on this model. A drawback with the model is that it has slow roll-off at high frequencies.

5. TIME DELAY AND DOUBLE LAG

Transfer function

$$G(s) = \frac{1}{(1 + sT)^2} e^{-s} \quad (5)$$

$T = 0, 0.1, 0.2, 0.5, 2, 5, 10$

This system is similar to (4) but it has more high frequency roll off. The system reduces to a pure time delay for $T = 0$.

6. HEAT CONDUCTION

Transfer function

$$G(s) = e^{-\sqrt{s}} \quad (6)$$

This system represents the dynamics of one dimensional heat conduction. The ultimate gain is $k_u = e^\pi$. Analog implementations of this system has been used by Eurotherm to test temperature controllers. Other common industrial examples are heat exchangers.

7. FAST AND SLOW MODES

Transfer function

$$G(s) = \frac{100}{(s + 10)^2} \left(\frac{1}{s + 1} + \frac{0.5}{s + 0.05} \right) \quad (7)$$

The essential dynamics of this system has a fast mode with time constant 1 and moderate gain (1) and a slow pole with time constant 20 and a large gain (10). Simple tuning rules based on the step response do normally not give good tuning for systems of this type because it is difficult to get a good estimate of the gain and the time constant.

8. CONDITIONALLY STABLE SYSTEM

Transfer function

$$G(s) = \frac{(s + 6)^2}{s(s + 1)^2(s + 36)} \quad (8)$$

This system is conditionally stable. The stability region under PI control consists of two disjoint sets.

9. OSCILLATORY SYSTEM

Transfer function

$$G(s) = \frac{\omega_0^2}{(s + 1)(s^2 + 2\zeta\omega_0s + \omega_0^2)}, \quad (9)$$

$\zeta = 0.1, \quad \omega_0 = 1, 2, 5, 10.$

Systems of this type with small damping ζ are not good candidates for PID control. The system is easy to control if ω_0 is large. The performance can often be improved drastically by more general controller structures.

10. UNSTABLE POLE

Transfer function

$$G(s) = \frac{1}{s^2 - 1} \quad (10)$$

This is a simple model of an inverted pendulum. An unstable batch reactors is an example from industry. Notice that particular care must be taken with saturating actuators in this case.

11. SYSTEMS WITH INTEGRAL ACTION

It is very useful to also have systems with integral action. A good collection is obtained by adding an integrator to the systems 1-5.

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